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## Imparting CO<sub>2</sub> reduction selectivity to ZnGa<sub>2</sub>O<sub>4</sub> photocatalysts by crystallization from hetero nano assembly of amorphous-like metal hydroxides†

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Imparting an enhanced CO<sub>2</sub> reduction selectivity to ZnGa<sub>2</sub>O<sub>4</sub> photocatalysts has been demonstrated by controlled crystallization from interdispersed nanoparticles of zinc and gallium hydroxides. The hydroxide precursor in which Zn(II) and Ga(III) are homogeneously interdispersed was prepared through an epoxide-driven sol-gel reaction. ZnGa<sub>2</sub>O<sub>4</sub> obtained by a heat-treatment exhibits a higher surface basicity and an enhanced affinity for CO<sub>2</sub> molecules than previously-reported standard ZnGa<sub>2</sub>O<sub>4</sub>. The enhanced affinity for CO<sub>2</sub> molecules of the resultant ZnGa<sub>2</sub>O<sub>4</sub> leads to highly-selective CO evolution in CO<sub>2</sub> photo-reduction with H<sub>2</sub>O reductants. The present scheme is promising to achieve desirable surface chemistry on metal oxide photocatalysts.

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#### Introduction

Heterogeneous catalysis for environmental-friendly production of resources has attracted remarkable attention.1 Especially, complex oxides, with high chemical/thermal stabilities and capability of their use in aqueous media, have been studied for various catalytic reactions such as CO2 reduction,2-4 watersplitting,5,6 biodiesel synthesis.7 Among many approaches, such as using co-catalysts,8-11 co-solvents,12 nanostructuration13-16 and Z-scheme photosynthesis, 17,18 surface modification of catalysts is especially a promising and versatile pathway to explore attracting catalytic activities, because the adsorption of reactants on a solid surface is a key reaction step in heterogeneous catalysis.19

Recently, we have reported the synthesis of metal hydroxide hydroxide NPs in a homogenous manner.<sup>23</sup> For example, hetero nanointerfaces constructed between cobalt and nickel hydroxide NPs (~2 nm) exhibit lower charge transfer resistance and improved electrochemical properties thanks to highly homogenous interdispersion of hydroxide NPs. Our motivation in the present work is to develop a straightforward route to access a "complex oxide" photocatalyst with a desirable surface chemistry of stoichiometric composition, through a lowtemperature thermal treatment on this class of metal hydroxides with hetero nanostructures.

We here choose ZnGa<sub>2</sub>O<sub>4</sub> as a representative system in order to demonstrate the present concept for yielding metal oxide photocatalysts with an enhanced catalytic activity originated from a high surface basicity. ZnGa2O4 has been reported as a promising oxide to photocatalytically reduce CO<sub>2</sub> into CO with H2O as an electron donor by loading of Ag co-catalyst.24 On the other hand, there still remains a challenge that competitive H<sub>2</sub> evolution as a result of the reduction of H<sub>2</sub>O solvent inevitably occurs on bare ZnGa<sub>2</sub>O<sub>4</sub> catalyst (without co-catalyst), resulting in a low reaction selectivity toward CO<sub>2</sub> reduction (<~30%).<sup>24</sup> A previous report on Zn-modified Ga<sub>2</sub>O<sub>3</sub> photocatalyst suggests that Zn-O-Ga linkages on the surface of catalysts play an important role to inhibit H<sub>2</sub> production in photocatalytic conversion of CO<sub>2</sub> with H<sub>2</sub>O.<sup>4</sup> The homogenous interdispersion of precursory metal hydroxide NPs is expected to allow for the formation of such kind of surface.

Herein, we demonstrate that a nanocomposite of precursory metal hydroxide NPs with hetero nanointerfaces can be used to prepare ZnGa<sub>2</sub>O<sub>4</sub> photocatalyst stoichiometrically-containing Zn(II) and Ga(III) on the oxide surface, leading to a highlyenhanced selectivity toward photocatalytic CO2 reduction. The precursory nanocomposite is prepared under a highly supersaturated condition induced by epoxide-mediated alkalization.25 ZnGa2O4 is obtained from the precursory nanocomposite

nanoparticle (NP) with a size of single nanometer by epoxidemediated alkalization.20,21 This synthesis pathway allows us to obtain metal hydroxide NPs as a stable suspension at a high yield without impurities.<sup>22</sup> Moreover, a unique and tailorable surface property has been demonstrated by the introduction of a large hetero-interface by interdispersing two different

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by heat-treatment ranging from 500 °C to 900 °C. Surface analyses confirm that ZnGa<sub>2</sub>O<sub>4</sub> prepared in the present scheme exhibits a higher base strength and a higher affinity for CO2 compared to those of standard ZnGa<sub>2</sub>O<sub>4</sub> obtained by a solid phase reaction from a mixture of metal oxide precursors. XPS measurement has revealed that ZnGa<sub>2</sub>O<sub>4</sub> prepared through the present scheme has a surface of stoichiometric composition that is not the case for standard ZnGa<sub>2</sub>O<sub>4</sub> catalysts prepared at 850 °C. As a result, the present ZnGa<sub>2</sub>O<sub>4</sub> heat-treated at 700 °C (without co-catalyst) exhibits a reaction selectivity of 48.0% toward CO evolution, more than double to that of standard ZnGa<sub>2</sub>O<sub>4</sub> (20.3%). Also, Ag co-catalyst, that is required to maximize the reaction selectivity toward CO evolution, can be decreased into 5% of the previous reports, thanks to the high affinity for CO<sub>2</sub> adsorption of the resultant ZnGa<sub>2</sub>O<sub>4</sub> surface. Based on these insights obtained in this representative ZnGa<sub>2</sub>O<sub>4</sub> system, synthesis of complex oxide catalysts through the crystallization of interdispersed hydroxides NPs is expected to be applied to design a wide range of complex oxide catalysts with an intended surface.

