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Novel tunable super-tough materials from biodegradable polymer blends: nano-structuring through reactive extrusion†

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Structuring blends on sub-micrometer scales, especially nano-scales, has a higher potential for improving their thermomechanical properties. Here, we propose a design strategy to fabricate compatible nano-blends by manipulating the reactions between two biodegradable polymers, e.g. polybutylene succinate (PBS) and polybutylene adipate terephthalate (PBAT), with extremely low free radical contents through reactive extrusion processing. Observed by transmission electron microscopy (TEM) and atomic force microscopy (AFM), it is found that PBAT is tightly surrounded by large amounts of PBS–PBAT co-polymers and dispersed in a PBS matrix with a particle size of less than 100 nm. We show how impact strength and polymer moduli can be improved simultaneously by decreasing the small amount of dispersed phase into nano-scale (droplet or lamina structures). With 5 wt% PBAT content in the PBS–PBAT blend, the notched impact strength of PBS is increased 1200% and the Young's modulus is increased 15%. Through *in situ* rheological monitoring and Fourier-transform infrared spectroscopy (FTIR) studies, the reason why nano-blends can be formed in such a low amount of peroxide is illustrated. Our investigation most significantly indicates the transformation of the partially compatible PBS–PBAT micro-blend into a fully compatible PBS–PBAT through nano-structuring. This work addresses the importance of reaction rate and mechanism in favoring the formation of co-polymers rather than homo-polymer crosslinking or self-decomposition in polymer blend modification *via* reactive extrusion design.

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Introduction

The development of super-toughened polymers with high impact strength possess great scientific significance and huge market potentials. This is because of the fact that high toughness can broaden the application of materials dramatically.¹ One of the widely used polymers in packaging applications is polystyrene (PS), which was discovered in 1839 and the PS market attained great commercial success with the discovery of high impact polystyrene (HIPS).^{2,3} From “living polymerization” to “accepted commercialization”, the HIPS family inspired scientists to develop high impact plastics *via* structure control. Extensive studies on the morphology of HIPS revealed the nano-phase separation of these polymers, between the polystyrene (PS) and its co-polymer with polyisoprene (PI) or polybutadiene (PB).⁴ The nano-structuring is the key factor to obtain high impact strength. Therefore, the structuring of polymer blends

or novel co-polymers on nano-scale by self-assembly of industrially available polymers raises much hope to fabricate the super-toughened materials.

At present, nearly 99% of all used plastics are non-biodegradable and of which 79% are discarded and accumulated in landfills or in the natural environment as of 2015.⁴ Roughly 12 000 Mt of plastic will be generated by 2050 if current production and management trends continue.⁵ This will become an increasingly pressing problem for governments, scientists and the general population. Therefore, the development of biodegradable polymers from renewable resources has increased worldwide.⁶ These biodegradable polymers are expected to replace traditional petroleum-based plastics in commodity and engineering applications.^{7,8} However, the amount of bio-plastic used in the world is significantly less than the potential market, due to the limited performance of important properties and higher cost of the few commodity biodegradable polymers in comparison to petrochemical plastics. To increase the use of biopolymers there is a need to improve their performance characteristics or to develop novel properties customized to satisfy specific applications. Taking polybutylene succinate (PBS) as an example, this material possesses high elongation, good biodegradable and high heat deflection temperature (HDT),⁹ however, the notched impact strength of the PBS is very low as reported (40 J m^{−1}).¹⁰ If high

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impact strength PBS is developed, the materials can find widespread applications in markets.

Blending has long been considered to be a simpler and lower cost strategy to modify in bringing new properties to the polymer families. However, blending different polymers naturally tends to lead to phase separation on the macroscopic scale; the dispersed phase normally exists at the micrometer scale, and therefore it cannot maximize the properties of the different components. Consequently, substantial improvement of the thermal and mechanical properties such as high toughness, high stiffness and high-temperature creep resistance can only be achieved by improving the miscibility and dispersion state, especially at the nano-scale¹¹ – as confirmed by the HIPS story. According to the drop breakup theory in polymer blends, the diameter of the droplet of the dispersed phase D can be determined by eqn (1):¹²

$$D = \frac{4\mathcal{T}\eta_r^{\pm 0.84}}{\dot{\gamma}\eta_m} \quad (1)$$

where $\mathcal{T}$ is the interfacial tension, $\dot{\gamma}$ is the shear rate, η_m is the viscosity of main matrix, $\eta_r = \frac{\eta_d}{\eta_m}$, η_d is the viscosity of the dispersed phase. Therefore, to decrease the diameter of the dispersed phase, the interfacial tension should be decreased, or increase the viscosity of the main matrix.

