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Synergistic and simultaneous biosorption of phenanthrene and iodine from aqueous solutions by soil indigenous bacterial biomass as a low-cost biosorbent

D. Zhang,^{ID} *^{abc} S. G. Lu,^{*a} X. Q. Song,^b J. F. Zhang,^b Z. M. Huo^b and H. T. Zhao^{ID} ^c

The removal of phenanthrene and iodine from aqueous solutions in single and binary systems by inactivated soil indigenous bacterial biomass (SIBB), as well as affecting factors, were evaluated. Sorption kinetic and isotherm studies were carried out to investigate the synergistic effects of phenanthrene and iodine. Optimal parameters for the biosorption process included a solution pH of 6.0 and biosorbent dosage of 0.75 g L⁻¹. The ionic strength significantly decreased the biosorption of both phenanthrene and iodine in single conditions, while no obvious influences were found in the binary conditions. A pseudo-second-order model was well fitted to the kinetic biosorption data for both phenanthrene and iodine. The results showed that the presence of co-solute accelerated the biosorption processes and the pseudo-second-order biosorption rates (k_2) for phenanthrene and iodine increased from 0.005441 to 0.009825 g mg⁻¹ min⁻¹ and from 0.000114 to 0.000223 g mg⁻¹ min⁻¹, respectively. The SIBB showed strong affinity with both phenanthrene and iodine, with a partition coefficient K_d (Linear model) of 6892.4 L kg⁻¹ for phenanthrene and affinity parameter K_L (Langmuir model) of 232 500 L kg⁻¹ for iodine. The presence of co-solute illustrated a synergistic effect on the biosorption of phenanthrene and iodine due to intermolecular forces between phenanthrene and iodine, enhancing the K_d of 34.7% for phenanthrene and K_L of 107.0% for iodine, respectively. The results suggested that SIBB was an effective material for the simultaneous biosorption of phenanthrene and iodine from aqueous solutions.

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1. Introduction

Contaminants harmful to the health of present and future generations involve nuclear fission products such as iodine radioisotopes. Iodine radioisotopes have been released into our environment due to anthropogenic activities such as the nuclear energy industry, nuclear accidents and wastewater discharge containing radioactive iodine.^{1,2} Iodine is potentially one of the most mobile radioisotopes^{3,4} and easily reaches the biosphere⁵ because of its weak affinity with many geological materials, low-organic-content soils and sediments. Therefore, iodine is potentially acutely and chronically toxic due to bioaccumulation through the food chain and may subsequently affect human health adversely.^{6,7} It is useful to understand the interactions between iodine and natural or artificial materials of the environment in contact with surface waters and groundwater, as well as co-existing pollutants.

Several recent studies reported that aromatic structures in natural organic matter (NOM) played an important role in the sorption of iodine to soil and/or sediment.^{4,8,9} Aromatic carbon in NOM participated in the oxidation of iodine to some form of intermediates, facilitating the formation of aromatic carbon-iodine bonds rather than aliphatic carbon-iodine bonds.^{8,10}

In addition, hydrophobic organic compounds (HOCs) are ubiquitous toxic contaminants,^{11,12} which can be highly likely to co-exist with iodine in soil and aquifer environments near nuclear power plants. These contaminants are highly transferable and easily to interact with soil particles, biota and microorganisms.^{4,5} Many HOCs, such as polycyclic aromatic hydrocarbons (PAHs) and polychlorinated biphenyls (PCBs), contain two or more aromatic structures. These co-existing pollutants may exhibit the same, or at least similar, interactions with iodine as NOM do. The formation of aromatic carbon-iodine bonds could affect the transport, fate, and removal of iodine and co-existing HOC pollutants, making it much more complex to evaluate their environmental behaviours and ecological risks. However, little information is available about the interactions of iodine and aromatic containing contaminants, as well as the influence on subsequent sorption and removal of the co-existing pollutants.

^aCollege of Environmental & Resource Sciences, Zhejiang University, Hangzhou, Zhejiang 310058, China. E-mail: zhangdong@hdu.edu.cn; lusg@zju.edu.cn; Tel: +86-571-86919158

^bZhejiang Wulong Chemical Industrial Stock Co. Ltd, Deqing, Zhejiang 313201, China

^cCollege of Materials and Environmental Engineering, Hangzhou Dianzi University, Hangzhou, Zhejiang 310018, China



To overcome (or at least limit the contribution of) this risk, it would be useful to find efficient scavengers for iodine, as well as HOCs. The use of natural biomaterials (served as adsorbents) is considered promising and the most attractive alternative due to their easy handling, versatility, cost-effectiveness, efficiency, low-selectivity and relative abundance compared with conventional techniques.^{13–15} Studies have reported that dead or metabolically inactive biomass materials were used as successful biosorbents for the treating or removal of dyes,^{16–19} heavy metals,^{20–23} HOCs^{24–26} and radioactive elements such as uranium^{27,28} from aqueous solutions. Several mechanisms were also proposed and summarized as follows:²⁹ (1) electrostatic binding for some cationic metals, dyes and radioactive elements due to negative groups in biosorbents;^{16,27,30} (2) hydrophobic interactions and partitioning for hydrophobic organic compounds;^{26,31} (3) specific molecular-level interactions such as cation- π interactions;³² and (4) deposition on the cell surface or within the cell wall structures.¹⁵ Simultaneous removal of metal-metal²⁰ and metal-organic compounds³³ were also reported. However, to our knowledge, limited information is available for the biosorption of iodine, as well as the synergistic influence of aromatic compounds.

Therefore, the main objectives of this study were to evaluate the biosorption capability of a low-cost soil indigenous bacterial biomass (SIBB) for the simultaneous removal of phenanthrene (typical PAHs) and iodine as a model of combined pollutants by (1) examining the biosorption potential of phenanthrene and iodine onto SIBB in single and binary systems, and (2) optimizing the parameters affecting the biosorption process.

