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Investigation on dispersion properties of CO₂ and ester solvent mixtures using *in situ* FTIR spectroscopy†

Zihao Yang,^{‡,*a} Taiheng Yin,[‡] Fengfan Zhang,^a Wei Wu,^a Meiqin Lin,[‡] Zhaoxia Dong^{ab} and Juan Zhang^{‡a}

To study the microscopic dispersion state of CO₂ in different ester solvents, the solubility, volume expansion coefficients and *in situ* Fourier transform infrared (FTIR) spectra of the CO₂–ester system were measured. The results show that the solubility and expansion coefficient of CO₂ in ester solvents decreases as the hydrocarbon chain increases. As the pressure increases, the infrared absorption peaks of CO₂ and the functional groups characteristic of ester molecules shift, indicating that CO₂ molecules interact with ester molecules and that CO₂ would destroy the interactions between the ester molecules. The hydrocarbon chain length of the ester molecules has a significant effect on the infrared absorption peak of the CO₂–ester system. As the hydrocarbon chain length increases, the CO₂ absorption peak shift and peak shift of the carbonyl groups in the ester gradually decrease.

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1. Introduction

It is easy to prepare supercritical CO₂. Supercritical CO₂ is very dense, highly soluble, chemically inert, safe and nontoxic and can be separated at room temperature; thus, it has been widely used in supercritical fluid extraction.^{1–7} Meanwhile, CO₂ has been used to improve oil recovery and has played an important role in petroleum production, especially in low permeability oilfields.^{8–11} The dissolution of CO₂ in crude oil and the resulting volume expansion are considered to be the two major mechanisms responsible for improving oil recovery.^{12–16} It is well known that both supercritical fluid extraction and CO₂ flooding are essentially equilibrium processes that occur between CO₂ and organic liquid systems under high temperatures and high pressures. Therefore, many researchers have studied the CO₂–organic liquid phase and accumulated various experimental data on the phases of CO₂ and the organic liquid systems.^{17–24}

Our recent research findings have shown that, when CO₂ molecules enter an organic liquid, instead of not dissolving in the organic liquid, the CO₂ molecules are dispersed in the organic liquid in the form of molecular aggregates.^{25,26} CO₂ molecules are dispersed in the organic liquid and have unique

microscale morphologies. Thus, a molecular dynamics technique was used to study the radial distribution function of each molecule in mixed systems containing CO₂ and an organic liquid, which included *n*-hexane, cyclohexane, toluene and ethanol, and simulations were performed for increasing pressures, revealing the microscopic morphology of dispersed CO₂ in these four organic liquids. It is believed that, in organic liquids, the dispersion state of the CO₂ molecules (including CO₂ molecule aggregates and aggregates of CO₂ and organic liquid molecules) directly affects the volume expansion of the CO₂–organic liquid system. However, molecular dynamics can only simulate parameters such as the radial distribution function, the distortion distribution function and the interaction energy of the molecules in the system to infer the intermolecular interactions, and thus, direct experimental results cannot be obtained.

As the pressure increases in the simulation, the infrared absorption spectra of the functional groups and hydrocarbon chains of the organic molecules will change due to the influence of the CO₂ molecules. Similarly, due to the effect of the organic liquid molecules, the infrared absorption spectra of CO₂ will also change. Therefore, we can study the microscopic interactions of the molecules in the system with high-temperature and high-pressure *in situ* infrared technology. However, this technique has mainly been used to study the interactions between CO₂ and polymer molecules and between CO₂ and organic powders.^{27–29} The existing experimental method cannot meet the requirements for studying the interaction between CO₂ and organic liquid molecules.^{27–29} Therefore, we have improved the *in situ* infrared device and previously used the improved device

^aUnconventional Petroleum Research Institute, China University of Petroleum (Beijing), Beijing, 102249, People's Republic of China. E-mail: zihao yang@cup.edu.cn; linmq@cup.edu.cn