So far in polymer science, three main methods have been proposed to obtain nano-structure in polymer blends based on the above theory: (i) high-shear flow processing,^{13,14} (ii) *ex situ* A–B block polymer synthesized and blended with A and B homopolymers,¹⁵ and (iii) polymerizing a monomer of one polymer in another matrix of macromolecules by reactive blending.^{16–19} Among them, reactive extrusion has been extensively researched for its simple and convenience in industrial processing.²⁰ However, compared to the synthesis of large macromolecular structure from monomer *via in situ* reactive extrusion, fewer research has been performed on melt blending of existing high molecular weight polymers though reactive extrusion as a method to obtain nano-scale blends, especially in the biodegradable plastic fields. Also, how to achieve large scale manufacturing of nano-dispersion *via* reactive extrusion in controlling the polymer properties through peroxide usage is unclear in the scientific literature to the best of our knowledge. Pernot *et al.*'s²¹ former research presents a principal design describing the formation of co-continuous nanostructure *via* lab-made polyethylene (PE) and polyamide (PA) in reactive blending. The research determined several fundamental facts as regards to structuring of nano-blends. For example, random graft co-polymer chains should be synthesized *in situ* by reactive blending two polymers which carry complementary reactive groups, followed by a coupling reaction that should be processed quickly.

Based on this fundamental work and previous research on nano-blends, here we present a general strategy to obtain high performance biodegradable blends (in the nano-scale) by improving miscibility for a pair of industrial biodegradable polymer pairs: PBS and PBAT. The chosen materials show different reactivity with peroxide at high temperatures, either

crosslinking – the main mechanism – or decomposition. It is determined that biodegradable binary nano-blends exhibiting exceptional properties like super toughness with high modulus, high melt strength and improved thermal stability which are unattainable by using classical micro-blends. For example, our group's former research shown that micro-blending of 70 wt% PBS/30 wt% PBAT could improve the toughness of the PBS but meanwhile the modulus decreased a lot.^{22,23} Here we find that only 5 wt% PBAT can improve the toughness of PBS dramatically without the loss of high modulus of PBS when dispersing the PBAT into nano-scale. Several goals are achieved in our current research: (i) by carefully choosing the polymer pairs, nano-blends can be obtained by reactive extrusion and the mechanism of the nano-blends formation has been discussed here to guide the future nano material designing; (ii) the effects of the peroxide usage and its reaction with the polymer components is discussed; (iii) high impact strength and high melt strength PBS nano-blends can be processed like traditional blending without the need to change the current equipment or production speed; (iv) the low contents of peroxide initiator in this research meets the development of industrial environmentally-friendly processes; and furthermore biodegradable blends are expected to be developed base on the formulation and concept proposed here.²⁴

Experiment and methods

Materials

Commercial PBS (Tunhe Th803s from Xinjiang Blueridge Tunhe Chemical Industry Co., Ltd. with weight-average molecular weight (M_w) $\approx 2.3 \times 10^4$ g mol^{−1}), PBAT (Tunhe Th801t from Xinjiang Blueridge Tunhe Chemical Industry Co., Ltd with $M_w \approx 7.50 \times 10^4$ g mol^{−1}), and peroxide(2,5-bis(*tert*-butylperoxy)-2,5-dimethylhexane, also known as 2,5-bis(*tert*-butylperoxy)-2,5-dimethylhexane or Luperox 101 from Sigma-Aldrich company) are used here. Chloroform (CHCl₃) for gel contents calculation is obtained from Sigma-Aldrich company and used without further purification. The PBS and PBAT are dried at 60 °C for 24 h before processing.

Sample preparation

The blending of PBS/PBAT in the presence of peroxide initiator is *in situ* extruded in a twin-screw extrusion (Leistritz Micro-27, Germany) with a screw diameter of 27 mm and an L/D ratio of 48 and defined as nano-blends base on the morphological structure. The blends are subjected to extruder processing at temperatures of 175–190 °C (feeding to melting zone), with feeding speed at 5 kg h^{−1} and screw speed at 100 rpm. Following the extrusion process, the over-night dried pellets are injected into mechanical testing samples by a DSM explore system (DSM 15cc Twin Screw Micro-Compounder, Netherlands) for characterization. The injection is completed in 2 min at 175 °C with a screw speed of 100 rpm. The blends of PBS/PBAT without peroxide are defined as micro-blends and experience the same processing as above.