2. Materials and methods

2.1 Biosorbent and sorbate preparation

The biosorbent was obtained from physically and thermally inactivated soil indigenous bacterial biomass as described in previous works.^{31,34} The indigenous bacteria were isolated from soil in an agricultural field of Zhejiang, China, near the Qinshan Nuclear Power Plant and then cultured in Lysogeny Broth. After harvest, bacteria were washed three times with deionized water to remove any remaining culture media. To obtain inactive biomass, indigenous bacteria were dried for 24 h at a temperature of 70 °C following mechanical grinding. The surface properties of SIBB material were measured according to our previous work.³⁴ The specific surface of the biosorbent was determined by a gas sorption analyzer (NOVA-1200, Quantachrome Corp., USA). The biosorbent was further characterized using Fourier transform infrared spectroscopy (FTIR, Shimadzu 8400S, Kyoto, Japan).

Stable iodine and phenanthrene were selected as representative iodine species and HOCs and were purchased from Aladdin Reagent Co. (China) with purities > 99.0%. Stock solutions (1000 mg L⁻¹ for phenanthrene in methanol and 200 mg L⁻¹ for iodine in deionized water) were prepared and stored in amber glass bottles at 4 °C. Working solutions in the range of 0–1.0 mg L⁻¹ for phenanthrene and 0–200 mg L⁻¹ for

iodine in single and binary systems were prepared by serial dilution. NaOH (0.1 mol L⁻¹) and/or HCl (0.1 mol L⁻¹) were used to adjust the pH of solutions. The inorganic reagents used for the growth of the microorganisms such as tryptone, yeast extract, and sodium chloride, were of analytical grade (Aladdin Reagent Co., China).

2.2 Sorption tests and analytical methods

Batch sorption experiments were carried out in a temperature-controlled shaker at 150 rpm at 25 °C, and tubes were prepared in duplicate, as described in our previous work.³¹ In the kinetic and isotherm sorption experiments, a certain amount of sorbents, 15 mg for SIBB, were weighted into 22 mL centrifuge tubes with 20 mL single iodine, single phenanthrene and their binary solutions. The concentrations of iodine and phenanthrene covered the range of 0–200 mg L⁻¹ and 0–1.0 mg L⁻¹, respectively. Control treatments without biosorbents were prepared to account for the possible solute loss by handling and other possible ways. Single-factor biosorption experiments were also conducted, and other factors were adjusted to suitable conditions: biosorbent dosage at 0.25, 0.5, 0.75, 1.0, and 1.25 g L⁻¹; ionic strength (CaCl₂) at 0, 0.1, 0.2, 0.3, 0.4, and 0.5 mol L⁻¹, pH at 3, 4, 5, 6, 7, 8, 9, and 10; and biosorption time of 60, 90, 120, 180, 240, 480, 720, 960, 1200, and 1440 min in single and binary conditions. The sorption equilibrium time was set up according to the biosorption kinetics experiments. At the equilibrium time, after being centrifuged for 20 min at 4000g, the supernatants were filtrated by 0.22 μ m filter membranes (ANPEL Co., Ltd., China).

The concentration of phenanthrene in the aqueous phase was determined using HPLC (Agilent 1260) equipped with a 4.6 \times 250 mm Eclipse PAH column and a fluorescence detector using a methanol and water mixture (v/v, 95 : 5) as mobile phase at a flow rate of 1.0 mL min⁻¹. The excitation and emission wavelengths of phenanthrene were 244 and 360 nm, respectively. The method quantification limit value for phenanthrene was 3.39 μ g L⁻¹, and the relative standard deviation for phenanthrene determination was 0.23%. The determination of iodine followed the method described by Madrakian *et al.*³⁵ and the concentration was measured using a spectrophotometer (Shimadzu UV-2600) at a wavelength of 460 nm.

The removal efficiency of phenanthrene and iodine by SIBB was determined using the following equation:

$$\text{Removal efficiency (\%)} = \left(1 - \frac{C_i}{C_t}\right) \times 100\% \quad (1)$$

where C_i and C_t (mg L⁻¹) represent the initial and final (at any time t) concentration of phenanthrene or iodine, respectively. The sorption capacity of bacterial biomass for phenanthrene or iodine at time t , Q_t (mg kg⁻¹), is obtained as follows:

$$Q_t = \frac{(C_i - C_t) \times V}{m} \quad (2)$$

where V (mL) is the volume of the solution and is equal to 20 mL in the present study; and m (mg) represents the mass of biosorbent, 15 mg for SIBB is used in the present study.



2.3 Kinetic sorption models

To determine the biosorption kinetics, the obtained dynamic experimental data was fitted with several kinetic models, such as the Morris–Weber model, Lagergren model and pseudo-second-order model. The Morris–Weber model³⁶ can be expressed as follows:

$$Q_t = K_{id}\sqrt{t} + C \quad (3)$$

where Q_t (mg g⁻¹) is the sorbed phenanthrene or iodine at time t . The values of the rate constant of Morris–Weber (K_{id}) are calculated using the slope of the linear plot.

The Lagergren pseudo-first-order model, which was the earliest known equation to explain the adsorption rate based on the adsorption capacity, was also used to stimulate the sorption kinetic data.³⁷ The equation is generally expressed as follows:

$$\lg(Q_e - Q_t) = \lg Q_e - k_1 t \quad (4)$$

where Q_e is the biosorbed amounts of phenanthrene or iodine at equilibrium time (mg g⁻¹), and k_1 is the rate constant (min⁻¹). The plot of $\lg(Q_e - Q_t)$ versus t gives a straight line for the pseudo-first-order sorption kinetics. The values of the pseudo-first-order rate constant k_1 are obtained from the slopes of the straight lines.