^bChina University of Geosciences (Beijing), Beijing, 100083, People's Republic of China

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‡ These authors contributed equally to this work.



to measure the infrared absorption peaks of CO₂ and 2-hexanone, hexanal, and 1-hexanol under high pressures.³⁰

The carbon dioxide + ester systems at high pressure are important in the separation process in a wide variety of field such as food, pharmaceutical and related industries.^{31,32} Although the volumetric properties and vapor–liquid equilibrium data for carbon dioxide + ester systems at high pressure have been extensively investigated, its microscopic dispersion states are still mostly uncovered.^{33–37} To further study the CO₂–organic liquid dispersion state, this study measured the solubility and volume expansion coefficient of CO₂ dispersed in esters with different hydrocarbon chain lengths under different pressures at 308.15 K and examined the effect of the hydrocarbon chain length on the solubility and volume expansion coefficient of CO₂. In addition, the *in situ* infrared absorption spectra of CO₂–ester systems under different pressure conditions were obtained to study the effects of the hydrocarbon chain length on the infrared absorption spectra of the CO₂–ester systems.

2. Experimental section

2.1. Materials

Carbon dioxide with a purity of 99.8% was purchased from Beijing Jingao Gases Co., Ltd. Ethyl acetate (99.0%), propyl propionate (98.0%) and butyl butyrate (99.5%) were supplied by Shanghai Aladdin Bio-Chem Technology Co., Ltd.

2.2. Experimental instruments and methods

The visible pressure–volume–temperature (PVT) apparatus and *in situ* FTIR apparatus were used for the experiments. The experimental setup is shown in Fig. 1. The main body of the device included an autoclave, a supercharging system and a sampling system. The internal temperature and pressure of the autoclave were monitored by temperature sensors and pressure sensors with accuracies of ± 0.1 °C and ± 0.1 MPa, respectively. The volumetric accuracy of the autoclave was ± 0.01 mL. The high-pressure *in situ* infrared liquid sample cell was heated by an internal thermocouple and controlled by an external controller. The maximum operating temperature was 200 °C, and the temperature accuracy was ± 0.1 °C. The highest operational pressure was 10 MPa, and the pressure accuracy was 0.1 MPa. Infrared absorption data were collected from 900 cm^{−1} to 4000 cm^{−1}. The detailed device information and operating procedures can be found in our previously published papers.^{18,30} Briefly, a known volume ($V_0 = 30$ mL) of ester solvent was first injected into the vacuumed PVT cell, and CO₂ was pressurized into the cell. After the system reached equilibrium, the liquid phase volume (V_1) was calculated from the image captured by the camera. Then, the mixed liquid was injected slowly into the optical cell, and the infrared spectrum of the samples was obtained by using a Bruker VERTEX 80v infrared spectrometer. Finally, the mixed liquid was taken from the cell and charged into a small steel vessel that has already been vacuumed and weighed (M_0), and the pressure of the cell is kept constant by moving the piston when discharging the organic solvent out of the cell. The mass of CO₂ dissolved in the ester solvent was calculated using the

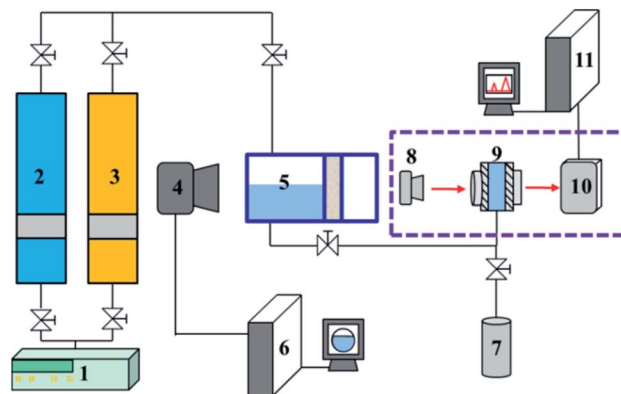


Fig. 1 Schematic of the PVT and *in situ* FTIR apparatus ((1) constant flow pump; (2) CO₂ gas bottle; (3) piston cylinder; (4) camera; (5) visible PVT cell; (6) computer; (7) little steel vessel; (8) infrared source; (9) sample optical cell; (10) infrared receptor; (11) computer).

