



Cite this: *Catal. Sci. Technol.*, 2019, 9, 5142

Towards coupling direct activation of methane with *in situ* generation of H₂O₂

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Due to the explosive nature of H₂, O₂ and CH₄ mixtures, the concept of coupling *in situ* synthesis of H₂O₂ with low-temperature single-step methane conversion to methanol has not received sufficient attention. This study aimed to investigate this process using a microchannel reactor, which offers the opportunity to explore the process under a wide range of concentrations. Direct methane activation with *in situ* generation of H₂O₂ was successfully demonstrated in a microcapillary containing Au-Pd nanoparticles embedded on its silica-coated walls. The effect of H₂, O₂ and CH₄ partial pressures, H₂/O₂ molar ratio, gas-to-liquid (G/L) ratio and liquid phase weight-hourly-space-velocity (WHSV) on the productivity and product distribution was investigated. CH₄ partial pressure had the most significant effect on the productivity, while H₂ and O₂ partial pressures influenced the productivity less. The methane activation rate was found to be correlated with the H₂O₂ formation rate. With only O₂ or pre-formed stabilized H₂O₂ methane activation was not found, *in situ* H₂O₂ synthesis was therefore essential. G/L affected neither the product distribution nor the productivity, however, lowering WHSV altered the product distribution favoring methanol formation.

Received 3rd July 2019,
Accepted 29th August 2019

DOI: 10.1039/c9cy01304k

rsc.li/catalysis

1. Introduction

Natural gas with methane as its main component is considered to be a relatively clean source of fossil energy and a potentially valuable raw material. However, full exploitation of the enormous methane resources is yet to be realized mainly due to the challenges associated with transportation and storage. Therefore, it is of great interest to convert methane to products (chemical or fuel) that can be easily shipped.^{1,2} Indirect methane conversion, to syngas and then to alcohols or hydrocarbons, is an advanced and mature technology being widely practiced in industry. This route involves an energy-intensive thermochemical oxidation (e.g. steam reforming and autothermal reforming) to convert methane to CO and H₂, which are then fed to a methanol synthesis process or to a Fischer-Tropsch synthesis process that involves production of a mixture of hydrocarbons including paraffins, olefins and alcohols.^{3–5} However, the costly nature of such multistep processes, mainly originating from the syngas production step, has triggered the development of an alternative low-temperature single-step approach for the direct selective oxidation of methane to methanol.⁶

Cleaving the C–H bonds of methane, which is relatively an inert molecule at low temperatures ($\Delta H_{C-H} = 439.57$ kJ

mol^{–1}), and activating the oxidant to form and regenerate the active sites are the major challenges of this approach.^{6,7} Hydrogen peroxide (H₂O₂) has been reported as a promising oxidant when used with catalysts such as CuFe–ZSM-5 (ref. 8 and 9) and Au–Pd nanoparticles.^{10,11} However, using pre-synthesized H₂O₂ is not only economically unviable, as it is more expensive than methanol, but it is also environmentally undesirable since the traditional anthraquinone process to produce H₂O₂ results in significant waste generation.¹² In this view, *in situ* generation of H₂O₂ coupled with direct methane oxidation seems to be a strategy worthy of intensive investigation. In spite of an early work¹³ reporting higher selectivity towards methanol in presence of *in situ* generated H₂O₂, the concept of coupling H₂O₂ synthesis with methane oxidation has not received sufficient attention in the literature. This basically stems from the fact that H₂, O₂ and CH₄ mixtures are explosive under a wide range of concentrations,¹⁴ and need to be diluted to guarantee safe operation, thus resulting in much lower methanol production rates.

This study aims to address this limitation by coupling the *in situ* generation of H₂O₂ with the direct methane conversion in an inherently safe washcoated microchannel reactor which offers the opportunity to explore the process under a wide range of concentrations. This catalytic washcoated microchannel reactor, which showed an outstanding performance for the direct H₂O₂ synthesis in our previous work,¹⁵ is obtained by embedding Au-Pd nanoparticles on the silica-coated walls of a microcapillary. In this context, the effects of

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CH_4 , O_2 and H_2 partial pressures, O_2/H_2 molar ratio, gas-to-liquid ratio and residence time on product yields were investigated.

