

## MINI REVIEW

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Cite this: *Catal. Sci. Technol.*, 2020, 10, 5740

## Enzyme production of D-gluconic acid and glucose oxidase: successful tales of cascade reactions

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This review mainly focuses on the use of glucose oxidase in the production of D-gluconic acid, which is a reactant of undoubtable interest in different industrial areas. The enzyme has been used in numerous instances as a model reaction to study the problems of oxygen supply in bioreactors. One of the main topics in this review is the problem of the generated side product, hydrogen peroxide, as it is an enzyme-inactivating reagent. Different ways to remove hydrogen peroxide have been used, such as metal catalysts and use of whole cells; however, the preferred method is the coupling glucose oxidase with catalase. The different possibilities of combining these enzymes have been discussed (use of free enzymes, independently immobilized enzymes or co-immobilized enzymes). Curiously, some studies propose the addition of hydrogen peroxide to this co-immobilized enzyme system to produce oxygen *in situ*. Other cascade reactions directed toward the production of gluconic acid from polymeric substrates will be presented; these will mainly involve the transformation of polysaccharides (amylases, cellulases, etc.) but will not be limited to those (e.g., gluconolactonase). In fact, glucose oxidase is perhaps one of most successful enzymes, and it is involved in a wide range of cascade reactions. Finally, other applications of the enzyme have been reviewed, always based on the production of D-gluconic acid, which produces a decrease in the pH, a decrease in the oxygen availability or the production of hydrogen peroxide; in many instances, cascade reactions are also utilized. Thus, this review presents many different cascade reactions and discusses the advantages/drawbacks of the use of co-immobilized enzymes.

Received 22nd April 2020,  
Accepted 14th July 2020

DOI: 10.1039/d0cy00819b

rsc.li/catalysis

## 1. D-Gluconic acid

### 1.1. Metabolic role

D-Gluconic acid, or (2R,3S,4R,5R)-2,3,4,5,6-penta-hydroxyhexanoic acid ( $C_6H_{12}O_7$ , also named dextronic acid), is the C1-oxidized form of D-glucose (or dextrose), where the aldehyde group has become oxidized to the corresponding carboxylic acid. It can also be obtained through the hydrolysis

of D-gluconolactone. The gluconate shunt, shown in Fig. 1, illustrates the production of D-gluconic acid from D-glucose and the subsequent steps in its degradation, leading to shorter molecules.<sup>1</sup> Metabolically, glucose, which is the main carbon source for most living organisms, after being phosphorylated to glucose 6-phosphate (G6P) in the first step of glycolysis, may follow two routes. It may either undergo glycolysis to provide energy as ATP (Embden–Meyerhof–Parnas pathway) or enter the pentose phosphate pathway (PPP) in order to furnish reducing equivalents (nicotinamide adenine dinucleotide phosphate [NADPH]) and pentose sugars. These compounds are precursors of nucleotide and serine/glycine/threonine biosynthesis.<sup>2</sup> The derivation of glucose between these two metabolic alternatives, glycolysis and PPP, depends on the environmental situation (the nutrient concentration and presence or absence of stressors).<sup>1,3</sup> In the gluconate shunt, glucose is oxidized by glucose dehydrogenase to furnish gluconate, the form in which D-gluconic acid is present at physiological pH. Subsequently, gluconate is phosphorylated by the action of gluconate kinase to produce 6-phosphogluconate, which is

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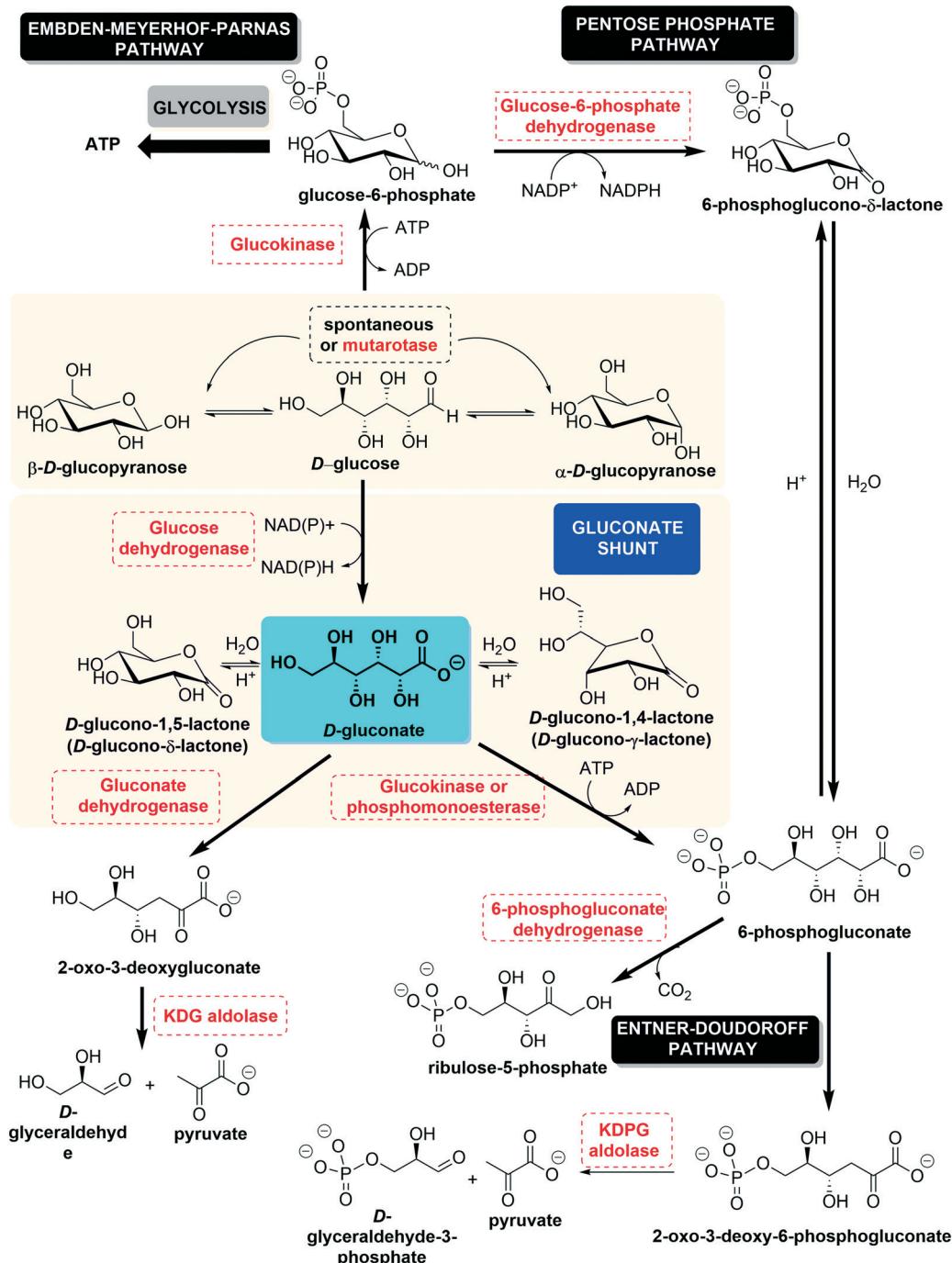


Fig. 1 The gluconate shunt.

the second intermediate of the pentose phosphate pathway (Fig. 1, *vide supra*). This gluconate shunt is mainly found in plants, algae, cyanobacteria and some bacteria, which all use the Entner-Doudoroff pathway (Fig. 1, *vide infra*) to degrade glucose or gluconate; this generates 2-keto-3-deoxygluconate-6-phosphate, which is then cleaved to generate pyruvate and glyceraldehyde 3-phosphate.<sup>4</sup> Glucose dehydrogenase and gluconate kinase activities are also present in mammals, fission yeast, and flies, none of which possess the key Entner-Doudoroff pathway enzymes.<sup>5</sup>

## 1.2. Chemical properties

D-Gluconic acid is widely present in nature, especially in plants, fruits, rice, dairy products, vinegar, meat, wine (up to 0.25%) and honey (1%).<sup>6</sup> Many fungi, yeasts and bacteria are able to produce D-gluconic acid.<sup>6,7</sup> Historically, Hlasiwetz and Habermann discovered D-gluconic acid during the oxidation of glucose with chlorine in 1870, and it was first isolated as its barium or calcium salt; the history of the discovery and production of D-gluconic acid is well illustrated in articles from Ramachandran *et al.*<sup>6,8</sup>

D-Gluconic acid is very soluble in water; the commercial 50% solution has a pH of 1.82 and a density of  $1.23 \text{ g} \times \text{cm}^{-3}$  at 20 °C. On the other hand, the acid is only faintly soluble in ethanol and almost insoluble in nonpolar organic solvents.<sup>9</sup> Free D-gluconic acid is difficult to prepare in crystalline form. The crystallization of the anhydrous substance (white and odorless crystalline powder, specific rotation  $[\alpha_D^{20}] - 6.7^\circ$ ,  $[\alpha_D^{25}] - 5.4^\circ$ )<sup>9</sup> is possible below 30 °C, and a monohydrate (mp *ca.* 85 °C) has been reported to crystallize at 0 °C to 3 °C.<sup>9,10</sup> By storing D-gluconic acid in a desiccant at room temperature or heating it above 50 °C, internal loss of water leads to the formation of lactones. This circumstance can be understood by looking at its chemical structure. D-Gluconic acid, being a poly-hydroxy acid, can undergo intramolecular cyclization to furnish either the D-glucono- $\delta$ -lactone ((3R,4S,5S,6R)-3,4,5-trihydroxy-6-(hydroxymethyl)tetrahydro-2H-pyran-2-one) or the D-glucono- $\gamma$ -lactone ((3R,4R,5R)-5-[(1R)-1,2-dihydroxyethyl]-3,4-dihydroxyoxolan-2-one) (Fig. 2). In aqueous media, an acid-catalyzed mechanism leads to an equilibrium where between 55% and 65% of the molecules exist as open D-gluconic acid because of its weak acidity ( $K_a = 1.99 \times 10^{-4}$  at 25 °C, reported  $pK_a$  from 3.62 to 3.7 at 25 °C).<sup>6,9,11</sup> This conformational equilibrium (first order with respect to  $[\text{H}^+]$ )<sup>9</sup> is reached very slowly, as the  $\gamma$ -lactone is produced around one hundred times more slowly than the  $\delta$ -lactone.<sup>9,11</sup>

Both lactones can be isolated in the solid state.  $\delta$ -Lactone is a white, crystalline substance with a weakly sweet taste (melting point of 153 °C,  $[\alpha_D^{20}] + 66.2^\circ$ ),<sup>9</sup> while  $\gamma$ -lactone crystallizes as fine needles (melting point 134 °C to 136 °C,  $[\alpha_D^{20}] + 67.8^\circ$  °C).<sup>9</sup> Because of the acid-catalyzed equilibrium, both the pH and the specific rotation of a lactone solution (up to 90 g of  $\alpha$ -lactone can be dissolved in water at 20 °C, reaching 205 g at 50 °C, while only small amounts dissolve in organic solvents)<sup>9</sup> decrease as hydrolysis proceeds.

By increasing the pH of the medium, upon addition of a base, the closed lactamic structures are quickly hydrolyzed<sup>9</sup>

to furnish gluconate, an anion which can effortlessly bind to di- or trivalent metallic cations to form very stable chemical salts<sup>11</sup> (Fig. 3). Both the lactones and the calcium salts can be oxidized by reagents such as nitric acid or hydrogen peroxide under mild reaction conditions to furnish a mixture of 2- and 5-oxo (keto)-D-gluconate (2-KGA and 5-KGA). The former is the major product of anodic oxidations, treatment with sodium chlorate or biological fermentation. It is also possible to obtain 2,5-dioxo(keto)-D-gluconate (2,5-DKGA) at different percentages.<sup>9</sup> Under extreme conditions (concentrated nitric acid or dinitrogen tetroxide), glucaric acid is produced.

### 1.3. Production

D-Gluconic acid and its derivatives are being increasingly used in different industries; their current production is estimated to be around  $10^5$  tons per year.<sup>7,11</sup> The production costs vary from 1.20 US\$ per kg for D-gluconic acid up to 8.50 US\$ per kg for calcium gluconate and glucono- $\delta$ -lactone. The most broadly marketed derivative is sodium gluconate (more than 80% of the world's gluconic acid production).<sup>11</sup> Most of the commercial methods for producing D-gluconic acid and its derivatives are based on the oxidation (chemical, electrolytical, catalytical or biochemical) of glucose or glucose-containing raw materials.<sup>6,7,11</sup> Purely chemical oxidations (mainly using transition metals such as Pd, Pt or Au supported on titania, alumina or activated carbon)<sup>11</sup> have the drawback of limited specificity and selectivity even when applying controlled and optimized reaction conditions; this leads to insufficient yields and the presence of several by-products. Thus, fermentation is the preponderant technique for the synthesis of D-gluconic acid. Many filamentous fungi and bacteria have been applied to obtain this product;<sup>6,11</sup> currently, the key organisms employed are the fungi *Aspergillus niger* and the bacteria *Gluconobacter oxydans*. Current industrial processes are based on the original work of

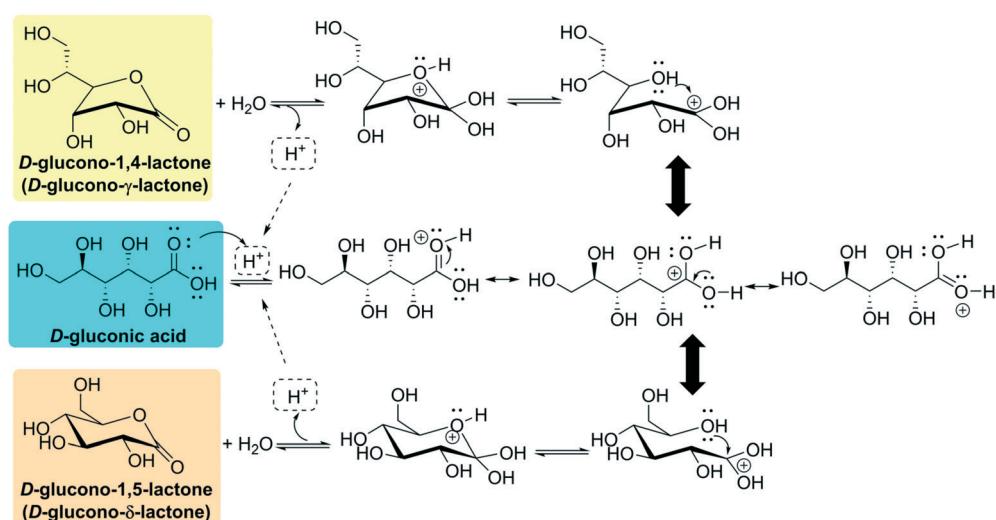


Fig. 2 Acid-catalyzed cyclization of D-gluconic acid to D-glucono- $\delta$ -lactone or D-glucono- $\gamma$ -lactone.



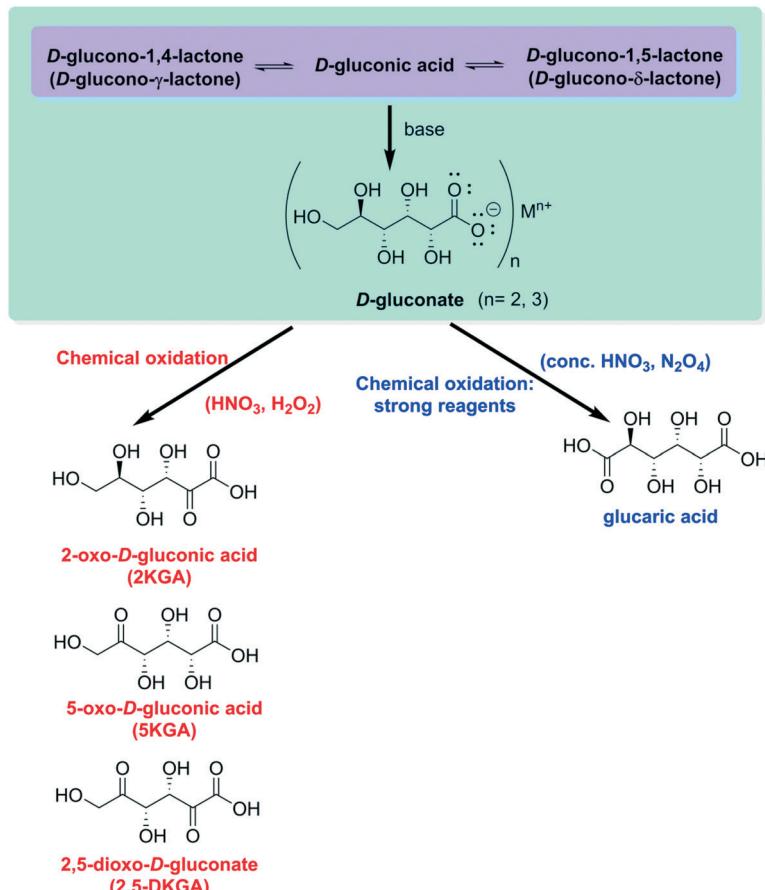


Fig. 3 Formation of D-gluconate and oxidation products.

Blom *et al.* in 1952 (ref. 12) with some modifications introduced by Ziffer *et al.* in 1971,<sup>13</sup> employing *A. niger* in a fed-batch process with periodical glucose feedings at 34 °C and using sodium hydroxide to maintain the fermentation pH value between 6.0 and 6.5. Using this procedure, glucose is converted to gluconic acid at a rate of 15 g L<sup>-1</sup> h<sup>-1</sup>. Some other important patents related to D-gluconic acid production are summarized elsewhere.<sup>6</sup>

#### 1.4. Uses

D-Gluconic acid, as a weak acid, can be used to dissolve combinations of polyvalent cations (oxides, hydroxides or carbonates) without attacking metallic or non-metallic surfaces, forming water-soluble complexes with the cations.<sup>9</sup> Therefore, D-gluconic acid is extremely useful for removing calcareous and rust layers from copper, aluminum and other metal surfaces. These include beer and milk flakes on galvanized iron, oxide coatings from metal alloys or stainless steel, and the safe removal of paint and varnish without damaging the underlying surfaces.<sup>9</sup> Conversely, sodium gluconate is present in many commercial cleansers due to its high stability to hydrolysis under extreme conditions (high temperature and pH values) as well as its sequestering properties for hardening agents in water. Although preferred

for metal components, gluconate solutions are used in some food processing plants as cleaning agents, mainly for glassware, as it helps prevent scale formation.<sup>6</sup> For example, the dairy industry uses solutions of D-gluconic acid derivatives to prevent the precipitation of calcium salts in their equipment and glass storage containers.<sup>11</sup> Alkaline sodium gluconate solutions, when applied at 95 °C to 100 °C, are excellent agents for the effective removal of paint and varnish without affecting underlying surfaces. Gluconate has also been applied for the pretreatment of certain surfaces in metallurgy, replacing the highly toxic cyanide ion. Finally, the bakery industry uses δ-gluconolactone to diminish the absorption of fatty compounds.<sup>8</sup>

D-Gluconic acid combined with magnesium salts is used in the textile industry as a stabilizer for peroxide bleach baths, while gluconate (sometimes mixed with polyphosphates) is employed for finishing natural cellulose fibers and desizing polyester or polyamide fabrics. Mixtures of gelatin and sodium gluconate are employed as sizing agents in the paper industry in order to obtain products displaying increased acid resistance.<sup>9</sup>

Sodium gluconate (0.02–0.2 wt%) is used as a highly effective agent for retarding the curing process of concrete. In fact, using this additive, a very homogeneous concrete is obtained, displaying high resistance to water, frost and cracking as well as

better stability upon setting. Additionally, sodium gluconate improves the flow properties of wet concrete mixtures.<sup>8,9</sup>

However, the main applications of D-gluconic acid (E574) and its derivatives are as additives in the food industry. In 1986,  $\delta$ -gluconolactone (E575) and sodium gluconate (E576) were granted GRAS (generally recognized as safe) status by the US FDA (Food and Drug Administration), authorizing their unlimited use as food ingredients. On the other hand, the United Nations agencies Food and Agriculture Organization (FAO) and World Health Organization (WHO) have also regulated the use of these food additives, including E577 (potassium gluconate), E578 (calcium gluconate), E579 (ferrous gluconate) and E580 (magnesium gluconate). For a detailed description of these additives, please see the review from Cañete-Rodríguez *et al.*<sup>11</sup> Low concentrations of D-gluconic acid, ranging from 0.02% to 0.1%, promote sucrose inversion without triggering the resulting fructose to undergo any further reaction. Usually, trace elements are administered as gluconate salts because of their rapid absorption and broad tolerance. D-Gluconic acid improves the organoleptic properties of food products, conferring a fresh and less bitter taste. In fruit juices, it prevents clouding by binding some metals (calcium or iron, mainly) present at trace levels.<sup>11</sup> These additives are extensively used in meat, dairy products and baked goods and as an ingredient of leavening agents for pre-leavened products. In sherbets, D-gluconic acid is used as a flavoring agent, while it can also be employed to reduce fat absorption in doughnuts or cones. Furthermore,  $\delta$ -gluconolactone is present in tofu, yogurt, cottage cheese, bread, meat, confectionery and pickling foods.<sup>6</sup> The lactone is generally preferred in cases where acidic conditions are required over a long period of time. Recently, the effects of D-gluconic acid and its derivatives as prebiotics, as well as their anti-oxidant properties, have been investigated, with promising results.<sup>11</sup> Finally, it must be remarked that the pharmaceutical industry uses gluconate salts ( $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{Fe}^{2+}$ ) as supplements to treat hypocalcaemia, hypomagnesaemia and anemia, respectively.

## 2. Glucose oxidase: sources and mechanism of action

### 2.1. Mechanism of action

Glucose oxidase catalyzes the oxidation of  $\beta$ -D-glucose to D-glucono- $\delta$ -lactone producing hydrogen peroxide ( $\text{H}_2\text{O}_2$ ) as a

by-product, with molecular oxygen acting as an electron acceptor. The first product is non-enzymatically hydrolyzed to D-gluconic acid (Fig. 4).<sup>14,15</sup>

Glucose oxidase is highly specific for the  $\beta$ -anomer of D-glucopyranose (the best substrate), while the  $\alpha$ -anomer is a very poor substrate (0.64% activity relative to  $\beta$ -D-glucose). Xylose and idose are very poor substrates (0.03% and 0.02% activities relative to  $\beta$ -D-glucose).<sup>14</sup> In general, glucose oxidase exhibits at least a 20-fold higher affinity and a 5-fold higher turnover rate for  $\beta$ -D-glucopyranose than for any other monosaccharides. In the cases of D-mannose, D-galactose, and D-xylose, the specificity constants are 400, 1000, and 3000-fold lower than that of  $\beta$ -D-glucopyranose. The product of  $\beta$ -D-glucopyranose oxidation, D-glucono- $\delta$ -lactone, has very weak enzyme inhibitory effects.<sup>16</sup>

The catalytic action of glucose oxidase is dependent on the FAD cofactor, which acts as an initial electron acceptor (as a hydride) and undergoes reduction to  $\text{FADH}^-$ . Then,  $\text{FADH}^-$  is oxidized, transferring electrons (as a hydride) to molecular oxygen, which is reduced to hydrogen peroxide.<sup>14,16-18</sup> The steady-state kinetics of the oxidation of  $\beta$ -D-glucopyranose by molecular oxygen obeys a ping pong bi-bi kinetic mechanism.<sup>14</sup> For the reductive half-reaction,  $\beta$ -D-glucopyranose is oxidized to D-glucono- $\delta$ -lactone by transferring a proton from its C1-hydroxyl to a basic group on the enzyme (His516), and a direct hydride transfer occurs from its C1 position to the N5 position of the isoalloxazine ring of FAD.<sup>14</sup> The oxidative half-reaction proceeds *via* one- or two-electron transfer mechanisms, depending on the type of the oxidizing substrate (oxygen, benzoquinones, naphthoquinones, ferrocene salts, organic metal complexes, *etc.*). In the case of oxygen, firstly, it diffuses into the active site very quickly (the diffusion of  $\text{O}_2$  to the active site is thermodynamically facilitated) and the reduced coenzyme ( $\text{FADH}^-$ ) is re-oxidized back to FAD by oxygen, which is reduced to hydrogen peroxide. This reaction proceeds *via* two single-electron transfer steps; a superoxide anion and a flavin semiquinone radical are the intermediates of the reaction.<sup>14</sup>

### 2.2. Glucose oxidase features and production

Glucose oxidase ( $\beta$ -D-glucose: oxygen 1-oxidoreductase; GOx, EC 1.1.3.4) is an oxidase with several large-scale technological applications, among them D-gluconic acid production.<sup>19-28</sup>

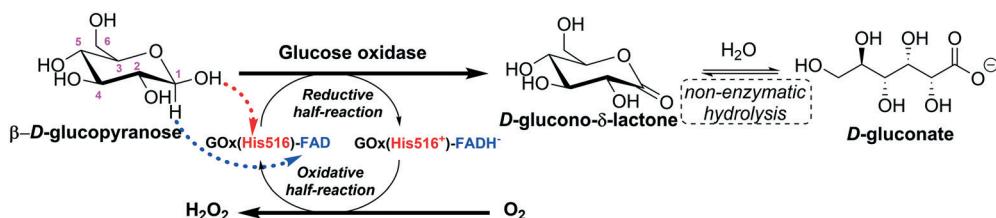


Fig. 4 Representation of the action mechanism of glucose oxidase in the oxidation of glucose to D-glucono- $\delta$ -lactone (adapted from Leskovac *et al.*<sup>14</sup> and Bankar *et al.*<sup>15</sup>).