weight difference method: the mass of the steel vessel containing organic solvents and CO₂ (M_1) minus the mass of the vessel after releasing CO₂ to atmosphere (M_2). The solubility (mole fraction) of CO₂ was also calculated using these data. The volume expansion coefficient (N) of ester solvent was calculated by $N = V_1/V_0$. The measurements are repeated three times, and the results are presented as the average of the replicates.

3. Results and discussion

3.1. The solubility and volume expansion coefficient of CO₂ in the ester liquids

Fig. 2 shows the solubility and volume expansion coefficient of CO₂ in ethyl acetate, propyl propionate and butyl butyrate under different pressure conditions at 308.15 K. The CO₂ solubility and volume expansion coefficients of CO₂ and ethyl acetate, propyl propionate, and butyl butyrate increase with increasing pressure. To our knowledge, literature vapor–liquid equilibrium data for the binary mixture of CO₂ and ethyl acetate, propyl propionate, and butyl butyrate at 308.15 K are not available. The predictive Soave–Redlich–Kwong (PRSK) equation of state (EOS) was used to evaluate the vapor–liquid equilibrium behavior of CO₂ and ethyl acetate mixtures at 308.15 K.³⁸ There is a good agreement between the experimental data obtained here and the theoretical data obtained using the PRSK equation of state. Under the same experimental conditions, the solubility of CO₂ and the volume expansion coefficient of the CO₂–ester liquid system with different hydrocarbon chain lengths both decrease in the following order: ethyl acetate > propyl propionate > butyl butyrate. This result indicates that the hydrocarbon chain length has a relatively large impact on the solubility of CO₂ in the ester liquids and the volume expansion coefficient of the CO₂–ester liquid system.

Previous studies have shown that the solubility of CO₂ in ester liquids is closely related to the intermolecular forces between CO₂ molecules, the intermolecular forces between CO₂ and ester molecules and the intermolecular forces between ester molecules.^{17,18} Ester liquids with longer chain lengths have larger contact areas for intermolecular interactions and

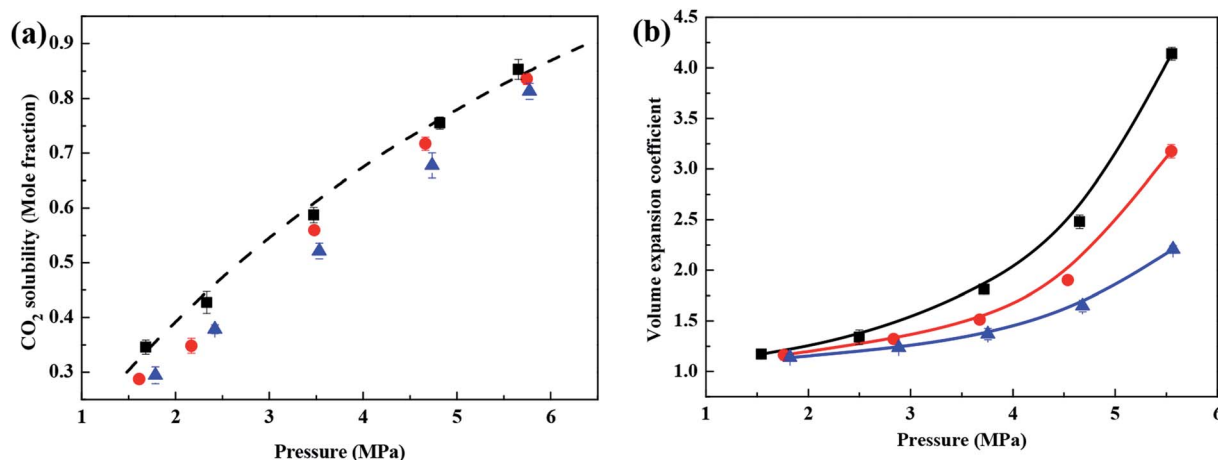


Fig. 2 (a) CO₂ solubility and (b) volume expansion coefficient of CO₂-ester liquids systems under different pressure conditions. (■) ethyl acetate, (●) propyl propionate, (▲) butyl butyrate, (---) PSRK EOS prediction of ethyl acetate.

