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# Fluorinated polysulfonamide based single ion conducting room temperature applicable gel-type polymer electrolytes for lithium ion batteries

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Single ion conducting polymer electrolytes (SIPES) comprised of homopolymers containing a polysulfonamide segment in the polymer backbone are presented. The polymer structure contains  $-C(CF_3)_2$  functional groups that due to better solubility allow for effective lithiation, yielding well-defined materials. An optimized polymer electrolyte membrane was fabricated as a 3 : 1 blend of single ion conducting polymer and PVdF-HFP, which exhibits a high ionic conductivity of  $0.52 \text{ mS cm}^{-1}$  and an impressive lithium ion transference number of 0.9, as well as a  $^7\text{Li}$  self-diffusion coefficient of  $4.6 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}$  at  $20^\circ\text{C}$ . The presented polymer electrolyte has superior oxidative stability and long-term stability against lithium metal, thus facilitating operation in  $\text{LiNi}_{1/3}\text{Mn}_{1/3}\text{CO}_{1/3}\text{O}_2$  (NMC111)/lithium metal cells at  $20^\circ\text{C}$  and  $60^\circ\text{C}$ , thereby clearly demonstrating the application potential of this class of materials.

## 1. Introduction

Lithium metal constitutes an attractive anode material for lithium ion batteries due to its high specific capacity and low electrochemical potential, thereby in principle facilitating batteries with high energy density.<sup>1,2</sup> Currently, the application of lithium metal in batteries is restricted due to safety issues associated with dendrite growth and rather instable solid electrolyte interphase (SEI) formation.<sup>3–7</sup> An approach to overcome this challenge comprises polymer electrolytes, which due to their beneficial mechanical properties can reduce dendrite growth.<sup>8–10</sup> Single ion conducting polymers are a particularly promising class of materials, which in contrast to typically applied dual ion conducting liquid electrolytes<sup>11,12</sup> afford high transference numbers and thus significantly reduced polarization effects, since merely lithium ions are mobile while the charge-balancing anions are covalently attached to the polymer backbone.<sup>13–15</sup> Based on theoretical work, an immobilization of anions allows for reduced dendrite formation considering that the dendrite initiation time (so-called Sand's time)  $\tau$  is reversely proportional to the anion transference number  $t_a$ ,<sup>16–18</sup> which in the case of single ion conducting polymer electrolytes tends to converge to zero provided that the lithium ion transference number  $t_{\text{Li}^+}$  approaches one.

For a successful implementation of single lithium ion conducting polymer electrolytes, various concepts were proposed. Different anionic anchor groups carrying Li ions may be

utilized, including carboxyl groups, sulfonate groups,<sup>15,19–22</sup> bis(sulfonyl)imides<sup>15,23–27</sup> and  $\text{sp}^3$  boron species.<sup>15,28–31</sup> In the case of carboxyl and sulfonate groups, the Li ions strongly associate with the anions so that merely a low concentration of free Li ions is present.<sup>19,32</sup> The B–O bond in boron based anions, however, is highly moisture sensitive; therefore long-term electrochemical stability appears questionable.<sup>14</sup> In view of the rather favorable properties in terms of high ion dissociation degrees, bis(sulfonyl)imides are considered as versatile anionic moieties.

Single ion conducting polymer electrolytes may be “dry” or gel-type polymers that are plasticized with a salt-free organic solvent or an ionic liquid (IL). In “dry” polymer electrolytes, the anionic groups should be attached to polymer side chains to enable sufficient ionic transport, *e.g. via* inter-chain hopping, whereas for a gel-type polymer electrolyte anions either can be located at side chains or at the polymer backbone, since the ion transport is likely dominated by the present solvent or IL.<sup>33–35</sup> The prominent advantages of gel-type polymer electrolytes comprise superior ionic conductivity and lower electrolyte–electrode interfacial resistances compared to rather “dry” materials, despite the fact that substantial progress was achieved for “dry” polymer electrolytes in recent years.<sup>8,13,36–39</sup> Notably, sufficient polymer flexibility results either from incorporation of rather flexible, linear polymer compounds into single ion conducting polymer structures or from blending of aromatic single ion conducting polymers (that tend to be brittle when fabricated as a self-standing membrane) with another polymer having a linear structure.<sup>34</sup> Previous reports indeed revealed the beneficial characteristics of single ion conducting gel-type polymer electrolytes derived from aromatic polysulfonamide-based homopolymers composed of

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polysulfonamide anionic moieties in the polymer backbone.<sup>26,27,40–47</sup> Due to its good mechanical properties demonstrated from application as a gel-type polymer electrolyte in lithium ion batteries,<sup>48,49</sup> PVdF-HFP was proposed as a possible blend partner. The membranes were fabricated by a solution cast method, yielding porous structures that were further plasticized with a salt-free and thermally stable solvent solution such as EC : PC or EC : DEC, respectively. The resulting polymer electrolyte membranes afforded a high oxidative stability of at least 4.0 V as well as adequate ionic conductivity ( $10^{-4}$  to  $10^{-3}$  S cm<sup>-1</sup>). To the best of our knowledge, in most reported work, the considered polymers were lithiated *via* treatment with lithium hydroxide. Based on significant signals at 3.33 ppm in the corresponding <sup>1</sup>H NMR spectra of the resulting materials in DMSO-(d<sub>6</sub>),<sup>26,27,40–47</sup> an unintentional but substantial presence of either residual water or unreacted lithium hydroxide within the polymers has to be assumed, even though for long-term battery application, extraordinary high purity and anhydrous electrolytes are essential in order to avoid continuous material degradation, while facilitating high electrochemical performance of lithium metal cells.

Herein, we introduce a homopolymer containing polysulfonamide moieties at the polymer backbone, which was tailored by introducing a -C(CF<sub>3</sub>)<sub>2</sub> functional group (Fig. 1). The obtained polymer exhibited enhanced solubility in aprotic polar solvents (such as THF), thereby allowing for the utilization of an improved lithiation method, affording fully defined lithiation and complete removal of residual solvent or unreacted species. A series of single ion conducting polymers (homopolymers) were prepared, where carboxyl(benzene sulphonyl)imide was combined with different dianiline units including *p*-phenylenediamine, benzidine, 4,4'-diaminodiphenylsulfone and 4,4'-(hexafluoroisopropylidene)dianiline, respectively. Nevertheless, merely the fluorinated species exhibited sufficient solvent solubility for processing, which is considered essential to reproducibly achieve full lithiation of the polymers. The derived single ion conducting polymer (5) was blended with

PVdF-HFP and swollen in a solvent solution composed of EC : PC (1 : 1, v/v) for the fabrication of polymer electrolyte membranes. Upon variation of the single ion conducting polymer to PVdF-HFP ratio, an optimized blend membrane with sufficient mechanical stability and improved ionic conductivity was successfully produced.

## 2. Experimental section

### 2.1 Materials

*p*-Toluenesulfonamide (97%), *p*-toluenesulfonyl chloride (97%), potassium permanganate (KMnO<sub>4</sub>), lithium hydroxide monohydrate, calcium chloride, *N*-methyl-2-pyrrolidone (NMP, anhydrous, 99.8%), pyridine (anhydrous, 99.8%), tetrahydrofuran (THF, anhydrous, 99.8%), lithium bis(trimethylsilyl) amide solution (1 M in THF), and terephthalic acid (98%) were purchased from Sigma Aldrich, Germany. 4,4'-(Hexafluoroisopropylidene)dianiline (98%) was obtained from TCI Europe and poly(vinylidene difluoride-*co*-hexafluoropropylene) PVdF-HFP (Kynar FLEX LBG) was purchased from Arkema, Austria. Concentrated hydrochloric acid, methanol (AR), dimethylsulfoxide (DMSO, AR) and triphenylphosphite (TPP, AR) were acquired from VWR. Ethylene carbonate (EC) and propylene carbonate (PC) were purchased from BASF, Germany. LiNi<sub>1/3</sub>Co<sub>1/3</sub>Mn<sub>1/3</sub>O<sub>2</sub> was obtained from Shanshan (China), carbon black (Super C65) was obtained from Imerys Graphite and carbon and polyvinylidene difluoride (PVdF, Solef 5130) from Solvay, Belgium. Calcium chloride was dried at 180 °C under vacuum for 48 hours, 4,4'-(hexafluoroisopropylidene)dianiline was dried at 100 °C under vacuum for 24 hours before use.

