Supported noble metal catalysts are widely used in industrial processes on account of their high activity and/or selectivity for many key chemical reactions. Usually, the noble metals are finely dispersed on a support to give a high specific surface area to effectively use the catalytically active component and increase the amount of active sites. Atomically dispersed metal/metal oxide catalysts have attracted widespread interest in diverse research areas, such as chemistry, material science and environmental science. Due to their low-coordination, unsaturated atoms often function as active sites in catalytic processes, suggesting that downsizing the particles or clusters to single atoms is ideal for catalytic reactions. Single atoms tend to aggregate and grow into clusters or nanoparticles during the catalytic reaction processes due to the significant surface free energy increases with decreases in particle size. Although several methods have been explored for the preparation of atomically dispersed noble-metal catalysts in the past decade, the fabrication of stable atomically dispersed noble metal catalysts is still a great challenge. It is well known that the interaction between single atoms and supported substrate is essential for stabilizing active single atoms. Many previous reports on oxide supported metal clusters show that surface defects of the carriers can be used as anchor points for metal clusters or even single atoms. Besides noble metal atoms as the active sites, metal oxide carriers can also play an important role in the catalytic process. The interaction between oxide carrier and metal atoms can change the electronic properties of metal atoms, so it is of great significance to the activity and selectivity of the catalysts, especially in the catalytic oxidation of CO.

The different properties of the catalyst may be caused by different coordination environments around the single atom metal center, which is similar to the so-called “support effect” in traditional heterogeneous catalysis.

Herein, we report the synthesis of atomically dispersed Pt catalysts on TiO2 supports during a topotactic transformation process of NH4TiOF3 mesocrystals. Topotactic transformation is a useful method for preparing crystals with a required morphology through conversion from a precursor or mother crystal, in which the crystal orientations of the precursors and the target crystals have a certain topotactic correspondence. NH4TiOF3 is a typical mesocrystal, which exists in similar structures to anatase TiO2 with an average lattice mismatch of only 0.02%. The NH4TiOF3 mesocrystals can be topotactically transformed into TiO2 mesocrystals by either washing with aqueous H3BO3 or calcination at high temperature. The topotactic transformation can be applied to anchor the single atom via atom trapping by the rough surface, crystalline defects and active vacancies.

As illustrated in Fig. 1, NH4TiOF3 mesocrystals were firstly impregnated with H2PtCl6 solution for a period of time, resulting in adsorption of [PtCl6]2− ions on the surface and an internal pore of NH4TiOF3 mesocrystals. Then, NH4TiOF3 began to form hollow anatase TiO2 with ordered arranged nanothorns by topotactic transformation under an aqueous H3BO3 environment, in which the rough surface of TiO2 can prevent the aggregation of Pt atoms and result in the formation of highly dispersed Pt single atoms on the TiO2 substrate (Fig. S1†). We compared the effects of topotactic transformation, noble metal loading content and calcination. Pt/TiO2-T catalysts were prepared with various Pt loading contents of 0.1%, 0.5%, 1% and 3%. The above samples were calcined in N2 at 450 °C for 4 h and the final products were labeled as Pt/TiO2-TC (experimental details are given in the ESI†).