### **Experimental section**

#### **Materials**

 $Zn(NO_3)_2 \cdot 6H_2O$  (99.0%),  $Ga(NO_3)_3 \cdot nH_2O$  (99.9%), ZnO (99.0%),  $Ga_2O_3$  (99.99%), ZnO (99.8%), bromothymol blue, phenolphthalein, 2,4-dinitroaniline, ZnO(90.5-100.3%), 0.1 M of ZnO(90.5%), 0.1 M of ZnO(90.5%),

#### Preparation of ZnGa<sub>2</sub>O<sub>4</sub>

 $Zn(NO_3)_2 \cdot 6H_2O$  (0.740 g; 2.49 mmol) and  $Ga(NO_3)_3 \cdot nH_2O$  (1.99 g; 4.98 mmol, n is set as 8 for the calculation.) were dissolved in a mixture of ultra-pure water (6.00 mL; 333 mmol) and ethanol (6.00 mL; 165 mmol). At 25 °C, PO (8.10 mL; 112 mmol) was added to the mixture solution and the solution was stirred for 30 s to form a homogeneous sol. Then, the sol kept in a closed container was placed under a static condition at 25 °C to form a wet gel. The wet gel was aged for 24 h at 25 °C. After aging process, the wet gel was dried at 40 °C to obtain a precursory xerogel. The xerogel was calcined at various temperatures ranging from 500 °C to 900 °C for 12 h to yield  $ZnGa_2O_4$ .  $ZnGa_2O_4$  was also prepared by a solid state reaction. The details are described in ESI.†

# Photocatalytic conversion of $\mathrm{CO}_2$ with $\mathrm{H}_2\mathrm{O}$ reductant in liquid phase

Photocatalytic conversion of  $CO_2$ , including the step of Agloading on  $ZnGa_2O_4$ , was carried out in a flow system using an inner-irradiation-type reaction vessel at 35 °C. Photocatalyst (0.5~g) was dispersed in ultra-pure water (1.0~L) containing 0.1~M of NaHCO $_3$ . Ag co-catalyst was loaded on  $ZnGa_2O_4$  by photo-

deposition method as follows; (1) AgNO3 was added at a concentration ranging from  $2.34 \times 10^{-6}$  M to  $46.8 \times 10^{-6}$  M. (2) Ar gas was bubbled into the suspension at a flow rate of 80 mL min<sup>-1</sup> to purge air for 1 h. (3) The flow rate was changed to 30 mL min<sup>-1</sup> and the suspension was illuminated with a 400 W high-pressure mercury lamp for 2 h. These steps for Ag-loading were skipped when photocatalytic reaction over the bare ZnGa<sub>2</sub>O<sub>4</sub> photocatalyst was examined. Then, CO<sub>2</sub> gas was bubbled into the suspension at a flow rate of 60 mL min<sup>-1</sup> for 1 h in order to purge Ar or air. The suspension was illuminated for 5 h with a 400 W high-pressure mercury lamp with a quartz filter equipped with a water cooling system, with a CO2 flow at a rate of 30 mL min<sup>-1</sup>. The outlet of the reactor was connected to a six-way valve with a sampling loop. Evolved gaseous products of H2, O2, and CO together with CO2 gas were collected and analyzed by thermal conductivity detector-gas chromatography (TCD-GC) using a GC-8A chromatograph (Shimadzu Corp.) with a Molecular Sieve 5A column and Ar as a carrier gas, and by flame ionization detector-gas chromatography (FID-GC) with a methanizer (Shimadzu Corp.), a Shin Carbon ST column, and N2 as a carrier gas. In an isotopic experiment with 13CO2, the formation of 13CO was detected by mass spectroscopy by using a quadrupole-type mass spectrometer (BEL Japan, BEL Mass).

#### Characterization

Crystal structures of samples were identified by powder X-ray diffraction (PXRD; MultiFlex, Rigaku, Japan). X-ray photoelectron spectroscopy (XPS) spectra were recorded by using X-ray photoelectron spectrometer (ESCA-3400, Shimadzu Corp.) under Mg Kα radiation. X-ray absorption fine structure (XAFS) spectra of Zn K-edge and Ga K-edge were collected in the transmission mode at room temperature on BL11 at the SAGA Light Source (Saga, Japan). A silicon (111) double-crystal monochrometor was used to obtain the incident X-ray beam. The intensity of the incident and transmitted X-ray was monitored by an ionization chamber. N<sub>2</sub> adsorption-desorption isotherms at -196 °C were obtained on a volumetric gas adsorption apparatus (BELSORP-mini II, Bel Japan Inc., Japan). Prior to the measurements, sample powders were pretreated at 200 °C under a vacuum condition overnight. Specific surface area of ZnGa<sub>2</sub>O<sub>4</sub> was estimated by the Brunauer-Emmett-Teller (BET) method. Morphologies of Zn-Ga AMH and ZnGa<sub>2</sub>O<sub>4</sub> catalysts were observed by a field emission scanning electron microscope (FE-SEM; S-4800, Hitachi, Japan, with a thin Pt coating), transmission electron microscopes (TEM; JEM-2000FX, JEOL, Japan and Hitachi 7650, Hitachi, Japan) and a field emission transmission electron microscope (FE-TEM; JEM-2100F, JEOL, Japan) equipped with EDS. The UV-Vis diffusion reflectance spectra of ZnGa<sub>2</sub>O<sub>4</sub> samples were measured by using UV-Visible spectrometer (V-670, JASCO, Japan) equipped with an integrating sphere. The energy gap  $(E_{\sigma})$  was estimated with the Davis-Mott method.26 Base strength of bare ZnGa2O4 catalysts was estimated by Hammett indicators; bromothymol Blue ( $pK_a = 7.2$ ), phenolphthalein (p $K_a = 9.8$ ) and 2,4-dinitroaniline (p $K_a = 15.0$ ) were used as coloring agents, and methanol was used as a solvent. When the color change of the indicator is observed,