2. Experimental

2.1. Catalyst preparation

Fused silica capillaries (320 μm ID) containing a 4 μm pre-coated layer of SiO_2 on the wall (CP-SilicaPLOT, Agilent) were used as the microchannel reactor. Adopting the catalyst synthesis and coating from our previous work,¹⁵ the silica layer was first treated by a 1 M ammonium nitrate solution which was flushed through the capillary using a syringe pump. The capillaries were then dried and calcined at 120 and 300 $^\circ\text{C}$, respectively. Prior to metal deposition, polyelectrolyte multilayers (PEMs) were built on the silica surface. It has been shown that PEMs enabled a facile control over metal ions loading and distribution by providing highly distributed charged surfaces.¹⁶ To form PEMs on the support, a layer-by-layer approach, in which 10 mg mL^{-1} polyacrylic acid (PAA, 35 wt% in H_2O , Sigma-Aldrich) and 2 mg mL^{-1} polyethylene imine (PEI, 50 wt% in H_2O , Sigma-Aldrich,) solutions were alternatively flushed through the microcapillary, was taken. A bi-layer polyelectrolyte was then obtained by repetition of the same procedure. Metal deposition was carried out upon formation of PEMs. For a desired metal loading of 5 wt%, considering coating weight and void fraction,^{15,17} a 5.7 $\text{mg}_{\text{metal}} \text{mL}^{-1}$ ($\text{Au}:\text{Pd} = 1:2$, molar ratio) solution in DI water was prepared using HAuCl_4 (Aldrich, 30 wt% in HCl) and K_2PdCl_4 (Sigma, 99.99%) as the precursors. The solution was then flushed and held still in the capillary, to ensure metal ion binding on the surface before removing the excess by N_2 . Metal deposition was followed by a reduction step, in which NaBH_4 solution was flushed until the capillary color turned into dark black, indicating a successful reduction of the deposited metal. Eventually, drying at 120 $^\circ\text{C}$ and calcination at 380 $^\circ\text{C}$ were carried out.

2.2. Catalyst characterization methods

Formation of PEMs on the silica support was examined using XL30-ESEM-FEG scanning electron microscope (SEM) operated at 5 kV with a working distance of 10 mm from the sample. Metal particles distribution on the surface was studied by a FEI Tecnai G2 Sphera transmission electron microscope (TEM). The capillaries for TEM analyses were crushed and suspended in drops of ethanol. The X-ray photoelectron spectroscopy (XPS) measurements of the powder catalyst were carried out with a Kratos AXIS Ultra spectrometer, equipped with a monochromatic X-ray source and a delay-line detector (DLD). Spectra were obtained using the aluminium anode ($\text{Al K}\alpha = 1486.6 \text{ eV}$) operating at 150 W.

2.3. Catalytic activity measurement

The schematic representation of the flow set-up is shown in Fig. 1. To keep a constant reaction temperature at 40 $^\circ\text{C}$, the

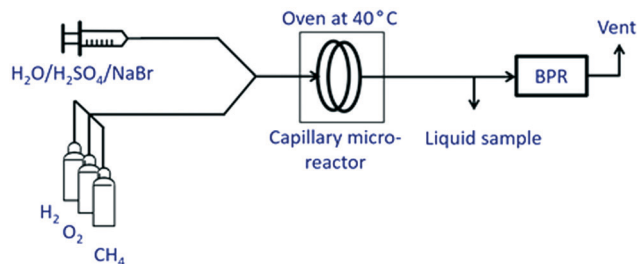


Fig. 1 Scheme of the setup used for conducting the experiments.

microcapillary was put in a thermostatic oven. Prior to the experiments, formation of a Taylor flow regime with alternating gas bubbles and liquid slugs under reaction conditions was confirmed using a transparent empty fused silica capillary. The liquid phase contained 0.05 M H_2SO_4 and 10 ppm NaBr (to inhibit H_2O_2 decomposition to H_2O (ref. 18)) in DI water, and was sent to the microreactor using a syringe pump (Teledyne ISCO 500D). To avoid any explosion risk in the downstream, the outlet gas mixture was diluted by N_2 . The pressure was kept constant in the system by a back-pressure regulator (BPR) placed in the downstream after the gas-liquid separation unit. The gas flow rates were adjusted by mass flow controllers before the capillary inlet. The pressure was measured and monitored before and after the capillary. As presented in Table 1, the reaction was studied at different H_2 , O_2 and CH_4 partial pressures, gas-to-liquid ratios (G/L, v./v.) and liquid phase weight-hourly-space-velocities (WHSV, $\text{kg}_{\text{Liq.}} \text{kg}_{\text{cat.}}^{-1} \text{h}^{-1}$). Gas samples were analyzed with an online compact GC (column: molsieve plot 5 m 0.32 mm) equipped with a TCD detector. As CH_4 conversion was typically low ($\leq 0.1\%$), it was not used for interpretation of the results. Liquid samples were collected every 45 min of reaction time. Part of the sample was used for the determination of H_2O_2 by titration using standard solution of cerium(IV) sulfate (Sigma Aldrich) and ferroin (VWR Chemicals) as an indicator. The other part of liquid sample was taken to quantify the formation of oxygenates. The amount of methanol in the sample was determined using an offline GC (Varian CP-3800). Aggregated concentration of methanol and methylhydroperoxide was measured by adding NaBH_4 to the liquid sample to convert the latter to