stronger intermolecular forces. Under the same pressure and temperature, these stronger intermolecular forces prevent CO₂ from entering the ester liquid, leading to CO₂ being less soluble in ester liquids with longer hydrocarbon chains. On the other hand, the evaporation enthalpy of a solvent can also indirectly reflect the stability of intermolecular interactions.^{30,39} The evaporation enthalpy of ethyl acetate, propyl propionate and butyl butyrate are 35.62, 42.14 and 51.12 kJ mol⁻¹ respectively at 298 K.⁴⁰⁻⁴³ Under the same conditions, the evaporation enthalpy decreases in the order butyl butyrate > propyl propionate > ethyl acetate, indicating that the molecular interactions of butyl butyrate are the most stable, followed by propyl propionate and ethyl acetate. This result also shows that, under the same conditions, CO₂ can more easily enter the liquid phase of ethyl acetate, thus making CO₂ more soluble in ethyl acetate than in the other two systems.

Esters with different hydrocarbon chain lengths have different distances between the ester molecules. Under the combined action of intermolecular forces, this difference in distance also causes different microscopic dispersions of CO₂ in the ester liquid, which will have a relatively large impact on the volume of the liquid system. Combined with the results of Fig. 2b, this shows that, when the temperature is constant, under the same pressure, the volume expansion is closely related to the magnitude of the intermolecular forces between the molecules of the organic liquid. The stronger the intermolecular force is, the lower the solubility of CO₂ and the smaller the expansion coefficient.^{25,26} The abovementioned results indicate that the molecular structure, intermolecular forces and microscopic dispersion state of the organic liquids are the key factors affecting the solubility of CO₂ and the corresponding volume expansion coefficient of the system.

3.2. *In situ* FTIR absorption spectra of the CO₂-ester liquids systems

The *in situ* FTIR technique can be used to detect the sample changes as a function of the environment, time, temperature, and pressure. These influencing factors can cause certain

regular patterns of the change in the intermolecular force and force constant of the molecules. These patterns can be reflected by *in situ* FTIR absorption peak shifts. When the intermolecular interaction is weakens, the force constant of the chemical bond will increase, and the corresponding absorption peak shifts to a higher wavenumber.^{44,45} In addition, when the concentration of the detected sample is relatively low, the intensity of the absorption peak is weak; when the concentration of the sample is relatively high, the intensity of the absorption peak is high.

Fig. 3a shows the FTIR spectra of raw CO₂ and the CO₂-ethyl acetate system, which were obtained at 308.15 K and at atmospheric pressure and 7.39 MPa. Specifically, the absorption peak at 1745 cm⁻¹ is characteristic of the ethyl acetate carbonyl ($\nu_{\text{C=O}}$) groups; the absorption peaks at 3704 cm⁻¹, 3600 cm⁻¹ and 2314 cm⁻¹ are characteristic of CO₂;³⁰ the absorption peak at 2989 cm⁻¹ corresponds to the stretching vibration of -CH₃; the absorption peaks at 1490 cm⁻¹ and 1350 cm⁻¹ are attributed to the bending vibrations of -CH₂ and -CH₃. At 7.39 MPa, intense CO₂ absorption peaks are observed at 3704 cm⁻¹, 3600 cm⁻¹ and 2314 cm⁻¹ in the CO₂-ethyl acetate system and no such peaks are detected at atmospheric pressure. This finding indicates that, when the pressure increases from atmospheric pressure to 7.39 MPa, the CO₂ concentration in the liquid phase significantly increases. This also shows that more CO₂ is dissolved in ethyl acetate at 7.39 MPa than at atmospheric pressure, which confirms that the solubility of CO₂ in ethyl acetate increases with increasing pressure.