the base strength  $(H_{-})$  of the tested solid sample is determined to be higher than the  $pK_a$  value of the indicator employed. <sup>27,28</sup> The affinity between  $CO_2$  and the surface of  $ZnGa_2O_4$  catalysts was assessed by thermal programmed desorption (TPD: BELCAT-B, Bel Japan Inc., Japan) of  $CO_2$ . He gas was flowed as a carrier gas and  $ZnGa_2O_4$  was degassed at 200 °C for 1 h. Then,  $CO_2$  was introduced and allowed to adsorb on  $ZnGa_2O_4$  at 30 °C for 30 min. After the adsorption of  $CO_2$ , the sample was heated from 30 °C to 800 °C at a heating rate of 5 °C min<sup>-1</sup>. Desorbed  $CO_2$  was monitored by using a quadrupole-type mass spectrometer (BEL Mass, Bel Japan Inc., Japan).

### Results and discussion

# Synthesis of ZnGa<sub>2</sub>O<sub>4</sub> through calcination of a gel composed of interdispersed metal hydroxide NPs with low crystallinities

A precursory xerogel for the synthesis of  $ZnGa_2O_4$  was obtained through epoxide-mediated alkalization from an aqueous solution of  $Zn(NO_3)_2 \cdot 6H_2O$  and  $Ga(NO_3)_3 \cdot nH_2O$  (Fig. 1(a)). Two small peaks at  $2\theta = 9.9^\circ$  and  $19.8^\circ$  and the broad diffraction pattern were observed in PXRD pattern of precursory xerogel (Fig. 1(b)). Two small peaks are assigned to 003 and 006 diffraction peaks of Zn–Ga layered double hydroxide (LDH) crystal, <sup>29</sup> whose  $Zn^{2+}/Ga^{3+}$  ratio was estimated as 1.5 from TEM-EDS mapping shown in Fig. S1.† By Bragg's law using the diffraction peak at  $2\theta = 9.9^\circ$ , the interlayer separation is calculated to be 0.89 nm, which corresponds to an interlayer space of LDH accommodating nitrate anions. <sup>30,31</sup> The broad diffraction on the PXRD pattern of the precursory xerogel is in

good agreement with that for low-crystalline Ga(OH)3 NPs with a size of 4.4 nm in diameter ( $S_{\text{BET}} = 349 \text{ m}^2 \text{ g}^{-1}$ ). The obtained gel is a nanocomposite of poorly-crystallized (amorphous-like) metal hydroxides containing a small amount of Zn-Ga LDH. The present epoxide-mediated alkalization allows us to yield a hydroxide gel corresponding with starting chemical composition because most of Zn<sup>2+</sup> and Ga<sup>3+</sup> species (96.3% of initial metals) are consumed during the reaction in a homogeneous manner (Fig. S2†). Scanning electron microscope (SEM) observation reveals that LDH platelets with a lateral size of 2 µm are embedded in the gel matrix composed of NPs (<10 nm in diameter) (Fig. 1(c-e)). Zn and Ga are homogeneously distributed in the precursory gel (Fig. S1(c)†), which confirms that both amorphous-like Zn(OH)2 and Ga(OH)3 NPs interdispersedly assembles to form the precursory gel (Fig. 1(e)). The present synthesis condition allows us to achieve a high degree of supersaturation and thereby the formation of abundant NPs to form a homogenous gel throughout the reaction solution. Hereafter, the present precursory composite gel is called as "Zn-Ga AMH" (Zn-Ga Amorphous Metal Hydroxide).

Fig. 2 shows powder X-ray diffraction (PXRD) patterns obtained from Zn–Ga AMH by the calcination at various temperatures ranging from 500 °C to 900 °C. Their diffraction patterns are ascribed to the typical pattern of  $\rm ZnGa_2O_4$  (ICDD PDF 00-038-1240). Interestingly, the synthesis of  $\rm ZnGa_2O_4$  as a single phase is possible even when the calcination temperature is as low as 500 °C by using the present Zn–Ga AMH as a precursor. Morphological observation by SEM (Fig. S3†) reveals that the size of  $\rm ZnGa_2O_4$  crystals obtained from Zn–Ga AMH by the

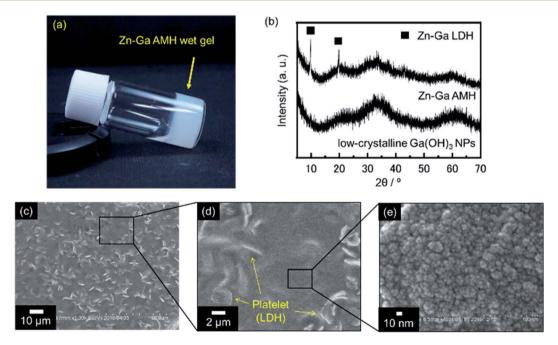


Fig. 1 (a) Photograph of precursory wet gel obtained from an aqueous solution of  $Zn(NO_3)_2 \cdot 6H_2O$  and  $Ga(NO_3)_3 \cdot nH_2O$  under a highly supersaturated condition induced by epoxide-mediated alkalization. (b) PXRD patterns of precursory xerogel and low-crystalline  $Ga(OH)_3$  NPs obtained from an aqueous solution of  $Ga(NO_3)_3 \cdot nH_2O$  (without  $Zn(NO_3)_2 \cdot 6H_2O$ ). (c-e) SEM images of precursory xerogel at different magnifications.