Table 1 Set of reactions conditions employed for the parametric study

Entry	P_{O_2}	P_{H_2}	P_{CH_4}	Total P (bar)	WHSV	G/L
1	1	1	18	20	4200	2.5
2	1	1	28	30	4200	2.5
3	1	1	8	10	4200	2.5
4	0.5	0.5	8	9	4200	2.5
5	3	3	8	14	4200	2.5
6	6	6	8	20	4200	2.5
7	1	0.5	28	29.5	4200	2.5
8	0.5	1	28	29.5	4200	2.5
9	1	1	28	30	4200	5
10	1	1	28	30	2100	5



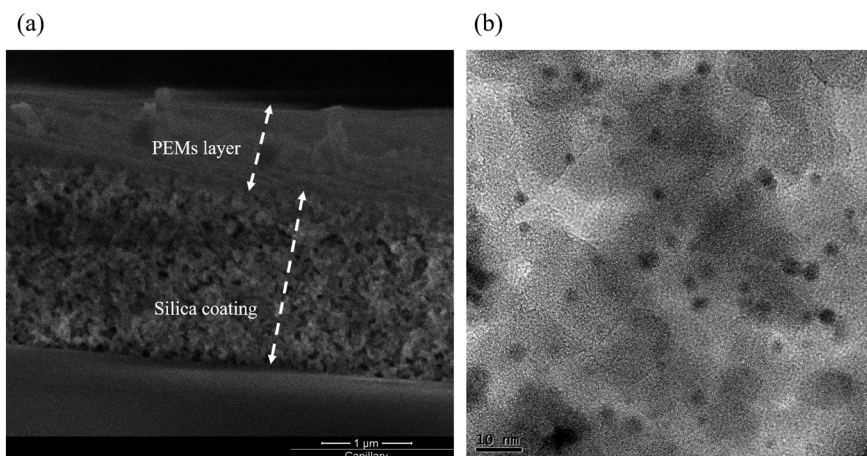


Fig. 2 (a) SEM showing the formation of PEMs, (b) TEM image of calcined Au-Pd capillary.

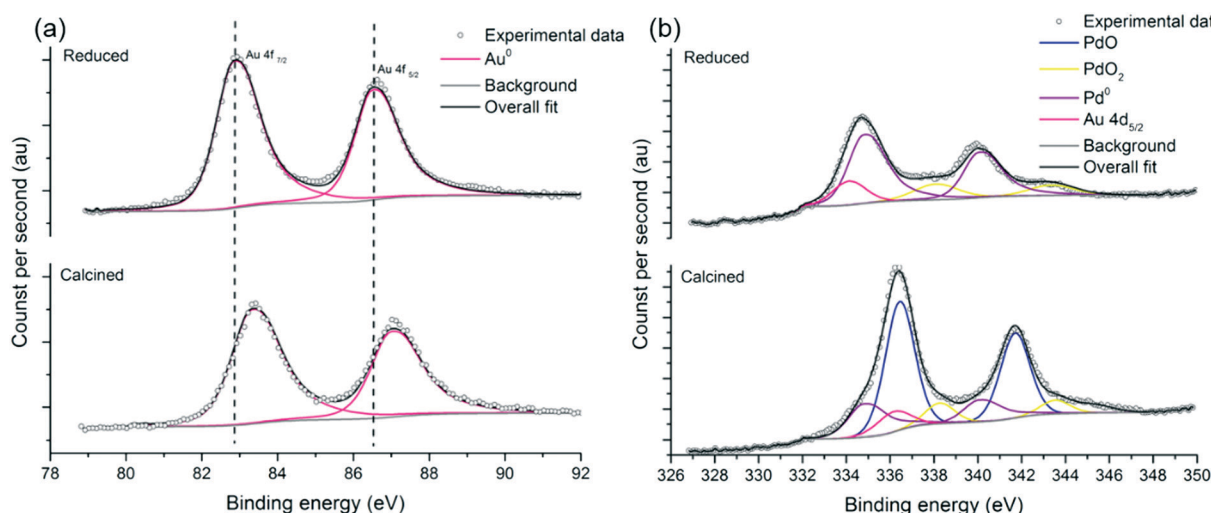


Fig. 3 Experimental and fitted (a) Au 4f and (b) Pd 3d XPS for reduced and calcined AuPd/SiO₂ powder catalysts.

