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Yttrium and europium separation by solvent extraction with undiluted thiocyanate ionic liquids[†]

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An yttrium/europium oxide obtained by the processing of fluorescent lamp waste powder was separated into its individual elements by solvent extraction with two undiluted ionic liquids, trihexyl(tetradecyl)phosphonium thiocyanate, [C101][SCN], and tricaprylmethylammonium thiocyanate, [A336][SCN]. The best extraction performances were observed for [C101][SCN], by using an organic-to-aqueous volume ratio of 1/10 and four counter-current extraction stages. The loaded organic phase was afterwards subjected to scrubbing with a solution of 3 mol L⁻¹ CaCl₂ + 0.8 mol L⁻¹ NH₄SCN to remove the co-extracted europium. Yttrium was quantitatively stripped from the scrubbed organic phase by deionized water. Yttrium and europium were finally recovered as hydroxides by precipitation with ammonia and then calcined to the corresponding oxides. The conditions thus defined for an efficient yttrium/europium separation from synthetic chloride solutions were afterwards tested on a leachate obtained from the dissolution of a real mixed oxide. The purity of Y₂O₃ with respect to the rare-earth content was 98.2%; the purity of Eu₂O₃ with respect to calcium was 98.7%.

Introduction

Rare-earth elements (REEs) are a group of seventeen chemical elements, specifically the fifteen lanthanides plus yttrium (Y) and scandium (Sc). Rare earths are moderately abundant in the Earth's crust and they occur in many minerals, but the major resources are just four, including bastnäsite, monazite, xenotime and ion-adsorption clays.¹ Due to their different abundance in the Earth's crust, an unwanted co-production of other REEs usually occurs together with the ones needed for the major applications. This is the so-called balance problem.² The ideal situation is a perfect match between demand and supply, which would result in the lowest market price. To mitigate the balance problem, different solutions can be considered, such as resources diversification, recycling, urban/landfill mining, substitution, reduced use and new high-volume applications.²⁻⁴

Phosphors used in fluorescent lamps contain a significant amount of the heavy REEs europium (Eu), terbium (Tb) and yttrium in comparison to primary ores and their recycling would help to keep the balance of those elements.² A fluorescent lamp consists of a glass tube filled with an inert gas and mercury vapor at low pressure and tungsten or stainless steel cathodes which are assembled at the end of the lamps. The internal surface of the glass tube is coated with a layer of phosphor powder to obtain the desired color rendering index. The powder consists of a blend of a red phosphor (Y₂O₃:Eu³⁺, YOX), a green phosphor

(LaPO₄:Ce³⁺, Tb³⁺, LAP; (Gd,Mg)B₅O₁₂:Ce³⁺, Tb³⁺, CBT; (Ce,Tb)MgAl₁₁O₁₉, CAT) and a blue phosphor (BaMgAl₁₀O₁₇:Eu²⁺, BAM).^{5,6} In addition to the tri-band phosphors, the powder also contains the halophosphate phosphor (Sr,Ca)₁₀(PO₄)₂(Cl,F)₂:Sb³⁺, Mn²⁺ (HALO), which emits broad-band cold white light. The HALO phosphor represents the largest mass fraction in the lamp phosphor waste (50 wt%), but it does not contain any REE. The red phosphor YOX accounts for about 20 wt% and it has the highest intrinsic value, since it contains high concentrations of the critical heavy REEs Y and Eu.⁷ Many approaches have been proposed for the recovery of REEs from lamp phosphor waste.^{5,6,8-10} For example, in the HydroWEEE process, the fluorescent powder is treated by dissolution in sulfuric acid, after which the obtained leachate is further treated by precipitation with oxalic acid giving a mixed Y/Eu oxalate.¹¹⁻¹⁴ Our research group developed a novel separation process to recover a mixed Y/Eu oxide by selective dissolution of the red phosphor YOX with the functionalized ionic liquid [Hbet][Tf₂N], followed by precipitation-stripping with oxalic acid and calcination at 950 °C to regenerate the YOX.⁷ In a recent paper, we described the recovery of terbium and other REEs from the residue obtained after dissolution of HALO and YOX.¹⁵ It must be stated, however, that the market demand for phosphors has moved to LED lamps.⁴ For this reason the mutual separation of yttrium and europium from recycled YOX is required for their use in applications other than lamp phosphors. Different approaches have been developed to separate europium and yttrium,¹⁶⁻¹⁸ but the most common method is solvent extraction.¹⁹⁻²¹ It must be stressed that the separation processes are often not efficient due to the low separation factors between adjacent REEs (1.5 to 2 on average), so that many extraction stages are required in order to obtain the desired purity.²²