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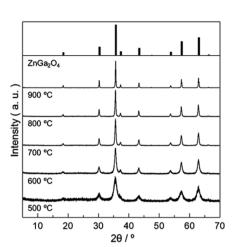


Fig. 2 PXRD patterns of  $\rm ZnGa_2O_4$  obtained from  $\rm Zn-Ga$  AMH by calcination in air at various temperatures for 12 h.

calcination at 500 °C is >10 nm and becomes larger with increasing calcination temperature due to crystal growth. The achievement of low-temperature synthesis of  $ZnGa_2O_4$  as a single phase is mainly due to highly-homogeneous dispersion of low-crystalline  $Zn(OH)_2$  and  $Ga(OH)_3$  NPs in Zn–Ga AMH as discussed in the former paragraph. As is well-known, cations are homogeneously distributed in hydroxide layers of Zn–Ga LDH in atomic scale, <sup>32,33</sup> suggesting that the contaminated small amount of Zn–Ga LDH also contributes to the low-temperature synthesis of  $ZnGa_2O_4$ .  $ZnGa_2O_4$  samples obtained as a single phase from Zn–Ga AMH are hereinafter named as "AMH-derived  $ZnGa_2O_4$ -X" (X is calcination temperature).

#### Surface basicity and affinity for CO2 of ZnGa2O4

The surface basicity of AMH-derived  $ZnGa_2O_4$  was investigated in comparison with previously-reported one. Hereafter,  $ZnGa_2O_4$  prepared at 850 °C through a solid phase reaction (Fig. S4†), whose catalytic activity is reportedly highest in the

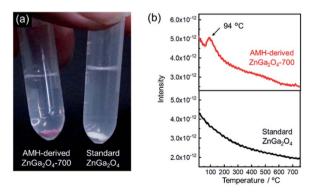


Fig. 3 (a) Photograph of AMH-derived  $ZnGa_2O_4$ -700 and standard  $ZnGa_2O_4$  immersed in a methanolic solution of Hammett indicator (phenolphthalein). (b)  $CO_2$ -TPD curves of AMH-derived  $ZnGa_2O_4$ -700 and standard  $ZnGa_2O_4$  (sample mass: 0.5 g).

report24 is called as "standard ZnGa2O4". We found that ZnGa<sub>2</sub>O<sub>4</sub> obtained from Zn-Ga AMH exhibits a unique surface nature different from standard ZnGa<sub>2</sub>O<sub>4</sub>. Fig. 3(a) shows AMHderived ZnGa<sub>2</sub>O<sub>4</sub>-700 and standard ZnGa<sub>2</sub>O<sub>4</sub> immersed in a methanolic solution of Hammett indicator (phenolphthalein). AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 changes its color from white to red upon the immersion in the indicator solution, whilst the change of color is not observed for standard ZnGa<sub>2</sub>O<sub>4</sub>, indicating that base strength of AMH-derived ZnGa2O4-700 in methanol is stronger than that of standard ZnGa<sub>2</sub>O<sub>4</sub>. Base strength, crystallite size, and specific surface area of ZnGa<sub>2</sub>O<sub>4</sub> samples are summarized in Table S1.† Base strength of AMHderived ZnGa2O4 decreases by the heat treatment above at 700 °C. Nonetheless, the base strength of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-900 is found to be still higher than that of standard ZnGa<sub>2</sub>O<sub>4</sub> prepared at a relatively lower calcination temperature of 850 °C. The difference in coloring behavior cannot be explained by difference in surface area, but difference in surface nature; AMH-derived  $ZnGa_2O_4$ -900 ( $S_{BET} = 0.53 \text{ m}^2 \text{ g}^{-1}$ ) exhibits a stronger surface basicity than standard  $ZnGa_2O_4$  ( $S_{BET} = 1.3$ m<sup>2</sup> g<sup>-1</sup>). The epoxide-mediated alkalization employed in the present study clearly contributes to yield ZnGa<sub>2</sub>O<sub>4</sub> with the high basic strength.

CO2 temperature programmed desorption (CO2-TPD) curves of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 and standard ZnGa<sub>2</sub>O<sub>4</sub> are plotted in Fig. 3(b). The peak at 94 °C, originated from desorption of CO2, is observed only for the TPD curve of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700, suggesting that the surface of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub> has a higher affinity and a stronger adsorptive nature for CO<sub>2</sub> than standard ZnGa<sub>2</sub>O<sub>4</sub>. The peak at 94 °C could be detected even when the sample mass of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 was decreased to 1/5 in order to compensate the difference in  $S_{\text{BET}}$  between AMH-derived  $\text{ZnGa}_2\text{O}_4$ -700 ( $S_{\text{BET}}$  = 5.0 m<sup>2</sup> g<sup>-1</sup>) and standard ZnGa<sub>2</sub>O<sub>4</sub> ( $S_{BET} = 1.3 \text{ m}^2 \text{ g}^{-1}$ ). The result reveals that the difference in  $S_{\text{BET}}$  is not the cause of the different CO<sub>2</sub> adsorption capacity of the two samples. The peak in low-temperature range is also observed for TPD curves of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-500 and AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-600 (not shown). From the above all results, we can conclude that single phase ZnGa<sub>2</sub>O<sub>4</sub> with a high base strength and a high affinity for CO<sub>2</sub> can be obtained by the calcination of Zn-Ga AMH.