methanol which is then readily detectable on the GC.¹⁹ The liquid samples were also quantified for formic acid formation

using an HPLC 155 (Shimadzu Sil-20AC). Oxygenate productivity was then calculated using following expression:

$$\text{Productivity} \left(\text{mol}_{\text{oxygenates}} \text{ kg}_{\text{metal}}^{-1} \text{ h}^{-1} \right) = \frac{\text{Liquid flow rate} (\text{mL h}^{-1}) \cdot C_{\text{oxygenate}} (\text{mol mL}^{-1})}{m_{\text{metal}} (\text{kg})} \quad (1)$$

Table 2 XPS binding energies for Au 4f_{7/2} and Pd 3d_{5/2}, relative amount of each Pd species and surface Au/Pd atomic ratios of AuPd/SiO₂ powder catalyst before and after calcination

Sample	Binding energy Au 4f _{7/2} (eV)	Pd 3d _{5/2}		Au/Pd
		Binding energy (eV)	Peak designation (relative %)	
Reduced	82.8	338.1	PdO ₂ (19%)	0.74
		334.8	Pd ⁰ (81%)	
Calcined	83.3	338.2	PdO ₂ (10%)	0.41
		336.4	PdO (65%)	
		334.8	Pd ⁰ (25%)	

3. Results and discussion

3.1. Catalyst characterization

The formation of PEMs layers of ~1 μm thickness was confirmed by SEM as presented in Fig. 2a. Successful deposition of metal nanoparticles on silica support was also evident as shown in TEM image (Fig. 2b). TEM indicated a narrow size distribution of metal nanoparticles over the support, yielding small particle size of 2.9 ± 1.2 nm. XPS was employed to evaluate the elemental composition and the oxidation state of Au and Pd at the surface of an AuPd/SiO₂ powder catalyst prepared in a similar way as the AuPd wall-coated capillary



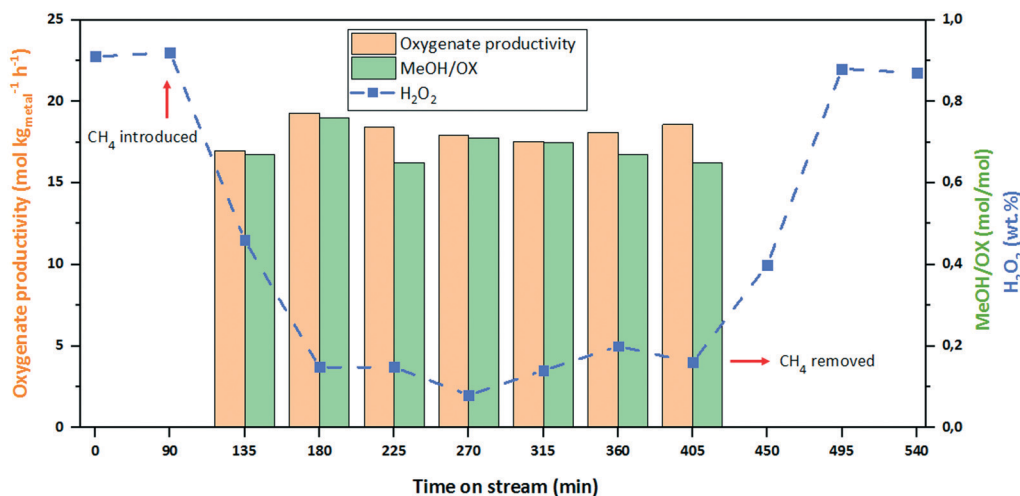


Fig. 4 Oxygenate productivity, MeOH/OX ratio and outlet H₂O₂ wt% over time at a total pressure of 20 bar. Gas composition was switched from H₂/O₂ = 50/50 to H₂/O₂/CH₄ = 5/5/90 after 90 min (see Table 1, entry 1). Gas composition was switched back to H₂/O₂ of 50/50 after 405 min.

(Fig. 3). The Au 4f_{7/2} and Pd 3d_{5/2} binding energies (BE) along with XPS-derived atomic ratios are shown in Table 2. The Pd 3d spectra characterized by two spin-orbit components of 3d_{5/2} and 3d_{3/2} exhibit three doublets attributed to three different Pd species-PdO₂, PdO and Pd⁰.^{20,21} The reduced sample predominantly consists of metallic Pd, with small amount of PdO₂, most likely formed due to oxidation in air during sample handling.²¹ The Au 4f spectra was typical of metallic Au. The BE of Au (4f_{7/2}) was found to be 82.8 eV, exhibiting a prominent negative shift when compared to bulk Au (84 eV) or small Au nanoparticles (83.5–84 eV).²² This was proposed to be due to charge transfer from Pd to Au and was evident of Au–Pd alloying.²² Upon calcination, the PdO phase dominated but 25% of the Pd was still present in its metallic form. This is in agreement with our previous finding,²³ where it was also found that during *in situ* generation of H₂O₂, the PdO phase present in the calcined catalyst was readily reduced and stayed at its metallic state. XPS also revealed no contamination from Cl, ensuring effectiveness of the washing step during synthesis.