Fig. 3a also shows that, when the pressure increases from atmospheric pressure to 7.39 MPa, the intensity of the $\nu_{\text{C=O}}$ absorption peak at 1745 cm⁻¹ and the intensity of the -CH- absorption peak at 2985 cm⁻¹ are significantly weakened. This occurs because, when the pressure rises, more CO₂ is dissolved in the ethyl acetate liquid, thus diluting the ethyl acetate liquid, causing the concentration of the ethyl acetate liquid to decrease and the intensity of the ethyl acetate absorption peak to decrease.

Fig. 3b shows the FTIR spectra of the $\nu_{\text{C=O}}$ absorption peak of ethyl acetate in the CO₂-ethyl acetate system from atmospheric pressure to 7.39 MPa at 308.15 K. When the liquid



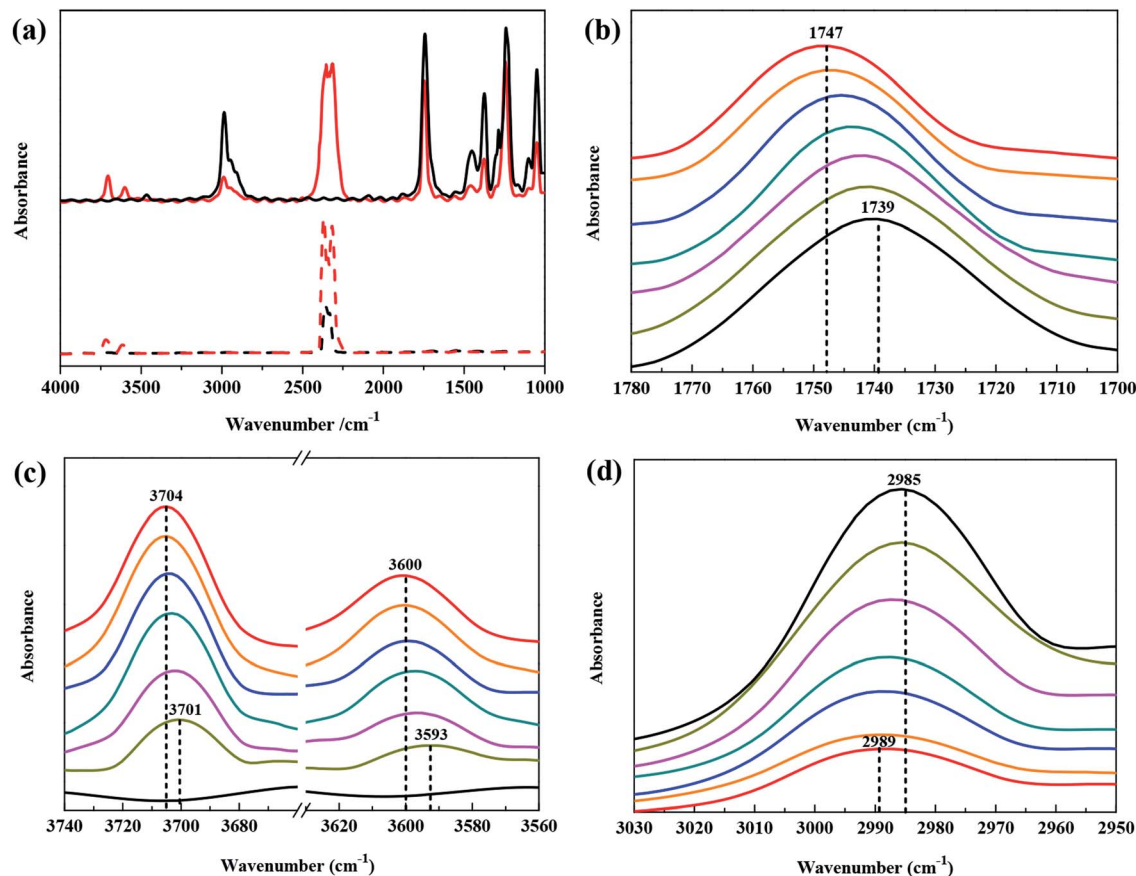


Fig. 3 FTIR spectra of CO₂–ethyl acetate system under different pressure conditions: (a) full spectrum; (b) the $\nu_{\text{C=O}}$ region of ethyl acetate; (c) the combination modes $2\nu_2 + \nu_3$ and $\nu_1 + \nu_3$ regions of CO₂ molecules; (d) the $\nu_{\text{-CH}_3}$ region of ethyl acetate. (—) ambient pressure, (—) 1.89 MPa, (—) 3.72 MPa, (—) 4.67 MPa, (—) 5.65 MPa, (—) 6.56 MPa, (—) 7.39 MPa, (---) raw CO₂ at ambient pressure, (---) raw CO₂ at 7.40 MPa.

system is under atmospheric pressure, the position of the carbonyl absorption peak is 1739 cm^{-1} ; when the pressure rises to 7.39 MPa , the position of the carbonyl absorption peak gradually shifts to 1747 cm^{-1} . As the pressure is increased, the position of the carbonyl absorption peak shifts to a high wavenumber by 8 cm^{-1} . A decreased intermolecular force will cause an absorption peak to shift to a high wavenumber in the *in situ* FTIR spectrum.