### 2.2 Synthesis

#### 2.2.1 Synthesis of the potassium(4-carboxyl benzene sulphonyl)imide monomer (2)

*Synthesis of bis(4-methyl benzene sulphonyl)imide (1).* The synthesis of the bis(4-methyl benzene sulphonyl)imide monomer (1) was achieved based on the Hinsberg reaction in previous work.<sup>26,27,42–45,50</sup> Using aqueous media for the reaction of the highly reactive sulfonyl chloride, however, often results in significantly reduced reaction yields (about 40%) due to a high degree of side reactions. Therefore, the Einhorn reaction was performed in anhydrous pyridine. Equivalent molar ratios of *p*-toluenesulfonamide (7.50 g, 43.80 mmol) and *p*-toluenesulfonyl chloride (8.45 g, 43.80 mmol) were dissolved in 10 ml of the solvent at 90 °C separately, and the *p*-toluenesulfonamide solution was stirred while the *p*-toluenesulfonyl chloride solution was added dropwise. The reaction mixture was stirred for 12 hours (Fig. 2). Afterwards, using a Schlenk line and an additional cooling trap the solvent was vaporized under reduced pressure at 100 °C, a condition where unreacted *p*-toluenesulfonamide sublimed. The obtained product was washed with 500 ml of distilled water, filtered and dried under vacuum at 100 °C for 48 hours. A white powder was obtained with a yield of 69% (9.88 g). The absence of the signal in the <sup>1</sup>H NMR spectrum corresponding to residual solvent (pyridine or H<sub>2</sub>O) or the

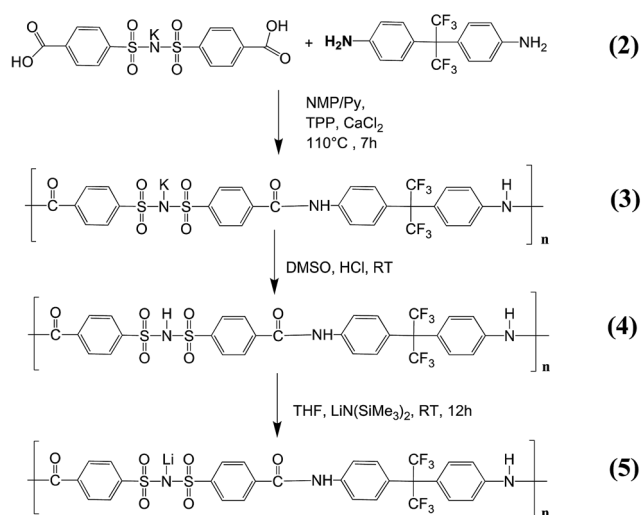


Fig. 1 Schematic route of the polycondensation and ion exchange yielding the final lithiated single ion conducting polymer (5).



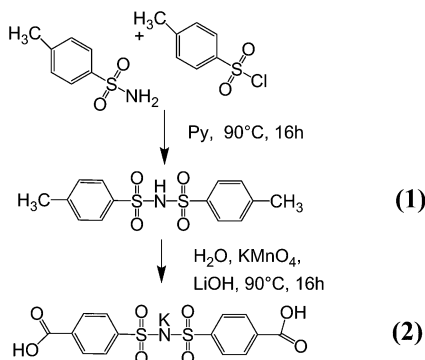


Fig. 2 Schematic route of the synthesis of the potassium(4-carboxyl benzene sulphonyl)imide monomer (2) under investigation of the Einhorn reaction (step 1) and end group functionalization (step 2).

reagent of the product indicates high purity of the bis(4-methyl benzene sulphonyl)imide.  $^1\text{H NMR}$  ( $\text{DMSO-d}_6$ ): 7.20 (d, 4H), 7.54 (d, 4H), and 2.33 (s, 6H);  $\text{ESI}^- m/z$ : 325.04 (100%,  $(\text{CH}_3-\text{C}_6\text{H}_4-\text{SO}_2)_2\text{N}^-$ ).

**Synthesis of the potassium(4-carboxyl benzene sulphonyl)imide monomer (2).** Functionalization of the methyl end groups of bis(4-methyl benzene sulphonyl)imide (1) was performed dissolving 9.50 g (29.15 mmol) of bis(4-methyl benzene sulphonyl)imide (1) and 1 equivalent (0.6258 g, 29.15 mmol)  $\text{LiOH}\cdot\text{H}_2\text{O}$  in 500 ml of deionized water at  $95^\circ\text{C}$  (Fig. 2). Then, 60.80 g of  $\text{KMnO}_4$  (3 eq., 87.45 mmol) were slowly added to the solution and the reaction solution was stirred for 12 hours under reflux. The solution was cooled down to  $50^\circ\text{C}$  and  $\text{MnO}_2$  was filtered off, yielding a clear filtrate. Precipitation of the raw product from the filtrate was achieved by acidification with concentrated  $\text{HCl}$  (until  $\text{pH} = 1$ ). The white precipitate was filtered off and washed with 1000 ml methanol, and then dried under vacuum at  $100^\circ\text{C}$ , yielding 8.00 g of product (65%) (2).  $^1\text{H NMR}$  ( $\text{DMSO-d}_6$ ): 7.73 (d, 4H), 7.90 (d, 42H), and 13.15 (s, 2H);  $\text{ESI}^- m/z$ : 384.99 (100%,  $(\text{COOH}-\text{C}_6\text{H}_4-\text{SO}_2)_2\text{N}^-$ ).

**2.2.2 Polycondensation.** Polycondensation of 4,4'-(hexafluoroisopropylidene)dianiline and potassium(4-carboxyl benzene sulphonyl)imide (2) was performed as described elsewhere.<sup>51,52</sup> 8.4 ml of pyridine, 30 ml of NMP, 2.16 g of calcium chloride (19.4 mmol), 8.42 ml TPP (32.12 mmol), 2.51 g (6.02 mmol) 4,4'-(hexafluoroisopropylidene)dianiline, and 3.12 g (6.02 mmol) potassium(4-carboxyl benzene sulphonyl)imide, were added subsequently to a 100 ml round-bottom flask under an argon atmosphere. The solution was heated to  $110^\circ\text{C}$  and the reaction continued under stirring for 7 h. Subsequently, the reaction mixture was cooled to room temperature (approximately  $25^\circ\text{C}$ ) and precipitated by dropwise addition into 1000 ml of methanol in an ice bath. The yield of the final substance (3) was 95% (5.09 g).

**2.2.3 Ion substitution.** Substitution of potassium with hydrogen ions was achieved by dissolving 5 g of the polymer (3) in 30 ml  $\text{DMSO}$  and subsequent precipitation by addition of concentrated  $\text{HCl}$ . The precipitate was filtered and washed well with 500 ml of deionized water; this process was repeated one more time and full exchange of potassium with hydrogen was

confirmed by total reflection X-ray fluorescence analysis (TXRF,  $K < 0.05\%$ , Cl not detected). The yield of (4) was 95% (4.5 g).

**Lithiation of the polymer (4).** The preparation of lithiated polymers based on the polysulfonamide monomer was often achieved upon application of lithium hydroxide ( $\text{LiOH}$ ) in previous reports,<sup>26,27,40–47</sup> despite the fact that the corresponding  $^1\text{H NMR}$  spectra of the polymers exhibited significant signals at 3.33 ppm, clearly indicating the unintentional presence of either unreacted  $\text{LiOH}$  or residual water. Since the fluorinated single ion conducting polymer introduced in this work shows good solubility in THF compared to polysulfonamides containing other functional groups, successful lithiation was achieved with 1 M lithium bis(trimethylsilyl)amide under reduced pressure at  $80^\circ\text{C}$ . The yield was 1.09 g (98%). Full lithiation was confirmed by inductively coupled plasma optical emission spectroscopy (ICP-OES). The corresponding  $^1\text{H NMR}$  spectrum of (5) (Fig. 3) showed four doublet signals at 7.35 ppm, 7.84 ppm, 7.91 ppm and 7.97 ppm attributed to aromatic compounds, and a singlet at 10.59 ppm related to  $\text{CO-NH}$  coupling of the monomers. The ratio of the integrated peak areas of the coupling proton to aromatic compounds was 1 : 8.4 (theoretically: 1 : 8). The absence of further signals confirmed the rather high purity and successful removal of solvents.