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Gaudernack and coworkers filed a patent on the solvent extraction of yttrium from ammonium nitrate solutions by using the thiocyanate and nitrate form of quaternary ammonium extractants, followed by scrubbing with ammonium nitrate solution and stripping with water or dilute acid solutions.²³ Other solvent extraction studies were performed with 2-ethylhexyl phosphonic acid (PC-88A) for the separation of Y, Eu and Tb from spent fluorescent lamp leach solutions.²⁴ Yttrium and europium were recovered with >98% and 100% purity, respectively, by using process simulation of a counter-current mixer-settler cascade followed by scrubbing and precipitation with oxalic acid. PC-88A was also used in the work reported by De Carolis *et al.* for the separation of yttrium and europium from spent fluorescent lamp leach solutions.²⁵ Tunsu *et al.* reported the results on the selective extraction of yttrium and europium with Cyanex 572 from nitrate leach solutions.¹⁹ The stripping of the REEs from the loaded organic phase was carried out with 3 mol L⁻¹ HCl, followed by precipitation with oxalic acid and calcination at 800 °C to obtain the corresponding yttrium and europium oxides with 99.82% and 91.6% purity, respectively. A process for the extraction and separation of yttrium and europium from thiocyanate leachates was developed which makes use of acid leaching, solvent extraction with trimethylbenzyl ammonium chloride, stripping, separation of europium from yttrium by selective dissolution in ethanol and thermal reduction to the metallic form.²⁶ Thakur reported on the Y/Eu separation by D2EHPA and PC-88A from dilute HNO₃/HCl/H₂SO₄ solutions.²⁷ Rhodia (presently Solvay) used molecular extractants for the processing of spent fluorescent lamp leach solution to separate yttrium and europium and other REEs by solvent extraction.²⁸ Vu *et al.* reported the selective recovery of europium and yttrium using various acid lixivants, followed by solvent extraction.²⁹ The obtained results showed that HNO₃ had the best leaching efficiency and PRIMENE-JM provided a higher selectivity than D2EHPA for the extraction of europium over yttrium.

In the present paper, the thiocyanate ionic liquids trihexyl(tetradecyl)phosphonium thiocyanate, [C101][SCN], and tricaprylmethylammonium thiocyanate [A336][SCN] were tested for the extraction and separation of yttrium(III) and europium(III) from chloride feed solutions. The structure is reported in Fig. 1. These ionic liquids in undiluted form have been proven to be useful for the extraction of REEs and transition metals.^{30–34} The process was first optimized using synthetic solutions and afterwards applied on a leachate obtained by the dissolution of a real mixed oxide.

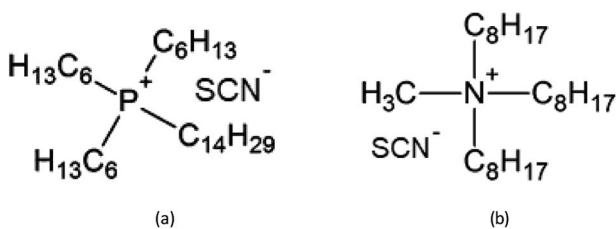


Fig. 1 Structures of the ionic liquids used in this study: (a) [C101][SCN]; (b) [A336][SCN] (main component).

Experimental

Chemicals

Ammonium thiocyanate (99%), calcium chloride dihydrate (>99.5%), and ammonium chloride (>99.8%) were purchased from Chem Lab (Zedelgem, Belgium). Ammonia solution (25%) was obtained from VWR Chemicals (Leuven, Belgium). Yttrium and europium chlorides (>99%) were purchased from Sigma Aldrich (Diegem, Belgium) and Alfa Aesar (Karlsruhe, Germany), respectively. Trihexyl(tetradecyl)phosphonium chloride (Cyphosil IL 101, [C101][Cl]) (97.7%) was purchased from Cytec Industries Inc. (Ontario, Canada). Tricaprylmethyl ammonium chloride (Aliquat 336, [A336][Cl]), a mixed quaternary ammonium salt containing mainly trioctylmethylammonium and tridecylmethylammonium chloride (88.2–90.6%) was purchased from Sigma-Aldrich (Diegem, Belgium). Oxalic acid ($\geq 99.9\%$) and the standard solutions of Ga and Sm (1000 $\mu\text{g mL}^{-1}$ in 3–5 wt% nitric acid) were obtained from Merck (Overijse, Belgium). Ethanol (PA absolute 99.8%) and Triton X-100 were purchased from Acros Organics (Geel, Belgium). The silicone-isopropanol solution was purchased from SERVA Electrophoresis GmbH (Heidelberg, Germany). Water was always of ultrapure quality, deionized to a resistivity of 18.2 M Ω cm with a Sartorius Arium® Pro ultrapure water system. All chemicals were used as received, without any further purification. The thiocyanate forms of the ionic liquids, [C101][SCN] and [A336][SCN], were synthesized according to a literature procedure.³¹ The chloride concentration in [C101][SCN] and [A336][SCN] was determined by both the AgNO₃ test and TXRF analysis and it resulted to be negligible.

Analytical techniques

The concentration of metals in the aqueous and organic phase was determined by total-reflection X-ray fluorescence spectrometry (TXRF) with a Bruker S2 Picofox TXRF spectrometer equipped with a molybdenum source.^{35,36} A small amount of ionic liquid (50 mg) was placed into propylene microtubes with an appropriate internal standard with the X-ray fluorescence energy as close as possible to that of the element to be determined, in order to reduce the effects caused by absorption of secondary X-rays, but minimising at the same time peaks overlap. Samples were further diluted with ethanol to 1 mL. After shaking the samples on a vibrating plate (IKA MS 3 basic), a small droplet (1.5 μL) was put on a quartz glass carrier, previously treated with a silicone-isopropanol solution to avoid spreading of the droplet. The quartz carriers were then dried for 30 min at 60 °C prior to analysis. Measurements in the aqueous phase were performed in the same way, but a 5 vol% Triton solution in water was used for diluting the sample. Each sample was measured for 500 s. Analyses were performed in duplicate and the error associated with the measurements was $\pm 5\%$. A Mettler-Toledo S220 Seven Compact pH/Ion meter was used for pH measurements. The purity of the obtained oxide was measured *via* Inductively Coupled Plasma-Optical Emission Spectrometry (ICP-OES) using a Perkin Elmer Optima 8300 spectrometer equipped with an axial/radial dual plasma view, a GemTip Cross-Flow II nebulizer and a Scott double pass with



inert Ryton spray chamber. The density of the two ionic liquids was measured with an Anton Paar DMA 4500M density meter and the viscosity with an Anton Paar LOVIS 2000 ME rolling-ball viscometer. Fourier Transform Infrared (FTIR) spectra of the initial ionic liquid and of the regenerated one were measured on a Bruker Vertex 70 spectrometer with a Platinum ATR module.