3.2. Catalytic activity

The catalytic microcapillary reactor was first tested at 20 bar, gas phase composition of H₂/O₂ = 50/50, WHSV of 4200 kg_{liq.} kg_{cat.}⁻¹ h⁻¹ and G/L of 2.5 to ensure *in situ* generation of H₂O₂. Upon reaching a stable concentration of ~0.9 wt% H₂O₂ in the liquid phase, a methane activation experiment was initiated by introducing CH₄ to the reactor, thus changing the gas phase composition to H₂/O₂/CH₄ = 5/5/90 (Table 1, entry 1). It is believed that CH₄ activation in the presence of H₂O₂ over Au–Pd catalyst proceeds through generation of methyl hydroperoxide (CH₃OOH), an intermediate which then is converted to methanol.¹¹ In addition to that, formation of formic acid and CO₂, originating from methanol and methyl hydroperoxide over-oxidation has also been reported in the literature, es-

pecially when pre-formed H₂O₂ is utilized as the oxidant.²⁴ In this study, the formation of neither formic acid nor CO₂ was evident. The absence of over-oxidation reactions may be attributed to the significantly shorter residence time (13 s) employed in this work compared to that of batch systems (>5 min). Of course, trace amounts (<1 ppm) of formic acid and CO₂ below the detection limit of the utilized instruments might be present. As shown in Fig. 4, a stable catalytic activity towards both H₂O₂ formation and CH₄ activation was observed over a period of 9 h. H₂O₂ concentration at the liquid phase reached a stable amount of ~0.2 wt%, and an oxygenate productivity of 18.1 mol kg_{metal}⁻¹ h⁻¹ was obtained. The product distribution was also stable over time, resulting in a methanol-to-oxygenates molar ratio (MeOH/OX) of ~70%. Upon removal of CH₄ from the reaction medium it was observed that the catalyst was able to retain its original activity towards H₂O₂ formation after being subjected to CH₄ oxidation for 5.25 h. The obtained oxygenate productivity was about one order of magnitude higher than that reported by Ab Rahim *et al.*²⁵ who used a batch system using a gas composition of 0.86% H₂, 1.72% O₂, 75.86% CH₄ and 21.55% N₂ over a TiO₂ supported Au–Pd bimetallic catalyst at total pressure of 32 bar. The very dilute H₂ and O₂ concentrations in the latter case leads to much lower (18–20 times) H₂O₂ formation rates compared to the microreactor system. Hence, the higher oxygenate productivity obtained here can be attributed to the higher rates of H₂O₂ generation in the microcapillary, suggesting that an effective coupling of the two reactions, is strongly dependent on the rate of peroxide formation. To further elucidate this conclusion, a parametric study was carried out, taking advantage of the inherently safe conditions of the microchannel reactor.

The effect of CH₄ partial pressure was studied by keeping H₂ and O₂ partial pressures at 1 bar, resulting in a roughly constant H₂O₂ (0.2 wt%) concentration in the reactor outlet. Although MeOH/OX remained unaffected, increasing CH₄