### 2.3 Preparation of the single ion conducting polymer electrolyte membrane

Four different membrane compositions were made, where the actual amount of lithiated polymer increased in order to obtain

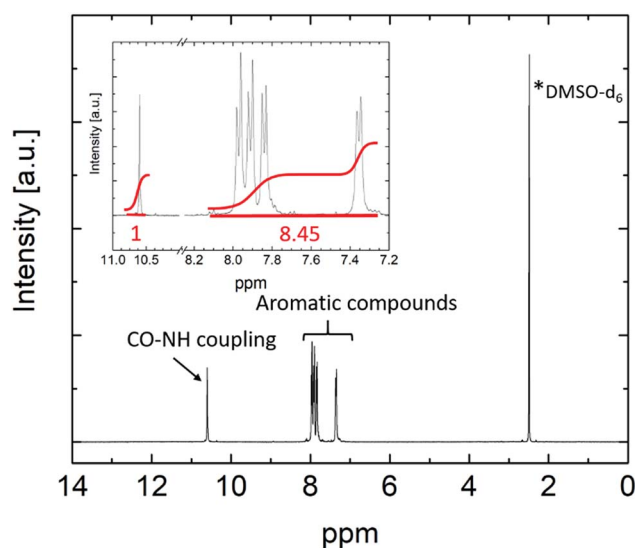


Fig. 3  $^1\text{H NMR}$  spectrum of the lithiated polymer (5). Doublets between 7 ppm and 8 ppm refer to the aromatic compounds and the singlet at 10.59 ppm can be assigned to the  $\text{CO-NH}$  coupling of the two monomers.



membranes with good ionic conductivity and sufficient mechanical flexibility. Weight ratios of 1 : 1, 3 : 5, 2 : 6 and 1 : 7, respectively, of PVdF-HFP to lithiated polymer were considered. For each membrane, a total amount of 400 mg of polymer (5) was dissolved in 4 ml NMP at 60 °C. The solution was cast in a Petri dish and placed into a vacuum oven at 80 °C overnight yielding a homogeneous polymer membrane of about 80 μm thickness. Disks of 12 or 13 mm diameter were cut from the membrane and further dried for 48 hours at 100 °C under vacuum prior to soaking them with EC : PC (1 : 1, v/v) solvent solution. EC : PC (1 : 1, v/v) was selected due to its superior thermal stability compared to other solvent mixtures used for battery applications, containing a linear carbonate compound such as *e.g.* diethyl carbonate (DEC), dimethyl carbonate (DMC) or ethyl methyl carbonate (EMC).<sup>53</sup> The weight of the membranes was measured after removing the residual liquid on the surface of the polymer film. The corresponding solvent uptake (SU) was derived from the following equation:

$$SU = \frac{w_s - w_0}{w_0} \times 100\% \quad (1)$$

with  $w_s$  and  $w_0$  denoting the weight of the swollen and dry membranes, respectively.

#### 2.4 Preparation of the cathode

For the preparation of LiNi<sub>1/3</sub>Co<sub>1/3</sub>Mn<sub>1/3</sub>O<sub>2</sub> (NMC111) containing cathode material, 0.132 g (3 wt%) PVdF was dissolved in 6 ml NMP and stirred overnight. Subsequently, 0.132 g (3 wt%) of carbon black, 0.132 g (3 wt%) of lithiated terephthalic acid and 4 g (91 wt%) of NMC were added and the viscous solution was transferred to a swing mill MM 400 (Retsch Technology, Haan, Germany) stirring for 30 min at a frequency of 30 Hz. The slurry was then cast onto an aluminum current collector using a doctor blade technique at a gap width of 50 μm. The obtained coating was dried at 80 °C overnight, followed by further drying at 80 °C under vacuum. The electrodes were calendered using a roll press. The thickness of the two rolls was decreased from the initial thickness of the electrodes (current collector + coating (20 μm + 26 μm = 46 μm)) down to the thickness of the current collector + half of the initial coating thickness in two steps (to 20 μm + 13 μm = 33 μm), thereby reaching a compression of the coating of 50%. The final electrode coating

thickness was 13 ± 1 μm and the mass loading was 2.8 mg cm<sup>-2</sup>.

#### 2.5 Methods

**2.5.1 Material characterization.** <sup>1</sup>H NMR spectra were recorded on a BRUKER 400 AVANCE III HD instrument using deuterated dimethyl sulfoxide (DMSO-d<sub>6</sub>) as the reference signal. Pulsed field gradient nuclear magnetic resonance (PFG-NMR) data were acquired on a BRUKER 200 AVANCE III spectrometer equipped with a (doubly tuned <sup>7</sup>Li/<sup>1</sup>H) 5 mm coil at either 20 °C or 40 °C (±0.1 °C). A 0.25 M LiCl in H<sub>2</sub>O solution was utilized for external calibration at 0 ppm. The gradient strength  $g$  was varied from 35–1050 G cm<sup>-1</sup> averaging up to 4750 scans with a gradient pulse length  $\delta$  of 1 ms and diffusion time  $\Delta$  of 40 ms. The self-diffusion coefficients  $D$  of the lithium species were derived from a stimulated echo sequence (“diffSte”) after fitting the attenuated signal amplitude to the Stejskal–Tanner equation, which describes the case of rather ideal (“free”) isotropic diffusion:

$$I = I_0 \times e^{(-D\gamma^2\delta^2g^2(\Delta - \frac{\delta}{3}))} \quad (2)$$

with  $I$  being the signal intensity,  $I_0$  the initial signal in the absence of a magnetic field gradient and  $\gamma$  the gyromagnetic ratio. Data analysis was done with BRUKER Topspin 3.5 and BRUKER Dynamics Center 2.5. For the measurement, the swollen membrane (exemplarily shown in Fig. 4a) was placed into a polytetrafluoroethylene (PTFE) tube (bottom part was cut open). Teflon tape was added above and below the SIPE, while the polymer electrolyte was gently pushed inside the tube. The PTFE tube was placed inside a 5 mm diameter glass tube (Fig. 4b).

ICP-OES measurements were performed using a Spectro ARCOS EOP device (Spectro Analytical Instruments GmbH, Kleve, Germany) after having the polymer dissolved using a microwave-assisted acid digestion (Anton Paar Multiwave Pro, Graz, Austria).

For total reflection X-ray fluorescence (TXRF) measurements, a Picofox S2 system equipped with Spectra 7.5 software (Bruker Corporation, Billerica, MA, USA) was used. The polymer sample was placed on a quartz glass carrier from Bruker Corporation.

Thermogravimetric analysis (TGA) was performed on a Q5000IR instrument (TA Instruments) applying a heating

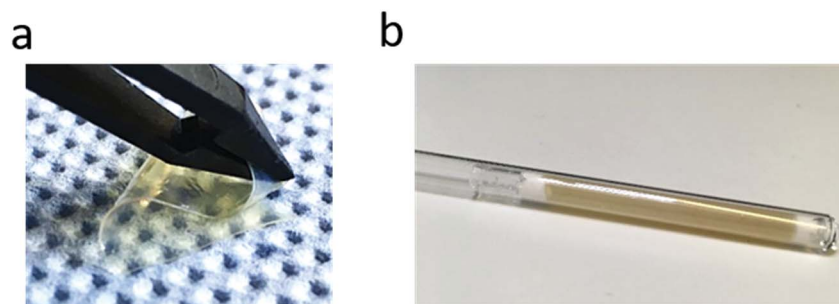


Fig. 4 (a) Picture of the swollen SIPE membrane (PVdF-HFP to lithiated polymer weight ratio 1 : 3) and (b) sample prepared for PFG-NMR measurements.



rate of  $10\text{ }^{\circ}\text{C min}^{-1}$  from room temperature to  $700\text{ }^{\circ}\text{C}$  under an oxygen gas atmosphere. Differential scanning calorimetry (DSC) was conducted between  $-150\text{ }^{\circ}\text{C}$  and  $150\text{ }^{\circ}\text{C}$  with a heating rate of  $10\text{ }^{\circ}\text{C min}^{-1}$  on a Q2000 device (TA Instruments).

