



# Intact mangrove root electrodes for desalination†

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Through the benefit of billions of years of evolution, biology has developed tremendous strategies on how to co-exist in high salinity and water scarce environments. Biologically-inspired abiotic systems are becoming a central pillar in how we respond to critical grand challenges that accompany exponential population growth, uncontrolled climate change and the harsh reality that 96.5% of the water on the planet is saltwater. One fascinating biologic adaptation to saltwater is the growth of mangrove trees in brackish swamps and along the coasts. Through a process of salt exclusion, the mangrove maintains a near freshwater flow from roots to leaves to survive. One abiotic approach to water desalination is capacitive deionization, which aims to desalinate low-salinity water sources at energy costs below current technologies, such as reverse osmosis and thermal distillation. In this work, we use one-step carbonization of a plant with developed aerenchyma tissue to enable highly-permeable, freestanding flow-through capacitive deionization electrodes. We show that carbonized aerenchyma from red mangrove roots reduces the resistance to water flow through electrodes by 65-fold relative to carbonized common woody biomass. We then demonstrate the practical use of the intact carbonized red mangrove roots as electrodes in a flow-through capacitive deionization system. These findings have implications in a range of fields including water desalination, bioinspired materials, and plant functionality.

## 1. Introduction

The ability to desalinate water is a critical area of exploration that will affect populations across the world. One organism that is able to desalinate water already is the mangrove. These plants have developed adaptations to thrive in these high salt environments.<sup>1,2</sup> Further enabling the growth of mangroves in high-salinity, flooded and oxygen-deprived environments is the development of aerenchyma tissue in the root. Aerenchyma tissue reduces the risk of asphyxiation by providing a low-resistance pathway for gas transport from the roots to the shoot of the plant.<sup>3-6</sup> We hypothesized that the architecture of

the mangrove could be used to generate a conductive synthetic aerenchyma mimic that would be an excellent electrode for a flow-through (FT) capacitive deionization (CDI) system.

CDI is a low-energy and cost-effective alternative to current desalination technologies for the removal of ionic species from low-salinity water sources. CDI uses electrostatic force to adsorb and store ions from a feed stream to a pair of charged electrodes.<sup>7-11</sup> A typical arrangement of the electrodes in a CDI system, termed flow-by (FB), has electrodes that are parallel to the direction of the feed stream. More recently an approach of arranging the electrodes perpendicular to the feed stream, termed FT, has shown promise for faster ion transport and full utilization of the electrode surface.<sup>12,13</sup> However, perpendicular FT electrodes typically require high feed pressures to drive water through the micro/meso-sized pores.<sup>12,14</sup> This limitation decreases the efficiency of the approach. Effective FT-CDI electrodes would need to combine high salt adsorption capacity (SAC) with low resistance to water flow through the material. One approach to address these interconnected needs involves the fabrication of hierarchical carbon electrodes comprised of both micron-scale and micro/meso-scale pores that function to increase hydraulic permeability while maintaining high SAC.<sup>14-17</sup> When considering the need for micron-sized interconnected pores in FT electrodes we were captivated by the idea that if mangrove aerenchyma was conductive, it would be an ideal electrode. We therefore explored to what degree aerenchyma architecture and micro- or nanostructure were retained during carbonization.

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Natural resources (*i.e.* – coconut shells, peanut shells, bio-char, leaves) have been used for decades to make porous carbon electrodes by carbonization.<sup>18–25</sup> After chemical or physical treatment of raw materials, activated carbons (ACs) exhibit high specific surface area, high electrical conductivity, and are low-cost due to abundance. Because of these characteristics, ACs are one of the most commonly used materials for a wide range of electrode applications (*i.e.* – supercapacitors, Li- and Na-batteries, CDI).<sup>9,26,27</sup> Remarkably, however, the raw material is almost never used with its intact natural architecture, and is instead crushed and treated to generate a final material. Retaining the microscale structure of an evolutionarily designed, high porosity structure during carbonization was a compelling opportunity to solve some of the vexing challenges of FT-CDI.

The carbonized aerenchyma that we fabricated and integrated into an FT-CDI system presents a new approach to CDI electrode fabrication (Fig. 1). We observed that carbonized red mangrove roots (RMRs) retained the flow characteristics of their living precursors, were conductive enough to perform well as electrodes in a FT-CDI system, and thereby reduced feed concentrations of saltwater by as much as 250 mg L<sup>-1</sup> while exhibiting a salt adsorption capacity (SAC) as high as 9.6 mg g<sup>-1</sup>.

## 2. Results and discussion

### 2.1 Carbonized mangrove root structure and characteristics

To develop our vision of a biologically derived FT-CDI system we first determined whether carbonization would destroy the low-

resistance structure in aerenchyma tissue of the RMR. We used a combination of confocal microscopy and electron microscopy to compare the microstructure before and after carbonization (Fig. 2). We found that, on average, the RMRs retained approximately one third of their dry weight after carbonization with a dramatic retention of microstructure. We imaged the naturally occurring autofluorescence in the tissue of the RMR to observe the structure of the aerenchyma in a fresh, unaltered state. Using our 2D confocal images we generated 3D constructions of the aerenchyma in both the transverse and longitudinal directions (Fig. 2b, c, Movie S1 and S2†). The natural architecture of the aerenchyma was composed of tube-like structures that were extremely well retained after carbonization (Fig. 2e and f). A higher magnification image revealed that there were interconnecting pores in the longitudinal walls of the tubular structures (Fig. S1, ESI†). These structures have been found in the aerenchyma of other mangrove species<sup>28,29</sup> and, if retained after carbonization, we hypothesized that they would keep flow resistance low in a FT-CDI system, thus enabling a high-efficiency desalination.