Microstructural observations

The microstructure is characterized by scanning electron microscope (SEM), transmission electron microscopy (TEM) and atomic force microscopy (AFM). SEM is performed under a Phenom ProX (Netherlands) set to an accelerating voltage of 15 kV, and TEM is examined by using a JEOL JEM-1200 Ex II operating at an accelerating voltage of 80 kV. Ultra-thin specimens (70 nm) for TEM observation are cut from the middle section of molded samples in a perpendicular direction to the flow. The cut is performed under cryogenic conditions with a RMC PowerTome XL ultra-microtome with RMC CRX cryo-sectioning attachment using a diamond knife at $-80\text{ }^{\circ}\text{C}$, and the film is retrieved on 300 mesh Cu grids. The specimens for AFM imaging are prepared by Leica Microtome (Germany) at room temperature and performed on a AFM instrument with Multimode 8 from Bruker Nano Inc., CA, U.S.A. The scanning is done at peak force tapping model at constant scanning rate of 0.401 Hz.

Rheological properties characterization

The biopolymer (PBS and PBAT)/peroxide *in situ* reaction is performed on rheometer (Anton Paar MCR320) at different temperatures and different peroxide concentrations. The time sweep of the PBS/peroxide and PBAT/peroxide is performed at $175\text{ }^{\circ}\text{C}$ with a fixed frequency of 1 Hz. All the rheological testing is under N_2 protection.

The evolution of the dynamic modulus and viscosity of the injection samples (micro-blends and nano-blends) are measured from 0.1 to 100 rad s^{-1} (1% strain) at different temperature – 180, 190, 200 and $210\text{ }^{\circ}\text{C}$. To calculate the flow activation energy of the blends, the zero-shear viscosity (η_0) of the blends is obtained from the dynamic frequency sweep along with fits to the following Carreau model:²⁵

$$\eta(\dot{\gamma}) = \frac{\eta_0}{[1 + (\tau\dot{\gamma})^2]^P} \quad (2)$$

where $\eta(\dot{\gamma})$ is the viscosity at shear rate $\dot{\gamma}$, τ is the relaxation time of the material, P is determined by least-squares regression. The flow activation energy of the blends is obtained by linear fitting the zero shear viscosity as a function of the characterization temperatures.

Differential scanning calorimetry (DSC)

The crystallization and melting points of the materials are characterized by DSC (DSC Q200, TA, US) with a cooling and heating rate of $10\text{ }^{\circ}\text{C min}^{-1}$ under N_2 protection. The crystallinity of PBS is calculated by the following eqn (3):

$$X_c = \frac{\Delta H_m}{w_f \Delta H_m^0} \times 100\% \quad (3)$$

where the ΔH_m is the melting enthalpies of PBS in the blends, ΔH_m^0 is the melting enthalpies of assuming 100% crystalline PBS (220 J g^{-1} here)²⁶ and w_f is the weight fraction of PBS in the blend.

FTIR spectrum characterization

The biopolymer/peroxide *in situ* reacted samples (on rheometer) are characterized immediately in Fourier Transform Infrared (FTIR) spectrometer equipped with a smart orbit ATR (Nicolet 6700, Thermo Scientific).

Mechanical and thermal mechanical testing

Uniaxial tensile tests are performed using dog-bone shaped tensile samples with a gauge length of 25 mm and a width of 6 mm at a strain rate of 50 mm min^{-1} according to ASTM D638. An extensometer is used to calibrate strain during uniform elongation. Notched impact tests are performed by a Testing Machine Inc. (TMI) instrument (Testing Machine Inc. US) according to ASTM D256. Each test is repeated at least 5 times.

Dynamic Mechanical Analysis (DMA) is carried out with a DMA Q800 from TA Instruments. A dual cantilever clamp is used at the frequency of 1 Hz and oscillating amplitude of 15 mm. The samples are heated from -70 to $185\text{ }^{\circ}\text{C}$ at a heating rate of $3\text{ }^{\circ}\text{C min}^{-1}$.

