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# Corrosion protection mechanism of Ce<sup>4+</sup>/organic inhibitor for AA2024 in 3.5% NaCl

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Cerium is a rare earth element that has been widely proposed for the corrosion protection of aluminium alloys (AA). Both cerium salts, Ce<sup>3+</sup> and Ce<sup>4+</sup>, have been used in combination with other compounds to offer synergistic inhibition, however, the inhibitive corrosion mechanism when using Ce<sup>4+</sup> with organic compounds is still not clear. In this study, the synergistic inhibition effect of Ce<sup>4+</sup> and melamine (M) on the corrosion of aluminium alloy 2024 (AA2024) in 3.5% NaCl solution was investigated. Potentiodynamic Polarization (PDP) and Electrochemical Impedance Spectroscopy (EIS) techniques were used to study the synergistic effect of different Ce<sup>4+</sup>/M ratios on the corrosion behaviour of AA2024. The PDP study showed that a combination of 50% Ce<sup>4+</sup> and 50% M leads to the lowest corrosion rates, both acting as cathodic inhibitors. Both PDP and EIS results indicated that M or Ce<sup>4+</sup> in isolation did not offer effective corrosion protection, while the combination of M and Ce<sup>4+</sup> significantly enhances the corrosion protection with a synergism parameter equal to 3.5. SEM and EDX observations confirm the findings from the electrochemical techniques. XPS was used to investigate the mechanism of protection, revealing that the reduction of Ce<sup>4+</sup> to Ce<sup>3+</sup> occurs during protection of AA2024. A new mechanism of corrosion synergistic inhibition by Ce<sup>4+</sup> and organic compounds is postulated where the role of the organic compounds is to enhance the reduction of Ce<sup>4+</sup>.

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## 1. Introduction

Aluminium is considered as the second most used metal in engineering applications. The continuous growth of aluminium consumption, especially in the fields of transport, engineering and packaging can be attributed to several of its properties, such as ease of recycling, low density, diversity of aluminium alloys and suitability for surface treatments.<sup>1</sup>

Aluminium alloy 2024 (AA2024) is perhaps the alloy that has been most widely used in aircraft applications.<sup>2</sup> The main alloying element of this alloy is copper, being added at 3.8–4.9%.<sup>3</sup> The high strength/weight ratio and good fatigue resistance of this alloy is a consequence of the presence of fine intermetallic particles (IMP). The IMPs are classified into three categories according to their size: (1) hardening precipitates (<0.1 μm), (2) dispersoids (0.01–0.1 μm) and (3) Inclusions (>1 μm). Although the latter do not provide a major contribution to the mechanical properties, they have a significant impact on the localized corrosion susceptibility of the alloy.<sup>4</sup> The localised corrosion includes pitting and stress corrosion cracking<sup>5</sup> where the IMP act as active cathodic sites accelerating corrosion of the aluminium matrix.<sup>6,7</sup>

A great deal of research and product development has been conducted to overcome this drawback including, mechanistic studies on conversion and organic coatings, and inhibitors.<sup>8–12</sup> Whilst many inhibitors have been used to control the corrosion of aluminium alloys, only a few of them can be used in industry due to restrictions derived from environmental legislation, most notably the ban on Cr(VI) systems. In order to reduce the environmental impact of chemical inhibitors, effective synergism is an important approach to decrease the concentration of chemicals within an inhibitor. This approach entails using a combination of inhibiting compounds whose effect is greater than the sum of any of the individual compounds. It can be achieved by the interaction between components of the inhibitor and/or between the inhibitor and ion(s) present in the solution.<sup>13</sup> The synergistic effect between organic–inorganic combinations has been studied for different alloys and solutions.<sup>14–18</sup> In general, the organic component is responsible for adsorption onto the metal surface through heteroatoms (N, O, S, and P), double/triple bonds or aromatic rings.<sup>19–21</sup>

Cerium salts have been widely used as corrosion inhibitors,<sup>11,22–25</sup> where the essential step of the inhibition mechanism involving cerium species, in an aerated neutral solution, is the formation of insoluble cerium oxides and/or hydroxides on the cathodic sites, where the oxygen reduction reaction is inhibited.<sup>25–27</sup> A number of workers have investigated the synergism of cerium with inorganic<sup>28–31</sup> and organic<sup>8,30,32–34</sup> materials as corrosion inhibitors. Also, the synergistic effect of using

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inhibitor anions, such as phosphate, with cerium cations to enhance corrosion inhibition efficiency has been studied.<sup>4,35</sup> However, only a few of these studies has been concerned with the use of  $\text{Ce}^{4+}$ .<sup>36–40</sup> The role of cerium in the corrosion inhibition process mainly depends on the oxidation state of cerium ion (*i.e.*  $\text{Ce}^{3+}$  or  $\text{Ce}^{4+}$ ) and the pH of the solution. Generally, the corrosion prevention property of cerium is related to the presence of  $\text{Ce}^{3+}$ .<sup>41–43</sup> Irrespective of cerium treatment, the prevention mechanism comprises two steps: (1) an insoluble oxide/hydroxide of  $\text{Ce}^{3+}$  is formed due to interaction with hydroxide ions on the cathodic sites where adequate concentration of  $\text{OH}^-$  is produced and (2) the formed insoluble Ce compound precipitates on the intermetallic particles.<sup>44–46</sup> Therefore, the cathodic reaction is inhibited and the corresponding anodic reaction significantly reduces. These two steps take more than 24 h to achieve suitable protection.<sup>47</sup> For AA2024 the reduction reaction was suppressed on intermetallic inclusions and it was found that the minimum concentration of  $\text{Ce}^{3+}$  in neutral NaCl electrolyte is 5 ppm.<sup>48</sup> For all cerium treatments, it can be concluded that the presence of  $\text{Ce}^{3+}$  is the key role in the protection of aluminium.

The synergistic effect of using  $\text{Ce}^{4+}$  with organic materials such as corrosion inhibitors has been studied.<sup>36,39,40,49–53</sup> Although,  $\text{Ce}^{3+}$  was not included in these studies and the crucial step of  $\text{Ce}^{3+}$  precipitation on the cathodic site was not clear, the inhibition efficiencies were improved by synergism.

Li *et al.*,<sup>40,49,51</sup> investigated the synergistic effect of using vanillin with  $\text{Ce}^{4+}$  for corrosion prevention of steel in HCl and  $\text{H}_2\text{SO}_4$ . In another study, iso-vanillin and  $\text{Ce}^{4+}$  were obtained and used for the corrosion prevention of steel in sulphuric acid.<sup>38</sup> Although, the XPS analysis clearly showed  $\text{Ce}^{3+}$  on the protected surface (>50% of the cerium components), the authors referred the presence of  $\text{Ce}^{3+}$  to the reduction of the protective  $\text{Ce}^{4+}$  film in air which is not feasible and further analyses were required to determine exactly or alternatively how  $\text{Ce}^{3+}$  is produced. In contrast to this findings, however, no evidence of that interaction with air was detected. In fact, vanillin is highly susceptible to oxidation<sup>54–56</sup> *i.e.* it can be used as a reducing agent, and consequently it may reduce  $\text{Ce}^{4+}$  to  $\text{Ce}^{3+}$ .