^{44–46} Therefore, the abovementioned results indicate that, in the process of injecting CO₂ and as the pressure increases, more CO₂ molecules enter the ethyl acetate liquid, and the intermolecular force between the ethyl acetate molecules decreases, resulting in an increase in the force constant of the carbonyl bond. As a result, the position of the carbonyl absorption peak shifts toward a high wavenumber.

Fig. 3c shows the FTIR spectra (the combination modes $2\nu_2 + \nu_3$ and $\nu_1 + \nu_3$ stretching vibrations of the CO₂ molecule) of the CO₂–ethyl acetate system at 308.15 K when the pressure increased from atmospheric pressure to 7.39 MPa . Fig. 3c shows that, at 1.89 MPa , the positions of the $2\nu_2 + \nu_3$ and $\nu_1 + \nu_3$ CO₂ absorption peaks are 3701 cm^{-1} and 3593 cm^{-1} , respectively. When the pressure is increased to 7.39 MPa , the positions of these two absorption peaks shift to 3704 cm^{-1} and 3600 cm^{-1} . This result indicates that, when the pressure is increased from atmospheric pressure to 7.39 MPa , the absorption peaks of the

CO₂–ethyl acetate system at 3700 cm^{-1} and 3600 cm^{-1} shift to higher wavenumbers by 3 cm^{-1} and 7 cm^{-1} , respectively. Due to an increase in the concentration, the FTIR absorption peak of pure CO₂ will increase with an increase in the pressure, but the position of the peak will not change.⁴⁷ When the pressure is 7.5 MPa , the absorption peak positions of pure CO₂ at these two locations are 3718 cm^{-1} and 3614 cm^{-1} .³⁰ Therefore, in the CO₂–ethyl acetate system, with an increase in the pressure, the interaction between the ethyl acetate molecules and CO₂ molecules leads to an increase in the force constant of CO₂, and the position of the FTIR CO₂ absorption peak shifts to a higher wavenumber.