Solvent extraction tests

Synthetic yttrium and europium solutions were prepared by dissolving hydrated YCl_3 and EuCl_3 in deionized water; the chloride concentration was set at 8 mol L^{-1} by addition of CaCl_2 . The general extraction and stripping experiments were carried out by using an organic-to-aqueous volume ratio (O/A) equal to 1. More specifically, 1 mL of the aqueous and organic phases were contacted at room temperature ($T = 30^\circ\text{C}$) for 30 min using a Nemus Life Thermo shaker (Model TMS-200). After each extraction and stripping experiment, samples were centrifuged using a Heraeus Megafuge 1.0 centrifuge for 3 minutes at 5000 rpm in order to separate the two phases. The distribution ratio (D) was calculated as the ratio between the metal concentration in the organic phase (C_{org}) to the metal concentration in the aqueous phase (C_{aq}) at equilibrium:

$$D = \frac{C_{\text{org}}}{C_{\text{aq}}} \quad (1)$$

From the D value, the percentage extraction ($\%E$) was calculated:

$$\%E = \frac{D}{D + V_{\text{aq}}/V_{\text{org}}} \times 100 \quad (2)$$

where V_{aq} and V_{org} are the volumes of the aqueous and the organic phase, respectively. The separation factor (α) was calculated according to the following equation:

$$\alpha = \frac{D_{m_1}}{D_{m_2}} \quad (3)$$

where m_1 represents yttrium and m_2 represents europium for the $[\text{C101}][\text{SCN}]$ extraction system, while for the $[\text{A336}][\text{SCN}]$ the opposite is applied (because, by definition α must be >1). Counter-current simulations were performed according to a literature procedure.³⁷

Precipitation and calcination tests

Precipitation of rare earths was performed by addition of an ammonia solution (25%). The precipitate was separated from the aqueous phase by filtration, placed in an oven for 24–48 h at $60\text{--}70^\circ\text{C}$ and finally calcined at $400\text{--}450^\circ\text{C}$ for 5 h to obtain the corresponding oxides Y_2O_3 and Eu_2O_3 .

Results and discussion

Solvent extraction tests with $[\text{C101}][\text{SCN}]$ and $[\text{A336}][\text{SCN}]$

The viscosity and density of the water-saturated ionic liquids are reported in Table 1. Preliminary solvent extraction tests were

Table 1 Viscosity and density of the ionic liquids used in this study (water-saturated, at $T = 25^\circ\text{C}$)

	$[\text{C101}][\text{SCN}]$	$[\text{A336}][\text{SCN}]$
Viscosity, mPa s	224.5	202.1
Density, g cm^{-3}	0.898	0.892

carried out from synthetic solutions with yttrium and europium concentrations similar to the ones obtained by dissolving a mixed oxide from the HydroWEEE process ($[\text{Y}(\text{m})] = 3415 \text{ mg L}^{-1}$, $[\text{Eu}(\text{m})] = 215 \text{ mg L}^{-1}$).^{11–14} In order to determine the contact time necessary for the extraction system to reach the equilibrium, a set of experiments was carried with both $[\text{C101}][\text{SCN}]$ and $[\text{A336}][\text{SCN}]$ by varying the contact time from 5 to 30 minutes at O/A = 1 : 1 and $T = 30^\circ\text{C}$ (Fig. S1†). It was found that equilibrium for $[\text{C101}][\text{SCN}]$ was obtained within 15 minutes. For $[\text{A336}][\text{SCN}]$, a slight increase in the extraction percentage was observed between 15 and 30 minutes. The percentage extraction values did not increase by increasing the contact time further in both systems. Based on these results, 30 minutes was selected as the optimal contact time. Further extraction tests were carried out as a function of the initial pH (Fig. S2†), which was varied from 1.3 to 3.8 by addition of dilute HCl or NaOH ($[\text{Cl}^-] = 8 \text{ mol L}^{-1}$, $t = 30 \text{ min}$, O/A = 1 : 1). The equilibrium pH was measured as well and the obtained values did not change by varying the initial pH, showing that there is no involvement of protons in the extraction process. The effect of temperature ($30\text{--}60^\circ\text{C}$) was also studied ($[\text{Cl}^-] = 8 \text{ mol L}^{-1}$, $t = 30 \text{ min}$, O/A = 1 : 1). It was found that extraction of $[\text{Y}(\text{m})]$ and $[\text{Eu}(\text{m})]$ slightly increased with increasing temperature in both systems, indicating that the extraction process is endothermic (Fig. S3†).

