



 Cite this: *RSC Adv.*, 2020, 10, 20009

Surface modification of biomaterials based on cocoa shell with improved nitrate and Cr(vi) removal†

 P. Nkuigue Fotsing,^{*a} E. Djoufac Woumfo,^a S. Mezghich,^b M. Mignot,^b N. Mofaddel,^b F. Le Derf^b and J. Vieillard^b 

The present work addresses the development of simple, low-cost and eco-friendly cocoa-shell-based materials for efficient removal of heavy metal hexavalent chromium (Cr(vi)), and toxic nitrate (NO₃⁻) from aqueous solution. A conventional treatment process was used to purify cocoa shell (CS) into an adsorbent, followed by chemical grafting of dendrimers to promote its surface properties for nitrate and Cr(vi) removal. The morphology, surface charge, structure and stability of the new adsorbent were investigated by scanning electron microscopy, Fourier transform infrared and UV-visible spectroscopies, zeta potential, X-ray photoelectron spectrometry, and differential scanning calorimetry. The successful chemical grafting of the dendrimer (polyethyleneimine, PEI) onto purified CS was confirmed. CS-T-PEI-P proved to be a very efficient candidate for the removal of nitrate and chromium(vi). Removal of the two pollutants at different initial concentrations and pH values was studied and discussed. Sorption of chromium and nitrate was found to obey 2nd-order kinetics and a Freundlich-type isotherm, affording an uptake adsorption of 16.92 mg g⁻¹ for NO₃⁻ and 24.78 mg g⁻¹ for Cr(vi). These results open promising prospects for its potential applications as a low cost catalyst in wastewater treatment.

 Received 3rd April 2020
 Accepted 20th May 2020

DOI: 10.1039/d0ra03027a

rsc.li/rsc-advances

1. Introduction

Widespread industrial activities and urbanization have increased the critical problem of the availability of drinkable water, and resulted in dangerous pollution of the surficial drinking water resources.¹ Numerous pollutants such as dyes, pharmaceuticals, phenolic molecules and heavy metals in the water supplies are hazardous, can have carcinogenic effects, and can cause several symptoms such as acute diarrhea, skin irritation, or severe headaches.^{2,3} Particularly, nitrate and heavy metal are considered as carcinogenic and very toxic pollutants that can cause cancer of the digestive tract, nephritis and gastrointestinal ulceration.⁴

Despite the interesting role of nitrogen (N) for living organisms, organic nitrogen such as nitrate (NO₃⁻), include a threat to the ecosystems and public health, due to its high concentrations contributing to eutrophication and various diseases, such as infant methemoglobinemia [2]. The same danger, even more can be caused by the metal iron based on hexavalent chromium (Cr(vi)), considering its easily absorption by the body

and to invade the human organs through the digestive, respiratory, and mucous membrane.

This is why a special, urgently interest could be devoted to adopt efficient technologies to remove both Cr(vi) and (NO₃⁻) from contaminated water, including low-pressure membrane filtration, ion exchange, chemical precipitation, reverse osmosis, and biological treatment.⁵

Recently, water treatments have involved so far numerous technologies including both physical and chemical processes like reverse osmosis, chemical reduction with iron nanoparticles, the adsorption and biological denitrification.^{6,7}

Most of these methods show practical limitations in the removal of nitrate and Cr(vi), especially, the poor stability of membrane filtration has limited its application in industry. Unlike the high operating costs, ion exchange and reverse osmosis are not economically attractive because of their high operating costs.^{8,9} Compared to these remediation techniques, adsorption and advanced oxidation techniques are simple, cheap and effective technologies.^{4,10-13} Therefore, there is an increasing demand for preparing new adsorbents with surface functional groups and high adsorption capacity. Adsorption is considered as the most promising procedure for the removal of heavy metal ions because it is simple and cost-effective. This is why, recently, a special interest was devoted to develop an ecofriendly materials with enhanced adsorption properties.¹⁴⁻¹⁶

Regarding to its poor economic feasibility, limited applicability and effectiveness, and a short lifetime often linked to low

^aLaboratory of Applied Inorganic Chemistry, Faculty of Sciences, University of Yaoundé I, P.O. Box 812, Yaoundé, Cameroon. E-mail: fotsing_p@yahoo.fr

^bNormandie Univ., UNIROUEN, INSA Rouen, CNRS, COBRA (UMR 6014), 55, rue Saint Germain, 27000 Evreux, France

† Electronic supplementary information (ESI) available. See DOI: 10.1039/d0ra03027a



and expensive regeneration capacities, the adsorbents are considered a good candidate for removing both (NO_3^-) and $\text{Cr}(\text{vi})$ from water.

Among the wide variety of materials used or investigated for adsorption of (NO_3^-) and $\text{Cr}(\text{vi})$, activated carbon, metal oxide, graphene oxide, zeolites and fibrous materials are of great interest for some environmental purposes. An interesting alternative consists in using biomass which has a natural composition, low costs and ecofriendly. Particularly, biomass-based adsorbents, are used for sustainable applications to attenuate the impacts of wastewater treatments.

The cocoa industry generates a large amount of waste byproduct each year. Cocoa-shell (CS) as biomass has recently been considered as an adsorbent of interest for a variety of environmental applications and drawn the researchers' attention for heavy metal removal from wastewater. Reportedly, CS as a raw biomass material have already been found to exhibit adsorptive properties toward gas.

Innovative technologies have led to major developments in preparing, for instance, functional biomass as adsorbent with easy-care properties, stability and low toxicity.

Up to now, García, J. C. *et al.* demonstrated that dilute alkali can damage the structure of cellulose, hemicelluloses, and lignin in wheat straw.¹⁷ Wu, M. examined the effects of various modification methods on wheat straw biadsorbents *via* microwave-assisted alkalization and microwave-assisted acid oxidation.¹⁸ Huang, Y. *et al.* studied the chemically activation of dewaxed cornstalk by nitrilotriacetic acid anhydride.¹⁹ In other works, dendrimer-based hyper-branched polymers, and chitosan are employed to provide useful information on the state of adsorbents and on how they enhance the surface properties of the materials.²⁰ Polymer grafted-biomass has been investigated as a suitable technique to upgrade the physicochemical properties of such types of CS minerals.²¹ In addition, such a study can also enrich the knowledge of the adsorption process for environmental remediation. Reports about the use of CS as a support for such applications are scarce, and information about the structure of the different CS supported dendrimers are scarce too. One of the commonly studied polymers integrated with biomass into a composite is chitosan. The compositing process results in a hybrid material of enhanced textural and adsorption properties for effective decontaminations of organic and inorganic pollutants.^{22–24}

This paper reports a simple, low-cost and environment-friendly protocol for the preparation and functionalization of cocoa-shell-based biomass using conventional physical treatments and chemical grafting of dendrimers. The purpose of this work was to investigate the surface properties and discuss in detail the application of such materials for heavy metal (hexavalent chromium) and nitrate removal from aqueous solution. The structure and morphology of synthesized materials were studied by UV-Vis spectroscopy, Fourier transform infrared spectroscopy, field emission scanning electron microscopy, zeta potential and X-ray photoelectron spectroscopy. The effect of the adsorbent concentration, pH and time were investigated to postulate a mechanism.

2. Material and methods

2.1. Chemicals

Potassium dichromate ($\text{K}_2\text{Cr}_2\text{O}_7$, 99%), potassium nitrate (KNO_3 , 99%), sulfuric acid (95%), absolute ethanol (EtOH, 99%) methanol (MeOH, 99%), 1,5-diphenylcarbazide ($\text{C}_{13}\text{H}_{14}\text{N}_4\text{O}$, 98%), branched polyethyleneimine (PEI, average M_w of 25 000), potassium chloride (99%), hydrochloric acid (37%), acetic acid (CH_3COOH , 96%), sodium hydroxide (98%), ethylenediaminetetraacetic acid disodium salt ($\text{C}_{10}\text{H}_{14}\text{N}_2\text{Na}_2\text{O}_8, 2\text{H}_2\text{O}$, 99%), sodium nitrate (NaNO_3 , 99%), salicylic acid ($\text{C}_7\text{H}_5\text{NaO}_3$, 99%), and sodium azide (NaN_3 , 99.5%) were purchased from Merck (France) and used as supplied. All the solutions were prepared using double distilled water (Milli Q, Merck, Millipore).