To further understand the structure of our carbonized RMR, we investigated the carbon structure, chemical composition, and specific surface area through Raman spectroscopy (Fig. S2 and Table S1, ESI†), energy-dispersive X-ray (EDX) spectroscopy (Fig. S3 and Table S2, ESI†), and Brunauer–Emmett–Teller (BET) analysis for nitrogen adsorption isotherms (Fig. S4, ESI†). The Raman peaks at 1336 cm<sup>-1</sup> and 1585 cm<sup>-1</sup> represented the defect (D) and graphitic (G) bands of carbon. The high  $I_D/I_G$  ratio, ranging from 1.05–1.15, indicated that disorder existed in

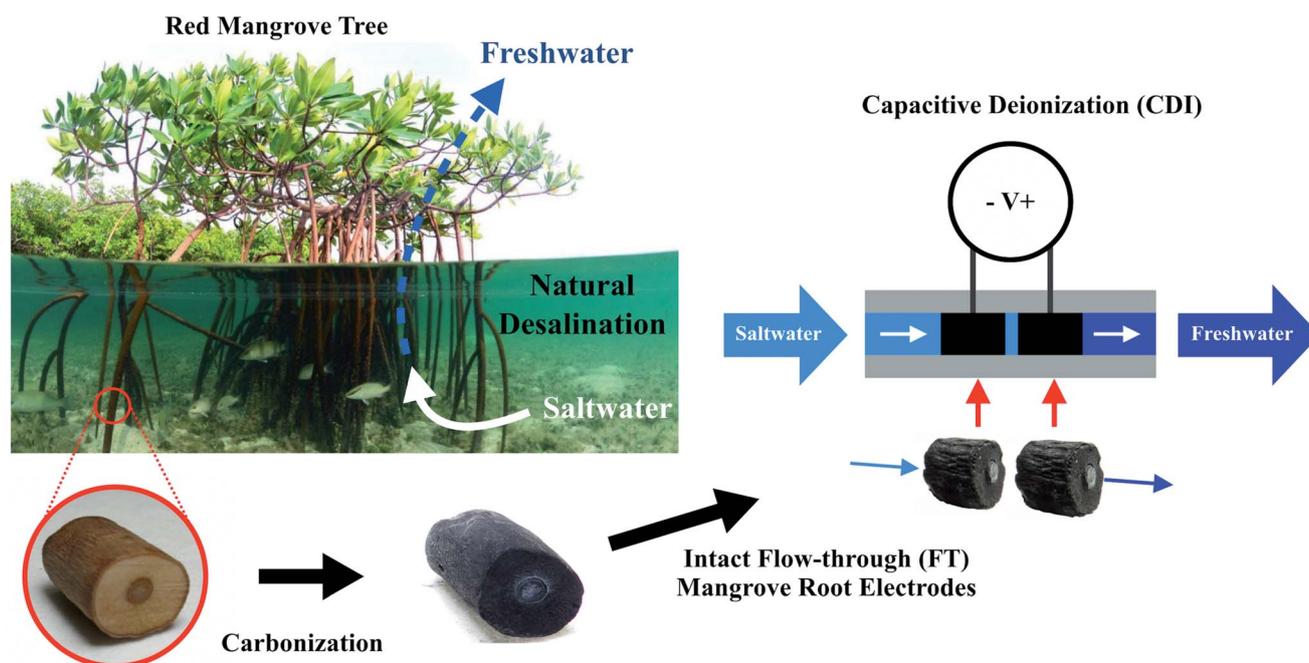
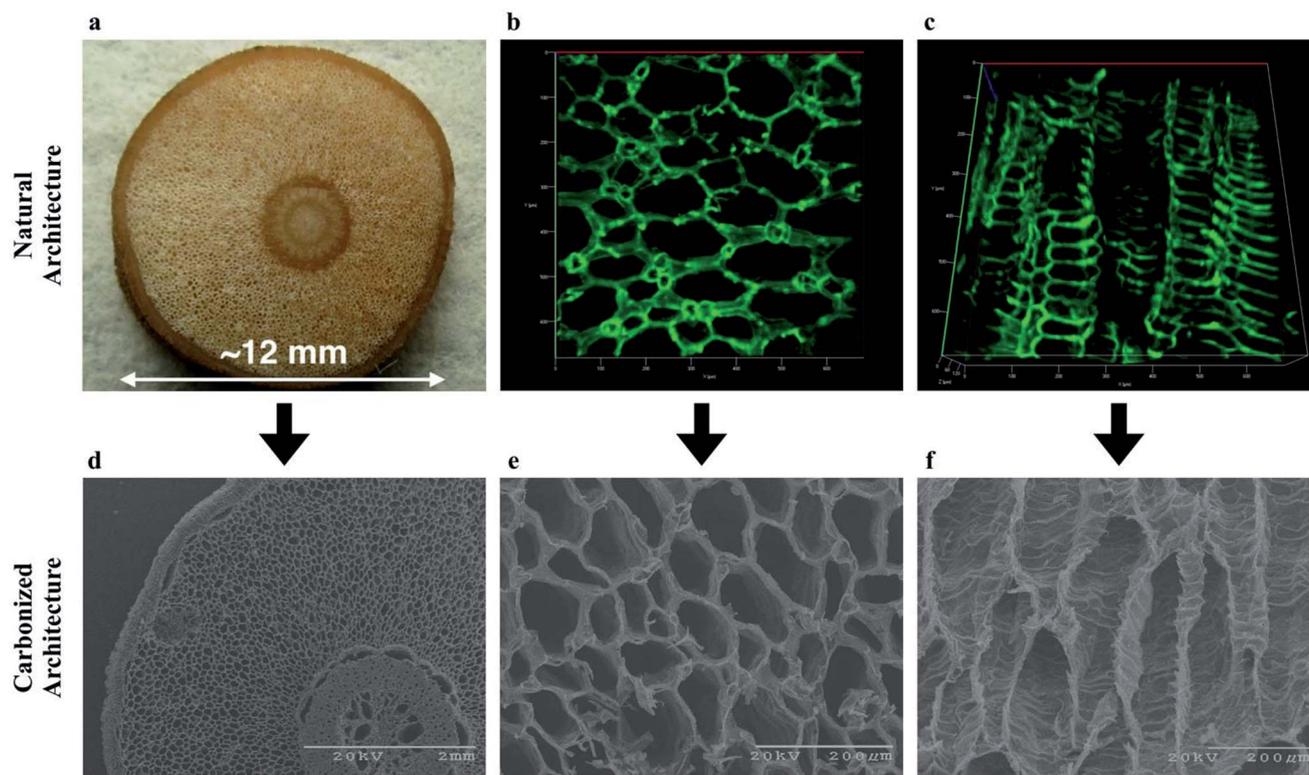


