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Preparation and characterization of petroleum-based mesophase pitch by thermal condensation with in-process hydrogenation

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A petroleum aromatic-rich component was used to prepare mesophase pitch by thermal condensation. In-process hydrogenation method was employed to achieve the hydrogenation reaction of intermediates generated during the thermal reaction using tetrahydronaphthalene (THN) as a hydrogen donor. Impacts of in-process hydrogenation on the properties of intermediates and mesophase pitches were investigated. It was found that the in-process hydrogenation was conducive to the generation of hydrogenated intermediates with concentrated extracted component distribution, uniform molecular structure and abundant naphthenic structures. The characterizations of mesophase pitches showed that the in-process hydrogenation contributed to the preparation of mesophase pitch with concentrated extracted component distribution, low softening point, large domain structure and ordered crystal structure. This was due to the increasing contents of naphthenic structures in intermediates. Moreover, the increase of methylene bridges in the product was the critical reason for improving the product's properties.

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1. Introduction

The petroleum-based mesophase pitch has been widely used for preparing carbon materials due to its outstanding performance, good processability, high carbon yield, low price, *etc.*^{1–3} As the by-product of heavy oil refining, the FCC slurry oil is generally applied to preparing aromatic plasticizers, oil additives, heat transfer oils, rubber additives, *etc.*, which resulted in environmental problems and waste of resources.⁴ The polycyclic aromatic compound in FCC slurry oil with low H/C atomic ratio is theoretically the ideal material for the generation of mesophase pitch.^{5,6} As a result, the formation and reaction mechanism of the petroleum-based mesophase pitch are the research priorities for high-value utilization of heavy oil and production of carbon materials.^{7,8}

Numerous research studies have been performed to study the effects of molecular structure and composition of raw material on the rheological properties, polarized structure and liquid-crystal structure of the carbonized product.^{9–11} Menéndez *et al.*¹¹ have suggested that the molecular composition of feedstock had an important influence on the properties of mesophase product by investigating the structural relationship of

petroleum pitches and their condensation products. Korai *et al.*¹² have explored the role of alkyl groups played on the properties of carbonized products, and they found that the present of methyl and methylene structures in mesophase molecules is benefit for the stacking and arrangement of mesogenic molecules. Shin *et al.*¹³ also suggested that the optical textures and crystal structures of mesophase pitches varied with the contents of alky groups in feedstock. Hydrogenation of feedstock or mesophase precursor is one of the effective and widely used methods for regulating the properties of mesophase pitch.^{14,15} After studying the impacts of alkyl groups on mesophase development during the hydrogenation of mesophase precursor, Miyake *et al.*¹⁵ proposed that the optical texture, molecular and crystal structures of mesophase pitch became better with raising the degree of hydrogenation. Machnikowski *et al.*^{16–18} have also stressed the importance of hydrogenation of coal-tar pitch during the generation of mesophase product.

The mesophase pitch was traditionally prepared by direct thermal condensation method^{19–21} which had some advantages, such as simple process and operation. However, it had special requirement on feedstock's structure and equipment material.²² Therefore, many studies have focused on the modification of feedstock and process. It was proved that the hydrogenation was an effective method to improve the quality of mesophase pitch.²³ The in-process hydrogenation means that a hydrogen donor is used to react with condensation intermediates generated during the formation of mesophase product. This method was generally used in the hydrovisbreaking process of residual

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oil, aiming to lower the viscosity and improve the rheology of reaction system.^{24–26} Theoretically, the in-process hydrogenation is conductive to the generation of improved mesophase pitch. Guo *et al.*²⁶ have investigated the roles of in-process hydrogenation played on the properties of residue during the hydrovisbreaking process. They found that the present of hydrogen donor was able to slow down the reaction rate, reduce the viscosity of reaction system and prolong the coking-induction period. Dehkissia²⁷ and Hidalgo-Herrador *et al.*^{28,29} have also noted that the hydrogen donor used in the hydrovisbreaking process could inhibit the formation of coke and improve the systematic rheological property.

As reported in our previous work,³⁰ the in-process hydrogenation was first used in the preparation of mesophase pitch. Tetrahydronaphthalene was selected as hydrogen donor to treat the intermediates generated during the thermal reaction. The study proposed that the optical structure of mesophase became better after in-process hydrogenation. However, the impacts of in-process hydrogenation on molecular and crystal structures of product have not been explored in the above researches. This work focused on the preparation of mesophase pitch with low softening point and ordered crystal structure through the thermal condensation with one-stage and two-stage in-process hydrogenations. The effects of in-process hydrogenation on the structural composition of intermediates and the properties of mesophase pitches were investigated.

2. Material and method

2.1 Material

The feedstock petroleum aromatic-rich component provided by CNOOC Company was named F. The elemental distribution, average molecular weight (M), SARA (including four components: saturates, aromatics, resin and asphaltene) and carbon residue of F are summarized in Table 1. The F has abundant carbon and little nitrogen, sulphur and oxygen. Besides, the aromatics component was enriched in F, while the asphaltene component was not found.

Table 1 Physicochemical properties of F^a

Sample	F
Elemental composition/wt%	
C	89.05 ± 0.06
H	10.87 ± 0.05
N	0.02 ± 0.01
S	0.03 ± 0.01
O	0.03 ± 0.01
M	372.19 ± 0.07
SARA/wt%	
Saturates	14.47
Aromatics	56.40
Resin	30.15
Asphaltene	0
Carbon residue/wt%	9.61 ± 0.05

^a The margins of error were obtained by calculating the average values of three parallel determination results.