A large number of microorganisms produce glucose oxidase, including plants, (red algae, citrus fruits), animals (e.g., insects), bacteria, and fungi. The main purpose of glucose oxidase in these sources is to generate hydrogen peroxide (a coproduct of the enzyme catalytic action), which acts as an anti-bacterial and anti-fungal agent.<sup>19,29–31</sup> For example, glucose oxidase is found in honey, and the anti-bacterial activity is strongly dependent on the accumulation of hydrogen peroxide in the product.<sup>30,32</sup>

For commercial applications, glucose oxidase has been produced and purified from fungi, especially from *Aspergillus* and *Penicillium* species.<sup>19,33–45</sup> The great success of these two species is mainly due to their metabolic versatility and their recognition as GRAS (generally recognized as safe).<sup>19,38</sup> Among the *Aspergillus* species, remarkable attention has been given to *A. niger* over the last 60 years.<sup>46–65</sup> Despite the great success of glucose oxidase production from *Aspergillus* and *Penicillium* species, efforts to find other glucose oxidase sources are being developed, including other glucose oxidase-producing fungi, e.g., *Cladosporium neopsychrotolerans*<sup>66</sup> and *Mucor circinelloides*,<sup>67</sup> other *Aspergillus* species, e.g., *A. tubingensis*,<sup>29</sup> *A. terreus*,<sup>68</sup> *A. oryzae*,<sup>69</sup> *A. carbonarius*,<sup>70</sup> and *A. nidulans*,<sup>71</sup> and some glucose oxidase-producing bacteria.<sup>72</sup>

The demand for glucose oxidase is increasing due to its growing applications in different industrial sectors. However, wild-type fungal strains producing glucose oxidase usually have low fermentation capacity, complicated purification processes and low enzyme efficiency. Additionally, impurities in glucose oxidase, including other enzymes (e.g., catalase, cellulase, and amylase), prevent its use in some applications<sup>15,19</sup> and require full enzyme purification. In this way, genetic and non-genetic engineering tools have been applied to increase the productivity of glucose oxidase. Genetic engineering has stood out since 1990 as a tool to build excellent glucose oxidase expression systems; it permits the development of strains with high enzyme production.<sup>19,66,73–80</sup> In addition, strategies of formulating the fermentation medium<sup>73,81</sup> and computational tools<sup>82</sup> have proven to be powerful tools to increase glucose oxidase productivity. As an example, Bankefa *et al.*<sup>73</sup> reported a strategy of co-feeding complex carbon sources (e.g., yeast extract) with methanol, combining a secretory pathway engineering in a *Pichia pastoris* strain containing the gene encoding glucose oxidase from *A. niger*. Using this strategy, the volumetric extracellular activity of glucose oxidase in a 1 L fermenter was enhanced by around 3-fold compared to that reached when utilizing a recombinant *P. pastoris* strain containing only the gene encoding glucose oxidase. In another communication, Darvishi *et al.*<sup>82</sup> reported the use of software to *in silico* analyze endogenous and exogenous signal peptides to secrete recombinant glucose oxidase in non-conventional *Yarrowia lipolytica* for further *in vivo* analysis. The recombinant *Y. lipolytica* strain produced up to 280 and 145 U L<sup>-1</sup> of extracellular and intracellular glucose oxidase, respectively, from *A. niger* after 7 days in YPD medium. In other approaches, mutagenesis of *A. niger*

by UV irradiation<sup>47</sup> and chemical mutagens<sup>83</sup> generated mutated strains that produced around two-fold and three-fold more glucose oxidase than their parental wild strains, respectively.

The structures of glucose oxidase from *A. niger* and *P. amagasakiense* are well-established. They were refined at 1.9 and 1.8 Å resolution, respectively.<sup>16</sup> Both glucose oxidases are homodimers with 581 and 587 amino acid residues per monomer, respectively, one flavin adenine dinucleotide (FAD) per monomer non-covalently bound to the active site, and eight and seven potential *N*-glycosylation sites, respectively. The residues Asn89, Asn161, Asn355 and Asn388 are sites for attachment of *N*-acetylglucosamine moieties. The Asn89 site contains an extended carbohydrate structure consisting of a second *N*-acetylglucosamine and three mannose molecules. This carbohydrate moiety forms a bridge between the two molecules of the protein dimer. Salt bridges and hydrogen bonds further stabilize the protein dimers.<sup>16</sup>

In addition to FAD coenzyme, glucose oxidase enzymes from *A. niger* and *P. amagasakiense* have two histidines in the active site, His516 (pK<sub>a</sub> 6.9) and His559 (pK<sub>a</sub> > 8.0), which act as general bases and acids in the reductive and oxidative half-reactions of the oxidation of β-D-glucose to D-gluconic acid, as discussed above. His559 is strongly bound to Glu412 (pK<sub>a</sub> 3.4) by a hydrogen bond and to one water molecule in front of the flavin ring. These three residues of amino acids are essential for the catalysis; the protonation of these residues strongly influences the kinetic constants.<sup>14,16,19,84</sup> Glycosylated glucose oxidases from *A. niger* and *P. amagasakiense* have a molecular mass of 150–160 kDa for the dimer, which is composed of two subunits of equal molecular mass. Both glucose oxidases are 10–16 wt% glycosylated with high-mannose type carbohydrates.<sup>14,16,18,75,84–87</sup>

Bankefa *et al.*<sup>73</sup> reported that the SDS-PAGE analyses of glucose oxidase from *A. niger* extracellularly expressed by a recombinant *P. pastoris* strain showed a protein band of approximately 80 kDa, while its theoretical size was 63.5 kDa. This higher molecular mass of the enzyme subunit was attributed to enzyme glycosylation (around 21 wt%). Kalisz *et al.*<sup>84</sup> reported that glycosylated and deglycosylated glucose oxidase from *P. amagasakiense* have molecular masses of 167 and 133 kDa (by PAGE analysis) for the dimer and 77 and 67 kDa for the monomers, respectively. On the basis of gas chromatography and SDS-PAGE analyses, for the glycosylated glucose oxidase, 13 wt% of the enzyme carbohydrates are high-mannose type.<sup>84</sup>

In general, fungal glucose oxidases have an isoelectric point in the range of pH 4.0–5.0,<sup>16</sup> optimal activity in the pH range from 4.0 to 7.0,<sup>14,15,29,31,33,40,75,84</sup> and optimal temperature in the range of 40–60 °C.<sup>15,29,33,40,75,84</sup> Glucose oxidase from *A. niger* does not require metal ions to express its activity; however, it is inhibited by Ag<sup>+</sup>, Hg<sup>2+</sup>, Cu<sup>2+</sup>, Mg<sup>2+</sup> and Ca<sup>2+</sup>.<sup>19</sup> Very importantly in the context of this review, hydrogen peroxide is a strong deactivating agent of glucose oxidase.<sup>15,88</sup>



### 3. Glucose oxidase immobilization

Enzymes are potentially useful industrial biocatalysts because they operate under mild conditions with high activity, selectivity and specificity.<sup>89–93</sup> However, due to their biological origin, they have some features that are far from ideal for industrial requirements.<sup>94</sup> Current developments in all areas related to enzyme biocatalyst design (*e.g.*, metagenomics,<sup>95–98</sup> directed evolution,<sup>99–101</sup> chemical modification,<sup>102</sup> and immobilization<sup>103–108</sup>) can solve these problems. For example, several new strategies have been published, such as the design of plurizymes (enzymes bearing a natural and an artificially designed active center), the design of irreversible inhibitors directed to one of these active center bearing a metal catalytic center and the use of modified plurizymes (bearing a free active center while the other active center presented the inhibitor with a metal catalysts) in a cascade reaction.<sup>109</sup>

Immobilization was the initial answer to the problem of enzyme solubility, which complicates the reuse of enzymes.<sup>106,110,111</sup> Currently, with the decreasing price of enzymes, enzyme immobilization should address many other enzyme limitations, such as improving activity, stability, selectivity and specificity, decreasing inhibition<sup>104</sup> or purifying the enzyme.<sup>103</sup> This will increase the interest in immobilization and will enlarge the window of conditions in which the biocatalyst can be utilized.<sup>112,113</sup> In this way, immobilization is not merely a tool to recover enzymes, but may also be a very powerful means to greatly improve enzyme performance.<sup>110</sup>

Immobilization may be also considered when using glucose oxidase. Although the enzyme is quite stable, the possibility of using it for longer times and many cycles may be very important for its industrial implementation. Therefore, proper glucose oxidase immobilization may be critical for the successful design of an industrial biocatalyst.<sup>110</sup>

Almost 1000 citations can be found using the keywords “glucose oxidase immob\*” when searching the publication titles in Scopus (see Fig. 5). Obviously, a comprehensive assessment of this topic is beyond the objective of this review. Glucose oxidase used in biosensors has also been

extensively reviewed;<sup>114–117</sup> therefore, this topic will not be included in this new review.

Therefore, we have included only some of the more relevant immobilization papers, mainly those that offer new strategies or unexpected results. For example, a comparison between different supports to immobilize glucose oxidase has been reported and offered some unexpected results.<sup>118</sup> Glucose oxidase was immobilized on glyoxyl agarose, epoxy Sepabeads and glutaraldehyde-activated supports. Although in general, glyoxyl agarose supports provide higher stabilization of enzymes, in this instance, the highest stabilization was achieved using supports pre-activated with glutaraldehyde. The stability could be further improved if the enzyme was first ionically adsorbed on an aminated support and then treated with glutaraldehyde. This new biocatalyst was also more stable in the presence of ethanol or hydrogen peroxide.<sup>118</sup>

Glucose oxidase has been used as an example enzyme to develop multilayer biocatalysts. For example, layers of glucose oxidase immobilized on films of chitosan have been built for use in biosensors.<sup>119</sup> This biocatalyst design was also used in the reduction of a gold salt to yield metallic gold nanoparticles.<sup>119</sup> In another paper, nylon-based microfiltration membranes or hydrophobic polyvinylidene fluoride were used to build multilayers using *in situ* polymerization of acrylic acid to obtain a polyanion.<sup>120</sup> An enzyme-based microcantilever sensor obtained by using layer-by-layer deposition of glucose oxidase was utilized in the design of a biosensor.<sup>121</sup>

#### 3.1. Design of glucose-sensitive supports using immobilized glucose oxidase

This application of immobilized glucose oxidase is far from being applied in the production of *D*-gluconic acid, but it is interesting enough to comment on at least briefly. It has been known for a long time that some membranes have been identified as sensitive to changes in media. Some researchers have attempted to exploit these membrane features using glucose oxidase to change the medium conditions (usually decreasing the pH) in the presence of high concentrations of glucose, mainly to release insulin.<sup>122–125</sup> For example, to achieve this goal, glucose oxidase has been immobilized on amine-containing polymers. When *D*-gluconic acid is produced by the action of glucose oxidase, it decreases the pH in the membrane, which then swells. This permits the release of drugs into the medium.<sup>125</sup> A membrane was produced using poly(acrylic acid)-grafted porous cellulose film and glucose oxidase was immobilized on it to build an insulin delivery system that responds to glucose concentration levels.<sup>126</sup> The system was based on conformational changes of the graft chains induced by changes in the medium pH as a consequence of changes in the ionic interactions in the matrix; the production of *D*-gluconic acid produced a decrease in the pH value, which led to a decrease in the

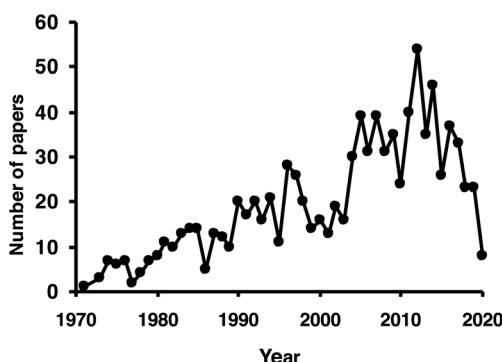


Fig. 5 Number of papers per year including the term glucose oxidase and immob\* in their titles. Source: Scopus (accessed 4/22/2020).



electrostatic repulsion between the poly(acrylic acid) side chains. This transformed the graft chains into coil-like forms and opened the pores of the membrane, enabling the release of the drug.<sup>126</sup>

Glucose-sensitive hydrogels can be used in a similar fashion; in some cases, they co-immobilize the enzyme with catalase to prevent hydrogen peroxide accumulation.<sup>127</sup> In one interesting paper,  $\beta$ -cyclodextrin was grafted on a polyethyleneimine hydrogel (a gel that also swells at low pH values) and used to immobilize glucose oxidase.<sup>128</sup> Other hydrogels have been described.<sup>129</sup> To reinforce the immobilization, the enzyme was modified with 5 palmitic acid-*N*-hydroxysuccinimide ester molecules per mole of enzyme; therefore, the release of fluorescein isothiocyanate dextran from the support could increase as the concentration of glucose increased.<sup>128</sup> Also, glucose-sensitive mesoporous silica nanoparticles have been designed for this goal.<sup>130,131</sup> This includes an expanded-pore silica matrix coated with 1-propyl-1-*H*-benzimidazole groups and bearing insulin labeled with fluorescein isothiocyanate. Cyclodextrin-modified glucose oxidase is immobilized by interaction with the benzimidazole groups. When glucose is transformed into  $D$ -gluconic acid, de-threading of the benzimidazole-cyclodextrin-glucose oxidase complexes is induced, permitting cargo release.<sup>131</sup> Multilayers of enzymes in this type of support have also been utilized for this goal.<sup>132</sup> Nanogels and microgels,<sup>133,134</sup> dextran nanoparticles,<sup>135</sup> and metal organic framework nanoparticles<sup>136</sup> have been also utilized for this purpose.

Co-immobilized enzymes have also been studied. The change of the membrane phase was studied in an interesting paper where two enzymes were coupled in a cascade reaction to accelerate the rate. Thus, gluconolactonase (an enzyme that hydrolyzes  $D$ -glucono-1,5-lactone) was co-immobilized with glucose oxidase.<sup>137</sup> They studied the shrinking kinetics of the polyelectrolyte gels in the form of a cylinder composed of a copolymer of *N*-isopropylacrylamide and acrylic acid with low crosslinking. Using the co-immobilized glucose oxidase and gluconolactonase, the gel swelled rapidly, and the process was not governed by the reaction rate. Using only glucose oxidase, very slow shrinking was observed, and it was found that the rate was determined by the enzyme reaction. The more rapid shrinking using the co-immobilized enzyme was attributed to the rapid  $D$ -glucono- $\delta$ -lactone hydrolysis catalyzed by gluconolactonase after its production by glucose oxidase.<sup>137</sup>

## 4. The hydrogen peroxide challenge

As stated in point 2, hydrogen peroxide is the by-product of the reaction of glucose oxidase, and this by-product possesses some potential uses and dangers.<sup>138</sup> Hydrogen peroxide is a simple and relatively mild oxidizing reagent; 47% of its weight is an oxidant, and it produces oxygen and water as its only by-products.<sup>139-141</sup> Due to its electrochemical potential,

hydrogen peroxide is suitable to be quantified in many of the applications of glucose oxidase in the biosensor area. Moreover, in some instances, glucose oxidase and glucose are utilized for the *in situ* production of this oxidant reagent as part of a cascade reaction involving other enzymes that use the *in situ* released hydrogen peroxide as a substrate (e.g., peroxidase, lipases).<sup>142,143</sup>

However, the current review is mainly focused on  $D$ -gluconic acid production. In this reaction, hydrogen peroxide will be produced in an equimolecular ratio with  $D$ -gluconic acid; under industrially relevant concentrations of glucose, the enzyme will be exposed to moderate-to-high concentrations of hydrogen peroxide (e.g., over 100 mM). At these concentrations, hydrogen peroxide is a very efficient inactivating agent for enzymes, including glucose oxidase.<sup>118,144</sup> The oxidation of proteins by hydrogen peroxide causes the conversion of some amino acid residues into carbonyl derivatives; chlorination, nitration or hydroxylation of aromatic amino acid moieties; hydroxylation of aliphatic groups; chlorination of primary amino groups; nitrosylation of sulphydryl groups; sulfoxidation of methionine residues; etc.<sup>145-164</sup> In this way, hydrogen peroxide is able to modify many of the amino acids of a protein (Arg, Cys, His, Lys, Met, Pro, Tyr, etc.).<sup>165-180</sup> It can also promote the cleavage of some peptide bonds by either the diamide or  $\alpha$ -amidation pathways; moreover, it can produce inter- or intramolecular protein crosslinks *via* different mechanisms.<sup>181-189</sup> For a proper review of this topic, the reader can consult Stadtman and Levine's paper.<sup>144</sup>

In the case of  $D$ -gluconic acid production, the concentration of hydrogen peroxide must be reduced to prevent glucose oxidase inactivation, although in some cases this is not considered (see section 5). There are many possible routes to achieve this goal, e.g., destruction of hydrogen peroxide using metal catalysts (see section 6), use of whole cells as catalysts with their full metabolic machinery (section 7), and the use of catalase (section 8).

## 5. Oxidation of glucose catalyzed by glucose oxidase to produce $D$ -gluconic acid

Although hydrogen peroxide is deleterious to the stability of glucose oxidase,<sup>138</sup> there are some examples in the literature in which the reaction is studied in the absence of catalase or using another strategy to eliminate this dangerous compound. Usually, authors use the reaction to evaluate reactor configurations or mass transfer problems more than pursuing the production of  $D$ -gluconic acid as a real objective.

For example, in well-established research, glucose oxidase was used to simulate the oxygen transfer rate in fermentation broths.<sup>190</sup> If there is enough lactonase activity in the fungus, the  $D$ -gluconic acid production rate is proportional to the oxygen uptake rate. Glucose oxidase was immobilized on a



carbon felt electrode with a catalytic current of 0.4 A and used to catalyze the oxidation of glucose employing benzoquinone to regenerate the electron acceptor.<sup>191</sup> The coupling between electrochemical and enzymatic reactions was very efficient because of the proximity of the two reaction sites. Most importantly, by using benzoquinone instead of oxygen, the operational stability of the biocatalyst was increased 50 fold.<sup>191</sup>

D-Gluconic acid was also produced using glucose oxidase immobilized on a low-density polyethylene membrane grafted with 4-vinylpyridine (an anion-exchange membrane), affording relatively low yields.<sup>27</sup> The immobilization of the enzyme on a membrane adjacent to the anion exchange membrane led to the selective removal of D-gluconic acid from the reaction medium and reduced enzyme inhibition by D-gluconic acid. The amount of D-gluconic acid increased 30 fold compared to the enzyme directly bound to the anion-exchange membrane. However, the concentration of glucose in this study was 1 g L<sup>-1</sup>, a very low concentration; this was very likely necessary because of the enzyme inactivation caused by accumulated hydrogen peroxide when using higher glucose concentrations.<sup>27</sup> Another paper compared a Millipore stirred ultrafiltration cell with a Bioengineering Enzyme Membrane Reactor in the production of D-gluconic acid catalyzed by glucose oxidase.<sup>192</sup> The maximum concentration of glucose was only 5.0 mM (also too low for practical applications), with a highest oxidation yield of 75% using 2.5 mM glucose. In other research, a falling-film micro-reactor was utilized in enzymatic glucose oxidation using free glucose oxidase.<sup>193</sup> It was determined that the volumetric mass-transfer oxygen coefficient was the most critical parameter, and it was evaluated by employing the combined online determination of dissolved oxygen in all systems. The use of this bubble-free reactor afforded a 50% oxidation yield, while a conventional bubble column yielded only 27%.<sup>193</sup> In other research, the inner wall of fused-silica capillaries was modified with different generations of polyamidoamine dendrimers by microwave irradiation and used to generate a capillary glucose oxidase micro-reactor.<sup>194</sup> The oxidation efficiency increased with the number of dendrimer generations.

An ultra-scaled down membrane bioreactor based on a parameter scanning ultrafiltration device was utilized to optimize the production of D-gluconic acid using soluble glucose oxidase.<sup>195</sup> The addition of sodium chloride reduced the yields, perhaps by reducing the concentration of available oxygen. Curiously, this paper showed that the addition of catalase had a negative effect on glucose conversion, which is difficult to explain considering that catalase should increase oxygen availability and also reduce enzyme inactivation by hydrogen peroxide.<sup>195</sup> The catalase may have contained some contaminant enzyme that the authors could not identify.

However, in these studies using glucose oxidase, the industrial production of D-gluconic acid was not actually pursued.

## 6. Combinations of glucose oxidase to oxidize glucose and metal catalysts to eliminate hydrogen peroxide

Several metal catalysts very efficiently destroy hydrogen peroxide,<sup>196</sup> although the reaction is not fully selective and can affect the enzyme.<sup>197,198</sup> However, some examples of the combined use of glucose oxidase and metals can be found in the literature. For example, glucose oxidase was used as a model to compare the liquid–solid and the volumetric gas–liquid oxygen transfer coefficients using a normal bubble column, an internal loop airlift or an external loop airlift bubble column by the steady state method.<sup>199,200</sup> In this study, glucose oxidase was trapped in a calcium alginate matrix in combination with fine palladium particles. These palladium particles were used to destroy the hydrogen peroxide in this study, and the external loop airlift bubble column offered the best results.