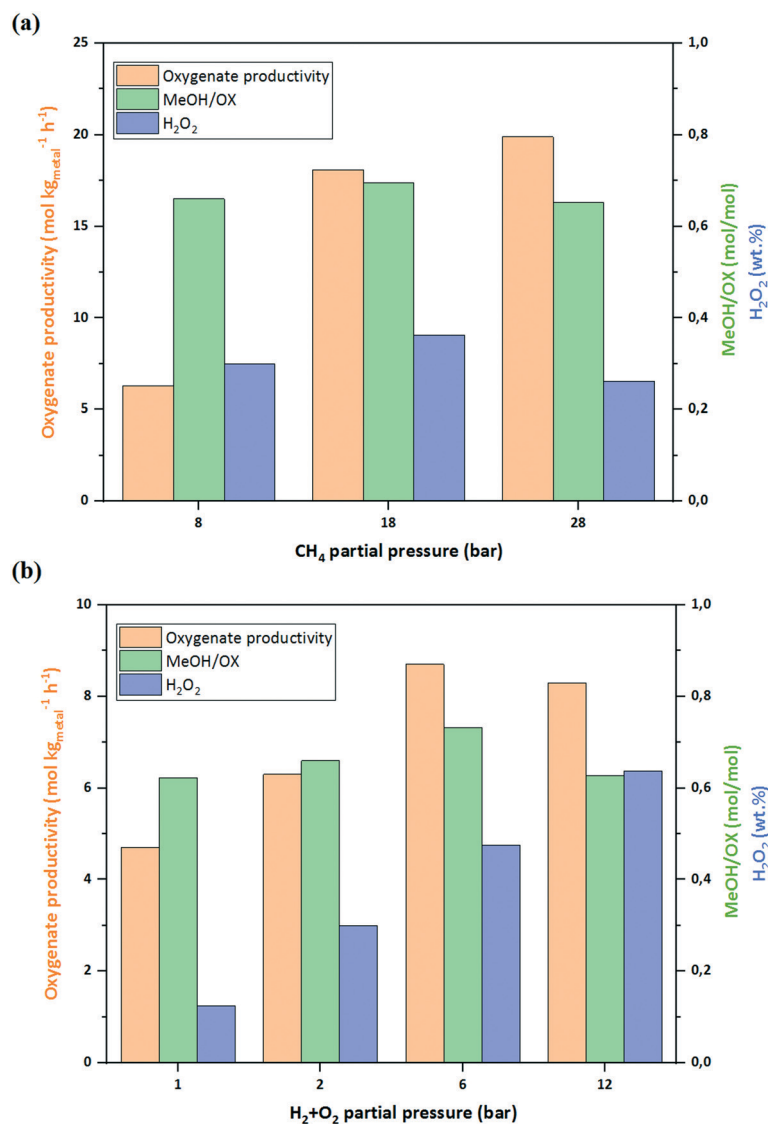


Fig. 5 (a) Effect of CH₄ partial pressure at $P_{O_2}(=P_{H_2})$ of 1 bar, G/L of 2.5 and WHSV of 4200 kg_{liq.} kg_{cat.}⁻¹ h⁻¹. (b) Effect of H₂ + O₂ partial pressure at P_{CH_4} of 8 bar, G/L of 2.5 and WHSV of 4200 kg_{liq.} kg_{cat.}⁻¹ h⁻¹. See Table 1, entries 1–6.

partial pressure from 8 to 18 bar resulted in a significant improvement in oxygenate productivity as it was raised from 6.3 to 18.1 mol kg_{metal}⁻¹ h⁻¹. Further CH₄ pressure increase did not have such a pronounced effect on the productivity (Fig. 5a), as the catalyst active sites seemed to be saturated at pressures above 18 bar. This behavior is in agreement with past studies where H₂O₂ was used as the oxidant.⁸

To study the effect of H₂ + O₂ pressure (H₂/O₂ = 1), CH₄ pressure was kept at 8 bar and H₂ + O₂ was raised from 1 bar to 12 bar (Fig. 5b). By raising H₂ + O₂ pressure, the concentration of accumulated H₂O₂ in the reactor outlet was elevated up to 0.36% wt%. Higher pressures of H₂ + O₂, and therefore higher H₂O₂ formation rates, had a positive effect on oxygenate productivity, although to a lesser extent than the CH₄ partial pressure. This suggests that H₂ and O₂ are also involved in the rate-determining step. As it

can be seen in Fig. 5b, a H₂ + O₂ pressure of 12 bar slightly reduces the oxygenate productivity. At such a gas phase gas composition (H₂/O₂/CH₄ = 0.3/0.3/0.4) there is possibly a competition for the active sites on the catalyst surface making initiation of CH₄ activation controlled by the number of available sites. Hence an optimum is required between H₂O₂ formation rate and its role in subsequent methane activation. Based on the obtained results, it can be inferred that the most favorable gas phase composition to obtain high oxygenate productivity is a CH₄-rich medium with an optimal H₂ + O₂ pressure.

In order to investigate the influence of oxidative conditions, the experiments were conducted at different H₂/O₂ ratios of 0, 0.5 and 2, see Fig. 6. The highest oxygenate productivity was achieved at H₂/O₂ of 0.5, suggesting that a more oxidative condition is favorable for methane activation as the productivity dropped from 15.3 to 11.5 mol kg_{metal}⁻¹ h⁻¹