Since $[\text{A336}][\text{SCN}]$ and $[\text{C101}][\text{SCN}]$ are both basic extractants, the anions from the aqueous phase are involved in the extraction mechanism to allow the formation of anionic complexes in the ionic liquid phase. Hence, salting-out agents play a significant role in the extraction mechanism. As shown in Fig. 2, the percentage extraction of $[\text{Y}(\text{m})]$ and $[\text{Eu}(\text{m})]$ increased by increasing the chloride concentration in the aqueous phase for

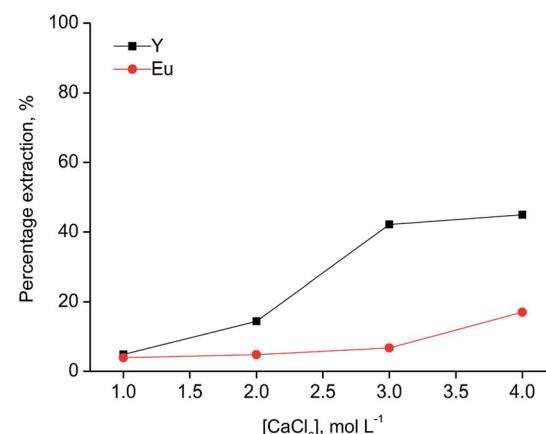


Fig. 2 Extraction of $[\text{Y}(\text{m})]$ and $[\text{Eu}(\text{m})]$ with the ionic liquid $[\text{C101}][\text{SCN}]$ as a function of the CaCl_2 concentration (aqueous phase: $[\text{Y}(\text{m})] = 3415 \text{ mg L}^{-1}$, $[\text{Eu}(\text{m})] = 215 \text{ mg L}^{-1}$, O/A = 1 : 1, $T = 30^\circ\text{C}$).



both ionic liquids, indicating that chloride ions have an influence on the extraction mechanism. When $[C101][SCN]$ was used, $Y^{(III)}$ was preferentially extracted over $Eu^{(III)}$. $Y^{(III)}$ extraction started at 2 mol L^{-1} $CaCl_2$ and reached a maximum value (about 50%) at 3 mol L^{-1} $CaCl_2$. At higher chloride concentrations, the percentage extraction did not increase significantly, but $Eu^{(III)}$ co-extraction occurred. Remarkably, the selectivity was reversed for extraction by $[A336][SCN]$ (Fig. 3). This behaviour was also observed by Larsson *et al.*³¹ They reported a similar distribution ratio for $Y^{(III)}$ in both $[A336][SCN]$ and $[C101][SCN]$, while the distribution ratio of $Eu^{(III)}$ was significantly lower in $[C101][SCN]$ than in $[A336][SCN]$. In other words, in $[A336][SCN]$ the distribution ratio of $Eu^{(III)}$ was slightly higher than $Y^{(III)}$, implying a preference of extraction of $Eu^{(III)}$ over $Y^{(III)}$, which was also observed in this work. In $[C101][SCN]$, the distribution ratio of $Eu^{(III)}$ was much lower than that of $Y^{(III)}$, implying a strong preference for $Y^{(III)}$ over $Eu^{(III)}$. The reason for the increase in the percentage extraction by increasing $CaCl_2$ concentration is a combination of the adjustment of the water activity levels by the addition of a salting-out agent with high ionic strength, resulting in a weaker hydration of the lanthanide ions, and the fact that chloride anions are involved in the extraction equilibrium and have to be co-extracted in order to enable metal extraction. Therefore higher concentrations push the equilibrium to the right.³¹ The extraction mechanism for extraction of the trivalent rare-earth ions by the ionic liquids $[C101][SCN]$ and $[A336][SCN]$ can be represented by the following equation:



where the subscripts (aq) and (org) denote the aqueous and organic phases, respectively, $[Q]$ represents the cation $[A336]$ or $[C101]$, and M^{3+} represents $Y^{(III)}$ or $Eu^{(III)}$.^{31,38}

To increase the selective extraction of $Y^{(III)}$ over $Eu^{(III)}$ with $[C101][SCN]$, further experiments were performed by addition of thiocyanate anions to the aqueous phase, with concentrations varying from 0.1 to 0.4 mol L^{-1} at different chloride

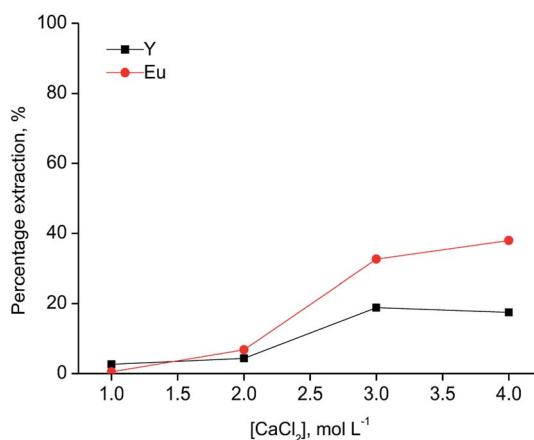
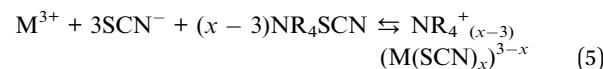


Fig. 3 Extraction of $Y^{(III)}$ and $Eu^{(III)}$ with the ionic liquid $[A336][SCN]$ as a function of the $CaCl_2$ concentration (aqueous phase: $[Y^{(III)}] = 3145\text{ mg L}^{-1}$, $[Eu^{(III)}] = 215\text{ mg L}^{-1}$, $[CaCl_2] = 3\text{ mol L}^{-1}$, $O/A = 1 : 1$, $T = 30\text{ }^\circ\text{C}$).