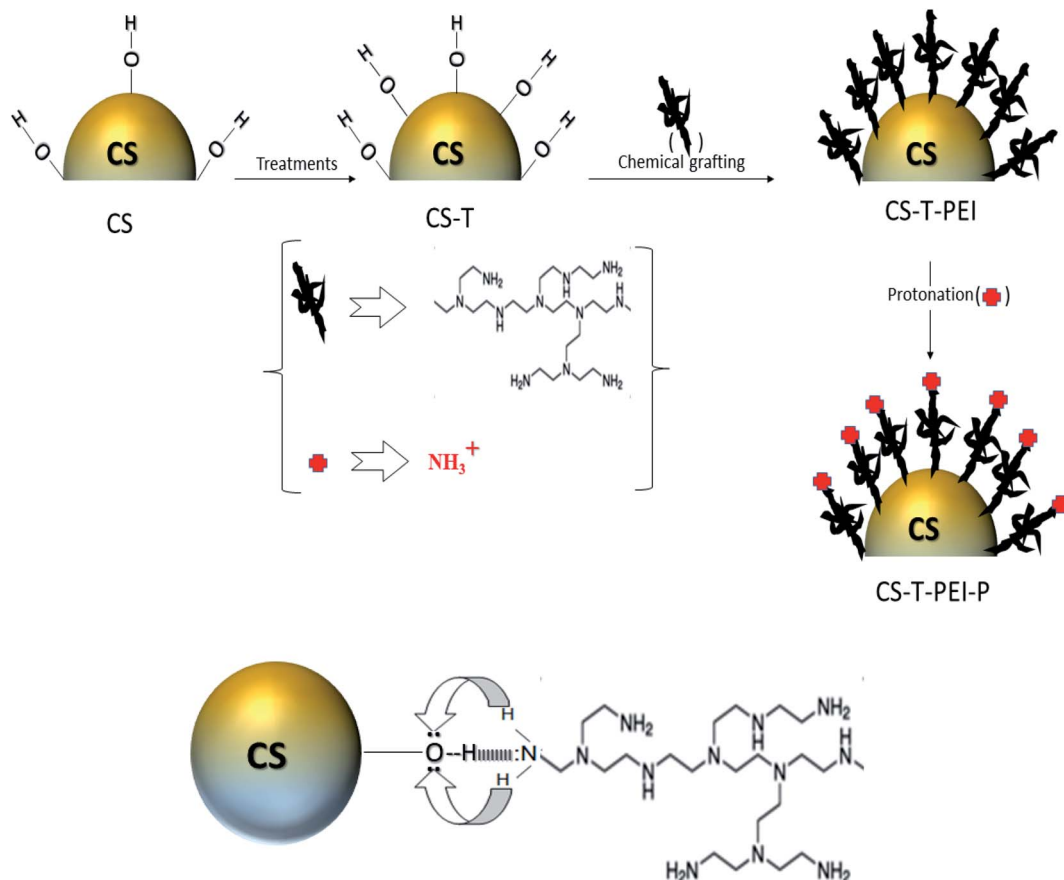
2.2. Cocoa cortex preparation and functionalization

The functional CS-T-PEI-P materials were synthesized as follows (Scheme 1). Firstly, cocoa-shell (CS) was collected from a local farm managed by the IRAD (Institute of Agricultural Research for Development) at Yaoundé, Cameroon. Cocoa shell was cut, washed with acidic water (HCl, 1 M) to remove organic matter, sun-dried for 5 days, and then heated at 70 °C overnight to remove moisture. Finally, it was ground and sifted at 160 μm and the resulting treated CS was named CS-T. Secondly, CS-T was modified with branched polyethyleneimine (PEI) by the impregnation method using the procedure described by Xu *et al.*^{25,26} Briefly, 30% of PEI was dissolved in 70 mL of methanol for 15 min. Then, the desired amount of CS-T was added to the solution. The slurry was continuously stirred for 3 hours at 23 °C. The PEI-modified adsorbent was filtered, washed several times using distilled water and then the resulting CS-T-PEI was dried at 50 °C overnight. Finally, CS-T-PEI (10 g L^{-1}) was acidified using HCl (0.5 M) solution for 2 h at 23 °C to protonate the amino groups leading to positively charged ammonium moieties.^{27,28} The protonated material, designated as CS-T-PEI-P was recovered by filtration, washed several times with distilled water and dried at 50 °C overnight.

2.3. Material characterization

The physicochemical properties of CS-T, CS-T-PEI and CS-T-PEI-P were characterized by scanning electron microscopy (SEM), Fourier transform infrared (FTIR) analysis, and differential scanning calorimetry (DSC). SEM micrographs of the samples were obtained using a ZEISS EVO 15 electron microscope after metallization of different samples by a gold layer at 18 mA for 360 s using a Biorad E5200 device. The functional groups present in CS-T, CS-T-PEI and CS-T-PEI-P were investigated by FTIR analysis using a Tensor 27 (Bruker) spectrometer with a ZnSe crystal over the 4000–500 cm^{-1} wavenumber range. 20 scans were recorded for each spectrum with a resolution of 4 cm^{-1} . DSC of the samples was carried out with a DSC-131 Setaram with a 20 °C–500 °C temperature range and a heating rate of 10 °C min^{-1} . The zeta potential of CS-T, CS-T-PEI and CS-T-PEI-P dispersions was measured *via* electrophoretic light scattering (ELS) combined with phase analysis light scattering (PALS) using a Malvern Zetasizer Nano ZS setup. Measurements





Scheme 1 Schematic illustration of the preparation of CS-T-PEI-P and the possible interactions between dendrimers and CS adsorbent.

were performed with suspensions of 0.1 g of the different adsorbents in 10 mL of distilled water. The pH at point of zero charge (pH_{pzc}) of CS-T, CS-T-PEI and CS-T-PEI-P was determined by the solid addition method.^{29,30} The pH value of each sample was determined using a Consort C 863 electronic multi-parameter analyzer. The initial pH values (pH_i) of 50 mL of 0.1 mol L⁻¹ of NaNO₃ solution were roughly adjusted in the 1.0–12.0 pH range by using 0.1 mol L⁻¹ of HCl and NaOH. Then, 0.1 g of each sample was added to previously prepared NaNO₃ solutions, and shaken for 3 h until reaching equilibrium at ambient temperature for 48 h. Then, the final pH (pH_f) of the solutions was measured and pH_{pzc} was determined as $\Delta\text{pH} = 0$ from a plot of $(\text{pH}_f - \text{pH}_i)$ versus pH_i .

2.4. Adsorption experiments

The adsorption performance of functionalized CS was evaluated in the batch adsorption of NO₃⁻ and Cr(vi) at 23 °C. 0.2 g of CS-T-PEI-P were mixed with different concentrations of NO₃⁻ and Cr(vi) solutions in flasks (from 50 to 400 mg L⁻¹). Then, the mixtures were shaken in a thermostatic shaker at 300 rpm until equilibrium was reached. Afterwards, the suspensions were filtered on 0.45 μm-filter paper under vacuum, and the concentrations of NO₃⁻ and Cr(vi) in the filtrate were determined calorimetrically using a UV-Vis spectrophotometer (SHIMADZU UV-1640). The Cr(vi) concentrations were in the filtrate was measured at a maximum wavelength of 540 nm after

complexation with 1,5-diphenylcarbazine,^{31,32} while the NO₃⁻ concentrations were measured at a wavelength adjusted to 415 nm and using the sodium salicylate method.³³ The pH was adjusted by adding small quantities of concentrated (0.1 M) HCl or NaOH solution. The adsorption kinetic was studied using 0.2 g of adsorbent in 50 mL of the NO₃⁻ and Cr(vi) ion solutions (natural pH) with varying initial pollutant concentrations (50, 100 and 150 mg L⁻¹) in 100 mL Erlenmeyer flasks. The suspensions were stirred during 5 to 420 min and 5 to 540 min for NO₃⁻ and Cr(vi) respectively. After a pre-determined time, the solution was filtered and then analyzed quantitatively. The equilibrium adsorption isotherms were performed to determine the maximum adsorption capacity (q_{max}) for NO₃⁻/Cr(vi) at 23 ± 2 °C. Modified CS (0.2 g) was mixed with 50 mL of solutions at different initial concentrations of the pollutants ranging between 50 and 400 mg L⁻¹ at natural pH. The suspensions were stirred until equilibrium times of 240 and 420 min were reached for NO₃⁻ and Cr(vi) respectively. The amounts of Cr(vi) or NO₃⁻ adsorbed at equilibrium (q_e) were calculated using eqn (1):

$$q_e = \frac{(C_0 - C_e) \times V}{m} \quad (1)$$

where C_0 and C_e are the initial and equilibrium concentration of Cr(vi) (mg L⁻¹). V is the volume of solution (L) and m is the mass of adsorbent used (g).