Scanning electron microscopy (SEM) was used to investigate the morphology (surface and cross section) of the polymer membranes. Cross sections were prepared by immersing the samples in liquid nitrogen and breaking the membranes. Multiple areas per sample were analyzed on an Auriga Cross-Beam workstation from Zeiss (Germany) at an acceleration voltage of 3 kV.

**2.5.2 Electrochemical investigations.** Electrochemical Impedance Spectroscopy (EIS) was conducted between  $-40\text{ }^{\circ}\text{C}$  and  $80\text{ }^{\circ}\text{C}$  in steps of  $10\text{ }^{\circ}\text{C}$  applying a NOVOCONTROL alpha-S-spectrometer. Impedance spectra were measured applying an alternating voltage signal having an amplitude of 5 mV over a frequency range from  $10^{-1}$  to  $4 \times 10^7$  Hz. A coin cell setup was used where the swollen membrane (12 mm diameter) was placed between two stainless steel electrodes. DC conductivity values were extracted from the plateau region of the frequency-dependent real part of the complex conductivity. A temperature ramp was applied from  $20\text{ }^{\circ}\text{C}$  to  $80\text{ }^{\circ}\text{C}$ , down to  $-40\text{ }^{\circ}\text{C}$  and back to  $80\text{ }^{\circ}\text{C}$ . This temperature ramp was performed twice and demonstrated reversible behavior.

The lithium-ion transference number ( $t_{\text{Li}^+}$ ) was determined using the combined potentiostatic polarization and complex impedance measurement technique proposed by Evans *et al.*<sup>54</sup> The membrane was sandwiched between two non-blocking lithium metal electrodes and the symmetrical cell was measured at  $40\text{ }^{\circ}\text{C}$  using an Autolab PGSTAT302N (Metrohm, Modul: FRA V2.0, Nova-Software 1.6). Impedance spectra were collected between 1 Hz and 2 GHz and a DC polarization voltage  $\Delta V$  of 10 mV was applied across the sample. Subsequently, the lithium ion transference number was determined by

$$t_{\text{Li}^+} = \frac{I_s(\Delta V - I_0 R_0)}{I_0(I_s R_s)} \quad (3)$$

with  $I_0$  and  $I_s$  the initial and steady state current, respectively.  $R_0$  and  $R_s$  are the initial and steady state resistances of the interfaces.

The electrochemical stability of the polymer blend was determined using a VSP instrument (Bio-Logic Science Instruments). Measurements were conducted in a three electrode cell setup using lithium as the counter and reference electrode and platinum or copper as the working electrode for oxidative or reductive stability, respectively. A scan rate of  $80\text{ }\mu\text{V s}^{-1}$  was applied in the potential range between  $-0.5\text{ V}$  and  $6\text{ V}$  (*vs.*  $\text{Li/Li}^+$ ).

Cycling investigations were performed on a Maccor 4000 battery analysis system (USA) between  $3.0\text{ V}$  and  $4.3\text{ V}$  *vs.*  $\text{Li/Li}^+$  (constant current charging, CC), while the cells are at constant temperature in a climatic chamber, at either  $60\text{ }^{\circ}\text{C}$  or  $20\text{ }^{\circ}\text{C}$ , respectively.

## 3. Results and discussion

### 3.1 Polymer membrane composition and ionic transport

Upon varying the contents of both aromatic single ion conducting polymer and mechanically stable PVdF-HFP, an optimized composition for superior polymer membrane performance was identified. Weight ratios of lithiated polymer and PVdF-HFP of 1 : 1,<sup>19,27,29</sup> 2 : 3,<sup>28</sup> 3 : 2 (ref. 41) and 2 : 1,<sup>27</sup> respectively, were utilized for membrane fabrication in previous studies of similar non-fluorinated polysulfonamide containing homopolymers, though none of the studies included an optimization of the blend composition. In the case of binary blends comprised of fluorinated polysulfonamide carrying the conducting species (in this case Li) and flexible PVdF-HFP, it can be expected that a higher content of aromatic polymer yields improved ionic conductivity of the resulting polymer electrolyte membrane. Nevertheless, sufficient mechanical stability has to be maintained for the fabrication of membranes that are applicable in Li ion batteries, so that a minimum amount of PVdF-HFP (or any other film-forming blend partner) should be present. Notably, four different membranes with corresponding PVdF-HFP to lithiated polymer ratios of 1 : 1, 3 : 5, 1 : 3 and 1 : 7 (wt% : wt%) were fabricated. The membrane containing 12.5 wt% of PVdF-HFP (sample 1 : 7) became chapped after drying under vacuum and removal of the glass substrate, but all other membrane compositions were found to be suitable as electrolyte membranes and were immersed in a solvent solution of EC : PC (v/v, 1 : 1) for 16 hours. The swollen membranes exhibited sufficient mechanical stability and flexibility, affording bending without damage of the membranes. For all fabricated membranes, the corresponding solvent uptake (eqn (1)) and ionic conductivities were determined (Fig. 5a). The weight uptakes of neat PVDF-HFP as well as neat SIPE were determined as reference values (note however that the neat SIPE membrane is highly brittle and cannot be considered for application). Fig. 5b displays the temperature dependent ionic conductivities for the different membrane compositions.

As anticipated at a higher content of Li ions, the achievable ionic conductivity significantly increased at a higher content of the aromatic polymer within the blend. Upon changing the membrane compositions from 50 wt% SIPC and 50 wt% PVdF-HFP (1 : 1) to 75 wt% SIPC and 25 wt% PVdF-HFP (1 : 3), an increase in ionic conductivity from  $0.10\text{ mS cm}^{-1}$  to  $0.52\text{ mS cm}^{-1}$  is observed at  $20\text{ }^{\circ}\text{C}$ , despite the fact that the actual solvent uptake is reduced from 147 wt% to 130 wt%. For all samples, the solvent uptake is comparatively low compared to a neat PVdF-HFP gel membrane taking up 533 wt% of solvent which is in good agreement with published data of PEO, PAN or PVdF-HFP based gel-type polymer electrolytes, where solvent weight uptakes of 300 wt% to 400 wt%, in some cases even up to 750 wt%, are feasible.<sup>55–60</sup>

The solvent uptake in principle can be correlated with the morphology of the membranes. The morphologies of all blend membrane compositions (surface and cross section) as well as those of neat PVdF-HFP and SIPE membranes (surface) were investigated by SEM and are shown in Fig. 6. For the PVdF-HFP



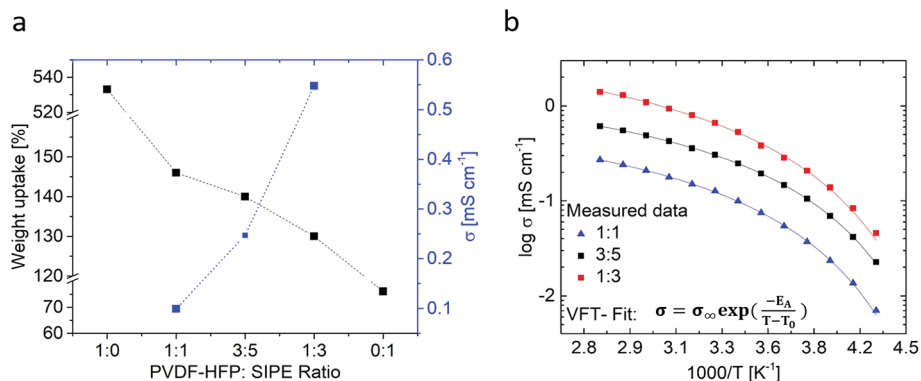


Fig. 5 (a) Solvent weight uptake and ionic conductivity at 20 °C for the different SIPE electrolyte membrane compositions. (b) Temperature dependent ionic conductivity of the different SIPE membranes (PVdF-HFP: lithiated polymer content).