concentration values ($2\text{--}6\text{ mol L}^{-1}$). It was found that $Y^{(III)}$ extraction increased by increasing the thiocyanate concentration. At 1 mol L^{-1} $CaCl_2$, the extraction efficiency was not significantly influenced by the thiocyanate concentration while the effect was more pronounced at 2 and 3 mol L^{-1} $CaCl_2$ (Fig. 4). Quantitative extraction of $Y^{(III)}$ was achieved at a thiocyanate concentration of 0.2 mol L^{-1} , with about 35% co-extraction of $Eu^{(III)}$. At higher thiocyanate concentrations, co-extraction of $Eu^{(III)}$ increases, reaching 75% at a thiocyanate concentration of 0.4 mol L^{-1} . The increase in the percentage extraction is due to the involvement of thiocyanate ions in the extraction process.^{31,38} From these results, it can be stated that both chloride and thiocyanate ions are required to obtain quantitative and selective extraction of yttrium over europium. The best separation was achieved at 3 mol L^{-1} $CaCl_2$ and 0.2 mol L^{-1} SCN^- , so that these conditions were selected as the optimal ones.

Further tests, not reported here, were carried out by varying the thiocyanate concentration from 0.1 to 0.4 mol L^{-1} at different chloride concentration values ($2\text{--}6\text{ mol L}^{-1}$) to get selective extraction of $Eu^{(III)}$ over $Y^{(III)}$ with $[A336][SCN]$. The highest separation factor ($\alpha = 17.6$) was observed at 3 mol L^{-1} $CaCl_2$ and 0.4 mol L^{-1} SCN^- .

By the addition of SCN^- to the aqueous phase, the extraction mechanism most likely does no longer correspond to eqn (4). Since SCN^- has a higher hydrophobicity than Cl^- , together with a higher affinity for coordination to rare earth ions, SCN^- is most likely co-extracted to the ionic liquid phase, rather than Cl^- . The expected modified extraction mechanism is presented in eqn (5):



The selectivity for either $Eu^{(III)}$ or $Y^{(III)}$ was rather low in both ionic liquids and depends on the choice of ionic liquid. In the case of $[C101][SCN]$, $Y^{(III)}$ was extracted, together with $Eu^{(III)}$, but the percentage extraction of $Eu^{(III)}$ was in all investigated experimental conditions lower than that of $Y^{(III)}$. For the

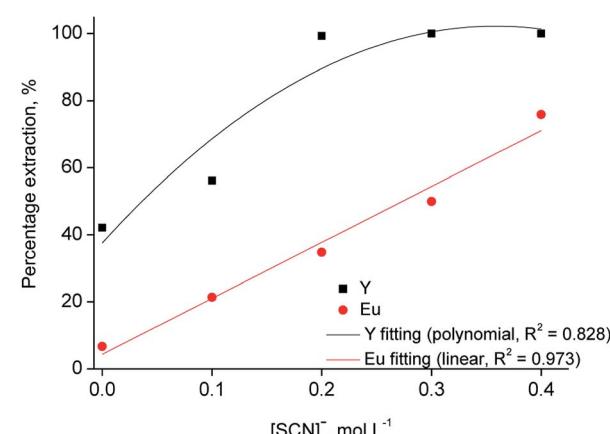


Fig. 4 Extraction of $Y^{(III)}$ and $Eu^{(III)}$ with the ionic liquid $[C101][SCN]$ as a function of the thiocyanate concentration (aqueous phase: $[Y^{(III)}] = 3145\text{ mg L}^{-1}$, $[Eu^{(III)}] = 215\text{ mg L}^{-1}$, $[CaCl_2] = 3\text{ mol L}^{-1}$, $O/A = 1 : 1$, $T = 30\text{ }^\circ\text{C}$).

extraction with [A336][SCN], Eu(III) was efficiently extracted, along with Y(III), and the percentage extraction of Eu(III) was always higher than that of Y(III). Therefore, the quaternary phosphonium thiocyanate ionic liquid [C101][SCN] is the most suitable for Y(III)/Eu(III) separation, due to the higher extraction efficiency and the higher separation factor values.

The theoretical number of counter-current stages required for quantitative extraction of Y(III) over Eu(III) by [C101][SCN] was predicted by constructing the McCabe-Thiele diagram. The extraction isotherm was determined by varying the organic-to-aqueous volume ratio from 1 : 30 to 1 : 1 and using a feed solution containing 0.2 mol L⁻¹ SCN and 3 mol L⁻¹ CaCl₂. It was found that at least three counter-current stages are required for quantitative extraction of Y(III) at an O/A ratio equal to 1 : 1.5 (Fig. 5). The achieved loading of Y(III) into the ionic liquid phase was about 4.5 g L⁻¹. A higher loading of Y(III) (about 29 g L⁻¹) can be obtained from aqueous feed solutions containing 0.8 mol L⁻¹ SCN⁻ + 3 mol L⁻¹ CaCl₂ at O/A = 1 : 10 (Fig. 6). Three to four stages were found to be necessary for quantitative Y(III) extraction in a real counter-current setup.

