


Cite this: *RSC Adv.*, 2020, 10, 13642

# Surface double coating of a $\text{LiNi}_a\text{Co}_b\text{Al}_{1-a-b}\text{O}_2$ ( $a > 0.85$ ) cathode with $\text{TiO}_x$ and $\text{Li}_2\text{CO}_3$ to apply a water-based hybrid polymer binder to Li-ion batteries†

Tatsuya Watanabe,<sup>a</sup> Kouji Hirai,<sup>a</sup> Fuma Ando,<sup>a</sup> Shoudai Kurosumi,<sup>b</sup> Shinsaku Ugawa,<sup>b</sup> Hojin Lee,<sup>b</sup> Yuta Irii,<sup>c</sup> Fumihiko Maki,<sup>c</sup> Takao Gunji,<sup>d</sup> Jianfei Wu,<sup>d</sup> Takao Ohsaka<sup>e</sup> and Futoshi Matsumoto<sup>\*,a</sup>

Recently a water-based polymer binder has been getting much attention because it simplifies the production process of lithium ion batteries (LIBs) and reduce their cost. The surface of  $\text{LiNi}_a\text{Co}_b\text{Al}_{1-a-b}\text{O}_2$  ( $a > 0.85$ , NCA) cathode with a high voltage and high capacity was coated doubly with water-insoluble titanium oxide ( $\text{TiO}_x$ ) and  $\text{Li}_2\text{CO}_3$  layers to protect the NCA surface from the damage caused by contacting with water during its production process. The  $\text{TiO}_x$  layer was at first coated on the NCA particle surface with a tumbling fluidized-bed granulating/coating machine for producing  $\text{TiO}_x$ -coated NCA. However, the  $\text{TiO}_x$  layer could not coat the NCA surface completely. In the next place, the coating of the  $\text{TiO}_x$ -uncoated NCA surface with  $\text{Li}_2\text{CO}_3$  layer was conducted by bubbling  $\text{CO}_2$  gas in the  $\text{TiO}_x$ -coated NCA aqueous slurry on the grounds that  $\text{Li}_2\text{CO}_3$  is formed through the reaction between  $\text{CO}_3^{2-}$  ions and residual  $\text{LiOH}$  on the  $\text{TiO}_x$ -uncoated NCA surface, resulting in the doubly coated NCA particles ( $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles). The  $\text{Li}_2\text{CO}_3$  coating is considered to take place on the  $\text{TiO}_x$  layer as well as the  $\text{TiO}_x$ -uncoated NCA surface. The results demonstrate that the double coating of the NCA surface with  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$  allows for a high water-resistance of the NCA surface and consequently the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particle cathode prepared with a water-based binder possesses the same charge/discharge performance as that obtained with a "water-uncontacted" NCA particle cathode prepared using the conventional organic solvent-based polyvinylidene difluoride binder.

Received 9th January 2020

Accepted 25th March 2020

DOI: 10.1039/d0ra00197j

rsc.li/rsc-advances

## 1. Introduction

In recent years, water-soluble and aqueous polymer binders, *i.e.*, water-based polymer binders, have become of great interest as alternatives to the poly(vinylidene difluoride) (PVdF) binder dissolved in *N*-methyl-2-pyrrolidone (NMP) for the cathodes of lithium ion batteries (LIBs) from the viewpoints of environmentally friendly electrode fabrication processes and reducing

the cost of LIBs.<sup>1–13</sup> However, cathode materials such as  $\text{LiNi}_{0.5}\text{Mn}_{1.5}\text{O}_4$ ,<sup>11</sup>  $\text{LiNi}_a\text{Co}_b\text{Al}_{1-a-b}\text{O}_2$  (NCA)<sup>12</sup> and Li-rich solid-solution layered cathodes,<sup>13</sup> which are promising candidates as next generation positive-electrode active materials with high energy density for LIBs, are not stable in water-based slurry solutions because they contain a small amount of alkaline species such as  $\text{LiOH}$  as a residue in their production process<sup>14</sup> and when they are dispersed in a water-based coating slurry, their surfaces are dissolved and its pH is increased, resulting in the corrosion of the Al foil current collectors and the falling off of active cathode materials from the current collector surfaces.<sup>12</sup> To prevent such a damage of cathode materials some ways have been proposed including the use of buffer agents to inhibit the increase in pH in the water-based slurry<sup>15</sup> and a stainless steel foil current collector<sup>16</sup> and the surface coating of cathode materials by carbon,<sup>11</sup> metal oxides<sup>12</sup> and  $\text{Li}_2\text{CO}_3$ .<sup>17,18</sup>

In a series of our studies on surface coating of cathode materials,<sup>11,12,19</sup> we have found that  $\text{Li}^+$  ions can relatively smoothly pass through the thin layers of carbon,  $\text{Al}_2\text{O}_3$  and  $\text{TiO}_x$  on NCA particles and the thin layer coating of NCA particles by

<sup>a</sup>Department of Materials and Life Chemistry, Kanagawa University, 3-27-1, Rokkakubashi, Kanagawa-ku, Yokohama, Kanagawa 221-8686, Japan. E-mail: fmatsumoto@kanagawa-u.ac.jp

<sup>b</sup>JSR Corporation, 100 Kawajiri-cho, Yokkaichi, Mie 510-8552, Japan

<sup>c</sup>Nihon Kagaku Sangyo Co., Ltd., 1-28-13 Nakane, Soka, Saitama 340-0005, Japan

<sup>d</sup>Qingdao Industrial Energy Storage Research Institute, Qingdao Institute of Bioenergy and Bioprocess Technology, Chinese Academy of Sciences, No. 189 Songling Road, 266101 Qingdao, China

<sup>e</sup>Research Institute for Engineering, Kanagawa University, 3-27-1, Rokkakubashi, Kanagawa-ku, Yokohama, Kanagawa 221-8686, Japan

† Electronic supplementary information (ESI) available. See DOI: 10.1039/d0ra00197j



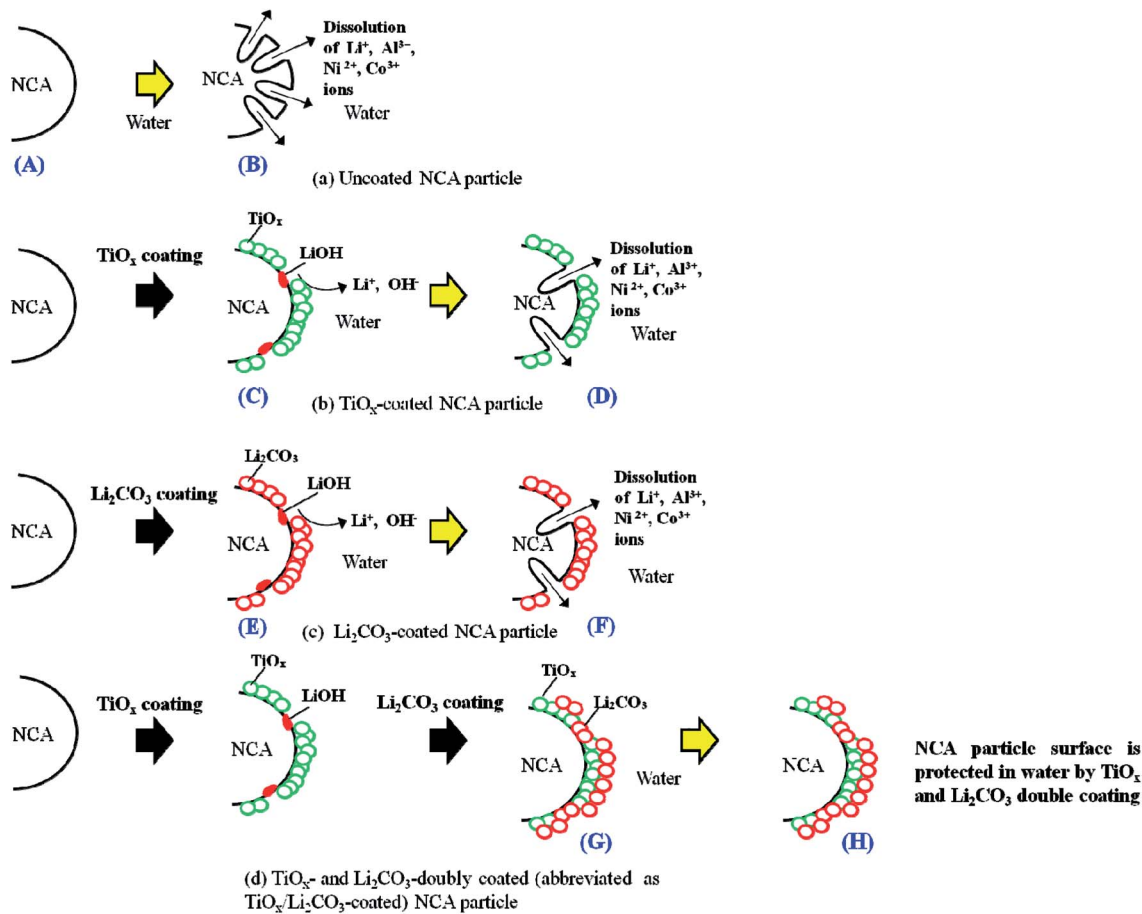


Fig. 1 A schematic illustration of (a) uncoated NCA particle and three types (b–d) of surface modification of NCA particles with  $\text{TiO}_x$ ,  $\text{Li}_2\text{CO}_3$  and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  indicating the different surface water-resistance. (A), (C), (E) and (G) indicate un-,  $\text{TiO}_x$ -,  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles, respectively and (B), (D), (F) and (H) show un-,  $\text{TiO}_x$ -,  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles treated with water, respectively.

$\text{TiO}_x$  significantly suppresses, though not completely, the degradation in charge/discharge cyclability which is caused by contacting their surfaces with water, *i.e.*,  $\text{TiO}_x$ -coated NCA cathode particles possess a water-resistant property when kept in the water-based slurry. The  $\text{TiO}_x$  coating process in this case is a so-called batch process and thus it is not suitable for the mass production of  $\text{TiO}_x$ -coated cathode materials.