The adsorption yields E (%) were estimated using eqn (2):

$$E(\%) = \frac{(C_0 - C_e) \times 100}{C_0} \quad (2)$$

The effect of the pH on nitrate and Cr(vi) adsorption was investigated at 23 ± 2 °C in the initial 2.0–12.0 pH range. Cr(vi) solution was prepared at 100 mg L^{-1} and the pH was adjusted by adding 0.1 M HCl or 0.1 M NaOH. Adsorbent (0.2 g) was added into each solution and reacted until the equilibrium times 240 and 420 min for nitrate and Cr(vi), respectively.

2.5. Desorption and regeneration experiments

The desorption experiments were performed using 0.1 M NaOH solution as eluent to estimate the reversibility of functionalized CS and recovery of NO_3^- and Cr(vi) ions.³⁴ The adsorbents were first equilibrated with NO_3^- and Cr(vi) ions in aqueous solution with an initial concentration of 100 mg L^{-1} , and then the desorption test was initiated by mixing in the presence of NaOH solution until equilibrium time of 4 h and 7 h for NO_3^- and Cr(vi), respectively. After the desorption test, the adsorbents were thoroughly washed with distilled water and reused in the next cycle of adsorption experiments. The desorption and regeneration experiments were carried out at 23 ± 2 °C. The amounts of desorbed NO_3^- and Cr(vi) ions (Q_{des}) and efficiency (% of desorption) were determined by eqn (3) and (4), respectively:

$$Q_{\text{des}} = \frac{C_{\text{des}} V}{m} \quad (3)$$

$$\text{Percent of desorption} = \frac{\text{amount of } \text{NO}_3^- \text{ or Cr(VI) desorbed} \times 100}{\text{amount of } \text{NO}_3^- \text{ or Cr(VI) adsorbed}} \quad (4)$$

where C_{des} is the concentration of desorbed Cr(vi) or NO_3^- (mg L^{-1}), V is the volume of solution (L) and m is the mass of adsorbent (g).

3. Results and discussion

3.1. Surface morphology and structure

SEM images of CS-T, CS-T-PEI and CS-T-PEI-P are shown in Fig. 1. The treated cocoa shell (CS-T) exhibits a lamellar structure with the smooth cell walls without mesopores and macropores. The lamellar structure of CS are attributed to the irregularly shaped lignocellulosic layers in which cellulose fibers can be distinguished from the lignin sheath. Comparing CS-T with CS-T-PEI, the surface becomes rough and cracked due to the decomposition of the components during chemical grafting of PEI and the drying at 50 °C. As seen in Fig. 1E and F, after modification, adsorbent exhibited serious shrinkage and

porous structure of the adsorbent collapsed as the result of shrinkage.

The IR spectra of CS-T, CS-T-PEI and CS-T-PEI-P are given in Fig. 2. The characteristic peaks of CS-T appeared at 3308 cm^{-1} and 2918 cm^{-1} and were assigned to the –OH and C–H stretching vibrations of cellulose, hemicellulose and lignin.³⁵ The peak at 1374 cm^{-1} was attributed to the C–H bending vibration, and the absorption band at 1150 cm^{-1} corresponded to the C–O asymmetric stretching vibration. The peaks at 1732 and 1023 cm^{-1} corresponded to the stretching vibrations of the C=O and C–O groups of hemicellulose and cellulose.³⁶ Compared with the spectrum of pristine CS-T, more peaks occurred in the spectra of PEI-modified CS-T. The peaks of the PEI spectrum at $2934\text{--}2810 \text{ cm}^{-1}$ and $3280\text{--}1588 \text{ cm}^{-1}$ were visible only on CS-T-PEI and CS-T-PEI-P and were attributed to the –CH, –CH₂– and N–H stretching vibration of the amide bond, respectively.^{34,37} The peaks of the O–H stretching vibration and N–H stretching vibration shifted to 3268 cm^{-1} and their intensity increased significantly.^{36,38} This suggests that no covalent bond was formed between CS and PEI. Reportedly, different strength of CS–O interaction with amines may be involved, resulting in a complex hydrogen-bonding network and residual water molecules from the synthesis. Therefore CS covering by PEI appears to rather involve ionic and hydrogen bridges interactions. Similar interaction type has already been reported for organic macromolecules bearing terminal groups with high affinity towards metal oxide.^{39–42} New peaks at 2926 and 2824 cm^{-1} were attributed to the C–H stretching vibration of –CH and –CH₂– from PEI.^{43,44} The strong peak at 1458 cm^{-1} visible on PEI and CS–PEI was ascribed to the stretching

vibration of the C–N–H bond.⁴⁵ The peaks at 1572 cm^{-1} , 1302 cm^{-1} and 1100 cm^{-1} corresponding to the bending of amino groups (N–H) from PEI were also visible in the spectrum of CS-T-PEI.^{34,46} These results clearly indicate that the macromolecular chains of PEI were successfully impregnated to the CS-T surface. After acidic treatment, the increase of the peak intensity at 3320 cm^{-1} was associated to the stretching vibration of NH_3^+ whereas the peaks at 1730, 1648 and 1450 cm^{-1} were

Table 1 Atomic composition of the elements detected on the surface of the samples according to XPS survey spectrum results

Samples	Atomic composition (%)		
	C	O	N
CS-T	40.98	23.09	2.43
CS-T-PEI	42.86	7.64	16.45
CS-T-PEI-P	19.37	20.90	3.03



assigned to the symmetric and asymmetric stretching vibration of N–H.³⁷

To ensure the proper grafting of dendrimers and identify any interaction that occurred during processing, the treated and untreated adsorbents were analyzed chemically by XPS. The broad-scan spectra and elemental quantifications are presented in Fig. S1† and Table 1. C, O and N were the main chemical species present in the samples. The occurrence of S in the scans was probably due to contamination when the samples were handled. The amine, oxygen and carbon percentages in the CS samples were 2.43%, 23.09% and 40.98%, respectively. After dendrimer grafting, XPS analysis revealed an increase in the carbon (from 40.98 to 42.86%) and nitrogen (from 2% to 16.45%) concentration, while the amount of oxygen is sharply decreased from 23.09 to 7.64%, suggesting that oxygen are well covered with amine. After protonation, the nitrogen concentration was decreased indicating that no covalent bond was formed between CS and PEI. Reportedly, different strength of CS–O interaction with amines may be involved, resulting in a complex hydrogen-bonding network. In addition, the

decreases of nitrogen and carbon concentration are attributed to the mean acidic condition that destabilize the amine and the CS structure, and then reduce the carbon quantity.

Regarding to the XPS curve of CS-T-PEI-P, peaks corresponding to the C 1s orbital can be deconvoluted into two peaks referred to the C–N bonds around 288 eV.⁴⁷ Furthermore, the increased C–NH₂ peak could be ascribed to the successful amine functionalization of CS. However, for CS-T-PEI-P, the N 1s spectra revealed a peak that could be separated into two peaks at approximately 399.5 and 401 eV. These peaks were assigned to C–NH and –NH₂/NH₃⁺ bonds, respectively.⁴⁷ The N 1s binding energy was lower after chemical coating of the dendrimer. This was explained by the contribution of the lone electrons from NH₃⁺ to increase the surface electron density of CS-T-PEI and CS-T-PEI-P, confirming protonation.⁴⁸

3.2. Thermal stability and surface properties

DSC analysis in the 25–400 °C temperature range was also performed to investigate the thermal stability of modified CS

