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Efficient removal of crystal violet dye using EDTA/graphene oxide functionalized corncob: a novel low cost adsorbent†

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In this study, EDTA functionalized corncob (EDTA-corn-cob) and EDTA/graphene oxide functionalized corncob (EDTA-GO/corn-cob) were prepared using disodium ethylenediamine tetraacetic acid and the graphene oxide immersion method. EDTA-corn-cob and EDTA-GO/corn-cob were characterized by SEM and FTIR spectroscopy. On this basis, the adsorption properties of EDTA-corn-cob and EDTA-GO/corn-cob were studied with crystal violet as the adsorbate. The optimum adsorption conditions were determined by the effect of samples on the adsorption properties of crystal violet at different times, temperatures and pH, and the reusability of the samples was studied. The results showed that adsorption capacity of crystal violet on EDTA-GO/corn-cob was higher compared with natural corncob and EDTA-corn-cob. The most suitable pH value of the solution is about 6.0, the adsorption equilibrium time is 200 min. EDTA-GO/corn-cob can be reused eight times. This study indicated that EDTA-GO/corn-cob is a reusable adsorbent for rapid, low-cost, and efficient removal of dye from waste water.

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1 Introduce

Water pollution is one of the major environmental problems nowadays.¹ Dyes are one of the important and basic pollutants in water pollution. With the accelerated process of industrialization development, more and more wastewater containing dyes is discharged from various human activities and causes serious threats to the environment.²⁻⁴

A wide range of physicochemical techniques, such as electrocoagulation, photocatalytic process, flocculation, ozonation, adsorption, and membrane filtration, have been employed to dispose of the wastewater.⁵⁻¹⁰ Among these various purification treatments, liquid-phase adsorption is believed to be the most effective way to remove organic dyes from wastewater. A variety of materials, which include chitosan,¹¹ leaves,¹² crab shell,¹³ waste coal gangue,¹⁴ peach gum polysaccharide,¹⁵ ganoderma lucidum,¹⁶ clays,¹⁷ and *Cucumis sativus* peel,¹⁸ were prepared or used as adsorbents for removal of dyes from water.

Biomass waste, such as corncob, has great potential to form inexpensive and environmental friendly adsorbents due to the large quantities produced, chemical and mechanical stability, high surface area and structural properties. But generally the adsorption capacity of natural corncob is not ideal. Therefore, many

modification methods have been invented to increase the capacity of corncob based adsorbents.^{19,20} Ma *et al.* reported that corncob was converted into a novel magnetic adsorbent (MCA) for removal of anionic and cationic dyes.¹⁹ Mesoporous activated carbon that was prepared from corncob was used as adsorbent for removal of ammonium from groundwater.²⁰ Hyperbranched polyamide modified corncob was synthesized and used as adsorbent for Cr(vi) with maximum adsorption capacity that could reach up to 131.6 mg g⁻¹.²¹ EDTA is a kind of complexing agent, EDTA-modified may produce adsorbents with strong metal-complexing property, thus, EDTA-modified materials have been widely used for heavy metal and dyes removal, such as bamboo activated carbon,²² β -cyclodextrin/chitosan,²³ electrospun polyacrylonitrile nanofibers.²⁴ Since the graphene was first reported in 2004, it has been widely investigated due to its excellent electrical conductivity, thermal stability, mechanical strength and adsorption capacity.^{25,26}

In this study, in addition to introducing EDTA onto corncob for enhancing adsorption capacity, graphene oxide would be also added. EDTA functionalized corncob (EDTA-corn-cob) and EDTA/graphene oxide functionalized corncob (EDTA-GO/corn-cob) were prepared successfully used to remove various dyes from water. Methylene blue, crystal violet, acridine orange, methyl red, acid chrome blue K, rhodamine B and orange IV, as typical anionic and cationic dye, were selected as the pollutants. At meantime, to fully understand the adsorption behavior of EDTA-corn-cob and EDTA-GO/corn-cob, studies were carried out under various parameters such as adsorbent dosage, pH, contact time. Adsorption kinetics of EDTA-corn-cob and EDTA-GO/corn-cob were investigated by pseudo first order model

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† Electronic supplementary information (ESI) available: Fig. S1 The pseudo first-order kinetics model. Fig. S2 The pseudo second-order kinetics model. See DOI: 10.1039/c9ra04003j



and pseudo second order model, respectively. Furthermore, the equilibrium data of EDTA-corn cob and EDTA-GO/corn cob were analyzed by Langmuir, Freundlich and Sips model, respectively. The reusability on adsorption capacity of EDTA-corn cob and EDTA-GO/corn cob were also tested. Our results demonstrate that EDTA-GO/corn cob is a cheap and efficient adsorbent for removal of dye in aqueous media.

2 Experimental section

2.1 Materials

Flake graphite (99.95%) was supplied by Qingdao Chenyang Graphite Co., Ltd. (Qingdao, China). Corn cob was purchased from Deep Processing of Huifeng Straw Agricultural Products (Lianyungang, China). Ethylenediamine tetraacetic acid, were purchased from the National Medicine Group Chemical Reagent Co., Ltd. (Shanghai, China). Acridine orange, methyl red, crystal violet, rhodamine B, orange IV, acidic chrome blue K and methylene blue were purchased from the Aladdin Chemical Reagent Co., Ltd. (Shanghai, China), and the other reagents were of analytical grade.

GO was prepared from the flake graphite powder using a modified Hummers–Offeman method.²⁷

2.2 Preparation of adsorbent

2.2.1 Pretreatment of corn cob. The corn cobs were washed with tap water and distilled water carefully to remove surface impurities and dried at 55 °C. Then the dried corn cobs were crushed by a grinder to obtain corn cob powder for storage.