membrane pores of a few micrometer size were clearly visible whereas for the SIPE membrane no obvious pore structure could be observed (images at the top). The blend membranes differed from both of the neat membranes. All compositions had a dense structure showing no micropores in both the surface (middle) and cross sectional images (bottom), though

nanopores could be assumed based on the respective high resolution images. The observed morphologies correlate well with the solvent uptake since for PVdF-HFP 500 wt% of solvent was taken up by the microporous structures while the dense blend membranes took up equally low amounts of about 130 wt% to 147 wt%, likely due to the absence of micropores. In

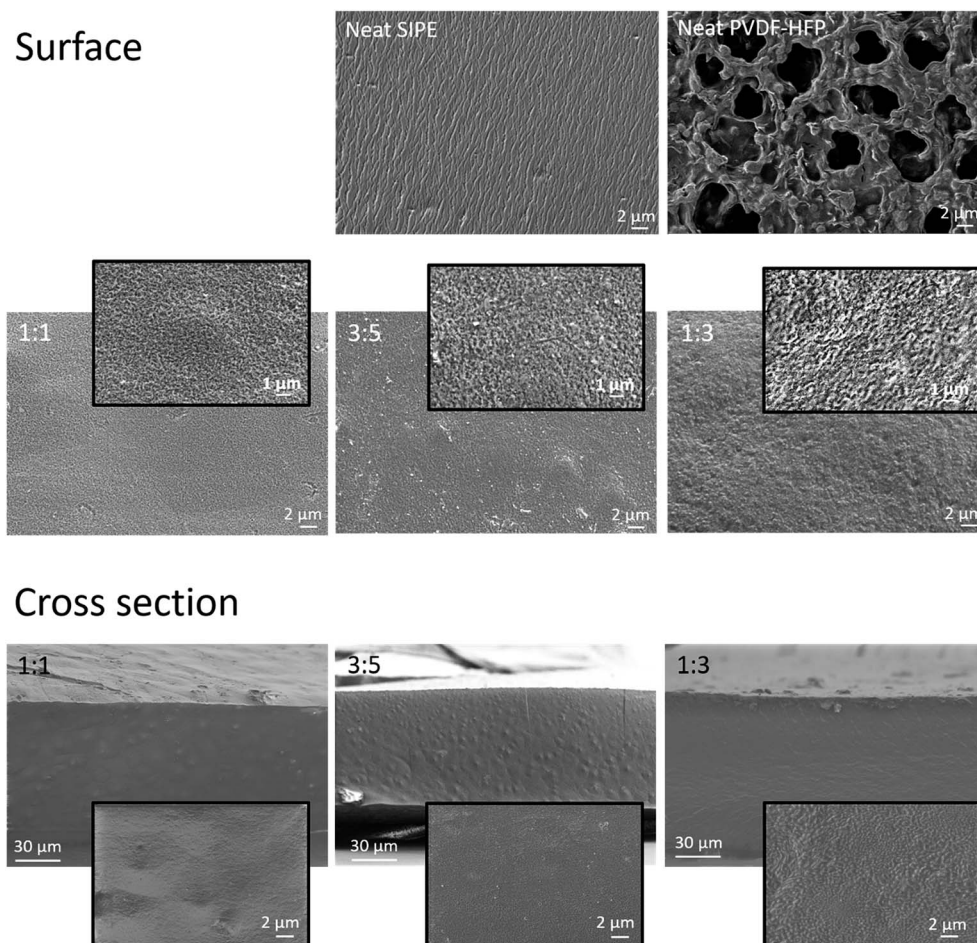


Fig. 6 SEM images of the surfaces of neat SIPE and PVdF-HFP membranes (top), the blend polymer membranes of different ratios of PVdF-HFP : SIPE (middle) and cross sections of the blend polymer membranes (bottom).



the case of similar polymer blend systems composed of SIPE and PVdF-HFP both microporous<sup>40,43,45,47</sup> and nanoporous<sup>46</sup> morphologies were identified. For equally prepared membranes the morphology may be either highly porous or rather dense based on the chemical structure of the SIPE, depending on the compatibility of the two polymer blend compounds.<sup>26,41,42</sup>

Regarding the polymer membranes with composition 1 : 3, ionic conductivities of 0.5 mS cm<sup>-1</sup> and 1.08 mS cm<sup>-1</sup> were achieved at 20 °C and 60 °C, respectively, which are among the highest values obtained for similar polymer blends comprised of PVdF-HFP and polysulfonamide based single Li-ion polymers.<sup>26,27,40-44</sup> It should be noted that the ionic conductivity measured here is based on the conduction of only lithium ions as no residual solvent or impurities of the synthesis are present that could otherwise contribute to the overall ionic conductivity.

All membranes show a rather comparable trend in ionic conductivity, reminiscent of Vogel-Fulcher-Tamann (VFT) behavior in the observed temperature range between -40 °C and 80 °C. Typically, fitting the curves with the VFT equation

$\sigma = \sigma_0 \times e^{-\frac{E_a}{k(T-T_0)}}$  yields values for  $E_a$ , an Arrhenius-type activation energy of ion transport, and for  $T_0$ , the so-called Vogel temperature. The apparent activation energy of ion transport in all considered polymer blend compositions within the error margin of the measurement amounts to  $\approx 3.4 \pm 0.2$  kJ mol<sup>-1</sup>, irrespective of the changes of the actual membrane composition. In the case of PEO/PPO-based “dry” single ion conducting

polymer systems containing SO<sub>3</sub><sup>-</sup> anchoring groups (that exhibit comparable charge carrier densities) 2 to 12 times higher apparent activation energies were obtained.<sup>32,61,62</sup> For other gel-type electrolytes (containing lithium salt and multiple times higher solvent content), 2 times higher values were reported.<sup>63</sup> However, a physically mixed blend polymer electrolyte strictly speaking does not reflect a single morphological “phase”, thus making a straightforward comparison of the derived data with other gel polymer electrolytes difficult.

Based on the obtained ionic conductivities  $\sigma_{DC}$ , the corresponding ion mobility  $\mu$  and lithium ion self-diffusion coefficients  $D$  can be estimated from eqn (4)

$$\mu = \frac{\sigma_{DC}}{ne} \quad (4)$$

and the Nernst Einstein equation (eqn (5))

$$\sigma_{DC} = \frac{ne^2}{kT}(D_+ + D_-) \quad (5)$$

where  $n$  is the charge carrier density,  $e$  is the elemental charge,  $k$  is the Boltzmann constant,  $T$  the temperature and  $D_+$  and  $D_-$  are the self-diffusion coefficients of cations and anions, respectively. Under ideal conditions, anions within the polymer electrolytes are considered rather immobile due to their attachment to the polymer backbone (with  $D_- \rightarrow 0$  and  $t_{Li^+} \rightarrow 1$ ), but in real cases the lithium-ion transference numbers are commonly between 0.85 and 0.95, indicating minor contributions of other species to the charge transport. Indeed, the lithium-ion transference number  $t_{Li^+}$  of the investigated polymer membrane was determined to be 0.9 (for sample 1 : 3) (Fig. 7), in agreement with single ion conducting behavior. In the following, it is assumed that a lithium-ion transference number of 0.9 is valid for all considered samples comprising the lithiated polymer (5) irrespective of the utilized blend ratio. Correspondingly, for the determination of lithium self-diffusion coefficients ( $D_{Li^+,calc}$ ) based on the conductivity values  $\sigma_{DC}$ , a correction factor is considered such that

$$\mu_{Li^+,calc} = \frac{\sigma_{Li^+,calc}}{ne} \approx \frac{\sigma_{DC} \times 0.9}{ne} \quad (6)$$

$$D_{Li^+,calc} \approx \frac{kT}{ne^2} \sigma_{Li^+,calc} \quad (7)$$

The charge carrier density  $n$  is estimated based on stoichiometric and geometric parameters (thickness, area, and weight) of the rather homogenous SIPE membranes. The

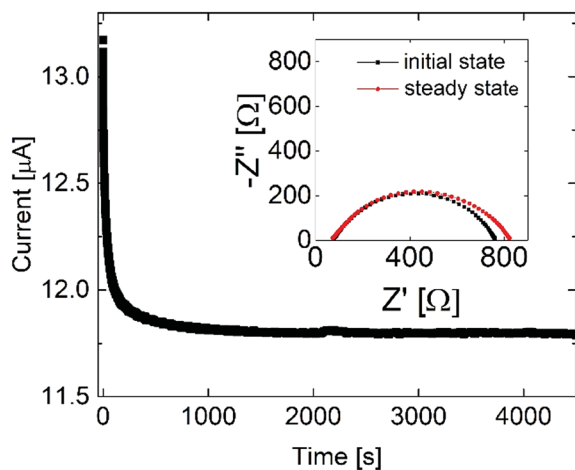


Fig. 7 Chronoamperometry and impedance measurement at 40 °C for the blend polymer membrane (sample 1 : 3).