Further, the synergistic inhibition effect of  $\text{Ce}^{4+}$  with sodium oleate has been used for corrosion prevention of steel in an acidic solution.<sup>39</sup> The authors proposed that the enhancement in corrosion protection was due to the formation of a  $\text{Ce}^{4+}$  complex which was adsorbed onto the metal surface forming a protective layer. However, sodium oleate can work as a reducing agent<sup>57,58</sup> by breaking the  $\text{C}=\text{C}$  group.<sup>59</sup>

Another study showed that L-phenylalanine/ $\text{Ce}^{4+}$  improved the corrosion prevention of copper in HCl solution.<sup>36</sup> The authors also related the corrosion inhibition to the formation of a complex; nevertheless, the ease of oxidation of L-phenylalanine in aqueous solution<sup>60</sup> was not taken in consideration.

Li *et al.* studied the synergistic inhibition effect of  $\text{Ce}^{4+}$  with 3,4-dihydroxybenzaldehyde on cold rolled steel in sulphuric acid<sup>50</sup> and hydrochloric acid solutions.<sup>61</sup> The corrosion prevention mechanism was based on the formation of a complex between  $\text{Ce}^{4+}$  and 3,4-dihydroxybenzaldehyde.

Although, this hypothesis was built upon the capability of  $\text{Ce}^{4+}$  to form a complex (*via* vacant orbits 4f, 5d and 6s), no chemical analysis was applied to confirm the composition of the complex. Again, the ease of oxidation of 3,4-dihydroxybenzaldehyde<sup>62–65</sup> was not discussed.

Hany<sup>66</sup> also studied the synergistic corrosion inhibition of  $\text{Ce}^{4+}$  with polyethylene glycols (PEG) on carbon steel in dilute sulphuric acid solution. The author referred the enhancement in the corrosion prevention to the formation of a complex that formed from  $\text{Ce}^{4+}$  and polyethylene glycols, however, no further analysis was performed to confirm this assumption. Other studies were performed confirming the ease of oxidation of PEG,<sup>67–71</sup> and also that  $\text{Ce}^{4+}$  can be used to catalyse the oxidation reaction of PEG in sulphuric acid solution.<sup>72,73</sup>

Finally, vanillin, iso-vanillin and 3,4-dihydroxybenzaldehyde have been used as electron donors<sup>74</sup> and, they have some activity in presence of  $\text{Al}_2\text{O}_3$ .<sup>75</sup> These properties were not taken in account during these studies.

This current study attempts to understand the potential synergistic effect between melamine and  $\text{Ce}^{4+}$ , in the form of cerium(IV) sulphate. A novel corrosion inhibitor (SY) consisting of melamine with cerium sulphate was developed for the corrosion resistance of AA2024 in 3.5% NaCl solution. The synergistic effect was investigated based on electrochemical measurements; PDP and EIS. Surface morphology was also studied using an SEM. A corrosion mechanism was postulated based on the results obtained from the electrochemical analysis along with X-ray photoelectron spectroscopy (XPS).

## 2. Experimental

### 2.1 Material

Aluminium alloy AA2024 samples were obtained from Q-panels with the following composition:

AA2024	Si	Fe	Cu	Mn	Mg	Cr	Zn	Ti	Al
	0.50	0.50	3.8–4.9	0.30–0.9	1.2–1.8	0.10	0.25	0.15	Remainder

Rectangular coupons of the alloy with dimensions 25 mm × 25 mm × 1 mm were used as the substrate material (working electrode). The surface of the coupon was first ground with 320, 600 and 1200 grit abrasive SiC paper to remove scale and contamination from the surface. The ground specimen were degreased in ethanol then with deionised water then dried by a stream of air for 30 s and kept in an airtight desiccator at room temperature.

All chemicals were used 'as received' without further purification or treatment and all the solutions were prepared with deionized water. Melamine, cerium(IV) sulphate and sodium chloride were obtained from Sigma-Aldrich. The blank corrosive electrolyte was prepared by dissolving NaCl in deionised water forming a 3.5 wt% solution, being representative of artificial sea water. This corrosive solution has been widely used for testing the corrosion resistance of aluminium alloys. Each inhibitor was then added separately to the blank corrosive solution forming different inhibited electrolyte.



## 2.2 Characterization techniques

All corrosion tests were conducted in a standard one litre three-electrode cell. The sample represents the working electrode; two platinum electrodes were used as the counter electrodes and a saturated calomel electrode (SCE) as the reference electrode. The ohmic contribution was minimized by coupling the SCE to a fine capillary tube that was kept close to the working electrode.

Potentiodynamic polarization (PDP) scans were performed using an initial delay time at steady open-circuit potential (OCP) for 60 min to stabilize the surface. The polarization scan commenced in the cathodic region, scanning positively to anodic region in the potential range of  $-250$  to  $+250$  mV with respect to OCP, at a rate of  $0.5 \text{ mV s}^{-1}$ .

From the results the inhibition efficiency (IE%) was calculated using eqn (1),<sup>12</sup>

$$\text{IE}\% = \frac{(I_{\text{corr}}^{\circ} - I_{\text{corr}})}{I_{\text{corr}}^{\circ}} \times 100 \quad (1)$$

where:  $I_{\text{corr}}^{\circ}$  is the corrosion current density of the blank sample and  $I_{\text{corr}}$  is the corrosion current density of the inhibited sample.

EIS tests were performed at room temperature in the same electrochemical cell used for potentiodynamic polarization. The EIS tests were performed over a frequency range of  $10^5$ – $10^{-2}$  Hz with 10 mV peak to peak amplitude, using an AC signal at OCP.

A Gamry™ potentiostat/galvanostat, model reference-600 was used for all electrochemical measurements, where, the ratio of corrosive solution volume to sample surface area is not less than  $40 \text{ ml cm}^{-2}$  for all experiments. The impedance experimental results were fitted to equivalent electrical circuits using the nonlinear least square fitting technique provided by the Gamry™ software.

Each experiment was performed at least three times to ensure reproducibility of the results. The electrochemical experimental results were plotted using SigmaPlot software and uncertainties were calculated and attached to appropriate results.

The morphology and composition of the corroded samples were investigated by scanning electron microscopy (SEM) using a Zeiss-EVO-10, equipped with Energy Dispersive X-ray Spectroscopy (EDX).

Photoelectron spectroscopic (XPS) analysis was performed using a mono-chromated Al K X-ray source (1486.6 eV) typically operated at 10 mA emission current and 10 kV anode potential  $-100 \text{ W}$ . The take-off angle for the photoelectron analyser is  $90^\circ$  and acceptance angle of  $30^\circ$  and the data analysis was carried out using CASAXPS software. The main C 1s peak (284.7 eV) was selected to correct the high resolution scans.<sup>76</sup> Survey scans were run for 10 minutes and high resolution scans were run for between 2–3 minutes depending on the signal. The analysis chamber pressure was better than  $5 \times 10^{-9} \text{ mmHg}$ . During XPS studies Shirley background subtraction and Gaussian shaped were applied in the XPS spectrum peak fitting procedure.

## 3. Results and discussion

### 3.1 Corrosion measurements of AA2024 in 3.5% NaCl solution

The inhibition effect of the novel inhibitor 'SY' on the corrosion behaviour of AA2024 in 3.5% NaCl solution was investigated by two electrochemical techniques; PDP and EIS. To select the optimum ratio of the mix of  $\text{Ce}^{4+}$  and melamine, the PDP technique was applied and the inhibition efficiency was calculated from the results.

Fig. 1 illustrates the polarization curves of AA2024 with different concentration ratios of melamine to  $\text{Ce}^{4+}$  at a total concentration of 10 ppm over a potential range of  $\pm 250$  mV versus OCP showing both cathodic and anodic polarization curves. The blank sample shows the highest corrosion current density with respect to different concentration ratios. Also, it seems that all additives improve the cathodic polarization than the anodic one. The ratio of 50 : 50% melamine to  $\text{Ce}^{4+}$  appears to have the minimum corrosion current density,  $I_{\text{corr}}$ .