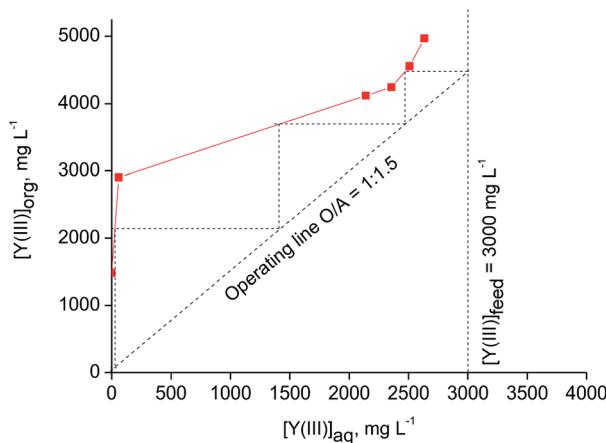


Fig. 5 McCabe-Thiele diagram for extraction of Y(III) with [C101][SCN] (aqueous phase: [Y(III)] = 3000 mg L⁻¹, [Eu(III)] = 215 mg L⁻¹, [CaCl₂] = 3 mol L⁻¹, [NH₄SCN] = 0.2 mol L⁻¹; T = 30 °C).

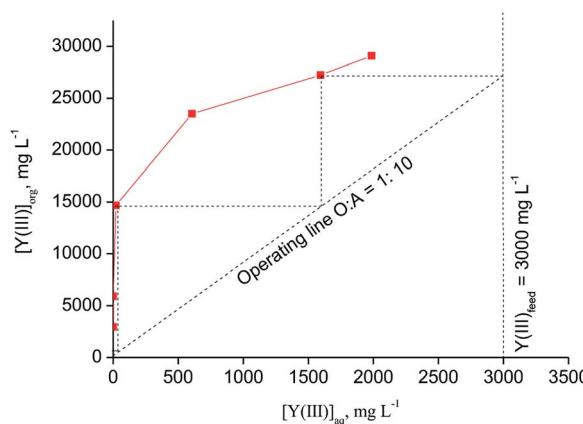


Fig. 6 McCabe-Thiele diagram for extraction of Y(III) with [C101][SCN] (aqueous phase: [Y(III)] = 3000 mg L⁻¹, [Eu(III)] = 215 mg L⁻¹, [CaCl₂] = 3 mol L⁻¹, [NH₄SCN] = 0.8 mol L⁻¹; T = 30 °C).

Scrubbing of [C101][SCN]

A sufficient amount of loaded ionic liquid phase [C101][SCN] was generated (O/A = 1 : 10, four counter-current stages, T = 30 °C, t = 30 min, 0.8 mol L⁻¹ SCN and 3 mol L⁻¹ CaCl₂; loaded organic phase: [Y(III)] = 31 709 ppm, [Eu(III)] = 338 ppm, [Ca(II)] = 989 ppm) and used for scrubbing and stripping tests. Besides Eu(III) and Y(III), also the scrubbing of Ca(II) was considered, since the mixed oxide material tested later in this work (*vide infra*) contains a high concentration of Ca(II). Scrubbing tests were carried out by contacting the loaded [C101][SCN] phase with various solutions (Table 2). Hot water, NH₄Cl, NH₄SCN, CaCl₂ and NH₄Cl + NH₄SCN solutions did not show any selectivity towards the scrubbing of Eu(III) and Ca(II) over Y(III), while better results were achieved with the feed itself (*i.e.* the synthetic yttrium and europium solution): 80.7% Eu(III) was selectively scrubbed by contacting the [C101][SCN] ionic liquid phase with the feed at O/A = 1 : 10. Based on these one-stage scrubbing tests, it is expected that Eu(III) can be quantitatively scrubbed by applying multi-stage scrubbing. A similar scrubbing efficiency could be obtained with the mixture 3 mol L⁻¹ CaCl₂ + 0.8 mol L⁻¹ NH₄SCN at O/A = 1 : 1 in several cross-current simulations, but the loss of yttrium would be about 5–6%.

Yttrium recovery from the loaded [C101][SCN] phase

The scrubbed ionic liquid was contacted with an equal volume of various stripping agents at room temperature to recover yttrium (Table 3). About 42.4% stripping of Y(III) could be achieved in a single contact with deionized water. This percentage could be increased up to 70.1% by employing two cross-current stages. With 0.3 mol L⁻¹ CaCl₂, a similar stripping efficiency was observed. Diluted HCl and H₂SO₄ showed an efficient stripping of Y(III) which resulted to be quantitative at 20 vol% and 10 vol%, respectively. A white precipitate of metal salt was formed at high H₂SO₄ concentration (7% and 10%), which might be due to the formation of Y₂(SO₄)₃. Similar stripping percentages were found by precipitation with oxalic acid solutions: over 99.9% of Y(III) could be stripped with 1 mol L⁻¹ oxalic

Table 2 Scrubbing of Eu(III), Ca(II) and Y(III) from the loaded [C101][SCN] phase

Reagent	Scrubbing, %		
	Eu	Ca	Y
Hot H ₂ O	66.2	70.8	45.2
2 mol L ⁻¹ NH ₄ Cl	51.8	53.6	30.5
2 mol L ⁻¹ NH ₄ NO ₃	22.0	45.7	12.8
0.1 mol L ⁻¹ NH ₄ SCN	62.5	76.9	41.0
0.1 mol L ⁻¹ ascorbic acid	64.5	85.8	44.6
6 mol L ⁻¹ NH ₄ NO ₃	14.2	68.9	7.49
2 mol L ⁻¹ NH ₄ Cl + 0.1 mol L ⁻¹ NH ₄ SCN	59.6	34.5	67.2
2 mol L ⁻¹ NH ₄ NO ₃ + 0.1 mol L ⁻¹ NH ₄ SCN	28.7	17.5	51.7
2 mol L ⁻¹ CaCl ₂	37.8	—	31
3 mol L ⁻¹ CaCl ₂	21.7	—	15.7
3 mol L ⁻¹ CaCl ₂ + 0.8 mol L ⁻¹ SCN	15	—	1
Synthetic Y and Eu solution, O/A = 1 : 1	3.1	—	—
Synthetic Y and Eu solution, O/A = 1 : 2	15.9	—	—
Synthetic Y and Eu solution, O/A = 1 : 10	80.7	—	—