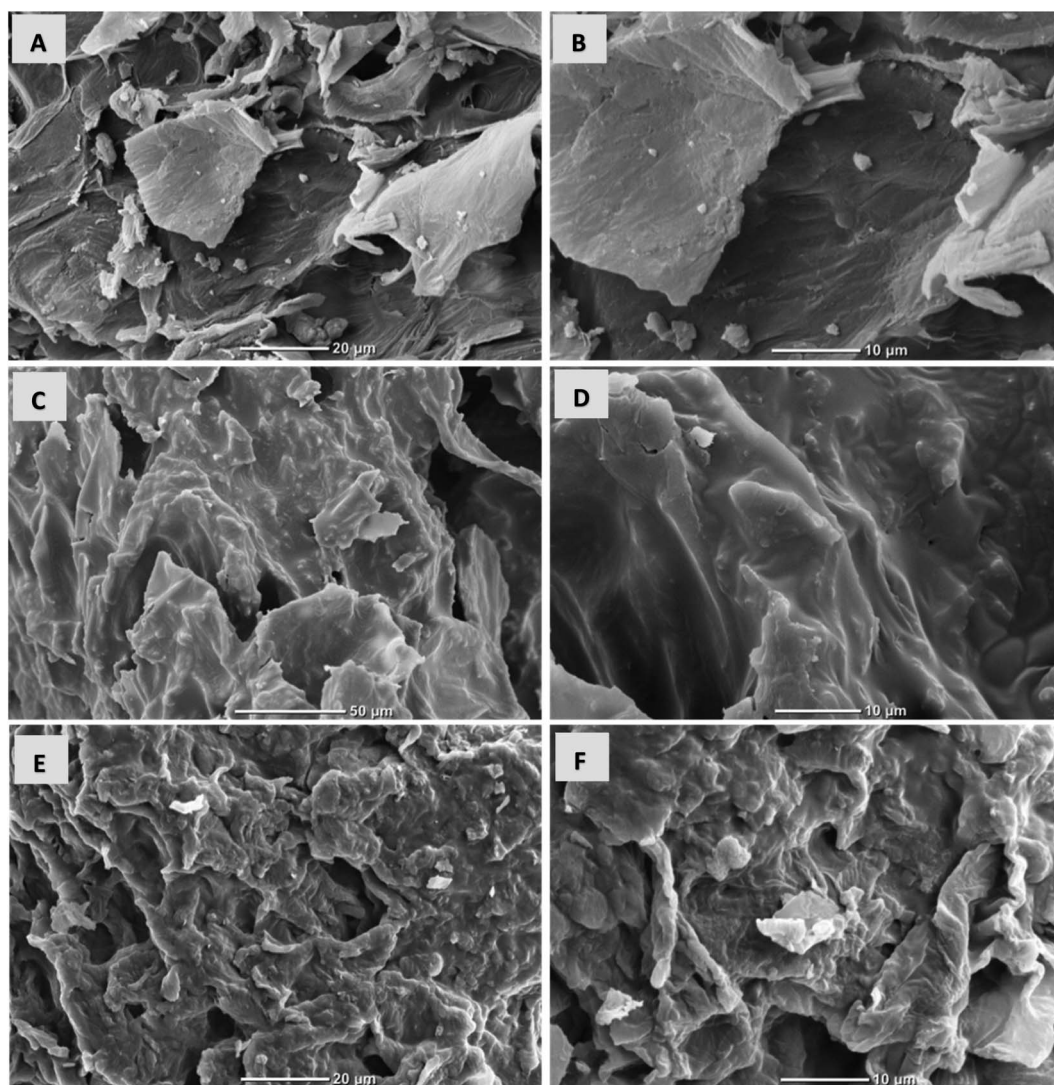


Fig. 1 SEM images of (A and B) CS-T, (C and D) CS-T-PEI, and (E and F) CS-T-PEI-P samples.



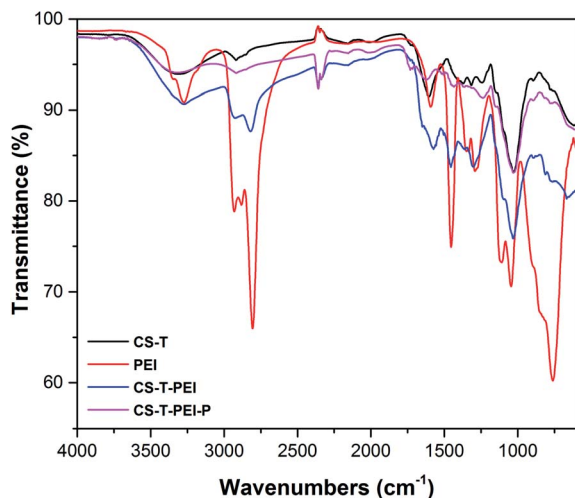


Fig. 2 FTIR spectra of CS-T, CS-T-PEI and CS-T-PEI-P.

(Fig. 3). The endothermic peak observed at around 109 °C was attributed to evaporation of free water from all samples.³⁵ The DSC curve of CS-T displayed a broad exothermic peak between 230 and 280 °C, which corresponded to the degradation of cellulose, lignin and hemicellulose.^{49–51} 3 exothermic peaks at 175, 250 and 326 °C corresponding to impregnated amine degradation were observed on CS-T-PEI-P.³⁷ Interestingly, a visible slight of both exothermic and endothermic peaks was observed for CS-T-PEI-P curve. Here, this slight toward the lower temperature, is a signal not only for the presence of PEI, but also for the improvement of the thermal stability. Therefore, PEI and PEI-P treatment increased the thermal stability of cocoa shells in the 140–400 °C range. All results were supported SEM and IR data, also in good agreement with literature.⁴⁹

Zeta potential analysis also provided important information about the surface charge density of the material. The average zeta potential for pristine CS-T was negative at -29.80 mV, probably resulting from the charge contribution of cellulose, hemicellulose and lignin.^{35,49} After PEI coating, the zeta potential shifted from -29.8 to 7.3 mV. The increase in zeta potential

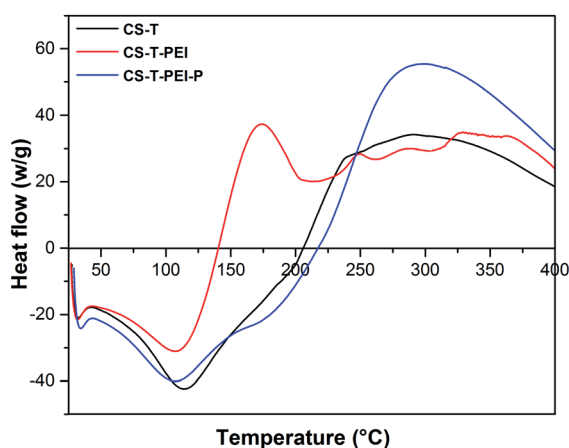


Fig. 3 DSC profiles of CS-T, CS-T-PEI and CS-T-PEI-P.

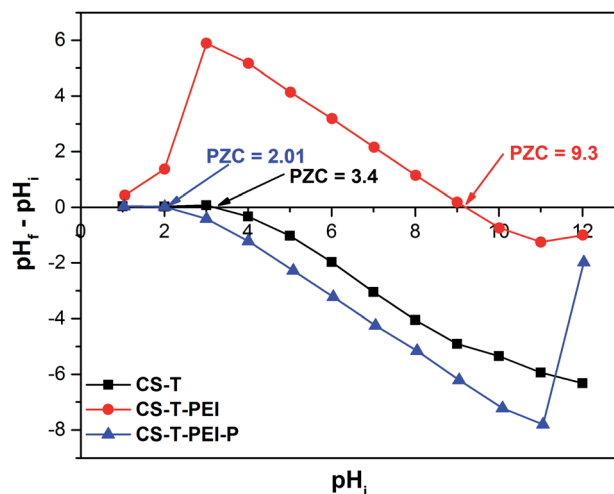


Fig. 4 Points of zero charge of CS-T, CS-T-PEI and CS-T-PEI-P.

revealed a strong modification of the surface, which can be explained by the positive charge of the PEI layer present on the cocoa cortex surface. HCl post-activation also changed the surface charge after the protonation step, the zeta potential increased from 7.3 to 18.6 mV, suggesting that some protons could still be entrapped in the CS-T-PEI-P structure.