Fig. 3d shows the absorption peaks (at approximately 2900 cm^{-1}) attributed to the -CH_3 groups in ethyl acetate in the CO₂–ethyl acetate system at 308.15 K when the pressure increases from atmospheric pressure to 7.39 MPa . These -CH_3 peaks are located at 2985 cm^{-1} and 2989 cm^{-1} at atmospheric pressure and at 7.39 MPa , respectively. As the pressure increases, the -CH_3 absorption peak shifts to a high wavenumber by 4 cm^{-1} . This result indicates that, with increasing pressure, more CO₂ enters the liquid molecules of ethyl acetate, which not only affects the interaction between the ethyl acetate molecules but also increases the force constant of the C–H bond

Table 1 The variation of the functional group high frequency offset of CO₂-different ester system with chain length under the same conditions

Ester type	CO ₂ (3700 cm ⁻¹) shift/cm ⁻¹	CO ₂ (3600 cm ⁻¹) shift/cm ⁻¹	-CH ₃ (2900 cm ⁻¹) shift/cm ⁻¹	C=O (1700 cm ⁻¹) shift/cm ⁻¹
Ethyl acetate	3	7	4	8
Propyl propionate	3	5	2	5
Butyl butyrate	1	2	—	3

in the -CH₃ group. Therefore, the infrared absorption peak of -CH₃ shifts toward a high wavenumber.

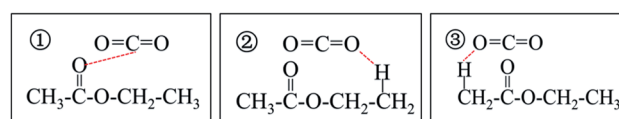
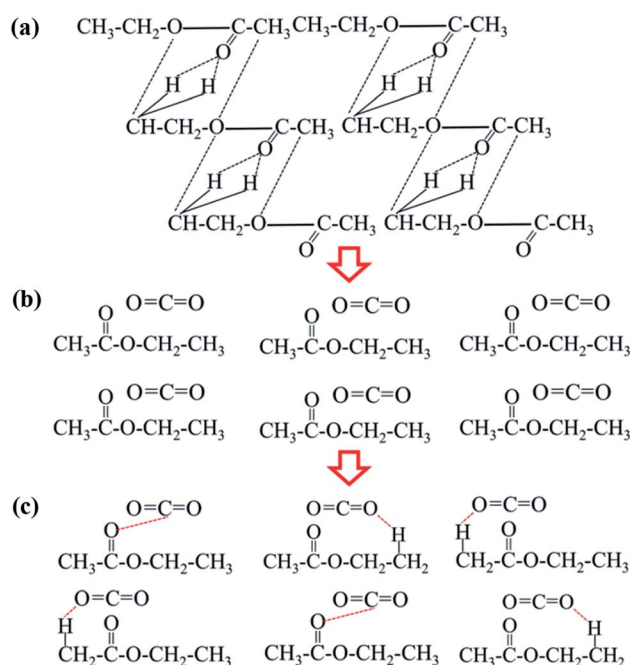
Fig. S1 and S2† show the FTIR absorption spectra of the CO₂-propyl propionate system and CO₂-butyl butyrate system under different pressure conditions, respectively. The infrared spectra analysis of the three systems under the same conditions shows that, for the same pressure variation range, the length of the hydrocarbon chains has a significant impact on the shift of the absorption peaks of various functional groups of the system, as shown in Table 1. Table 1 shows that, under the same pressure variation condition, as the ester hydrocarbon chain length increases, the shift of the CO₂ absorption peak at 3600 cm⁻¹ and the shift of the carbonyl absorption peak at 1700 cm⁻¹ gradually decrease. The solubility and volume expansion analyses show that the ester chain length greatly affects the solubility of CO₂ in the ester and the volume expansion coefficient of the CO₂-ester system. The longer the chain length, the more difficult it is for CO₂ to dissolve and the smaller the volume expansion coefficient. The *in situ* infrared spectra show that the CO₂ absorption peak shift and carbonyl absorption peak shift are smaller in the esters with longer hydrocarbon chains, indicating that the longer the chain length, the more unfavorable it is for CO₂ to disperse in the ester liquid and the more difficult it is for CO₂ to enter the ester liquid to break the structure between the ester molecules. This also explains the lower solubility of CO₂ in long-chain esters under the same conditions and the smaller volume expansion of the CO₂-long-chain ester system.