The non-linear form of the pseudo-second-order model can be written as follows according to Ho:^{38,39}

$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{1}{Q_e} t \quad (5)$$

where k_2 is the pseudo-second-order rate constant (g mg⁻¹ min⁻¹).

2.4 Isothermal sorption models

The Langmuir, Freundlich, linear, D–R and Temkin models were used to describe the isothermal sorption of phenanthrene and iodine in single and binary systems by the bacterial biomass. The Langmuir isotherm is represented as:

$$\frac{C_e}{Q_e} = \frac{1}{Q_m K_L} + \frac{C_e}{Q_m} \quad (6)$$

where C_e and Q_e are the equilibrium concentration (mg L⁻¹) and adsorption capacity (mg g⁻¹) of phenanthrene or iodine on the bacterial biomass, respectively, at equilibrium conditions. The isotherm constants Q_m and K_L are the maximum adsorption capacity for monolayer coverage (mg g⁻¹) and the coefficient related to the affinity between the sorbent and the sorbate (L mg⁻¹), respectively.

The logarithmic form of the Freundlich model (original form: $Q_e = K_F C_e^{1/n}$) is used to calculate the Freundlich parameters and is expressed as shown in the following equation:

$$\log Q_e = \log K_F + \frac{1}{n} \log C_e \quad (7)$$

where Q_e is the amount adsorbed per unit weight of sorbent (mg kg⁻¹); C_e is the equilibrium concentration (mg L⁻¹); K_F [(mg kg⁻¹) · (mg L⁻¹)⁻¹, equal to L kg⁻¹] and n (dimensionless) are the

Freundlich isotherm constants, describing the sorption capacity and the isotherm curvature, respectively.

The Linear isotherm model is also used to estimate the sorption of phenanthrene and iodine onto SIBB. The linear model is described as the form of the following equation:

$$Q_e = K_d C_e \quad (8)$$

where K_d is the distribution coefficient of sorbate (phenanthrene or iodine) between water and sorbent (L kg⁻¹).

The Dubinin–Radushkevich (D–R) isotherm model is applied to the data to deduce the heterogeneity of the surface energies of adsorption and the characteristic porosity of the biosorbent. The linear form of the D–R model is given as follows:

$$\ln Q_e = \ln X_m - \beta F^2 \quad (9)$$

where F can be calculated by

$$F = RT \ln \left(1 + \frac{1}{C_e} \right) \quad (10)$$

where Q_e is the experimental adsorption capacity (mol g⁻¹); F is the Polanyi sorption potential; R is the gas constant (8.314 J K⁻¹ mol⁻¹); C_e is the concentration of phenanthrene or iodine at equilibrium (mol L⁻¹); and T is the absolute temperature (298 K). The D–R isotherm constants X_m and β are the calculated maximum adsorption capacity (mol g⁻¹) and the activity coefficient (mol² J⁻²) related to adsorption mean free energy (kJ mol⁻¹), respectively. The mean sorption energy E , which is defined as the free energy transfer of 1 mol of the solute from infinity on the surface of the sorbent, can be calculated by:

$$E = \frac{1}{\sqrt{-2\beta}} \quad (11)$$

The Temkin isotherm model suggests an equal distribution of binding energies over a number of exchange sites on the surface. The linear form of the Temkin isotherm can be written as:

$$Q_e = B \ln K_T + B \ln C_e \quad (12)$$

where B is equal to RT/b and corresponds to the heat of sorption, with R being the universal gas constant (8.314 J mol⁻¹ K⁻¹) and T being the absolute temperature in Kelvin (298 K). b is the variation of the adsorption energy (J mol⁻¹); K_T is the equilibrium binding constant; and C_e and Q_e are the equilibrium concentration (mol L⁻¹) and sorption capacity (mol kg⁻¹), respectively.

3. Results and discussion

3.1 Biosorbent characterization

Fig. 1 showed the FTIR spectrum of the biosorbent used in the present study. The peak assignments of bacterial biomass were as follows. At 980 cm⁻¹, the =C–H stretching of unsaturated hydrocarbons was observed. Complementary information could



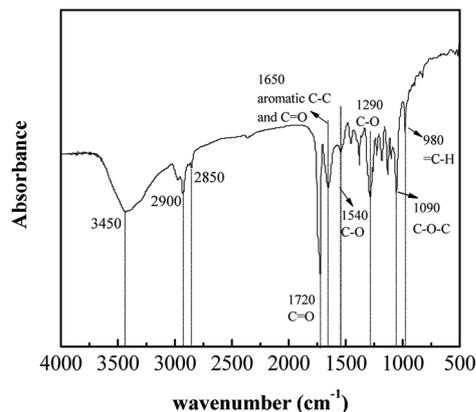


Fig. 1 The FTIR spectrum of bacterial biomass.

be deduced from the bands between 1200 and 900 cm^{-1} , where the C–O–C and C–O–P functional groups were observed. The region between 1250 and 1200 cm^{-1} exhibited the >P=O double-bond stretching vibrations.²⁶ The bands at 1290 cm^{-1} and 1540 cm^{-1} were dominated by C–O stretching of phenolic compounds and the amid II, respectively. The C–C and C=O of aromatic carbons asymmetric stretching frequency could be determined near 1650 cm^{-1} . A characteristic peak at 1720 cm^{-1} was formed due to the vibrational C=O of –COOH stretching frequency. A cluster of bands at the range of 3000–2850 cm^{-1} referred to saturated aliphatic groups (e.g., –CH₃, –CH₂–). A broad and strong band at approximately 3450 cm^{-1} represented the symmetric stretching vibration from water molecules.²⁶ The results confirmed that the bacterial surface was abundant with carboxyl, phosphate, amino groups, saturated and unsaturated aliphatic carbons and aromatic structures.