## 7. Use of whole cell biocatalysts to produce D-gluconic acid from glucose

One solution to avoid the risks of glucose oxidase inactivation by hydrogen peroxide is the use of whole cells as biocatalysts, as the whole metabolic machinery may eliminate the produced hydrogen peroxide.<sup>201–204</sup> However, this approach has some problems, such as risk of substrate contamination and side-reactions. For example, *Aspergillus niger* cells presenting catalase and glucose oxidase activities were permeabilized by treatment with organic solvents.<sup>205</sup> Curiously, in this case, exogenous hydrogen peroxide was added to obtain oxygen after its destruction by catalase. The authors observed good stability of both enzymes in the cell. In other research, *Gluconobacter oxydans suboxydans* cells were described to accumulate D-gluconic acid in the medium in almost stoichiometric concentrations.<sup>206</sup> These cells were entrapped in diverse alginate gels. The activity increased when the concentration of alginate and the size of the particles decreased and when the aeration increased (suggesting a diffusion limitation problem). When increasing the number of cells, the authors reported that the transport of oxygen became a rate-limiting parameter.<sup>206</sup> *Aspergillus niger* containing glucose oxidase was utilized in the oxidation of glucose employing oxygen-enriched air from 30% to 100% saturation at 1 bar, and a three-fold increase in the enzyme activity was observed.<sup>207</sup> At the highest dissolved oxygen concentration, the activity of glucose oxidase increased more than three times, while the production rate of D-gluconic acid increased by a factor of two. It was found that the microorganism produced an endo- (main component) and an exo- (minority component) cellular glucose oxidase. Due to the oxygen transport limitations inside the mycelium, the activity of the endocellular glucose oxidase was reduced (reaching just 50–80%); however, it was still the main source



of glucose oxidase activity.<sup>207</sup> Later, the same research group compared the performance of *Gluconobacter* spp. and *Aspergillus niger* in D-gluconic acid production (using glucose oxidase and glucose dehydrogenase).<sup>208</sup> The reactor was an airlift reactor (9.25 m) to generate a deep, wide gradient in the dissolved oxygen. The authors reported that the local dissolved oxygen concentration affected neither product formation nor cell growth, independently from the microorganism studied. This was explained by the short residence time for the cultures to pass through the area where the lowest dissolved oxygen concentration existed due to the single circulation loop. *Aspergillus niger* production of glucose oxidase increased with the local dissolved oxygen concentration. The authors claimed that a periodic high dissolved oxygen concentration was sufficient to induce enzyme synthesis, and this was obtained in tower-shaped reactors.<sup>208</sup> Other researchers used *Penicillium variabile* P16, a strain presenting glucose oxidase and catalase activities, to study this reaction.<sup>209</sup> The cells were immobilized using different protocols, and the best results in long-term experiments were obtained using polyurethane sponge. However, the highest mean volumetric productivity of D-gluconic acid was achieved using agar as a cell immobilizing matrix. Later, the same research group used this biocatalyst in a fluidized-bed reactor.<sup>209</sup> Also, *Aspergillus terreus* was used to produce D-gluconic acid.<sup>210</sup> It rapidly metabolized glucose to D-gluconic acid at pH 6.5 (with 70% conversion of D-glucose to D-gluconic acid); however, after using all the D-glucose in the reaction medium, the produced D-gluconic acid was employed as a carbon source. Later, glucose oxidase and a mutant enzyme (doubling the activity of the native enzyme at pH 5.5) were expressed in *Aspergillus niger* as C-terminal fusions with the Aga2 protein from *Saccharomyces cerevisiae*.<sup>211</sup> This permitted expression of the

enzymes on the surface of the yeast cells and their use for the production of D-gluconic acid.

## 8. Use of catalases and glucose oxidase to produce D-gluconic acid: a pseudo-cascade reaction

Although metals can be used to destroy hydrogen peroxide, the most efficient way to reduce the hydrogen peroxide concentration in the glucose oxidase environment is the use of catalase in free, individually immobilized or co-immobilized (with glucose oxidase) forms (Fig. 6 and 7). The glucose–glucose oxidase–hydrogen peroxide–catalase system was studied *in vitro* in the field of “nonlinear chemical dynamics”.<sup>212</sup> These reactions produce a natural basis of fluctuations in biological systems, belonging to the family of oscillatory enzymatic reactions.<sup>213,214</sup> Catalases catalyze the decomposition of hydrogen peroxide in water and oxygen without risk of promoting some undesired side reactions. In fact, catalases produce oxygen that can be used again by glucose oxidase, even improving glucose oxidase activity.

A cascade reaction can be described as a reaction where the product of one enzyme is the substrate of another, and the final product is the target. The destruction of hydrogen peroxide to prevent glucose oxidase inactivation, even if it is not a real cascade reaction,<sup>212</sup> can be considered as one because hydrogen peroxide is produced by glucose oxidase (enzyme 1), which also produces the target product (D-gluconic acid), while catalase (enzyme 2) destroys the by-product of enzyme 1 to yield only water and oxygen. In these cases, the researchers mainly used co-immobilized enzymes. As will be discussed below, glucose oxidase can participate in many cascade reactions.

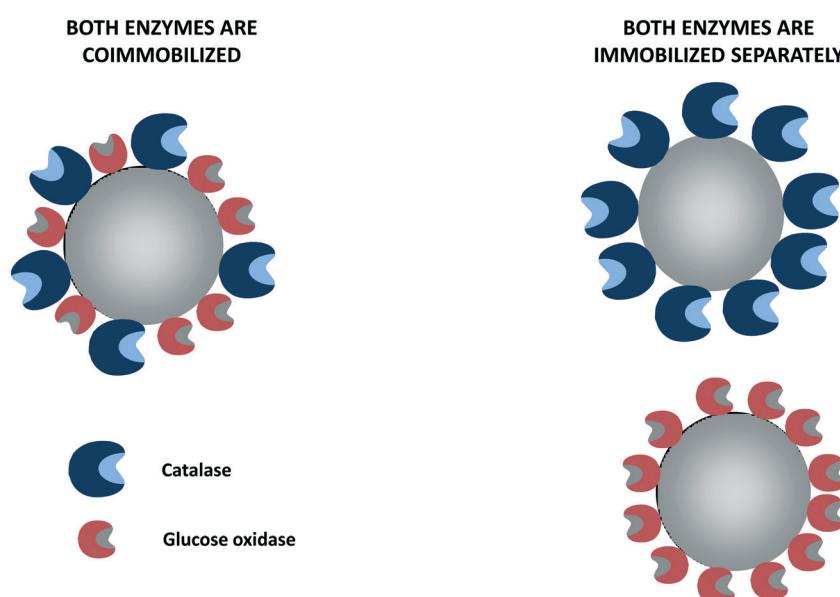


Fig. 6 Glucose oxidase and catalase co-immobilized or immobilized separately using non-porous supports.



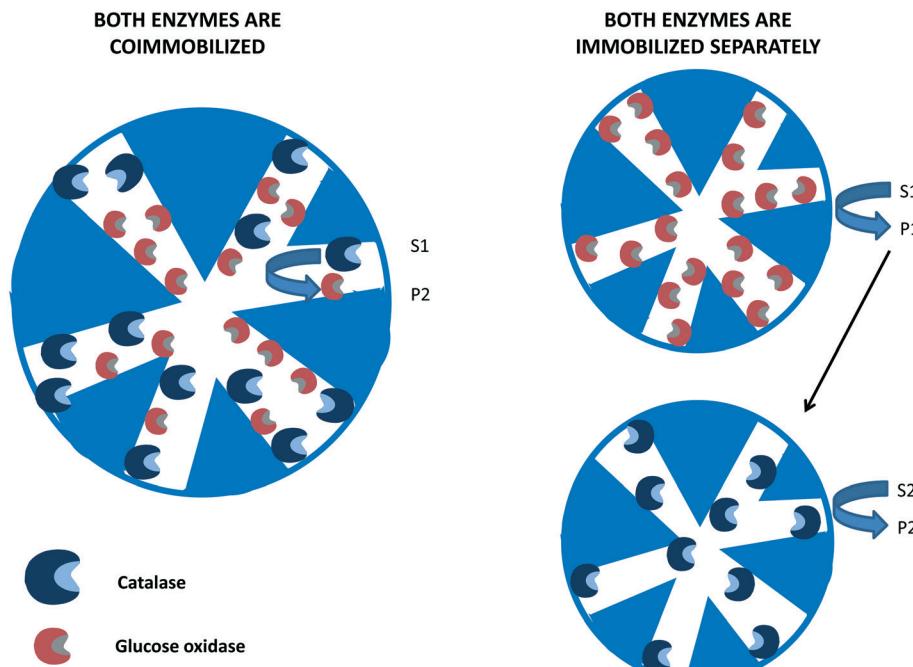


Fig. 7 Glucose oxidase and catalase co-immobilized or immobilized separately using porous supports.

### 8.1. Co-immobilized biocatalysts or individually immobilized enzymes?

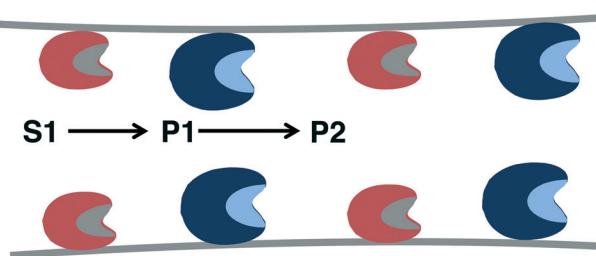
In many instances, if several enzymes are used in a cascade reaction, it is assumed that enzyme co-immobilization is the best alternative.<sup>215–221</sup> However, co-immobilization, that is, the immobilization of two or more enzymes on the same particle, has advantages but also has some serious drawbacks that in many instances are not taken into account.<sup>222</sup> Among the clearest advantages, we can note the shortening of the induction time for the second enzyme to act, which increases the initial rate of the global process<sup>105,106</sup> (Fig. 8). This may be a key point if the intermediate product/products are unstable and can be destroyed if they are not rapidly modified.<sup>223–232</sup>

Co-immobilization may be also necessary if cofactors and enzymes are immobilized in porous supports, as the enzyme will only have access to the cofactors located in the same porous particles.<sup>233–236</sup> On the negative side, it can be noted that in a co-immobilized biocatalyst, all enzymes should be immobilized using the same surface, and the stability of the least stable enzyme will determine the stability of the whole co-immobilized enzyme biocatalyst.<sup>106,237–239</sup> Therefore, enzyme co-immobilization should be performed only after a careful evaluation of the pros and cons of individual immobilization *versus* enzyme co-immobilization.<sup>222</sup>

### 8.2. Examples of D-gluconic acid production using catalase and glucose oxidase

**8.2.1. Use of soluble catalase and glucose oxidase in the production of D-gluconic acid.** As stated above, immobilization is a powerful tool to improve the features of

enzymes.<sup>103–108</sup> However, some papers describe the utilization of free catalase and glucose oxidase. In many instances, these are only model reactions to determine kinetic parameters, oxygen supply, *etc.*, as the industrial implementation of this process using free enzymes is quite unlikely due to issues with enzyme stability. Many examples show the use of membrane reactors.<sup>240–243</sup> This is not an actual immobilization system but can be included in a wide understanding of enzyme immobilization provided that the enzymes are physically located in a confined space; re-use of



P1 is rapidly modified because E2 has high concentrations of P1 available in a confined space from the start of the reaction.



Fig. 8 Reduction of time lapse in the destruction of hydrogen peroxide using catalase and glucose oxidase co-immobilized on porous supports.



the enzymes, if they are stable enough, is also possible using these reactors.

In a very old paper, a polarographic protocol to determine the activities of soluble catalase or catalase/glucose oxidase mixtures was designed based on the determination of hydrogen peroxide and oxygen.<sup>244</sup> Later, the kinetics of the oxidation of glucose catalyzed by glucose oxidase in the presence of a large excess of catalase was studied both experimentally and theoretically.<sup>245</sup> The mutarotation rate between the  $\alpha$  and  $\beta$  forms was considered in these studies. The kinetics were adjusted to the Michaelis-Menten equation for glucose and oxygen, correlating the observed oxygen concentration profiles with those supplied by the model.<sup>245</sup> In another paper, the authors utilized air-saturated solutions to study the kinetics of the oxygen consumption or the oxidation of glucose by glucose oxidase and the destruction of hydrogen peroxide to regenerate oxygen.<sup>246</sup> The oxygen concentrations were determined by monitoring the phosphorescence decay of a Pd-phosphor in solution.

To analyze the adsorption rate of oxygen in a batch stirred tank reactor, the oxidation of glucose was studied using different loads of catalase and glucose oxidase.<sup>247</sup> Pure oxygen was supplied to the D-glucose solution in the presence of active enzymes or using inactivated enzymes. In another paper, the oxidation of glucose to gluconic acid was performed in a membrane reactor.<sup>248</sup> As catalysts, catalase and glucose oxidase were trapped between two semipermeable membranes of regenerated cellulose. The reaction mixture consisted of a glucose solution at pH 5.5 saturated with oxygen, which was continuously fed through one grooved section outside the membranes (liquid side). Oxygen was delivered at a pressure over 1 atm to the opposite grooved compartment (gas side). The studies were carried out under conditions where the oxygen transfer was a key process. It was concluded that the membrane permeation coefficient and oxygen pressure were the most important parameters influencing the reaction rate.<sup>248</sup> In another publication, a commercial mixture of free glucose oxidase and catalase called hyderase was utilized to oxidize glucose.<sup>249</sup> The kinetics studies agree with a Michaelis-Menten type reaction with two kinetic parameters, *i.e.*,  $k_1$  denotes the reaction between the oxidized enzyme and glucose (the apparent activation energy was 49.6 kJ mol<sup>-1</sup>), and  $k_c$  is related to a combination of the other reaction steps (the apparent activation energy was 26.7 kJ mol<sup>-1</sup>). The oxygen transfer enhancement in the oxidation of glucose by catalase/glucose oxidase was accomplished using an antifoam agent (KM-70), *n*-hexadecane or soybean oil as additives.<sup>250</sup> Antifoam agents diminished the oxygen transfer rate; also, *n*-hexadecane or soybean oil (more significantly) decreased this parameter. This was correlated with the spreading coefficient of the oil on water. However, the combined use of antifoam agent and other additives increased the oxygen concentration. This was explained by the elimination of the antifoam-agent molecules away from the air-water interface. The enzyme kinetics remained unaltered by the addition of

KM-70, *n*-hexadecane and/or soybean oil.<sup>250</sup> A commercial pyranose 2-oxidase in combination with catalase was used to oxidize  $\beta$ -D-glucopyranose.<sup>251</sup> The kinetic model of the reaction was ping-pong bi-bi type, and the authors also included the inactivation of the oxidase by hydrogen peroxide and the *in situ* hydrogen peroxide destruction catalyzed by catalase (with generalized Yano-Koya kinetics) in the model. Catalase reduced the oxidase inactivation; however, it also reduced the reaction rate.<sup>251</sup>

Some papers bear special interest, such as those where the authors modified free catalase and glucose oxidase to improve their performance while maintaining the enzymes in soluble form. For example, glutaraldehyde was utilized to produce soluble copolymerized catalase, glucose oxidase or catalase/glucose oxidase biocatalysts (when using glucose oxidase, bovine serum albumin was utilized as a feeder protein).<sup>252</sup> These soluble aggregates exhibited better thermal stability than the untreated enzymes.

**8.2.2. Use of catalase/glucose oxidase co-immobilized biocatalysts.** It should be noted that the main objective of co-immobilization is to reduce or even fully eliminate the lag time found in many cascade reactions<sup>222</sup> (Fig. 7 and 8). In the case of utilization of catalase and glucose oxidase to produce D-gluconic acid, the function of catalase is double: produce oxygen, which should be used by glucose oxidase (this will be mainly a kinetic advantage)<sup>222</sup> and prevent the inactivation of glucose oxidase caused by hydrogen peroxide<sup>138</sup> (Fig. 9). In this case, the lag time in destroying the inactivating agent may expose the glucose oxidase to high concentrations of the reagent. The hydrogen peroxide concentration increases with the glucose oxidase activity and the biocatalyst particle size. Therefore, at first glance, the advantage of co-immobilization of the enzymes to maintain minimal exposure of glucose oxidase to hydrogen peroxide may be very relevant for glucose oxidase stability. Moreover, if the oxygen produced by hydrogen peroxide destruction is located in other particles, the activity of the glucose oxidase will not be affected.

The advantages of using co-immobilized catalase and glucose oxidases compared to glucose oxidase alone have been exemplified in many papers. For example, the enzymes were covalently immobilized in ultrafiltration membranes from acrylonitrile copolymer oxidized with hydrogen peroxide to obtain amide groups in the modified membranes.<sup>253</sup> This system showed double the activity of glucose oxidase alone. Moreover, glucose oxidase without catalase was deactivated by hydrogen peroxide more rapidly than a co-immobilized biocatalyst. The enzymes were also immobilized onto an anion-exchange membrane reactor composed of low-density polyethylene modified with 4-vinylpiridine, then compared to co-immobilized catalase/glucose oxidase or glucose oxidase alone.<sup>27</sup> The D-gluconic acid production was low using glucose oxidase alone. The amount of produced D-gluconic acid increased 30 fold if glucose oxidase was immobilized next to an anion-exchange membrane, as this permitted the selective removal of the D-gluconic acid and reduced the



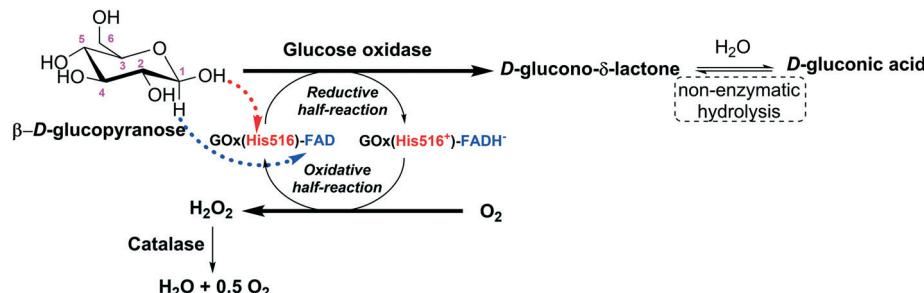


Fig. 9 Destruction of hydrogen peroxide by catalase in the oxidation of glucose catalyzed by glucose oxidase.

enzyme inhibition. Using the co-immobilized enzymes in this system, the oxidation yield reached a value of 95%.<sup>254</sup>

Moreover, in some publications, a real comparison between free, immobilized or co-immobilized enzymes is described. In an interesting paper, glucose oxidase and catalase, individually or co-immobilized in silanized nickel silica alumina activated with glutaraldehyde, were compared in the production of D-gluconic acid.<sup>254</sup> The amount of product formed depended on the activity of both enzymes in the system. The oxidation efficiency increased as the ratio glucose oxidase/catalase decreased. Moreover, the efficiency increased when the activities of both enzymes increased even if the relationship between both enzymes was unaltered. The paper compared co-immobilized enzymes, individually immobilized enzymes and soluble enzymes. The results showed that the co-immobilized enzyme afforded the best results.<sup>254</sup>

The efficiency of individually immobilized glucose oxidase-containing liposomes<sup>255</sup> was improved by adding the channel protein OmpF from *Escherichia coli* to the liposome and co-immobilizing the glucose oxidase with catalase.<sup>256</sup>

OmpF increases the speed of entry of the glucose molecules into the liposome (Fig. 10). Both strategies increased the production of D-gluconic acid up to 17 times compared to the previous glucose oxidase, with no leakage of any of the enzymes. Then, the liposomes containing the enzymes and the transport protein were covalently immobilized in chitosan gel beads, improving the operational stability of the system.<sup>256</sup> The same group later studied the stability of catalase immobilized in liposomes, without the membrane protein, adding hydrogen peroxide or co-immobilizing catalase and glucose oxidase and adding glucose and oxygen.<sup>257</sup> A test tube and an external loop airlift bubble column were used as static liquid and circulating liquid flow systems, respectively. The immobilization of catalase inside the liposome reduced enzyme dissociation by increasing the catalase concentration, which increased the enzyme stability.<sup>258</sup> Immobilized catalase was able to successively decompose 10 mM hydrogen peroxide, while the free enzyme lost activity with each hydrogen peroxide addition. This high stability of the liposome-catalase was explained by the diffusional limitation of the liposome towards hydrogen

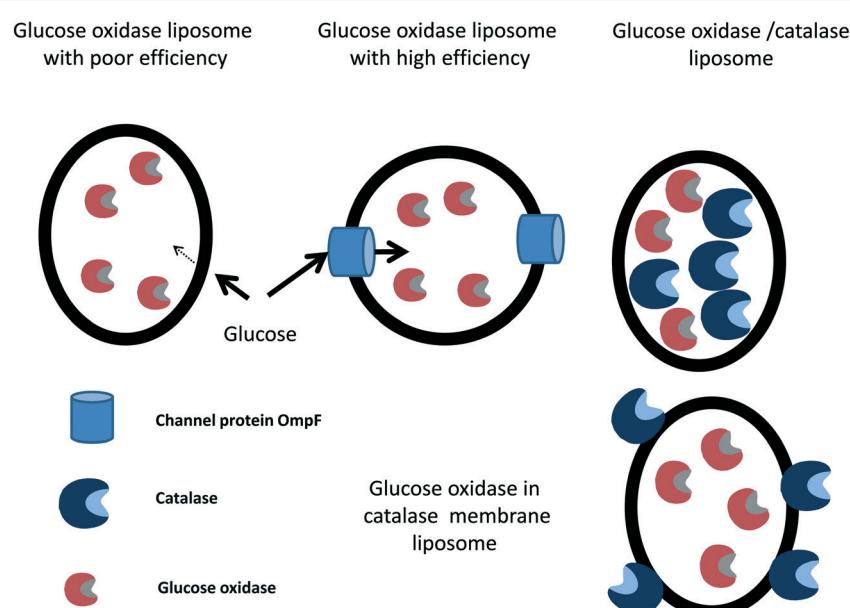


Fig. 10 Different liposomes developed for the oxidation of glucose.



peroxide, which avoided exposure of the enzyme to the full concentration of this deleterious reagent.<sup>138</sup> Using catalase and glucose oxidase and 10 mM of glucose in the static liquid in a test tube, the free catalase and immobilized catalase could be reused continuously because the low glucose oxidase activity (due to poor permeability of the liposome membrane to glucose) enabled the hydrogen peroxide to remain at low concentration. The D-gluconic acid production reaction rates were increased in the airlift. Much larger oxidation rates were observed because of an increase in the permeability of the liposome membrane to glucose in the gas-liquid two-phase flow. Using glucose oxidase immobilized in the liposomes and free catalase, the oxidation rate was lower than that using the co-immobilized system<sup>257</sup> (Fig. 10). Later, catalase was conjugated to the membrane of the liposomes using 1,2-dioleoyl-sn-glycero-3-phosphoethanolamine-N-(glutaryl), and this was utilized to trap different amounts of glucose oxidase<sup>259</sup> (Fig. 10). After using the liposome for 75 h, scarce accumulation of hydrogen peroxide was appreciated. Utilizing liposome sub-lytic concentrations of cholate, the liposome permeability to glucose could be increased.<sup>259</sup> The authors proposed the use of this catalase-liposome for other oxidase reactions. In a further research effort, these catalase-liposomes containing glucose oxidase were utilized in an external loop airlift bubble column to produce D-gluconic acid, and the results were compared with those achieved using a static liquid system.<sup>260</sup> Using the latter, the activity was quite low because of the low permeability of the liposome membrane to the glucose molecules. In the airlift reactor, the reaction rates significantly increased because the reactor induced permeabilization of the liposomes. The structural stability of the liposomes in the airlift was dependent on its initial mean diameter: if it was 168.8 nm, the liposomes remained unaltered, while if it was 269.5 nm, the liposomes were partly disrupted and the catalase was deactivated.<sup>260</sup>

Another paper compares membrane containing glucose oxidase and catalase using independently immobilized and co-immobilized systems using a rotating disk electrode device.<sup>261</sup> In this study, the intrinsic kinetic parameters and mass transfer (internal and external diffusion) of the different systems were analyzed. Enzyme immobilization decreases maximum enzyme intrinsic activity but does not affect Michaelis constants.<sup>261</sup> In another paper, magnetic mesoporous bioactive glasses were modified with polyethylene glycol and were utilized to co-immobilize glucose oxidase and catalase using glutaraldehyde, giving better results than the individually immobilized enzymes.<sup>262</sup> Another study shows the co-immobilization of previously chemically modified enzymes<sup>263</sup> to enable the promotion of a self-assembling supramolecular structure. To achieve this goal, glucose oxidase and catalase were co-immobilized through the supramolecular recognition of  $\beta$ -cyclodextrin (attached to glucose oxidase) and adamantine (bound to catalase).<sup>264</sup> This self-assembled multi-enzyme system was spontaneously formed immediately after mixing the two modified enzymes. The efficiency of the system

improved compared to that of the free enzymes (activity by a 3.7 fold factor,  $k_{cat}/K_M$  by 7 times). This was related to the rapid destruction of hydrogen peroxide. The advantages of the co-immobilized biocatalyst increased as the glucose concentration increased.<sup>264</sup>