Fig. 2 shows the inhibition efficiency ( $E\%$ ) of the Tafel extrapolation curves. It can be seen that the synergism between melamine and  $\text{Ce}^{4+}$  ion was revealed. Specifically, the inhibition efficiency for the combination of melamine and  $\text{Ce}^{4+}$  is much greater than the summation of that for melamine and  $\text{Ce}^{4+}$  individually. The greatest inhibition efficiency,  $90.4 \pm 1.8\%$ , was achieved by a blend of 5 ppm  $\text{Ce}^{4+}$  and 5 ppm melamine which was chosen to represent the SY composition throughout the rest of this study.

To evaluate the synergistic effect of  $\text{Ce}^{4+}$  and melamine, blank solutions (B), containing either melamine (M), or ceric sulphate (C) were prepared at a concentration of 5 ppm.

The AA2024 samples were separately tested with different inhibitor solutions; M, C, and SY. The typical potentiodynamic polarization curves for different samples as measured in aerated 3.5% NaCl solution are superimposed in Fig. 3. The figure demonstrates anodic and cathodic polarization behaviour of the AA2024. The associated corrosion kinetics

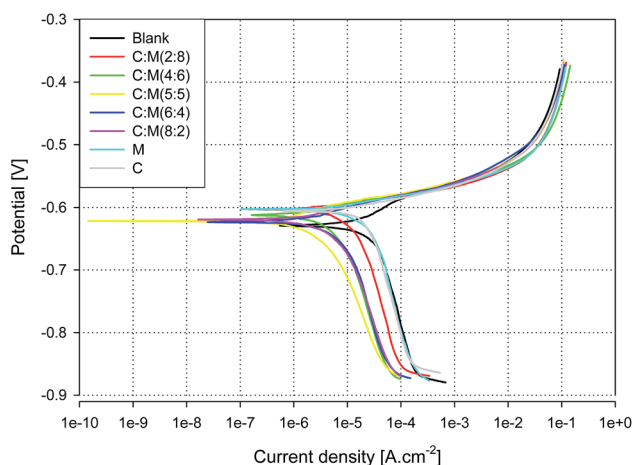


Fig. 1 Tafel curves of AA2024 in 3.5% NaCl at room temperature with different concentration ratios  $\text{Ce}^{4+}$  to melamine at a total blend concentration of 10 ppm.

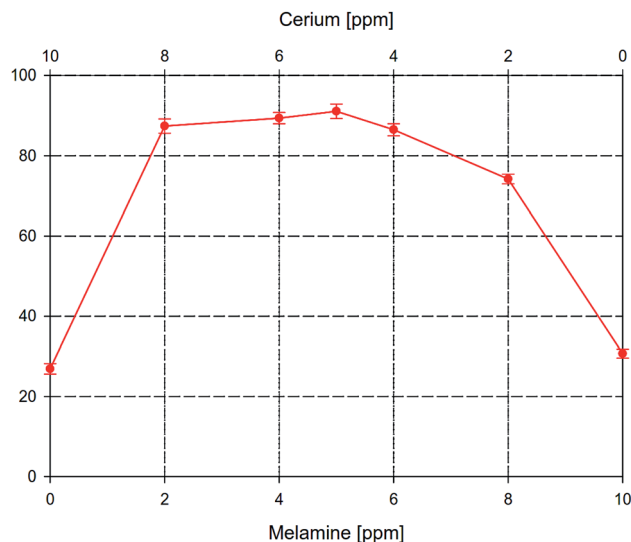


Fig. 2 The inhibition efficiency of AA2024 in 3.5% NaCl at room temperature with different concentration ratios  $Ce^{4+}$  to melamine.

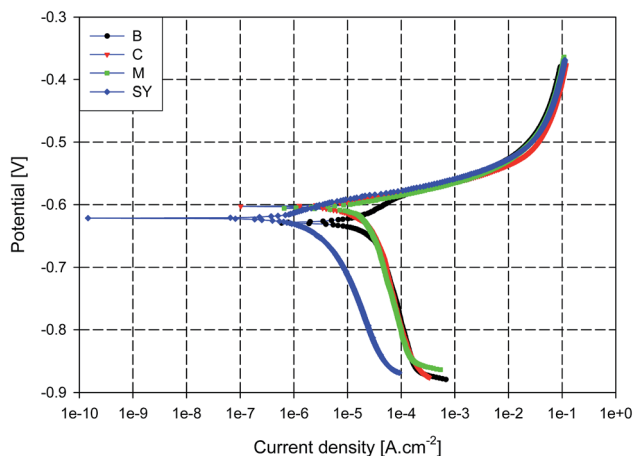


Fig. 3 Tafel plots of AA2024 in 3.5% NaCl solution with different addition at room temperature.

parameters ( $E_{corr}$ ,  $\beta_c$ ,  $\beta_a$ ,  $I_{corr}$ , IE%) were determined by extrapolating the cathodic and anodic Tafel lines of each curve.

It can be seen from Fig. 3 that the corrosion current density of SY sample is much smaller than the other three solution conditions. Also, the anodic branch of all samples seems to be identical that the decrease in  $I_{corr}$  appears to be due to a decrease in the cathodic current suggesting that SY

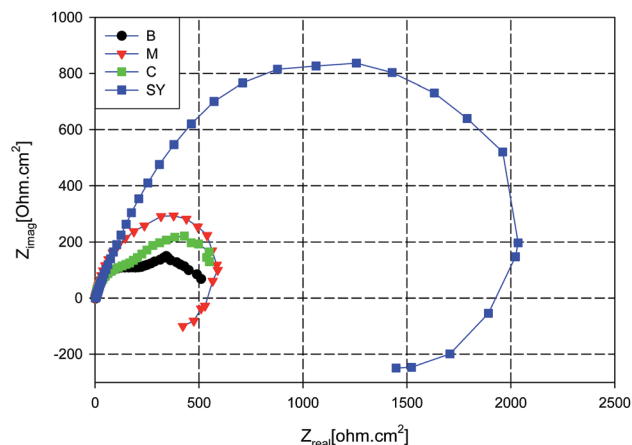


Fig. 4 Nyquist plots for AA2024 after 24 h in 3.5% NaCl solution with different additives at room temperature.

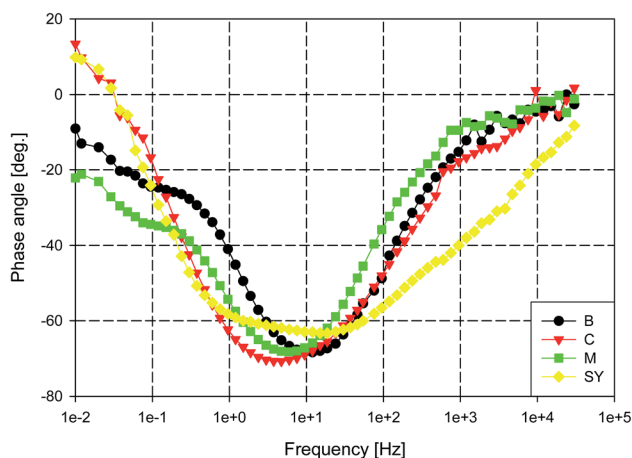


Fig. 5 Phase angle plots for AA2024 in 3.5% NaCl solution with different additives at room temperature.

acts as a cathodic type inhibitor.<sup>77–79</sup> Also, samples M and C show little effect on the corrosion behaviour of AA2024 sample where M and C have a typical corrosion current which is marginally smaller than that of B. These results are consistent with previous results<sup>41</sup> where low concentration of  $Ce^{4+}$  did not offer corrosion protection for AA2024. For all samples, the current density abruptly increases in the anodic polarization direction beyond the corrosion potential,  $E_{corr}$ , and no passive region is observed reflecting the risk of localized corrosion.