Fig. 1 Intact mangrove root electrodes for desalination through flow-through (FT) capacitive deionization (CDI). Using mangroves as an inspiration for desalination, highly permeable FT-CDI electrodes were synthesized in a one-step carbonization process by heating red mangrove roots (RMRs) with developed aerenchyma tissue. The electrodes were then arranged in series through our custom-fabricated silicone coupling and connected to a voltage source *via* thin graphite rods to form a FT-CDI cell. Upon applying a voltage potential, sodium and chloride ions were adsorbed from the feed stream to the electrode surface resulting in a desalted permeate stream (red mangrove photograph taken by Joost van Uffelen).





**Fig. 2** Porous architecture of aerenchyma tissue from RMR for the bioinspired FT-CDI electrodes before and after carbonization. Carbonization was achieved through thermal treatment at 800 °C for 1 hour under argon flow. (a) Digital image of the cross-section of the RMR; (b) confocal image of the autofluorescence of the cross-section for the aerenchyma tissue indicating the porous structures in the tissues; a 3D video of the rendered 3D confocal stack is in Movie S1;† (c) confocal longitudinal image of the autofluorescence for the aerenchyma tissue indicating the repeatable architecture along the length of the tissue; a 3D video of the rendered 3D confocal stack is in Movie S2;† (d) scanning electron microscope (SEM) image of the cross-section of the carbonized RMR indicating the overall structure of the root is maintained through the carbonization process; (e) higher magnification SEM image of the carbonized cross-section for the aerenchyma tissue indicating the porous architecture of the tissue is well-maintained through the carbonization process; (f) SEM longitudinal image of the carbonized aerenchyma tissue indicating the repeatable architecture along the length of the tissue is well-maintained through the carbonization process.

the carbon matrix.<sup>30–32</sup> EDX analysis showed high carbon content in the carbonized RMRs with trace amounts of Mg, O, Cl, and Ca. The specific surface area of the carbonized RMRs was between 3 to 216 m<sup>2</sup> g<sup>-1</sup>. Although this range was large, micro/macro-scale features of the harvested aerenchyma (*i.e.* – cross sectional area of tubular structures) would be expected to vary within the root of the mangrove plant as a function of specific root type, distance from the root apex, and developmental maturity.<sup>28,29</sup>

## 2.2 Flow-through characteristics of carbonized mangrove root and common woody biomass

We next compared the structure of the carbonized RMR to other plants which lacked aerenchyma. We carbonized non-specific common woody biomass from trees that do not grow in high salinity or oxygen deprived environments. Within these trees the secondary xylem occupied most of the cross-section and contained tube-like structures,<sup>33</sup> similar to the aerenchyma in RMRs. Detailed microscopic comparisons of the carbonized plant tissues (Fig. 3a and b) revealed that the average cross-sectional area of the tube-like structures in the aerenchyma

was approximately 10 times more than that of the secondary xylem (Fig. S5a and b, ESI†). Furthermore, the total cross-sectional area percentage that the tube-like structures occupied, which represents potential permeation area for water flow, was 18% higher in the aerenchyma when compared to the secondary xylem. These points suggested that the aerenchyma would provide less resistance to water flow in comparison to the secondary xylem. To understand this approach further, we predicted the permeability of both structures using a bundle of capillaries model for FT-CDI electrodes.<sup>14</sup> The permeability was expressed as:

$$k = \varepsilon r^2 / 8\tau$$

where  $\varepsilon$  is the porosity of the carbonized cross-section,  $r$  is the radius of the tube-like structures, and  $\tau$  is the tortuosity of the tube-like structures. The porosity was estimated to be the total cross-sectional area percentage that the tube-like structures occupied in the aerenchyma or secondary xylem; unity was assumed for tortuosity. The permeability of the aerenchyma was predicted to be an order of magnitude greater than that of the secondary xylem.