The specific surface area determined by the BET method was 1.43 $\text{m}^2 \text{g}^{-1}$, which was quite small but comparable with other research.¹⁷

3.2 Biosorption of phenanthrene and iodine by SIBB in single and binary systems

Effect of biosorbent dosage. Biosorbent dosage determines the number of active sites for pollutant binding, and it greatly affects the biosorption capacity and efficiency. In Fig. 2a, with the increasing dosage (0.25 to 1.25 g L^{-1}), the biosorption efficiency escalated from 60.65% to 78.78% for phenanthrene and from 34.49% to 86.06% for iodine, respectively. Additionally, the biosorption capacities of phenanthrene and iodine decreased from 2111.7 to 547.9 mg kg^{-1} and from 151 840 to 73 408 mg kg^{-1} , respectively (Fig. 2b). The decreasing capacity with increasing dosage could mainly be related to the number of available binding functional groups and sites on the biosorbent due to aggregation.²⁴ Similar trends had been observed for the biosorption of metals, dyes, uranium and organic compounds onto several biosorbents.^{17,21,38} In addition, the biosorption processes of phenanthrene and iodine were found to reach their optimum conditions at the dosage of 0.75 g L^{-1} (Fig. 2a), where the biosorption capacities caught 900 and 11 600 mg kg^{-1} , respectively.

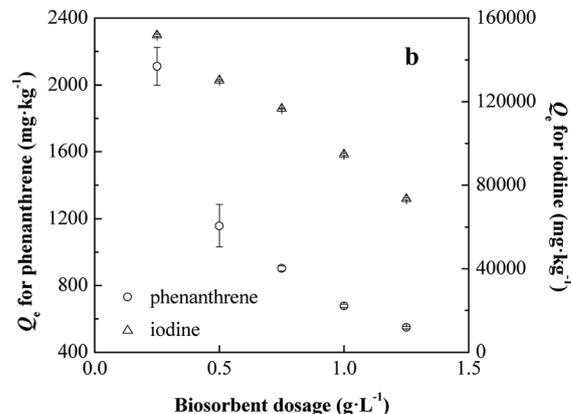
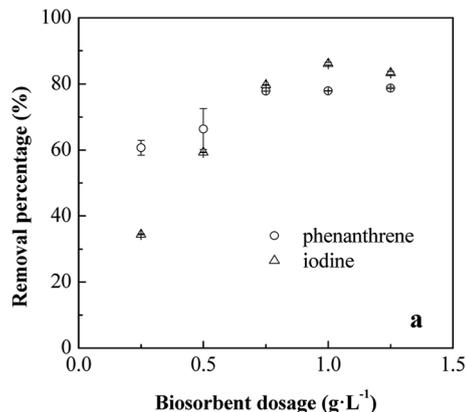


Fig. 2 Effect of biosorbent dose on the biosorption removal (a) and sorption capacity (b) of phenanthrene and iodine. Open circles represent the sorption of phenanthrene and open triangles represent the sorption of iodine.

Effects of contact time. The influence of contact time on the biosorption capacity of phenanthrene and iodine in single and binary systems were illustrated in Fig. 3. Results showed that the biosorbed phenanthrene and iodine increased with contact time up to proximately 480 minutes, after which maximal biosorption capacities or equilibrium biosorption were reached. The graduated slow-down of sorption, and finally equilibrium, were mainly due to the decrease of available sites for sorption or saturation of functional bonds.⁴⁰ Therefore, 480 minutes was selected as the optimum contact time for all further experiments.

According to Fig. 3, the maximum biosorption amounts of phenanthrene by SIBB were around 1363.8 mg kg^{-1} and 1494.0 mg kg^{-1} in single and binary systems and were 204 020 mg kg^{-1} and 212 320 mg kg^{-1} for iodine in single and binary systems, respectively. The biosorption of HOCs such as phenanthrene onto biomass mainly *via* hydrophobic interaction due to the presence of aliphatic carbons and aromatic structures, which have been extensively studied.^{34,41,42} Choung *et al.* proposed a possible mechanism for the sorption iodine species onto natural organic matters based on XANES spectra.⁸ The uptake of iodine associated with the formation of intermediate iodine species through oxidation by quinones and ketones of the black carbon. In the present study, as shown in the FTIR spectra (Fig. 1), there are quinones (C=O of aromatic



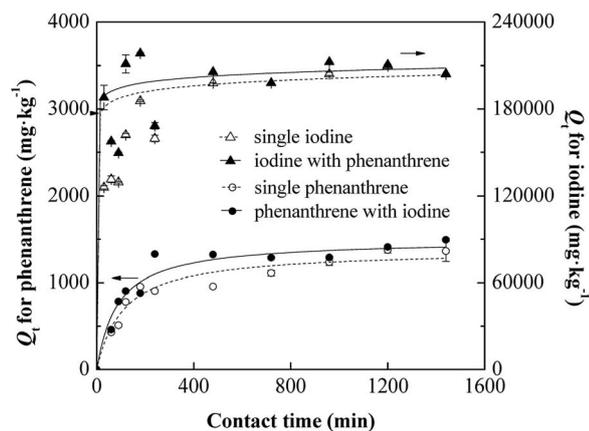


Fig. 3 Effect of contact time on the biosorption of phenanthrene and iodine in single and binary systems. Open circles with dashes represent the sorption of phenanthrene in single condition. Solid circles with a solid line represent the sorption of phenanthrene in binary condition. Open triangles with dashes represent the sorption of iodine in single condition. Solid triangles with a solid line represent the sorption of iodine in binary condition.