Table 1 Corrosion kinetic parameters of AA2024 with different inhibitors

Conc. [ppm]	$\beta_a$ [mV dec <sup>-1</sup> ]	$\beta_c$ [mV dec <sup>-1</sup> ]	$E_{corr}$ [mV]	$I_{corr}$ [mA cm <sup>-2</sup> ]	IE%
B	32	248	$-629 \pm 2$	$5.2 \pm 0.3 \times 10^{-5}$	—
M	28	249	$-603 \pm 4$	$3.8 \pm 0.2 \times 10^{-5}$	$26.9 \pm 1.3$
C	25	238	$-606 \pm 2$	$3.6 \pm 0.3 \times 10^{-5}$	$30.7 \pm 1.5$
SY	30	225	$-615 \pm 3$	$0.5 \pm 0.1 \times 10^{-5}$	$90.4 \pm 1.8$





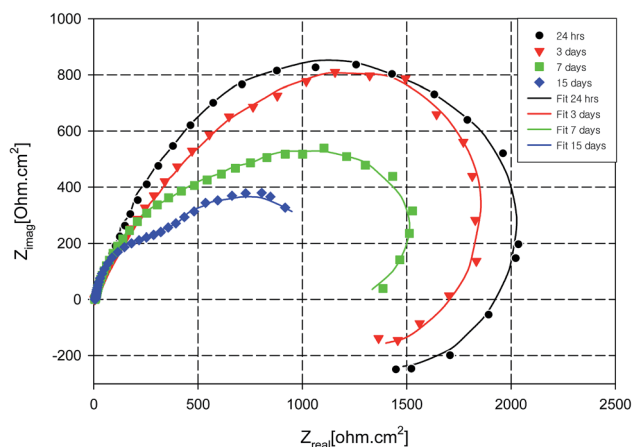


Fig. 6 Temporal Nyquist plots for AA2024 in 3.5% NaCl solution with SY inhibitor at room temperature.

Table 1 gives the electrochemical kinetic parameters of Tafel extrapolations ( $E_{\text{corr}}$ ,  $\beta_c$ ,  $\beta_a$ ,  $I_{\text{corr}}$ , IE%). From the table, the anodic,  $\beta_a$ , and the cathodic,  $\beta_c$ , slopes of all samples are close to each other. This behaviour suggests that the presence of different additives does not affect the mechanism of both anodic and cathodic reactions but changes the rates of corrosion. The table also shows that the corrosion current density ( $I_{\text{corr}}$ ) of SY sample is much smaller than those of other samples. Finally, the addition of  $\text{Ce}^{4+}$  ion alone does not significantly decrease the corrosion rate of AA2024 alloy which is in a good agreement with previous studies.<sup>49,50</sup>

The synergistic parameter ( $S$ ) is an expression to compare the expected corrosion rate, when either A or B is present and does not interact, with the experimentally measured rate in the presence of the inhibitor mixture. The mathematical expression of synergism parameter,  $S$ , for a mixture of two inhibitors, A and B, is given in eqn (2);<sup>80,81</sup>

$$S = \frac{1 - \eta_A - \eta_B - (\eta_A \eta_B)}{1 - \eta_{(AB)}} \quad (2)$$

where  $\eta_A$  and  $\eta_B$  are the inhibition efficiencies determined for compounds A and B respectively and  $\eta_{AB}$  is the inhibition efficiency for the mixture A + B (concentrations of A and B in the mixture should be the same as in the corresponding separate situations).<sup>50,53</sup> The synergism between the two substances manifests itself when the value of  $S$  is greater than unity, whereas when  $S$  is less than unity the synergy is antagonistic.

The value of  $S$  was calculated from Table 1 and it was found to be 3.5 indicating ceric sulphate and melamine have a synergistic effect in corrosion prevention of alloy AA2024 in 3.5% NaCl solution.

From the above discussion, it can conclude that AA2024 is susceptible to localized corrosion when immersed in 3.5% NaCl solution. In addition, melamine or  $\text{Ce}^{4+}$  sulphate solely cannot protect AA2024 from corrosion in that electrolyte.

For a better understanding of the corrosion performance of SY and to confirm the PDP results, electrochemical impedance spectroscopy (EIS) measurements were performed after 24 h of immersion in 3.5% NaCl solution. EIS was conducted for B, C, M and SY samples.

Fig. 4 illustrates the Nyquist plots of AA2024 in aerated 3.5% NaCl at open circuit potential with different additives. In addition, EIS for the blank sample was also presented for comparison. The plots do not show perfect semicircles due to the frequency dispersion and the inhomogeneity of the surface.<sup>82,83</sup> It can be seen that the diameter of the SY Nyquist' semicircle is much greater than for the other additives which indicates that SY affords superior corrosion protection for AA2024 in this electrolyte. Also, the diameters of M and C Nyquist' capacitive loop are slightly greater than that of the blank sample which reflects the slight improvement in the corrosion resistance due to addition of each of them. The figure also shows an inductive behaviour for both M and SY samples. The physical explanation of an inductive loop at low-frequency range is not sufficiently clear; it has been attributed to adsorption processes and/or formation of passive layer and/or redox activity.<sup>84</sup> The inductive loop of the M sample may be due to the relaxation process occurred by adsorption of organic compound, melamine, on the metal surface.<sup>85,86</sup> Also, SY shows an inductive loop at low frequency range which may point to redox activity<sup>7,87</sup> and/or the relaxation process of adsorption. The adsorption process may be attributed to the presence of the organic component, melamine; however the redox activity would be due to the presence of  $\text{Ce}^{4+}$  which is the candidate undergoing the redox process.

The total diameter of the semicircles can be used to represent the total resistance of the metal with different additives;<sup>88</sup> consequently it is used to calculate the synergistic factor,  $S$ , according to eqn (1), where it is equal to 3.4 which is comparable with that of PDP measurements.

The phase plots of these samples are presented in Fig. 5, where B and M samples show a time constant at low frequency

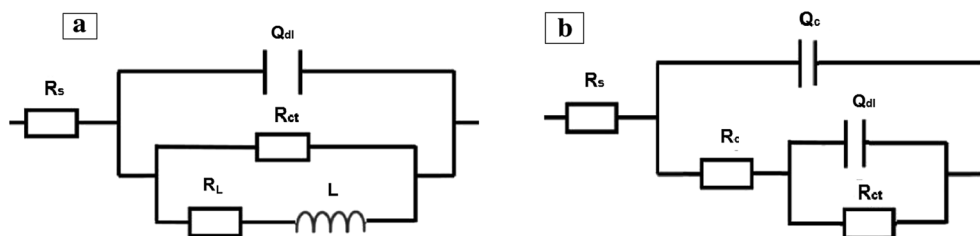


Fig. 7 Typical (a) one-time and (b) two-times constant electrical equivalent circuits used for modelling of impedance data.