Recently, Yanagida *et al.*<sup>17,18</sup> have developed a simple continuous method to decrease the pH value of the NCA cathode aqueous slurry with  $\text{CO}_2$  gas treatment using a cavitation effect in which the NCA particle surfaces are covered with the  $\text{Li}_2\text{CO}_3$  layer formed by reacting the  $\text{LiOH}$  dissolved in the cathode slurry with the  $\text{CO}_2$  gas introduced into it and the  $\text{Li}_2\text{CO}_3$  layer prevents the electrolyte decomposition and reaction of the NCA particle surfaces with the electrolyte, resulting in improvement of the cyclability, coulombic efficiency and high-capacity retention rate of the  $\text{Li}_2\text{CO}_3$ -coated NCA cathode. They have claimed that their  $\text{CO}_2$  gas treatment can be a continuous process for mass production. The  $\text{CO}_2$  gas treatment of cathode particles is thus effective to protect their surface against water<sup>17,20,21</sup> and could be scaled up to the mass production of  $\text{Li}_2\text{CO}_3$ -coated cathode materials. However, it should be also noted that  $\text{Li}_2\text{CO}_3$  is electrochemically insulating

which may block the electronic transport of the  $\text{Li}_2\text{CO}_3$ -coated cathode materials and consequently leads to the capacity degradation due to the accumulation of  $\text{Li}_2\text{CO}_3$  in the interface between the cathode particle surface and electrolyte.<sup>22,23</sup> Thus, a suitable  $\text{Li}_2\text{CO}_3$  layer coating is desirable. In addition, as mentioned later based on our examination on the water-resistance of NCA cathode particles coated with  $\text{Li}_2\text{CO}_3$  layer by the  $\text{CO}_2$  gas treatment,  $\text{CO}_2$  gas-treated NCA samples could not exhibit full charge/discharge capacities because they suffered from a small surface damage (surface dissolution) by contacting with water owing to the uncomplete coating of the whole surface of NCA particles by the  $\text{Li}_2\text{CO}_3$  layer, *i.e.*, the NCA surface coating only by the  $\text{Li}_2\text{CO}_3$  layer was not adequate for the present purpose.

In order to protect the NCA surfaces from the damage caused by contacting them with water during their production process using water-based binder, in this study, we aimed at doubly coating the NCA particle surfaces with  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$  layers, by using a surface coating procedure which may be applicable for the mass production of surface-coated NCA particles for commercially available LIBs, *i.e.*, by at first coating the NCA surface with  $\text{TiO}_x$  layer using a tumbling fluidized-bed granulating/coating machine, which is used to form coating



layers in a wide range of industries including pharmaceuticals, foods and battery materials,<sup>24</sup> (producing  $\text{TiO}_x$ -coated NCA particles which are not coated completely by the  $\text{TiO}_x$  layer) and then by coating the  $\text{TiO}_x$ -coated as well as  $\text{TiO}_x$ -uncoated NCA surfaces with  $\text{Li}_2\text{CO}_3$  layer by bubbling  $\text{CO}_2$  gas in the  $\text{TiO}_x$ -coated NCA aqueous slurry (finally producing the doubly coated NCA particles, abbreviated as  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles), as schematically shown in Fig. 1. We found that the  $\text{TiO}_x$  layer does not coat the NCA surface completely and thus there are some  $\text{TiO}_x$ -uncoated parts, but such  $\text{TiO}_x$ -uncoated surfaces are covered with the subsequent  $\text{Li}_2\text{CO}_3$  layer coating and consequently the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles have a high water-resistance and that the charge/discharge performance of the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode prepared with a water-based binder is significantly superior to those of the  $\text{TiO}_x$ - or  $\text{Li}_2\text{CO}_3$ -coated cathodes and almost comparable to that obtained with “water-uncontacted” NCA cathode prepared using the conventional organic solvent (NMP)-based PVdF binder. The samples of un-,  $\text{TiO}_x$ -,  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles that are prepared and treated with water after the preparation will hereinafter be denoted using the upper-case alphabetic characters of A–H, as shown Fig. 1.

## 2. Experimental

### 2.1 Preparation of $\text{TiO}_x$ -coated NCA cathode material and NCA cathode electrodes

NCA particles (NC-02,  $\text{LiNi}_a\text{Co}_b\text{Al}_{1-a-b}\text{O}_2$  ( $a > 0.85$ )) were provided by Nihon Kagaku Sangyo Co., Ltd., Japan and used without any purification. In order to coat the surface of NCA with  $\text{TiO}_x$  layer, a tumbling fluidized-bed granulating/coating machine (MP-micro, Powrex Corporation, Japan) was used (Fig. 2). The temperature in the chamber was set at 80 °C. During the operation, NCA particles were floated in the chamber with air and a  $\text{TiO}_x$ -precursor solution in which titanium tetraisopropoxide (TTIP, 95%, Wako Pure Chemicals Co. Ltd. (Wako), Japan) was dissolved in 2-propanol (99.7%, Wako) was sprayed in the chamber. After a very small amount of droplets of the solution was deposited on the surface of NCA particles, the solvent of the

**Table 1** Spray conditions of  $\text{TiO}_x$  precursor to prepare  $\text{TiO}_x$ -coated NCA particles using a tumbling fluidized bed granulating/coating machine

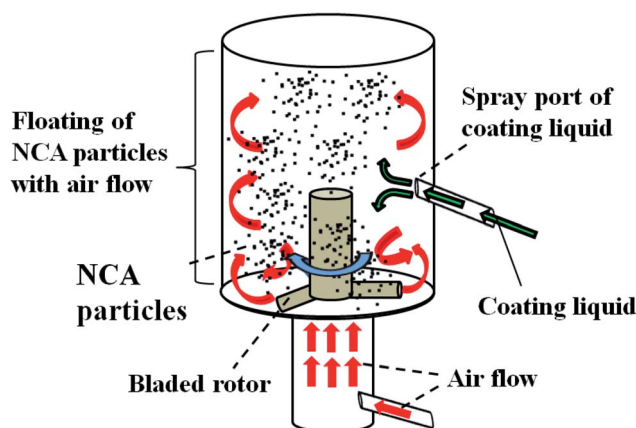
Sample number	C-1	C-2	C-3	C-4	C-5
Concentration of TTIP (wt%)	5.3	36	36	36	36
Spray speed ( $\text{g min}^{-1}$ )	20	20	2.0	2.0	20
Total amount of the solution sprayed (g)	0.50	0.50	0.50	0.25	0.25

droplets was evaporated and then the  $\text{TiO}_x$  precursor was coated on the NCA surfaces. The optimum spray conditions were examined by changing the concentration of TTIP, the spray speed and the total amount of the solution sprayed. After coating the  $\text{TiO}_x$  precursor, the NCA particles were sintered at 450 °C for 2 h under argon atmosphere to form the  $\text{TiO}_x$  layer on their surface, resulting in  $\text{TiO}_x$ -coated NCA particles.  $\text{TiO}_x$ -coated NCA samples C-1–C-5 were prepared at different spray conditions as summarized in Table 1.

$\text{TiO}_x$ -coated NCA cathode was prepared as follows: 910 mg of accurately weighed  $\text{TiO}_x$ -coated NCA particles and 50 mg of acetylene black (AB, Denka Black, Denki Kagaku Gogyo, Japan) were mixed on a mortar with a pestle, and 10 mg of carboxymethyl cellulose (CMC, Polyscience Inc, cat.#6139) and 30 mg of water-based hybrid polymer binder (TRD202A, JSR, Japan) were mixed in Milli-Pore water (1.1 g, >18 MΩ). Then, the mixture of  $\text{TiO}_x$ -coated NCA particles and AB was added to the CMC/TRD202A-mixed aqueous solution. The resulting mixed solution containing  $\text{TiO}_x$ -coated NCA particles, TRD202A, AB and CMC was further mixed with a planetary mixing equipment (Mazerustar, KK-250S, KURABO, Japan) until it became a homogenous slurry. The weight% of  $\text{TiO}_x$ -coated NCA powder : TRD202A : AB : CMC in the slurry was 91 : 3 : 5 : 1. The homogenous slurry was casted on Al current collector (thickness: 20 μm) with a doctor-blade having the gap of 100 μm. The slurry layer on the Al current collector was dried by evaporating water at 130 °C for 5 h in a vacuum drying oven. For comparison, polyvinylidene difluoride (PVdF, KF9130, Kureha, Japan) was also used as a binder. The weight% of the cathode films was kept as pristine NCA : PVdF : AB = 91 : 4 : 5. In every case, the loading amount of the cathode material on the Al current collector was 3.0–3.4  $\text{mg cm}^{-2}$ .

### 2.2 Preparation of $\text{Li}_2\text{CO}_3$ - and $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode electrodes

$\text{Li}_2\text{CO}_3$ -coated NCA cathode electrode was prepared using the homogeneous aqueous slurry containing NCA particles, TRD202A, AB and CMC with the same weight% as in the preparation of  $\text{TiO}_x$ -coated NCA cathode, by bubbling  $\text{CO}_2$  gas into the slurry for 3 min and then flowing  $\text{CO}_2$  gas over the slurry for a specified time of 1 h or 7 days. The samples of  $\text{Li}_2\text{CO}_3$ -coated NCA particles prepared by flowing  $\text{CO}_2$  gas for the specified time of 1 h, 1 day, 3 days and 7 days will be named E-1, E-2, E-3 and E-4, respectively. Immediately after stopping the  $\text{CO}_2$  gas flow, the slurry was casted on an Al current collector



**Fig. 2** Schematic drawing of a tumbling fluidized-bed granulating/coating machine to prepare  $\text{TiO}_x$ -coated NCA particles.



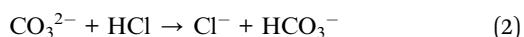
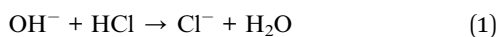
with a doctor blade and was dried at 130 °C for 5 h in a vacuum drying oven.

In the case of the preparation of  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode electrodes, at first, the slurry composed of  $\text{TiO}_x$ -coated NCA particles, TRD202A, AB and CMC was prepared at the same mixing percentages of NCA, TRD202A, AB and CMC as in the preparation of  $\text{TiO}_x$ - and  $\text{Li}_2\text{CO}_3$ -coated NCA cathodes and then  $\text{CO}_2$  gas was bubbled into the slurry as in the preparation of  $\text{Li}_2\text{CO}_3$ -coated NCA cathode electrode. When  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA samples, G-1 and G-2, were prepared by bubbling  $\text{CO}_2$  gas into the slurry for 1 h and 7 days, respectively. The casting of the slurry on an Al current collector and the subsequent drying process were conducted in a similar way as above.