Curiously, one paper offers a result where enzyme co-immobilization was not the best solution. In that paper, the objective was to transform all glucose to D-gluconic acid; however, the aim was to facilitate the purification of xylose using free or immobilized catalase and glucose oxidase.<sup>265</sup> In this paper, hydrogen peroxide was utilized as an oxygen source (without considering the negative effect of this reagent on the stability of the enzymes).<sup>138</sup> To accomplish this, only immobilized glucose oxidase, co-immobilized glucose oxidase and catalase or soluble glucose oxidase and catalase were compared using a membrane bioreactor.<sup>265</sup> The enzymes were immobilized on an ultrafiltration membrane. Under optimal conditions, the best productivity was obtained using the free enzymes because of the diffusion limitations found using co-immobilized enzymes and the poor performance of the individual immobilized catalyst of glucose oxidase.<sup>265</sup>

In other papers, the only objective was to develop strategies that permitted the co-immobilization of catalase and glucose oxidase without confirming the advantages/problems of this procedure.<sup>106,222</sup> For example, glucose oxidase and catalase were co-immobilized *via* adsorption in controlled-pore titania particles.<sup>266</sup> This yielded stable enzymes, and as expected, the authors found that catalase played a double role: it increased both the activity and stability of glucose oxidase. Other authors followed similar strategies and obtained similar results.<sup>267–269</sup>

Catalase and glucose oxidase were co-immobilized on a support of Ni-impregnated silica alumina, and the efficiency of the catalase as result of the activities of the two enzymes was assessed.<sup>270</sup> The authors found that using a constant ratio of enzymes, the performance of the catalase increased when the global enzyme activities increased. The co-immobilized biocatalyst showed the maximum activity at pH 5.5, which corresponds to the optimal pH for glucose oxidase. This optimal pH was not observed using a system composed of individually immobilized enzymes or free enzymes.<sup>270</sup> Catalase and glucose oxidase have been also immobilized in polyamide hollow fibers.<sup>271</sup> The immobilization yield and final loading were improved if the fibers were coated with Cibacron Blue F3GA. Fluorescence spectrophotometry showed that the enzyme immobilization did not produce significant conformational changes.<sup>271</sup> In other research, the enzymes were covalently co-immobilized onto magnesium silicate (florisil) by covalent coupling in the presence of glucose and oxygen (that is, the reaction produced D-gluconic acid and hydrogen peroxide).<sup>272</sup> The activities of immobilized glucose oxidase and catalase reached a maximum upon the addition of glucose (15 and 20 mM glucose respectively). In another paper, this group analyzed the differences in the performance of co-immobilized biocatalysts that were sequentially and



simultaneously co-immobilized at different enzyme activity ratios using the same support.<sup>273</sup> The sequentially co-immobilized biocatalyst showed a higher efficiency than the simultaneously co-immobilized glucose oxidase–catalase. The individually immobilized glucose oxidase has 30% of the activity of the best co-immobilized biocatalyst. The improved activity and reusability of glucose oxidase of the co-immobilized biocatalyst was attributed to the protection afforded by the destruction of hydrogen peroxide by catalase and the generation of oxygen.<sup>273</sup> The effect of the enzyme immobilization order was further studied. Glucose oxidase and catalase were sequentially co-immobilized in D301T resin to analyze the effects of the immobilization order and the amounts of enzymes in the final co-immobilized biocatalyst.<sup>274</sup> The results were better when catalase was first immobilized (that is, immobilized in the external volume of the support).<sup>222</sup> The treatment of the co-immobilized biocatalyst with glutaraldehyde, an efficient crosslinking reagent,<sup>275</sup> improved the recovery activity and the operational stability of the co-immobilized biocatalyst (retaining over 85% of the initial activity after 10 reuses).<sup>274</sup> However, in another paper, the results were completely different. This paper demonstrated that matching of the dimensions of the enzymes and the hierarchical pore sizes of the carriers activated with glutaraldehyde are critical to the success of immobilization processes.<sup>276</sup> However, the simultaneous immobilization obtained in this case afforded better results than the sequential immobilization of the enzymes.

Catalase and glucose oxidase have been immobilized using non-porous glass beads coated with  $\gamma$ -aminopropyltriethoxysilane and polyethyleneimine activated with glutaraldehyde.<sup>277</sup> Polyethyleneimine coating offered the best results. The concentrations of polyethyleneimine and glutaraldehyde, the glucose oxidase/catalase ratio, and the load of the beads were found to be relevant to the immobilization yields. Activation of carbon fiber by treatment with nitric acid or sulfuric acid afforded the best results. Using this support, the effects of the amounts of both enzymes, glutaraldehyde concentration and time of the glutaraldehyde treatment on the immobilization efficiency were studied. The optimal biocatalysts improved the storage and operational stabilities and enlarged the range of pH values and temperatures where the enzymes can be used. After 10 reaction cycles, more than 70% of the enzyme activity was recovered.<sup>278</sup> In another study, the enzymes were also co-immobilized on carbon fiber and activated by following diverse support activation protocols.<sup>278</sup> Recently, polyglycidyl methacrylate spheres were utilized to co-immobilize glucose oxidase and catalase.<sup>279</sup> The support was activated with a combination of amination and plasma. Immobilization increases the optimal pH (from 5.5 to 7.5) and temperature (from 25 °C to 40 °C) so that 82% of the initial activity was maintained after three glucose oxidation batches; although this value was considered good by the authors, it is not high enough for industrial implementation of the biocatalyst.<sup>279</sup>

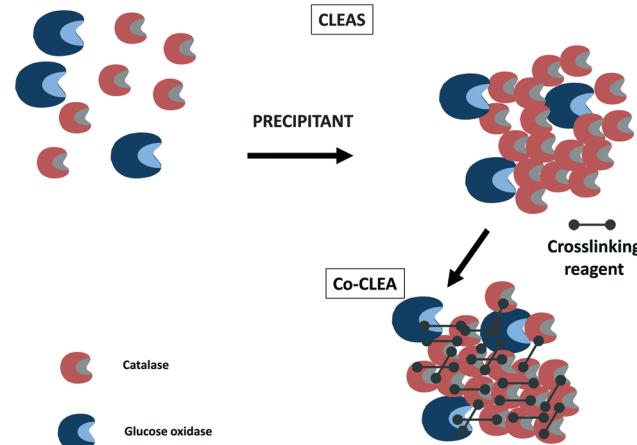


Fig. 11 Co-immobilization of glucose oxidase and catalase using crosslinking enzyme aggregate technology.

Crosslinked enzyme aggregates<sup>280–282</sup> have been also utilized in some instances to co-immobilize catalase and glucose oxidase (Fig. 11). For example, the effects of the precipitant and crosslinking agents as well as the presence of a feeder protein were studied in the preparation of cross-linked aggregates of catalase and glucose oxidase.<sup>22</sup> Differences in enzyme stabilities are a problem in enzyme co-immobilization,<sup>106,222</sup> however, few papers demonstrate the stabilities of all the co-immobilized enzymes. This paper showed that the stabilities of both immobilized enzymes were very similar. Therefore, the difference in the stabilities of the co-immobilized enzymes was no longer a problem in this case. The biocatalyst enabled around 96% conversion of D-glucose into D-gluconic acid in a bubble column reactor.<sup>22</sup>

Catalase and glucose oxidase have also been co-immobilized using the copolymer technique<sup>283</sup> (Fig. 12). Catalase and glucose oxidase were crosslinked using genipin<sup>284</sup> and subsequently employed for oxidizing glucose.<sup>20</sup> Genipin-crosslinked glucose oxidase/catalase increased its activity 10-fold compared to the unmodified glucose oxidase/catalase mixture.

In some instances, the co-immobilized catalase/glucose oxidase system is used to perform some kinetic studies, including substrate diffusional limitation problems, enzymes deactivation by hydrogen peroxide, etc. For example, the macro-kinetics of D-gluconic acid production was studied using co-immobilized glucose oxidase and catalase in continuous and batch reactions.<sup>285</sup> The results showed that the effectiveness is improved using a co-immobilized biocatalyst. However, hydrogen peroxide caused the inactivation of both enzymes. This enzyme inactivation increases as the activity of glucose oxidase increases.<sup>285</sup> Therefore, even when using co-immobilized enzymes, it is necessary to carefully design the biocatalyst to reduce the inactivation of both enzymes. Later, this research group performed a theoretical analysis of the interactions between the reaction and diffusion rates using this system.<sup>286</sup> The efficiency of the glucose oxidase reaction depended on the



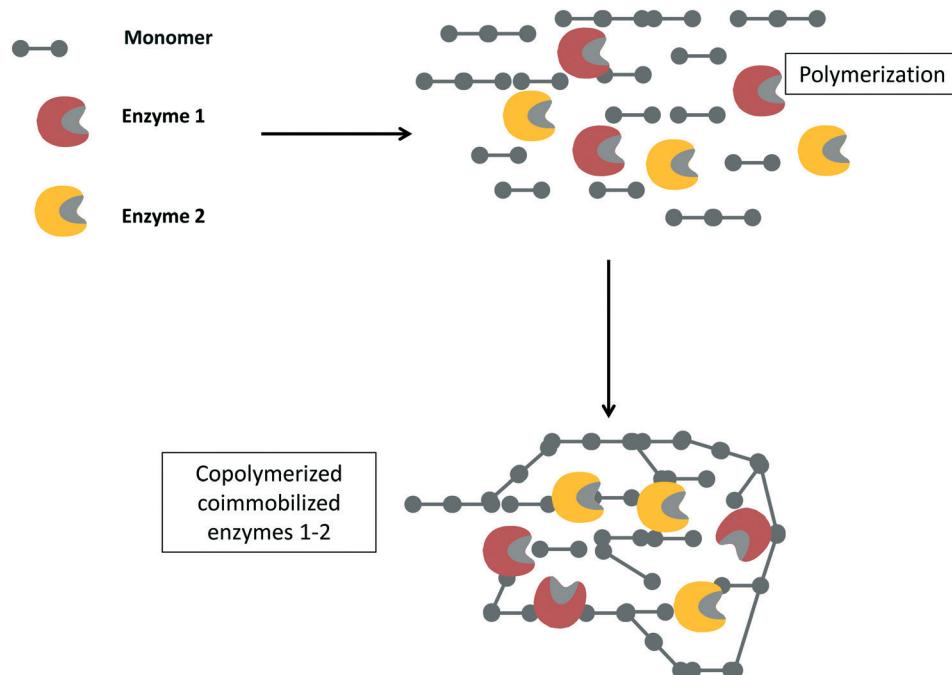


Fig. 12 Co-immobilization of glucose oxidase and catalase using copolymerization technology.

concentrations of glucose and oxygen. They stated that external mass-transfer limitations may produce a change from glucose limitation to oxygen limitation. The predicted efficiency of the co-immobilized biocatalysts was higher than that for the uncoupled reaction; however, the main problem was enzyme deactivation. Similar results were found in another study, where a commercial cocktail containing glucose oxidase and catalase was co-immobilized on pumice and a titania carrier, then activated with a copolymer of phenylenediamine and glutaraldehyde.<sup>287</sup> This co-immobilized biocatalyst was utilized in the production of D-gluconic acid in a differential-bed loop reactor. The kinetics of the reaction was first order regarding the oxygen concentration, suggesting severe external mass-transfer resistance in the range of the utilized flow rates. These results suggest that catalase is the first enzyme that becomes inactivated by hydrogen peroxide. Only by using a large excess of catalase can the inactivation of glucose oxidase be prevented.<sup>287</sup>

The problem of diffusional limitations of substrates was also studied using a co-immobilized biocatalyst in a flow micro-calorimetry study.<sup>288</sup> To study the diffusivity of glucose, catalase and glucose oxidase were covalently co-immobilized in polyacrylonitrile membranes with different pore sizes and in a microfiltration polyamide membrane.<sup>289</sup> As expected, the glucose diffusion increased when the pore size increased, and it also decreased when the enzyme membranes were inactivated.

In other research, using a continuous-flow stirred reactor coupled with a membrane and a continuous-flow reservoir containing hydrogen peroxide, evidence of periodic and aperiodic oscillations in an enzymatic system of glucose

oxidase-catalase was obtained.<sup>290</sup> This was accomplished by matching experimental data obtained under oscillatory instability with the stoichiometric restrictions of the mechanism formulated by considering the stability theory of the reaction networks, focusing on the catalase reaction. The model agreed with the experimentally achieved oscillatory dynamics, including apparently chaotic intermittent behavior.<sup>290</sup>

Another topic studied in this reaction system is enzyme inactivation; in many instances, it is promoted by hydrogen peroxide,<sup>138</sup> while in others, it is caused by the dissociation of the monomers of the multimeric enzymes.<sup>258</sup> This was the subject of a paper using a membrane containing both enzymes, using conditions where the inactivation was homogeneous throughout the membrane.<sup>291</sup> The results pointed again towards hydrogen peroxide inactivation being the main reason for the decreased efficiency of the co-immobilized biocatalyst. In another paper, glucose oxidase and catalase were co-immobilized at optimal activity ratios on 2-amino-4-chloro-s-triazine-cellulose and acrolein/styrene copolymer activated with diaminohexane and glutaraldehyde and used in a recycling fluid-bed reactor to produce D-gluconic acid.<sup>292</sup> The deactivation rates of the enzymes were first-order depending on the presence of hydrogen peroxide. Similar studies were performed using the enzyme co-immobilized in processed perlite, also using recycling fluid bed reactors.<sup>293</sup> Other paper analyzed the inactivation of catalase and glucose oxidase co-immobilized in alginate beads in a continuous stirred tank reactor, proposing a general model of three-parameter irreversible deactivation.<sup>294</sup>

Thus, co-immobilization of catalase and glucose oxidase, if properly performed, is a successful example of the effects

of enzyme co-immobilization on improving enzyme stability and activity because it is important to avoid any delay in the destruction of hydrogen peroxide.

## 9. Conversion of polysaccharides to D-gluconic acid

Glucose-based polysaccharides such as cellulose and starch have been used as substrates in cascade reactions using multienzymatic systems to obtain D-gluconic acid or its derivatives.

### 9.1. Conversion of cellulose to D-gluconic acid

An interesting process involving an enzymatic cascade reaction is the conversion of cellulose to D-gluconic acid or its derivatives.<sup>295</sup> The proposed enzymatic cascade reaction uses a combination of cellulases,  $\beta$ -glucosidase, glucose oxidase and catalase to produce D-gluconic acid from waste cellulosic material. This represents a five-enzyme cascade reaction because cellulase cocktails comprise endo and exoglucanases. In a first case, a DNA-guided approach was used to assemble the five-component enzyme co-immobilized biocatalyst for direct conversion of cellulose to D-gluconic acid and  $H_2O_2$ .<sup>296</sup> The authors found that site-specific co-localization of  $\beta$ -glucosidase and glucose oxidase resulted in an improvement in peroxide production, highlighting the benefits of substrate channeling.

The production of sodium gluconate from cellulose was also reported by a multi-enzymatic reaction.<sup>297,298</sup> Firstly, a cellulase cocktail with high  $\beta$ -glucosidase activity was produced by a fed-batch process using *Penicillium oxalicum* I1-13 with simultaneous cellulose saccharification. Then, glucose oxidase and catalase were co-immobilized to produce sodium gluconate.<sup>297</sup> Later, the same group tested the feasibility of a consolidated bioprocess for sodium gluconate production from cellulose. A recombinant strain named z19 was constructed from *Penicillium oxalicum* wild-type strain 114-2 for simultaneous expression of glucose oxidase and catalase from *Aspergillus niger*. The mutant maintained the cellulolytic ability of the wild-type strain and secreted certain amounts of glucose oxidase and catalase. Using cellulose (filter paper power) as the initial substrate, a total of 13.54 g L<sup>-1</sup> sodium gluconate was obtained at the end of the fermentation.<sup>298</sup>

In a final example, cellulase and glucose oxidase were co-immobilized on graphene oxide to produce D-gluconic acid from carboxymethyl cellulose.<sup>299</sup> The enzymes were immobilized by a step-by-step method. The graphene surface was activated with 2,4,6-trichlorotriazine followed by conjugation with cellulase (*N*-hydroxysuccinimide/1-ethyl-(3-dimethylaminopropyl) carbodiimide hydrochloride) and glutaraldehyde were used to activate the graphene residues and primary amino groups of cellulase, allowing glucose oxidase to be immobilized. The multi enzymatic biocatalyst

could be reused for 7 cycles, and the conversion of cellulose to D-gluconic acid reached almost 64% in 2 h.<sup>299</sup>

### 9.2. Conversion of starch to D-gluconic acid

In a similar way, starch can be converted to D-gluconic acid by a cascade reaction involving its initial hydrolysis by a glucoamylase and further conversion of glucose to D-gluconic acid by glucose oxidase. Curiously, these examples do not use catalase to control the deleterious effects of hydrogen peroxide on the enzymes. In the first example, both glucoamylase and glucose oxidase were assembled in an ultrafilter by layer-by-layer adsorption using polyethylenimine as a coupling poly-cation.<sup>300</sup> Reaction products and unreacted starch were readily separated by filtration when the substrate solution was passed through these multi-enzyme films. Later, the same enzymes were co-immobilized by hydrophobic adsorption on chemically reduced graphene oxide.<sup>301</sup> This multi-enzyme system was used as a biocatalyst in the starch-to-gluconic acid reaction in one pot, and it yielded 82% D-gluconic acid in 2 h.

In an elegant example, glucoamylase and glucose oxidase were immobilized on silver dendrites with a hierarchical nanostructure<sup>302</sup> (Fig. 13). The obtained biocatalyst was employed for the one-pot transformation of starch to D-gluconic acid, and the final product was obtained in high yield. Moreover, the co-immobilized biocatalyst exhibited high stability and reusability. The authors claimed that their results showed that the co-immobilization of enzymes on hierarchical structures could be extended to other biocatalytic cascade reactions.<sup>302</sup>

### 9.3. Conversion of disaccharides to D-gluconic acid

Several disaccharides, such as sucrose, maltose and lactose, have been used for D-gluconic acid production by combining a disaccharide hydrolytic enzyme to release glucose molecules and glucose oxidase to convert glucose to D-gluconic acid. In some cases, the objective was the preparation of a biosensor to detect the respective disaccharide; in these cases, D-gluconic acid was not the final target. Biosensors were prepared to determine sucrose,<sup>303</sup> maltose<sup>304</sup> and lactose.<sup>305,306</sup> The biosensors were assembled by co-immobilizing glucose oxidase with  $\alpha$ -glucosidase, invertase or  $\beta$ -galactosidase for detection of maltose, sucrose and lactose, respectively. A special case is the assembly of an integrated nanodevice with bi-enzymatic cascade control for on-command cargo release. The nanocarrier is based on Au-mesoporous silica Janus nanoparticles capped at the mesoporous face with benzimidazole/ $\beta$ -cyclodextrin-glucose oxidase pH-sensitive gate-like ensembles and functionalized with invertase on the gold face. The rationale for this delivery mechanism is based on the invertase-mediated hydrolysis of sucrose to yield glucose, which is further transformed into D-gluconic acid by glucose oxidase, causing disruption of the pH-sensitive supramolecular gates at the Janus nanoparticles. This enzyme-powered device was successfully employed in



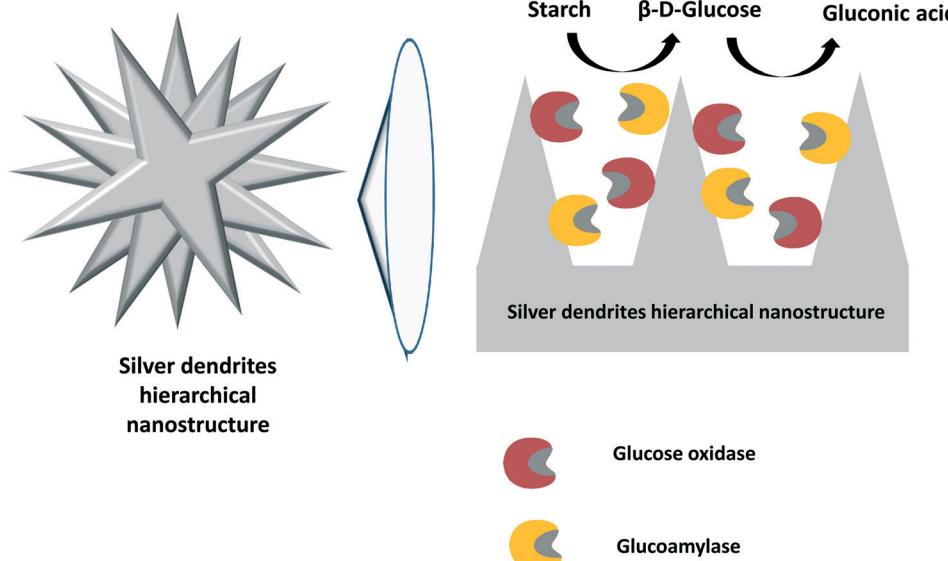


Fig. 13 Co-immobilization of glucose oxidase and glucoamylase using silver dendrite hierarchical nanostructures.

the autonomous and on-demand delivery of doxorubicin in HeLa cancer treatment.<sup>307</sup>

Some studies reported the use of maltose and sucrose as substrates for D-gluconic acid production in batches using catalase to destroy the hydrogen peroxide<sup>21,308,309</sup> and using fed-batch,<sup>310</sup> continuous<sup>311</sup> and membrane-continuous<sup>309,310</sup> processes. In general, all processes were satisfactory, reaching high yields of conversion of maltose and sucrose to D-gluconic acid.

## 10. Use of D-gluconic acid or glucose oxidase to alter the inhibition of other enzymes

Glucose oxidase has been used in other enzymatic reactions with the intention of removing glucose from the medium or to accumulate D-gluconic acid. This may alter the main enzyme inhibition mechanism (increasing or decreasing it depending on whether the inhibition is caused by D-gluconic acid). One example where the objective was to increase the imbibition of one enzyme is the production of cellobiose from cellulose. When the cellulase cocktail hydrolyzes cellulose, cellobiose is released synergistically by endo- and exoglucanases. The cellobiose is then hydrolyzed to glucose by  $\beta$ -glucosidase.<sup>312</sup> Blocking  $\beta$ -glucosidase activity increased the accumulation of cellobiose. In this sense, D-gluconic acid inhibits  $\beta$ -glucosidase activity in that cellulase system. Thus, directly adding D-gluconic acid or adding glucose oxidase to produce *in situ* D-gluconic acid by glucose oxidation resulted in accumulation of cellobiose.<sup>313,314</sup> This indicates that both exo- and endoglucanases can act synergistically without the hydrolytic action of  $\beta$ -glucosidase in this cellulase cocktail during cellulose hydrolysis in the presence of D-gluconic acid as an inhibitor.

Another interesting application of glucose oxidase, in this case to avoid enzyme inhibition, is in the synthesis of

oligosaccharides from sucrose or lactose to produce fructooligosaccharides (FOS) or galactooligosaccharides (GOS). In the transglycosylation reaction, the galactosyl or the fructosyl moiety (from lactose or fructose, respectively) are transferred to another sugar molecule instead of water, resulting in oligosaccharide formation.<sup>315,316</sup> Glucose is the by-product in both reactions and inhibits the transglycosylating activity. The reaction rate increases if glucose is removed; therefore, a higher yield of oligosaccharides can be obtained. Thus, the combination of glucose oxidase with  $\beta$ -fructofuranosidase or  $\beta$ -galactosidase has been reported to improve FOS and GOS yields by the removal of glucose from the reaction medium.<sup>317-320</sup> The subsequent D-gluconic acid in the final product was easily removed by cationic ion exchange resin.