Table 2 EIS fitting parameters of AA2024 immersed in 3.5% NaCl solution with different additives

	$Q_c$			$Q_{dl}$					
	$R_s [\Omega \text{ Cm}^2]$	$Y_o [\mu\Omega^{-1} \text{ cm}^{-2} \text{ s}^n]$	$n$	$R_c [\Omega \text{ Cm}^2]$	$Y_o [\mu\Omega^{-1} \text{ cm}^{-2} \text{ s}^n]$	$n$	$R_{ct} [\Omega \text{ Cm}^2]$	$R_L [\Omega \text{ Cm}^2]$	$L [\text{kH cm}^{-2}]$
B	$1.2 \pm 0.4$	$10\,472.1 \pm 107$	$0.931 \pm 0.03$	$191 \pm 14$	$786.3 \pm 24$	$0.945 \pm 0.01$	$326 \pm 27$	—	—
C	$1.2 \pm 0.3$	$1013.4 \pm 94$	$0.906 \pm 0.04$	$162 \pm 33$	$758.8 \pm 39$	$0.947 \pm 0.03$	$407 \pm 14$	—	—
M	$1.9 \pm 0.2$	—	—	—	$890.3 \pm 54$	$0.981 \pm 0.04$	$510 \pm 54$	$231 \pm 34$	$16.06 \pm 11$
SY	$1.5 \pm 0.3$	—	—	—	$599.9 \pm 12$	$0.721 \pm 0.02$	$2092 \pm 92$	$541 \pm 31$	$462.7 \pm 9$
SY 3 days	$0.8 \pm 0.1$	—	—	—	$519.6 \pm 32$	$0.888 \pm 0.01$	$1863 \pm 91$	$461 \pm 22$	$143.9 \pm 12$
SY 7 days	$1.1 \pm 0.3$	—	—	—	$359.7 \pm 43$	$0.910 \pm 0.03$	$1573 \pm 72$	$214 \pm 42$	$139.7 \pm 14$
SY 15 days	$1.4 \pm 0.2$	$199.5 \pm 12$	$0.365 \pm 0.01$	$239 \pm 34$	$531.1 \pm 27$	$0.971 \pm 0.01$	$828 \pm 31$	—	—

range. For aluminium alloys, this time constant with low impedance typically represents the formation of corrosion products at the metal surface.<sup>77,89</sup> Visual inspection clearly indicated that B, M and C were corroded after 3 days of immersion and the corrosion products were observed on the metal surface. In addition, the adsorption process related to the presence of melamine seems insufficient to offer corrosion protection to AA2024. On the other hand, SY sample continues to offer corrosion protection to AA2024 over a longer period of immersion, 15 days, as indicated by Fig. 6. The inductive behaviour at low frequency decreases with immersion time and finally, after 15 days, a capacitive behaviour is observed instead of that inductive one. Although, the total impedance of the SY sample decreases gradually with immersion time, visual inspection clearly indicated that there is no corrosion products on the sample surface. Also, the optical observation of SY sample (not presented) showed yellowish stains which may accompany the presence of the cerium inhibitive layer on the metal surface.<sup>90,91</sup> This behaviour suggests that the initial inductive loop was not related to the corrosion process.

The EIS experimental data was fitted to equivalent electrical circuits and all EIS parameters were calculated. The circuit shown in Fig. 7a was used to fit the experimental results of melamine and SY sample during the immersion in the corrosive solution in the first week of immersion period, while the circuit presented in Fig. 7b was used to fit the data for immersion periods beyond 1 week. The circuit in Fig. 7b was also used to fit the experimental result of the blank and cerium-only samples. A constant phase element ( $Q$ ) is used instead of pure capacitance due to the porous corrosion products and surface roughness.<sup>92,93</sup> In the circuits shown,  $R_s$  represents the solution

electrical resistance,  $R_{ct}$  is the charge transfer resistance,  $Q_{dl}$  is the double layer capacitance,  $R_L$  is the inductance resistance,  $L$  is the inductance element,  $R_c$  is the resistance of the layer formed on the metal surface and  $Q_c$  is the layer capacitance. The layer formed in the case of the SY sample is considered to be a protective layer, while in the case of B, and C samples this layer is considered to be corrosion products. The fitting results of the Nyquist plots are listed in Table 2. It can be noticed that the charge transfer resistance of SY sample is much greater than that of B, C, or M samples after 24 h of immersion in the NaCl corrosive electrolyte. Also, the charge transfer resistance of SY sample decreased with time of immersion indicating the decrease of corrosion protective performance for the AA2024 substrate. This behaviour may be due to the long immersion term with low inhibitor concentration. The capacitive behaviour of the double layer capacitance did not significantly change ( $n$  closes to unity).

From the above discussion, it is concluded that melamine or  $\text{Ce}^{4+}$ , in isolation, does not offer corrosion protection for AA2024 in artificial sea water. Although SY contains the same amount of cerium as the C sample and the same amount of melamine as the M sample, the combination of M + C significantly decreases the corrosion rate of AA2024 in 3.5% NaCl solution, confirming the synergistic effect.

### 3.2 Surface analysis

Fig. 8 depicts the appearance of a blank aluminium sample surface after 72 h of immersion in the 3.5% NaCl electrolyte. The image and EDX analysis clearly show pitting corrosion around the IMP containing copper, magnesium and iron. The pitting (arrowed) comprises dissolution of aluminium matrix