### 2.3 Characterization of $\text{TiO}_x$ -, $\text{Li}_2\text{CO}_3$ -, and $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode materials

The atomic percentages of Ti atom on  $\text{TiO}_x$ -coated NCA particle samples were determined by X-ray fluorescence (XRF, ZSX Primus IV, Rigaku). Particle size and surface morphology of the  $\text{TiO}_x$ -coated NCA particles and the distribution of Co, Ni, Al and Ti atoms on the particles were observed with a field-emission scanning electron microscope (FE-SEM, S-4000, Hitachi) equipped with an energy dispersive X-ray spectrometer (EMAXEvolution (X-Max80), HORIBA). The crystal structures of  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$  layers and NCA were characterized with powder X-ray diffraction (pXRD, RINT-Ultima III diffractometer). As an X-ray source,  $\text{CuK}\alpha$  ( $\lambda = 0.1548$  nm) was used. The equipments for STEM, STEM-EELS and STEM-EDX measurements and their measurement conditions are mentioned in the Experimental section of ESI.†

The amounts of  $\text{Li}_2\text{CO}_3$  formed on the  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA electrodes were determined by a Warder titration,<sup>25</sup> *i.e.*, the amounts of both hydroxide and carbonate ions in a given titration solution were determined. 2.0 g of  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles were dispersed in 50 mL water for 60 min to dissolve the  $\text{Li}_2\text{CO}_3$  layer. The concentration of  $\text{CO}_3^{2-}$  ions dissolved in it was quantified by a titration with hydrochloric acid using phenolphthalein and methyl orange pH indicators. Phenolphthalein and methyl orange indicate the ends of the following reactions, *i.e.*, eqn (1)–(3), respectively. Hydroxide ions originate from LiOH residua on the NCA particles' surface.<sup>14,26</sup>



The concentration of  $\text{CO}_3^{2-}$  ion was determined from the volume of HCl titrant used to complete the reaction (3). The amounts of  $\text{Li}_2\text{CO}_3$  on  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles (2.0 g) were calculated using the thus-determined concentration of  $\text{CO}_3^{2-}$  ion. Finally, the amount of  $\text{Li}_2\text{CO}_3$  in each case was expressed as the surface concentration ( $\text{mg cm}^{-2}$ ) using the Brunauer–Emmett–Teller (BET) surface area of NCA particles evaluated with a TriStar 3000 (Micromeritics Instrument Corporation).

### 2.4 Cell preparation and electrochemical tests

Charging/discharging cycle and rate performance tests of the cathode materials prepared were performed using a CR2032 coin-type cell. In the test cell, each cathode was paired with a lithium metal anode and both electrodes were separated by a porous polypropylene film (Celgard 3401). The electrolyte solution containing 1 M  $\text{LiPF}_6$  in the mixture of ethylene carbonate (EC)/dimethyl carbonate (DMC) (1/2 volume ratio) (Ube Chemicals, Japan) was impregnated into the separator. The charge/discharge cycle and rate performance tests were carried out using a multi-channel battery tester (HJ1001SD8, Hokuto Denko Corporation, Japan) in thermostatic oven at room temperature ( $25 \pm 1$  °C). A constant-current/constant-voltage (CC–CV) mode was used for the charging/discharging cycle processes. The upper and lower voltage limits for the charging/discharging cycle processes were 4.25 and 2.5 V (*vs.*  $\text{Li}/\text{Li}^+$ ), respectively. The charge/discharge capacities ( $\text{mA h g}^{-1}$ ) were calculated using the weight of NCA particles loaded on the Al current collector in which the weight of the  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$  coating was neglected. The charging/discharging cycle tests were done with 0.1C-rate for 3 cycles and then 0.5C-rate for 30 cycles, and finally the charging/discharging performance was checked at 0.1C-rate. The C rate was calculated using the specific capacity of  $200 \text{ mA h g}^{-1}$  which was obtained with the cathode prepared from pristine (*i.e.*, uncoated) NCA, PVdF binder and AB at a low C-rate of 0.1C. In the case of high C-rate performance tests, discharge capacity retentions were evaluated assuming that the discharge capacity obtained at 0.1C corresponds to 100% of discharge capacity retention.

## 3. Results and discussion

### 3.1 Characterization of $\text{TiO}_x$ -, $\text{Li}_2\text{CO}_3$ -, and $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA materials

Fig. 3 shows the SEM images of (A) pristine NCA particles and (B, D, F and H) NCA particles exposed to water (in each case NCA particles (50 mg) were exposed to 5 mL water for 1 h and then dried at 130 °C for 1 h in a vacuum drying oven). The image B was obtained for the uncoated NCA particles, while the images D, F and H for  $\text{TiO}_x$ -,  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles, respectively. When compared with SEM images of NCA particles prior to water treatment (Fig. S1†), we can see that the uncoated NCA (B) is damaged significantly due to the dissolution of the surface into water. The TEM image of the damaged NCA surface has been reported in our previous paper.<sup>12</sup> On the damaged NCA surfaces, a Li-poor layer (2–3 nm in thickness) could be observed. On the other hand, the coated ones (D, F and H) seem not to be damaged. Fig. S1† shows SEM images of NCA particles prior to water treatment. The  $\text{Li}_2\text{CO}_3$  coating (Fig. S1(E)†) smooths the NCA surface, while the surface coating by  $\text{TiO}_x$  (Fig. S1(C)†) produces the rough surface. Also in the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  coating (Fig. S1(G)†), the NCA surface is rough probably reflecting  $\text{TiO}_x$  coating and interesting the roughness is larger than in the case of  $\text{TiO}_x$  coating.

The TEM-EDX elemental mapping images of  $\text{TiO}_x$ -coated NCA samples C-1–C-5 prepared at different spray conditions





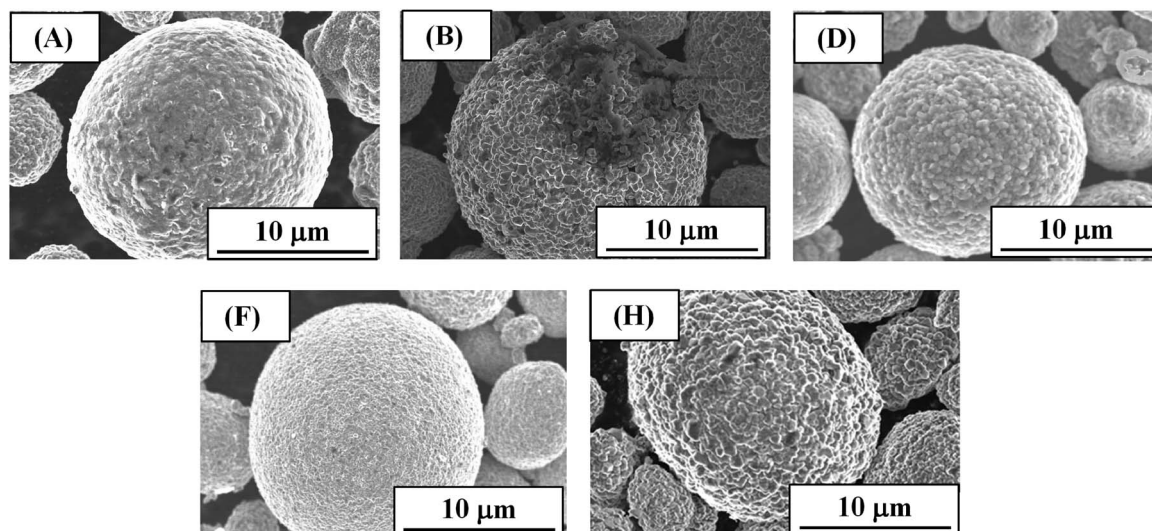


Fig. 3 SEM images of NCA particles. The image (A) was obtained for the pristine NCA not exposed to water. The images (B, D, F and H) were obtained for (B) un-coated, (D)  $\text{TiO}_x$ -coated, (F)  $\text{Li}_2\text{CO}_3$ -coated and (H)  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles which were exposed to water for 1 h.

(Table 1) are shown in Fig. S2† where blue, red and green colors show the distribution of Co, Ni and Ti atoms, respectively, in the NCA particles. The overlapped elemental mapping images of Co, Ni and Ti indicate that NCA particle surfaces are Ti-riched and the degree of the Ti-coating is different depending on the spray conditions. Clearly, samples C-2 and C-5 have thicker  $\text{TiO}_x$  layers on NCA particle surfaces. From the XRF experiments (Fig. S3†), samples C-2 and C-5 were found to have higher atomic ratios of Ti to Ni when compared with samples C-1, C-3 and C-4, suggesting that the former samples are coated with higher amount of  $\text{TiO}_x$ . The thickness of  $\text{TiO}_x$  coating on NCA particle surfaces is controlled by the concentration and spray speed of TTIP solution, *i.e.*, the high concentration and spray speed of TTIP solution resulted in the increased thickness of  $\text{TiO}_x$ . In addition, in order to confirm a thin and uniform coating of the NCA particles with  $\text{TiO}_x$  layer, SEM-EDX images for typical particles of samples C-3 and C-4 which showed better cathode performance among the  $\text{TiO}_x$ -coated NCA samples tested as described below were also obtained (Fig. S4†). They indicated that NCA particles are uniformly covered with  $\text{TiO}_x$  layer even at the low coating amount of  $\text{TiO}_x$ .

In order to identify the crystal structures of  $\text{TiO}_x$ -coated layer and NCA, powder X-ray diffraction (pXRD) patterns of  $\text{TiO}_x$ -coated NCA samples C-1~C-5 were measured and the results are shown in Fig. 4. The pXRD profiles obtained matched that of a layered  $\alpha\text{-NaFeO}_2$ -type structure with the space group  $R\bar{3}m$ ,<sup>26</sup> in which the Na sites are occupied by  $\text{Li}^+$  ions and the Fe sites by transition metal (Ni, Co and Al) ions. It was found that the pXRD peaks corresponding to the layered  $\alpha\text{-NaFeO}_2$ -type structure do not shift even at high degree of  $\text{TiO}_x$  coating (*e.g.*, samples C-2 and C-5), indicating that the  $\text{TiO}_x$  layers formed on the NCA surfaces do not affect the crystal structure of the NCA particles themselves. On the other hand, the pXRD peaks for  $\text{TiO}_x$  layer could not be observed in the pXRD patterns of NCA samples C-1~C-5 as found in recent studies<sup>12,19</sup> in which the  $\text{TiO}_x$  crystal

structure is considered to grow “epitaxially” on the NCA particle surface based on the high angle annular-dark-field (HAADF)-scanning transmission electron microscopic (STEM) measurements.