10.0 g of corn cob powder was immersed in 20% isopropanol solution, stirred for 24 hours, filtered, washed with 20% isopropanol and distilled water to be colorless, dried for 24 hours at 55 °C, then added 0.1 mol L⁻¹ of sodium hydroxide solution to the sample, stirred for 1 hour at room temperature, filtered, then added distilled water to stir for 45 minutes, washed repeatedly to pH 7.0, and filtered. The obtained products were dried at 55 °C for storage.

2.2.2 Preparation of EDTA functionalized corn cob/graphene oxide. The pretreated corn cob powder was soaked in 2.5% EDTA solution for 24 hours, filtered and washed with distilled water, and dried at 55 °C. The obtained products were EDTA-corn cob.

0.10 g of GO was dispersed in 2.5% EDTA solution under ultrasound. Then the pretreated corn cob powder was soaked in 2.5% EDTA/GO solution. After 24 hours, it was filtered and washed with distilled water. The EDTA-GO/corn cob sample was dried at 55 °C and stored for reserve.

2.3 Characterization of materials

Fourier infrared spectrometry (FT-IR) of GO, corn cob, EDTA-corn cob and EDTA-GO/corn cob were obtained using a Nicolet iS10 FT-IR spectrophotometer (Thermo Fisher Scientific, USA). Scanning electron microscope of corn cob and EDTA-GO/corn cob were carried out by an EVO MA10 scanning electron microscope (ZEISS, Germany). Zeta potential of EDTA-corn cob and EDTA-GO/corn cob were carried out on Zetasizer Nano Series (Malvern, British).

2.4 Adsorption experiments

2.4.1 Comparison of adsorption capacity. Seven copies of 0.0100 g EDTA-GO/corn cob were added to 25.00 mL of methylene blue, crystal violet, acridine orange, methyl red, acid chrome blue K, rhodamine B and orange IV with initial concentrations 20 mg L⁻¹, respectively. Then, 0.0100 g of corn cob and 0.0100 g of EDTA-corn cob were studied in the same fashion with the above steps. All flasks were shaken at 298 K to reach adsorption equilibrium. After that, absorbance of methylene blue, crystal violet, acridine orange, methyl red, acid chrome blue K, rhodamine B and orange IV in supernatant were determined by UV-Vis spectrophotometer at 662 nm, 582 nm, 490 nm, 435 nm, 524 nm, 554 nm and 443 nm, respectively. The adsorption capacity (q_e , expressed in mg g⁻¹) was calculated according to formula (1).

$$q_e = \frac{(C_0 - C_e) \times V}{m} \quad (1)$$

where C_e is the equilibrium concentration (mg L⁻¹), C_0 is the initial concentration (mg L⁻¹), V is the solution volume (L), m is the weight of the adsorbent (g).

2.4.2 Effect of pH on adsorption capacity. Effect of pH on adsorption capacity of 0.0100 g of EDTA/corn cob and 0.0100 g of EDTA-GO/corn cob were carried out and the initial concentration of crystal violet was set as 20 mg L⁻¹ with varying pH at 298 K. After reach to adsorption equilibrium, the other steps were studied in the same fashion with the 2.4.1 comparison of adsorption capacity.

2.4.3 Adsorption kinetics. 0.1000 g of EDTA-GO/corn cob was added to 250 mL crystal violet solution with initial concentrations 40 mg L⁻¹ at pH 6.09. The flask was shaken at 298 K to reach adsorption equilibrium. Then the absorbance of crystal violet in supernatant at different time intervals were determined by UV-Vis spectrophotometer at 582 nm. Each experiment was repeated three times. The capacity of crystal violet adsorbed (q_t , expressed in mg g⁻¹) was calculated according to the formula (2):

$$q_t = \frac{(C_0 - C_t) \times V}{m} \quad (2)$$

where C_0 and C_t are the initial and temporary concentration of the dye (mg L⁻¹), m is the weight of the adsorbent (g), and V is the solution volume (L).

2.4.4 Adsorption isotherm. Adsorption isotherm studies were carried out with 25 mL of crystal violet with the initial concentrations ranging from 20 to 140 mg L⁻¹. Adsorptions onto 0.0100 g of EDTA/corn cob and 0.0100 g of EDTA-GO/corn cob were carried out at 298 K with varying initial concentration at pH 6.09. After reach to adsorption equilibrium, the other steps are the same as the adsorption kinetics.

The influence of ionic strength on the adsorption of crystal violet on EDTA/corn cob and EDTA-GO/corn cob was studied in the same fashion with the adsorption isotherm, except that sodium chloride was varied and the initial concentration of crystal violet was set as 40 mg L⁻¹.

2.4.5 Recycling experiments. The adsorption experiment was conducted with initial concentration of crystal violet was set



as 40 mg g^{-1} with 0.01 g of EDTA-GO/corncob at pH 6.09. After 8 h, the absorbance of crystal violet in supernatant was determined at 582 nm while the EDTA-GO/corncob was desorbed with ethanol for 5 h. Then EDTA-GO/corncob was filtered and washed repeatedly with distilled water. Finally, they were dried in vacuum oven at $55 \text{ }^\circ\text{C}$. Recycling experiments of EDTA/corncob were studied in the same fashion with EDTA-GO/corncob. According to the above steps, the adsorption/desorption were repeated nine times. The capacity of crystal violet adsorbed (q_e , expressed in mg g^{-1}) was calculated according to the formula (1).

3 Results and discussion

3.1 Characterization of materials

Scanning electron microscope (SEM) for corn cob and EDTA-GO/corncob is shown in Fig. 1. The structure of corn cob (Fig. 1a and c) and EDTA-GO/corncob (Fig. 1b and d) were clearly revealed by SEM investigations. The SEM micrograph of corn cob shows porous surface structure (Fig. 1a and c). Comparing to the SEM images of corn cob, EDTA-GO/corncob is mainly lamellar structure.