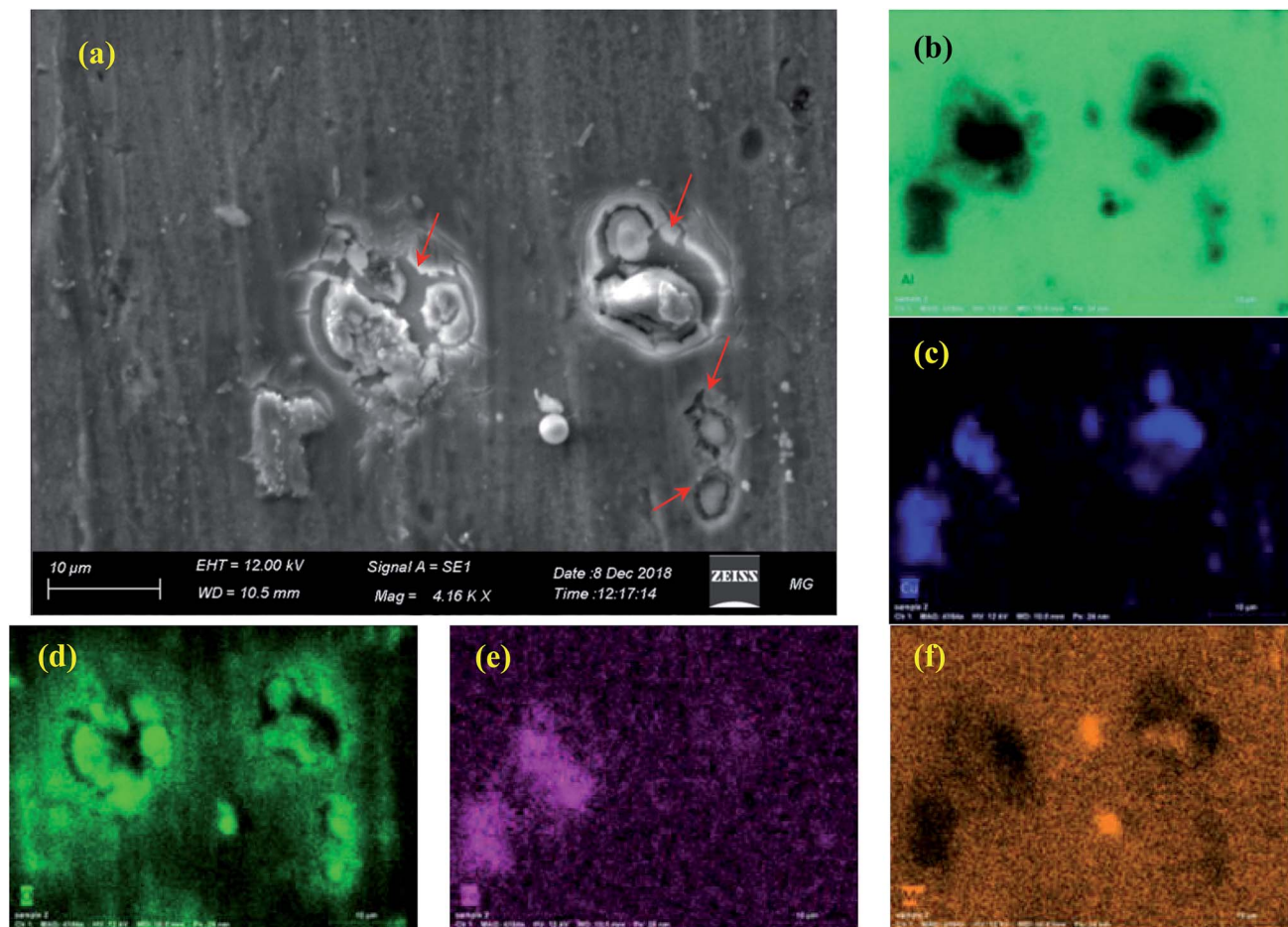


Fig. 8 (a) SEM image with corresponding (b) Al, (c) Cu, (d) O, (e) Fe and (f) Mg EDX maps. of the blank sample after 72 h immersion in 3.5% NaCl at room temperature.

around IMP containing copper, which are cathodic with respect to the aluminium matrix.

Fig. 9 illustrates the SEM images of AA2024 after immersion in NaCl electrolyte in the present of melamine and ceric sulphate separately. The images demonstrate that both of sample surfaces show pitting corrosion covering the entire surface (arrows). These results indicate that each of  $\text{Ce}^{4+}$  and

melamine, in isolation, cannot protect AA2024 in a neutral NaCl solution, confirming the electrochemical results.

Fig. 10 illustrates the SEM analysis of the SY sample, which clearly shows that there is negligible sign of localized corrosion on the aluminium surface after 72 h of immersion in the corrosive electrolyte. The SY inhibitor provides higher corrosion protection to AA2024 when compared to that of the blank,

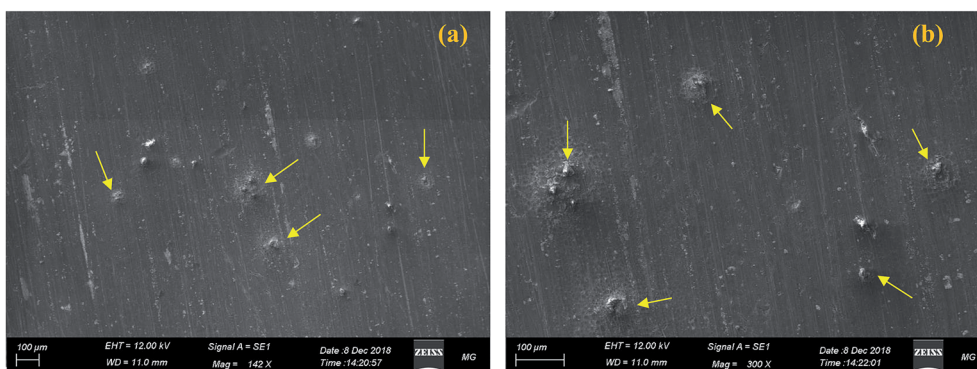


Fig. 9 SEM images of AA2024 after 72 h immersion in 3.5% NaCl containing 5 ppm of (a) C and (b) M.





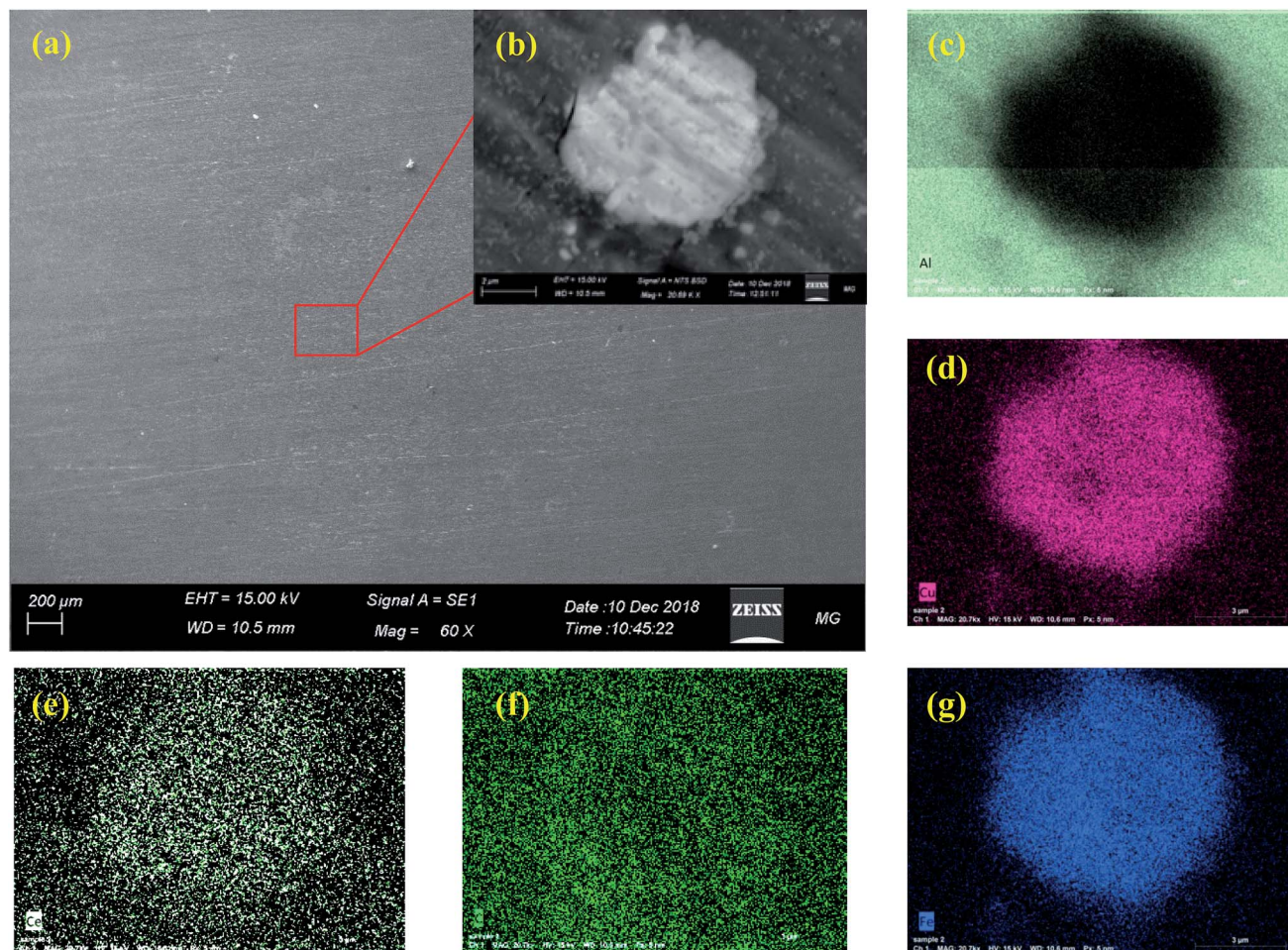


Fig. 10 SEM images of SY sample (a) low and (b) high magnification, with corresponding (c) Al, (d) Cu, (e) O, (f) Fe and (g) Mg EDX mapping after 72 h immersion in 3.5% NaCl at room temperature.