Fig. 5 (I) shows the pXRD patterns of  $\text{Li}_2\text{CO}_3$ -coated (E-1) and pristine (A) NCA samples. As mentioned above, the pXRD peaks for NCA particles could be observed, but there was no difference in pXRD peaks of both samples. In the expanded pXRD profile ((E-1) in (II)), as expected, three peaks for  $\text{Li}_2\text{CO}_3$  could be observed clearly at  $21.5^\circ$ ,  $30.1^\circ$  and  $32.0^\circ$ . On the other hand, also in the pristine NCA, the peaks for  $\text{Li}_2\text{CO}_3$  could be observed ((A) in (II)) probably because a small amount of  $\text{Li}_2\text{CO}_3$  was formed by exposing the pristine NCA sample to air.

The pristine and  $\text{Li}_2\text{CO}_3$ -coated NCA samples had the Brunauer–Emmett–Teller (BET) surface areas of  $0.11\text{--}0.12\text{ m}^2\text{ g}^{-1}$ , *i.e.*, the NCA surface areas are almost the same in both samples. In order to calculate the surface coating (in a unit of  $\text{mg cm}^{-2}$ ) and layer thickness of  $\text{Li}_2\text{CO}_3$ ,  $0.155\text{ m}^2\text{ g}^{-1}$  and  $2.11\text{ g cm}^{-3}$  were used as a surface area of NCA particles and a density of  $\text{Li}_2\text{CO}_3$  layer, respectively.<sup>27</sup> From the Warder titration experiments, the  $\text{Li}_2\text{CO}_3$ -coated NCA samples prepared by bubbling  $\text{CO}_2$  gas for 1 h (E-1) and 7 days (E-4) were found to have the average  $\text{Li}_2\text{CO}_3$  thicknesses of 16 and 22 nm, respectively. As can be seen from this, the thickness of  $\text{Li}_2\text{CO}_3$  coating layer could be controlled by the period of bubbling of  $\text{CO}_2$  gas into the sample solutions. The  $\text{Li}_2\text{CO}_3$  coating layer grew slowly over several hours.

Fig. 6 shows the typical TEM images of (A) pristine, (E-1 and E-2)  $\text{Li}_2\text{CO}_3$ -coated, (C-3)  $\text{TiO}_x$ -coated and (G-1 and G-2)  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA samples. The water-based  $\text{Li}_2\text{CO}_3$ -coated and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA slurries were kept under  $\text{CO}_2$  atmosphere for 1 h (E-1 and G-1) and 7 days (E-4 and G-2). When the slurry solution of NCA particles was kept under  $\text{CO}_2$  atmosphere for 1 h (E-1 and G-1) and 7 days (E-4 and G-2), the  $\text{Li}_2\text{CO}_3$  layer could be observed clearly on their surfaces as can be seen



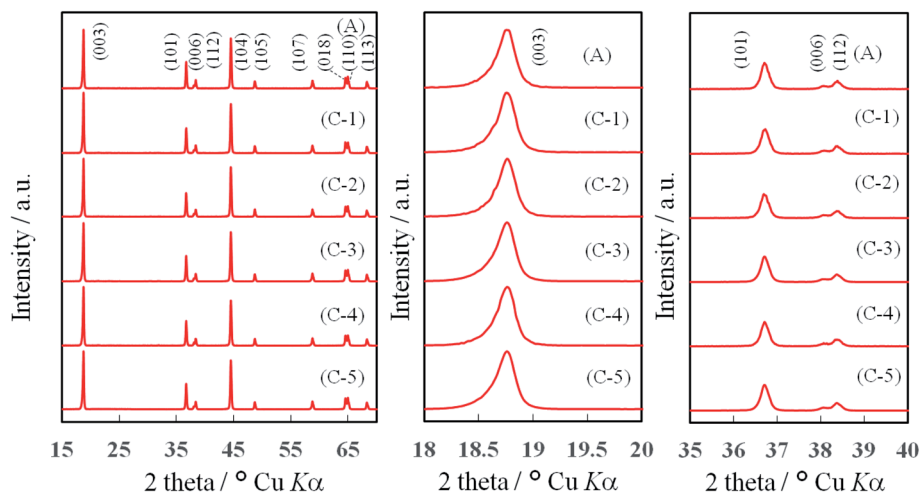


Fig. 4 pXRD profiles of pristine (A) and  $\text{TiO}_x$ -coated NCA (C-1–C-5) samples.

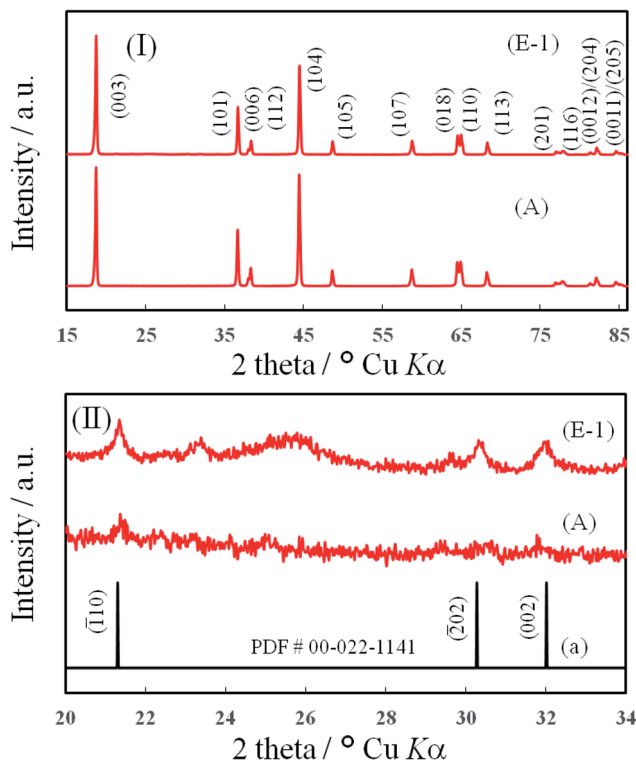


Fig. 5 pXRD profiles of  $\text{Li}_2\text{CO}_3$ -coated (E-1) and pristine (A) NCA. The  $\text{Li}_2\text{CO}_3$ -coated NCA sample was prepared by bubbling  $\text{CO}_2$  gas into an aqueous solution containing NCA particles for 1 h. The pXRD profiles (I) are expanded in the region of  $2\theta$  from 20 to  $34^\circ$  and shown as (II). (a) Indicates the simulated pXRD peak pattern for  $\text{Li}_2\text{CO}_3$ .

from the comparison with the TEM image of pristine NCA (A), *i.e.*, the average thicknesses of the  $\text{Li}_2\text{CO}_3$  layer were 13.5 (E-1) and 15.8 (E-4) nm. In addition, needle-like crystals were found to be formed when kept under  $\text{CO}_2$  atmosphere for 7 days (E-4) in the case of the water-based  $\text{Li}_2\text{CO}_3$ -coated NCA slurry. In this case, it is thought that water invades into the coarse  $\text{Li}_2\text{CO}_3$  layer and  $\text{Li}^+$  ions extracted from the NCA surfaces react with  $\text{CO}_3^{2-}$

ions to form needle-like crystals of  $\text{Li}_2\text{CO}_3$  on the  $\text{Li}_2\text{CO}_3$  layer. The whole surface of NCA particles seems to be coated with the  $\text{TiO}_x$  layer (Fig. 6 (C-3)). When the slurry composed of  $\text{TiO}_x$ -coated NCA particles, water-based hybrid polymer binder (TRD202A), AB and CMC was kept under  $\text{CO}_2$  atmosphere for 1 h or 7 days,  $\text{Li}_2\text{CO}_3$  layer may be formed on the  $\text{TiO}_x$  layer (as it is not dense) as well as the  $\text{TiO}_x$ -uncoated part in which  $\text{LiOH}$  as a residue on the NCA surface is the source of  $\text{Li}^+$  ions for the formation of  $\text{Li}_2\text{CO}_3$ . The average thicknesses of the  $\text{Li}_2\text{CO}_3$  layer prepared on  $\text{TiO}_x$ -coated NCA particles under  $\text{CO}_2$  atmosphere for 1 h (G-1) and 7 days (G-2) were 12.5 and 13.2 nm, respectively. However, needle-like crystals could not be observed being distinct from the case (E-4).

In order to confirm the formation of  $\text{Li}_2\text{CO}_3$  layer on the NCA surface and  $\text{TiO}_x$  layer, the STEM-EELS images of  $\text{Li}_2\text{CO}_3$ - and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA samples were measured and the typical results are shown in Fig. 7–9. In the case of  $\text{Li}_2\text{CO}_3$ -coated NCA sample (E-1, Fig. 7), the signals corresponding to Li, O and C elements could be observed over the whole surface, indicating that the NCA surface is on a whole coated by the  $\text{Li}_2\text{CO}_3$  layer. The average thickness of the  $\text{Li}_2\text{CO}_3$  layer evaluated from the TEM image was *ca.* 15.7 nm, which was comparable to that calculated from the amount of  $\text{Li}_2\text{CO}_3$  layer on the NCA surface estimated with a Wader titration using the density of  $\text{Li}_2\text{CO}_3$  ( $d = 2.11 \text{ g cm}^{-3}$ ).<sup>27</sup> The STEM-EELS images of  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particle (G-1, Fig. 8) confirmed Fig. 6 (G-1), *i.e.*, the  $\text{Li}_2\text{CO}_3$  layer is formed on the  $\text{TiO}_x$  layer the average thickness of which was evaluated to be *ca.* 12.4 nm. From Fig. 9, it was further speculated that the needle-like crystals (shown in Fig. 6 (E-4)) observed after keeping the slurry solution containing pristine NCA particles under  $\text{CO}_2$  atmosphere for 7 days correspond to  $\text{NiCO}_3$  and  $\text{Li}_2\text{CO}_3$ . This fact suggests that the  $\text{Li}_2\text{CO}_3$  layer formed on NCA particle surfaces is insufficient as a water-proof layer and as a result  $\text{Ni}^{2+}$  ions of NCA dissolve to form  $\text{NiCO}_3$ . On the contrary, the  $\text{TiO}_x$  layer on NCA particle surfaces inhibited the formation of the needle-like crystals under the same exposure to the  $\text{CO}_2$  atmosphere, indicating