Structure analysis of ZnGa<sub>2</sub>O<sub>4</sub> catalysts were performed by XAFS and XPS. The difference of surface structure between AMH-derived ZnGa<sub>2</sub>O<sub>4</sub> and standard ZnGa<sub>2</sub>O<sub>4</sub> was investigated by XPS. XAFS measurement was employed as a technique to understand local environments of the atoms for bulk samples. Fig. 4 shows Zn K-edge and Ga K-edge EXAFS and Fourier transforms (FT) of EXAFS spectra of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 and standard ZnGa<sub>2</sub>O<sub>4</sub>. The same characteristic distance is observed in the first neighbor peaks (Zn–O shells in Zn K-edge EXAFS and Ga–O shells in Ga K-edge EXAFS) and the second neighbor peaks (Zn–Ga and Zn–Zn shells in Zn K-edge EXAFS, and Ga–Ga and Ga–Zn shells in Ga K-edge EXAFS). These results support that the average local environments of Zn and Ga atoms are comparable in AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 and standard ZnGa<sub>2</sub>O<sub>4</sub>.

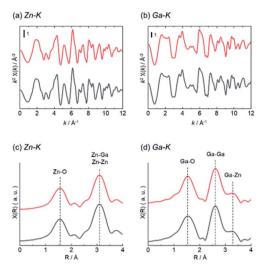


Fig. 4 (a) Zn K-edge and (b) Ga K-edge EXAFS (c and d) Fourier transforms of EXAFS spectra of AMH-derived  $ZnGa_2O_4$ -700 (red line) and standard  $ZnGa_2O_4$  (black line).

XPS analysis was employed to compare the chemical composition for AMH-derived  $\rm ZnGa_2O_4$ -700 and standard  $\rm ZnGa_2O_4$ , where the sampling depth is estimated to be  $\it ca.$  3.0 nm. The XPS peaks of Zn 3d, Ga 3d, Zn 3p, Ga 3p, Zn 3s, Ga 3s, O 1s, Zn 2p and Ga 2p are observed in wide-scan XPS spectra of both  $\rm ZnGa_2O_4$  catalysts (Fig. S5†). Narrow spectra and estimated molar ratio values of  $\rm Zn/Ga$  of two  $\rm ZnGa_2O_4$  catalysts are summarized in Fig. 5. The peak positions of  $\rm Zn$  2p and Ga 2p in narrow scan XPS spectra are comparable for two  $\rm ZnGa_2O_4$  catalysts. It should be highlighted that there is a clear difference in  $\rm Zn/Ga$  ratio between two  $\rm ZnGa_2O_4$  photocatalysts. Preferential segregation of Zn on the surface ( $\rm Zn/Ga=0.7$ ) is confirmed

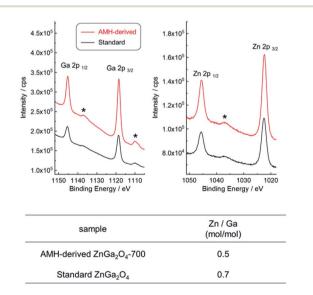


Fig. 5 Narrow scan XPS spectra of AMH-derived  $ZnGa_2O_4$ -700 (red line) and standard  $ZnGa_2O_4$  (black line) and the values of molar ratio of Zn/Ga. Surface chemical composition of  $ZnGa_2O_4$  photocatalysts analyzed by XPS measurement \*: satellite peaks.

for standard ZnGa<sub>2</sub>O<sub>4</sub>. A higher temperature would be required to obtain ZnGa<sub>2</sub>O<sub>4</sub> with the surface of stoichiometric composition in this solid state reaction, whereas the calcination at a higher temperature promotes the sintering of complex oxide particles, leading to decrease of accessible sites by reactants on complex oxide catalyst. On the other hand, the stoichiometric Zn/Ga molar ratio (Zn/Ga = 0.5) on the surface is confirmed for AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700, thanks to the highly-homogeneous distribution of hydroxide NPs in Zn-Ga AMH precursor. The results of XPS analyses suggest that a larger amount of Zn-O-Ga linkages is formed in the case of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 compared to standard ZnGa2O4. Although the further study is required to elucidate exact adsorption sites on the surface for CO<sub>2</sub>, such as hydroxyl groups, and oxygen in Zn-O-Ga linkages, it can be concluded that AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 with the stoichiometric surface exhibits the higher affinity for CO2 molecules because of the introduction of the stronger Lewis basic sites. The use of interdispersed amorphous Zn and Ga metal hydroxide NPs is a key to yield complex oxide with the surface of stoichiometric composition even by a lowtemperature synthesis.

#### Photocatalytic CO<sub>2</sub> reduction over bare ZnGa<sub>2</sub>O<sub>4</sub> (without cocatalyst)

Photocatalytic properties of AMH-derived  $ZnGa_2O_4$  catalysts were systematically investigated under the experimental condition optimized in a literature. AMH-derived  $ZnGa_2O_4$ -700 and standard  $ZnGa_2O_4$  exhibit the best catalytic activities in terms of CO evolution and reaction selectivity after the calcination temperature of 700 and 850 °C, are respectively (Fig. S6†). These two best catalysts for respective systems were closely examined in the following section.