Gel contents calculation

The gel contents of the PBS/PBAT blends with peroxide are calculated by dissolve-extraction method in accordance with ASTM D2765. The blends are dissolved in chloroform for 48 h and the insoluble parts are extracted and dried for 3 days in a vacuum oven at $50\text{ }^{\circ}\text{C}$ to remove the CHCl_3 . The residue of insoluble polymer is reported as % gel content.

Results and discussion

Super-toughened binary nano-blends

The TEM images of the as-formed nano-blends with different PBAT contents are shown in Fig. 1. A clear, homogeneous dispersed phase made of nano-scale PBAT is observed with characteristic particle diameters below 100 nm. The nano-structures are tailored by changing the composition ratio of the main PBS and dispersed PBAT. At low PBAT loadings (5 wt% PBAT shown in Fig. 1a and 10 wt% PBAT shown in Fig. 1b), the homogeneous phase is dispersed with a diameter of approximately 20 nm. The dispersed nano-droplet develops to the nano-lamina structure with characteristics nano-dots of about 10 nm at 15 wt% PBAT loading as shown in Fig. 1c, and further develops to nano-droplet of $\sim 120\text{ nm}$ at 20 wt% PBAT as shown in Fig. 1d. Nano-droplet or nano-lamina structures can be obtained by changing the contents of the dispersed phase. It is hypothesized that PBS–PBAT co-polymer contents formed during reactive extrusion increased with increasing PBAT content. And the existence of the co-polymer decreases the interfacial tension between PBS and PBAT, thus decreases the diameter of the PBAT droplet based on eqn (1). However, the diameter of the PBAT droplet further increased to $\sim 120\text{ nm}$ resulting from the highest PBAT loadings (20 wt%) as the diameter of the droplet increased with increasing disperse contents.²⁷

The blends are dissolved in chloroform to separate the possible homo-polymer gelation formed by the reactive

Fig. 1 Super-toughened nano-structured PBS/PBAT binary blend. Transmission electron micrographs for: (a) extruded 95PBS/5PBAT blends with 0.02 phr peroxide initiator; (b) extruded 90PBS/10PBAT blends with 0.02 phr peroxide initiator; (c) extruded 85PBS/15PBAT blends with 0.02 phr peroxide initiator; (d) extruded 80PBS/20PBAT blends with 0.02 phr peroxide initiator.

extrusion process. It is found that the gel contents (shown in Table S1†) decrease from 15.8% (5 wt% PBAT) to 0% with increasing PBAT contents (15 wt% PBAT). The high gel contents of PBS95–PBAT5 blends with 0.02 phr peroxide is mainly caused by the self-crosslinking of the PBS. With increasing PBAT contents, the homo-polymers' gelation is suppressed and PBS–PBAT co-polymers are largely formed, resulting to the zero-gel at 15 wt% and higher PBAT. The low gel contents and strong shear thinning produced by the dynamic crosslinking network ensured the success of the melt processability of these materials in twin-screw extrusion, and the flow activation energy did increase slightly to $38.24 \text{ kJ mol}^{-1}$ compared to the micro-blends of $28.68 \text{ kJ mol}^{-1}$ (confirmed by zero-shear viscosity at different temperatures as shown in Fig. S1†), indicating the low energy processing of these nano-blends as the traditional processing of the micro-blends. This is because of the low dosage of peroxide used in the current research.

The influence of the morphology and PBAT contents on the mechanical performance of the blends is shown in Fig. 2. The notched impact strength of the blends to reflect the toughness is shown in Fig. 2a. The formation of the nano-structure results in a high impact strength up to 720 J m^{-1} , which infers that the

material displays super-toughness.²⁸ The presence of only 5 wt% PBAT endows the nano-blends with much higher impact strength ($\sim 503 \text{ J m}^{-1}$) compared to that of 20 wt% PBAT in the micro-blends (200 J m^{-1}), with a transition from complete break to hinge impact behaviour. The reduced use of PBAT ensure the super-toughened blends without sacrifice of the modulus of the PBS matrix, broadening the application of this blend.