The FTIR spectra of GO, corn cob, EDTA-corn cob and EDTA-GO/corn cob are shown in Fig. 2. The characteristic peaks for GO appear at 1110 , 1580 , 1650 and 3450 cm^{-1} which correspond to stretching vibrations of C–O–C, C=C, C=O and –OH bonds, respectively (Fig. 2a). The EDTA-GO/corn cob and EDTA-corn cob presented peaks for N–H ($\nu_{\text{N-H}}$, 3450 cm^{-1}), C=O ($\nu_{\text{C=O}}$, 1660 cm^{-1}), N–H ($\delta_{\text{N-H}}$, 1590 cm^{-1}) and C–O–C ($\nu_{\text{C-O-C}}$, 1110 cm^{-1}), all these functional groups are expected from EDTA and GO (Fig. 2c and d). These peaks at 1110 and 1660 cm^{-1} are not present in the spectra of unmodified corn cob (Fig. 2b), indicating that EDTA and GO are attached successfully on the surface of EDTA-GO/corn cob.

3.2 Adsorption experiment

3.2.1 Effect of dyes on adsorption capacity. Effect of methylene blue, crystal violet, acridine orange, methyl red, acid chrome blue K, rhodamine B and orange IV on adsorption capacity of corn cob, EDTA-corn cob and EDTA-GO/corn cob are shown in Fig. 3. It can be seen that corn cob, EDTA-corn cob and EDTA-GO/corn cob can adsorb the seven dyes. Adsorption capacity of the seven dyes on corn cob and EDTA-corn cob are litter, while adsorption capacity of the seven dyes on EDTA-GO/

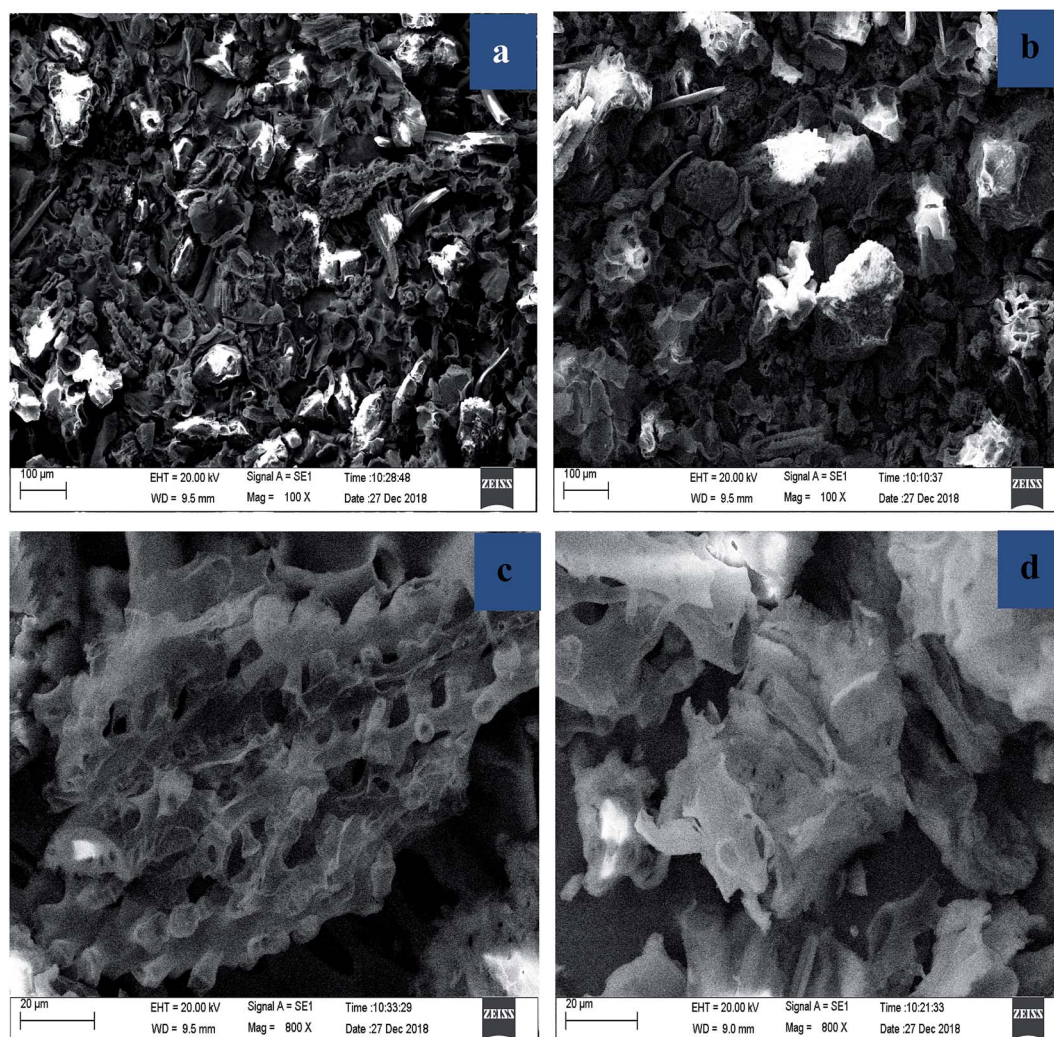


Fig. 1 SEM of corn cob (a and c) and EDTA-GO/corn cob (b and d).



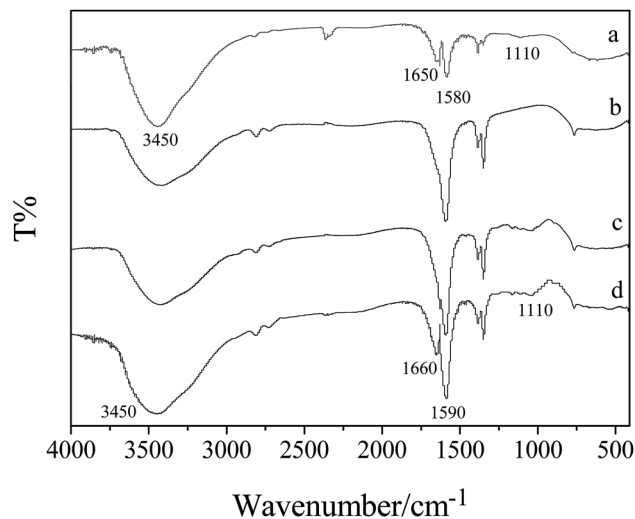


Fig. 2 FTIR spectra of adsorbents. (a) GO; (b) corncob; (c) EDTA/corncob; (d) EDTA-GO/corncob.