The isotopic experiment was also carried out using  $^{13}\text{CO}_2$  as a gaseous reactant. Q-Mass spectra in m/z = 28 and m/z = 29 were collected for the photocatalytic conversion of  $^{13}\text{CO}_2$  with  $\text{H}_2\text{O}$  over AMH-derived  $\text{ZnGa}_2\text{O}_4$ -700 (Fig. 6). The peak derived from  $^{13}\text{CO}$  is observed on Q-Mass spectrum of m/z = 29. It has

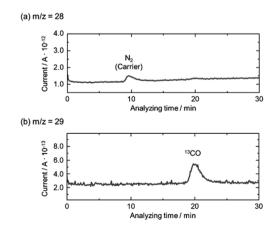


Fig. 6 Mass spectra of (a) m/z=28 and (b) m/z=29 in the photocatalytic conversion of  $^{13}CO_2$  by  $H_2O$  over bare AMH-derived  $ZnGa_2O_4$ -700 photocatalyst.

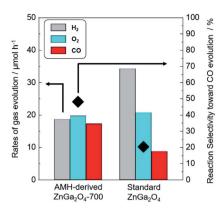


Fig. 7 Rates of  $H_2$  (grey),  $O_2$  (sky blue) and CO (red) evolution and reaction selectivity toward CO evolution ( $\spadesuit$ ) over bare AMH-derived  $ZnGa_2O_4$ -700 and bare standard  $ZnGa_2O_4$ .

been evidenced that AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 photocatalytically reduces introduced <sup>13</sup>CO<sub>2</sub> into <sup>13</sup>CO. Fig. S7† shows time course of gas evolutions for photocatalytic conversion of CO2 with water over AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700. The linear increase of evolved gases indicates that the present ZnGa2O4 catalyst possesses the stability in the photocatalytic reaction in aqueous solution. Furthermore, any impurities are not observed on the XRD pattern of the spent catalyst, which also supports the stability of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 (Fig. S8†). Rates of gas evolution (eqn (1)-(3)) and reaction selectivity toward CO evolution (eqn (4)) over bare ZnGa<sub>2</sub>O<sub>4</sub> catalysts (without cocatalysts) are represented in Fig. 7. Both ZnGa<sub>2</sub>O<sub>4</sub> catalysts work as photocatalysts for CO2 reduction along with evolving gaseous products by reduction and oxidation in a stoichiometric ratio,  $(H_2 + CO)/O_2 = 2.0$ . This further supports that the formation of CO over both ZnGa2O4 catalysts is derived from not a decomposition of contaminated organic compounds but photocatalytic conversion of introduced CO<sub>2</sub> molecules.<sup>34</sup>

$$H_2O + e^- \rightarrow \frac{1}{2}H_2 + OH^-$$
 (1)

$$CO_2 + 2H^+ + 2e^- \rightarrow CO + H_2O$$
 (2)

$$H_2O + 2h^+ \rightarrow \frac{1}{2}O_2 + 2H^+$$
 (3)

Reaction selectivity toward CO evolution (%)

$$= \frac{\text{CO mol}}{\text{H}_2 \text{ mol} + \text{CO mol}} \times 100 \tag{4}$$

There is no difference between two photocatalysts in the formation rates of oxidation product  $(O_2)$  and sum of reduction products  $(H_2 + CO)$ . The rates of gas evolution do not degrade during photocatalytic reaction for 5 h for both photocatalysts. It is interesting to note that the clear difference is observed in the reaction selectivity toward the CO evolution between bare AMH-derived  $ZnGa_2O_4$ -700 (48.0%) and bare standard  $ZnGa_2O_4$  (20.3%). Energy gap  $(E_g)$  estimated by UV-Vis spectroscopy,

crystallite size, and specific surface area of  $ZnGa_2O_4$  catalysts are summarized in Fig. S9 and Table S2.† There can be seen no relationship between these parameters and reaction selectivity toward CO evolution. More clearly, a high reaction selectivity toward CO evolution with a stoichiometric ratio,  $(H_2 + CO)/O_2 = 2.0$ , is observed even in the case of AMH-derived  $ZnGa_2O_4$ -900 (47.3%) whose  $E_g$  and  $S_{BET}$  are comparable to and smaller than standard  $ZnGa_2O_4$ , respectively. As discussed in the previous section,  $CO_2$  adsorption capacity per unit surface area of catalysts is larger for AMH-derived  $ZnGa_2O_4$ -700. The high reaction selectivity toward CO evolution over AMH-derived  $ZnGa_2O_4$ -700 can be reasonably explained by the high affinity for  $CO_2$  of AMH-derived  $ZnGa_2O_4$ -700.

#### Photocatalytic CO<sub>2</sub> reduction over Ag-loaded ZnGa<sub>2</sub>O<sub>4</sub>

It has been well-known that metal co-catalysts, including Ag NP, are capable to reduce the recombination between excited electrons and holes. 35,36 Fig. 8(a) shows the rates of gas evolution for  $H_2$ ,  $O_2$  and CO, and the reaction selectivity toward CO evolution over AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 with Ag co-catalyst at various loadings. The rate of H2 evolution decreases with increasing the loaded amount of Ag co-catalyst. This trend is corresponding to those demonstrated in previous reports.24,37,38 Ag was reported to work as a preferential active sites for CO2 reduction and thereby inhibits H<sub>2</sub> evolution with increasing coverage with Ag, resulting in enhanced reaction selectivity toward CO evolution. The maximum activity for CO evolution (32.3  $\mu$ mol h<sup>-1</sup>) could be achieved at 0.05 wt% of Ag co-catalyst with a drastically improved reaction selectivity toward CO evolution (75.9%). Compared to a previous ZnGa2O4 catalyst with an optimized Ag loading of 1 wt%,24 95% of Ag can be cut down in the present case, thanks to the high affinity for CO2 of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700. Fig. 8(b) shows a TEM image of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 at Ag loading of 0.1 wt%. The surface of AMHderived ZnGa<sub>2</sub>O<sub>4</sub>-700 is partially covered by dispersedly-loaded Ag NPs. Fig. 8(c) represents a schematic illustration explaining the relationship between surface properties and photocatalytic activity toward CO2 reduction. The surface of AMHderived ZnGa<sub>2</sub>O<sub>4</sub>-700 with a homogeneous distribution of Zn and Ga works as an efficient CO2 absorber and concentrate CO2 to be reduced. The preferential adsorption of CO2 on AMHderived ZnGa2O4-700, evidenced by CO2-TPD measurement (Fig. 3(b)), allows for the photocatalytic reduction of CO<sub>2</sub> at catalytic active sites, vicinity of Ag co-catalysts, in a more selective manner even at a low Ag-loading.