carbon, 1650 cm^{-1}) and ketones ($\text{C}=\text{O}$, 1720 cm^{-1}) groups present in the SIBB material, which mainly contribute to the sorption of iodine. Therefore, the SIBB material showed relatively large sorption capacities for both phenanthrene and iodine. Furthermore, the results indicated that the co-existence of iodine or phenanthrene enhanced the biosorption of phenanthrene and iodine in the binary conditions. The synergistic effect on phenanthrene and iodine biosorption could be attributed to the specific bonding between the iodine molecules and carbon atoms of polycyclic aromatic hydrocarbons.⁸

Phenanthrene and iodine biosorption in various pH solutions. The pH of a solution is one of the most important parameters affecting the biosorption process because pH primarily affects the surface properties of the biosorbent and the chemical property of pollutants.^{18,40} A wide range of pH (3–10) was used to examine the influence of pH on the biosorption capacity of phenanthrene and iodine in single and binary systems. As shown in Fig. 4, the biosorption capacity of phenanthrene was not obviously affected by pH, regardless of the presence or absence of iodine. The biosorption of hydrophobic organic compounds such as phenanthrene by inactivated bacterial biomass was considered to be a result of the partition mechanism to hydrophobic surfaces.³¹ The partition process was insensitive to the change of solution pH; therefore, the biosorption capacity kept a relative stable value ($1077\text{--}1321\text{ mg kg}^{-1}$) in various pH solutions. However, the biosorption capacity of iodine was strongly affected by pH especially higher pH, as shown in Fig. 4. The biosorption capacity of iodine increased with increasing pH and reached maximum at a pH of 6.0 in both single and binary conditions. In the single iodine condition, the biosorption capacity dramatically decreased when the pH was higher than 7.0. However, the presence of phenanthrene postponed the slump point of the biosorption efficiency, up to pH = 9.0, which may extend the practical application.

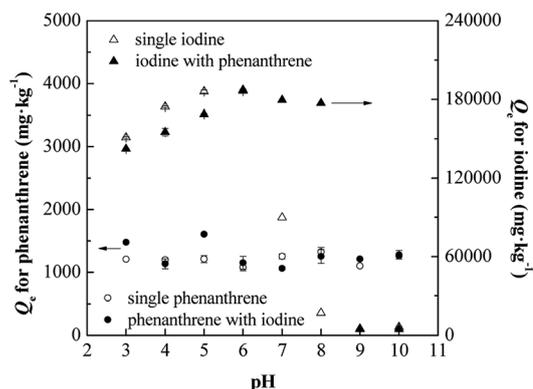


Fig. 4 Effect of solution pH on the biosorption of phenanthrene and iodine in single and binary systems. Open circles represent the sorption of phenanthrene in single condition. Solid circles represent the sorption of phenanthrene in binary condition. Open triangles represent the sorption of iodine in single condition. Solid triangles represent the sorption of iodine in binary condition.

Effect of ionic strength. Generally, solution chemical conditions such as ionic strength could affect the biosorption efficiency. Fig. 5 showed the effect of ionic strength at a range of $0\text{--}0.5\text{ mol L}^{-1}$ of CaCl_2 on the biosorption of phenanthrene and iodine by inactivated SIBB. It could be seen that the presence of CaCl_2 affected the biosorption of both contaminants in the single condition, in accord with results reported by Mahmoud *et al.*⁴³ However, there was no obvious difference at various ionic strength conditions for binary systems, as shown in Table 1. The coexisting iodine or phenanthrene may act as a “buffer” to reduce the influence on biosorption by ion strength under various environmental conditions.

3.3 Kinetics modelling

To evaluate the rate of phenanthrene and iodine biosorption in single or binary conditions and to examine the diffusion mechanism involved during the biosorption process, the

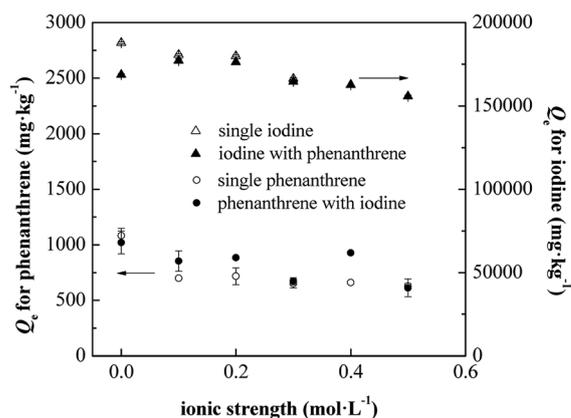


Fig. 5 Effect of ionic strength on the biosorption of phenanthrene and iodine in single and binary systems. Open circles represent the sorption of phenanthrene in single condition. Solid circles represent the sorption of phenanthrene in binary condition. Open triangles represent the sorption of iodine in single condition. Solid triangles represent the sorption of iodine in binary condition.



Table 1 Significant difference analysis (standard *t* test) for the biosorption capacity of phenanthrene and iodine for SIBB under different ionic strength

	Single phenanthrene	Phenanthrene with iodine	Single iodine	Iodine with phenanthrene
<i>t</i>	4.385 ^a	1.865	2.909 ^a	2.168
<i>n</i>	7	7	7	7
<i>P</i> _{0.05} ^b	2.365	2.365	2.365	2.365

^a Significant difference. ^b Both sides.

obtained dynamic experimental data was fitted with several kinetic models, such as the Morris-Weber model, Lagergren model and pseudo-second-order model. The applicability of these kinetic models was determined by the correlation coefficients (*R*²), as well as the biosorption capacity as suggested by Kausar *et al.*²⁸