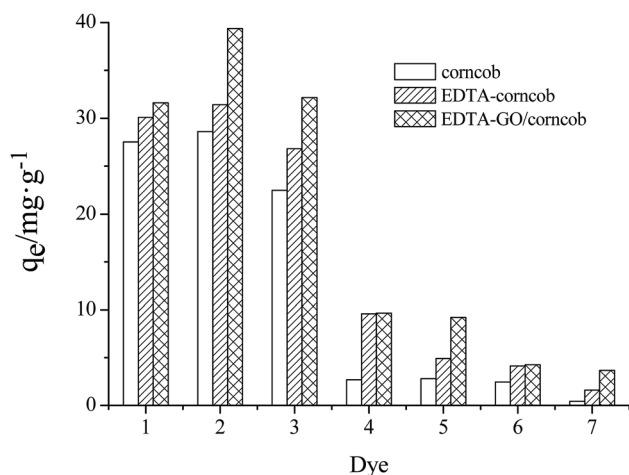


Fig. 3 Comparisons of adsorption capacity (pH = 7.0) (1) methylene blue; (2) crystal violet; (3) acridine orange; (4) methyl red; (5) acid chrome blue K; (6) rhodamine B; (7) orange IV.

corn-cob are higher than corncob and EDTA-corn-cob. Especially, the adsorption capacity of crystal violet on EDTA-GO/corn-cob is the most. So crystal violet was chosen as the object dye in the following experiments. Chemical structure of crystal violet is shown in Fig. 4.

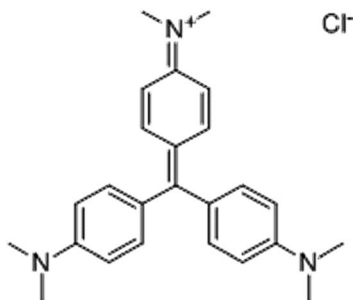


Fig. 4 Chemical structure of crystal violet.

3.2.2 Adsorption kinetics. Fig. 5 showed the adsorption capacity of crystal violet on EDTA-corn-cob and EDTA-GO/corn-cob *versus* adsorption time at 298 K. According to the kinetics data (Fig. 5), the adsorption capacity of crystal violet on EDTA-corn-cob and EDTA-GO/corn-cob increased very fast at 0–100 min and reached equilibrium at 200 min.

In order to explain the adsorption mechanism, the adsorption kinetic data of crystal violet on EDTA-corn-cob and EDTA-GO/corn-cob were treated with pseudo-first-order and pseudo-second-order models, as shown in Fig. S1 and S2 (ESI†), and the experimental data was listed in Table 1.

The pseudo first-order kinetics model (eqn (3)) and the pseudo-second-order kinetics model (eqn (4)) can be expressed as follows:

$$\log(q_e - q_t) = \log q_e - K_1 \frac{t}{2.303} \quad (3)$$

$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{t}{q_e} \quad (4)$$

where q_e and q_t are the capacity of the dye adsorbed on the adsorbents at equilibrium and at time t (mg g^{-1}), respectively, K_1 (min^{-1}) and K_2 ($\text{g mg}^{-1} \text{min}^{-1}$) are the rate constant of pseudo-first-order and pseudo-second-order kinetics models.

As listed in Table 1, the adsorption kinetics of EDTA-corn-cob and EDTA-GO/corn-cob were nicely described by pseudo-second-order model ($R = 0.99$) and the calculated q_e was very close to the experimental q_e . This indicated that chemisorption or chemical bonding between active sites of EDTA-corn-cob and EDTA-GO/corn-cob and crystal violet might dominate the adsorption process.

3.2.3 Adsorption isotherms. The adsorption isotherms of crystal violet on EDTA-corn-cob and EDTA-GO/corn-cob were studied at 298 K in Fig. 6. The adsorption capacity of the crystal violet on EDTA-corn-cob and EDTA-GO/corn-cob reaches the maximum as the initial concentration of the crystal violet increase gradually as shown in Fig. 6.

The experimental adsorption equilibrium results on EDTA-corn-cob and EDTA-GO/corn-cob were fitted by the Langmuir model (eqn (5) and (6)), Freundlich isotherm model (eqn (7))

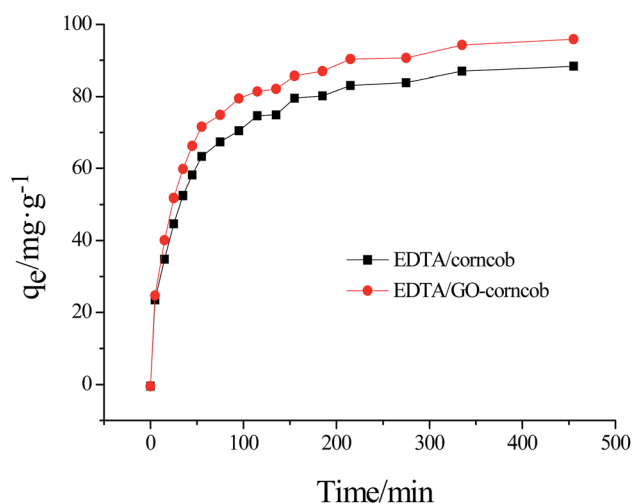


Fig. 5 Adsorption kinetics.