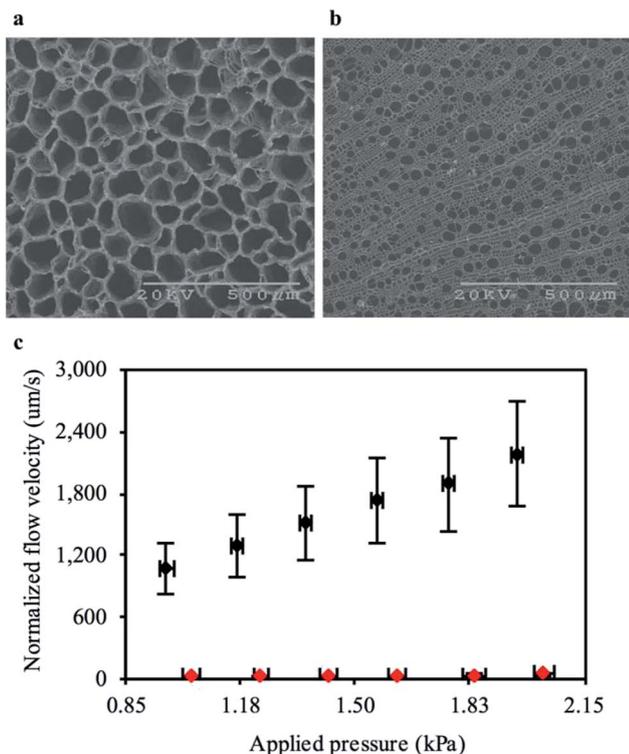


Fig. 3 Hydraulic permeability of water flowing through carbonized RMR and common woody biomass. (a) SEM image of tube-like structures in the carbonized RMR aerenchyma; (b) SEM image of tube-like structures in the carbonized secondary xylem of common woody biomass; (c) Normalized flow velocity through each respective carbonized structure versus applied pressure indicating aerenchyma of carbonized RMR (black diamonds) had approximately 65 times less resistance to water permeation than secondary xylem of carbonized common woody biomass (red diamonds). Mean  $\pm$  s.e.m.,  $n = 8$  (carbonized RMR) and  $n = 3$  (carbonized common woody biomass) independent experiments.

To determine experimentally if the aerenchyma posed less resistance to water flow than the secondary xylem, we measured the flow velocity of water through each carbonized structure at low pressures. The flow velocity through the carbonized RMR was on average 65 times faster when compared to the common woody biomass at similar pressures (Fig. 3c). The large difference in flow resistance between the samples in comparison to the theoretical calculations was likely due to a portion of the tube-like structures in the secondary xylem being closed-cell, where the water could permeate into the structure but not through it. In addition, a portion of the tube-like structures in the aerenchyma may not extend all the way through the carbonized RMR samples. However, interconnecting pores (Fig. S1, ESI†) between the tubes could allow for radial flow, enabling an otherwise closed-cell to conduct water. The average hydraulic permeability of the carbonized RMR ( $1.13 \times 10^{-11} \text{ m}^2$ ) was calculated to be 65-fold greater than that of the common woody biomass ( $1.66 \times 10^{-13} \text{ m}^2$ ) and on the same order of magnitude as the highest reported value for flow-through electrodes.<sup>14</sup>

### 2.3 Desalination performance of intact mangrove root electrodes in flow-through capacitive deionization system

After demonstrating that the intact carbonized RMR exhibited high flow-through characteristics, our next objective was to characterize their performance as electrodes in a FT-CDI system. We used a flexible, custom-fabricated silicone coupling to maintain the carbonized RMR in series. The coupling fit tightly around the outer diameter of the carbonized RMR and directed water flow through the aerenchyma. To provide power for the desalination, the electrodes were connected to a power supply using 0.3 mm graphite rods, which were pressed through the coupling and brought into contact with the carbonized RMR (Fig. S6, ESI†).

The FT-CDI experiments were conducted in single-pass (SP) mode with an initial stopped-flow charging (salt adsorption) phase. The SP mode more closely resembles a CDI application,<sup>9</sup> although the CDI cell can also be charged while continuously recycling the feed solution as batch-mode (BM). In FT-CDI experiments the electrodes were initially dry and then a  $1200 \text{ mg L}^{-1}$  NaCl solution was pumped through the carbonized RMRs at  $0.475 \text{ mL min}^{-1}$  for approximately 15 minutes. The flow was then stopped and a potential of 1.5 V was applied to the carbonized RMRs for 15, 45, or 135 minutes. After the initial stopped-flow charging stage, the stock  $1200 \text{ mg L}^{-1}$  NaCl solution was pumped into the FT-CDI cell at  $0.475 \text{ mL min}^{-1}$  for 30 minutes while the voltage potential was maintained. The partially desalinated volume in the carbonized RMRs was subsequently displaced and flowed downstream to the conductivity meter. The salt concentration downstream of the FT-CDI cell was  $1200 \text{ mg L}^{-1}$  until flow resumed.