In another paper, trehalose was obtained from starch by a multi-enzymatic system. Initially, starch was hydrolyzed to maltose by amylases and pullulanase.<sup>321</sup> The obtained high-maltose syrup was further converted into trehalose by a one-step enzymatic process using trehalose synthase as a biocatalyst.<sup>322</sup> The final reaction product mixture contains glucose, trehalose and unreacted maltose. This mixture can be treated with glucoamylase and glucose oxidase to facilitate the separation of trehalose by sequential conversion of maltose to glucose and glucose to D-gluconic acid.<sup>323-325</sup> After separation by ionic exchange, trehalose can be successfully purified, crystallized and identified with 92.6% purity and a recovery yield of 94.2%.<sup>325</sup>

## 11. Other applications of glucose oxidase

The glucose oxidase reaction, as an oxygen-depleting system, producer of D-gluconic acid or hydrogen peroxide, and pH-decreasing agent in combination (or not) with catalase, has



many other applications in addition to the production of *D*-gluconic acid. We will end this review by summarizing some of these applications, excluding the field of biosensors, which has been the subject of many recent specific reviews.<sup>114–117</sup>

### 11.1. Improvement of food quality

Glucose oxidase has found many applications in food quality improvement.<sup>326</sup> The conversion of glucose to *D*-gluconic acid using glucose oxidase–catalase was used to prevent the deteriorative Maillard reaction.<sup>327</sup> Albumen desugaryzation was used as a model reaction, and the treatment enabled reduction of the Maillard reaction by 40%.

Glucose oxidase has been used to improve the organoleptic properties of many food products. For example, the treatment of white grape juice with glucose oxidase–catalase improved its color stability; moreover, the aroma and taste (non-flavonoid phenolic content) were enhanced.<sup>328</sup> In another study, glucose oxidase/catalase, ascorbic acid and peroxidase systems were compared in the removal of oxygen to reduce the browning of Golden Delicious apple and Kaiser pear purées during storage.<sup>329</sup> Glucose oxidase was the most effective treatment to reduce the dissolved oxygen content in the apple and pear purées and exhibited an ability to modulate the non-enzymatic browning during fruit processing and purée storage.

Another application of this enzyme in food quality management is in the stabilization of oil/water emulsions *versus* oxidation.<sup>330</sup> Glucose oxidase/catalase was employed to stabilize salad dressing emulsions and measure peroxide values.<sup>331</sup> The desired oxygen concentration decrease was improved at pH near neutrality using a glucose concentration of 0.5% and a temperature near 50 °C. The oxygen concentration also decreased with increasing amount of enzyme. In another study, the glucose oxidase/catalase system showed an antioxidant effect in mayonnaises containing different amounts of fish oil when stored at low temperature.<sup>332</sup> The amount of enzyme required to slow the lipid oxidation increased when the lipid oxidation rate increased. This effect was achieved by the reduction of oxygen in the medium. Moreover, glucose oxidase/catalase was explored as an antioxidant in a food model consisting of an oil/water emulsion (a model of mayonnaises and other high-fat dressings) packed in an oxygen-permeable plastic bag.<sup>333</sup> The results showed that the speed of lipid oxidation is inversely proportional to a term containing the glucose oxidase concentration. Later, the oxidative stability of a model salad dressing was studied by measuring the volatile compounds of sample bottles and peroxide values.<sup>334</sup> Upon adding 1.0% glucose, glucose oxidase/catalase acted as an anti- or pro-oxidant depending on the enzyme concentrations. At moderate concentrations of enzymes, the volatile compounds and peroxide values decreased, that is, the biocatalyst behaved as an antioxidant. When using higher enzyme concentrations, the enzymes functioned as pro-

oxidants.<sup>334</sup> Obviously, the situation could change if the ratio of glucose oxidase to catalase were altered; however, the researchers did not alter it.

The enzyme was also used to improve the preservation of fish. Glucose oxidase and catalase were used in artificial seawater bearing 4% w/v glucose for on-board shrimp preservation.<sup>335</sup> The system decreased browning by ~80% and also inhibited the release of ammonia and total volatile nitrogen. Due to the increase in nitrogen compounds, it was necessary to replace the enzyme solution after 14 days.<sup>335</sup>

Preservation of eggs was also enhanced using glucose oxidase. Thus, glucose oxidase at different concentrations of glucose was evaluated as a bactericide agent in liquid whole egg.<sup>336</sup> This treatment could fully eliminate *Salmonella enteritidis*, *Micrococcus luteus* and *Bacillus cereus* and presented bacteriostatic activity against *Pseudomonas fluorescens*. When the efficacy of this strategy was assayed on the natural contamination flora of liquid egg, it was found that this treatment prolonged the lag phase by 6 days. The authors explained this effect by the production of hydrogen peroxide.<sup>336</sup> Other uses related to the egg industry involve improving the organoleptic properties of processed eggs. Catalase and glucose oxidase were co-immobilized on polyethylenimine-dressed cotton cloth by ion exchange and then treated with glutaraldehyde.<sup>337</sup> The biocatalyst was utilized for the de-sugaring of egg mélange in a batch reactor to produce a spray-dried, sugar-free egg powder.

### 11.2. Reduction of sugar in juice to reduce the alcohol concentration after fermentation

Wine with reduced alcohol content may have healthy effects. To this end, without increasing the amount of remaining glucose, some authors have proposed to treat the grape juice prior to fermentation (Fig. 14). In this way, glucose oxidase was utilized to optimize the glucose content of grape juice to produce low-alcohol wines.<sup>338</sup> The acidity of grape juice slowed the reaction and determined the conversion of glucose by glucose oxidase; however, after optimization, an 87% reduction in glucose was obtained (the *D*-gluconic acid concentration in the grape juice was 73 g l<sup>-1</sup>). Later, the same research group characterized the final properties of the wine obtained by reducing the glucose content (to around 20%).<sup>339</sup> The ethanol concentrations of the produced wine ranged between 6.3% and 6.5%. Part of the formed *D*-gluconic acid precipitated, reducing the high *D*-gluconic acid concentration in the juice; the pH was fairly similar to that of the standard wine (with alcohol content over 13%), although the titrated acidity was higher, very likely due to the presence of more quinone and oxidizable phenolic compounds.<sup>339</sup>

Later, the *Aspergillus niger* gene encoding glucose oxidase was cloned in *Saccharomyces cerevisiae*. This strategy, with glucose oxidase present during the fermentation, decreased the sugar content and, thus, the final alcohol concentration.<sup>340</sup> This strategy also inhibited the growth of wine spoilage organisms (e.g., lactic acid or acetic acid



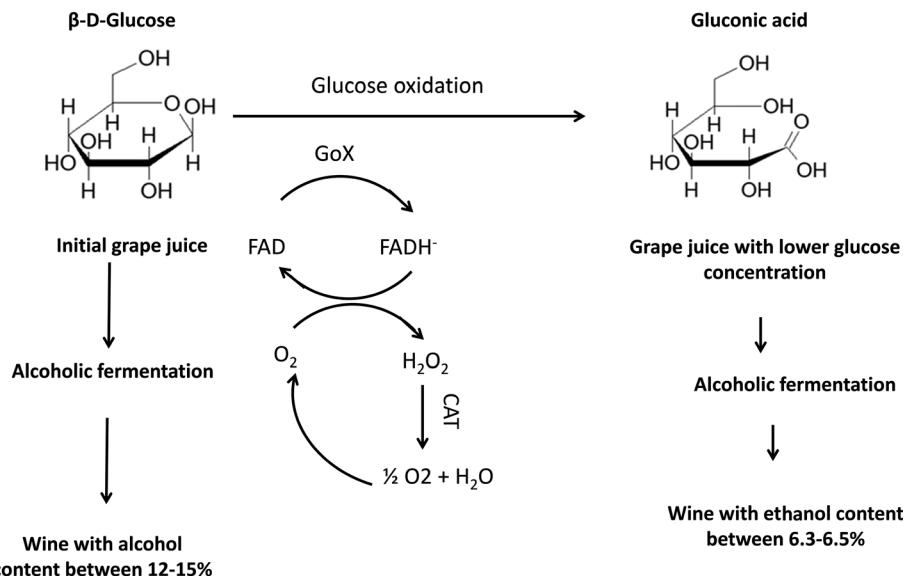


Fig. 14 Reduction of glucose content in grape juice to reduce the final alcohol concentration after fermentation using a glucose oxidase–catalase biocatalyst.

bacteria). The results showed a reduction in ethanol content of 1.8–2.0%. A more recent paper discussed the problem of the increasing glucose levels in grapes due to global warming.<sup>341</sup> In this instance, glucose oxidase was used in combination with catalase in its free form. Aeration influenced the wine, and the researchers obtained a 2% reduction in ethanol content.<sup>341</sup>

### 11.3. Use of glucose oxidase to facilitate monosaccharide purification

Glucose is presented in many monosaccharide mixtures and can complicate the purification of the most valuable sugars.<sup>342–345</sup> The modification of glucose with glucose oxidase facilitates separation and the achievement of a higher added value product. For example, using a membrane system, the separation of glucose and xylose, which are very similar, is quite difficult.<sup>346</sup> The full oxidation of glucose by glucose oxidase in the presence of catalase simplifies the separation by using the anionic nature of D-gluconic acid as a distinctive feature. In this way, xylose and D-gluconic acid can be easily separated.<sup>346</sup> This was later utilized in biorefinery liquors obtained from hydrothermal pretreatment of wheat straw, corn stover and *Miscanthus* stalks.<sup>347</sup> In another research effort, glucose oxidase and catalase were co-immobilized using a sol–gel protocol on silica inverse opals and utilized to oxidize glucose (with a yield of 98.97%) from commercial isomaltoligosaccharide preparations.<sup>348</sup> The operational stability requires improvement, as less than 80% of the enzyme activity remained after 6 reuses.

### 11.4. Application of glucose oxidase in textile industries

Glucose oxidase has been used for the production of hydrogen peroxide required for bleaching cellulose fibers,

e.g., using glucose during desizing.<sup>349</sup> Also, the produced D-gluconic acid plays some role in this bleaching because of its outstanding chelating properties for metal ions. This process is milder from an environmental point of view than the common addition of hydrogen peroxide, and it has already been reviewed.<sup>350</sup>

### 11.5. Glucose oxidase in fuel cells

The use of glucose oxidase in fuel cells was proposed a long time ago. In this contribution, it was suggested that because glucose is present in the bloodstream, glucose oxidase should be a good catalyst for supplying the electrical energy needed for the operation of devices implanted in the human body.<sup>351</sup> Later, a glucose/O<sub>2</sub> biofuel cell was built using a surface glucose oxidase monolayer as an anode, where the cathode presented a cytochrome c/cytochrome oxidase complex.<sup>352</sup> Glucose oxidase oxidized glucose to D-gluconic acid, whereas the enzymes in the cathode reduced O<sub>2</sub> to water. The appropriate genetic engineering of the proteins permitted a correct assembly on the electrodes, improving the power of the biofuel cell.<sup>352</sup>

More recently, thiophene-3-acetic acid and the conducting copolymer 3-methylthiopene were used to modify a carbon paper electrode on which glucose oxidase was covalently immobilized.<sup>353</sup> The modification of the paper increased the surface area, permitting higher enzyme loading and a high speed of electron transfer between the electrode and the electron mediator (*p*-benzoquinone). In another paper, carboxylated multi-walled carbon nanotubes were used to coat a polyester-supported screen-printed carbon paste electrode; then, glucose oxidase, 2,5-dihydroxybenzaldehyde, bovine serum albumin, and glutaraldehyde were used to crosslink the composite.<sup>354</sup> This composite increased the



electron-shuttling process and exhibited an electrocatalytic effect on D-gluconic acid, which enabled the removal of more electrons from a glucose molecule. The authors showed that this glucose biofuel cell coupled to a laccase/ABTS cathode generated electric power of  $45 \mu\text{W cm}^{-2}$  in the presence of 1 M glucose at  $37^\circ\text{C}$ .<sup>354</sup> In another paper, glucose oxidase and laccase were suspended in a membraneless, single-chamber cell.<sup>355</sup> Nickel mesh was the oxidative current collector and a carbon-based air electrode enclosed in an acrylic casing was the reductive current collector. The anolyte was glucose oxidase, 200 mM glucose and 3.8 mM FAD, while the catholyte contained laccase enzyme and 216  $\mu\text{M}$  syringaldazine (Fig. 15). An open circuit voltage at pH 5.0 of around 960 mV was obtained, and the electrode could sustain a continuous discharge current of 30  $\mu\text{A}$  for about 31.75 h.<sup>355</sup> Later, glucose oxidase was entrapped in Nafion and multiwalled carbon nanotubes as an anode to build an EFC device that employed sulfonated polyether ketone as an electrolyte membrane.<sup>356</sup> In another paper, glucose oxidase was immobilized on cross-linked carbon-chitosan, which functioned as a conductive enzymatic membrane for electrode applications in biofuel cells.<sup>357</sup> The conductivity was increased by modifying the matrix with ferrocene derivatives. The stability of the enzyme was increased by glutaraldehyde treatment. This device produced a power output of up to  $32.8 \mu\text{W cm}^{-2}$  depending on the redox mediator utilized. Another study demonstrated a cell chamber with oxygen in the cathode cell and glucose in the anode cell; a Nafion membrane was used as an ion transporter.<sup>358</sup> The prototype cell chamber used NaCl in the cathode cell and glucose oxidase in the anodic chamber. Du Toit and collaborators immobilized glucose oxidase onto highly porous gold electrodes and assayed it as an anode in a glucose/O<sub>2</sub> enzymatic biofuel cell, leading to a peak power density of  $6 \mu\text{W cm}^{-2}$  at a potential of 0.2 V.<sup>359</sup> Glucose oxidase was immobilized on ZnO nanoparticles used to coat electrodes, using ferrocenyl  $\pi$ -stacked into a supramolecular architecture as a mediator.<sup>360</sup> This provides a highly efficient architecture and delivers a catalytic current for glucose oxidation. This electrode was incorporated in a glucose/air Nafion-based biofuel cell under "air breathing" conditions at room temperature. A conventional platinum–carbon electrode

was utilized as a cathode.<sup>360</sup> The stability of glucose oxidase was increased by immobilization in Nafion, and it maintained its activity for 120 days.<sup>361</sup> This biocatalyst was bound into a carbon cloth electrode and assembled in a EFC fed with glucose. Nafion permitted the process of electron transfer to the electrode. A micro-fluidic channel plate in which the glucose solution was driven into the fuel cell by capillary force was designed and fabricated using glucose oxidase.<sup>362</sup> The fuel cell proposal comprised both end plates and a microfluidic flow channel plate. The results showed a lower output power than that obtained using an active pumping method; however, in the long term, a constant voltage suggested that the self-pumping fluid enzymatic fuel cell may function stably under a continuous fuel supply.<sup>362</sup> Glucose oxidase was immobilized on a double-layered hydroxide of NiAl electrode and utilized to carry out oxidation of glucose present in blood for energy conversion to be employed as a self-feeding electrode in Lab-on-a-Chip devices.<sup>363</sup>

Glucose oxidase does not always produce the best results. A paper suggested that if laccase is used in a cathode, the negative effect of the hydrogen peroxide on the laccase stability would make it advisable to change glucose oxidase to FAD-dependent glucose dehydrogenase (an O<sub>2</sub>-insensitive enzyme).<sup>364</sup> The cathode was rapidly inactivated using glucose oxidase; meanwhile, its stability was much higher when using the new enzyme. The same group, in another communication, compared both enzymes in an enzymatic biological fuel cell using the cathode with direct electrocatalytic bilirubin oxidase using anthracene-modified multi-walled carbon nanotubes.<sup>365</sup> A glucose oxidase cell produced in an open circuit at pH 6.5 using 200 mM glucose obtained higher maximum current densities and maximum power densities. In this case, the hydrogen peroxide does not affect the short term stability of the cathode; however, it has negative effects in the long term.<sup>365</sup> Another research group compared the same enzymes again when using multi-walled carbon nanotubes to produce enzymatic electrodes.<sup>366</sup> Glucose oxidase provided a higher current density at 0.12 V but a lower current density *versus* Ag/AgCl in synthetic medium; however, at physiologically relevant glucose concentrations (5 mM), flavin-dependent glucose dehydrogenase afforded higher current densities.

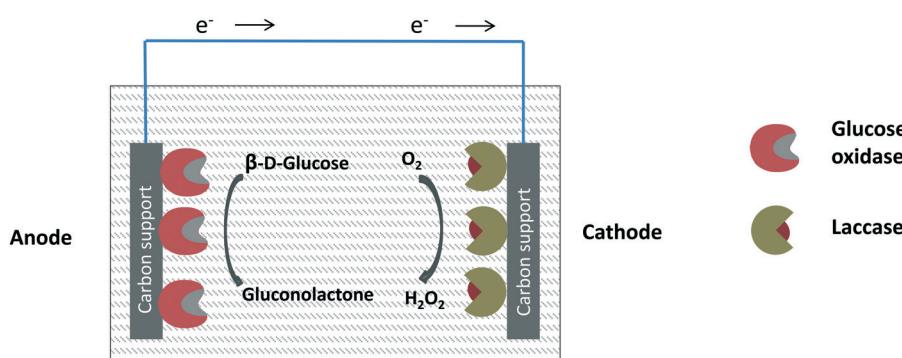


Fig. 15 Co-immobilization of glucose oxidase and laccase using carbon nanotubes as an electrode for fuel cell design.



Another study compared the performance of glucose oxidase and aldoze dehydrogenase as oxidizing agents in an anode, while ABTS and a fungal laccase were employed for reduction of oxygen at the cathode.<sup>367</sup> Cells based on filter paper coated with conducting carbon inks, enzymes and mediators were used. The highest power production, although with low stability, was obtained using aldoze dehydrogenase anodes mediated by an osmium complex.<sup>367</sup>

Glucose oxidase and catalase were co-immobilized on carbon nanotubes coated with polyethyleneimine,<sup>368</sup> and their performance in glucose oxidation was analyzed<sup>369</sup> (Fig. 16). Utilizing the current density peak derived from the FAD redox reaction, the authors determined the Michaelis-Menten constants, electron transfer rate, and sensitivity. The electrical performance using a membraneless glucose biofuel cell was determined; a maximum power density of  $180.8 \pm 22.3 \mu\text{W cm}^{-2}$  was produced, which is the highest value among MPDs obtained by adoption of catalysts.<sup>369</sup>

### 11.6. Use of glucose oxidase and glucose as antimicrobial agents

Hydrogen peroxide has strong antibacterial effects; however, it may also produce some side-damage.<sup>370–372</sup> Therefore, the production of hydrogen peroxide by glucose oxidase has been used in some papers to eliminate or reduce the infectivity of some pathogens, to reduce bacterial infections and to facilitate destruction of bacteria in a milder way than by the direct use of hydrogen peroxide. Glucose oxidase from the caterpillar *Helicoverpa zea* was used to decrease the infectivity

of *Pseudomonas aeruginosa* and *Serratia marcescens* when supplemented with glucose.<sup>373</sup> In another paper, an ultrathin two-dimensional metal-organic framework (two-dimensional 2Cu-TCPP(Fe)) nano-sheet with peroxidase-like activity was used to immobilize glucose oxidase.<sup>374</sup> In this way, glucose could be converted to hydrogen peroxide and D-gluconic acid, decreasing the damaging side effects that directly result from high concentrations of hydrogen peroxide. Moreover, D-gluconic acid decreased the pH to 3.0–4.0, promoting the activation of the peroxidase-like activity of the metal-organic framework and producing a hydroxyl radical that presented antibacterial capacity.<sup>374</sup>

### 11.7. Use of glucose oxidase and glucose as an antitumoral cell agent

Glucose oxidase has different applications in cancer research. It has been used in different methods for the detection of cancer biomarkers.<sup>375</sup> Even more interestingly, various cancer healing approaches have been developed based on the use of this enzyme. This has been recently reviewed;<sup>375</sup> as a short summary, the positive effects may be derived from the consumption of glucose (which produces cancer-starvation therapy); the reduction of oxygen (which increases tumor hypoxia, the so-called hypoxia-activated therapy); and the generation of D-gluconic acid, which produces medium acidification and can be used to release a drug that is contained in a pH-responsive particle, as discussed in section 3.1. for insulin release; the production of hydrogen peroxide induces oxidative stress in tumors and can produce toxic

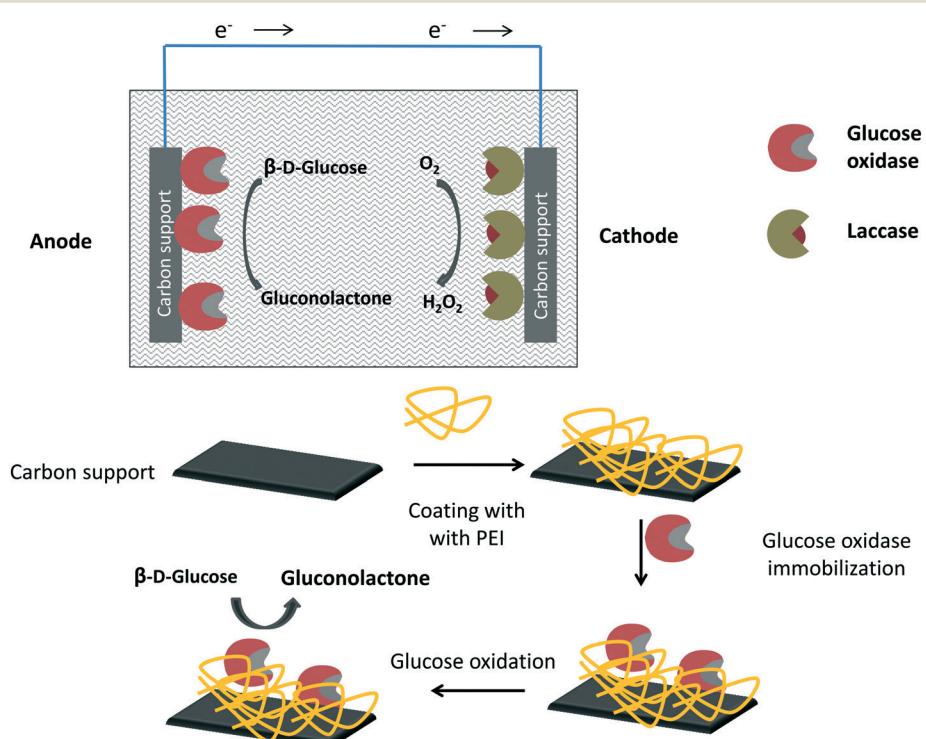


Fig. 16 Co-immobilization of glucose oxidase and laccase using carbon coated with polyethyleneimine as a support.



hydroxyl radicals that can kill tumor cells upon exposure to light irradiation or *via* the Fenton reaction.<sup>376</sup> Glucose oxidase can also be combined with hypoxia-activated prodrugs, Fenton or photosensitizer reagents, or other enzymes to generate multi-modal synergistic cancer therapies based on cancer oxidation therapy, hypoxia-activated therapy, starvation therapy, photodynamic therapy, and/or photothermal therapy.<sup>375</sup>

We will mention a few recent contributions in this regard. In the area of tumor biosensors, this technology is based on the fact that cancer cells undergo a transition from oxidative phosphorylation to anaerobic glycolytic metabolism, which provides proof of cancer progression. In an interesting study, nano-pipettes were developed to determine glucose concentrations in individual cells.<sup>377</sup> These devices were used to covalently immobilize glucose oxidase, followed by measuring the change in impedance generated by the decrease in the medium pH value. The nanopipettes could measure this parameter at different times in the cells, as this change did not affect their viability.<sup>377</sup>

In the area of cancer therapy, one example of drug-controlled release using glucose oxidase oxidation of metabolic glucose is the use of anti-PD-1 as a target molecule.<sup>378,379</sup> To achieve this goal, a microneedle was fabricated using hyaluronic acid and with pH-sensitive dextran nanoparticles that encapsulate anti-PD-1 and glucose oxidase.<sup>380</sup> When glucose oxidase converts glucose into D-gluconic acid and the pH decreases, the dextran nanoparticles dissociated and released anti-PD-1 more effectively than from a microneedle without this pH-triggered release or employing the free antibody, using B16F10 mouse melanoma as a model system. In another paper, glucose oxidase was immobilized on a polymer nano-gel, and the biocatalyst was employed for synergistic cancer-starving and oxidation therapy.<sup>381</sup> This immobilized biocatalyst showed high anti-melanoma efficacy without detectable systemic toxicity, whereas the free enzyme was nonfunctional and systemically toxic. In other research, glucose oxidase was trapped in hollow mesoporous organo-silica nanoparticles combined with L-Arg.<sup>382</sup> Hydrogen peroxide at acidic pH produces NO from Arg. In this way, this system starves the tumor by eliminating glucose in the tumor. On the other hand, the decrease in the pH and the presence of hydrogen peroxide produced a remarkable H<sub>2</sub>O<sub>2</sub>-NO cooperative anticancer effect with minimal adverse effects.<sup>382,383</sup>

In another approximation, glucose oxidase was immobilized on stealth liposomes to reduce oxygen and glucose availability for tumor growth. Intravenous injection permitted the effective tumor retention of these liposomes, and this exhausts the glucose and the oxygen inside the tumor (Fig. 10). The release of cytotoxic hydrogen peroxide contributes to the anticancer effect of this strategy. If this system is combined with stealth liposomes loaded with baxoxantrone dihydrochloride (a hypoxia-activated pro-anticancer drug),<sup>384-386</sup> synergistic inhibition of tumor growth is accomplished.