Table 1 Kinetic parameters for the adsorption of crystal violet on EDTA/corn cob and EDTA-GO/corn cob at 298 K

Adsorbent	$q_{e,eq}/\text{mg g}^{-1}$	Pseudo-first-order kinetics model			Pseudo-second-order kinetics model		
		$K_1 (\times 10 \text{ min}^{-1})$	$q_e/\text{mg g}^{-1}$	R	$K_2 (\times 10^2 \text{ g mg}^{-1} \text{ min}^{-1})$	$q_e/\text{mg g}^{-1}$	R
EDTA/corn cob	88.33	0.1497	67.74	0.9231	0.05535	88.50	0.9949
EDTA-GO/corn cob	95.87	0.1566	71.12	0.9421	0.05171	95.24	0.9981

and Sips model (eqn (8)). The Langmuir model base on three assumptions:²⁸ (1) the adsorption of molecule is a monolayer adsorption; (2) the adsorption of adsorbent surface is uniform; (3) there is no interaction among adsorbed molecules. The Freundlich model assumes that the adsorption surface is heterogeneous, that interactions between adsorbed molecules can occur, and that multilayer adsorption is possible. Sips model is an improved Langmuir model.

$$q_e = \frac{q_m C_e}{K_d + C_e} \quad (5)$$

$$\frac{C_e}{q_e} = \frac{1}{q_m K_L} + \frac{C_e}{q_m} \quad (6)$$

$$\log q_e = \log K_F + \left[\frac{1}{n}\right] \log C_e \quad (7)$$

$$q_e = \frac{q_m K_S C_e^{m_S}}{1 + K_S C_e^{m_S}} \quad (8)$$

where q_e , C_e , K_L , q_m and K_d are the equilibrium adsorption capacity (mg g^{-1}), the equilibrium concentration (mg L^{-1}), Langmuir adsorption constant, the maximum adsorption capacity (mg g^{-1}) and effective dissociation constant. K_F is the Freundlich adsorption coefficient, which is related to the dosage and properties of adsorbent, the properties and temperature of adsorbate, n is the Freundlich constant, which is related to the nature of adsorption system. K_S is the Sips adsorption coefficient, m_S is the Sips constant, which indicates the heterogeneity of adsorbent. The closer the m_S value is to 1, the more homogeneous the adsorbent surface is.²⁹

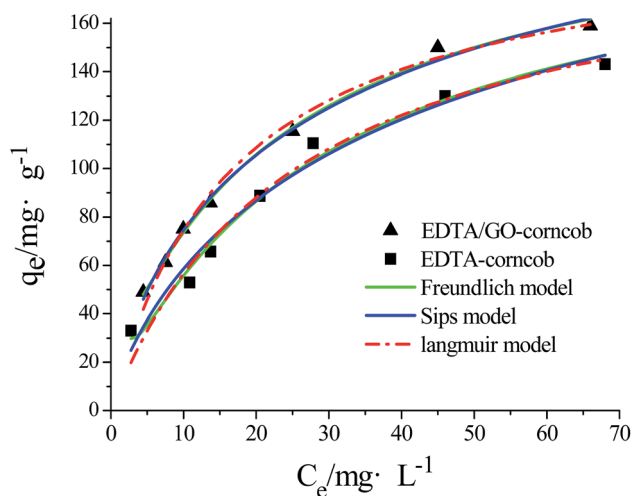


Fig. 6 Adsorption isotherms.

The Freundlich model provided a slightly better fit for the adsorption data of crystal violet onto EDTA-corn cob and EDTA-GO/corn cob (Table 2) than Langmuir model and Sips model. Therefore, the adsorption of crystal violet onto EDTA-corn cob and EDTA-GO/corn cob is heterogeneous adsorptions.

A comparison of the maximum adsorption capacities (q_m) of EDTA-corn cob and EDTA-GO/corn cob for crystal violet are listed in Table 3 with literature values of q_m of other adsorbents. It can be seen that the maximum adsorption capacities of EDTA-corn cob and EDTA-GO/corn cob for crystal violet are higher than that of other materials which might be attributed to the higher specific surface area of graphene and the EDTA groups.

3.3 Adsorption mechanism

The pH of solution affects the surface charge of the adsorbents as well as the degree of ionization of pollutants. Change of pH value affects the adsorptive process through dissociation of functional groups on the adsorbent surface active site.³⁸

The impact of initial pH in the range of 2.0–10.0 on crystal violet adsorption by the EDTA/corn cob and EDTA-GO/corn cob are shown in Fig. 7a. The highest adsorption capacities of crystal violet on EDTA/corn cob and EDTA-GO/corn cob were detected at pH of 6.0. The adsorption of crystal violet on EDTA/corn cob and EDTA-GO/corn cob are pH dependent, the adsorption capacity of crystal violet on EDTA/corn cob and EDTA-GO/corn cob increases with the increase of pH ($\text{pH} < 6.0$), but the adsorption capacity of crystal violet on EDTA/corn cob and EDTA-GO/corn cob decreases with the increase of pH ($\text{pH} > 6.0$).

The results may be attributed to the electrostatic attraction between the anions on the adsorbent and the cations on the dye. Fig. 7b showed the zeta potentials of EDTA/corn cob and EDTA-GO/corn cob. As shown in Fig. 7b, the isoelectric point (pH_{zpc}) of EDTA/corn cob and EDTA-GO/corn cob are 2.05 and 1.98, respectively. At low pH ($\text{pH} > 2.05$), the surface of EDTA/corn cob is negative charge because of the $-\text{COO}^-$ groups on the surface of EDTA/corn cob. At low pH ($\text{pH} > 1.98$), the surface of EDTA-GO/corn cob is negative charge, which is attributed to more $-\text{COO}^-$ groups. The negative charge on the surface of EDTA/corn cob and EDTA-GO/corn cob increases from pH 2.0 to 6.0 and then decreases with the increase of pH, and reaches the maximum at pH 6.0. The surface of acridine orange is positive charge. At pH around 6.0, the electrostatic interaction between crystal violet and EDTA/corn cob or EDTA-GO/corn cob is strongest, so the adsorption capacity of crystal violet on the adsorbents reaches the maximum.