The change in salt concentration over time was an important measure of how well our mangrove-inspired CDI system functioned. The sharp decrease in salt concentration at the start of the 30 minute flow phase (Fig. 4a) was the displaced volume from one pair of carbonized RMRs. We tested multiple independently prepared sets of carbonized RMRs to investigate how reproducible the performance was in the FT-CDI system. The total mass of the electrode pairs was 58.3, 70.4, and 83.9 mg. For each pair of electrodes, increasing the stopped-flow charging time enabled the carbonized RMRs to adsorb more salt, which resulted in greater reductions in feed concentration (Fig. 4b). The highest reduction in feed concentration we observed was  $250 \text{ mg L}^{-1}$ . As flow continued, the salt concentration of the permeate gradually returned to the concentration of the feed solution. Even after a stopped-flow charging time of 15, 45, or 135 minutes and 30 minutes of flow, the carbonized RMRs were still adsorbing salt (the permeate solution did not return to  $1200 \text{ mg L}^{-1}$ ). The extended time to reach a saturated state was most likely due to the large length of, and gap between, the electrodes (the electrodes were approximately 5 and 40 times the length and gap, respectively, of other reported FT-CDI systems<sup>12</sup>). Surprisingly, although the carbonized RMRs did not reach a saturated state, they still exhibited an average SAC as high as  $7 \text{ mg g}^{-1}$  (Fig. 4b) and a maximum observed SAC of  $9.6 \text{ mg g}^{-1}$ . This SAC is competitive with recently reported FT-CDI electrodes (Table 1) and biomass-based CDI electrodes