**Table 1** Calculated charge carrier density  $n$ , ion mobility  $\mu$  and diffusion coefficients  $D_{Li^+,calc}$  (based on ionic conductivity measurements) and lithium ion diffusion coefficients  $D_{Li^+,meas}$  obtained by PFG-NMR measurements

Sample	Temperature [°C]	$n[\times 10^{20} \text{ cm}^{-3}]$	$\mu_{Li^+,calc} [\times 10^{-6} \text{ cm}^2 \text{ V}^{-1} \text{ s}^{-1}]$	$D_{Li^+,calc} [\times 10^{-11} \text{ m}^2 \text{ s}^{-1}]$	$D_{Li^+,meas} [\times 10^{-11} \text{ m}^2 \text{ s}^{-1}]$	$1-\alpha$
1 : 1	20	$3.49 \pm 0.03$	$1.60 \pm 0.01$	$0.40 \pm 0.01$	$1.03 \pm 0.04$	$0.39 \pm 0.01$
	40		$2.42 \pm 0.01$	$0.65 \pm 0.01$	$3.26 \pm 0.13$	$0.20 \pm 0.01$
3 : 5	20	$4.27 \pm 0.03$	$3.26 \pm 0.01$	$0.82 \pm 0.03$	$3.65 \pm 0.12$	$0.22 \pm 0.01$
	40		$4.71 \pm 0.02$	$1.27 \pm 0.04$	$4.35 \pm 0.25$	$0.29 \pm 0.01$
1 : 3	20	$4.90 \pm 0.03$	$6.11 \pm 0.02$	$1.54 \pm 0.01$	$4.62 \pm 0.06$	$0.33 \pm 0.01$
	40		$9.17 \pm 0.03$	$2.48 \pm 0.01$	$8.43 \pm 0.12$	$0.29 \pm 0.02$



calculated values for  $n$ ,  $D_{\text{Li}^+, \text{calc}}$  and  $\mu_{\text{Li}^+, \text{calc}}$  are collected in Table 1. Note that the estimated charge carrier density  $n$  in all cases has a similar order of magnitude known for PEO based electrolytes.<sup>32,64</sup> At a higher content of single ion conducting polymer in the membrane  $n$  as well as the observable ionic conductivity increases, in addition to improved ion mobility or lithium ion diffusivity. This observation is not trivial, since ion mobility depends on both the charge carrier density  $n$  and ionic conductivity  $\sigma$  (cf. eqn (4)). If  $\sigma$  and  $n$  increase similarly, then no major change in ion mobility  $\mu$  is expected ( $\mu \propto 1/n, \sigma$ ). Therefore, the observed increase in ion mobility likely reflects morphology changes of the membranes, thereby facilitating better transport of the lithium ions.

The measured and calculated values of lithium-ion self-diffusion coefficients have a similar order of magnitude, exhibiting an increase with higher temperatures. Lithium ion diffusion was enhanced upon increasing the total lithium ion content within the polymer membrane; the obtained values for the lithium self-diffusion are within the range of self-diffusion coefficients known for PEO based systems. In the case of a gel-type electrolyte containing lithium salt (between 0.5 M and 1.5 M) lithium self-diffusion coefficients between  $3 \times 10^{-11}$  and  $6 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}$  at 22 °C were found, despite the fact that the electrolytes had significantly higher amounts of solvent uptake.<sup>65</sup> For a solid SIPE, a self-diffusion coefficient of  $1.2 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}$  at 20 °C was determined.<sup>32</sup> From comparison of experimental and estimated self-diffusion coefficients, it is evident that  $D_{\text{Li}^+, \text{calc}}$  is lower than  $D_{\text{Li}^+, \text{meas}}$  derived from PFG-NMR. This is reasonable considering that for ionic conductivity measurements an external electric field is applied, so that primarily charged species are taken into account, whereas data from PFG-NMR reflect diffusion from all lithium species present in the electrolyte, including neutral clusters or aggregates as well as motion of otherwise associated lithium ions.<sup>66</sup> In principle, the degree of ion association  $\alpha$  may be determined from the ratio of the two diffusion coefficients, as reported for some liquid or polymer electrolytes suitable for lithium ion batteries,<sup>34,65,67–70</sup> as dividing  $D_{\text{Li}^+, \text{calc}}$  by  $D_{\text{Li}^+, \text{meas}}$  yields  $(1 - \alpha)$ , the degree of Li ion dissociation (cf. Table 1). Note that the error margins given are based on error propagation of measurement

inaccuracies and membrane geometry, where a homogenous distribution of the constituent polymer species within the electrolyte membrane was assumed. It is estimated that roughly 30% of the lithium ions are dissociated, though no further trends can be extracted for different samples or different temperatures.

The degree of ion dissociation strongly depends on the polymer chemistry, most importantly on the choice of the coordinating anionic group, where particularly sulfonamides allow for high degrees of ion dissociation.<sup>13,14</sup> Nevertheless, lithium ion association may also occur with (other) functional groups of the polymer backbone or sidechains. For perfluoropolyether based electrolytes containing different end groups such as diol, dimethyl carbonate, ethoxy-diol, and ethoxy-dimethyl carbonate, respectively, and ca. 0.5 M LiTFSI as the electrolyte salt, corresponding degrees of lithium ion dissociation of 0.01 to 1 were reported, thereby clearly reflecting that lithium ion dissociation also depends on available polymer end groups (where polar end groups tend to increase the ion dissociation).<sup>67</sup> Therefore, a further increase of lithium ion dissociation may be achieved by tailoring the structure of the considered single ion conducting polymer or by changing the blend partner.

### 3.2 Thermal stability

TGA and DSC measurements were performed to analyze the thermal behavior and stability of the lithiated polymer powder. No thermal phase transformation or glass transition occurred within the observed temperature range between  $-150$  °C and  $150$  °C (Fig. 8a), while the TGA data (Fig. 8b) exhibited significant weight losses and a sharp peak in the derivative at  $449$  °C (starting at  $385$  °C) indicating the onset of thermal degradation of the polymer.

DSC measurements of the blend partner PVdDF-HFP, the solvent solution EC : PC (1 : 1, v/v), the “dry” and swollen membrane are shown in Fig. 9. For PVdF-HFP, a glass transition at  $-40$  °C, an  $\alpha$ -transition at  $50$  °C and a melting signal at  $148$  °C can be observed which are related to the thermal behavior of PVdF and are in good agreement with literature data.<sup>59,71</sup> For the “dry” membrane, a melting signal at  $143$  °C was also observed,

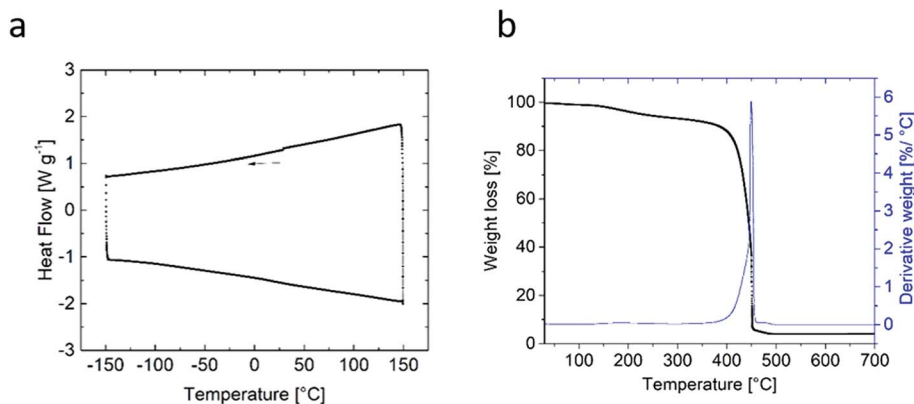


Fig. 8 (a) DSC and (b) TGA of the lithiated single ion conducting polymer powder.