In addition to the super-toughness qualities, the nano-blends also exhibit superior performance in other mechanical properties. The nano-blends exhibit higher tensile modulus compared to the micro-blends, as shown in Fig. 2b. Compared to the micro-blends where the tensile modulus is located between the pure PBS ($613 \pm 23 \text{ MPa}$) and PBAT ($70 \pm 7.5 \text{ MPa}$) which is demonstrated in Table S2 in ESI Section,† the modulus of PBS95/PBAT5 nano-blends is higher than that of pure PBS, reaching $705 \pm 41 \text{ MPa}$, overcoming PBAT's shortcoming of low modulus. Furthermore, the moduli of nano-blends are higher than that of the micro-blends at same composition ratios. The unusually high modulus is believed to be a result of the reinforcement of the nano-dispersion PBAT especially as the crystallinity of PBS decreased compared to the micro-blends because of the branching/crosslinking (the crystallinity of the blends obtained from 1st

Fig. 2 Superior properties of the binary nano-blends. (a) Notched impact strength of the nano-blends and micro-blends with different PBAT contents, (b) dependence of tensile modulus on PBAT for micro and nano-blends; (c) dependence of elongation at break on PBAT contents for micro and nano-blends; (d) dependence of elongation at yield on PBAT contents for micro and nano-blends.

heating DSC curves are shown in Fig. S2†). The elongation at break (ϵ_b) of the blends is shown in Fig. 2c and it's found that that the ϵ_b of nano-blends decrease compared to the micro-blends, a characteristic of highly entangled materials.²¹ However, the elongation at yield of the nano-blends is much higher compared to the micro-blends, with a transition from plastic-like to hard elastomer-like fracture behaviour as illustrated in Fig. 2d.

Biodegradable materials with high melt strength are obtained in our research because of the high entanglement of the molecular chains by reactive branching, as indicated from the melt dynamic moduli in Fig. 3. The storage modulus (G') and loss modulus (G'') of the blends with and without peroxide are shown in Fig. 3a. The micro-blends of PBS/PBAT exhibits liquid-like viscoelastic behaviour with G'' higher than G' . After

Fig. 3 High melt strength of the nano-blends revealed by rheological studies at 190 °C. (a) The dependence of storage modulus (G') and loss modulus (G'') on frequency; (b) the dependence of complex viscosity on frequency.

Fig. 4 Improved high temperature creep ability of nano-blends revealed by dynamic mechanical analysis – dual-cantilever frequency sweep.

peroxide curing, both the G' and G'' increase and are much higher than the micro-blends. More importantly is that the G' is higher than the G'' in the nano-blends (solid-like behaviour), indicating the improved elasticity of the melt. The solid-like viscoelastic reflects that the nano-blends possess high melt strength.²⁹ The complex viscosity is also improved dramatically with the introduction of peroxide, as shown in Fig. 3b. Also, because of the branching and improved compatibility, the blends show strong shear thinning behaviour in the whole frequency range, indicating the disentanglement of the molecular chains in the testing frequency, especially in the long time scale (low frequency).³⁰ It's suggested that the relaxation in long time scale is ascribed to the high entanglement branching chains formed during the reactive extrusion.³¹ The high melt strength ensures the broad processing window and an array of applications for the nano-blends, such as blowing,

Fig. 6 Nano-structure PBS/PBAT binary blend formation mechanism. (a) curing of PBS and PBAT with 0.2 phr peroxide at 175 °C in the rheometer (solid: storage modulus; hollow: loss modulus); (b) the evolution of storage modulus (at 6.28 rad s⁻¹) on time in the continue frequency sweep for PBS and PBAT/peroxide at 175 °C.

thermoforming, and foaming to replace the widely used non-biodegradable petro-based plastics, expanding their applications in packaging market. Resistance to high temperature

Fig. 5 Crystallization and melting behavior of the nano-PBS/PBAT blends revealed by DSC curves: (a) cooling at 10 °C min⁻¹; (b) heating at 10 °C min⁻¹.

Fig. 7 The influence of peroxide concentrations and temperature on the chain structures of PBAT and PBS: (a) PBAT/0.2 phr peroxide at different temperatures; (b) PBAT/peroxide at 175 °C with different peroxide contents; (c) PBS/0.2 phr peroxide at different temperatures; (d) PBS/peroxide at 175 °C with different peroxide contents.

creep properties is also an important parameter for material to evaluate its dimensional stability at high temperature. The nano-blends possess high resistance to high temperature creep compared to the traditional micro-blends from the DMA testing shown in Fig. 4. It can be found that the storage modulus of the nano-blends declines slowly at temperature higher than the melting point of PBS (114 °C). In contrast, the storage modulus of the micro-blends without reaction decrease to zero directly at the melting point of PBS. The high temperature resistant of the nano-blends is believed to result from the high levels of entanglement of the molecular chains as revealed by the rheological studies.