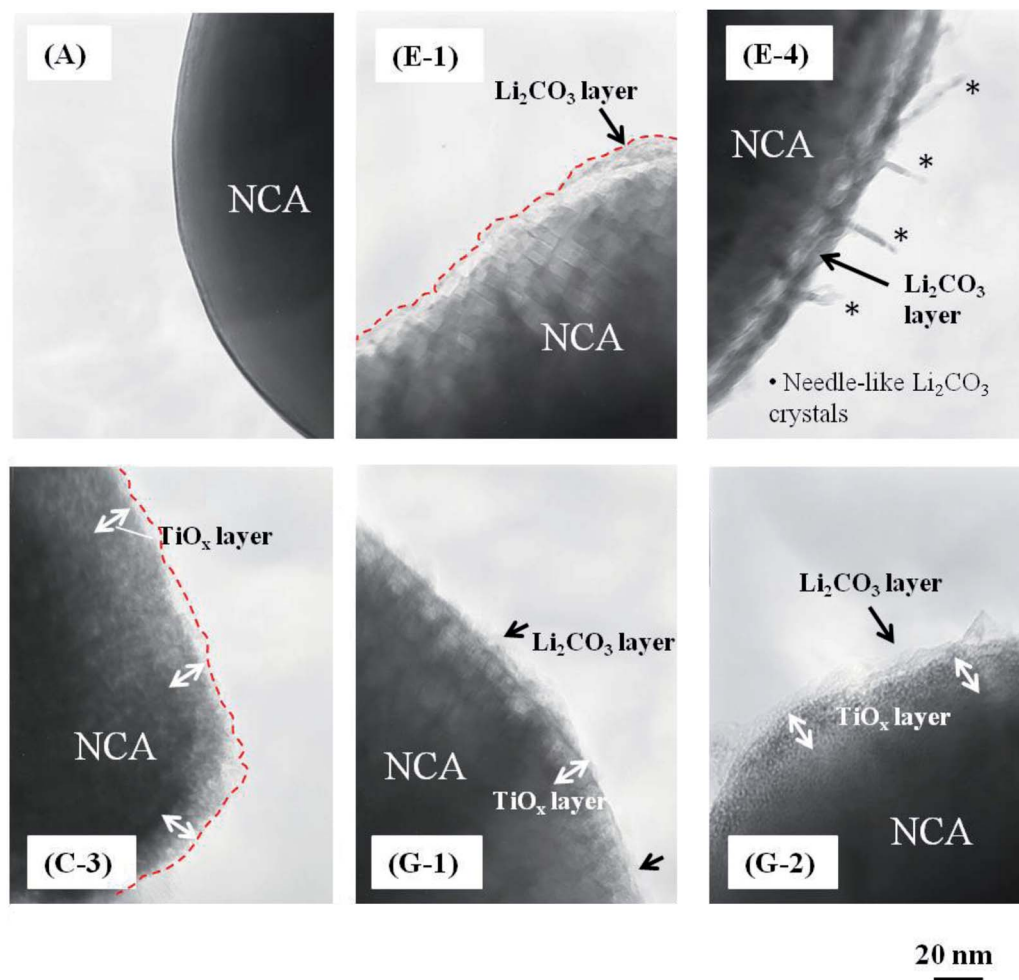


Fig. 6 Typical TEM images of (A) pristine, (E-1)  $\text{Li}_2\text{CO}_3$  ( $\text{CO}_2$  bubbling for 1 h)-coated, (E-4)  $\text{Li}_2\text{CO}_3$  ( $\text{CO}_2$  bubbling for 7 days)-coated, (C-3)  $\text{TiO}_x$ -coated, (G-1)  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  ( $\text{CO}_2$  bubbling for 1 h)-coated and (G-2)  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  ( $\text{CO}_2$  bubbling for 7 days)-coated NCA samples.

that the double coating of NCA surface by  $\text{TiO}_x$  layer and then  $\text{Li}_2\text{CO}_3$  layer is effective for giving a water-resistance to it.

### 3.2 Charging/discharging performance tests with $\text{TiO}_x$ -, $\text{Li}_2\text{CO}_3$ - and $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA materials

Fig. 10 shows the charging/discharging cycle performance obtained with the cathodes prepared from pristine NCA and  $\text{TiO}_x$ -coated NCA samples C-1–C-5. The charge/discharge was conducted with the 0.1C-rate for first 3 cycles and then with 0.5C-rate for 30 cycles and again with 0.1C-rate for 3 cycles to confirm the initial charge/discharge performance. Clearly, the pristine NCA (A) cathode prepared with PVDF binder exhibited the highest discharge performance among the NCA samples tested. The cycle performance is in the order of pristine > sample C-1 = sample C-3 > sample C-4 > sample C-2 > sample C-5. The performance order of the  $\text{TiO}_x$ -coated samples is similar to the order of atomic ratio of Ti to Ni (Fig. S3†), indicating that an excessive  $\text{TiO}_x$  coating reduces the discharge capacity because the  $\text{TiO}_x$  retards the intercalation/deintercalation of  $\text{Li}^+$  ion to/from the NCA cathode active material. The samples C-1 and C-3 exhibited the highest discharge performance among

the  $\text{TiO}_x$ -coated NCA samples, but their performance was a little inferior to that obtained with the pristine NCA. This small decrease in the discharge capacity of samples C-1 and C-3 is considered to reflect that they are damaged by contact with water in the course of their preparation. The NCA particle surfaces of samples C-1 and C-3 might be partly uncoated with the  $\text{TiO}_x$  layer and/or coated with the coarse  $\text{TiO}_x$  layer and consequently the NCA surface might partially suffer from the damage by contact with water. From the discharge capacities obtained at 0.1C-rate after 30 cycles at 0.5C-rate, the discharge capacity retentions (%) which are defined as (discharge capacity at the 34<sup>th</sup> cycle)/(discharge capacity at the 3<sup>rd</sup> cycle)  $\times$  100 of the pristine and  $\text{TiO}_x$ -coated NCA samples C-1–C-5 were calculated to be 93, 92, 83, 94, 89 and 78%, respectively. The samples C-2 and C-5 coated with larger amount of  $\text{TiO}_x$  are considered to suffer from larger damage by the discharge at 0.5C-rate because thicker  $\text{TiO}_x$  layers of these samples more significantly retard the intercalation/deintercalation of  $\text{Li}^+$  ions. In addition, the high rate performance of  $\text{TiO}_x$ -coated NCA samples was examined with the C-rate of 0.1, 0.2, 0.5, 1, 2, 3 and 5C (Fig. S5†). The samples C-1, C-3 and C-4 exhibited nearly the same





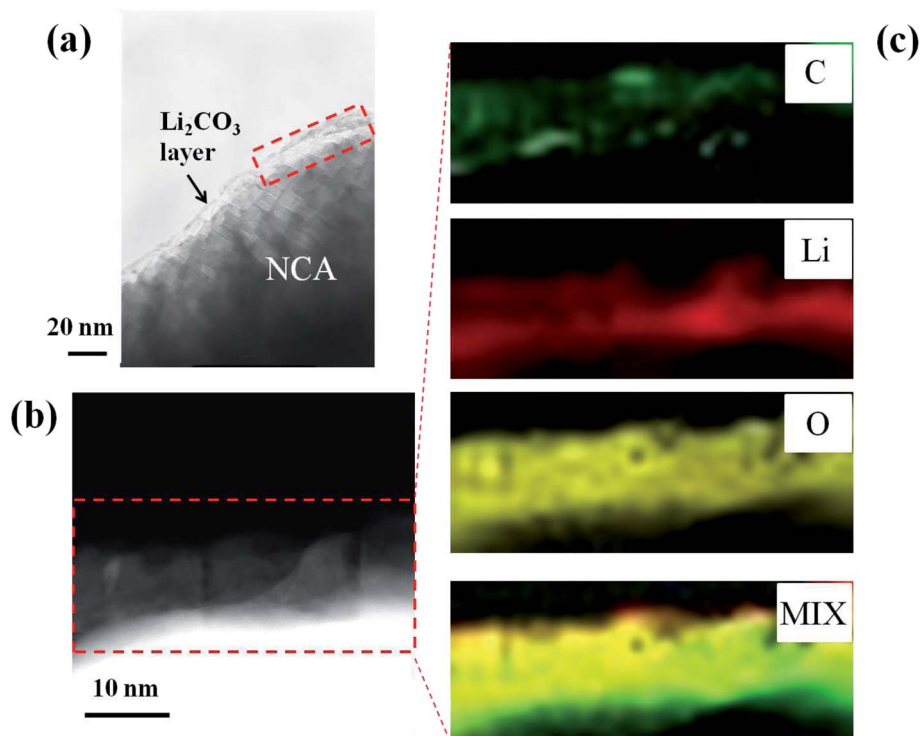


Fig. 7 (a and b) Typical TEM images of  $\text{Li}_2\text{CO}_3$  ( $\text{CO}_2$  bubbling for 1 h)-coated NCA (E-1) and (c) STEM-EELS mapping of C, Li and O elements and their mixed mapping.

performance as that obtained with the pristine NCA sample, while the samples C-2 and C-5 indicated significantly lower performance especially at higher C-rates. These results are

similar to those obtained at the charging/discharging cycle tests at 0.1 and 0.5C (mentioned above). That is, the thick  $\text{TiO}_x$  layer retarded actually the transfer of  $\text{Li}^+$  ions from/to cathode

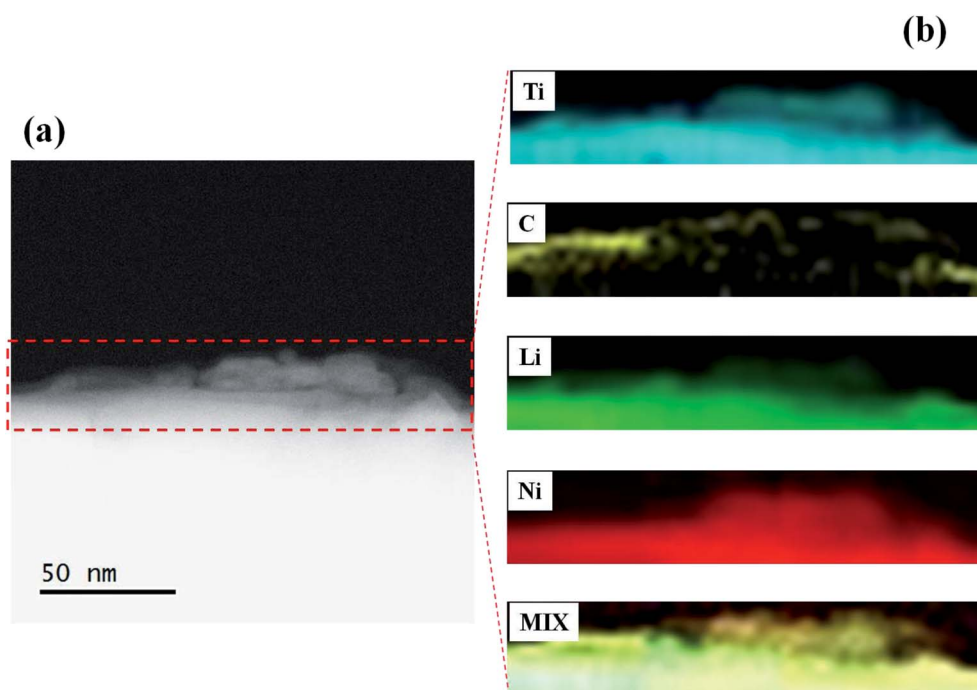


Fig. 8 (a) Typical TEM image of  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  ( $\text{CO}_2$  bubbling for 1 h)-coated NCA (G-1) and (b) STEM-EELS mapping of Ti, C and Li elements and their mixed mapping.