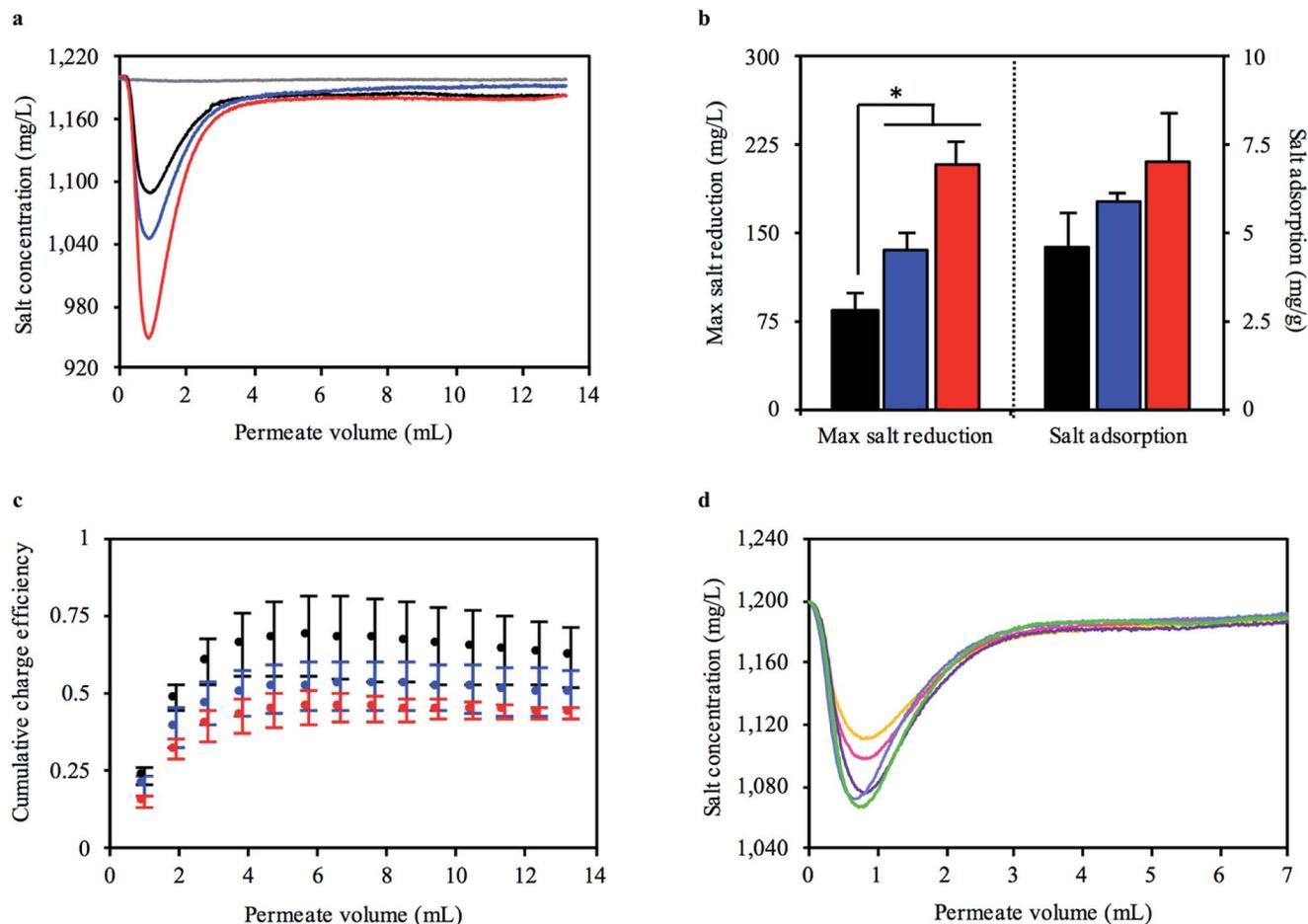


Fig. 4 Capacitive deionization performance of bioinspired FT-CDI system utilizing carbonized RMR as electrodes that have little resistance to water flow. (a) Representative experiment of salt concentration of permeate from bioinspired FT-CDI system after 15 (black), 45 (blue), and 135 (red) minutes of stopped-flow charging at an applied potential of 1.5 V with carbonized RMR electrodes (net mass = 58.3 mg). The dark grey line is a control with identical system and operation for a stopped-flow charging time of 45 minutes without carbonized RMRs. (b) Increasing stopped-flow charging time enabled larger reductions in salt concentration (mean  $\pm$  s.e.m.,  $n = 3$  independent experiments,  $*p < 0.05$ ), (c) but tended to reduce the charge efficiency of the bioinspired FT-CDI system. (d) Salt concentration of permeate from bioinspired FT-CDI system during cyclic operation (cycle 1 = orange; cycle 2 = pink; cycle 3 = purple; cycle 4 = light blue; cycle 5 = green). The reduction in salt concentration of the permeate from the FT-CDI cell,  $\Delta$  and ASAR (Fig. S7, ESI $^\dagger$ ) noticeably increased after the first cycle.

(Table 2). Furthermore, our intact mangrove root electrodes require far less fabrication material and processing compared to most FT and biomass-based electrodes (Tables 1 and 2).

We further examined the performance of the carbonized RMRs in the FT-CDI system by calculating the charge efficiency ( $\Delta$ ), which is the ratio of salt adsorbed to the electric charge that accumulated in the electrode pair. Energy consumption for the CDI process normally decreases with increasing  $\Delta$ , therefore, values as close to unity (theoretical maximum) are highly desirable.<sup>47</sup> Common reported values for  $\Delta$  range between 0.5 to 0.8.<sup>48</sup> We observed an average  $\Delta$  of 0.62, 0.50, and 0.43 for stopped-flow charging times of 15, 45, and 135 minutes, respectively (Fig. 4c) relative to the end of the 30 minute flow phase. The maximum  $\Delta$  during the flow-phase was reached at a permeate volume of approximately 6 mL and then decreased thereafter.

CDI systems are continuously cycled through adsorption and desorption phases to produce a desalted solution and brine

solution, respectively. Therefore, we also investigated the desalination performance of the carbonized RMRs when operated cyclically. In each cycle the flow was first stopped for 15 minutes and a potential of 1.5 V was applied. Next, flow was initiated at 0.475 mL min<sup>-1</sup> while maintaining the applied potential for 15 minutes. Finally, the potential was reduced to 0 V and flow continued for 30 minutes. We observed a sharp decrease in salt concentration as the partially desalinated solution was being displaced from the carbonized RMRs when the flow was initiated (Fig. 4d). Interestingly, the performance of the carbonized RMRs increased after the first cycle. A larger reduction in feed concentration was observed, as well as an increased  $\Delta$  and average salt adsorption rate (ASAR) (Fig. S7, ESI $^\dagger$ ). The FT electrode arrangement has been shown to enable a higher ASAR, which allows more desalinated water to be produced in a given time frame.<sup>12</sup> The ASAR of the mangrove-based CDI system during cyclic operation ranged between 0.063 to 0.075 mg g<sup>-1</sup> min<sup>-1</sup>, which was not as fast as some FT-



Table 1 Comparison of fabrication materials and electrosorption capacities for various FT-CDI electrodes

Electrode	Fabrication materials	Applied voltage (V)	Electrosorption capacity (mg g <sup>-1</sup> )
Electrospun porous hierarchical carbon nanofibers <sup>17</sup>	Polyvinylpyrrolidone Polyacrylonitrile Dimethylformamide Carbon dioxide	1.2	7.61
N-doped porous carbon <sup>34</sup>	Zinc nitrate hexahydrate Cobalt nitrate hexahydrate Methanol 2-Methylimidazole Hydrofluoric acid Acetylene black Polytetrafluoroethylene	1.4	16.63
3D graphitic carbon/SiC <sup>35</sup>	Graphite paper Silicon carbide foam Methane	1.5	3.2
3D foam-like carbon nanoarchitectures <sup>36</sup>	Activated carbon Colloidal silica 3-(Trimethoxysilyl)propylmethacrylate Epoxy acrylate resin 1,4-Butanediol diglycidyl ether Sodium hydroxide Polytetrafluoroethylene Ethanol	1.4	20.9
3D graphene with hierarchical porous structure <sup>16</sup>	Graphite substrate Polystyrene nanospheres Ammonium molybdate Graphite oxide Hydrochloric acid Polytetrafluoroethylene Carbon black Graphite sheet	1.2	14.7
Hierarchical carbon aerogel monolith <sup>12</sup>	Resorcinol Formaldehyde Acetic acid Carbon dioxide	1.5	10.2
Laser-perforated activated carbon <sup>14</sup>	Activated carbon electrodes (PAC MM 203)	1.0	3
Intact mangrove root (this work)	<i>R. mangle</i> root Epoxy resin	1.5	9.6

CDI systems, but comparable to FB-CDI systems. As previously mentioned, however, the length of, and gap between, the carbonized RMR electrodes were much larger than fully optimized FT-CDI systems and would be expected to decrease the ASAR.<sup>12</sup> Lastly, the charging current for each cycle was very consistent (Fig. S8, ESI†) and exhibited a repeatable increase when flow was initiated after the stopped-flow charging phase. Once the applied potential was reduced to 0 V, the current direction reversed (discharge current).