In summary, the present work has demonstrated the formation of desirable surfaces on complex metal oxides by using precursors of interdispersed nanometric hydroxides. ZnGa<sub>2</sub>O<sub>4</sub> was chosen as a representative system to demonstrate the present concept for yielding metal oxide photocatalysts with an enhanced catalytic activity originated from a high surface basicity. The scheme of using NPs as precursors is further expected to be available for designing a wide range of metal oxide catalysts with nano/macrotextures by integrating with the nano building block approach.<sup>20,22,39</sup>

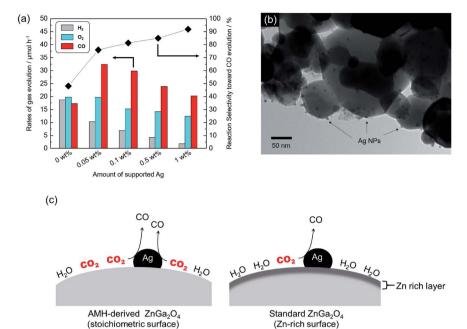


Fig. 8 (a) Rates of gas evolution for  $H_2$  (grey),  $O_2$  (sky blue) and CO (red) and reaction selectivity toward CO evolution over Ag-loaded AMH-derived  $ZnGa_2O_4$ -700 at different Ag loadings. (b) TEM image of Ag-loaded AMH-derived  $ZnGa_2O_4$ -700 with 0.1 wt% of Ag co-catalyst. (c) Schematic illustration of photocatalytic CO<sub>2</sub> reduction over AMH-derived  $ZnGa_2O_4$  (left) and standard  $ZnGa_2O_4$  (right) with Ag loading.

#### Conclusions

The metal hydroxides precursor (Zn-Ga AMH) with a large hetero-interfaces of Zn(OH)2 and Ga(OH)3 NPs was prepared through an epoxide mediated alkalization. ZnGa<sub>2</sub>O<sub>4</sub> catalysts as a single phase were synthesized using the Zn-Ga AMH precursor. Surface analysis with Hammett indicators reveals that AMHderived ZnGa<sub>2</sub>O<sub>4</sub> catalysts exhibit the stronger base strength even after the calcination at high temperature, ≥700 °C, compared to ZnGa<sub>2</sub>O<sub>4</sub> prepared through a solid phase reaction. CO<sub>2</sub>-TPD measurements revealed that the peak at 94 °C, originated from desorption of CO<sub>2</sub>, was observed only for the TPD curve of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700, suggesting that the surface of AMH-derived ZnGa<sub>2</sub>O<sub>4</sub> has a higher affinity and a stronger adsorptive nature for CO2 than standard ZnGa2O4. Structural analysis by XPS reveals that AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 has a surface of the stoichiometric composition, resulting in a higher affinity for CO<sub>2</sub> than standard ZnGa<sub>2</sub>O<sub>4</sub>. The bare AMH-derived ZnGa<sub>2</sub>O<sub>4</sub>-700 with a high affinity for CO<sub>2</sub> exhibits the highest reaction selectivity toward the CO2 reduction (48.0%) among previously-reported co-catalysts-free metal oxide catalysts for the photocatalytic conversion of CO<sub>2</sub> with liquid H<sub>2</sub>O. Additionally, the loading amount of Ag co-catalyst decreased by 95% due to the higher affinity for CO<sub>2</sub>. Based on these insights obtained in this representative ZnGa<sub>2</sub>O<sub>4</sub> system, the present scheme using interdispersed hydroxide nanoparticles will pave the way to general method to tune the surface properties of metal oxide catalysts.

#### Conflicts of interest

There are no conflicts to declare.

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#### Notes and references

- 1 Y. Liu, G. Zhao, D. Wang and Y. Li, Natl. Sci. Rev., 2015, 2, 150.
- 2 K. Li, B. Peng and T. Peng, ACS Catal., 2016, 6, 7485.
- 3 J. L. White, M. F. Baruch, J. E. Pander III, Y. Hu, I. C. Fortmeyer, J. E. Park, T. Zhang, K. Liao, J. Gu, Y. Yan, T. W. Shaw, E. Abelev and A. B. Bocarsly, *Chem. Rev.*, 2015, 115, 12888.
- 4 Z. Wang, K. Teramura, Z. Huang, S. Hosokawa, Y. Sakata and T. Tanaka, *Catal. Sci. Technol.*, 2016, **6**, 1025.
- 5 I. Papadas, J. A. Christodoulides, G. Kioseoglou and G. S. Armatas, *J. Mater. Chem. A*, 2015, 3, 1587.
- 6 K. Maeda and K. Domen, J. Phys. Chem. Lett., 2010, 1, 2655.
- 7 E. Santacesaria, G. M. Vicente, M. Di Serio and R. Tesser, *Catal. Today*, 2012, **195**, 2.