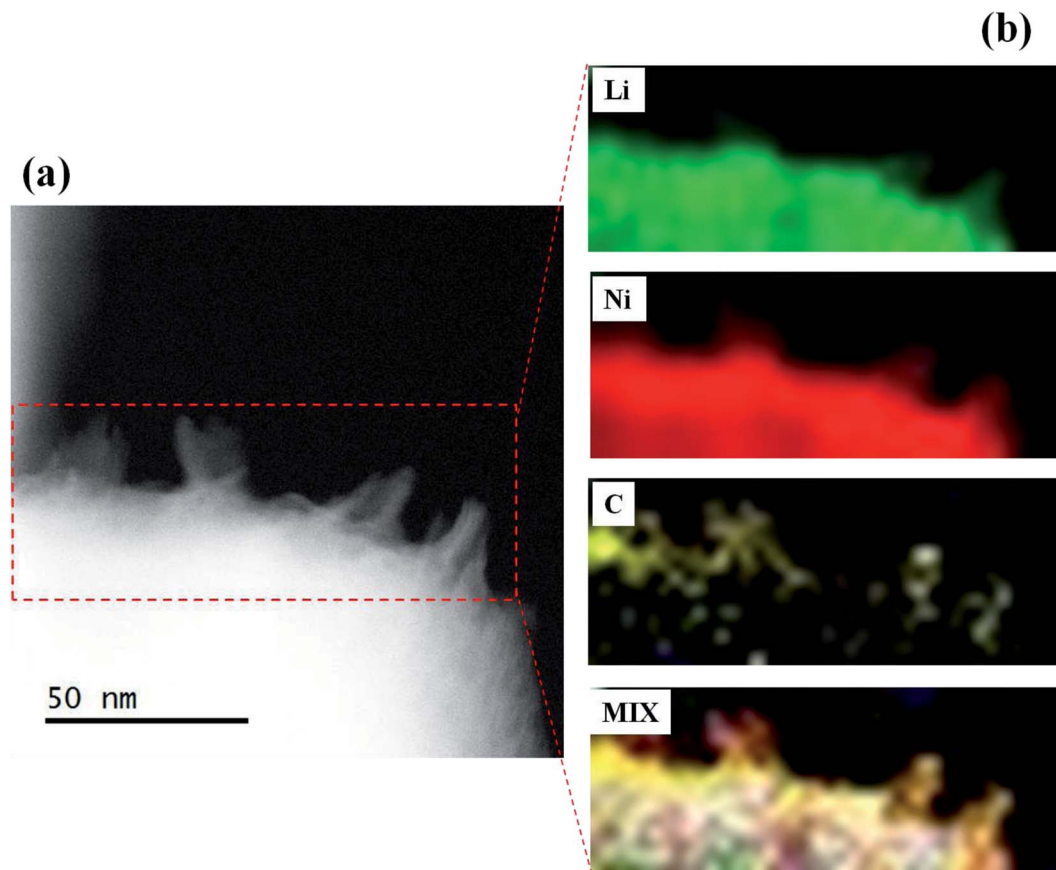


Fig. 9 (a) Typical TEM image of  $\text{Li}_2\text{CO}_3$  ( $\text{CO}_2$  bubbling for 7 days)-coated NCA (E-4) and (b) STEM-EELS mapping of Li, Ni and C elements and their mixed mapping.

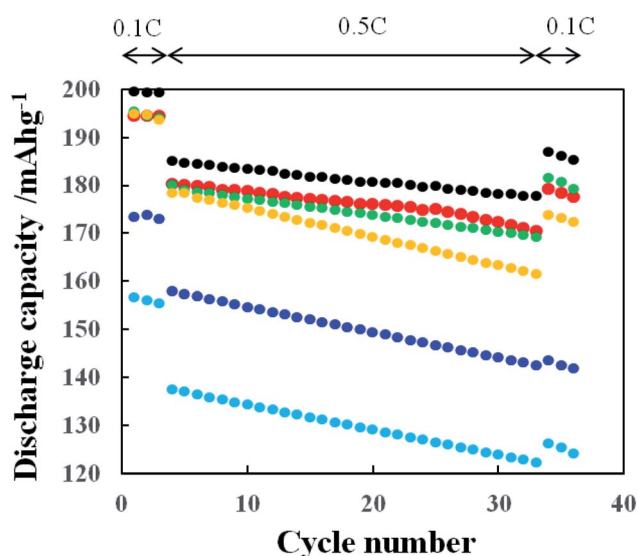


Fig. 10 Charge/discharge cycle performance obtained with pristine and  $\text{TiO}_x$ -coated NCA (samples C-1–C-5) cathodes at the charging/discharging rate of 0.1 and 0.5C at 25 °C. Pristine A (●: black), samples C-1 (●: red), C-2 (●: blue), C-3 (●: green), C-4 (●: yellow) and C-5 (●: light blue). The cathode with pristine NCA was prepared using PVdF binder. In all the charging processes, the C-rate of 0.1C was used.

particle surfaces and consequently degraded the cathode performance. The samples C-1, C-3 and C-4 exhibited the charging/discharging cycle performance and high rate performance comparable to that obtained with the  $\text{TiO}_x$ -coated NCA samples prepared by reacting  $\text{TiO}_x$ -precursor with NCA surface in beaker,<sup>12,19</sup> indicating that the present  $\text{TiO}_x$  coating using a tumbling fluidized-bed granulating/coating machine enables to prepare the NCA particles coated with  $\text{TiO}_x$  layer which rarely inhibit the transfer of  $\text{Li}^+$  ions from/to NCA particle surfaces by suitably adjusting the concentration of  $\text{TiO}_x$  precursor solution which is sprayed in the reaction chamber.

The effect of  $\text{Li}_2\text{CO}_3$  coating on NCA cathodes on their cycle performance was examined and the results are shown in Fig. 11, in which the slurry solution containing pristine NCA particles, TRD202A binder, CMC and conductive additive (AB) was kept under  $\text{CO}_2$  atmosphere for 1 h (E-1), 1 (E-2), 3 (E-3) and 7 (E-4) days. The reason why the  $\text{CO}_2$  treatment of 1 h to 7 days was examined in this study is that slurry solutions of electrode active materials are used, once prepared, typically for 7 days in the production line of commercially available LIBs. The discharge capacity decreased largely with increasing the  $\text{CO}_2$  treatment period. As mentioned above, longer  $\text{CO}_2$  treatment may produce thicker  $\text{Li}_2\text{CO}_3$  and consequently leads to lower discharge capacity. Here we should also consider the damage of NCA particles by contact with water during the  $\text{CO}_2$  treatment for the



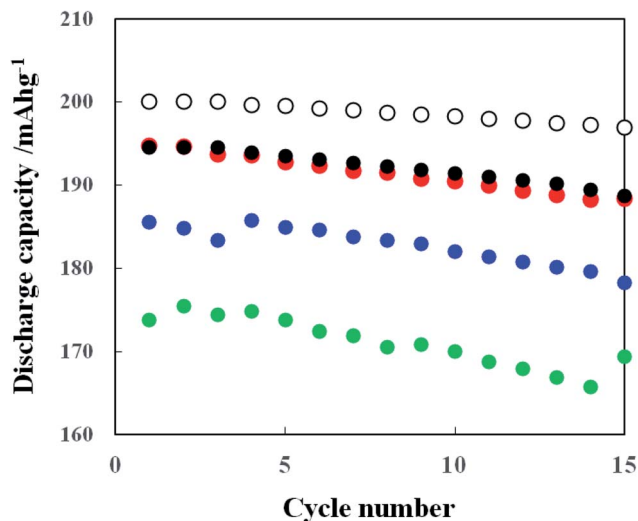


Fig. 11 Charge/discharge cycle performance obtained with  $\text{Li}_2\text{CO}_3$ -coated NCA cathodes at the charging/discharging rate of 0.1C at 25 °C.  $\text{Li}_2\text{CO}_3$  coating was conducted by bubbling  $\text{CO}_2$  gas into the homogeneous aqueous slurry containing NCA particles, TRD202A, AB and CMC for 1 h (●: black, E-1), 1 day (●: red, E-2), 3 days (●: blue, E-3) and 7 days (●: green, E-4). Pristine NCA (○, A) cathode was prepared using PVdF binder.

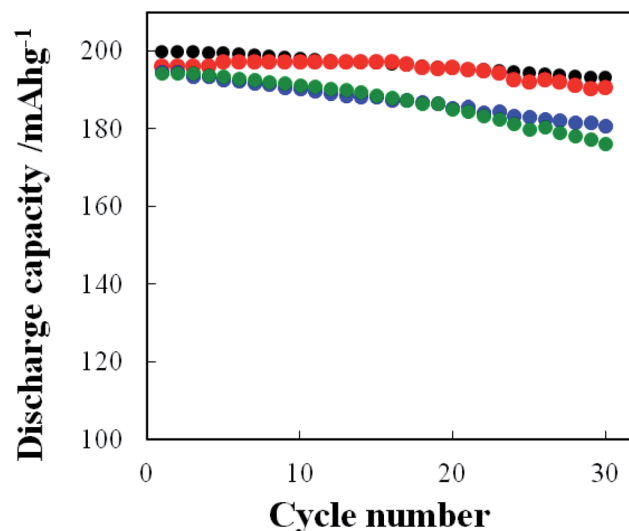


Fig. 12 Charge/discharge cycle performance obtained with the cathodes prepared from (●: black, A) the slurry consisting of pristine NCA, PVdF and AB, (●: red, G-2) the water-based slurry consisting of  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA (the slurry was kept for 7 days under  $\text{CO}_2$  atmosphere), TRD202A, CMC and AB, (●: blue, C-3) the water-based slurry consisting of  $\text{TiO}_x$ -coated NCA, TRD202A, CMC and AB and (●: green, E-1) the water-based slurry consisting of  $\text{Li}_2\text{CO}_3$ -coated NCA (the slurry was kept for 1 h under  $\text{CO}_2$  atmosphere), TRD202A, CMC and AB at the charging/discharging rate of 0.1C at 25 °C.