The dispersion and configuration of atomically dispersed Pt catalysts were characterized by atomic-resolution high-angle annular dark-field scanning transmission electron microscopy.
HAADF-STEM, which can identify the heavy atoms in the actual catalyst. A panoramic SEM image of the NH₄TiOF₃ precursors clearly showed the well-defined uniform NH₄TiOF₃ nanobricks with an average length of 400 nm and a thickness of 70 nm (Fig. 2A). After topotactic transformation and calcination, the resulting Pt/TiO₂ turned rough on the surface and became a mesoporous hollow structure, as shown in Fig. 2B. From common TEM images, shown in Fig. 2C (also see Fig. S2†), we clearly see that the sample is a hierarchical structure composed of regularly arranged nanocrystals. The inset of Fig. 2C shows a lattice spacing of 0.35 nm, which can be assigned to the (101) plane of TiO₂ nanocrystals. No Pt cluster or particle can be observed on the surface in the normal TEM observation, suggesting that the resulting Pt is highly dispersed and has a sub-nanometer size. In order to verify that Pt atoms have been successfully deposited on TiO₂, we performed atomic-resolution HAADF-STEM observations of the 1% Pt/TiO₂-TC. Large amounts of marked bright points show that individual Pt atoms (marked by the red circles) uniformly dispersed on the surfaces of the TiO₂ nanocrystals (Fig. 2D). Examination of different areas showed that only Pt single atoms existed in the sample 1% Pt/TiO₂-TC (Fig. S3†). Fig. 2D clearly shows that each Pt atom (red circles) occupies the lattice position of a Ti atom. The statistical size distributions of Pt in 1% Pt/TiO₂-TC and 3% Pt/TiO₂-TC are 0.9 nm and 1.09 nm (Fig. S4†), respectively, indicating that only subnanometer clusters and single atoms of Pt are formed on the TiO₂ substrate after the topotactic transformation and calcination. Energy dispersive spectroscopy (EDS) shows that Pt is uniformly dispersed on the surface of TiO₂ (Fig. 2E).

The structures of Pt/TiO₂-TC catalysts with certain Pt contents were analyzed by using powder X-ray diffraction (XRD) in order to assess the impact of Pt addition upon the nanoparticles. XRD analysis shows the structure transformation process from the NH₄TiOF₃ (Fig. S5†) to TiO₂ (Fig. 3A). All the diffraction peaks are attributed to the anatase TiO₂. No Pt diffraction peaks were detected in these samples, indicating the presence of highly dispersed clusters or single atoms on TiO₂. Even after 450 °C of calcination in N₂ for 4 h, the catalysts exhibited no Pt diffractions, suggesting that the calcination did not cause Pt atom aggregation. The N₂ adsorption/desorption isotherms display that the BET specific areas of the 1% Pt/TiO₂-TC and 3% Pt/TiO₂-TC were 130.06 m² g⁻¹ and 132.14 m² g⁻¹, respectively (Fig. 3B).

Fig. 1 Schematic diagram of the synthesis of Pt/TiO₂-TC.

Fig. 2 SEM images of (A) NH₄TiOF₃ mesocrystals and (B) 1% Pt/TiO₂-TC catalysts. (C) A TEM image of 1% Pt/TiO₂-TC; the inset shows the crystal lattice of anatase TiO₂. (D) High-resolution HAADF-STEM images of 1% Pt/TiO₂-TC. (E) EDS elemental mapping of a single 1% Pt/TiO₂-TC crystal.