Table 3 Stripping of Y(III) from the loaded [C101][SCN] ionic liquid phase by using various reagents

Stripping agent	Stripping, %
H ₂ O	42.4
HCl 1%	41.7
HCl 5%	47.9
HCl 7%	53.7
HCl 10%	59.6
HCl 15%	78.9
HCl 20%	100
CaCl ₂ 0.3 mol L ⁻¹ – stage 1	36.9
CaCl ₂ 0.3 mol L ⁻¹ – stage 2	70.4
H ₂ O – stage 2	70.1
HCl 1% – stage 2	74.3
HCl 5% – stage 2	82.9
H ₂ SO ₄ 1%	46.8
H ₂ SO ₄ 5%	52.6
H ₂ SO ₄ 7%	86.1
H ₂ SO ₄ 10%	99.8
H ₂ C ₂ O ₄ 0.1 mol L ⁻¹	—
H ₂ C ₂ O ₄ 0.5 mol L ⁻¹	66
H ₂ C ₂ O ₄ 1 mol L ⁻¹	99.9

acid. Although equally good stripping results were achieved with HCl, H₂SO₄, oxalic acid and water, the latter is selected as the preferable stripping agent. If HCl, H₂SO₄ and oxalic acid would be used, an extra washing step would be necessary to allow recycling of the solvent in a continuous process. When using water, this extra washing step is avoided.

The strip solution containing yttrium was subjected to precipitation with ammonia solution (25 vol%), followed by

calcination at $T = 400\text{--}450\text{ }^{\circ}\text{C}$ for 5 h. The purity of the obtained Y₂O₃, as determined through ICP-OES analysis, was >99% with respect to Eu(III) and Ca(II). The stripped organic phase was recycled and tested for the extraction of Y(III) under similar conditions. The effluent streams after yttrium recovery could be treated to remove trace amounts of HSCN by activated carbon in order to meet the current environmental regulations.²³

Precipitation of europium from the raffinate

To recover europium from the raffinate solutions, preliminary experiments were conducted by addition of various equivalent ratios of oxalic acid from 1 to 8 with respect to europium. The results showed no selective precipitation of Eu(III) over Ca(II). Europium recovery from the raffinate was therefore performed by precipitation in alkaline conditions by the addition of ammonia. At pH 8.6, 89% Eu(III) was precipitated as Eu(OH)₃, while quantitative precipitation was achieved at pH 9.6, with a high selectivity over Ca(II). Co-precipitation of Ca(II) occurred at pH 10, so 9.6 was selected as the optimal pH value.

Application of the process to the mixed REE oxide from HydroWEEE

The whole process described so far was also tested on a real mixed oxide obtained from the HydroWEEE process.^{11–14} The composition of the oxide was determined by dissolving the solid in 6 mol L⁻¹ HCl. The yttrium and europium content was found to be 68.1 wt% and 5.1 wt%, respectively. Gadolinium (3.5%), cerium (0.9%) and terbium (0.6%) impurities were found to be present as well. A leaching step was then performed with