$\text{Li}_2\text{CO}_3$  formation in the  $\text{CO}_2$ -saturated aqueous slurry solution containing NCA particles. Interestingly, the NCA samples  $\text{CO}_2$ -treated for 1 h (E-1) and 1 day (E-2) gave almost the same charge/discharge performance, although it is thought that the NCA sample  $\text{CO}_2$ -treated for 1 h is less damaged by contact with water and the  $\text{Li}_2\text{CO}_3$  layer formed is thinner compared with the 1 day  $\text{CO}_2$ -treated one. Thus, under the present  $\text{CO}_2$  treatment condition the  $\text{CO}_2$  treatment of 1 h is enough to form the  $\text{Li}_2\text{CO}_3$  layer.

Fig. 12 shows the charge/discharge performance obtained with the cathodes prepared from the slurry containing pristine NCA, PVdF and AB as well as the water-based slurries containing  $\text{TiO}_x$ -(C-3),  $\text{Li}_2\text{CO}_3$ -(E-1)- or  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -(G-2)-coated NCA, TRD202A, CMC and AB. The pristine NCA (A) cathode prepared with PVdF binder exhibited the discharge capacities of 199 and 186  $\text{mA h g}^{-1}$  at the 1<sup>st</sup> and 30<sup>th</sup> cycles, respectively and the discharge capacity retention was 93% at the 30<sup>th</sup> cycle. On the other hand, the discharge capacities of the  $\text{TiO}_x$ -coated ( $\text{Li}_2\text{CO}_3$ -coated) NCA cathodes at the 1<sup>st</sup> and 30<sup>th</sup> cycles are 195 (196) and 177 (177)  $\text{mA h g}^{-1}$ , respectively. The discharge capacity retentions for  $\text{TiO}_x$ - and  $\text{Li}_2\text{CO}_3$ -coated NCA samples were 91 and 88% at the 30<sup>th</sup> cycles, respectively. The  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode, which was prepared by keeping the water-based slurry for 7 days under  $\text{CO}_2$  atmosphere which means that the cathode was actually exposed to water for 7 days, exhibited the discharge capacities of 196 and 187  $\text{mA h g}^{-1}$  at the 1<sup>st</sup> and 30<sup>th</sup> cycles, respectively and the discharge capacity retention of 95% at the 30<sup>th</sup> cycle. Thus, it is obvious that the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode is superior in both the discharge capacity and capacity retention to  $\text{TiO}_x$ - and  $\text{Li}_2\text{CO}_3$ -coated NCA cathodes and the discharge capacity retention of the former is comparable to that of the pristine NCA cathode prepared with PVdF

binder. The  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathodes gave, even though the NCA particles were exposed as the water-based slurry to water for 7 days, high charge/discharge capacities as a result of the surface double coating with  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$ . In Fig. S6,<sup>†</sup> the SEM images of NCA particles on cathodes after the charging/discharging cycles of 30 times (done in Fig. 12) are shown. In this case, the NCA particles are covered with PVdF and AB or TRD202A, CMC and AB and thus their surfaces look rough due to the adsorption of PVdF and AB or TRD202A, CMC and AB. The difference of surface morphology could not be observed among the four samples examined. Also in the comparison of the SEM images of the four samples before and after the charging/discharging cycles of 30 times (the SEM images obtained after the cycles are not shown in this paper), the surface morphology change could not be observed. Moisture contents of the cathode electrodes after drying NMP or water solvent were measured with thermogravimetry (TG) (Experimental in ESI and Fig. S7<sup>†</sup>). The cathode (a) composed of pristine NCA, PVdF and AB did not exhibit the change in weight of its scratched layer, indicating that the water content is almost zero. The  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA (G-2) particles just after synthesis of the coated powder was showed a significantly large weight loss in the temperature region from 100 to 200 °C. However, the sample powder obtained from the cathode prepared with the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA (G-2) particles exhibited only a very small loss, *i.e.*, the weight loss was 0.23 wt% because the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles on the cathode was dried well in the fabrication processes of cathodes. It can be considered that such a low content of water in the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode do not influence the cathode



performance. The charge/discharge voltage–capacity curves of pristine (A),  $\text{TiO}_x$ - (C-3),  $\text{Li}_2\text{CO}_3$  (E-1)- and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  (G-2)-coated NCA cathodes are shown in Fig. S8.† These curves are, though there is a small difference in the charge/discharge capacity, typical for the NCA and show several small shoulders corresponding to the redox reaction of Co and Ni ions in NCA,<sup>27</sup> indicating that the samples tested have the essentially same charge/discharge property except for the individual capacities.

The rate performance of the above-mentioned cathodes of typical four types was examined and the results are shown in Fig. 13. As predicted, the pristine NCA (A) without a coating layer exhibited the highest C-rate performance. The rate performance of the coated NCA cathodes was in the order of the  $\text{TiO}_x$ - (C-3),  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ - (G-2) and  $\text{Li}_2\text{CO}_3$ -coated (E-1) ones. These results are considered to reflect the different degree of the inhibition of  $\text{Li}^+$  ion transfer in the intercalation/deintercalation processes by the individual coatings. In order to check the conductivity change after the coating of NCA particles, the direct current internal resistance (DC-IR) drop which can be seen in the early stage of the discharging process was compared. Fig. S9-(a)† shows the discharge voltage–discharge capacity curves of pristine (A),  $\text{TiO}_x$ - (C-3),  $\text{Li}_2\text{CO}_3$  (E-1)- and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  (G-2)-coated NCA cathodes obtained at 5C-rate in the rate performance test of Fig. 13. The DC-IR drop can be related to the conductivity of coated NCA particles. In the enlarged discharge voltage–discharge capacity curves shown in Fig. S9-(b),† no difference in the DC-IR drop could be observed.

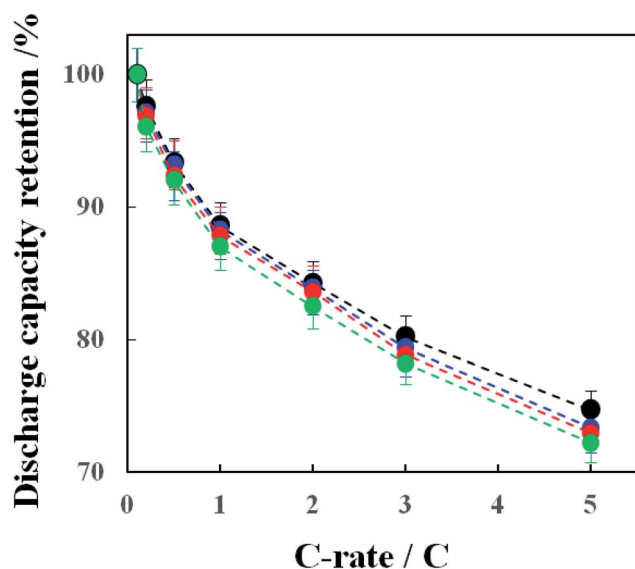


Fig. 13 Plots of discharge capacity retention vs. C-rate obtained with the cathodes prepared from (●: black) the slurry consisting of pristine NCA, PVdF and AB, (●: red, A) the water-based slurry consisting of  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA (the slurry was kept for 7 days under  $\text{CO}_2$  atmosphere, G-2), TRD202A, CMC and AB, (●: blue, C-3) the water-based slurry consisting of  $\text{TiO}_x$ -coated NCA, TRD202A, CMC and AB and (●: green, E-1) the water-based slurry consisting of  $\text{Li}_2\text{CO}_3$ -coated NCA (the slurry was kept for 1 h under  $\text{CO}_2$  atmosphere), TRD202A, CMC and AB at 25 °C. In the calculation of the discharge capacity retention, the discharge capacity obtained at 0.1C with each cathode was considered as 100% of capacity retention.

Thus, the change of conductivity before and after the coating with  $\text{TiO}_x$ ,  $\text{Li}_2\text{CO}_3$  and  $\text{TiO}_x/\text{Li}_2\text{CO}_3$  was not seen in the samples used in the rate performance test in Fig. 13. As mentioned in our previous paper,<sup>12</sup> it is found that when thin  $\text{TiO}_x$  coating layers are formed on NCA surface, they scarcely block the  $\text{Li}^+$  transportation through them. Certainly, also in Fig. 13, the rate performance of  $\text{TiO}_x$ -coated NCA particles is almost the same as that of the pristine NCA particles within the experimental error.  $\text{Li}_2\text{CO}_3$  coating, on the contrary, blocks somewhat the  $\text{Li}^+$  transportation through its layer because the discharge capacity retention obtained at the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode is lower than that obtained at the pristine and  $\text{TiO}_x$ -coated ones. Therefore, we think that un-coated the gaps left by incomplete  $\text{TiO}_x$  coating are infilled by  $\text{Li}_2\text{CO}_3$  coating and thus the  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode is inferior in the rate performance to the  $\text{TiO}_x$ -coated NCA ones.

## 4. Conclusions

In this study, we originally proposed the surface double coating of NCA cathode with water-stable  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$  layers with a view of applying water-based binders to the preparation of the cathodes for LIBs because the use of water-based binders simplifies their production process and reduces their cost. NCA cathodes possess a high voltage and high charge/discharge capacity, but they are heavily damaged when contacted to water during their preparation processes. The NCA surface was coated firstly with  $\text{TiO}_x$  layer by spraying  $\text{TiO}_x$  precursor slurry using a tumbling fluidized-bed granulating/coating machine followed by sintering at 450 °C under argon atmosphere (producing  $\text{TiO}_x$ -coated NCA particles) and then with  $\text{Li}_2\text{CO}_3$  layer by bubbling  $\text{CO}_2$  gas in the  $\text{TiO}_x$ -coated NCA aqueous slurry and consequently the NCA particles coated doubly with  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$  layers ( $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA particles) were prepared. The TEM and STEM-EELS measurements confirmed that the whole surface of NCA particles is actually coated doubly with  $\text{TiO}_x$  and  $\text{Li}_2\text{CO}_3$  layers. The  $\text{TiO}_x/\text{Li}_2\text{CO}_3$ -coated NCA cathode possessed a significantly higher charge/discharge performance compared with the  $\text{TiO}_x$ - or  $\text{Li}_2\text{CO}_3$ -coated NCA cathodes and almost the same charge/discharge capacities as obtained at the NCA cathode prepared using the conventional organic solvent-based PVdF binder although the high rate discharge performance was a little inferior to the latter due to a small resistance of  $\text{Li}^+$  ion transfer through the coated layers. In addition, it should be noted that the present double coating procedure using a tumbling fluidized-bed granulating/coating machine and  $\text{CO}_2$  gas bubbling is promising at a viewpoint of the mass production of surface-coated cathode materials for LIBs using water-based binders. Further study along with this line is progress.