The electrokinetic properties of the sorbent were investigated to elucidate the mechanism of the reaction between CS-T-PEI-P and nitrate or Cr(vi). The pH at point zero charge of CS-T, CS-T-PEI and CS-T-PEI-P were measured at different initial pH values (1.0–12.0) (Fig. 4). The pH_{pzc} is the pH at which the amount of negative charges on the adsorbent surface just equals the amount of positive charges.³⁰ The pH_{pzc} values of CS-T and CS-T-PEI were 3.4 and 9.3 , respectively. The pH_{pzc} of CS-T-PEI was significantly higher than that of CS-T owing to the basic nature of the amino groups on the CS-T-PEI surface.^{50,52} This value was higher than that of PEI-modified rice husk ash (9.0)⁵² and PEI-modified corn stalks (6.5),⁵⁰ suggesting a greater amount of basic groups present on CS-T-PEI. Therefore, pH_{pzc} confirmed the grafting of amino groups on the CS-T surface, in accordance with DSC, SEM and FTIR analysis, and indicated that CS-T-PEI could sequester Cr(vi) and nitrate by electrostatic interaction. After acidic activation, pH_{pzc} value is reduced from 9.3 for CS-T-PEI to 2.01 for CS-T-PEI-P indicating the acidic behavior of the surface (H^+ donor). This may be attributed to the protonation of the amine groups on the CS-T-PEI-P surface.⁵³

3.3. Parameter effects and surface interactions

The adsorption properties of the materials were studied for the removal of Cr(vi), and nitrate. All materials had affinity towards the adsorption of nitrate and chromate (Fig. 5). Interestingly, post-treatment of CS played a role in the enhancement of NO_3^- and Cr(vi) adsorption. The grafting of PEI and the protonation steps particularly increased the adsorption properties of the materials. Therefore, our functionalization method can be employed as an efficient way to increase the adsorption capacity for removing pollutants.



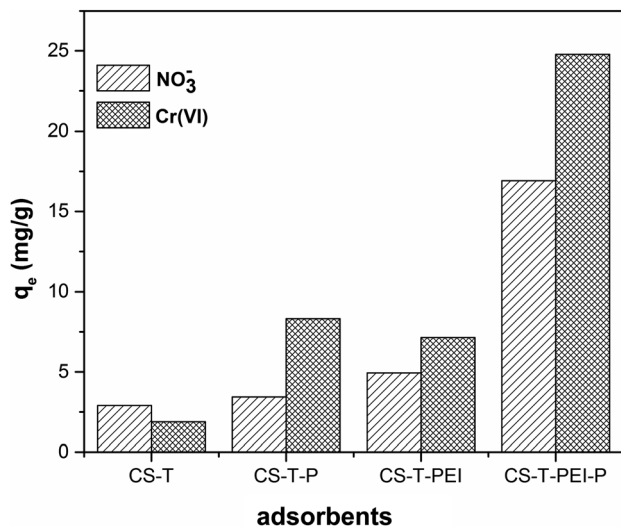


Fig. 5 Adsorption of nitrate and chromate onto different adsorbents ($C_i = 100 \text{ mg L}^{-1}$, $V = 50 \text{ mL}$, time of contact 6 h, 300 rpm, $m_{\text{ads}} = 0.2 \text{ g}$, $23 \text{ }^\circ\text{C}$ and initial pH = 2).

The sorption of nitrate and Cr(vi) onto CS-T-PEI-P as a function of the pH is shown in Fig. S2.† For nitrate, the adsorption capacity of CS-T-PEI-P increased from pH 2.0 to 5.0, with a maximum experimental adsorption capacity of 16.71 mg g^{-1} at pH 5.0. Further increases up to pH 10.0 remained close to the maximum value and then decrease drastically above pH 11.0. Other studies have reported maximum nitrate adsorption at lower pH values, for example 31 mg g^{-1} at pH 4.5.⁵⁴ These differences might be due to the interference of Cl^- ions (from the HCl solution used to adjust the pH) which occupied the adsorbent surface and compete with nitrate.⁵⁵ At higher pH values, competition between OH^- and NO_3^- may have occurred, resulting in decreased NO_3^- adsorption, and causing electrostatic repulsion between the surface and NO_3^- ions.^{56,57} For Cr(vi), no significant change occurred in terms of Cr(vi) removal capacity in the 2.0–11.0 pH range, indicating that the adsorption process was almost independent of initial pH.⁵⁸ In these cases, the experimental adsorption capacity decreased from 24.98 to 24.10 mg g^{-1} , and the corresponding removal rate decreased from 99.93 to 96.40%. Various anionic forms of Cr(vi) were present in the solution, including chromate CrO_4^- at alkaline pH, and other anionic forms (HCrO_4^- , $\text{Cr}_2\text{O}_7^{2-}$, CrO_4^-) at acidic pH.^{50,59} Amino groups on CS-T-PEI reacted with H^+ after acidic treatment, producing $-\text{NH}_3^+$ on the surface, and this group strongly adsorbed Cr(vi) through electrostatic attraction.^{50,59} The adsorption capacity and the corresponding removal rate decreased drastically when the initial pH was greater than 11.0. This poor capacity of CS-T-PEI-P may be attributed to the increasing competition for sites between OH^- and Cr(vi).⁶⁰

The adsorption equilibrium time is defined as the time required for the pollutant concentration to reach a constant value. The kinetic plots of the studied developed in this work are presented in Fig. S3 and S4.†

Table 2 Quantities of nitrate and Cr(vi) adsorbed on different adsorbents

Adsorbents	$Q_{\text{NO}_3^-}$ (mg g^{-1})	$Q_{\text{Cr(vi)}}$ (mg g^{-1})
CS-T	2.90	1.89
CS-T-P	3.43	8.32
CS-T-PEI	4.94	7.15
CS-T-PEI-P	16.92	24.78

Natural cocoa cortex was a poor candidate for nitrate and Cr(vi) adsorption. Only 1.9 mg g^{-1} and 2.9 mg g^{-1} of ions were adsorbed respectively. HCl treatment of CS-T multiplied by almost 8 the amount of adsorbed Cr(vi). However, the increase was limited for nitrate adsorption. PEI coating on CS-T was also a good strategy to increase the amount of adsorbed Cr(vi) but the adsorption yield of nitrate still remained limited. The synthesis of CS-T-PEI-P yielded the best adsorbent based on cocoa cortex. More than 24 mg g^{-1} of Cr(vi) and 16 mg g^{-1} of nitrate were adsorbed by CS-T-PEI-P, confirming that this composite is promising for pollutant removal (Table 2).

3.4. Kinetic studies

Adsorption kinetics are proposed for understanding the mechanism involved in the adsorption process (Fig. 6 and S3†). Numerous theoretical models provide an insight into the mechanism whereby the adsorbate accumulates on the biosorbent surface.^{60,61} To study the adsorption kinetics of nitrate and chromium(vi) onto CS-T-PEI-P, experimental datas were simulated by Lagergren pseudo-first order model (eqn (S5)†), pseudo-second order model (eqn (S6)†), Elovich equation (eqn (S7)†) and the intra-particle diffusion model (eqn (S8)†).^{50,62–64} The adsorption kinetics constants and correlation coefficients of nitrate and chromium(vi) adsorption onto CS-T-PEI-P are shown in Table S1.† Experimental data were best fitted with the pseudo-second order with a correlation coefficient of around 1. According to the pseudo-second order equation, the $q_{e,\text{cal}}$ values (8.80 , 17.12 and 22.27 mg g^{-1} for NO_3^- and 12.50 , 25.06 and 37.17 mg g^{-1}) for Cr(vi) were markedly similar to the experimental values ($q_{e,\text{exp}} = 8.76$, 17.04 and 22.12 mg g^{-1} for NO_3^- and 12.45 , 24.82 and 36.63 mg g^{-1}) for Cr(vi). These results suggest that the process controlling the adsorption rate may be chemical sorption involving valency forces through sharing or exchange of electrons between biosorbent and adsorbate.^{56,65}

Diffusion from the solid-liquid interface to the interior of the solid particles plays a very important role in adsorption. Fig. 6b plots q_t versus $t^{0.5}$ where the curve did not pass through the origin. It indicates that although intra-particle diffusion was involved in the sorption process, it was not the only rate-limiting step, and boundary layer diffusion controlled sorption. Other kinetic processes occurred simultaneously and contributed to the sorption mechanism.^{60,66}

3.4.1. Isotherm study. Adsorption isotherms describe how adsorbates interact with adsorbents. Therefore, studying these isotherms is critical for optimizing the development of the adsorbent.^{65,67} To optimize the design of an adsorption system,