The effect of ionic strength on the adsorption of crystal violet on EDTA/corn cob or EDTA-GO/corn cob were studied by carried out a series of experiments at NaCl solutions (0.00, 0.02, 0.04,



Table 2 Adsorption isotherm parameters of crystal violet onto on EDTA/corn cob and EDTA-GO/corn cob at 298 K

Adsorbent	Langmuir model			Freundlich model			Sips model		
	$q_m/\text{mg g}^{-1}$	K_d	R	$K_F \text{ mg}^{-1} \text{ g}^{-1}$	n	R	K_S	m_S	R
EDTA/corn cob	185.2	20.81	0.9494	18.08	1.943	0.9808	0.01798	0.6117	0.9538
EDTA-GO/corn cob	203.9	16.54	0.9929	22.91	1.985	0.9982	0.03865	0.5864	0.9981

Table 3 Comparison of maximum adsorption capacities of different adsorbents (298 K)

Adsorbent	Dye	$q_m/\text{mg g}^{-1}$	Ref.
AC-AgNPLs	Crystal violet	87.2	30
Chitosan/nanodiopside nanocomposite	Crystal violet	104.66	31
Gum Arabic-cl-poly(acrylamide) nanohydrogel	Crystal violet	90.90	32
ZVI-GAM	Crystal violet	172.41	33
Chitin nanowhiskers	Crystal violet	39.56	34
Zinc oxide nanorods loaded on activated carbon	Crystal violet	113.64	35
Surfactant modified magnetic nanoadsorbent	Crystal violet	166.67	36
NH ₂ -MIL-125(Ti) modified MOF	Crystal violet	129.87	37
EDTA/corn cob	Crystal violet	185.2	This work
EDTA-GO/corn cob	Crystal violet	203.9	This work

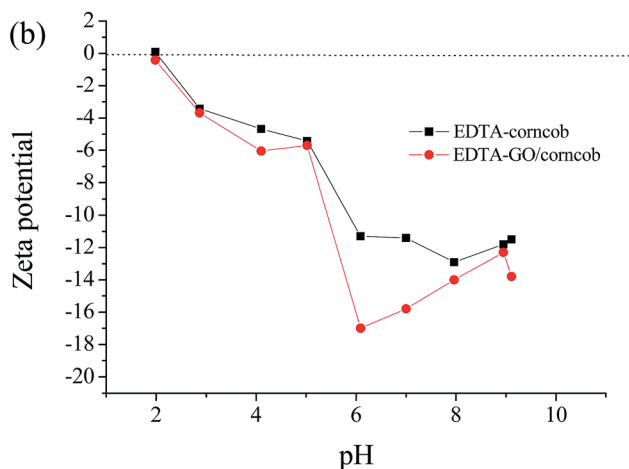
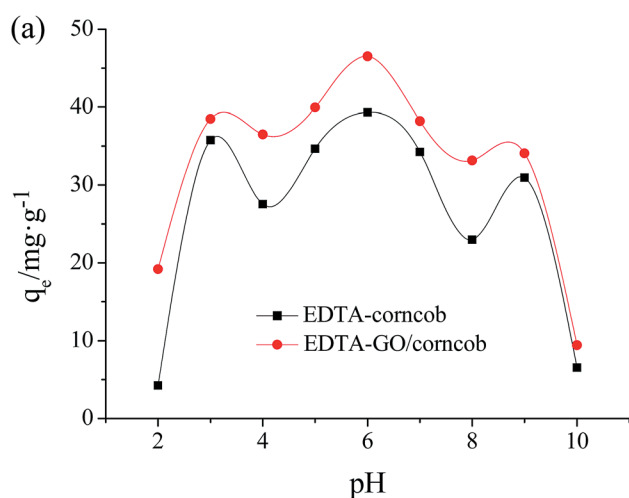


Fig. 7 (a) Effect of pH on the adsorption capacity. (b) Zeta potential at the different pH.

0.06, 0.08, 0.10 mol L⁻¹), and solution pH was adjusted to 6.0 before adsorption. The results are shown in Fig. 8. It is observed that the adsorption capacity of crystal violet on EDTA/corn cob or EDTA-GO/corn cob under the condition of 0.10 M NaCl remains 81.31% and 82.63% that of without addition of NaCl. The adsorption processes of crystal violet on EDTA/corn cob or EDTA-GO/corn cob are dependent on NaCl concentrations, which showed that electrostatic attraction dominates the adsorption process. The interaction mechanisms of crystal violet adsorption with EDTA/corn cob and EDTA-GO/corn cob were showed in Fig. 9.

3.4 Adsorbent recycling

Taking into account the practical application, the adsorption capacity and the reusability property are two key parameters to

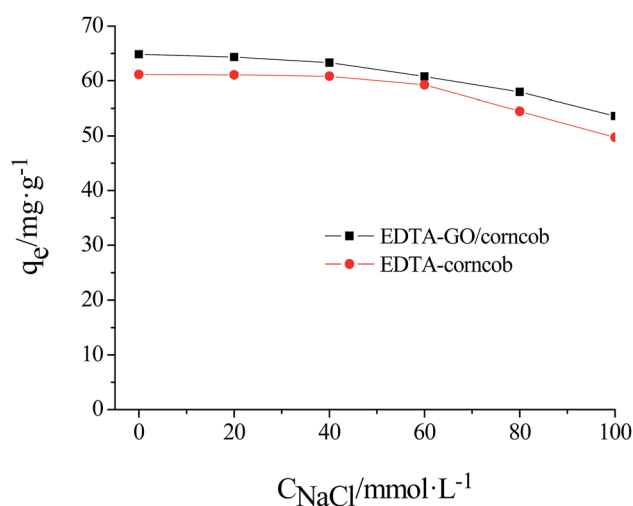


Fig. 8 Effect of NaCl on the adsorption capacity.