melamine and ceric sulphate samples which confirms the results of the electrochemical techniques. Also, the EDX mapping of a high magnification back scatter image of an IMP, Fig. 10b, depicts that it contains copper, iron, carbon and cerium as indicated by Fig. 10c–g. Also, it does not show any sign of localized corrosion due to the deposition of cerium on this spot. This IMP with a high content of copper would be

cathodic with respect to the aluminium matrix. Also, the EDX map of cerium seems to be identical as that of copper. The presence of copper as the main alloying elements of AA2024 enhances the nucleation and precipitation of cerium on cathodic sites.<sup>94</sup> These results confirm that cerium acts as a cathodic inhibitor and are in a good agreement with the potentiodynamic polarization results. Also, EDX mapping

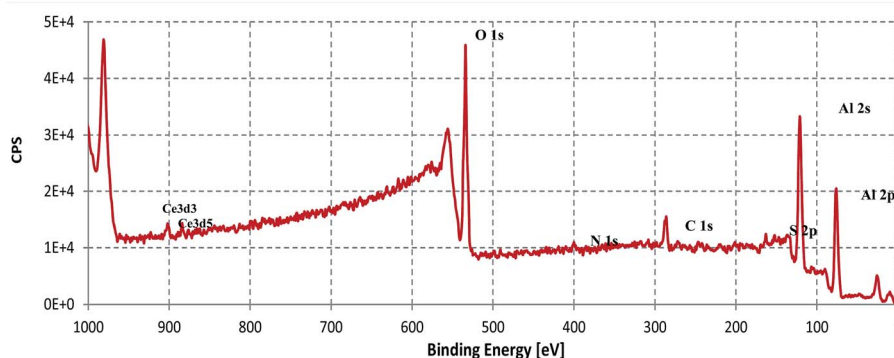


Fig. 11 XPS survey scan of the SY sample immersed in 3.5% NaCl for 48 h at room temperature.





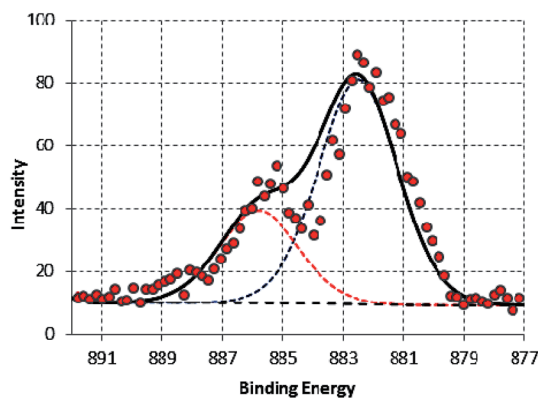


Fig. 12 High-resolution XPS Ce 3d5 of SY sample after 48 h immersion in 3.5% NaCl at room temperature.

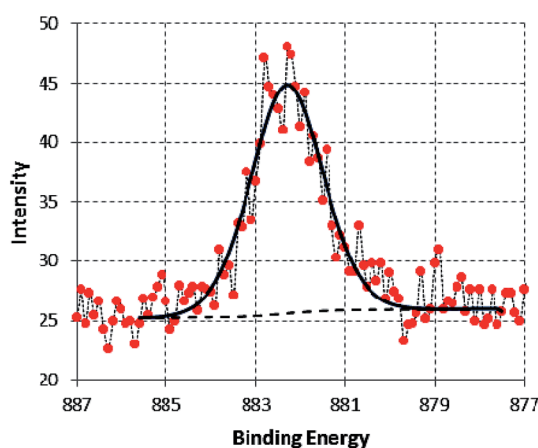


Fig. 13 High-resolution XPS Ce 3d5 of  $\text{Ce}(\text{SO}_4)_2$  powder.

shows that the carbon appears mainly around the IMP where the main source of this carbon is the melamine. These results indicate that Ce and melamine do not cover the exact same area indicating they are not in the same molecule.

### 3.3 Corrosion mechanism

**3.3.1 XPS study.** Determination of the oxidation state of the precipitated cerium on the substrate surface is key to understanding the mechanism of corrosion inhibition. In this respect, XPS is a suitable tool to study the cerium oxidation state at the metal surface.

The XPS survey scan of the SY sample immersed in 3.5% NaCl for 48 h, at room temperature, is shown in Fig. 11. The figure contains Al, O, C, N, Ce and S.

A high-resolution spectrum of the Ce 3d peak is shown in Fig. 12. The overall envelope indicates that it contains two components located at  $885.8 \pm 0.2$  eV and  $882.6 \pm 0.2$  eV corresponding to  $\text{Ce}^{3+}$  and  $\text{Ce}^{4+}$  (ref. 40, 47 and 95) with 31.1%  $\text{Ce}^{3+}$ . To investigate the source of  $\text{Ce}^{3+}$ , XPS analysis was applied for the raw source of cerium,  $\text{Ce}(\text{SO}_4)_2$ . The corresponding high-resolution spectra of Ce 3d is illustrated in Fig. 13. The spectra clearly shows a single component at  $882.5 \pm 0.2$  which

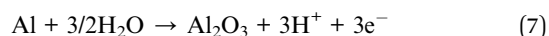
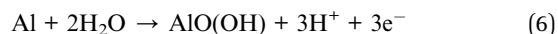
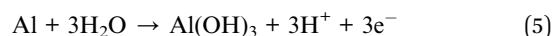
corresponding to  $\text{Ce}^{4+}$ . These results confirm that  $\text{Ce}^{4+}$  reduces to  $\text{Ce}^{3+}$  in this corrosive electrolyte containing melamine besides the metal substrate. This result is consistent with the findings of Matter *et al.*<sup>41</sup> although, the authors did not point to the reduction reaction of  $\text{Ce}^{4+}$  to form  $\text{Ce}^{3+}$ .

**3.3.2 Corrosion of AA2024.** Generally, the corrosion mechanism of copper–aluminium alloys, 2xxx series, is predominantly influenced by the presence of IMPs. Cu-containing alloys such as AA2024 are subjected localized corrosion in solutions that contains  $\text{Cl}^-$  as a result of the presence of, for instance;  $\text{AlCuMnFe}$ ,  $\text{Al}_2\text{CuMg}$  and  $\text{AlCu}_2$ , each having a different corrosion potential to that of the aluminium matrix. The shape and size of the localized pitting, varies according to the nature and size of these IMPs.<sup>3</sup> Inclusions with particle size  $>1 \mu\text{m}$  are not only responsible for initiating pitting corrosion, but they also do not contribute to the mechanical properties of the alloys.<sup>4,44,96,97</sup>

In aerated NaCl solution, the oxygen reduction reaction (low over-potentials) governs the cathode process of an AA2024 sample (eqn (3)), being the electron acceptor reaction from the oxidation of the metal (eqn (4));



Dissolution of the aluminium matrix, in  $\text{Cl}^-$  containing solutions, occurs through a series of oxidation reactions producing a  $\text{Al}(\text{OH})\text{Cl}^+$  complex which is dissolved in such aqueous solution as follows;



IMP provide the cathodic sites at which the oxygen reduction reactions occur. The matrix adjacent to the IMP is the site at which pitting corrosion takes place. Therefore the key to an effective inhibition is to hinder or stop one or both of the cathodic and anodic reactions.