- 8 K. Iizuka, T. Wato, Y. Miseki, K. Saito and A. Kudo, *J. Am. Chem. Soc.*, 2011, 133, 20863.
- 9 Y. Sakata, Y. Matsuda, T. Yanagida, K. Hirata, H. Imamura and K. Teramura, *Catal. Lett.*, 2008, **125**, 22.
- 10 Y. Wei, X. Wu, Y. Zhao, L. Wang, Z. Zhao, X. Huang, J. Liu and J. Li, *Appl. Catal.*, *B*, 2018, **236**, 445.
- 11 Y. Zhao, Y. Wei, X. Wu, H. Zheng, Z. Zhao, J. Liu and J. Li, *Appl. Catal.*, *B*, 2018, **226**, 360.
- 12 Z. B. Todorović, O. S. Stamenković, I. S. Stamenković, J. M. Avramović, A. V. Veličković, I. B. Banković-Ilić and V. B. Veljković, *Fuel*, 2013, **107**, 493.
- 13 Q. Liu, D. Wu, Y. Zhou, H. Su, R. Wang, C. Zhang, S. Yan, M. Xiao and Z. Zou, ACS Appl. Mater. Interfaces, 2014, 6, 2356.
- 14 S. C. Yan, S. X. Ouyang, J. Gao, M. Yang, J. Y. Feng, X. X. Fan, L. J. Wan, Z. S. Li, J. H. Ye, Y. Zhou and Z. G. Zou, *Angew. Chem., Int. Ed.*, 2010, 49, 6400.
- M. Zhao, Y. Gu, P. Chen, Z. Xin, H. Zhu, B. Wang, K. Zhu,
  S. Yan and Z. Zou, J. Mater. Chem. A, 2019, 7, 9316.
- 16 X. Wu, C. Wang, Y. Wei, J. Xiong, Y. Zhao, Z. Zhao, J. Liu and J. Li, J. Catal., 2019, 377, 309.
- 17 R. Abe, J. Photochem. Photobiol., C, 2010, 11, 179.
- 18 C. Wang, Y. Zhao, H. Xu, Y. Li, Y. Wei, J. Liu and Z. Zhao, *Appl. Catal.*, *B*, 2020, **263**, 118314.
- 19 J. Zhu and X. Lin, J. Colloid Interface Sci., 1997, 196, 110.
- 20 Y. Tokudome, T. Morimoto, N. Tarutani, P. D. Vaz, C. D. Nunes, V. Prevot, G. B. Stenning and M. Takahashi, ACS Nano, 2016, 10, 5550.
- 21 Y. Tokudome, M. Fukui, S. Iguchi, Y. Hasegawa, K. Teramura, T. Tanaka, M. Takemoto, R. Katsura and M. Takahashi, J. Mater. Chem. A, 2018, 6, 9684.
- 22 N. Tarutani, Y. Tokudome, M. Jobbágy, F. A. Viva, G. J. A. A. Soler-Illia and T. Masahide, *Chem. Mater.*, 2016, 28, 5606.
- 23 N. Tarutani, Y. Tokudome, M. Jobbágy, G. J. A. A. Soler-Illia and M. Takahashi, *J. Mater. Chem. A*, 2019, 7, 25290.

- 24 W. Zheng, T. Kentaro, H. Saburo and T. Tsunehiro, J. Mater. Chem. A, 2015, 3, 11313.
- 25 E. G. Alexander, M. T. Thomas, H. S. Joe Jr, F. P. John, W. H. Lawrence and L. S. Randall, *Chem. Mater.*, 2001, 13, 999
- 26 E. A. Davis and N. F. Mott, Philos. Mag., 1970, 22, 903.
- 27 J. L. Shumaker, C. Crofcheck, S. A. Tackett, E. Santillan-Jimenez and M. Crocker, *Catal. Lett.*, 2007, **115**, 56.
- 28 W. Xie and H. Li, J. Mol. Catal. A: Chem., 2006, 255, 1.
- 29 G. S. Thomas and P. V. Kamath, *Solid State Sci.*, 2006, 8, 1181.
- 30 H.-Y. Zeng, X. Deng, Y.-J. Wang and K.-B. Liao, *AIChE J.*, 2009, 55, 1229.
- 31 G. A. Caravaggio, C. Detellier and Z. Wronski, *J. Mater. Chem.*, 2001, 11, 912.
- 32 M. Vucelic, W. Jones and G. D. Moggridge, *Clays Clay Miner.*, 1997, 45, 803.
- 33 S. Cadars, G. r. Layrac, C. Gérardin, M. l. Deschamps, J. R. Yates, D. Tichit and D. Massiot, *Chem. Mater.*, 2011, 23, 2821.
- 34 K. Teramura and T. Tanaka, Phys. Chem. Chem. Phys., 2018, 20, 8423.
- 35 J. Yang, D. Wang, H. Han and C. Li, Acc. Chem. Res., 2013, 46, 1900.
- 36 Y. Liu, S. Yang, S. Zhang, H. Wang, H. Yu, Y. Cao and F. Peng, *Int. J. Hydrogen Energy*, 2018, 43, 5551.
- 37 K. Teramura, H. Tatsumi, Z. Wang, S. Hosokawa and T. Tanaka, *Bull. Chem. Soc. Jpn.*, 2015, **88**, 431.
- 38 Z. Wang, K. Teramura, S. Hosokawa and T. Tanaka, *Appl. Catal.*, *B*, 2015, **163**, 241.
- 39 N. Tarutani, Y. Tokudome, M. Jobbágy, G. J. A. A. Soler-Illia, Q. Tang, M. Müller and M. Takahashi, *Chem. Mater.*, 2018, 31, 322.