In a final example, glucose oxidase was immobilized on Fe<sub>3</sub>O<sub>4</sub> functionalized with polypyrrole to achieve photothermal-enhanced, tumor microenvironment-specific sequential nano-catalytic tumor therapy and diagnostic imaging-guided cancer therapy.<sup>387</sup> When the glucose oxidase consumed intra-tumoral glucose, the hydrogen peroxide concentration increased, and Fe<sub>3</sub>O<sub>4</sub> catalyzed the transformation of hydrogen peroxide into very toxic hydroxyl radicals that promote cancer-cell death. The high photothermal-conversion efficiency of the poly-pyrrole increased the local tumor temperature, improving the metal catalytic activity. All these synergistic processes promoted great anticancer effects with minimal side effects.<sup>387</sup>

### 11.8. Unexpected uses of glucose oxidase

Some uses of glucose oxidase are very different from the usual applications in food, medicinal or analytical applications. However, all utilize the consumption of oxygen, the properties of D-gluconic acid or hydrogen peroxide or the decrease in the pH promoted during the oxidation of D-glucose to D-gluconic acid. For example, glucose oxidase and catalase were co-immobilized on nano-porous SiO<sub>2</sub>, and the biocatalyst was utilized for the removal of oxygen dissolved in water in order to avoid boiler corrosion.<sup>388</sup> In another application, a glucose oxidase/catalase system using glucose as a substrate was employed to generate D-gluconic acid; this system was used to neutralize and precipitate hydrous tin oxide powders under mild conditions.<sup>389</sup> A high concentration of the enzyme was required to obtain full precipitation. The hydrous tin oxide, which had a large surface area, was obtained when a high concentration of enzymes was used as a solution. The precipitates were converted to tin oxide *via* calcination at temperatures >400 °C.<sup>389</sup>

One interesting use of glucose oxidase is its use in the decontamination of water using both D-gluconic acid and hydrogen peroxide features. The Fenton reaction is an oxidation technology utilized for the oxidation of pollutants.<sup>390-392</sup> Some researchers propose the use of glucose and glucose oxidase (both in free and immobilized forms) to generate on-site D-gluconic acid, which acts as a chelating agent, and hydrogen peroxide, which acts as an oxidant.<sup>393</sup> This enables the de-chlorination of 2,4,6-trichlorophenol under very mild conditions, first by fully transforming glucose in hydrogen peroxide and D-gluconic acid, then by performing the Fenton reaction.

## 12. Conclusion

The production of D-gluconic acid using glucose oxidase is a reaction that is receiving ongoing interest because of the many applications of this compound and the possibility of obtaining it from fully renewable sources. Moreover, this reaction is used as a model for many enzyme reaction design problems. It is a bi-substrate reaction (glucose and oxygen) and is a good model for oxygen diffusional limitation



problems. Therefore, many studies use this reaction to analyze the possibilities of addressing these limitations. Even more interestingly from a basic point of view, due to its side product (hydrogen peroxide), this system is adequate for studying the effects of the inactivation of the enzyme by this deleterious agent in different reactor operation models. One of the logical evolutions in the development of this reaction is the design, perhaps using directed evolution, of glucose oxidases with high stability in high concentrations of hydrogen peroxide. The current solution to this problem is the destruction of this deleterious reagent; among the different solutions, the preferred one is the use of catalase. Therefore, this reaction is one of the most studied enzymatic cascade reactions. As in this case, the critical point is to avoid the exposition of glucose oxidase to high concentrations of hydrogen peroxide; enzyme co-immobilization has been the preferred solution. However, in many papers, this advantage has not been examined. It is granted that enzyme co-immobilization must be the best solution while ignoring some of the problems that this co-immobilization may cause. Although many methods of catalase/glucose oxidase co-immobilization have been developed, the stabilities of the two immobilized enzymes have been analyzed in only a few, and no research has attempted to solve the problems derived from the co-immobilization of two enzymes with very different stabilities.

Glucose oxidase has also been co-immobilized with other enzymes, such as gluconolactonase; it has been utilized in many other enzymatic cascade reactions, in some instances involving even a half dozen enzymes, to achieve the one-pot transformation of polysaccharides to D-gluconic acid. In these reactions, the role of glucose oxidase/catalase has changed from simply providing D-gluconic acid to facilitating the purification of valuable saccharides by eliminating glucose and producing ionic compounds. Therefore, the production of D-gluconic acid using glucose oxidase is one of the successful examples involving a wide range of enzymatic cascade reactions, in some cases expanding the concept of combienzymes.<sup>394</sup> With the current focus on bio-refineries as a solution to environmental problems (involving lignocellulosic materials), the necessity for the chemical industry to use renewable sources to substitute current petroleum chemistry, and the green chemistry requirements arising from societal demand, the number of processes, in many cases cascade processes, where glucose oxidase may play relevant roles should even increase in the immediate future.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

We gratefully recognize the financial support from Ministerio de Ciencia e Innovación-Spanish Government and FEDER funds (project number CTQ2017-86170-R, RTI2018-095291-B-

100, MAT2017-87579-R) and Generalitat Valenciana (PROMETEO/2018/076). DC thank to Ministerio de Ciencia e Innovacion-Spanish Government by a FPI. PWT thanks to the Coordenação de Aperfeiçoamento de Pessoal de Nível Superior – Brasil (CAPES) – Finance Code 001.

## References

- 1 M. E. Corkins, S. Wilson, J.-C. Cocuron, A. P. Alonso and A. J. Bird, *J. Biol. Chem.*, 2017, **292**, 13823–13832.
- 2 B. C. Mulukutla, A. Yongky, T. Le, D. G. Mashek and W.-S. Hu, *Trends Biotechnol.*, 2016, **34**, 638–651.
- 3 E.-J. Kim, Y.-J. Cho, W.-H. Chung and J.-H. Roe, *FEBS J.*, 2020, **287**, 878–896.
- 4 X. Chen, K. Schreiber, J. Appel, A. Makowka, B. Fähnrich, M. Roettger, M. R. Hajirezaei, F. D. Sönnichsen, P. Schönheit, W. F. Martin and K. Gutekunst, *Proc. Natl. Acad. Sci. U. S. A.*, 2016, **113**, 5441–5446.
- 5 N. Rohatgi, T. K. Nielsen, S. P. Bjørn, I. Axelsson, G. Paglia, B. G. Voldborg, B. O. Palsson and Ó. Rolfsson, *PLoS One*, 2014, **9**, e98760.
- 6 S. Ramachandran, S. Nair, C. Larroche and A. Pandey, in *Current Developments in Biotechnology and Bioengineering*, ed. A. Pandey, N. Negi and C. R. Soccol, Elsevier, Amsterdam, 2017, pp. 577–599.
- 7 P. Pal, R. Kumar and S. Banerjee, *Chem. Eng. Process.*, 2016, **104**, 160–171.
- 8 S. Ramachandran, P. Fontanille, A. Pandey and C. Larroche, *Food Technol. Biotechnol.*, 2006, **44**(2), 185–195.
- 9 H. Hustedt, H.-J. Haberstroh and E. Schinzig, in *ULLMANN'S Encyclopedia of Industrial Chemistry*, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim, 2000, pp. 37–44.
- 10 R. O. Marshall, E. R. Kooi and G. M. Moffett, *Science*, 1957, **125**, 648–649.
- 11 A. M. Cafete-Rodríguez, I. M. Santos-Dueñas, J. E. Jiménez-Hornero, A. Ehrenreich, W. Liebl and I. García-García, *Process Biochem.*, 2016, **51**, 1891–1903.
- 12 R. H. Blom, V. F. Pfeifer, A. J. Moyer, D. H. TraufRer, H. F. Conway, C. K. Crocker, R. E. Farison and D. V. Hannibal, *Ind. Eng. Chem.*, 1952, **44**, 435–440.
- 13 J. Ziffer, A. S. Gaffuey, S. Rothenberg and T. J. Cairney, *British Pat.*, 1249347, 1971.
- 14 V. Leskovac, S. Trivić, G. Wohlfahrt, J. Kandrač and D. Peričin, *Int. J. Biochem. Cell Biol.*, 2005, **37**, 731–750.
- 15 S. B. Bankar, M. V. Bule, R. S. Singhal and L. Ananthanarayan, *Biotechnol. Adv.*, 2009, **27**, 489–501.
- 16 G. Wohlfahrt, S. Witt, J. Hendle, D. Schomburg, H. M. Kalisz and H. J. Hecht, *Acta Crystallogr., Sect. D: Biol. Crystallogr.*, 1999, **55**, 969–977.
- 17 P.-R. Kommoju, Z. Chen, R. C. Bruckner, F. S. Mathews and M. S. Jorns, *Biochemistry*, 2011, **50**, 5521–5534.
- 18 H. J. Hecht, H. M. Kalisz, J. Hendle, R. D. Schmid and D. Schomburg, *J. Mol. Biol.*, 1993, **229**, 153–172.
- 19 M. K. Dubey, A. Zehra, M. Aamir, M. Meena, L. Ahirwal, S. Singh, S. Shukla, R. S. Upadhyay, R. Bueno-Mari and V. K. Bajpai, *Front Microbiol.*, 2017, **8**, 1–22.



20 C. Cui, H. Chen, B. Chen and T. Tan, *Appl. Biochem. Biotechnol.*, 2017, **181**, 526–535.

21 A. C. O. Mafra, F. F. Furlan, A. C. Badino and P. W. Tardioli, *Bioprocess Biosyst. Eng.*, 2015, **38**, 671–680.

22 A. C. O. Mafra, L. G. Ulrich, J. F. Kornecki, R. Fernandez-Lafuente, P. W. Tardioli and M. P. A. Ribeiro, *Catalysts*, 2019, **9**, 657.

23 X. Shen, M. Yang, C. Cui and H. Cao, *Colloids Surf., A*, 2019, **568**, 411–418.

24 R. Jaquish, A. K. Reilly, B. P. Lawson, E. Golikova, A. M. Sulman, B. D. Stein, N. V. Lakina, O. P. Tkachenko, E. M. Sulman, V. G. Matveeva and L. M. Bronstein, *Int. J. Biol. Macromol.*, 2018, **120**, 896–905.

25 D. Pečar, D. Vasić-Rački and A. Vrsalović Presečki, *Chem. Biochem. Eng. Q.*, 2018, **32**, 511–522.

26 E. J. Tomotani and M. Vitolo, *Enzyme Microb. Technol.*, 2007, **40**, 1020–1025.

27 T. Godjevargova, R. Dayal and S. Turmanova, *Macromol. Biosci.*, 2004, **4**, 950–956.

28 G. Richter and H. Heinecker, *Starch/Staerke*, 1979, **31**, 418–422.

29 M. Kriaa, I. Hammami, M. Sahnoun, M. C. Azebou, M. A. Triki and R. Kammoun, *Bioprocess Biosyst. Eng.*, 2015, **38**, 2155–2166.

30 M. Bucekova, I. Valachova, L. Kohutova, E. Prochazka, J. Klaudiny and J. Majtan, *Naturwissenschaften*, 2014, **101**, 661–670.

31 C. M. Wong, K. H. Wong and X. D. Chen, *Appl. Microbiol. Biotechnol.*, 2008, **78**, 927–938.

32 A. I. Schepartz and M. H. Subers, *Biochim. Biophys. Acta, Spec. Sect. Enzymol. Subj.*, 1964, **85**, 228–237.

33 B. A. Hassan, M. A. Jebor and Z. M. Ali, *Int. J. Pharm. Qual. Assur.*, 2018, **9**, 273–281.

34 R. Mikhailova, A. G. Lobanok, Z. F. Shishko and M. I. Yasenko, *Mikol. Fitopatol.*, 1998, **32**, 60–61.

35 M. Petruccioli, M. Ceccarelli and F. Federici, *World J. Microbiol. Biotechnol.*, 1993, **9**, 77–79.

36 T. Nakamatsu, T. Akamatsu, R. Miyajima and I. Shioi, *Agric. Biol. Chem.*, 1975, **39**, 1803–1811.

37 K. Jagathy, K. Kalpana and S. Rajeshkumar, *Res. J. Pharm. Technol.*, 2017, **10**, 1924.

38 T. Konishi, T. Aoshima, F. Mizuhashi, S. S. H. Choi and A. Roberts, *Regul. Toxicol. Pharmacol.*, 2013, **66**, 13–23.

39 R. G. Bodade, C. N. Khobragade and S. Arfeen, *Eng. Life Sci.*, 2010, **10**, 35–39.

40 H. N. Bhatti and N. Saleem, *Food Technol. Biotechnol.*, 2009, **47**, 331–335.

41 S. Sabir, H. N. Bhatti, M. A. Zia and M. A. Sheikh, *Food Technol. Biotechnol.*, 2007, **45**, 443–446.

42 T. V. Semashko, R. V. Mikhailova and A. G. Lobanok, *Microbiology*, 2004, **73**, 286–291.

43 Z. I. Pavlovskaya, R. Mikhailova and I. V. Moroz, *Mikol. Fitopatol.*, 2004, **38**, 77–82.

44 S. Manivannan and K. Kathiresan, *Res. J. Microbiol.*, 2007, **2**, 294–298.

45 M. Petruccioli, P. Piccioni and F. Federici, *Enzyme Microb. Technol.*, 1997, **21**, 458–462.

46 T. Tu, Y. Wang, H. Huang, Y. Wang, X. Jiang, Z. Wang, B. Yao and H. Luo, *Food Chem.*, 2019, **281**, 163–170.

47 I. Haq, A. Nawaz and A. Rehman, *Pak. J. Bot.*, 2015, **47**, 329–332.

48 A. A. Khattab and W. A. Bazaraa, *J. Ind. Microbiol. Biotechnol.*, 2005, **32**, 289–294.

49 R. P. Kona, N. Qureshi and J. S. Pai, *Bioresour. Technol.*, 2001, **78**, 123–126.

50 A. Rothberg, J. Weegar, R. von Schalien, K. Fagervik, M. Rydström and K. Lind, *Bioprocess Eng.*, 1999, **21**, 307–312.

51 T.-H. Li and T.-L. Chen, *J. Ferment. Bioeng.*, 1994, **78**, 298–303.

52 F. B. Cor Witteveen, P. van de Vondervoort, K. Swart and J. Visser, *Appl. Microbiol. Biotechnol.*, 1990, **33**, 683–686.

53 J. Markwell, L. G. Frakes, E. C. Brott, J. Osterman and F. W. Wagner, *Appl. Microbiol. Biotechnol.*, 1989, **30**, 166–169.

54 Z. Fencl and M. Novák, *Folia Microbiol.*, 1969, **14**, 314–321.

55 S. Nakamura and Y. Ogura, *J. Biochem.*, 1968, **63**, 308–316.

56 J. Pásková and V. Munk, *Folia Microbiol.*, 1963, **8**, 215–220.

57 V. Munk, J. Pásková and J. Hanus, *Folia Microbiol.*, 1963, **8**, 203–214.

58 G. Kovačević, M. Blažić, B. Draganić, R. Ostafe, M. Gavrović-Jankulović, R. Fischer and R. Prodanović, *Mol. Biotechnol.*, 2014, **56**, 305–311.

59 M. A. Farid, E. A. Ghoneimy, M. A. El-Khawaga, A. Negm-Eldein and G. E. A. Awad, *Ann. Microbiol.*, 2013, **63**, 523–531.

60 R. Samreen, A. Z. Muhammad, A. S. Munir and I. Tehreema, *Afr. J. Biotechnol.*, 2011, **10**, 14522–14533.

61 S. Khurshid, M. A. Kashmiri, Z. Quershi and W. Ahmad, *Afr. J. Biotechnol.*, 2011, **10**, 1674–1678.

62 C. Yang, C. Li and T. Tan, *Beijing Huagong Daxue Xuebao, Ziran Kexueban*, 2011, **38**, 97–100.

63 S. B. Bankar, M. V. Bule, R. S. Singhal and L. Ananthanarayan, *Food Bioprocess Technol.*, 2009, **2**, 344–352.

64 M. H. Sarrafzadeh and A. R. Jafari, *Pak. J. Biotechnol.*, 2008, **5**, 11–20.

65 O. V. Singh, *Appl. Biochem. Biotechnol.*, 2006, **135**, 43–57.

66 J. Ge, X. Jiang, W. Liu, Y. Wang, H. Huang, Y. Bai, X. Su, B. Yao and H. Luo, *Food Chem.*, 2020, **310**, 125970.

67 A. Bredenkamp, H. Velankar, W. H. van Zyl and J. F. Görgens, *Yeast*, 2010, **27**, 849–860.

68 A. A. N. Gunny, D. Arbain and L. Sithamparam, *Pak. J. Biol. Sci.*, 2013, **16**, 960–964.

69 V. Silano, C. Bolognesi, L. Castle, K. Chipman, J.-P. Cravedi, P. Fowler, R. Franz, K. Grob, R. Gürtler, T. Husøy, S. Kärenlampi, W. Mennes, M. R. Milana, K. Pfaff, G. Riviere, J. Srinivasan, M. D. F. Tavares Poças, C. Tlustos, D. Wölfle, H. Zorn, A. Chesson, B. Glandorf, L. Herman, K.-D. Jany, F. Marcon, A. Penninks, A. Smith, H. van Loveren, D. Želježić, M. Andryszkiewicz, Y. Liu, A. Rossi and K.-H. Engel, *EFSA J.*, 2018, **16**(7), e05319.

70 L. Yang, M. Lübeck and P. S. Lübeck, *AMB Express*, 2014, **4**, 54.

71 R. Luque, M. Orejas, N. I. Perotti, D. Ramón and M. E. Lucca, *J. Appl. Microbiol.*, 2004, **97**, 332–337.



72 H. Xiao-Yue, M. Ri-Jian, X. De-Feng, Y. Ki-Ying, S. Li-Jun and W. Ya-Ling, *Zhongguo Shengwu Zhipinxue Zazhi*, 2018, **31**, 1268–1273.

73 O. E. Bankefa, M. Wang, T. Zhu and Y. Li, *Bioresour. Bioprocess.*, 2018, **5**, 25.

74 X. Liu, J. Zhang, J. Chen and G. Du, *Shipin Yu Shengwu Jishu Xuebao*, 2018, **37**, 1233–1241.

75 F. Khadivi Derakshan, F. Darvishi, M. Dezfulian and C. Madzak, *Mol. Biotechnol.*, 2017, **59**, 307–314.

76 M. Zakhartsev and C. Momeu, *J. Chromatogr., B*, 2007, **858**, 151–158.

77 K. Kojima, W. Tsugawa and K. Sode, *Biochem. Biophys. Res. Commun.*, 2001, **282**, 21–27.

78 A. Kapat, J.-K. Jung and Y.-H. Park, *Biotechnol. Lett.*, 1998, **20**, 319–323.

79 A. Kapat, J.-K. Jung and Y.-H. Park, *Biotechnol. Lett.*, 1998, **20**, 683–686.

80 K. R. Frederick, J. Tung, R. S. Emerick, F. R. Masiarz, S. H. Chamberlain, A. Vasavada, S. Rosenberg, S. Chakraborty, L. M. Schopfer and V. Massey, *J. Biol. Chem.*, 1990, **265**(7), 3793–3802.

81 Y. Shen, L. Gu, J. Zhang, J. Chen and G. Du, *Shengwu Gongcheng Xuebao*, 2013, **29**, 927–936.

82 F. Darvishi, A. Zarei and C. Madzak, *World J. Microbiol. Biotechnol.*, 2018, **34**, 128.

83 I. Haq, A. Nawaz, H. Mukhtar, Z. Mansoor, M. Riaz, M. Ahmed and S. Ameer, *Pak. J. Bot.*, 2014, **46**, 1109–1114.

84 H. M. Kalisz, J. Hendle and R. D. Schmid, *Appl. Microbiol. Biotechnol.*, 1997, **47**, 502–507.

85 J. H. Pazur, K. Kleppe and A. Cepure, *Arch. Biochem. Biophys.*, 1965, **111**, 351–357.

86 J. J. O'Malley and J. L. Weaver, *Biochemistry*, 1972, **11**, 3527–3532.

87 H. Tsuge, O. Natsuaki and K. Ohashi, *J. Biochem.*, 1975, **78**, 835–843.

88 J. Bao, K. Furumoto, M. Yoshimoto, K. Fukunaga and K. Nakao, *Biochem. Eng. J.*, 2003, **13**, 69–72.

89 X. Huang, M. Cao and H. Zhao, *Curr. Opin. Chem. Biol.*, 2020, **55**, 161–170.

90 A. Fryszkowska and P. N. Devine, *Curr. Opin. Chem. Biol.*, 2020, **55**, 151–160.

91 J. M. Woodley, *Curr. Opin. Green Sustain. Chem.*, 2020, **21**, 22–26.

92 D. J. Pollard and J. M. Woodley, *Trends Biotechnol.*, 2007, **25**, 66–73.

93 A. Schmid, J. S. Dordick, B. Hauer, A. Kiener, M. Wubbolts and B. Witholt, *Nature*, 2001, **409**, 258–268.

94 H. E. Schoemaker, *Science*, 2003, **299**, 1694–1697.

95 P. Lorenz, K. Liebeton, F. Niehaus and J. Eck, *Curr. Opin. Biotechnol.*, 2002, **13**, 572–577.

96 J. M. Almeida, R. C. Alnoch, E. M. Souza, D. A. Mitchell and N. Krieger, *Biochim. Biophys. Acta, Proteins Proteomics*, 2020, **1868**, 140320.

97 I. Castilla, D. Woods, F. Reen and F. O'Gara, *Mar. Drugs*, 2018, **16**, 227.

98 L. Fernández-Arrojo, M.-E. Guazzaroni, N. López-Cortés, A. Beloqui and M. Ferrer, *Curr. Opin. Biotechnol.*, 2010, **21**, 725–733.