Fig. 3 (A) XRD patterns of Pt/TiO₂-TC catalysts with different Pt loading content. (B) N₂ adsorption–desorption isotherms and pore size distributions (inset) of Pt/TiO₂-TC catalysts. (C) O 1s XPS spectra and (D) Pt 4f XPS spectra for Pt/TiO₂ catalysts.
X-ray photoelectron spectroscopy (XPS) analysis was carried out to evaluate the surface composition and valence states of the Pt/TiO₂ catalyst. The representative XPS survey scan spectrum indicates the existence of Ti, O, and Pt elements (Fig. S6†). Ti 2p spectra at 458.6 and 464.3 eV belong to the Ti 2p3/2 and Ti 2p1/2 peaks of Ti⁴⁺ (Fig. S7†). The binding energy of Ti 2p did not change after calcination. Fig. 3c shows O 1s core-level XPS spectra of Pt/TiO₂–T and Pt/TiO₂–TC; the catalysts contained two kinds of O species. The main peak centered at 530 eV is considered to be the oxygen band of Ti–O–Ti that can be assigned to the lattice oxygen of bulk TiO₂ and the shoulder peak at 531.35 eV can be ascribed to the surface OH species (Ti–OH) which could be correlated with an oxygen vacancy. It is obvious that the Pt/TiO₂–TC catalyst has more surface OH groups than the Pt/TiO₂–T catalyst. It is reported that surface OH groups are formed through water dissociation on oxygen vacancies or on metal surfaces by water–oxygen interaction. After calcination at 450 °C, peak shifts occurred and the two peaks corresponding to O 1s core-level XPS spectra were 529 and 531.6 eV, respectively, indicating that electron transfer occurred. The oxidation state of Pt in the catalyst is shown in Fig. 3d. The spectra collected for the 1% Pt/TiO₂–TC and 3% Pt/TiO₂–TC catalysts show two peaks at the Pt 4f edge with binding energies of 70.2 and 73.7 eV, which are assigned to the 4f7/2 and 4f5/2 states of Pt⁰, respectively. For 3% Pt/TiO₂–TC, the Pt 4f bimodal peak shows a downshift by 0.2 eV in binding energy. Deconvolution analysis reveals that there are two additional peaks at 71.4 and 75.8 eV, respectively, for 3% Pt/TiO₂–TC, which can be attributed to the same spin-orbital split of Pt⁰. The spectra collected for the 1% Pt/TiO₂–T and 3% Pt/TiO₂–T samples also show four peaks at the Pt 4f edge, in which the binding energies of 70.6 and 73.8 eV are assigned to the 4f7/2 and 4f5/2 states of Pt⁰, and the binding energies of 72.5 and 76 eV are assigned to the 4f7/2 and 4f5/2 states of Pt²⁺. For Pt/TiO₂–T and Pt/TiO₂–TC catalysts, the binding energies of Pt²⁺, Pt⁰, and Pt⁰ are decreased by 0.3 eV and 0.8 eV, respectively, which indicates that the surface reconstruction occurred during the calcination pre-treatment and enhanced the interaction between the metal and the support. The peak area of Pt⁰ increased obviously after calcination, which may be the reason for the decomposition of the oxidation state Pt at a high temperature. The existence of Pt²⁺ suggests a strong interaction between Pt and O, which is of benefit for the thermal stability of a Pt single atom, and also propitious for the charge transfer during CO oxidation. According to the XPS spectra, it is inferred that the actual content of Pt in the catalyst is very low (Table S1†) and is favorable for atom-level dispersion.

CO oxidation was chosen as a probe reaction to study the catalytic performance of single Pt atom supported on TiO₂ because such a reaction is highly sensitive to the chemical environment of the metal centers. Fig. 4 shows the catalytic performance of catalysts with different Pt loading contents. The data show that a CO oxidation reaction onset at near 50 °C and a total conversion at near 130 °C, indicating an excellent catalytic performance for low temperature CO oxidation. Controlled experiments were carried out with catalysts prepared by non-topotactic transformation and non-calcedined methods. Using a high-performance commercial TiO₂ photocatalyst, P25, as the supporting substrate, the resulting Pt/TiO₂–P25 catalyst also shows a much lower activity on CO oxidation in comparison with Pt/TiO₂–TC (Fig. S9†). All of the samples of Pt/TiO₂–T (non-calcined) and Pt/TiO₂–NC (non-topotactic transformed) did not show good catalytic activity for CO oxidation. We summarize the CO oxidation reaction temperature in Table S2, in which T100 denotes the temperature at which 100% of CO was converted into CO₂ and T50 is the temperature required for a 50% CO conversion. The T50 and T100 of 1% Pt/TiO₂–TC were 108 °C and 130 °C, respectively, which are lower than those of all other catalysts. The atomically dispersed Pt/TiO₂ catalysts show a higher catalytic performance in the CO oxidation reaction in comparison with previously reported single atom catalysts, such as Pt/La–Al₂O₃, Pt/0–Al₂O₃ (ref. 10a) and Pd/La–γ–Al₂O₃ (ref. 10b) (Table S3†). To illustrate the high activity of Pt/TiO₂–TC, Arrhenius plots are depicted in Fig. 4b. The corresponding Arrhenius plots of the CO reaction rate ln(TOF) show an approximate linear relation versus 1/T for the CO oxidation reaction. The apparent activation energy (Eₐ) is ~10 kJ mol⁻¹, much lower than for Pt/Al₂O₃ or Pt/CoO₂ (Eₐ = 90–100 kJ mol⁻¹).²² 1% Pt/TiO₂–TC has the smallest apparent activation energy, which is one of the main reasons that it shows the highest catalytic activity. The TOFs with different Pt SACs are summarized in Table 1. Among the four Pt/TiO₂–TC catalysts prepared in this work, the 0.5% Pt/TiO₂–TC catalyst shows the highest TOF of 0.36 s⁻¹. However, the 1% Pt/TiO₂–TC catalyst also shows a high TOF value of 0.262 s⁻¹. The TOF with 3% Pt/TiO₂–TC dramatically reduced to 0.048 s⁻¹, indicating that the Pt atoms begin to aggregate and the active sites of the catalyst are no longer increased to enhance the catalytic activity. The single atom Pt/TiO₂ catalysts in our work show a superior catalytic performance in both the low reaction temperature and the high reaction activity in comparison with other reported Pt SACs on different substrates. It is inferred that the catalyst prepared by the topotactic conversion method can anchor the Pt atoms on the surface of the porous TiO₂ carrier, and calcination can enhance the interaction between the Pt atoms on the surface and the carrier, which is attributed to a synergetic effect for low temperature CO oxidation.
with a 1% Pt loading content displayed the highest catalytic activity resulting in CO total conversion at 130 °C. Based on this method, we ultimately achieved an atomically dispersed Pt catalyst supported on TiO₂ with high activity and strong high temperature resistance. Further studies show that the high stability of the catalyst can be ascribed to sufficient interaction between the Pt and TiO₂ support.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