**3.3.3 Proposed mechanism.** In the case of corrosion inhibition by an active organic component with  $\text{Ce}^{4+}$ , two mechanisms of corrosion prevention are suggested:

(1) A complex is formed between the organic component and  $\text{Ce}^{4+}$  via vacant orbital filling. In this mechanism, the complex is adsorbed on the metal substrate to hinder both cathodic and anodic reactions. In this case the inhibitor would be of a mixed type inhibitor.

(2) The second mechanism is a reduction reaction of  $\text{Ce}^{4+}$  to form  $\text{Ce}^{3+}$  (eqn (9)), which takes place within 24 h.<sup>47,98</sup> It is acceptable to assume that the anodic reaction is the oxidation of aluminium matrix (eqn (4)).<sup>99</sup> The formed  $\text{Ce}^{3+}$  in turn reacts to form a thin hydroxide layer of  $\text{Ce}^{3+}$  (eqn (10)).  $\text{H}_2\text{O}_2$  is formed as an intermediate of oxygen reduction, (eqn (11a)) from which



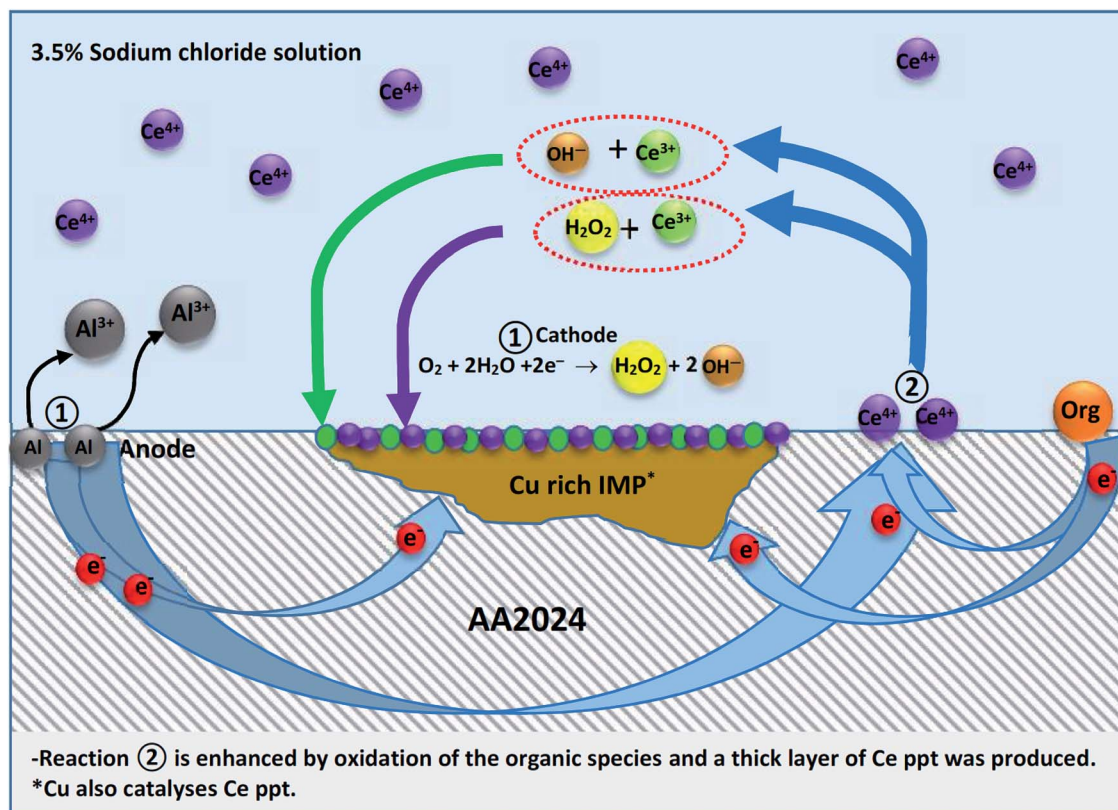
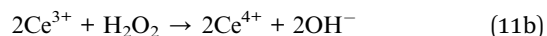
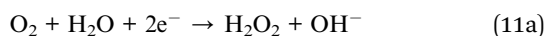


Fig. 14 Proposed corrosion protection mechanism of  $\text{Ce}^{4+}$ /organic inhibitor for AA2024.

$\text{Ce}^{4+}$  precipitation at the cathodic IMP sites occurs (eqn (11b)).<sup>41,99</sup> This thin cerium salt layer does not appear to be sufficient to achieve corrosion protection *via* inhibiting the cathodic reactions. When another compound susceptible to oxidation reaction is present (such as melamine and the other previously used compounds: vanillin, iso-vanillin, sodium oleate and 3,4-dihydroxybenzaldehyde) more electrons are offered to enhance the reduction of  $\text{Ce}^{4+}$  forming a thicker layer of cerium precipitate protecting the metal surface. In this case, cathodic type inhibitor is predominant.



Both mechanisms are valid and the predominant mechanism may depend on the total concentration of the inhibitor (organic component and  $\text{Ce}^{4+}$ ), the organic component/ $\text{Ce}^{4+}$  ratio and the pH.

In the present case, the total concentration of the inhibitor is limited to 10 ppm, and the organic component/ $\text{Ce}^{4+}$  ratio is 1 : 1. Also, the SY ( $\text{Ce}^{4+}$ /melamine) sample clearly showed superior protection for AA2024 where cerium precipitation was observed at the cathodic sites. In addition, the PDP results

showed that SY is predominantly a cathodic inhibitor. Further, EIS indicated that the SY sample may exhibit a redox reaction(s) during immersion of AA2024 in the aerated NaCl solution. In the same context, this redox activity does not appear in the absence of melamine indicating that melamine facilitates the redox process. This process was reflected in the XPS analysis where, it showed  $\text{Ce}^{3+}$  at the SY sample surface. Therefore, the second corrosion prevention mechanism, discussed above, seems to be predominant and the mechanism is displayed in Fig. 14.

The mechanism of protection AA2024 in the presence of both  $\text{Ce}^{4+}$  and melamine can be summarized as follows;  $\text{Ce}^{3+}$  is produced from a set of complicated reduction reaction(s) of  $\text{Ce}^{4+}$  that is improved in the presence of melamine. Melamine can not only be oxidized<sup>100,101</sup> but also can be used as a structure-director and stabilizing agent<sup>102</sup> during the precipitation of cerium on the metal surface. In addition, its molecule contains 6 nitrogen atoms than enhances the chance of adsorption on the aluminium substrate. Furthermore the copper rich IMP also catalyses cerium salts precipitation on the cathodic sites.

## 4. Conclusions

PDP and EIS has shown that the combination of  $\text{Ce}^{4+}$  and melamine can offer a synergistic effect for the corrosion prevention of AA2024 in aerated 3.5% NaCl solution. PDP also



indicates that this combination acts as a cathodic inhibitor and EIS results confirm the PDP data. The SEM results along with optical observation indicate that melamine and  $\text{Ce}^{4+}$ , individually, cannot offer suitable corrosion prevention for AA2024 in this NaCl electrolyte. For the 1 : 1 melamine:  $\text{Ce}^{4+}$  sample, the EDX mapping showed that cerium compounds were precipitated at the cathodic IMP sites on the metal surface leading to an inhibition of the oxygen reduction reaction. The XPS revealed that  $\text{Ce}^{4+}$  was reduced to  $\text{Ce}^{3+}$  in the presence of melamine, this step is considered crucial in the proposed protection mechanism.

## Conflicts of interest

There are no conflicts to declare.

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