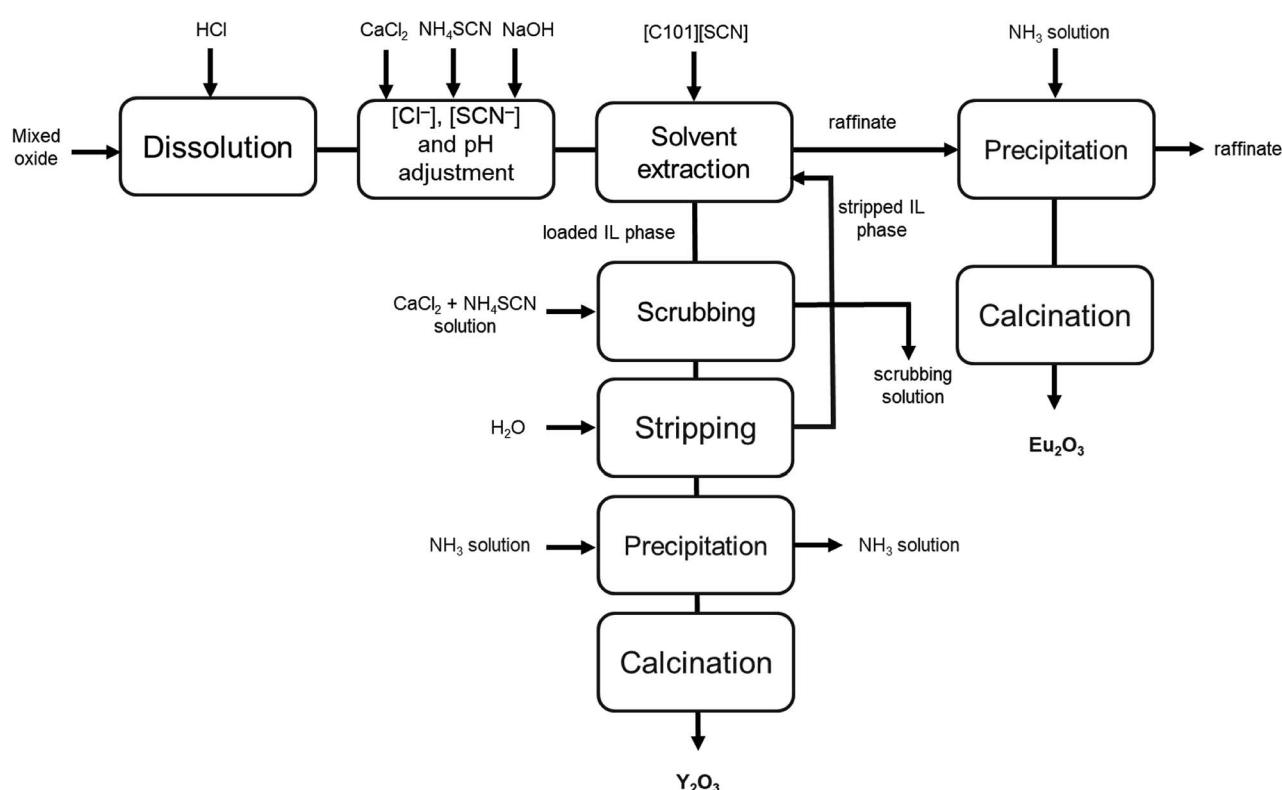


Fig. 7 Process flow sheet for the separation of yttrium and europium from a mixed oxide recovered from lamp phosphor waste.

6 mol L⁻¹ HCl by employing a liquid-to-solid ratio of 20 mL g⁻¹. Full dissolution of the mixed oxide was achieved in 24 h at a temperature of 50 °C. The leachate was diluted ten times with deionized water and then CaCl₂ and NH₄SCN were added in order to adjust chloride and thiocyanate concentration to the desired values. After pH adjustment (pH = 4.2) with NaOH, the leachate ([Y(III)] = 2886 mg L⁻¹, [Eu(III)] = 165 mg L⁻¹) was contacted with the undiluted ionic liquid at O/A = 1 : 10 in four counter-current steps. An yttrium extraction efficiency of 94% was achieved, with a few percentages of gadolinium, terbium and europium co-extracted. These results are in agreement with the ones reported from synthetic solutions, where three to four counter-current stages were necessary for quantitative Y(III) extraction. The loaded ionic liquid phase was further contacted with a mixture of 3 mol L⁻¹ CaCl₂ and 0.8 mol L⁻¹ NH₄SCN or with the feed (yttrium and europium solution coming from the leaching of the mixed oxide) to remove trace amount of co-extracted rare earths in five cross-current simulations. Yttrium was finally stripped with deionized water at O/A ratio 1 : 5 in two cross-current stages. Yttrium and europium were recovered from the solutions as their hydroxides by addition of an ammonia solution, followed by calcination at 400–450 °C. The purities of the yttrium and europium oxides were over 98.2% and 98.7%, respectively. Regarding the overall recovery efficiencies, they were 94% for Y(III) and 98% for Eu(III).

In the work of Nakamura *et al.* (2007), the purity of the obtained oxides was >98% for Y₂O₃ and 100% for Eu₂O₃, however only 53% of the Eu(III) was recovered.²⁴ Tunsu *et al.* (2016) obtained Y(III) and Eu(III) oxides with purity equal to 99.82% and 91.6%, respectively; the major impurity in Eu₂O₃ was found to be gadolinium.¹⁹ Both processes make use of classical organic solvents for the solvent extraction step, such as PC-88A and Cyanex 572.

The regenerated ionic liquid [C101][SCN] was tested for the extraction of Y(III) under similar experimental conditions and it was found that the changes in the extraction efficiency are negligible. The FTIR of the initial ionic liquid phase and of the regenerated one have been recorded as well (Fig. S4†).

A flow sheet for the process is shown in Fig. 7. This process makes use of the undiluted ionic liquid [C101][SCN] for the separation of yttrium and europium from chloride solutions obtained by the dissolution of a mixed rare-earth oxide. Its main advantages are the use of only a few process steps, the possibility to regenerate the ionic liquid, thus reducing reagent consumption, and the relatively high purity of the obtained oxides.

Conclusions

In this work the separation of Y(III) and Eu(III) by undiluted quaternary ammonium and phosphonium thiocyanate ionic liquids was investigated. The process was first applied on synthetic solutions and then the conditions defined for an efficient yttrium/europium separation were tested on a real leachate obtained from the dissolution of a mixed yttrium/europium oxide recovered from lamp phosphor waste. It was found that extraction with the quaternary phosphonium ionic

liquid [C101][SCN] (O/A = 1 : 10, four counter-current stages) was more effective than extraction with the quaternary ammonium ionic liquid [A336][SCN] under similar experimental conditions. The co-extracted Eu(III) could be scrubbed with either 3 mol L⁻¹ CaCl₂ + 0.8 mol L⁻¹ NH₄SCN or feed solution at O/A = 1 : 1 and 1 : 10, respectively, in several cross-current simulations. Y(III) could be quantitatively stripped by deionized water at O/A = 1 : 5 in two cross-current simulations. The raffinate and the strip solutions were further treated for the recovery of Y(III) and Eu(III) by precipitation with ammonia solution, followed by calcinations at 400–450 °C. The purity of the obtained Y(III) and Eu(III) oxides were more than 98.2% and 98.7%, respectively. The present work can be considered as a novel separation technique which makes use of non-volatile and non-flammable organic solvents and with a limited number of process steps.

Conflicts of interest

There are no conflicts to declare.

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