The crystallization behaviour of the micro and nano-blends is studied by DSC and shown in Fig. 5. Compared to that of the micro-blends, the crystallization temperature has been increased after dispersing PBAT into nano-scale, as shown in Fig. 5a. It indicates that the nano-dispersed PBAT can be act as a more efficient nucleation agent for PBS, the same phenomenon has been observed in the previous research on nano-

blends of poly(vinylidene fluoride) (PVDF)/acrylic rubber (ACM).³² It can also be found that the double-melting peaks in the micro-blends are disappeared and transformed into one high temperature melting peak in nano-blends, as shown in Fig. 5b, which resulted from the improved perfection of the crystals in nano-blends, such as smaller crystal size or fully growth crystals.³³ It is suggested that the more perfect crystals also contribute the higher modulus in nano-blends. The crystallinity of the blends is shown in Fig. S2.† The crystallinity of the nano-blends reaches highest at 15 wt% PBAT is probably resulted from the large formation of the nano-lamina structure in the blends, as shown by the TEM in Fig. 1c.

Nano-blends formation mechanism

The aim of this work is to obtain PBS-PBAT co-polymer to improve the compatibility of different phases by a reactive extrusion process. Unfortunately, this reaction is difficult to control; it is difficult to obtain enough co-polymer but not over-

crosslinked or decomposed homopolymers in which the large formation of block co-polymers is the guaranteeing to decrease the size of dispersed phase into nano-scale. To solve this problem, we start from two biodegradable polymers which possess similar molecular structures and close radical reaction rates: PBS, a homo-polymer consisting of butylene succinate, and PBAT which can be regarded as a co-polymer of butylene succinate and dimethyl terephthalate. In other words, the polymers chosen here are a homo-polymer A and a co-polymer with structure A-B, similar to the former discussed HIPS.⁴ Although the PBS and PBAT have similar chain segments and close glass transition temperature (T_g) (shown as DMA testing in Fig. S3†), our research on morphology, completed by SEM (Fig. S4†), shows that the blends are partially compatible which form co-continuous structure with macroscopically noticeable phase separation at 15 wt% PBAT.

The reactivity of PBS/PBAT resulted from free radical attack on the hydrogen atoms along the hydrocarbon skeleton. The free radicals which are generated by peroxide decomposition attacked the labile protons on the secondary carbon sites of PBS/PBAT. The free radicals of PBS/PBAT underwent either grafting or chain cleavage degradation.³⁴ Furthermore, due to the high instability and reactivity of secondary free radicals, the grafting and degradation processes are extremely fast at high temperatures (>melting temperature) and led to either over cross-linking or serious degradation, respectively. While the over cross-linking of one phase in the reactive extrusion led to the phase separation as micelles,³⁵ consequently nano-structures could not be obtained. Thus, stabilization and consumption of free radicals in favor of branching on the backbone of the chains is most important to obtain stable nano-structures rather than experiencing over cross-linking or serious chain degradation.²¹ Suppressing over cross-linking through decreasing the amount of initiators is the key factor in this method. However, to obtain enough reacted co-polymers in the final blends, which increased the interfacial entropy to improve the miscibility of the components, a proper amount of initiator should be used. Our hypothesis is that this complication is overcome by the complementary reaction between the PBS, PBAT and the low dose radical initiator. This ensured the formation of large amounts of PBS-PBAT co-polymer rather than over-crosslinked PBS or degraded PBAT. Other than suppressing over-crosslink or thermal decomposition, another difficulty of free radical grafting arose from the competition between co-polymer formation and homopolymers cross-linking. It is suggested that this obstacle could be overcome by a close reaction rate between the PBS/PBAT and free radicals. To verify this, we simulated the reaction between PBS, PBAT and the radical initiator with different amounts at various temperatures in a rheometer. The rheometer is used to detect the chain structure evolution by real-time monitoring of the modulus variation.

Firstly, the dependence of modulus on reaction time for PBS/peroxide and PBAT/peroxide demonstrated in Fig. 6a reveals the possible reaction between the polymers and peroxide. The evolution of the modulus with time shows that the two polymers possess a fast and close reaction rate. It is known that the

reaction rates measured in homogeneous melts are close to that of rates under mixing.³⁶ The sharp increase of G' at 175 °C (Fig. 6a) during crosslinking of homo-polymers in the rheometer shows that the reaction took place quickly, even under static conditions. Also, the kinetics of reaction are very similar for both materials as indicated by the identical G' initial slopes³⁷ (Fig. 6a). The fast and close coupling reaction plays a key role during the PBS/PBAT co-polymer formation rather than cross-linked homopolymers, while the amounts of co-polymer work as *in situ* compatibilizer to promote stability of the nano-structures.