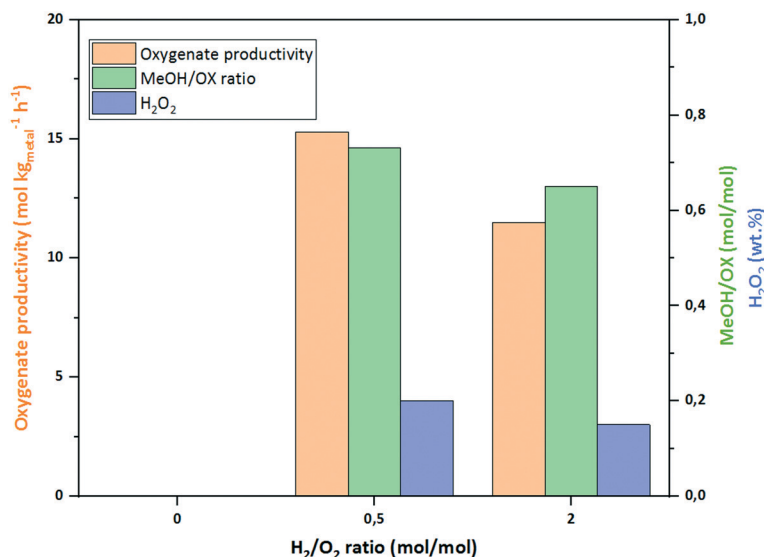


Fig. 6 Effect of H₂/O₂ ratio at P_{CH_4} of 28 bar, G/L of 2.5 and WHSV of 4200 kg_{liq.} kg_{cat.}⁻¹ h⁻¹. See Table 1, entries 7 and 8.

when H₂/O₂ ratio was raised to 2. Completely removing H₂ from the reaction medium (H₂/O₂ = 0) led to no methane activation. Remarkably, this was also the case when using pre-formed H₂O₂ (0.25 wt%) as the oxidant. This implies species generated during *in situ* H₂O₂ formation are essential and the intermediates for methane activation. It can be explained by the mechanism of methane activation (Fig. 7) over Au–Pd catalysts, which has been suggested to be a radical mechanism starting from formation of methyl radicals (·CH₃) through H abstraction from methane by hydroxyl radicals (·OH).¹⁹ The primary oxygenates are then generated by having ·CH₃ radicals going through a termination step which is either a reaction with an ·OOH radical or a molecular O₂.⁸ The ·OOH and ·OH radicals have been reported to be formed during *in situ* generation H₂O₂,^{19,26} and it can be the reason why in absence of H₂ (H₂/O₂ = 0) no methane activation was evident. However, the observation that in the simultaneous presence of the H₂ and O₂, an O₂-rich gas phase was more beneficial can be explained by considering that O₂ plays a dual role in the reaction, being involved

both in generation of ·OH, needed for ·CH₃ formation, and also in ·CH₃ termination step. This finding is in line with Agarwal *et al.*,¹⁹ who demonstrated O₂ significant incorporation in the methanol product using an isotopic labeling technique. Another source of O₂ and, also reactive intermediates including ·OH and ·OOH, can be the H₂O₂ decomposition.^{8,19} However, decomposition was observed to be well-suppressed (<5% decomposition) under the employed reaction conditions with the liquid phase containing 0.05 M sulfuric acid and 10 ppm NaBr, explaining why methane was not activated by using pre-formed H₂O₂ as the oxidant in these experiments.

Keeping G/L constant (= 5), the WHSV of the liquid phase was reduced from 4200 to 2100 kg_{liq.} kg_{cat.}⁻¹ h⁻¹, see Fig. 8a. The lower WHSV increased the concentration of H₂O₂ in the aqueous phase from 0.28% to 0.34% wt%, while the oxygenate productivity was unaffected, as expected from the near-differential operation conditions of the reactor. The proportional increase of oxygenates concentration with residence time also shows that the over-oxidation of oxygenates was not significant, since otherwise a drop in the productivity towards methanol and methylhydroperoxide would have been observed with decreasing WHSV. On the other hand, reducing WHSV resulted in an increase of MeOH/OX ratio from 0.65 to 0.84, suggesting a series reaction and confirming the reaction mechanism with methane first being converted to methylhydroperoxide that is further converted to methanol (Fig. 7).

The effect of G/L ratio on the performance was studied by changing gas flow rate at a constant liquid phase WHSV of 4200 kg_{liq.} kg_{cat.}⁻¹ h⁻¹. By increasing G/L from 2.5 to 5, peroxide concentration in the outlet slightly increased from 0.21 to 0.28 wt%, which is in agreement to our previous study on H₂O₂ synthesis.²⁷ However, neither the oxygenate productivity nor the MeOH/OX ratio (Fig. 8b) were affected by G/L ratio. Varying WHSV and G/L can alter the size of gas bubbles and liquid slugs, and consequently gas–liquid–

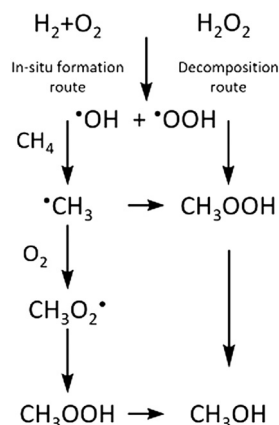


Fig. 7 Proposed reaction mechanism adapted from ref. 6, 16 and 22.