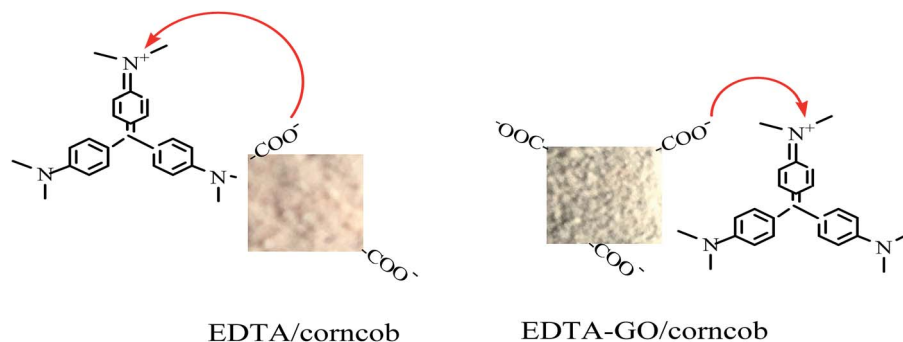


Fig. 9 The interaction mechanisms.

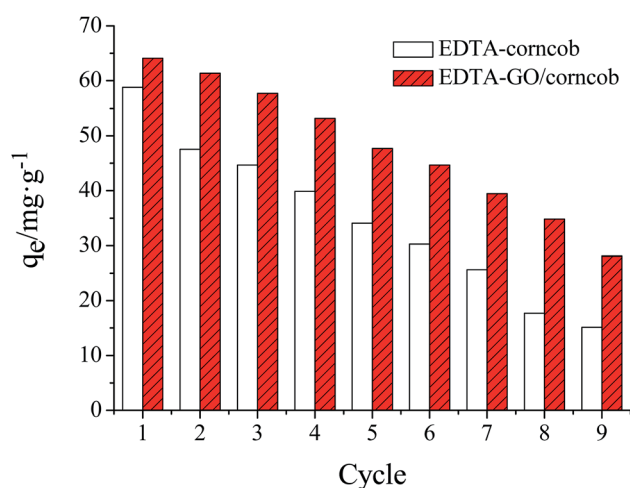


Fig. 10 Reusability of EDTA/corncob and EDTA-GO/corncob.

evaluate an adsorbent. An ideal adsorbent should not only possess higher adsorption capability, but also show better reusability property, which will significantly reduce the overall cost for the adsorbents.³⁹

Reusability of EDTA/corncob or EDTA-GO/corncob is shown in Fig. 10. The crystal violet solutions with the concentration of 40 mg L^{-1} were prepared and EDTA/corncob or EDTA-GO/corncob was recycled for nine times to investigate the adsorption cycle number of EDTA/corncob or EDTA-GO/corncob. At the first adsorption equilibrium, the maximum adsorption capacity of EDTA/corncob or EDTA-GO/corncob was 58.8 and 64.1 mg g^{-1} , respectively. With the increase of cycle number, the adsorption capacity showed a trend of decreasing. The adsorption capacity of EDTA/corncob was 30.3 mg g^{-1} at the sixth adsorption, while the maximum adsorption capacity of EDTA-GO/corncob is 28.1 mg g^{-1} at the ninth adsorption. This result showed that EDTA/corncob can be reused for five times and EDTA-GO/corncob can be reused for eight times.

4 Conclusions

In summary, EDTA/corncob and EDTA-GO/corncob were prepared successful and could be used as an efficient and recyclable adsorbent for crystal violet. The adsorption capacity

of crystal violet on EDTA-GO/corncob is higher than EDTA/corncob. The most suitable pH of adsorption of crystal violet on EDTA-GO/corncob was around 6.0. The adsorption equilibration time was 200 minutes. The adsorption kinetics fit well with pseudo-second-order model and the adsorption isotherm fit well with Freundlich isotherm model. Adsorption mechanism of crystal violet on EDTA/corncob and EDTA-GO/corncob were electrostatic attraction. EDTA/corncob can be reused for five times and EDTA-GO/corncob can be reused for eight times. The facile regeneration of EDTA-GO/corncob definitely could reduce the operating cost. We believe that EDTA-GO/corncob will have potentially wide application in the removal of dye pollutants from aquatic systems.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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References

- M. G. Dosskey, *Environ. Manage.*, 2001, **28**, 577–598.
- A. J. Jafari, B. Kakavandi, R. R. Kalantary, H. Gharibi, A. Asadi, A. Azari, A. A. Babaei and A. Takdastan, *Korean J. Chem. Eng.*, 2016, **33**(10), 2878–2890.
- K. Shakir, A. F. Elkafrawy, H. F. G. Shokry, G. E. Beheir and M. Refaat, *Water Res.*, 2010, **44**(5), 1449–1461.
- H. Zhang, Q. Luan, H. Tang, F. Huang, M. Zheng, Q. Deng, X. Xiang, C. Yang, J. Shi, C. Zheng and Q. Zhou, *Cellulose*, 2017, **24**(2), 903–914.
- J. Núñez, M. Yeber, N. Cisternas, R. Thibaut, P. Medina and C. Carrasco, *J. Hazard. Mater.*, 2019, **371**, 705–711.