3.3. Microscopic dispersion state of CO₂ in the ester liquids

The results of this study show that, as the pressure increases, the infrared absorption peak of CO₂ and the absorption peaks characteristic of the ester functional groups shift, which indicates that CO₂ is likely to interact with ester molecules. In addition, the interactions between CO₂ and ester molecules increase with the increasing of pressure. The CO₂ and ester molecules can have many different interaction modes.^{48–50} The C atoms in the CO₂ molecule and the O atom in the carbonyl group of the ester molecule interact *via* Lewis acid–Lewis base (LA–LB) modes. A proton on the α-C on the alcohol side of the ester molecule and an O atom in CO₂ interact in the form of C–H···O. A proton on the α-C on the carbonyl side of the ester molecule and an O atom in CO₂ interact in the form of C–H···O. Taking ethyl acetate as an example, a specific interaction between the CO₂ and ethyl acetate molecules is shown in Fig. 4.

Based on the *in situ* infrared data analysis of CO₂ + ethyl acetate system under different pressures, the possible dispersion process of CO₂ in ethyl acetate can be inferred as follows

(Fig. 5). In the ethyl acetate liquid, the ethyl acetate molecules form a network structure with three low-stability interactions (Fig. 5a). As the pressure increases, the solubility of CO₂ in the ethyl acetate liquid continuously increases, and the carbonyl absorption peak of the ethyl acetate molecules gradually shifts to a higher wavenumber, and the force constant of the carbonyl group gradually increases, indicating that the interactions between the ethyl acetate molecules gradually weaken. As increasing numbers of CO₂ molecules enter into the ethyl acetate liquid, the distance between the ethyl acetate molecules becomes larger. In the microscopic state, the original network structure of the ethyl acetate molecules is destroyed, and some of the ethyl acetate molecules are present as single molecules in

**Fig. 4** Types of interaction between CO₂ and ethyl acetate molecules.**Fig. 5** Schematic of intermolecular interaction of CO₂ and ethyl acetate from ambient pressure to supercritical conditions: (a) ambient pressure; (b) 2.50 MPa; (c) the supercritical condition of CO₂.

the ethyl acetate system (Fig. 5b). CO₂ molecules form interactions with ethyl acetate through three non-covalent bonds, furthering disassembling the network structure of ethyl acetate. When supercritical conditions are reached, non-covalent bonds form between the CO₂ and ethyl acetate molecules, resulting in a completely dissociated ethyl acetate network structure (Fig. 5c).

4. Conclusions

In this work, the phase equilibrium data and FTIR spectra for the CO₂ and ester solvents mixtures under different pressures were obtained with a static analytical method using the PVT instrument and improved *in situ* infrared spectrometer under different pressure. At the same temperature, the CO₂ solubility and volume expansion coefficient of the CO₂-ester liquid system increase with increasing pressure. Longer hydrocarbon chains are associated with greater intermolecular forces, which can decrease the solubility of CO₂ in the ester liquid and decrease the volume expansion of the system. For the CO₂-ester liquid system, as the pressure increases, the infrared absorption peaks of CO₂ and the carbonyl group of the ester molecules gradually shift to higher wavenumbers, and the longer the hydrocarbon chain is, the smaller the shift. The microscopic dispersion state of CO₂ in ester solvents was further described based on the experimental results from the perspective of intermolecular interactions of the CO₂ molecules and ester molecules. Under supercritical CO₂ conditions, CO₂ molecules form interactions with ethyl acetate through three non-covalent bonds, resulting in the original network structure of the ethyl acetate molecules is destroyed. This study will enhance the understanding of the dispersion properties of CO₂ and ester solvents mixtures and facilitate their applications.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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