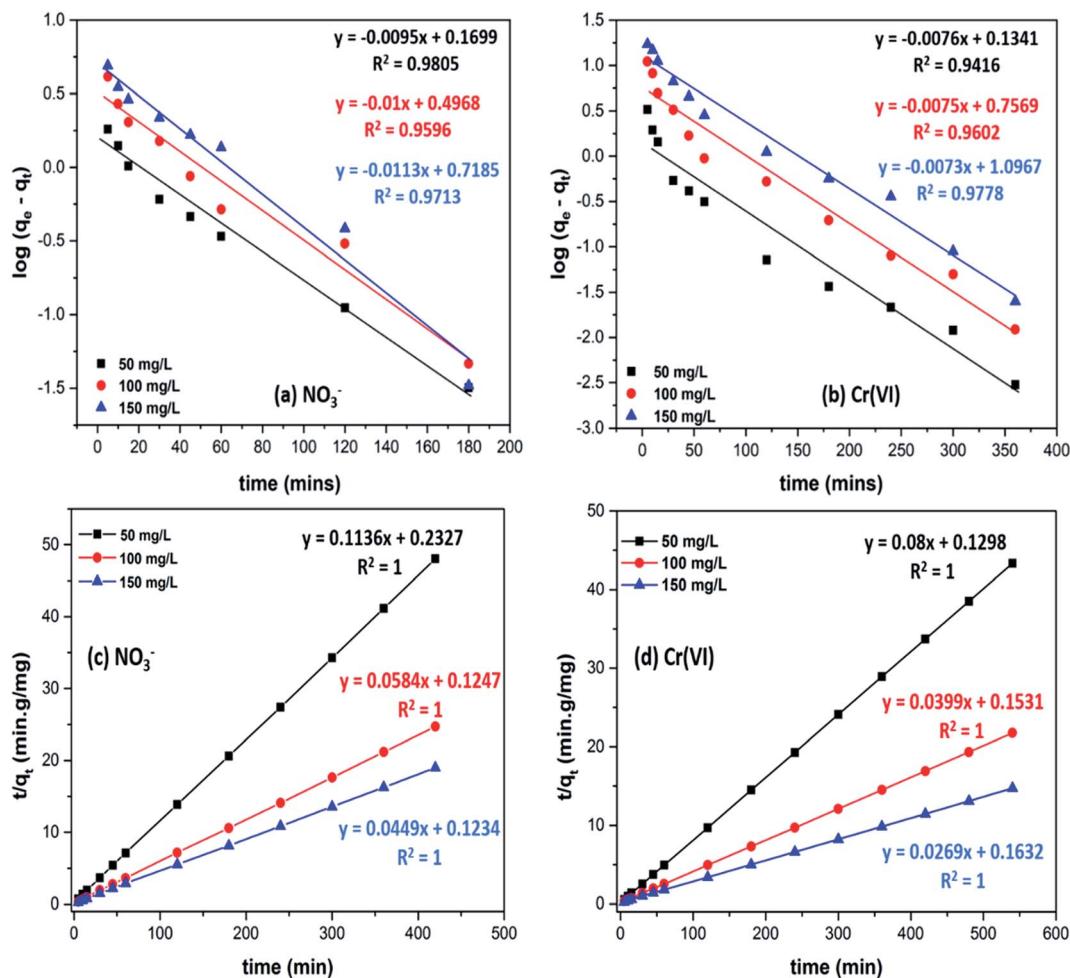


Fig. 6 Evolution in time of $\log(q_e - q_t)$ and t/q_t for the pseudo-first order and pseudo-second order kinetics of NO_3^- (a and c) and Cr(VI) (b and d) ions adsorption onto CS-T-PEI-P ($m_{\text{ads}} = 0.2$ g, initial pH, 300 rpm, $V = 50$ mL and 23°C).

it is essential to establish the most appropriate correlation for the equilibrium curve (Fig. S4–S6[†]).

Several isotherm equations are available for analyzing experimental data. Four important isotherms were selected for this study, namely the Freundlich (eqn (S9)[†]), Langmuir (eqn (S10)[†]), Temkin (eqn (S11)[†]) and Dubinin–Radushkevich (eqn (S12)–(S14)[†]) models.^{68–71} The equilibrium data for adsorption of Cr(VI) and nitrate were fitted to the previous model. They are presented in Fig. S4 and S5.[†] The theoretical parameters of the isotherms were determined from and listed with the regression coefficients in Tables S1 and S2.[†]

The Freundlich isotherm best described the adsorption of NO_3^- and Cr(VI) onto CS-T-PEI-P, suggesting (Fig. S6[†]) multilayer adsorption.^{38,72,73} However, monolayer adsorption may also have played determining role in pollutants adsorption onto CS-T-PEI-P because the values of the correlation coefficient were close to 1. The maximum monolayer adsorption capacity for NO_3^- and Cr(VI) onto CS-T-PEI-P was estimated from Langmuir model at 86.956 mg g^{-1} for NO_3^- and 94.340 mg g^{-1} for Cr(VI) . The largest amounts of adsorbed NO_3^- and Cr(VI) molecules recorded during the first step of the adsorption process

(Fig. S6[†]). The maximum monolayer adsorption capacities (q_{max}) for NO_3^- and Cr(VI) adsorption onto CS-T-PEI-P were compared with the q_{max} of other adsorbents available in the literature (Table 3). CS-T-PEI-P appeared highly competitive, with higher performance than other adsorbents previously reported in the literature.

The Freundlich model constants n_F were 1.460 and 2.864 for NO_3^- and Cr(VI) , respectively reflecting that the adsorption process between NO_3^- and Cr(VI) with CS-T-PEI-P was favorable ($1 < n < 10$).^{38,45} The correlation with the Freundlich model supported the existence of electrostatic interactions between NO_3^- and Cr(VI) on the one hand– NH_3^+ of CS-T-PEI-P on the other hand.⁷² The adsorption energy (E) values estimated from Dubinin–Radushkevich (D–R) isotherms were 0.090 and 2.610 kJ mol^{-1} for NO_3^- and Cr(VI) , respectively, suggesting that NO_3^- and Cr(VI) were sorbed onto CS-T-PEI-P by physisorption.⁷⁴

3.4.2. Adsorption thermodynamics. Adsorption thermodynamic parameters were determined to provide information on the inherent energy and the mechanism involved in the adsorption process. The thermodynamic parameters include enthalpy (ΔH° , kJ mol^{-1}), Gibbs free energy (ΔG° , kJ mol^{-1}) and



Table 3 Capacity of various biosorbents for adsorption of NO_3^- and $\text{Cr}(\text{vi})$ in aqueous solutions

Biosorbent name	Functionalization	Capacity (mg g^{-1})	Reference
NO_3^-			
Modified granular activated carbon	[3-(Methacryloylamino)propyl]-trimethylammonium chloride	26	75
Virgin reed	Triethylamine	118.9	76
Corn stalks	Ethylenediamine	65.359 (298K)	56
Sugarcane bagasse biochar	Ethylenediamine	28.21	54
PEG/chitosan and PVA/chitosan	Polyethylene glycol and polyvinyl alcohol	50.68–35.03	20
Modified steel slag	Aluminium hydroxide	16.396	77
Corn stalks	Diethylamine	13.6054	78
Modified cocoa cortex	PEI-HCl	86.956	This study
$\text{Cr}(\text{vi})$			
Modified granular activated carbon	[3-(Methacryloylamino)propyl]-trimethylammonium chloride	81.00	75
Sugarcane bagasse	Iron(III)-impregnated	13.72	58
Brown algae	Hydrochloric acid	52.631	79
Virgin reed	Triethylamine	135.00	76
Coarse sugarcane bagasse (biochar)	Amino-terminated hyperbranched polymer	75.36	73
Masau stone	Diethylenetriamine	87.32	80
Spent substrate (<i>Auricularia auricular</i>)	Cetyl trimethyl ammonium bromide and immobilized by sodium alginate	27.25	81
Modified cocoa cortex	PEI-HCl	94.340	This study

entropy (ΔS° , $\text{J mol}^{-1} \text{K}^{-1}$), which were calculated using the Van't Hoff equations (eqn (S15)–(S17)†). The adsorption experiments were performed at the temperatures of 23, 30, 40 and 50 °C (Fig. S7†) and the values of ΔH° and ΔS° were calculated from the plot of $\ln k_c$ vs. $1/T$ and presented in Table S3.†