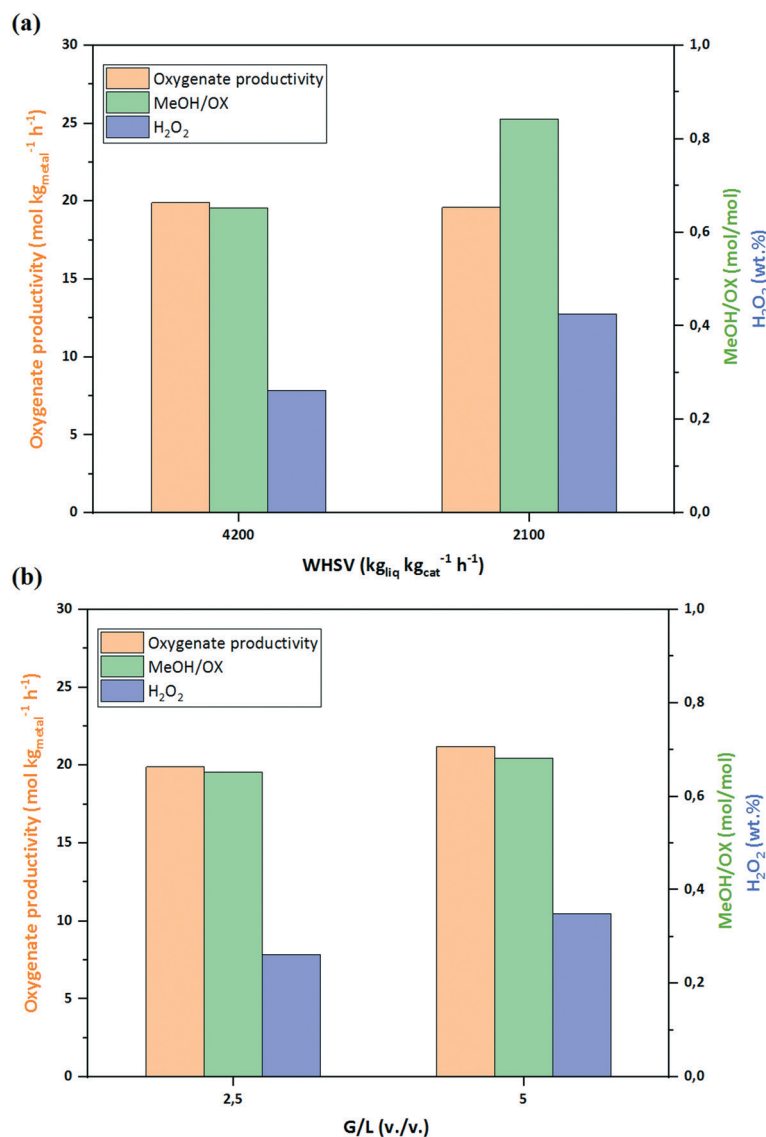


Fig. 8 (a) Effect of WHSV at G/L of 5 and (b) effect of G/L at WHSV of 4200 kg_{liq} kg_{cat}⁻¹ h⁻¹. P_{O_2} ($= P_{H_2}$) = 1 bar and P_{CH_4} = 28 bar. See Table 1, entries 2, 9 and 10.

solid mass transfer rates.²⁷ The unaffected productivities in both cases confirms that with the very slow kinetic of methane activation, mass transfer is not the limiting factor in the process.

4. Conclusions

Single-step selective methane oxidation was successfully coupled with *in situ* formation of H₂O₂ in a wall-coated microcapillary reactor, achieving an enhanced oxygenate productivity compared to what has been reported in the literature for supported Au-Pd nanoparticles. This improvement was mainly attributed to a significantly increased H₂O₂ formation rate in the microcapillary. The Au-Pd/SiO₂ catalyst also showed a good stability in terms of productivity and product distribution. In order to have a better understanding of the process, the operational parameters that

could affect the performance were identified and evaluated. CH₄ partial pressure turned out to have a more significant effect compared to that of H₂ and O₂ partial pressures, suggesting that a CH₄-rich medium and an optimal H₂ + O₂ partial pressures were favorable. Oxygenate productivity improved under a more oxidative medium (lower H₂/O₂), while in the presence of only O₂, no activity was observed. Using pre-formed H₂O₂ also did not result in methane activation as it was highly stabilized. As a result, 'OOH and 'OH radicals which are either formed during H₂O₂ synthesis or during H₂O₂ decomposition were found to be essential for methane activation. A decrease in WHSV favored methanol formation over methylhydroperoxide formation, indicating that methanol is formed out of methylhydroperoxide. Over-oxidation towards formic acid and CO₂ was not observed. The G/L ratio changed neither product distribution nor productivity of oxygenates.



Conflicts of interest

There are no conflicts to declare.

Acknowledgements

This work was supported by The Netherlands Organization for Scientific Research (NWO), Project (10017587). We acknowledge the support of Carlo Buijs for SEM and TEM measurement.

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