99 U. T. Bornscheuer and M. Pohl, *Curr. Opin. Chem. Biol.*, 2001, **5**, 137–143.

100 A. Currin, N. Swainston, P. J. Day and D. B. Kell, *Chem. Soc. Rev.*, 2015, **44**, 1172–1239.

101 C. A. Denard, H. Ren and H. Zhao, *Curr. Opin. Chem. Biol.*, 2015, **25**, 55–64.

102 B. G. Davis, *Curr. Opin. Biotechnol.*, 2003, **14**, 379–386.

103 O. Barbosa, C. Ortiz, Á. Berenguer-Murcia, R. Torres, R. C. Rodrigues and R. Fernandez-Lafuente, *Biotechnol. Adv.*, 2015, **33**, 435–456.

104 C. Mateo, J. M. Palomo, G. Fernandez-Lorente, J. M. Guisan and R. Fernandez-Lafuente, *Enzyme Microb. Technol.*, 2007, **40**, 1451–1463.

105 R. C. Rodrigues, C. Ortiz, Á. Berenguer-Murcia, R. Torres and R. Fernández-Lafuente, *Chem. Soc. Rev.*, 2013, **42**, 6290–6307.

106 C. Garcia-Galan, Á. Berenguer-Murcia, R. Fernandez-Lafuente and R. C. Rodrigues, *Adv. Synth. Catal.*, 2011, **353**, 2885–2904.

107 P. V. Iyer and L. Ananthanarayan, *Process Biochem.*, 2008, **43**, 1019–1032.

108 I. Eş, J. D. G. Vieira and A. C. Amaral, *Appl. Microbiol. Biotechnol.*, 2015, **99**, 2065–2082.

109 S. Alonso, G. Santiago, I. Cea-Rama, L. Fernandez-Lopez, C. Coscolín, J. Modregger, A. K. Ressmann, M. Martínez-Martínez, H. Marrero, R. Bargiela, M. Pita, J. L. Gonzalez-Alfonso, M. L. Briand, D. Rojo, C. Barbas, F. J. Plou, P. N. Golyshin, P. Shahgaldian, J. Sanz-Aparicio, V. Guallar and M. Ferrer, *Nat. Catal.*, 2020, **3**, 319–328.

110 R. A. Sheldon and S. van Pelt, *Chem. Soc. Rev.*, 2013, **42**, 6223–6235.

111 R. Di Cosimo, J. Mc Auliffe, A. J. Poulose and G. Bohlmann, *Chem. Soc. Rev.*, 2013, **42**, 6437–6474.

112 L. Dal Magro, J. F. Kornecki, M. P. Klein, R. C. Rodrigues and R. Fernandez-Lafuente, *Int. J. Biol. Macromol.*, 2019, **138**, 234–243.

113 L. Dal Magro, J. F. Kornecki, M. P. Klein, R. C. Rodrigues and R. Fernandez-Lafuente, *Enzyme Microb. Technol.*, 2020, **132**, 109397.

114 J. M. Harris, C. Reyes and G. P. Lopez, *J. Diabetes Sci. Technol.*, 2013, **7**, 1030–1038.

115 J. H. T. Luong, J. D. Glennon, A. Gedanken and S. K. Vashist, *Microchim. Acta*, 2017, **184**, 369–388.

116 Q. Husain, *Biointerface Res. Appl. Chem.*, 2018, **8**, 3060–3074.

117 L. V. Danyleyko, O. N. Schuvailo, V. M. Arkhypova, A. P. Soldatkin and S. V. Dzyadevych, *Biopolym. Cell*, 2003, **19**, 76–80.

118 L. Betancor, F. López-Gallego, A. Hidalgo, N. Alonso-Morales, G. Dellamora-Ortiz, J. M. Guisán and R. Fernández-Lafuente, *J. Biotechnol.*, 2006, **121**, 284–289.

119 L. Caseli, D. S. dos Santos, M. Foschini, D. Gonçalves and O. N. Oliveira, *Mater. Sci. Eng., C*, 2007, **27**, 1108–1110.

120 S. Datta, C. Cecil and D. Bhattacharyya, *Ind. Eng. Chem. Res.*, 2008, **47**, 4586–4597.

121 X. Yan, X. K. Xu and H.-F. Ji, *Anal. Chem.*, 2005, **77**, 6197–6204.



122 L.-Y. Chu, Y. Li, J.-H. Zhu, H.-D. Wang and Y.-J. Liang, *J. Controlled Release*, 2004, **97**, 43–53.

123 K. Zhang and X. Y. Wu, *J. Controlled Release*, 2002, **80**, 169–178.

124 T. Traitel, Y. Cohen and J. Kost, *Biomaterials*, 2000, **21**, 1679–1687.

125 T. A. Horbett, J. Kost and B. D. Ratner, Swelling behavior of glucose sensitive membranes, in *Polymers as Biomaterials*, ed. S. W. Shalaby, A. S. Hoffman, B. D. Ratner and T. A. Horbett, Springer USA, Boston, MA, 1984, pp. 193–207.

126 Y. Ito, M. Casolaro, K. Kono and Y. Imanishi, *J. Controlled Release*, 1989, **10**, 195–203.

127 R. Luo, H. Li and K. Y. Lam, *Biomaterials*, 2009, **30**, 690–700.

128 X. Yang and J.-C. Kim, *Int. J. Biol. Macromol.*, 2011, **48**, 661–666.

129 S. Il Kang and Y. H. Bae, *J. Controlled Release*, 2003, **86**, 115–121.

130 M. Sönmez, D. Ficai, A. Ficai, L. Alexandrescu, M. Georgescu, R. Trusca, D. Gurau, M. A. Titu and E. Andronescu, *Int. J. Pharm.*, 2018, **549**, 179–200.

131 M. Oroval, P. Díez, E. Aznar, C. Coll, M. D. Marcos, F. Sancenón, R. Villalonga and R. Martínez-Máñez, *Chem. – Eur. J.*, 2017, **23**, 1353–1360.

132 W. Zhao, H. Zhang, Q. He, Y. Li, J. Gu, L. Li, H. Li and J. Shi, *Chem. Commun.*, 2011, **47**, 9459–9461.

133 C. Li, X. Liu, Y. Liu, F. Huang, G. Wu, Y. Liu, Z. Zhang, Y. Ding, J. Lv, R. Ma, Y. An and L. Shi, *Nanoscale*, 2019, **11**, 9163–9175.

134 Y. Wu, H. Hu, J. Hu and S. Liu, *Macromol. Rapid Commun.*, 2012, **33**, 1852–1860.

135 S. Jamwal, B. Ram, S. Ranote, R. Dharela and G. S. Chauhan, *Int. J. Biol. Macromol.*, 2019, **123**, 968–978.

136 W.-H. Chen, G.-F. Luo, M. Vázquez-González, R. Cazelles, Y. Sohn, R. Nechushtai, Y. Mandel and I. Willner, *ACS Nano*, 2018, **12**, 7538–7545.

137 K. Ogawa, T. Nakajima-Kambe, T. Nakahara and E. Kokufuta, *Biomacromolecules*, 2002, **3**, 625–631.

138 K. Hernandez, A. Berenguer-Murcia, R. C. Rodrigues and R. Fernandez-Lafuente, *Curr. Org. Chem.*, 2012, **16**, 2652–2672.

139 G. De Faveri, G. Ilyashenko and M. Watkinson, *Chem. Soc. Rev.*, 2011, **40**, 1722–1760.

140 A. Podgoršek, M. Zupan and J. Iskra, *Angew. Chem., Int. Ed.*, 2009, **48**, 8424–8450.

141 S. Schrader and E. V. Dehmlow, *Org. Prep. Proced. Int.*, 2000, **32**, 123–152.

142 D. M. Vriezema, P. M. L. Garcia, N. Sancho Oltra, N. S. Hatzakis, S. M. Kuiper, R. J. M. Nolte, A. E. Rowan and J. C. M. van Hest, *Angew. Chem., Int. Ed.*, 2007, **46**, 7378–7382.

143 S. F. M. van Dongen, M. Nallani, J. J. L. M. Cornelissen, R. J. M. Nolte and J. C. M. van Hest, *Chem. – Eur. J.*, 2009, **15**, 1107–1114.

144 E. R. Stadtman and R. L. Levine, *Amino Acids*, 2003, **25**, 207–218.

145 S. P. Wolff, A. Garner and R. T. Dean, *Trends Biochem. Sci.*, 1986, **11**, 27–31.

146 S. K. Grandhee and V. M. Monnier, *J. Biol. Chem.*, 1991, **266**, 11649–11653.

147 T. G. Huggins, M. C. Wells-Knecht, N. A. Detorie, J. W. Baynes and S. R. Thorpe, *J. Biol. Chem.*, 1993, **268**, 12341–12347.

148 J. W. Heinecke, W. Li, H. L. Daehnke and J. A. Goldstein, *J. Biol. Chem.*, 1993, **268**, 4069–4077.

149 R. C. Armstrong and A. J. Swallow, *Radiat. Res.*, 1969, **40**, 563–579.

150 R. V. Winchester and K. R. Lynn, *Int. J. Radiat. Biol. Relat. Stud. Phys., Chem. Med.*, 1970, **17**, 541–548.

151 K. Kikugawa, T. Kato and Y. Okamoto, *Free Radical Biol. Med.*, 1994, **16**, 373–382.

152 R. L. Levine, L. Mosoni, B. S. Berlett and E. R. Stadtman, *Proc. Natl. Acad. Sci. U. S. A.*, 1996, **93**, 15036–15040.

153 R. L. Levine, J. Moskovitz and E. R. Stadtman, *IUBMB Life*, 2000, **50**, 301–307.

154 W. Vogt, *Free Radical Biol. Med.*, 1995, **18**, 93–105.

155 V. Y. Reddy, P. E. Desrochers, S. V. Pizzo, S. L. Gonias, J. A. Sahakian, R. L. Levine and S. J. Weise, *J. Biol. Chem.*, 1994, **269**, 4683–4691.

156 M. A. Ciorba, S. H. Heinemann, H. Weissbach, N. Brot and T. Hoshi, *Proc. Natl. Acad. Sci. U. S. A.*, 1997, **94**, 9932–9937.

157 M. A. Smith, L. M. Sayre, V. E. Anderson, P. L. R. Harris, M. F. Beal, N. Kowall and G. Perry, *J. Histochem. Cytochem.*, 1998, **46**, 731–735.

158 C. E. Robinson, A. Keshavarzian, D. S. Pasco, T. O. Frommel, D. H. Winship and E. W. Holmes, *Anal. Biochem.*, 1999, **266**, 48–57.

159 Z. Maskos, J. D. Rush and W. H. Koppenol, *Arch. Biochem. Biophys.*, 1992, **296**, 521–529.

160 M. C. Wells-Knecht, T. G. Huggins, D. G. Dyer, S. R. Thorpe and J. W. Baynes, *J. Biol. Chem.*, 1993, **268**, 12348–12352.

161 I. Balakrishnan and M. P. Reddy, *J. Phys. Chem.*, 1970, **74**, 850–855.

162 K. J. Davies, M. E. Delsignore and S. W. Lin, *J. Biol. Chem.*, 1987, **262**, 9902–9907.

163 R. T. Dean, S. Gieseg and M. J. Davies, *Trends Biochem. Sci.*, 1993, **18**, 437–441.

164 S. Proteasome, C. Giulivisq, K. J. A. Daviesti, C. Giulivi and K. J. Davies, *J. Biol. Chem.*, 1993, **268**, 8752–8759.

165 C. Taggart, D. Cervantes-Laurean, G. Kim, N. G. McElvaney, N. Wehr, J. Moss and R. L. Levine, *J. Biol. Chem.*, 2000, **275**, 27258–27265.

166 B. Nidetzky, *Biochem. Soc. Trans.*, 2007, **35**, 1588–1592.

167 E. R. Stadtman, B. S. Berlett and P. B. Chock, *Proc. Natl. Acad. Sci. U. S. A.*, 1990, **87**, 384–388.

168 J. M. Farber and R. L. Levine, *J. Biol. Chem.*, 1986, **261**, 4574–4578.

169 I. Climent, L. Tsai and R. L. Levine, *Anal. Biochem.*, 1989, **182**, 226–232.

170 J. A. Sahakian, L. I. Szweda, B. Friguet, K. Kitani and R. L. Levine, *Arch. Biochem. Biophys.*, 1995, **318**, 411–417.

171 S. P. Fernandes, R. Dringen, A. Lawen and S. R. Robinson, *Neurosci. Lett.*, 2011, **490**, 27–30.

172 W. M. Garrison, *Chem. Rev.*, 1987, **87**, 381–398.



173 S. S. Ju, L. L. Lin, H. R. Chien and W. H. Hsu, *FEMS Microbiol. Lett.*, 2000, **186**, 215–219.

174 C. Li, S. Sun, D. Park, H. O. Jeong, H. Y. Chung, X.-X. Liu and H.-M. Zhou, *Int. J. Biol. Macromol.*, 2011, **49**, 910–916.

175 H. Zhou, H. Singh, Z. D. Parsons, S. M. Lewis, S. Bhattacharya, D. R. Seiner, J. N. LaButti, T. J. Reilly, J. J. Tanner and K. S. Gates, *J. Am. Chem. Soc.*, 2011, **133**, 15803–15805.

176 J. A. Rosas-Rodríguez and E. M. Valenzuela-Soto, *Chem.-Biol. Interact.*, 2011, **191**, 159–164.

177 A. Slavica, I. Dib and B. Nidetzky, *Appl. Environ. Microbiol.*, 2005, **71**, 8061–8068.

178 R. L. Levine, *J. Biol. Chem.*, 1983, **258**, 11828–11833.

179 A. J. Rivett, J. E. Roseman, C. N. Oliver, R. L. Levine and E. R. Stadtman, *Prog. Clin. Biol. Res.*, 1985, **180**, 317–328.

180 L. Fucci, C. N. Oliver, M. J. Coon and E. R. Stadtman, *Proc. Natl. Acad. Sci. U. S. A.*, 1983, **80**, 1521–1525.

181 H. Schuessler and K. Schilling, *Int. J. Radiat. Biol. Relat. Stud. Phys., Chem. Med.*, 1984, **45**, 267–281.

182 K. Uchida, Y. Kato and S. Kawakishi, *Biochem. Biophys. Res. Commun.*, 1990, **169**, 265–271.

183 J. Q. Zhou and A. Gafni, *J. Gerontol.*, 1991, **46**, B217–B221.

184 A. E. Brodie and D. J. Reed, *Arch. Biochem. Biophys.*, 1990, **276**, 212–218.

185 R. Takahashi and S. Goto, *Arch. Biochem. Biophys.*, 1990, **277**, 228–233.

186 N. Verzijl, J. Degroot, E. Oldehinkel, R. A. Bank, S. R. Thorpe, J. W. Baynes, M. T. Bayliss, J. W. J. Bijlsma, F. P. J. G. Lafeber and J. M. Tekoppele, *Biochem. J.*, 2000, **350**, 381–387.

187 K. J. Wells-Knecht, D. V. Zyzak, J. E. Litchfield, S. R. Thorpe and J. W. Baynes, *Biochemistry*, 1995, **34**, 3702–3709.

188 K. Uchida and E. R. Stadtman, *J. Biol. Chem.*, 1993, **268**, 6388–6393.

189 B. Friguet, E. R. Stadtman and L. I. Szweda, *J. Biol. Chem.*, 1994, **269**, 21639–21643.

190 D. P. H. Hsieh, R. S. Silver and R. I. Mateles, *Biotechnol. Bioeng.*, 1969, **11**, 1–18.

191 C. Bourdillon, R. Lortie and J. M. Laval, *Biotechnol. Bioeng.*, 1988, **31**, 553–558.

192 E. J. Tomotani, L. C. M. das Neves and M. Vitolo, *Appl. Biochem. Biotechnol.*, 2005, **121**, 149–162.

193 S. Illner, C. Hofmann, P. Löb and U. Kragl, *ChemCatChem*, 2014, **6**, 1748–1754.

194 S. Wang, P. Su, H. E and Y. Yang, *Anal. Biochem.*, 2010, **405**, 230–235.

195 J. Liu and Z. Cui, *J. Membr. Sci.*, 2007, **302**, 180–187.

196 I. Ullah, M. Sirajuddin, M. Khan, A. Shah and A. Badshah, *J. Chem. Soc. Pak.*, 2013, **35**, 775–782.

197 S. Otokesh, E. Kolvari, A. Amoozadeh and N. Koukabi, *RSC Adv.*, 2015, **5**, 53749–53756.

198 J. Mlochowski and H. Wojtowicz-Mlochowska, *Mini-Rev. Org. Chem.*, 2017, **13**, 473–487.

199 K. Nakao, T. Harada, K. Furumoto, A. Kiefner and M. Popovic, *Can. J. Chem. Eng.*, 1999, **77**, 816–825.

200 K. Nakao, A. Kiefner, K. Furumoto and T. Harada, *Chem. Eng. Sci.*, 1997, **52**, 4127–4133.

201 X. Zhang, N. Xu, J. Li, Z. Ma, L. Wei, Q. Liu and J. Liu, *Enzyme Microb. Technol.*, 2020, **136**, 109530.

202 J.-W. Song, J.-H. Seo, D.-K. Oh, U. T. Bornscheuer and J.-B. Park, *Catal. Sci. Technol.*, 2020, **10**, 46–64.

203 W. A. Duetz, J. B. Van Beilen and B. Witholt, *Curr. Opin. Biotechnol.*, 2001, **12**, 419–425.

204 R. León, P. Fernandes, H. M. Pinheiro and J. M. S. Cabral, *Enzyme Microb. Technol.*, 1998, **23**, 483–500.

205 W. Hartmeier and T. Döppner, *Biotechnol. Lett.*, 1983, **5**, 743–748.

206 J. Tramper, K. C. A. M. Luyben and W. J. J. van den Tweel, *Eur. J. Appl. Microbiol. Biotechnol.*, 1983, **17**, 13–18.

207 M. Traeger, G. N. Qazi, U. Onken and C. L. Chopra, *J. Chem. Technol. Biotechnol.*, 1991, **50**, 1–11.

208 M. Träger, G. N. Qazi, R. Buse and U. Onken, *J. Ferment. Bioeng.*, 1992, **74**, 274–281.

209 M. Petruccioli, P. Piccioni, M. Fenice and F. Federici, *Biotechnol. Lett.*, 1994, **16**, 939–942.

210 C. Dowdells, R. L. Jones, M. Matthey, M. Benčina, M. Legiša and D. M. Mousdale, *Lett. Appl. Microbiol.*, 2010, **51**, 252–257.

211 M. Blazic, G. Kovacevic, O. Prodanovic, R. Ostafe, M. Gavrovic-Jankulovic, R. Fischer and R. Prodanovic, *Protein Expression Purif.*, 2013, **89**, 175–180.

212 M. Číp, L. Schreiberová and I. Schreiber, *Russ. J. Phys. Chem. A*, 2011, **85**, 2322–2326.

213 I. Schreiber, Y.-F. Hung and J. Ross, *J. Phys. Chem.*, 1996, **100**, 8556–8566.

214 S. Sasaki, T. Uchida, D. Nakano and T. Hidemitsu, *Electroanalysis*, 2004, **16**, 1598–1602.

215 E. T. Hwang and S. Lee, *ACS Catal.*, 2019, **9**, 4402–4425.

216 O. Idan and H. Hess, *Curr. Opin. Biotechnol.*, 2013, **24**, 606–611.

217 F. Jia, B. Narasimhan and S. Mallapragada, *Biotechnol. Bioeng.*, 2014, **111**, 209–222.

218 F. Kazenwadel, M. Franzreb and B. E. Rapp, *Anal. Methods*, 2015, **7**, 4030–4037.

219 S. Ren, C. Li, X. Jiao, S. Jia, Y. Jiang, M. Bilal and J. Cui, *Chem. Eng. J.*, 2019, **373**, 1254–1278.

220 J. Wang and G. Zhang, *Shengwu Gongcheng Xuebao*, 2015, **31**, 469–480.

221 Y. Zhang and H. Hess, *ACS Catal.*, 2017, **7**, 6018–6027.

222 S. Arana-Peña, D. Carballares, R. Morellon-Sterling, Á. Berenguer-Murcia, A. R. Alcántara, R. C. Rodrigues and R. Fernandez-Lafuente, *Biotechnol. Adv.*, DOI: 10.1016/j.biotechadv.2020.107584, in press.

223 S. Butò, L. Pollegioni, L. D'Angiuro and M. S. Pilone, *Biotechnol. Bioeng.*, 1994, **44**, 1288–1294.

224 A. Chmura, S. Rustler, M. Paravidino, F. Van Rantwijk, A. Stoltz and R. A. Sheldon, *Tetrahedron: Asymmetry*, 2013, **24**, 1225–1232.

225 R. Fernández-Lafuente, V. Rodriguez and J. M. Guisán, *Enzyme Microb. Technol.*, 1998, **23**, 28–33.

226 A. Lopalco and V. J. Stella, *J. Pharm. Sci.*, 2016, **105**, 2879–2885.

227 F. Lopez-Gallego, L. Betencor, A. Hidalgo, C. Mateo, R. Fernandez-Lafuente and J. M. Guisan, *Adv. Synth. Catal.*, 2005, **347**, 1804–1810.



228 E.-M. Trost and L. Fischer, *J. Mol. Catal. B: Enzym.*, 2002, **19–20**, 189–195.

229 R. Upadhyay, H. Nagajyothi and S. G. Bhat, *Process Biochem.*, 1999, **35**, 7–13.

230 G. Volpato, R. Rodrigues and R. Fernandez-Lafuente, *Curr. Med. Chem.*, 2010, **17**, 3855–3873.

231 A. H. Orrego, F. López-Gallego, A. Espaillat, F. Cava, J. M. Guisan and J. Rocha-Martin, *ChemCatChem*, 2018, **10**, 3002–3011.

232 F. van Rantwijk, C. Mateo, A. Chmura, B. C. M. Fernandes and R. A. Sheldon, in *Modern Biocatalysis*, ed. W.-D. Fessner and T. Anthonsen, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim, Germany, 2009, pp. 261–272.

233 S. Velasco-Lozano, A. I. Benítez-Mateos and F. López-Gallego, *Angew. Chem., Int. Ed.*, 2017, **56**, 771–775.

234 S. Velasco-Lozano and F. López-Gallego, *Biocatal. Biotransform.*, 2018, **36**, 184–194.

235 A. I. Benítez-Mateos, M. L. Contente, S. Velasco-Lozano, F. Paradisi and F. López-Gallego, *ACS Sustainable Chem. Eng.*, 2018, **6**, 13151–13159.

236 A. I. Benítez-Mateos, E. San Sebastian, N. Ríos-Lombardía, F. Morís, J. González-Sabín and F. López-Gallego, *Chem. – Eur. J.*, 2017, **23**, 16843–16852.

237 S. Peirce, J. J. Virgen-Ortíz, V. G. Tacias-Pascacio, N. Rueda, R. Bartolome-Cabrero, L. Fernandez-Lopez, M. E. Russo, A. Marzocchella and R. Fernandez-Lafuente, *RSC Adv.*, 2016, **6**, 61707–61715.

238 S. Arana-Peña, C. Mendez-Sánchez, N. S. Ríos, C. Ortiz, L. R. B. Gonçalves and R. Fernandez-Lafuente, *Int. J. Biol. Macromol.*, 2019, **131**, 989–997.

239 N. S. Ríos, S. Arana-Peña, C. Mendez-Sánchez, C. Ortiz, L. R. B. Gonçalves and R. Fernandez-Lafuente, *Catalysts*, 2019, **9**, 487.