The calculated values of *K*_{id}, *k*₁, *k*₂, *Q*_e and *h* are listed in Table 2. As exhibited in Fig. 6, the biosorption of phenanthrene and iodine in both single and binary conditions were superbly suitable for the pseudo-second-order kinetic model in contrast to the Morris-Weber model and pseudo-first-order model (shown in Table 2). The theoretical biosorption capacities calculated from the pseudo-second-order model (1.444 and 1.458 mg g⁻¹ for phenanthrene, and 212.3 and 212.8 mg g⁻¹ for iodine, respectively) were very close to the experimental biosorption capacities (1.364 and 1.490 mg g⁻¹ for phenanthrene, and 204.0 and 212.3 mg g⁻¹ for iodine, respectively). The applicability of pseudo-second-order model to the experimental data suggested that chemisorption was the dominant rate-limiting factor in controlling phenanthrene and iodine biosorption on SIBB.²⁸

The biosorption rates of phenanthrene and iodine in single and binary conditions were compared, and results showed that the presence of co-contaminants accelerated the biosorption process. In binary conditions, the pseudo-second-order biosorption rates for phenanthrene and iodine increased from 0.005441 to 0.009825 g mg⁻¹ min⁻¹ and from 0.000114 to 0.000223 g mg⁻¹ min⁻¹, respectively. The initial biosorption rate *h* (mg g⁻¹ min⁻¹) of the pseudo-second-order model was calculated as follows and listed in Table 2:

$$h = k_2 Q_e^2 \quad (13)$$

The initial rate might be a better parameter to evaluate the sorption rate considering the importance of an initial fast process in biosorption. Similar to the pseudo-second-order rate (*k*₂), we could find a much larger initial rate (*h*) for both phenanthrene and iodine in binary conditions. In the binary system, improvements of 88.3% and 97.1% for phenanthrene and iodine, respectively, were achieved compared to single biosorption.

3.4 Isothermal modelling

The applications of the linear, Langmuir, Freundlich, D-R and Temkin models for the biosorption of phenanthrene and iodine in single and binary conditions by inactivated SIBB were

explored, and the regression parameters are listed in Table 3. Comparing to Freundlich, D-R and Temkin models, biosorption of phenanthrene on SIBB fits well with the linear equation, while biosorption data of iodine fits well with the Langmuir model.

Table 2 Kinetic constants for phenanthrene and iodine in single or binary conditions by bacterial biomass

Morris-Weber model	<i>K</i> _{id} , mg kg ⁻¹ min ^{-1/2}	<i>R</i> ²
Phenanthrene (single)	32.46	0.8830
Phenanthrene (binary)	33.13	0.7681
Iodine (single)	2562	0.8011
Iodine (binary)	1267	0.3099

^a Single condition. ^b Binary condition.

Lagergren model	<i>k</i> ₁ , min ⁻¹	<i>R</i> ²
Phenanthrene (single)	0.0008186	0.7770
Phenanthrene (binary)	0.0003880	0.2608
Iodine (single)	0.001170	0.8084
Iodine (binary)	0.000418	0.1383

Pseudo-second-order model	<i>k</i> ₂ , g mg ⁻¹ min ⁻¹	<i>Q</i> _e , mg g ⁻¹	<i>h</i> , mg g ⁻¹ min ⁻¹	<i>R</i> ²
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Type 1 $t/Q_t = 1/(k_2 Q_e^2) + (1/Q_e)t$ $t/Q_t \sim t$

Phenanthrene (S) ^a	0.00544	1.444	0.0111	0.9920
Phenanthrene (B) ^b	0.00983	1.458	0.0209	0.9913
Iodine (S)	0.00011	212.3	5.1308	0.9986
Iodine (B)	0.00022	212.8	10.111	0.9978

Type 2 $1/Q_t = 1/Q_e + 1/k_2 Q_e^2 (1/t)$ $1/Q_t \sim 1/t$

Phenanthrene (S)	0.00641	1.424	0.013	0.9432
Phenanthrene (B)	0.00714	1.473	0.016	0.8967
Iodine (S)	0.00025	194.2	9.372	0.7234
Iodine (B)	0.00022	211.9	9.728	0.5128

Type 3 $Q_t = Q_e - 1/k_2 Q_e (Q_e/t)$ $Q_t \sim Q_e/t$

Phenanthrene (S)	0.00920	1.342	0.017	0.8025
Phenanthrene (B)	0.00890	1.449	0.019	0.6054
Iodine (S)	0.00023	198.1	8.846	0.6883
Iodine (B)	0.00029	208.9	12.58	0.3183

Type 4 $Q_e/t = k_2 Q_e^2 - k_2 Q_e Q_t$ $Q_e/t \sim Q_t$

Phenanthrene (S)	0.00696	1.422	0.014	0.8025
Phenanthrene (B)	0.00468	1.670	0.013	0.6054
Iodine (S)	0.00015	209.2	6.432	0.6883
Iodine (B)	0.00008	241.5	4.630	0.3183