Besides the partial compatibility and fast/close reaction rate of the two polymers with peroxide, more importantly, the dependence of peroxide concentrations on the reaction of these two polymers are totally different. When the peroxide concentrations are increased it is found that the equilibrium storage modulus of PBAT decreased with increasing peroxide concentrations as shown in Fig. 6b. This resulted from the more serious degradation of the PBAT chains caused by more free radicals, rather than increased crosslinking. The extent of cross-linking in PBS increases with increasing peroxide concentrations as expected; which is reflected from the increased equilibrium storage modulus in the continuous time sweeps shown in Fig. 6b. The above description of the dependence of crosslink or chain degradation on peroxide contents and temperature is also verified by the FTIR studies.

The evolution of the structure of PBAT with the temperature and peroxide concentrations is revealed by FTIR and shown in Fig. 7a and b. Among the structure-related peaks, two peaks at 2853 and 2924 cm^{-1} appear in the range of 2800–3000 cm^{-1} are used to follow the structure evolution of the polymer chains

Fig. 8 The reaction mechanism between the biodegradable polymers and free radical initiators.

during the reaction with free radicals. These two peaks, which are caused by the vibration of $-\text{CH}$ group,³⁸ are believed to be from the free radicals attract of methylene on the carbon backbone of PBS and PBAT chains. Since the $-\text{CH}_2$ on the backbone of PBS and PBAT will be attacked by the free radicals and transformed into $-\text{CH}$. The peak intensity can be used to demonstrate the degree of the crosslinking or branching. The new peak intensity of PBAT/peroxide decreases with increasing peroxide concentrations and temperature, as shown in Fig. 7a and b. It means that with increasing peroxide concentrations/temperature, less $-\text{CH}_2$ is attracted by the free radicals, leading to the limited branching of the molecular chains at high peroxide concentrations. The evolution of the structure of PBS with the temperature and peroxide concentrations is also revealed by FTIR and shown in Fig. 7c and d. As indicated by the FTIR spectrums, the increasing intensity of the PBS/peroxide peaks with increasing peroxide content and temperature means that more $-\text{CH}_2$ groups are attracted by the free radicals and transformed to $-\text{CH}$, and finally more branching/crosslinking points are generated on the main chains, leading to the high crosslinking or branching. This is the first time we observed from FTIR spectrum showing the influence of

peroxide concentration on the structure evolutions of polymers in free radical reactions. The reaction mechanism based on the FTIR spectrum evolution is illustrated in Fig. 8.

Through decreasing the concentration of peroxide into small amount, both the over-crosslink of PBS and serious chain scission of PBAT are suppressed. Our hypothesis is that these complementary reactions between the PBS, PBAT and the low dose radical initiator ensured the formation of large amounts of PBS-PBAT co-polymer rather than over-crosslinked PBS or thermal degraded PBAT, which is the key factor to form nano-blends in this method. The similar chemical structure, fast and close reaction rate, as well as the complementary reaction worked together in the formation of nano-structures in the blends *via* reactive extrusion.

To verify the peroxide concentrations on the formation morphology of these two blends, the morphology of the PBS/PBAT blends with higher peroxide (0.2 phr used here) and lower peroxide (0.007 phr) is observed and compared to the nano-blends (0.02 phr peroxide), as shown in Fig. 9. By introducing different amounts of peroxide into PBS95/PBAT5 blends, it is found that only nano-structure could be formed with the appropriate peroxide contents (0.02 phr here). At 0.2 phr

Fig. 9 Schematic diagram and morphology observation of the structure evolution of the PBS95/PBAT5/peroxide blends on peroxide concentrations: (I) $C_{\text{peroxide}} = 0.2$ phr; (II) $C_{\text{peroxide}} = 0.02$ phr; (III) $C_{\text{peroxide}} = 0.007$ phr.

peroxide, the blend is over-crosslinked and difficult to melt-process (the gel contents reach as high as 38%), leading to the phase separation in micro-scale, as indicated by the red circle in the SEM photo (high peroxide concentrations) in Fig. 9I. It's suggested that the micro-separated droplet is the over-crosslinked micelles,³⁵ as indicated by case I; at low peroxide (0.007 phr), the PBS-PBAT co-polymers are deficient because of the less of free radicals. Therefore, the compatibility cannot be improved with small amount of peroxide, leading to the micro-dispersed PBAT in the extruded materials, as indicated by case III in Fig. 9. From the SEM in Fig. 9III, the PBAT dispersed in the PBS as a droplet with diameter of $\sim 2\ \mu\text{m}$, reflecting the phase separation.