240 L. Giorno and E. Drioli, *Trends Biotechnol.*, 2000, **18**, 339–349.

241 P. Jochems, Y. Satyawali, L. Diels and W. Dejonghe, *Green Chem.*, 2011, **13**, 1609–1623.

242 G. T. Vladisavljević, *Phys. Sci. Rev.*, 2019, **1**, 1–35.

243 E. Nagy, *Curr. Org. Chem.*, 2017, **21**, 1713–1724.

244 J. Pickova and O. Svabensky, *J. Food Sci.*, 1964, **29**, 400–406.

245 V. Linek, P. Beneš, J. Sinkule, O. Holeček and V. Malý, *Biotechnol. Bioeng.*, 1980, **22**, 2515–2527.

246 Z. Tao, R. A. Raffel, A.-K. Souid and J. Goodisman, *Biophys. J.*, 2009, **96**, 2977–2988.

247 S. Fukushima, A. Uyama and S. Katayama, *J. Chem. Eng. Jpn.*, 1978, **11**, 227–233.

248 M. Hashimoto, T. Tsukamoto, S. Morita and J. Okada, *Chem. Pharm. Bull.*, 1983, **31**, 1–11.

249 P. Beltrame, M. Comotti, C. Della Pina and M. Rossi, *J. Catal.*, 2004, **228**, 282–287.

250 T.-H. Li, Y.-F. Su, C.-H. Hong and T.-L. Chen, *J. Chem. Eng. Jpn.*, 1994, **27**, 205–210.

251 G. Maria, M. D. Ene and I. Jipa, *J. Mol. Catal. B: Enzym.*, 2012, **74**, 209–218.

252 M. T. Atallah and H. O. Hultin, *J. Food Sci.*, 1977, **42**, 7–10.

253 T. Godjenvargova, R. Dayal and I. Marinov, *J. Appl. Polym. Sci.*, 2004, **91**, 4057–4063.

254 J. C. Bouin, M. T. Atallah and H. O. Hultin, *Biochim. Biophys. Acta, Enzymol.*, 1976, **438**, 23–36.

255 S. Wang, M. Yoshimoto, K. Fukunaga and K. Nakao, *Biotechnol. Bioeng.*, 2003, **83**, 444–453.

256 M. Yoshimoto, S. Wang, K. Fukunaga, D. Fournier, P. Walde, R. Kuboi and K. Nakao, *Biotechnol. Bioeng.*, 2005, **90**, 231–238.

257 M. Yoshimoto, Y. Miyazaki, Y. Kudo, K. Fukunaga and K. Nakao, *Biotechnol. Prog.*, 2006, **22**, 704–709.

258 R. Fernandez-Lafuente, *Enzyme Microb. Technol.*, 2009, **45**, 405–418.

259 M. Yoshimoto, N. Takaki and M. Yamasaki, *Colloids Surf., B*, 2010, **79**, 403–408.

260 M. Yoshimoto, M. Inoue and N. Takaki, *J. Chem. Eng. Jpn.*, 2012, **45**, 645–650.

261 P. H. S. Tse, J. K. Leyboldt and D. A. Gough, *Biotechnol. Bioeng.*, 1987, **29**, 696–704.

262 P.-W. Li, R.-R. Li, D.-L. Liu, D.-D. Min, Q. Yang and Q. Hao, *Xiandai Shipin Keji*, 2013, **29**, 2180–2185+2130.

263 N. Rueda, J. C. S. dos Santos, C. Ortiz, R. Torres, O. Barbosa, R. C. Rodrigues, Á. Berenguer-Murcia and R. Fernandez-Lafuente, *Chem. Rec.*, 2016, **16**, 1436–1455.

264 C. Cui, Y. Fang, B. Chen and T. Tan, *Catal. Sci. Technol.*, 2019, **9**, 477–482.

265 S. T. Morthensen, A. S. Meyer, H. Jørgensen and M. Pinelo, *Biochem. Eng. J.*, 2017, **117**, 41–47.

266 R. A. Messing, *Biotechnol. Bioeng.*, 1974, **16**, 897–908.

267 P. E. Markey, P. F. Greenfield and J. R. Kittrell, *Biotechnol. Bioeng.*, 1975, **17**, 285–289.

268 P. F. Greenfield and R. L. Laurence, *J. Food Sci.*, 1975, **40**, 906–910.

269 J. C. Bouin, M. T. Atallah and H. O. Hultin, *Methods Enzymol.*, 1976, **44**, 478–488.

270 J. C. Boujn, P. H. Dudgeon and H. O. Hultin, *J. Food Sci.*, 1976, **41**, 886–890.

271 S. Akgöl, H. Yavuz, S. Şenel and A. Denizli, *React. Funct. Polym.*, 2003, **55**, 45–51.

272 G. Ozyilmaz and S. S. Tukel, *Appl. Biochem. Microbiol.*, 2007, **43**, 29–35.

273 S. S. T. G. Ozyilmaz, *J. Microbiol. Biotechnol.*, 2007, **17**, 960–967.

274 T. T. F. Cui, *Beijing Huagong Daxue Xuebao, Ziran Kexueban*, 2012, **39**, 63–67.

275 O. Barbosa, C. Ortiz, Á. Berenguer-Murcia, R. Torres, R. C. Rodrigues and R. Fernandez-Lafuente, *RSC Adv.*, 2014, **4**, 1583–1600.

276 W. Zhuang, J. Huang, X. Liu, L. Ge, H. Niu, Z. Wang, J. Wu, P. Yang, Y. Chen and H. Ying, *Food Chem.*, 2019, **275**, 197–205.

277 S. B. Bankar, M. V. Bule, R. S. Singhal and L. A. Ananthanarayan, *Int. J. Food Eng.*, 2011, **7**, 8.

278 M. Hui, Z. Dong, Q. Tian, J. Huang and Y. Zi, *Zhongguo Shipin Xuebao*, 2018, **18**, 134–140.

279 L. Liao, Y. Meng, R. Wang, B. Jia and P. Li, *Front. Bioeng. Biotechnol.*, 2019, **7**, 426.

280 L. Cao, F. Van Rantwijk and R. A. Sheldon, *Org. Lett.*, 2000, **2**, 1361–1364.



281 R. Schoevaart, M. W. Wolbers, M. Golubovic, M. Ottens, A. P. G. Kieboom, F. van Rantwijk, L. A. M. van der Wielen and R. A. Sheldon, *Biotechnol. Bioeng.*, 2004, **87**, 754–762.

282 R. A. Sheldon, *Appl. Microbiol. Biotechnol.*, 2011, **92**, 467–477.

283 A. Pollak, H. Blumenfeld, M. Wax, R. L. Baughn and G. M. Whitesides, *J. Am. Chem. Soc.*, 1980, **102**, 6324–6336.

284 V. G. Tacias-Pascacio, E. García-Parra, G. Vela-Gutiérrez, J. J. Virgen-Ortiz, Á. Berenguer-Murcia, A. R. Alcántara and R. Fernandez-Lafuente, *Catalysts*, 2019, **9**, 1035.

285 K. Buchholz and B. Gödelmann, *Biotechnol. Bioeng.*, 1978, **20**, 1201–1220.

286 M. Reuss and K. Buchholz, *Biotechnol. Bioeng.*, 1979, **21**, 2061–2081.

287 J. E. Prenosil, *Biotechnol. Bioeng.*, 1979, **21**, 89–109.

288 R. K. Owusu and A. Finch, *Biochim. Biophys. Acta, Protein Struct. Mol. Enzymol.*, 1986, **872**, 83–91.

289 R. Dayal and T. Godjevargova, *Enzyme Microb. Technol.*, 2006, **39**, 1313–1318.

290 F. Muzika, R. Jurašek, L. Schreiberová, V. Radojković and I. Schreiber, *J. Phys. Chem. A*, 2017, **121**, 7518–7523.

291 P. H. S. Tse and D. A. Gough, *Biotechnol. Bioeng.*, 1987, **29**, 705–713.

292 L. Tarhaqn and A. Telefoncu, *Appl. Biochem. Biotechnol.*, 1990, **26**, 45–57.

293 L. Tarhan and A. Telefoncu, *Process Biochem.*, 1992, **27**, 11–15.

294 L. E. Romero and D. Cantero, *Prog. Biotechnol.*, 1998, **15**, 107–112.

295 A. V. Ruales-Salcedo, J. C. Higuita, J. Fontalvo and J. M. Woodley, *Z. Naturforsch. C: J. Biosci.*, 2019, **74**, 77–84.

296 Q. Chen, S. Yu, N. Myung and W. Chen, *J. Biotechnol.*, 2017, **263**, 30–35.

297 X. Han, G. Liu, W. Song and Y. Qu, *Bioresour. Technol.*, 2018, **248**, 248–257.

298 X. Han, G. Liu, Y. Pan, W. Song and Y. Qu, *Bioresour. Technol.*, 2018, **251**, 407–410.

299 H. Zhang, S.-F. Hua and L. Zhang, *J. Chem. Technol. Biotechnol.*, 2020, **95**, 1116–1125.

300 M. Onda, Y. Lvov, K. Ariga and T. Kunitake, *J. Ferment. Bioeng.*, 1996, **82**, 502–506.

301 F. Zhao, H. Li, Y. Jiang, X. Wang and X. Mu, *Green Chem.*, 2014, **16**, 2558–2565.

302 S. Rezaei, A. Landarani-Isfahani, M. Moghadam, S. Tangestaninejad, V. Mirkhani and I. Mohammadpoor-Baltork, *Chem. Eng. J.*, 2019, **356**, 423–435.

303 H. Gürce, S. S. Çelebi, H. Özyörük and A. Yıldız, *J. Electroanal. Chem.*, 1995, **397**, 217–223.

304 L. B. Marshall, G. D. Christian and A. Kumar, *Analyst*, 1977, **102**, 424–428.

305 F. Conzuelo, M. Gamella, S. Campuzano, M. A. Ruiz, A. J. Reviejo and J. M. Pingarrón, *J. Agric. Food Chem.*, 2010, **58**, 7141–7148.

306 W. Yang, P. Pang, X. Gao, Q. Cai, K. Zeng and C. A. Grimes, *Sens. Lett.*, 2007, **5**, 405–410.

307 S. Jimenez-Falcao, N. Joga, A. García-Fernández, A. Llopis Lorente, D. Torres, B. de Luis, F. Sancenón, P. Martínez Ruiz, R. Martínez-Máñez and R. Villalonga, *J. Mater. Chem. B*, 2019, **7**, 4669–4676.

308 Y. K. Cho and J. E. Bailey, *Biotechnol. Bioeng.*, 1977, **19**, 185–198.

309 A. R. da Silva, E. J. Tomotani and M. Vitolo, *Braz. J. Pharm. Sci.*, 2011, **47**, 399–408.

310 F. A. Taraboulsi, E. J. Tomotani and M. Vitolo, *Appl. Biochem. Biotechnol.*, 2011, **165**, 1708–1724.

311 T. T. H. Obata and J. Tanishita, *Technol. Rep. Kansai Univ.*, 1983, 193–198.

312 B. Henrissat, T. T. Teeri and R. A. J. Warren, *FEBS Lett.*, 1998, **425**, 352–354.

313 M. Kim and D. F. Day, *Appl. Biochem. Biotechnol.*, 2010, **162**, 1379–1390.

314 D. F. Day, G. Dequeiroz, C. H. Chung and M. Kim, *Int. Sugar J.*, 2008, **110**, 7–11.

315 A. Gosling, G. W. Stevens, A. R. Barber, S. E. Kentish and S. L. Gras, *Food Chem.*, 2010, **121**, 307–318.

316 M. B. Alvarado-Huallanco and F. Maugeri Filho, *Catal. Sci. Technol.*, 2011, **1**, 1043–1050.

317 D. C. Sheu, P. J. Lio, S. T. Chen, C. T. Lin and K. J. Duan, *Biotechnol. Lett.*, 2001, **23**, 1499–1503.

318 K. Hoon Jung, J. Hwan Kim, Y. Joong Jeon and J. Heung Lee, *Biotechnol. Lett.*, 1993, **15**, 65–70.

319 C. Fischer and T. Kleinschmidt, *Enzyme Microb. Technol.*, 2019, **121**, 45–50.

320 F. Rico-Rodríguez, J. C. Serrato, A. Montilla and M. Villamiel, *Ultrason. Sonochem.*, 2018, **44**, 177–183.

321 S.-W. Chang, W.-H. Chang, M.-R. Lee, T.-J. Yang, N.-Y. Yu, C.-S. Chen and J.-F. Shaw, *J. Agric. Food Chem.*, 2010, **58**, 2908–2914.

322 T. Nishimoto, M. Nakano, T. Nakada, H. Chaen, S. Fukuda, T. Sugimoto, M. Kurimoto and Y. Tsujisaka, *Biosci., Biotechnol., Biochem.*, 1996, **60**, 640–644.

323 T.-T. Wu, S.-C. Lin and J.-F. Shaw, *Biotechnol. Prog.*, 2013, **29**, 83–90.

324 T.-T. Wu, C.-C. Ko, S.-W. Chang, S.-C. Lin and J.-F. Shaw, *Process Biochem.*, 2015, **50**, 928–934.

325 S. W. Chang, P. T. Liu, L. C. Hsu, C. S. Chen and J. F. Shaw, *Food Chem.*, 2012, **134**, 1745–1753.

326 L. S. Pripitina, I. D. Obbarius and E. A. Nikol'skaia, *Vopr. Pitan.*, 1971, **30**, 39–42.

327 D. Scott, *J. Agric. Food Chem.*, 1953, **1**, 727–730.

328 M. Castellari, L. Matricardi, G. Arfelli, G. Carpi and S. Galassi, *Food Sci. Technol. Int.*, 2000, **6**, 17–23.

329 G. P. Parpinello, F. Chinnici, A. Versari and C. Riponi, *Lebensm.-Wiss. Technol.*, 2002, **35**, 239–243.

330 B. Mistry and D. B. Min, *J. Food Sci.*, 1992, **57**, 196–199.

331 D. B. Min and B. S. Mistry, in *Developments in Food Science*, ed. G. Charalambous, Elsevier, Amsterdam, 1992, vol. 29, pp. 617–631.

332 A. Isaksen and J. Adler-Nissen, *Lebensm.-Wiss. Technol.*, 1997, **30**, 841–846.

333 A. Isaksen and J. Adler-Nissen, *Lebensm.-Wiss. Technol.*, 1997, **30**, 847–852.

334 S. Min, B. S. Mistry and H.-O. Lee, *J. Food Sci.*, 2003, **68**, 1272–1275.



335 C. A. Kantt, J. Bouzas, M. Dondero and J. A. Torres, *J. Food Sci.*, 1993, **58**, 104–107.

336 D. Dobbenie, M. Uyttendaele and J. Debevere, *J. Food Prot.*, 1995, **58**, 273–279.

337 K. Sankaran, S. S. Godbole and S. F. D'Souza, *Enzyme Microb. Technol.*, 1989, **11**, 617–619.

338 G. J. Pickering, D. A. Heatherbell and M. F. Barnes, *Food Res. Int.*, 1998, **31**, 685–692.

339 G. J. Pickering, D. A. Heatherbell and M. F. Barnes, *Am. J. Enol. Vitic.*, 1999, **50**, 291–298.

340 D. F. Malherbe, M. Du Toit, R. R. Cordero Otero, P. Van Rensburg and I. S. Pretorius, *Appl. Microbiol. Biotechnol.*, 2003, **61**, 502–511.

341 J. Röcker, M. Schmitt, L. Pasch, K. Ebert and M. Grossmann, *Food Chem.*, 2016, **210**, 660–670.

342 A. E. Gal, *Anal. Biochem.*, 1968, **24**, 452–461.

343 G. Karlsson, S. Winge and H. Sandberg, *J. Chromatogr. A*, 2005, **1092**, 246–249.

344 K. H. Mah, H. W. Yussof, N. A. Jalanni, M. N. Abu Seman and N. Zainol, *J. Teknol.*, 2014, **70**, 93–98.

345 K. H. Mah, H. W. Yussof, M. N. Abu Seman and A. W. Mohammad, *Sep. Purif. Technol.*, 2019, **209**, 211–222.

346 S. T. Morthensen, J. Luo, A. S. Meyer, H. Jørgensen and M. Pinelo, *J. Membr. Sci.*, 2015, **492**, 107–115.

347 S. T. Morthensen, B. Zeuner, A. S. Meyer, H. Jørgensen and M. Pinelo, *Sep. Purif. Technol.*, 2018, **194**, 73–80.

348 B. Zhao, L. Zhou, L. Ma, Y. He, J. Gao, D. Li and Y. Jiang, *Int. J. Biol. Macromol.*, 2018, **107**, 2034–2043.

349 H. Schacht, W. Kesting and E. Schollmeyer, *Textilveredlung*, 1995, **30**, 237–243.

350 N. Špička and P. Tavčer, *Tekstilec*, 2011, **54**, 16–29.

351 L. B. Wingard Jr and C. C. Liu, *Proc 8th Int Conf on Med & Bio Eng & 22nd Annu Conf on Eng in Med & Biol*, Chicago, 1969, 1.

352 E. Katz, I. Willner and A. B. Kotlyar, *J. Electroanal. Chem.*, 1999, **479**, 64–68.

353 T. Kuwahara, H. Ohta, M. Kondo and M. Shimomura, *Bioelectrochemistry*, 2008, **74**, 66–72.

354 C.-M. Yu, M.-J. Yen and L.-C. Chen, *Biosens. Bioelectron.*, 2010, **25**, 2515–2521.

355 N. Asrul, R. Othman, M. Z. A. Yahya, H. M. Salleh, F. Yusof and A. A. Ahmad, *Adv. Mater. Res.*, 2012, **512–515**, 1499–1502.

356 B. Mecheri, A. D'Epifanio, A. Geracitano, P. Targon Campana and S. Licoccia, *J. Appl. Electrochem.*, 2013, **43**, 181–190.

357 C. E. La Rotta and E. R. González, *J. Electrochem. Soc.*, 2013, **160**, G37–G45.

358 S. Naidoo, Q. Naidoo, H. Blottnitz and G. Vaivars, *IOP Conf. Ser.: Mater. Sci. Eng.*, 2013, **49**, 012062.

359 H. du Toit and M. Di Lorenzo, *Electrochim. Acta*, 2014, **138**, 86–92.

360 R. Haddad, J.-G. Mattei, J. Thery and A. Auger, *Nanoscale*, 2015, **7**, 10641–10647.

361 B. Mecheri, D. De Porcellinis, P. T. Campana, A. Rainer, M. Trombetta, A. Marletta, O. N. Oliveira and S. Licoccia, *ACS Appl. Mater. Interfaces*, 2015, **7**, 28311–28318.

362 Y.-F. Tsai, C.-J. Shieh and H. Yang, *Microsyst. Technol.*, 2017, **23**, 3927–3935.

363 J. Galindo-De-La-Rosa, M. G. Araiza-Ramírez, A. Hernández-Torres, J. Ledesma-García and L. G. Arriaga, *J. Phys.: Conf. Ser.*, 2019, **1407**, 0–4.

364 R. D. Milton, F. Giroud, A. E. Thumser, S. D. Minteer and R. C. T. Slade, *Phys. Chem. Chem. Phys.*, 2013, **15**, 19371–19379.

365 R. D. Milton, F. Giroud, A. E. Thumser, S. D. Minteer and R. C. T. Slade, *Electrochim. Acta*, 2014, **140**, 59–64.

366 I. Osadebe and D. Leech, *ChemElectroChem*, 2014, **1**, 1988–1993.

367 P. Jenkins, S. Tuurala, A. Vaari, M. Valkiainen, M. Smolander and D. Leech, *Bioelectrochemistry*, 2012, **87**, 172–177.

368 J. J. Virgen-Ortíz, J. C. S. dos Santos, Á. Berenguer-Murcia, O. Barbosa, R. C. Rodrigues and R. Fernandez-Lafuente, *J. Mater. Chem. B*, 2017, **5**, 7461–7490.

369 M. Christwardana, Y. Chung and Y. Kwon, *Nanoscale*, 2017, **9**, 1993–2002.

370 C. Zhang, S. Zhang, W. Liu, T. Guo, R. Gu and J. Kong, *Appl. Biochem. Biotechnol.*, 2019, **189**, 822–833.

371 W.-N. Du and S.-T. Chen, *Biocontrol Sci.*, 2019, **24**, 97–101.

372 M. G. C. Baldry, *J. Appl. Bacteriol.*, 1983, **54**, 417–423.

373 R. O. Musser, H. S. Kwon, S. A. Williams, C. J. White, M. A. Romano, S. M. Holt, S. Bradbury, J. K. Brown and G. W. Felton, *Arch. Insect Biochem. Physiol.*, 2005, **58**, 138–144.

374 X. Liu, Z. Yan, Y. Zhang, Z. Liu, Y. Sun, J. Ren and X. Qu, *ACS Nano*, 2019, **13**, 5222–5230.

375 L.-H. Fu, C. Qi, J. Lin and P. Huang, *Chem. Soc. Rev.*, 2018, **47**, 6454–6472.

376 L.-H. Fu, C. Qi, Y.-R. Hu, J. Lin and P. Huang, *Adv. Mater.*, 2019, **31**, 1808325.

377 R. A. S. Nascimento, R. E. Özel, W. H. Mak, M. Mulato, B. Singaram and N. Pourmand, *Nano Lett.*, 2016, **16**, 1194–1200.

378 B. Choi, J. S. Lee, S. J. Kim, D. Hong, J. B. Park and K.-Y. Lee, *Cancer Lett.*, 2020, **478**, 56–69.

379 M. Gao, T. Wang, L. Ji, S. Bai, L. Tian and H. Song, *Front. Immunol.*, 2020, **11**, 366.

380 C. Wang, Y. Ye, G. M. Hochu, H. Sadeghifar and Z. Gu, *Nano Lett.*, 2016, **16**, 2334–2340.

381 W. Zhao, J. Hu and W. Gao, *ACS Appl. Mater. Interfaces*, 2017, **9**, 23528–23535.

382 W. Fan, N. Lu, P. Huang, Y. Liu, Z. Yang, S. Wang, G. Yu, Y. Liu, J. Hu, Q. He, J. Qu, T. Wang and X. Chen, *Angew. Chem., Int. Ed.*, 2017, **56**, 1229–1233.

383 R. Zhang, L. Feng, Z. Dong, L. Wang, C. Liang, J. Chen, Q. Ma, R. Zhang, Q. Chen, Y. Wang and Z. Liu, *Biomaterials*, 2018, **162**, 123–131.

384 W. R. Wilson and M. P. Hay, *Nat. Rev. Cancer*, 2011, **11**, 393–410.

385 S. R. McKeown, R. L. Cowen and K. J. Williams, *Clin. Oncol.*, 2007, **19**(6), 427–442.

386 K. M. Bailey, J. W. Wojtkowiak, A. I. Hashim and R. J. Gillies, *Adv. Pharmacol.*, 2012, **65**, 63–107.



387 W. Feng, X. Han, R. Wang, X. Gao, P. Hu, W. Yue, Y. Chen and J. Shi, *Adv. Mater.*, 2019, **31**, 1805919.

388 F. Mahdizadeh and M. Eskandarian, *J. Ind. Eng. Chem.*, 2014, **20**, 2378–2383.

389 S. Kato, H. Unuma, T. Ota and M. Takahashi, *J. Am. Ceram. Soc.*, 2000, **83**, 986–988.

390 B. Jain, A. K. Singh, H. Kim, E. Lichtfouse and V. K. Sharma, *Environ. Chem. Lett.*, 2018, **16**, 947–967.

391 M. Kahoush, N. Behary, A. Cayla and V. Nierstrasz, *Process Biochem.*, 2018, **64**, 237–247.

392 P. V. Nidheesh, *RSC Adv.*, 2015, **5**, 40552–40577.

393 D. K. Ahuja, L. G. Bachas and D. Bhattacharyya, *Chemosphere*, 2007, **66**, 2193–2200.

394 S. Arana-Peña, D. Carballares, A. Berenguer-Murcia, A. R. Alcántara, R. C. Rodrigues and R. Fernandez-Lafuente, *Catalysts*, 2020, **10**, 605.