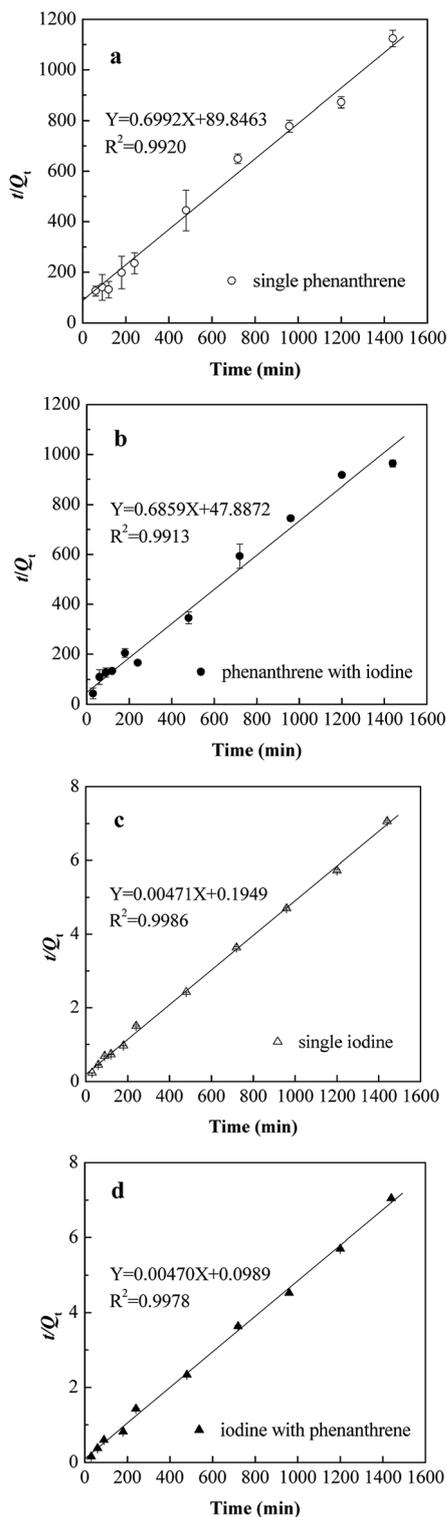


Fig. 6 Sorption kinetics for phenanthrene and iodine in single or binary conditions by bacterial biomass stimulated by the pseudo-second-order model. Open circles represent the sorption of phenanthrene in single condition (a). Solid circles represent the sorption of phenanthrene in binary condition (b). Open triangles represent the sorption of iodine in single condition (c). Solid triangles represent the sorption of iodine in binary condition (d).

Table 3 Isotherm sorption constants for phenanthrene and iodine in single or binary conditions by bacterial biomass

Linear model	K_d , L kg ⁻¹	R^2
Phenanthrene (S) ^a	6892.4 ± 10.95	0.9999
Phenanthrene (B) ^b	9283.7 ± 192.3	0.9962
Iodine (S)	1443.7 ± 702.4	0.3496
Iodine (B)	1359.7 ± 736.5	0.2864

^a Single condition. ^b Binary condition.

Langmuir model	K_L , L mg ⁻¹	Q_m , mg g ⁻¹	R_L	R^2
Phenanthrene (S)	—	—	—	0.2153
Phenanthrene (B)	—	—	—	0.0029
Iodine (S)	0.2325	216.9	0.044–0.387	0.9953
Iodine (B)	0.4813	199.6	0.023–0.234	0.9987

Freundlich model	K_F , L kg ⁻¹	n	R^2
Phenanthrene (S)	9034.4	0.8949	0.9854
Phenanthrene (B)	7856.0	1.0082	0.9394
Iodine (S)	146 892	13.550	0.8757
Iodine (B)	162 630	25.252	0.8530

D–R model	β , mol ² J ⁻²	Q_m , mol g ⁻¹	R^2	E , kJ mol ⁻¹
Phenanthrene (S)	1.19×10^{-8}	237.56	0.9918	6.482
Phenanthrene (B)	1.01×10^{-8}	143.87	0.9327	7.036
Iodine (S)	2.48×10^{-9}	814.77	0.7518	14.20
Iodine (B)	1.32×10^{-9}	769.40	0.7313	19.48

Temkin model	b , kJ mol ⁻¹	K_T , L kg ⁻¹	R^2
Phenanthrene (S)	0.6351	6297.4	0.9302
Phenanthrene (B)	0.7834	8525.4	0.8319
Iodine (S)	0.0448	5.93×10^6	0.8537
Iodine (B)	0.0851	7.38×10^{11}	0.8431

Biosorption of organic pollutants to biomass could involve surface sorption, chemical reactions and partitioning processes. The well-fit with linear model for phenanthrene (Fig. 7a and b) indicated that the primary mechanism of phenanthrene biosorption was partitioning. This was consistent with the previous studies about dead or inactivated bacterial and fungal biomass^{31,41} and the FTIR results. In the present study, the FTIR spectrum showed that the SIBB was abundant with saturated (3000–2850 cm⁻¹, -CH₃, -CH₂-) and unsaturated (near 980 cm⁻¹, C=C) aliphatic carbon and aromatic structure (1650 cm⁻¹), which provided effective binding sites for phenanthrene. Calculated partition coefficients (K_d) of phenanthrene in single and binary conditions were 6892.4 and 9283.7 L kg⁻¹, respectively. These results showed that SIBB had a high affinity for phenanthrene compared with reported data.^{31,41} In addition, the presence of iodine highly enhanced the partition coefficient of phenanthrene with an increase of 34.7%. A specific binding would occur between iodine and carbon atoms in aromatic hydrocarbons according to the mechanism illustrated by Choung *et al.*⁸ The interaction or binding of phenanthrene with iodine was theoretically possible. As partitioning was the dominant mechanism for biosorption of phenanthrene, the biosorption of iodine on SIBB should not occupy the partition