The negative values of ΔG° at all temperatures for nitrate (-1.566 , -1.318 , -0.963 and -0.608 kJ mol^{-1}) and chromate (-12.10 , -13.963 , -16.624 and -19.285 kJ mol^{-1}) indicated that the adsorption process was spontaneous. For nitrate, the spontaneity of the adsorption process decreased when temperature increased whereas for chromium ions it increased when temperature increased. In the case of nitrate, the negative value of ΔH° (-12.071 kJ mol^{-1}) suggested that the reaction was exothermic, further confirming that higher temperature was not favorable for nitrate adsorption. The negative value of entropy change ΔS° (-35.488 $\text{J K}^{-1} \text{mol}^{-1}$) reflected the affinity of NO_3^- for CS-T-PEI-P. It indicated variation in CS-T-PEI-P structure and decreasing randomness at the adsorbent–aqueous solution.^{82,83} The standard enthalpy and entropy values of $\text{Cr}(\text{vi})$ were 66.677 kJ mol^{-1} and 266.139 $\text{J K}^{-1} \text{mol}^{-1}$, respectively. The positive value of ΔH° proved that the adsorption of $\text{Cr}(\text{vi})$ onto CS-T-PEI-P was endothermic, further confirming that higher temperature was favorable for $\text{Cr}(\text{vi})$ adsorption. The value of ΔS° was positive suggesting the increase of randomness at the solid–solution interface during the adsorption of $\text{Cr}(\text{vi})$ ions on the active site of the adsorbent.^{23,75}

3.5. Desorption and regeneration studies

For industrial application, sorbents have to be recoverable and reusable with a limited loss of efficiency. We conducted desorption experiments using 0.1 M NaOH solution with different contact times. The desorption kinetics of CS-T-PEI-P for NO_3^- and $\text{Cr}(\text{vi})$ are shown in Fig. 7. The desorption

process was rapid, and the maximum yield was reached after 180 minutes for NO_3^- (corresponding to 84% of desorption) and 200 minutes for $\text{Cr}(\text{vi})$ (corresponding to 70% of desorption). The regeneration studies of CS-T-PEI-P were conducted over 5 cycles (Fig. 8). After 5 consecutive adsorption–desorption cycles, the adsorption capacities were reduced from 16.88 to 12.95 mg g^{-1} (from 67.51 to 51.81%) for nitrate removal and from 24.82 to 19.23 mg g^{-1} (from 99.30 to 61.16%) for $\text{Cr}(\text{vi})$ removal. This slight decrease is due to the loss of adsorbent particles, during the filtration and recover steps. However, the presence of considerable amount of amine at the CS surface endorses the potential reusability. The different data indicated that CS-T-PEI-P had good recyclability and reusability.

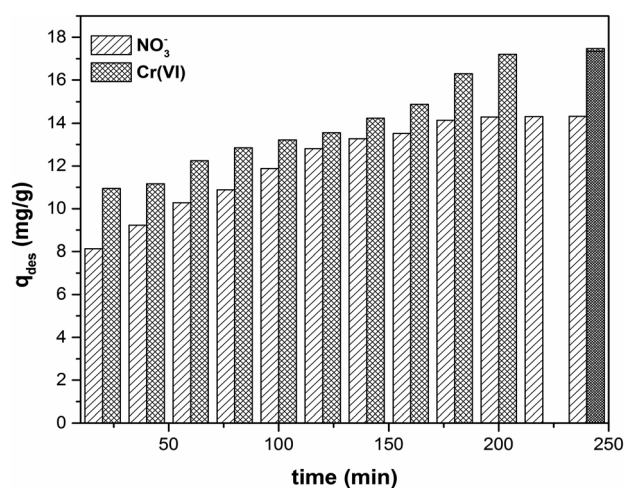


Fig. 7 Desorption of NO_3^- and $\text{Cr}(\text{vi})$ from CS-T-PEI-P ($C_i = 100$ mg L^{-1} , $V = 50$ mL, $m_{\text{ads}} = 0.2$ g, initial pH, RT, 300 rpm).



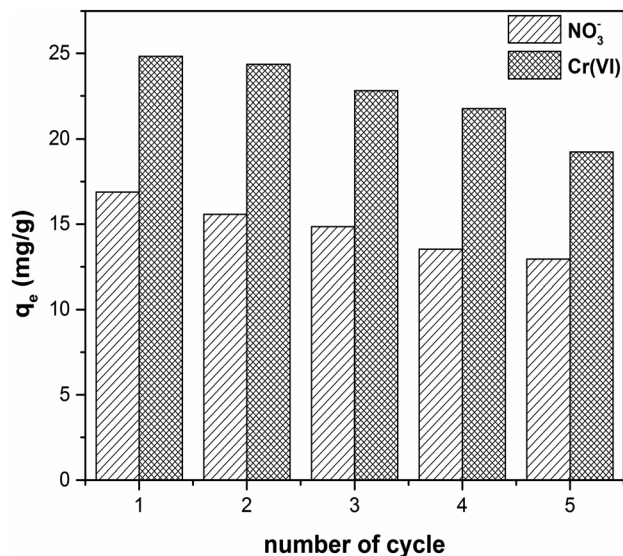


Fig. 8 Reusability of CS-T-PEI-P for NO₃⁻ and Cr(VI) removal in five successive adsorption/desorption cycles ($C_i = 100 \text{ mg L}^{-1}$, $V = 50 \text{ mL}$, $m_{\text{ads}} = 0.2 \text{ g}$, initial pH, RT, 300 rpm).

4. Conclusion

In summary, this work introduces a facile approach to functionalize biomaterials based on cocoa shells, using physical treatment, chemical grafting of dendrimer and protonation. The resulting materials CS-T-PEI-P were fully characterized and the surface properties, thermal stability and morphology were investigated. CS covering by PEI appears to rather involve ionic and hydrogen bridges interactions with high stability. The synergistic effect of protonate dendrimer on a CS surface become a promising candidate as adsorbent of hexavalent chromium and nitrate ions from aqueous solution. Experimental parameters such as pH, equilibration time, pollutant concentration and temperature were optimized. The removal phenomena followed by Freundlich model and the sorption reaction was well fitted to be pseudo-second order kinetic model. The maximum monolayer adsorption capacities achieved 86.956 mg g^{-1} for NO₃⁻ and 94.340 mg g^{-1} for Cr(VI). Results on desorption and regeneration studies proved that the new functionalized support based on cocoa-shell has good recyclability and reusability.

Author contribution

P. Nkuigwe Fotsing: investigation and writing original draft, Prof. E. Djoufack Woumfo: conceptualization and supervision, Dr S. Mezghich: investigation, Dr M. Mignot: resources and validation, N. Mofaddel: validation, F. Le Derf: funding administration, J. Vieillard: project administration, supervision, writing review and editing.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

This work was partially supported by INSA Rouen, Normandy Rouen University, CNRS, Labex SynORG (ANR-11-LABX-0029), the French Embassy in Cameroon (879327A), the Haute Normandie Region (CRUNCH and SéSa networks) and Grand Evreux Agglomération.