- 6 K. Sirirerkratana, P. Kemacheevakul and S. Chuangchote, *J. Cleaner Prod.*, 2019, **215**, 123–130.
- 7 Q. Y. Yue, B. Y. Gao, Y. Wang, H. Zhang, X. Sun, S. G. Wang and R. R. Gu, *J. Hazard. Mater.*, 2008, **152**(1), 221–227.
- 8 J. Liang, X. A. Ning, J. Sun, J. Song, Y. Hong and H. Cai, *J. Cleaner Prod.*, 2018, **204**, 12–19.
- 9 I. Chaari, E. Fakhfakh, M. Medhioub and F. Jamoussi, *J. Mol. Struct.*, 2019, **1179**, 672–677.
- 10 N. Nikoee and E. Saljoughi, *Appl. Surf. Sci.*, 2017, **413**, 41–49.
- 11 J. Zhao, Z. Zou, R. Ren, X. Sui, Z. Mao, H. Xu, Y. Zhong, L. Zhang and B. Wang, *Eur. Polym. J.*, 2018, **108**, 212–218.
- 12 N. A. H. M. Zaidi, L. B. L. Lim and A. Usman, *Environmental Technology & Innovation*, 2019, **13**, 211–223.
- 13 L. Dai, W. Zhu, L. He, F. Tan, N. Zhu, Q. Zhou, M. He and G. Hu, *Bioresour. Technol.*, 2018, **267**, 510–516.
- 14 L. Zhou, H. Zhou, Y. Hu, S. Yan and J. Yang, *J. Environ. Manage.*, 2019, **234**, 245–252.
- 15 Y. Song, J. Tan, G. Wang and L. Zhou, *Carbohydr. Polym.*, 2018, **199**, 178–185.
- 16 J. Wu, T. Zhang, C. Chen, L. Feng, X. Su, L. Zhou, Y. Chen, A. Xia and X. Wang, *Bioresour. Technol.*, 2018, **266**, 134–138.
- 17 N. Abidi, J. Duplay, A. Jada, E. Errais, M. Ghazi, K. Semhi and M. Trabelsi-Ayadi, *C. R. Chim.*, 2019, **22**(2–3), 113–125.
- 18 S. Shakoore and A. Nasar, *Groundwater for Sustainable Development*, 2017, **5**, 152–159.
- 19 H. Ma, J. B. Li, W. W. Liu, M. Miao, B. J. Cheng and S. W. Zhu, *Bioresour. Technol.*, 2015, **190**, 13–20.
- 20 M. T. Vu, H. P. Chao, T. V. Trinh, T. T. Le, C. C. Lin and H. N. Tran, *J. Cleaner Prod.*, 2018, **180**, 560–570.
- 21 H. Lin, S. Han, Y. Dong and Y. He, *Appl. Surf. Sci.*, 2017, **412**, 152–159.
- 22 D. Lv, Y. Liu, J. Zhou, K. Yang, Z. Lou, S. A. Baig and X. Xu, *Appl. Surf. Sci.*, 2018, **428**, 648–658.
- 23 D. Wu, L. Hu, Y. Wang, Q. Wei, L. Yan, T. Yan, Y. Li and B. Du, *J. Colloid Interface Sci.*, 2018, **523**, 56–64.
- 24 E. F. C. Chauque, L. N. Dlamini, A. A. Adelodun, C. J. Greyling and J. C. Ngila, *Physics and Chemistry of the Earth, Parts A/B/C*, 2017, **100**, 201–211.
- 25 Y. Yang, S. Song and Z. Zhao, *Colloids Surf., A*, 2017, **513**, 315–324.
- 26 M. Lv, L. Yan, C. Liu, C. Su, Q. Zhou, X. Zhang, Y. Lan, Y. Zheng, L. Lai, X. Liu and Z. Ye, *Chem. Eng. J.*, 2018, **349**, 791–799.
- 27 L. Sun, H. Yu and B. Fugetsu, *J. Hazard. Mater.*, 2012, **203–204**, 101–110.
- 28 X. Xin, W. Si, Z. Yao, R. Feng, B. Du, L. Yan and Q. Wei, *J. Colloid Interface Sci.*, 2011, **359**, 499–504.
- 29 G. McKay, A. Mesdaghinia, S. Nasserri, M. Hadi and M. S. Aminabad, *Chem. Eng. J.*, 2014, **251**, 236–247.
- 30 A. H. AbdEl-Salam, H. A. Ewais and A. S. Basaleh, *J. Mol. Liq.*, 2017, **248**, 833–841.
- 31 S. G. Nasab, A. Semnani, A. Teimouri, M. J. Yazd, T. M. Isfahani and S. Habibollahi, *Int. J. Biol. Macromol.*, 2019, **124**, 429–443.
- 32 G. Sharma, A. Kumar, M. Naushad, A. García-Peñas, A. H. Al-Muhtaseb, A. A. Ghfar, V. Sharma, T. Ahamad and F. J. Stadler, *Carbohydr. Polym.*, 2018, **202**, 444–453.
- 33 J. Liu, Y. Wang, Y. Fang, T. Mwamulima, S. Song and C. Peng, *J. Mol. Liq.*, 2018, **250**, 468–476.
- 34 S. Gopi, A. Pius and S. Thomas, *Journal of Water Process Engineering*, 2016, **14**, 1–8.
- 35 E. A. Dil, M. Ghaedi, A. Ghaedi, A. Asfaram, M. Jamshidi and M. K. Purkait, *J. Taiwan Inst. Chem. Eng.*, 2016, **59**, 210–220.
- 36 C. Muthukumar, S. V. Murugaiyan and M. Thirumarimurugan, *J. Taiwan Inst. Chem. Eng.*, 2016, **63**, 354–362.
- 37 G. Wen and Z. G. Guo, *Colloids Surf., A*, 2018, **541**, 58–67.
- 38 C. Yang, L. Lei, P. Zhou, Z. Zhang and Z. Lei, *J. Colloid Interface Sci.*, 2015, **443**, 97–104.
- 39 H. T. Xing, J. H. Chen, X. Sun, Y. H. Huang, Z. B. Su, S. R. Hu, W. Weng, S. X. Li, H. X. Guo, W. B. Wu, Y. S. He, F. M. Li and Y. Huang, *Chem. Eng. J.*, 2015, **263**, 280–289.