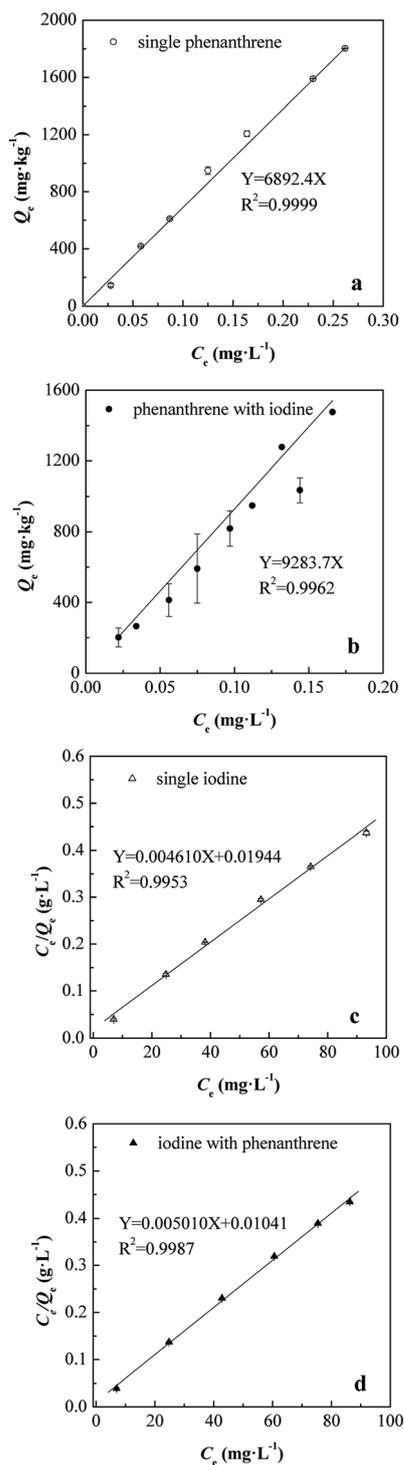


Fig. 7 Isothermal sorption for phenanthrene and iodine in single or binary conditions by bacterial biomass simulated by the Linear model (for phenanthrene, (a) and (b)) and by the Langmuir model (for iodine, (c) and (d)). Open circles represent the sorption of phenanthrene in single condition (a). Solid circles represent the sorption of phenanthrene in binary condition (b). Open triangles represent the sorption of iodine in single condition (c). Solid triangles represent the sorption of iodine in binary condition (d).

site for phenanthrene. Therefore, the sorbed iodine molecules might provide extra chemical bonding sites for the biosorption of phenanthrene, leading to a significant increase in sorption affinity for phenanthrene of SIBB.

The partition coefficient (K_d) is a useful parameter to evaluate the distribution of organic compounds between solid and solution phases, and hence, their fate and mobility in the environment. Based on K_d values, the affinity of organic pollutants to biosorbents or solid phases from the aqueous phase can be estimated. The determined $\log K_d$ values of phenanthrene by SIBB were 3.84 and 3.97 for single and bi-solute conditions, respectively. These values were much higher than those of soil–water systems (1.48–2.30), due to the higher carbon content of SIBB.^{44,45} The $\log K_d$ of phenanthrene valued within a wide range of 2.98 to 4.76 for natural organic matter, microbiological biomass and plant residues, as summarized by Chen *et al.*⁴⁶ The $\log K_d$ values obtained in this study were higher than live tissues such as wood chips (3.40), plant roots (3.32–3.70), tender tea leaves (3.52–3.54)⁴⁶ and algae and planktons (3.36–3.89).⁴² Additionally, these values were lower than the cuticle of plants (4.21–4.73) and humic acid (4.45). Therefore, bacterial biosorption may play an important role in the fate of phenanthrene in soils and surface water.⁴¹

The sorption mechanism of iodine onto biomass could be proposed to be specific bonding with carbon atoms according to the mechanisms illustrated by Choung *et al.*⁸ Accordingly, the aromatic carbon in organic matter participated in the oxidation of iodine to some form of intermediates, facilitating the formation of aromatic carbon–iodine bonds rather than aliphatic carbon–iodine bonds. According to the postulates of the Langmuir model, a good fit would indicate that the monolayer chemical biosorption occurred at a given number of specific homogenous sites due to intermolecular forces.²¹ Affinity parameter K_L values for iodine were 0.2325 and 0.4813 L mg^{-1} (232 500 and 481 300 L kg^{-1}), as illustrated in Fig. 7c and d. A significant increase of the K_L value of 107.0% in the presence of phenanthrene was found compared to the single iodine condition. As mentioned above, the biosorption of phenanthrene followed the partition mechanism and did not occupy the binding sites for iodine. Furthermore, the co-solute (phenanthrene) improved the sorption affinity of SIBB by introducing active binding sites and forming new functional groups that favoured iodine biosorption, which could be attributed to their interaction.⁸

The separation factor or equilibrium parameter constant (R_L) was an important characteristic of the Langmuir isotherm and was represented as follows:

$$R_L = \frac{1}{1 + K_L C_i} \quad (14)$$

The separation factors (R_L) were 0.044–0.387 and 0.023–0.234 following the range of 0–1.0, indicating a favourable biosorption of iodine, as listed in Table 3.²¹



4. Conclusions

The present work showed that soil indigenous bacterial biomass was successfully applied for the simultaneous biosorption of phenanthrene and iodine from aqueous solutions. Synergistic effects were also found in binary conditions. The pseudo-second-order dynamic model agreed very well for the biosorption of phenanthrene and iodine onto SIBB. Calculated pseudo-second-order rates (k_2) illustrated that the co-solute accelerated the biosorption process, with improvements of 80.6% and 95.6% for phenanthrene and iodine, respectively. The SIBB showed strong affinity with both phenanthrene and iodine, with a partition coefficient K_d (Linear model) of 6892.4 L kg⁻¹ for phenanthrene and affinity parameter K_L (Langmuir model) of 232 500 L kg⁻¹ for iodine. The presence of co-solute illustrated a synergistic effect on biosorption due to intermolecular forces between phenanthrene and iodine, enhancing the K_d by 34.7% for phenanthrene and K_L by 107.0% for iodine, respectively. Affecting factors were also tested to optimize biosorption parameters. Ideal conditions for the biosorption process included a pH of the solution of 6.0 and a 0.75 g L⁻¹ biosorbent dosage within a 480 minutes time contact between the biosorbent and sorbates. The ionic strength significantly affected the biosorption of both phenanthrene and iodine in single condition, while no obvious influences were found in the binary conditions.

Conflicts of interest

There are no conflicts to declare.

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