### 3. Conclusions

In this work, we demonstrated that the intact natural architecture of a biomass can serve as an effective and easily fabricated, low-cost intact FT-CDI electrode. The carbonized RMRs were shown to decrease the feed concentration of a 1200 mg L<sup>-1</sup> salt solution by as much as 250 mg L<sup>-1</sup> and exhibit a SAC as high as 9.6 mg g<sup>-1</sup>. We also demonstrated that the properties of the biomass have important implications on the performance of the electrodes. Biological adaptations, such as the development of

aerenchyma tissue, improve the hydraulic permeability of the freestanding electrode by almost two orders of magnitude in comparison to common plant structures. Intact carbonized plant materials couple the exquisite designs of nature with the ruggedness of the synthetic world.

## 4. Experimental section

### 4.1 Plant material and carbonization process

Red mangrove (*Rhizophora mangle*) plants (~1 meter tall) were grown indoors (20–25 °C) and provided with 16 g L<sup>-1</sup> saltwater every 3–4 days as well as being grown in a 12 hour photoperiod. Common woody biomass samples were collected from non-specific woody trees (*i.e.* – plants that synthesize wood, also known as the secondary xylem, as their main structural component). RMRs and common woody biomass samples were cut to a length of approximately 7.5–10 mm immediately before carbonization. The carbonization was accomplished through heating the samples to 800 °C for 1 hour under 95–100 cm<sup>3</sup> min<sup>-1</sup> argon flow at a heating rate of 5 °C min<sup>-1</sup> in



Table 2 Comparison of electrosorption capacity for various biomass-based CDI electrodes and treatment/materials for electrode fabrication

Biomass	Activation/treatment	Binder/additives	Current collector	Applied voltage (V)	Electrosorption capacity (mg g <sup>-1</sup> )
Citrus peel <sup>37</sup>	ZnCl <sub>2</sub>	PTFE	Titanium mesh	1.5	10.79, 16.2 <sup>a</sup>
	KOH	PTFE	Titanium mesh	1.5	8.58
	H <sub>3</sub> PO <sub>4</sub>	PTFE	Titanium mesh	1.5	5.22
	—	PTFE	Titanium mesh	1.5	8.44
Bacterial-cellulose <sup>38</sup>	NH <sub>3</sub>	—	—	1.2	17.29
Bacterial-cellulose <sup>39</sup>	H <sub>3</sub> PO <sub>4</sub>	—	—	1.2	16.20
Bacterial-cellulose <sup>40</sup>	—	—	—	1.2	12.81
Palm shell <sup>41</sup>	ZnCl <sub>2</sub> , CO <sub>2</sub>	PVdf, DMAc	—	1.2	3.3
Wheat straw <sup>42</sup>	KOH, SiO <sub>2</sub> sol	PTFE	Graphite sheet	N/A	2.67
Silk cocoon <sup>43</sup>	—	Acetylene black, PVA	Graphite substrate	1.2	12.02
	CO <sub>2</sub>	Acetylene black, PVA	Graphite substrate	1.2	16.56
<i>L. leucocephala</i> wood <sup>24</sup>	KOH, CO <sub>2</sub>	PVDF	—	1.0	2.1
Coconut shell <sup>44</sup>	KOH, CO <sub>2</sub>	PVDF	—	1.0	20.91
Woody biomass <sup>45</sup>	KOH	Nafion	Carbon cloth	N/A	5.39
Basswood <sup>46</sup>	CO <sub>2</sub>	—	—	1.2	5.7
Mangrove root (this work)	—	—	—	1.5	9.6

<sup>a</sup> Electrode only used as anode in CDI system.

a Lindberg 54553-VH tube furnace. After carbonization, the samples were rinsed with DI H<sub>2</sub>O three times and then dried at 80 °C for at least 6 hours. The length and diameter of the RMR samples post-carbonization ranged from 5.5–7.5 mm and 7.0–9.5 mm, respectively. The mass of each sample ranged from 25–45 mg.

In preparation for examining the hydraulic permeability and integration into the FT-CDI experiments, the pith (center) of each sample was filled with epoxy to limit water transport to the aerenchyma and the secondary xylem (Fig. S9, ESI<sup>†</sup>), which represents the bulk of the cross-section for RMRs and common woody biomass, respectively. In preparation for the FT-CDI experiments, approximately 250 mL of DI H<sub>2</sub>O was delivered through the aerenchyma of the carbonized RMRs to remove residual salts and minerals. After each FT-CDI experiment, 50 mL of DI H<sub>2</sub>O was delivered through the aerenchyma of the carbonized RMRs. The samples were then dried at 80 °C for at least 6 hours and stored at room temperature until further testing.

## 4.2 Imaging and cross-sectional pore area analysis

The structure of the aerenchyma tissue was determined by imaging the natural plant autofluorescence using a Zeiss Cell Observer Spinning Disk Confocal Microscope (excitation – 488 nm; emission – 525 nm). Layers of these images were processed and combined together to create 3D image stacks. Post-carbonization images were generated by scanning electron microscopy (SEM) using a Jeol JSM 6400 and Philips XL-30 FEG SEM.

Cross-sectional area analysis of the tube-like structures in the aerenchyma of the carbonized RMR and in the secondary xylem of the carbonized common woody biomass samples was done using ImageJ. SEM images were converted to black-and-white images using the automatic thresholding tool in ImageJ. The periphery of each pore was then identified using

the particle analysis tool, which calculated the cross-sectional area for each element. Pores that intersected the scale bar or that were cut off at the edge were not considered for analysis.