## Author contribution

T. W. and K. H. performed charge/discharge test and preparation of coated cathode materials. F. A. and T. G. characterized the synthesized materials with STEM, EELS and EDS. S. K., S. U. and H. L performed coating treatment of cathode materials with





coating machine. Y. I. and F. M. (Nihon Kagaku Sangyo) performed a preparation of bare cathode material. J. W., T. O. and F. M. (Kanagawa University) wrote the manuscript, summarized the work.

## Conflicts of interest

The authors declare no competing financial interest.

## Acknowledgements

This work was financially supported by the Kato Foundation for Promotion of Science, Japan (T. Watanabe). This work was supported by NIMS microstructural characterization platform as a program of "Nanotechnology Platform" of the Ministry of Education, Culture, Sports, Science and Technology (MEXT), Japan.

## References

- 1 M. Li, J. Lu, Z. Chen and K. Amine, 30 Years of Lithium-Ion Batteries, *Adv. Mater.*, 2018, **30**, 1800561.
- 2 H. Lu, M. Behm, S. Leijonmarck, G. Lindbergh and A. Cornell, Flexible paper electrodes for Li-ion batteries using low amount of TEMPO-oxidized cellulose nanofibrils as binder, *ACS Appl. Mater. Interfaces*, 2016, **8**, 18097–18106.
- 3 J. Xie and Q. Zhang, Recent progress in rechargeable lithium batteries with organic materials as promising electrodes, *J. Mater. Chem. A*, 2016, **4**, 7091–7106.
- 4 M. Secchiaroli, S. Calcaterra, H. Y. Tran, S. J. Rezvani, F. Nobili, R. Marassi, M. W. Mehrens and S. Dsoke, Development of non-fluorinated cathodes based on  $\text{Li}_3\text{V}_{1.95}\text{Ni}_{0.05}(\text{PO}_4)_3/\text{C}$  with prolonged cycle life: a comparison among Na-alginate, Na-carboxymethyl cellulose and poly(acrylic acid) binders, *J. Electrochem. Soc.*, 2017, **164**, A672–A683.
- 5 M. Kuenzel, D. Bresser, T. Diemant, D. V. Carvalho, G.-T. Kim, R. J. Behm and S. Passerini, Complementary strategies toward the aqueous processing of high-voltage  $\text{LiNi}_{0.5}\text{Mn}_{1.5}\text{O}_4$  lithium-ion cathodes, *ChemSusChem*, 2018, **11**, 562–573.
- 6 T.-W. Kwon, J. W. Choi and A. Coskun, The emerging era of supramolecular polymeric binders in silicon anodes, *Chem. Soc. Rev.*, 2018, **47**, 2145–2164.
- 7 Y. Shi, X. Zhou and G. Yu, Material and structural design of novel binder systems for high-energy, high-power lithium-ion batteries, *Acc. Chem. Res.*, 2017, **50**, 2642–2652.
- 8 J.-T. Li, Z.-Y. Wu, Y.-Q. Lu, Y. Zhou, Q.-S. Huang, L. Huang and S.-G. Sun, Water soluble binder, an electrochemical performance booster for electrode materials with high energy density, *Adv. Energy Mater.*, 2017, **7**, 1701185.
- 9 D. L. Wood III, J. Li and C. Daniel, Prospects for reducing the processing cost of lithium ion batteries, *J. Power Sources*, 2015, **275**, 234–242.
- 10 Z. Chena, G.-T. Kim, D. Chao, N. Loeffler, M. Copley, J. Lin, Z. Shen and S. Passerini, Toward greener lithium-ion batteries: aqueous binder-based  $\text{LiNi}_{0.4}\text{Co}_{0.2}\text{Mn}_{0.4}\text{O}_2$  cathode material with superior electrochemical performance, *J. Power Sources*, 2017, **372**, 180–187.
- 11 T. Tanabe, T. Gunji, Y. Honma, K. Miyamoto, T. Tsuda, Y. Mochizuki, S. Kaneko, S. Ugawa, H. Lee, T. Ohsaka and F. Matsumoto, Preparation of water-resistant surface coated high-voltage  $\text{LiNi}_{0.5}\text{Mn}_{1.5}\text{O}_4$  cathode and its cathode performance to apply a water-based hybrid polymer binder to Li-ion batteries, *Electrochim. Acta*, 2017, **224**, 429–438.
- 12 T. Tanabe, Y. B. Liu, K. Miyamoto, Y. Irii, F. Maki, F. Maki, T. Gunji, S. Kaneko, S. Ugawa, H. Lee, T. Ohsaka and F. Matsumoto, Synthesis of water-resistant thin  $\text{TiO}_x$  layer-coated high-voltage and high-capacity  $\text{LiNi}_a\text{Co}_b\text{Al}_{1-a-b}\text{O}_2$  ( $a > 0.85$ ) cathode and its cathode performance to apply a water-based hybrid polymer binder to Li-ion batteries, *Electrochim. Acta*, 2017, **258**, 1348–1355.
- 13 K. Notake, T. Gunji, S. Kosemura, Y. Mochizuki, T. Tanabe, S. Kaneko, S. Ugawa, H. Lee and F. Matsumoto, The application of a water-based hybrid polymer binder to a high-voltage and high-capacity Li-rich solid-solution cathode and its performance in Li-ion batteries, *J. Appl. Electrochem.*, 2016, **46**, 267–278.
- 14 J. Paulsen and J. H. Kim, *High Nickel Content Cathode Material Having Low Soluble Base Content*, US Pat., US2014/0054495A1, 2013.
- 15 K. Soeda, M. Yamagata and M. Ishikawa, Alginic Acid as a New Aqueous Slurry-Based Binder for Cathode Materials of LIB, *ECS Trans.*, 2015, **64**, 13–22.
- 16 M. Morishita, T. Mukai, T. Sakamoto, M. Yanagida and T. Sakai, Improvement of Cycling Stability at 80 °C for 4 V-Class Lithium-Ion Batteries and Safety Evaluation, *J. Electrochem. Soc.*, 2013, **160**(8), A1311–A1318.
- 17 K. Kimura, T. Sakamoto, T. Mukai, Y. Ikeuchi, N. Yamashita, K. Onishi, K. Asami and M. Yanagida, Improvement of the cyclability and coulombic efficiency of Li-ion batteries using  $\text{Li}[\text{Ni}_{0.8}\text{Co}_{0.15}\text{Al}_{0.05}]\text{O}_2$  cathode containing an aqueous binder with pressurized  $\text{CO}_2$  gas treatment, *J. Electrochem. Soc.*, 2018, **165**, A16–A20.
- 18 K. Kimura, K. Onishi, T. Sakamoto, K. Asami and M. Yanagida, Achievement of the high-capacity retention rate for the  $\text{Li}[\text{Ni}_{0.8}\text{Co}_{0.15}\text{Al}_{0.05}]\text{O}_2$  (NCA) cathode containing an aqueous binder with  $\text{CO}_2$  gas treatment using the cavitation effect (CTCE), *J. Electrochem. Soc.*, 2019, **166**, A5313–A5317.
- 19 Y. Liu, T. Tanabe, Y. Irii, F. Maki, T. Tsuda, T. Gunji, S. Ugawa, Y. Asai, H. Lee, T. Ohsaka and F. Matsumoto, Optimization of Synthesis Condition of Water-Resistant and Thin Titanium Oxide Layer-Coated Ni-rich Layered Cathode Materials and Their Cathode Performance, *J. Appl. Electrochem.*, 2019, **49**, 99–110.
- 20 W. S. Kim, K. I. Chung, J. H. Cho, D. W. Park, C. Y. Kim and Y. K. Choi, Studies of a solid electrolyte interface coated with  $\text{Li}_2\text{CO}_3$  on the carbon electrode in Li-ion batteries, *J. Ind. Eng. Chem.*, 2003, **9**, 699–703.
- 21 X. Dai, A. Zhou, J. Xu, Y. Lu, L. Wang, C. Fan and J. Li, Extending the high-voltage capacity of  $\text{LiCoO}_2$  cathode by direct coating of the composite electrode with  $\text{Li}_2\text{CO}_3$  via magnetron sputtering, *J. Phys. Chem. C*, 2016, **120**, 422–430.





- 22 Z. Chen, C. Liu, G. Sun, X. Kong, S. Lai, J. Li, R. Zhou, J. Wang and J. Zhao, Electrochemical degradation mechanism and thermal behaviors of the stored  $\text{LiNi}_{0.5}\text{Co}_{0.2}\text{Mn}_{0.3}\text{O}_2$  cathode materials, *ACS Appl. Mater. Interfaces*, 2018, **10**, 25454–25464.
- 23 T. Hayashi, J. Okada, E. Toda, R. Kuzuo, N. Oshimura, N. Kuwata and J. Kawamura, Degradation Mechanism of  $\text{LiNi}_{0.82}\text{Co}_{0.15}\text{Al}_{0.03}\text{O}_2$  positive electrodes of a lithium-ion battery by long-term cycling test, *J. Electrochem. Soc.*, 2014, **161**, A1007–A1011.
- 24 <https://www.powrex.co.jp/mp-series-en>.
- 25 R. de Levie, *Aqueous Acid-base Equilibria and Titrations*, Oxford University Press, 1st edn, 1999.
- 26 M. Bichon, D. Sotta, N. Dupré, E. D. Vito, A. Boulineau, W. Porcher and B. Lestriez, Study of immersion of  $\text{LiNi}_{0.5}\text{Mn}_{0.3}\text{Co}_{0.2}\text{O}_2$  material in water for aqueous processing of positive electrode for Li-ion batteries, *ACS Appl. Mater. Interfaces*, 2019, **11**, 18331–18341.
- 27 R. Robert and P. Novák, Switch of the charge storage mechanism of  $\text{Li}_x\text{Ni}_{0.80}\text{Co}_{0.15}\text{Al}_{0.05}\text{O}_2$  at overdischarge conditions, *Chem. Mater.*, 2018, **30**, 1907–1911.