This work was supported by the National Natural Science Foundation of China (No. 21571028, No. 21601027), and the Fundamental Research Funds for the Central Universities (No. DUT16TD19, No. DUT17LK33, and No. DUT18LK28).

Notes and references


Table 1 Specific rates and TOFs of Pt/TiO₂ catalysts compared with reported Pt SACs catalysts

<table>
<thead>
<tr>
<th>Catalyst</th>
<th>Pt loading (wt%)</th>
<th>Temperature (°C)</th>
<th>Specific rate (mol h⁻¹ g⁻¹)</th>
<th>TOF (s⁻¹)</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.1% Pt/TiO₂-TC</td>
<td>0.1</td>
<td>100</td>
<td>3.91</td>
<td>0.212</td>
</tr>
<tr>
<td>0.5% Pt/TiO₂-TC</td>
<td>0.5</td>
<td>100</td>
<td>6.65</td>
<td>0.360</td>
</tr>
<tr>
<td>1% Pt/TiO₂-TC</td>
<td>1</td>
<td>100</td>
<td>4.60</td>
<td>0.262</td>
</tr>
<tr>
<td>3% Pt/TiO₂-TC</td>
<td>3</td>
<td>100</td>
<td>6.65</td>
<td>0.360</td>
</tr>
<tr>
<td>0.18% Pt/Al₂O₃</td>
<td>0.18</td>
<td>200</td>
<td>—</td>
<td>0.12³</td>
</tr>
<tr>
<td>1.0% Pt/Al₂O₃</td>
<td>1</td>
<td>200</td>
<td>—</td>
<td>0.013³</td>
</tr>
<tr>
<td>2.0% Pt/Al₂O₃</td>
<td>2</td>
<td>200</td>
<td>—</td>
<td>0.051³</td>
</tr>
<tr>
<td>Pt₁/FeO</td>
<td>0.01</td>
<td>300</td>
<td>41.6</td>
<td>2.25⁵</td>
</tr>
</tbody>
</table>

TOFs of this work were calculated based on the metal dispersion. For the 0.1% and 0.5% Pt loading samples, TOF was calculated with 100% dispersion. For the 1% and 3% Pt loading samples, dispersion was estimated by the Pt particle size according to D = 1/dₚ. ³From ref. 16; ⁵from ref. 10a, ⁶from ref. 6b.