## 4.3 Characterization

The specific surface area of the carbonized mangrove root samples was characterized by Brunauer–Emmett–Teller (BET) for nitrogen adsorption isotherms using a Micromeritics Gemini VII Surface and Porosity instrument. Raman spectroscopy was performed by NT-MDT NTEGRA spectra using a laser power of 2.38 mW and 532 nm excitation. The spectra were recorded with an acquisition time of 30 seconds at five separate locations on three independently prepared carbonized RMRs. The  $I_D/I_G$  ratio was calculated using the peak intensity at the D-band and G-band. EDX was performed using a Philips XL-30 FEG SEM. Measurements were conducted at three separate locations on four independently prepared carbonized RMRs.

## 4.4 Hydraulic permeability

Flow velocity through carbonized plant tissue was examined using a water column pressure system (Fig. S10, ESI<sup>†</sup>). Samples were wrapped in Parafilm and connected to the bottom of a water column using a custom-fabricated silicone coupling. The samples were wrapped in Parafilm to direct the bulk flow of water through the carbonized tissue rather than between the sample and the coupling. The time for the meniscus of the water column to drop 2 cm, which equaled a permeate volume of 1 mL, was recorded and used to calculate the flow rate for six different applied pressures ranging from 0.96–2.04 kPa. The applied pressure was calculated by averaging the pressure head of the water column before and after 1 mL of water permeated through the plant tissue based on:

$$\Delta P = \rho g(H - \Delta h/2)$$



where  $\Delta P$  is the pressure,  $\rho$  is the density of water,  $g$  is the acceleration of gravity,  $H$  is the height of the water column before any water permeated through the carbonized plant tissue, and  $\Delta h$  is the change in the height of the water column after 1 mL of water permeated through the carbonized plant tissue. The flow rate through each sample was normalized by the ratio of the sample length to the average sample length. This is important because the flow rate under a given applied pressure is inversely proportional to the length of the sample based on Darcy's law. The normalized flow velocity of water through each sample was calculated by dividing the respective normalized flow rate by the available cross-sectional permeation area of each sample. The hydraulic permeability was calculated at each applied pressure using Darcy's law:

$$k = (Q\mu L)/(\Delta PA)$$

where  $k$  is permeability ( $\text{m}^2$ ),  $Q$  is flow rate ( $\text{m}^3 \text{s}^{-1}$ ),  $\mu$  is dynamic viscosity ( $\text{Pa s}$ ),  $L$  (m) is length of the sample,  $\Delta P$  (Pa) is the applied pressure differential, and  $A$  ( $\text{m}^2$ ) is the available cross-sectional area of the sample (*i.e.* total cross-sectional area–pith cross-sectional area).

#### 4.5 Flow-through capacitive deionization

Flow-through CDI experiments were conducted in single-pass mode with an initial stopped-flow charging phase. Two carbonized RMRs were individually wrapped in Parafilm and arranged in series approximately 1–3 mm apart through a custom-fabricated silicone coupling. The length and diameter of the RMR electrodes ranged from 5.5–7.5 mm and 7.0–9.5 mm, respectively. The carbonized RMRs were connected to a DC power supply (BK Precision Model 1670) through 0.3 mm graphite rods (Fig. S6 and S11, ESI†). Three independently prepared carbonized RMR electrode pairs with a net mass of 58.3, 70.4, and 83.9 mg were tested. In each experiment the FT-CDI cell was initially dry. A 1200  $\text{mg L}^{-1}$  NaCl solution was then delivered through the FT-CDI system for approximately 15 minutes at a flow rate of 0.475  $\text{mL min}^{-1}$ . The flow was then stopped for 15, 45, or 135 minutes while a potential of 1.5 V was applied to the FT-CDI cell. After the stopped-flow charging phase, flow was reinitiated for 30 minutes at 0.475  $\text{mL min}^{-1}$  while maintaining the applied voltage potential.

The NaCl concentration of the permeate from the FT-CDI cell was calculated using conductivity measurements with a custom-built flow-through system (Fig. S11, ESI†). A calibration curve which related salt concentration to conductivity was generated before and after each experiment by flowing NaCl standards ranging from 800–1300  $\text{mg L}^{-1}$  through the conductivity meter. Salt adsorption was calculated by measuring the area under the curve of the permeate during the 30 minute flow phase with respect to the stock salt concentration of 1200  $\text{mg L}^{-1}$ . Fig. S12, Table S3 and S4 (ESI†) are control experiments to determine the accuracy of our measurement and calculation techniques for quantifying the change in salt concentration and total salt adsorption.

The charging current in each experiment was measured using a Fluke 287 multimeter with a sampling frequency of 0.5 Hz. The charge efficiency was calculated according to:

$$A = (I \times F)/\Sigma$$

where  $I$  is the salt adsorption capacity ( $\text{mol g}^{-1}$ ),  $F$  is the Faraday constant ( $96485 \text{ C mol}^{-1}$ ), and  $\Sigma$  is the net charge passed through the CDI circuit from the power supply ( $\text{C g}^{-1}$ ). The net charge was calculated by integrating the charging current with respect to time. The ASAR during cyclic operation was calculated by dividing the SAC measured from the 15 minute flow phase by the total cycle time (60 minutes).

#### 4.6 Statistical analysis

All statistical analysis was conducted using a two-tailed paired Student's *t*-test.

### Conflicts of interest

There are no conflicts to declare.

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