As discussed, the formation of a large amount of co-polymer is the guarantee of the nano-dispersed of PBAT in PBS. To observe the morphology, AFM is applied to check the nano-blend structures. The AFM photographs of PBS95/PBAT5/0.02 phr peroxide and PBS85/PBAT15/0.02 phr peroxide which

show two different structures in TEM are given in Fig. 10. At low PBAT contents (shown as Fig. 10a and c), finely dispersed phase (low modulus PBAT indicated as dark points) as small as 80 nm can be clearly seen. Since the large amounts of the co-polymer are formed and tightly surrounded the PBAT phase, the size of the dispersed phase seems like larger than that shown in TEM. The brown phase detected in the AFM technology surrounding the low modulus PBAT is believed to be the co-polymer phase which possesses tapping modulus between neat PBS and PBAT. Thus, a core-shell structure with high affinity to the matrix are successfully formed in the nano-blends, which is believed to attribute the super-toughness of PBS. With increasing PBAT to 15 wt%, it can be found the dispersed morphology has been greatly changed. The AFM phase contrast micrograph of this blend is shown in Fig. 10b. No obvious dispersed PBAT phase can be found in this blends because of the large formation of co-polymers, same as the TEM observations. From the log(modulus) diagram shown in

Fig. 10 The AFM photograph of the PBS/PBAT nano-blends: height morphology: (a) PBS95/PBAT5/0.02 phr peroxide, (b) PBS85/PBAT15/0.02 phr peroxide; log modulus morphology: (c) PBS95/PBAT5/0.02 phr peroxide, (d) PBS85/PBAT15/0.02 phr peroxide.

Fig. 10d, elongated strips with core-shell structures are observed in the PBS matrix. The low modulus PBAT (shown as dark in AFM) parts are surrounded by large amounts of co-polymer phase shown as brown parts in the diagram. It is suggested that the co-polymers exhibit as nano-lamina structures in the TEM photos as indicated by Fig. 1c.

Conclusion

In summary, our research found that nano-scale blends with high performance which are unattainable from classical micro-blends can be obtained through reactive extrusion by selecting appropriate polymer pairs. Super-toughened PBS/PBAT nano-blends are prepared with small amount of PBAT dispersed as nano-scale phase in the continuous PBS phase. The nano-blends show higher modulus compared to the neat PBS, without sacrifice of the stiffness when introducing low modulus toughening PBAT. A 12-fold improvement in notched impact strength and 1.2-fold increasing in modulus has been achieved in the nano-blends. The DSC studies shown that, the PBAT can be acted as a nucleating agent for PBS to increase the crystallization temperature and crystal perfection when dispersing the toughening phase into nano-scale. The morphology observation by AFM show the formation of large amounts of co-polymers surrounding the toughening phase, leading to the fine dispersion of the PBAT.

In reactive extrusion, favoring the formation of co-polymers rather than self-crosslinking or chain decomposition is the key factor in improving the performance of polymer blends, including thermomechanical performance and processability. The *in situ* rheology time sweeping monitoring and FTIR in this study indicates the important considerations concerning the reaction rates and the influence of peroxide amounts on the reaction mechanism of polymers in reactive extrusions, to co-polymer formations. The final dispersion morphology of the polymer blends is influenced by the peroxide amounts in the reactive extrusion.

The cost-effective preparation method used in this work does not require any solvents or extra catalysts and the extremely low amount of peroxide initiator used ensures the green processing of the products. The nano-structured materials engineered from binary biodegradable polymer blends show super toughness with high modulus and improved melt strength. The newly developed materials show promising application in sustainable packaging use where high toughness, high melt strength and potential biodegradability are required. Since the materials are developed from two biodegradable polymers and very low concentration of peroxide is used here, it is expected to be biodegradable. However, the detailed composability studies need to be finished to claim the biodegradability of these developed nano-blends.

Conflicts of interest

There are no conflicts to declare.

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