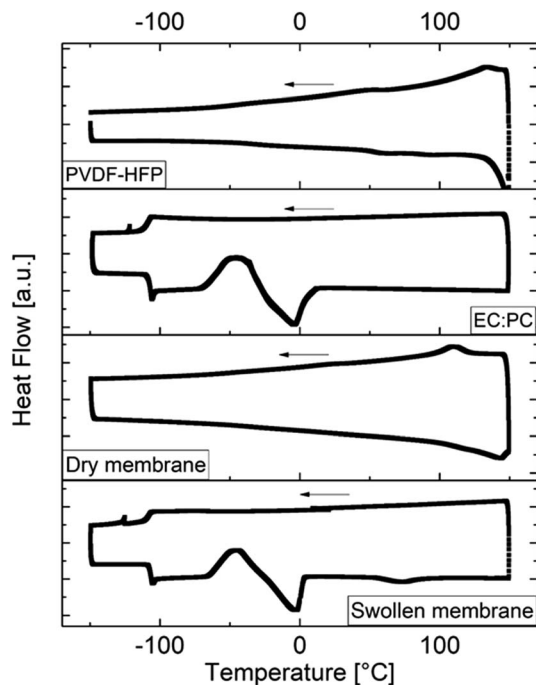


Fig. 9 DSC thermograms of PVdF-HFP, solvent solution (EC : PC), and dry and swollen SIPE membranes.

attributed to the melting temperature of the PVdF-HFP compound. A glass transition might be present at  $\approx -50$  °C and would be reasonable due to the glass transition of PVdF-HFP, which is shifted due to blending, though it cannot be clearly observed. The solvent solution shows a glass transition at  $-105.91$  °C, cold crystallization at  $-50$  °C and melting at  $-5$  °C.

In the case of the swollen membrane, identical signals compared to the solvent solution are present, in addition to a signal at  $73$  °C related to PVdF-HFP. The addition of a plasticizer significantly reduces the melting temperature of the crystalline phase of PVdF-HFP.<sup>59</sup> To estimate the influence of melting of the plasticized blend partner PVdF-HFP on the SIPE membrane, it was put onto a heating plate at  $80$  °C. The membrane increased its flexibility but maintained its shape, while ionic conductivity measurements of the SIPE performed between  $80$  °C and  $-40$  °C demonstrated reversible behavior (Section 3.1). A disassembly of the respective cells revealed that membrane dimensions do not change during the conductivity measurements. Hence, it may be concluded that the observed behavior does not restrict the application of the membranes for temperatures higher than  $73$  °C. Nevertheless, in future studies other polymers will be considered as blend partners for membrane fabrication, possibly allowing for improved thermal stability of the polymer blends.

### 3.3 Electrochemical investigations

**3.3.1 Electrochemical stability window (ESW).** The linear sweep voltammetry curve of the swollen SIPE membrane (1 : 3) is shown in Fig. 10. Oxidative stability, shown in red, was

determined vs. the Pt electrode and reductive stability (black) vs. Cu (both at  $20$  °C). The reduction curve shows the plating signal of metallic lithium in the low electrode potential range  $\approx 0$  V vs. Li/Li<sup>+</sup>. In the oxidative part, starting from ca.  $4.6$  V vs. Li/Li<sup>+</sup>, an exponential increase in current density occurs, illustrating the onset of degradation of the SIPE membrane.

Hence, the membrane is electrochemically stable up to  $4.6$  V vs. Li/Li<sup>+</sup>, implying compatibility with the most commonly applied active cathode materials, including LiCoO<sub>2</sub>, LiFePO<sub>4</sub>, LiN<sub>x</sub>M<sub>y</sub>Co<sub>z</sub>O<sub>2</sub> and LiNi<sub>x</sub>Co<sub>y</sub>Al<sub>z</sub>O<sub>2</sub>, respectively.<sup>72,73</sup> However, it should be noted that electrochemical stability investigations using rather inert working electrode materials may not directly reflect the actual electrochemical stability of the polymer electrolytes in application-oriented cell setups with typical cathode materials, e.g. due to different chemical environments.<sup>73</sup> Therefore, additional cycling investigations are required to demonstrate the electrochemical stability of the electrolyte material within a given cell setup.

**3.3.2 Lithium stripping and plating.** The major aim of developing polymer electrolytes for LIBs is the application of lithium metal cells in order to increase the safety of the cells while reducing dendrite growth compared to standard liquid electrolyte systems. Thus, the electrochemical stability of polymer electrolytes against lithium metal is mandatory and of high interest. To analyze the stability of the herein presented SIPE membrane against lithium metal, stripping plating experiments were performed in a symmetrical Li/Li cell at elevated temperature ( $60$  °C). A current density of  $0.1$  mA cm<sup>-2</sup> was applied for 1 hour per half cycle for a total of 1100 hours (550 full cycles). The obtained voltage-time response is shown in Fig. 11. During the first cycles, a slight decrease in voltage implying a decrease in resistance can be observed, likely attributed to the build-up of a (SEI like) surface layer on the lithium metal, e.g. due to some minor solvent decomposition reactions resulting in rougher electrode surfaces.<sup>4,74</sup> After this

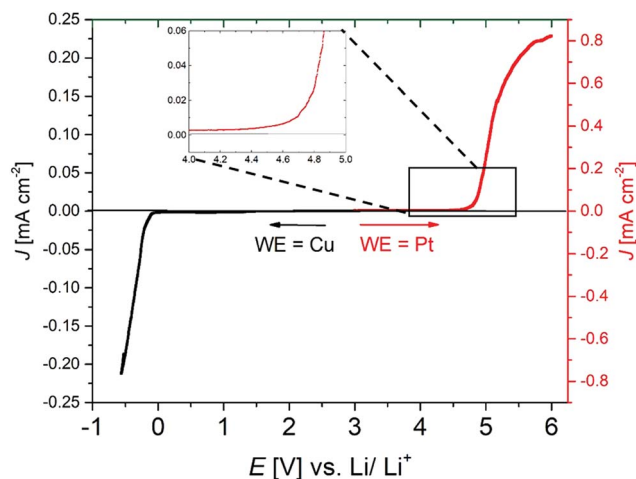


Fig. 10 Electrochemical stability window of the blend SIPE membrane measured in a three electrode setup (Li metal as the reference and counter electrode, platinum as the working electrode for oxidation and copper as the working electrode for reduction) at room temperature using a scan rate of  $80$   $\mu$  V s<sup>-1</sup>.



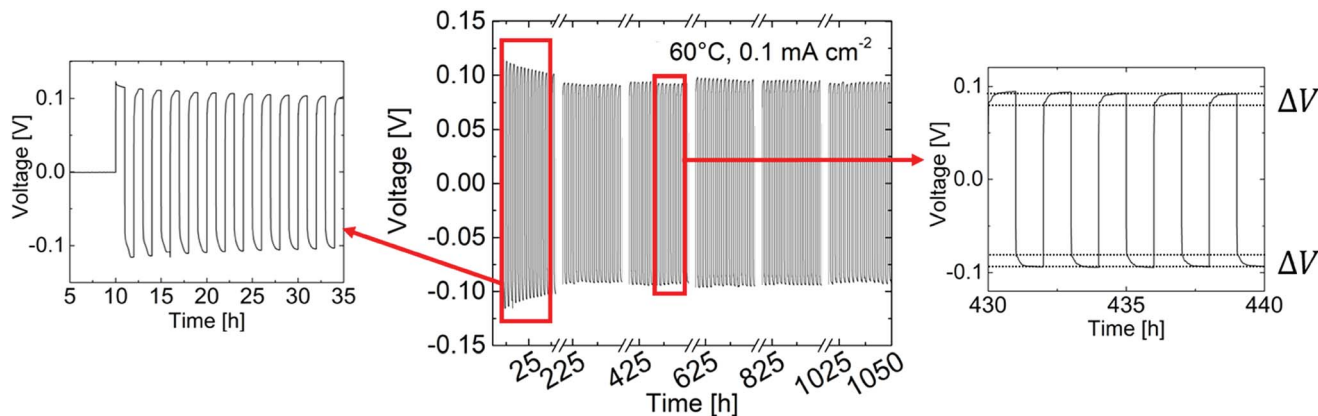


Fig. 11 Voltage versus time plot for a symmetrical lithium cell (Li metal/SIPE membrane/Li metal).

initial process, the voltage time profiles are rather stable and no significant changes of the peak voltages are monitored, demonstrating the high stability of the SIPE membrane against lithium metal electrodes.