References

- 1 C. J. Vörösmarty, *et al.*, *Nature*, 2010, **467**, 555.
- 2 M. M. Ayad and A. A. El-Nasr, *J. Phys. Chem. C*, 2010, **114**, 14377–14383.
- 3 J. Lin, *et al.*, *Bioresour. Technol.*, 2010, **101**, 34–40.
- 4 M. R. Abukhadra, *et al.*, *Ecotoxicol. Environ. Saf.*, 2018, **157**, 358–368.
- 5 N. K. Lazaridis and D. D. Asouhidou, *Water Res.*, 2003, **37**, 2875–2882.
- 6 N. D. Suzaimi, *et al.*, *J. Environ. Chem. Eng.*, 2019, **7**, 103235.
- 7 C. V. Lazaratou, *et al.*, *Appl. Clay Sci.*, 2020, **185**, 105377.
- 8 J. Hu, *et al.*, *Langmuir*, 2005, **21**, 11173–11179.
- 9 H. Liu, *et al.*, *Water Res.*, 2011, **45**, 145–154.
- 10 J. Cao, *et al.*, *Chem. Eng. J.*, 2018, **353**, 126–137.
- 11 W. Xiong, *et al.*, *Chemosphere*, 2018, **210**, 1061–1069.
- 12 M. R. Abukhadra, *et al.*, *Adv. Powder Technol.*, 2018, **29**, 2501–2511.
- 13 M. Yang, *et al.*, *J. Colloid Interface Sci.*, 2017, **506**, 669–677.
- 14 M. Hua, *et al.*, *J. Hazard. Mater.*, 2012, **211–212**, 317–331.
- 15 F. Mohamed, *et al.*, *Sci. Total Environ.*, 2018, **640–641**, 352–363.
- 16 C. Zhou, *et al.*, *ACS Sustainable Chem. Eng.*, 2018, **6**, 4174–4184.
- 17 J. C. García, *et al.*, *Biochem. Eng. J.*, 2013, **71**, 127–133.
- 18 M. Wu, *et al.*, *Int. J. Environ. Res. Public Health*, 2019, **16**, 205.
- 19 Y. Huang, *et al.*, *RSC Adv.*, 2015, **5**, 11475–11484.
- 20 A. Rajeswari, *et al.*, *J. Water Process Eng.*, 2016, **9**, 123–134.
- 21 E. M. S. Azzam, *et al.*, *Int. J. Biol. Macromol.*, 2016, **89**, 507–517.
- 22 V. N. Tirtom, *et al.*, *Desalin. Water Treat.*, 2012, **39**, 76–82.
- 23 Q. Liu, *et al.*, *Int. J. Biol. Macromol.*, 2015, **72**, 1129–1135.
- 24 B. N. Narayanan, *et al.*, *Mater. Sci. Eng., B*, 2010, **168**, 242–244.
- 25 M. S. Sajab, *et al.*, *Bioresour. Technol.*, 2013, **128**, 571–577.
- 26 X. Xu, *et al.*, *Energy Fuels*, 2002, **16**, 1463–1469.
- 27 M. Arora, *et al.*, *Cold Reg. Sci. Technol.*, 2010, **62**, 92–97.
- 28 K. Jaafari, *et al.*, *Water SA*, 2001, **27**, 9–14.
- 29 E. Kiefer, *et al.*, *Environ. Sci. Technol.*, 1997, **31**, 759–764.
- 30 A. E. Ofomaja, *et al.*, *J. Hazard. Mater.*, 2009, **168**, 909–917.
- 31 J. Maity and S. K. Ray, *Int. J. Biol. Macromol.*, 2016, **89**, 246–255.
- 32 S. Chen, *et al.*, *Chem. Eng. J.*, 2011, **168**, 909–917.
- 33 A. M. E. Khalil, *et al.*, *Chem. Eng. J.*, 2017, **309**, 349–365.
- 34 Y. Ma, *et al.*, *Bioresour. Technol.*, 2014, **169**, 403–408.
- 35 J. Vieillard, *et al.*, *Chem. Eng. J.*, 2018, **342**, 420–428.
- 36 N. B. Mohamed, *et al.*, *Chem. Eng. Trans.*, 2017, **56**, 103–108.
- 37 Y. Liu, *et al.*, *RSC Adv.*, 2013, **3**, 18803–18810.
- 38 L. You, *et al.*, *Int. J. Biol. Macromol.*, 2018, **107**, 1620–1628.



- 39 Y. Coppel, *et al.*, *Chem.–Eur. J.*, 2012, **18**, 5384–5393.
- 40 N. Bouazizi, *et al.*, *Int. J. Hydrogen Energy*, 2016, **41**, 11232–11241.
- 41 R. D. Bach, *et al.*, *J. Adhes. Sci. Technol.*, 1994, **8**, 249–259.
- 42 P. Joshi, *et al.*, *Phys. Chem. Chem. Phys.*, 2011, **13**, 476–479.
- 43 Y. Wang, *et al.*, *Mater. Chem. Phys.*, 2018, **207**, 105–113.
- 44 H. He, *et al.*, *Sci. Rep.*, 2017, **7**, 3913.
- 45 W. Zhan, *et al.*, *RSC Adv.*, 2018, **8**, 18723–18733.
- 46 N. Rao, *et al.*, *Energy Fuels*, 2018, **32**, 670–677.
- 47 C. Hu, *et al.*, *J. Colloid Interface Sci.*, 2019, **553**, 372–381.
- 48 Y.-H. Ding, *et al.*, *Dalton Trans.*, 2018, **47**, 684–692.
- 49 R. Bargougui, *et al.*, *J. Environ. Chem. Eng.*, 2018, **6**, 325–331.
- 50 W.-H. Chen and P.-C. Kuo, *Energy*, 2011, **36**, 6451–6460.
- 51 R. Ianchis, *et al.*, *J. Nanopart. Res.*, 2012, **14**, 1233.
- 52 A. Imyim and E. Prapalimrungsi, *J. Hazard. Mater.*, 2010, **184**, 775–781.
- 53 S. Deng and Y. P. Ting, *Environ. Sci. Technol.*, 2005, **39**, 8490–8496.
- 54 L. Divband Hafshejani, *et al.*, *Ecol. Eng.*, 2016, **95**, 101–111.
- 55 M. A. Khan, *et al.*, *Sep. Sci. Technol.*, 2011, **46**, 2575–2584.
- 56 W. Song, *et al.*, *J. Hazard. Mater.*, 2016, **304**, 280–290.
- 57 S. Jain, *et al.*, *J. Environ. Chem. Eng.*, 2015, **3**, 2342–2349.
- 58 Y. Zhu, *et al.*, *Int. J. Environ. Sci. Technol.*, 2012, **9**, 463–472.
- 59 P. C. Okafor, *et al.*, *Int. J. Electrochem. Sci.*, 2012, **7**, 12354–12369.
- 60 Q.-Q. Zhong, *et al.*, *Carbohydr. Polym.*, 2014, **111**, 788–796.
- 61 S. S. Gupta and K. G. Bhattacharyya, *Adv. Colloid Interface Sci.*, 2011, **162**, 39–58.
- 62 S. Lagergren, *K. Sven. Vetenskapsakad. Handl.*, 1898, **24**, 1–39.
- 63 Y. S. Ho and G. McKay, *Process Biochem.*, 1999, **34**, 451–465.
- 64 J. W. J. Weber and J. C. Morris, *J. Sanit. Eng. Div., Am. Soc. Civ. Eng.*, 1963, **89**, 31–59.
- 65 Y. Li, *et al.*, *Cellulose*, 2018, **25**, 4757–4769.
- 66 K. Nithya, *et al.*, *Desalin. Water Treat.*, 2016, **57**, 25097–25113.
- 67 T. Zang, *et al.*, *Ecol. Eng.*, 2017, **99**, 358–365.
- 68 H. M. F. Freundlich, *J. Phys. Chem.*, 1906, **57**, 385–470.
- 69 I. Langmuir, *J. Am. Chem. Soc.*, 1916, **38**, 2221–2295.
- 70 M. Temkin and V. Pyzhev, *Acta Physicochim. URSS*, 1940, **12**, 327–356.
- 71 M. M. Dubinin and L. V. Radushkevich, *Proc. Acad. Sci. Phys. Chem. Sec. USSR*, 1947, **55**, 331–333.
- 72 D.-M. Guo, *et al.*, *RSC Adv.*, 2017, **7**, 54039–54052.
- 73 L. Xia, *et al.*, *Polymers*, 2018, **10**, 931.
- 74 A. A. Inyinbor, *et al.*, *Water Resources and Industry*, 2016, **15**, 14–27.
- 75 D.-W. Cho, *et al.*, *Chem. Eng. J.*, 2011, **175**, 298–305.
- 76 Z. Ren, *et al.*, *J. Colloid Interface Sci.*, 2016, **468**, 313–323.
- 77 L. Yang, *et al.*, *Water*, 2017, **757**, 1–17.
- 78 C. Fan and Y. Zhang, *J. Geochem. Explor.*, 2018, **188**, 95–100.
- 79 T. Ainane, *et al.*, *J. Mater. Environ. Sci.*, 2014, **5**, 975–982.
- 80 A. B. Albadarin, *et al.*, *J. Environ. Manage.*, 2017, **204**, 365–374.
- 81 C. Zhang, *et al.*, *RSC Adv.*, 2017, **7**, 34182–34191.
- 82 T. Wu, *et al.*, *Water Res.*, 2016, **93**, 30–37.
- 83 Y. Wu, *et al.*, *J. Taiwan Inst. Chem. Eng.*, 2016, **66**, 191–199.