**3.3.3 Cycling performance.** Single ion conducting polymer electrolyte membranes were already applied in LFP/lithium metal cells or  $\text{LiFePO}_4/\text{LiTi}_5\text{O}_{12}$  lithium ion cells,<sup>15,26,27,40–45,52,75</sup> despite the fact that the often used active material for lithium ion batteries constitutes  $\text{LiNi}_x\text{Mn}_y\text{Co}_z\text{O}_2$  (NMC), primarily due to its high energy density. To demonstrate the applicability of the presented SIPE membrane in a lithium metal cell, NMC111 was chosen as the cathode active material. Note that the interfacial resistance between the cathode and polymer membrane is significantly reduced upon addition of small amounts of lithiated monomer into the structure of the cathode. This may be explained by an increase in the volume fraction of the so-called *triple-phase contact boundaries* formed by the electronic conductor, lithium ion conductor and active material that comprise the sites for electrochemical reactions.<sup>44</sup> Rather than the lithiated monomer, 3 wt% of lithiated terephthalic acid was added to the cathode slurry, mainly due to its higher relative lithium content but also considering that lithiated terephthalic acid is practically insoluble in the solvent (EC : PC (1 : 1)) while being electrochemically stable in the relevant voltage range of 3 V–4.3 V vs.  $\text{Li}/\text{Li}^+$ . Fig. 12a and b show the cycling stability of NMC111/Li cells at 60 °C and 20 °C, respectively.

The first five cycles were performed at C/20, whereas for later cycles a charge/discharge rate of C/10 was applied. At both temperatures, the first cycle exhibited a reduced coulombic efficiency of 79.9% at 60 °C and 82.8% at 20 °C, which is well known from NMC/liquid electrolyte cell systems, and often attributed to structural changes, and formation of a solid permeable interphase (SPI) on the cathode electrolyte interphase (CEI),<sup>76–78</sup> as well as kinetically hindered re-lithiation of NMC.<sup>53,79,80</sup> For the following cycles, high coulombic efficiencies of 97.5% (60 °C) and 99.2% (20 °C) were observed. Note that at elevated temperatures, degradation mechanisms may take place faster resulting in better capacity retention for cells cycled at 20 °C. The specific capacity of the cells is higher at 60 °C ( $163 \text{ mA h g}^{-1}$  at 0.05C and  $161 \text{ mA h g}^{-1}$  at 0.1C) compared to 20 °C ( $142 \text{ mA h g}^{-1}$  at 0.05C and  $116 \text{ mA h g}^{-1}$  at 0.1C), in agreement with higher ionic conductivity of the electrolyte membrane at increased temperatures. Indeed, the presented cycling investigations emphasize the high oxidative stability of the SIPE membranes, similarly to the data from linear sweep voltammetry (Fig. 10), thereby demonstrating the compatibility of the SIPE membrane with the NMC active material.

Fig. 13 shows the voltage profiles obtained by cycling the NMC111/Li metal cells at different C-rates. Typical voltage profiles for the NMC material with gradually decreasing or increasing specific capacity could be observed. The voltage profiles and specific capacity values at 0.05C and 0.1C are

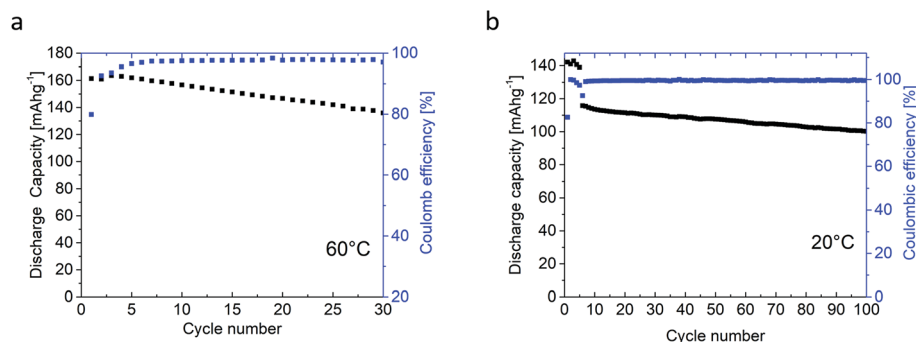


Fig. 12 Cycle stability of the NMC111/lithium metal cell with the polymer blend electrolyte membrane (a) at 60 °C and (b) at 20 °C.



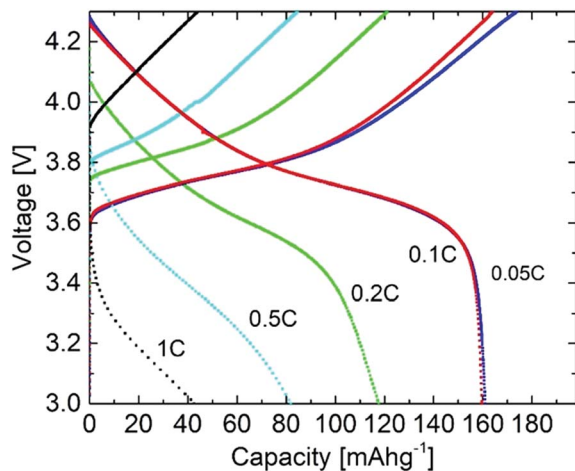


Fig. 13 Charge/discharge profiles of the NMC111/SIPE membrane/lithium metal cell obtained at different C-rates at 60 °C.

almost identical, despite higher over-potentials at increasing C-rates, leading to a decrease in specific capacity, *e.g.* due to interfacial resistances between the electrodes and SIPE membrane as well as due to rather low content of lithiated species within the cathode. Nevertheless, the actual rate performance should be further enhanced, *e.g.* by invoking different options such as optimization of the cathode composition or improvement of the electrolyte–electrode contacts. An analysis and better understanding of structure–interface relationships *via* spatially resolved (*in operando*) magnetic resonance imaging (MRI) techniques<sup>8†</sup> in principle could facilitate or contribute to the tailored design of electrolyte–electrode interfaces with improved cycling performance and cycling with higher C-rates, paving the way for even better electrochemical storage devices.

## 4. Conclusion

A new homopolymer is successfully prepared for application as a single ion conducting polymer electrolyte in lithium ion or lithium metal batteries. The polymer structure was tailored by introducing a functional C(CF<sub>3</sub>)<sub>2</sub> group into the polymer backbone, thereby improving the solubility behavior such that an optimized synthesis affording a pure and solvent free product could be performed. Optimized gel-type blend polymer electrolyte membranes were produced by variation of the PVDF-HFP to single ion conducting polymer ratio, where higher fractions of SIPE significantly increased the achievable ionic conductivity and lithium ion diffusivity, despite the fact that the corresponding solvent uptake was reduced. A ratio of PVDF-HFP to the fluorinated single ion conducting polymer of 1 : 3 was found to be ideal, resulting in flexible membranes with a high ionic conductivity of 0.5 mS cm<sup>-1</sup> at 20 °C, a corresponding transference number of 0.9 (that indeed reflects single-ion conducting behavior) and a <sup>7</sup>Li self-diffusion coefficient of 4.6 × 10<sup>-11</sup> m<sup>2</sup> s<sup>-1</sup> at 20 °C, respectively. Based on the obtained ion transport properties, a lithium ion dissociation degree of 30% was estimated. The long-term stability of the polymer electrolyte

membrane against lithium metal and, in contrast to previous studies considering LFP as the cathode material, its applicability in NMC/lithium metal cells was demonstrated by cycling investigations, both performed at 20 °C as well as at 60 °C, highlighting the great potential of the introduced materials.

## Conflicts of interest

There are no conflicts to declare.

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