Chemical agents used in this work, such as tetrahydronaphthalene ($C_{10}H_{12}$, ≥ 97.0%), *n*-heptane (C_7H_{16} , ≥ 99.0%), toluene ($C_6H_5CH_3$, ≥ 99.5%), quinolone (C_9H_7N , ≥ 98.0%) and pyridine (C_5H_5N , ≥ 99.5%) were all purchased from Sinopharm Chemical Reagent Co., Ltd.

2.2 Thermal condensation and in-process hydrogenation

The preparation process of mesophase pitches through thermal condensation with in-process hydrogenation was presented in Fig. 1. The thermal reaction of F was run in a 100 ml autoclave at 430 °C under 2 MPa. The intermediate generated at 2.0 h was named I. Then I was treated by 6 wt% of tetrahydronaphthalene (THN) at 390 °C under 8 MPa for 45 min and the hydrogenated intermediate was labeled as I₂, while the intermediate without treatment using THN was hydrogen donor was named I₁. This was the one-stage in-process hydrogenation. Subsequently, the I₂ was treated at 430 °C under 2 MPa for 2.0 h, and the resultant intermediate was called N. Then the two-stage in-process hydrogenation process was conducted. The intermediate N was treated by 6 wt% of THN at 390 °C under 8 MPa for 45 min and the resultant hydrogenated intermediate was named N₃, while the intermediate without the second hydrogenation was named N₂. Meanwhile, I₁ was treated without hydrogen donor under the same reaction condition as that of I₂, and the resultant unhydrogenated intermediate was named N₁. After that, the thermal condensation of intermediates N₁, N₂ and N₃ were carried out at 430 °C under 2 MPa for 2 h. The final products were labeled as N₁-MP, N₂-MP and N₃-MP.

2.3 Characterization

A Carlo EL elemental analyzer (made by Elementar Company) was used to analyze the elemental composition of sample.

The average molecular weight of feedstock was characterized on a JJG 877-2011 vapor pressure osmometer using benzyl as standard substance and calculated according to VPO method.³¹

The volatiles of intermediates were tested according to the SH/T 0026-90 standard.

The carbon residues of feedstock and intermediates were analyzed in accordance with ASTM D4530 standard.

The SARA of feedstock was characterized according to the SH/T 0509-98 standard.

The solubility of sample was analyzed by the contents of sample's four solvent extracted components,³² including heptane-soluble component (HS), heptane-insoluble/toluene-soluble component (HI-TS), toluene-insoluble/quinoline-soluble component (TI-QS) and quinoline-insoluble component (QI).

The condensation intermediates and mesophase pitches' pyridine-soluble (PS) components were characterized by a Varian AS600 NMR spectrometer with tetramethylsilane as internal standard and deuterated pyridine as solvent.

The softening points (SP) of intermediate and mesophase pitch were measured by the ring-and-ball method (ASTM D3461 standard) and penetrometer method.³³

The polarized structures of products were obtained on a XP-1500 polarizing microscope made by the Milite Company.



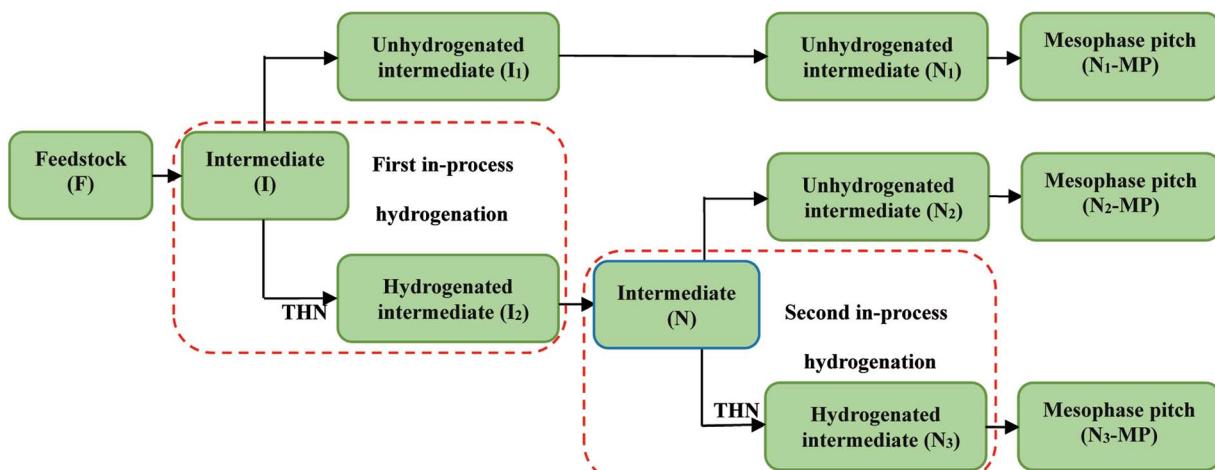


Fig. 1 Preparation scheme of mesophase pitches.

The products were characterized by an inVia Raman spectrometer (Renishaw Company) at 75 mW laser power with Ar monochromatic light source as excitation source ($\lambda = 633$ nm).

The crystal structures of products were determined by a D/MAX/2500PC X-ray diffractometer made by Rigaku Corporation.

3. Results and discussion

3.1 Characterization of intermediates

3.1.1 Elemental composition, softening point and solubility analyses. The elemental compositions, softening points (SP), extracted component distributions, volatiles and carbon residues of intermediates N_1 , N_2 and N_3 are listed in Table 2. The contents of nitrogen, sulphur and oxygen in the three intermediates were all below 0.5%. The H/C atomic ratios of the intermediates N_1 , N_2 and N_3 were 0.8157, 0.8913 and 0.9778, respectively. The higher H/C atomic ratios, lower softening points (SP), and less volatiles and carbon residues of N_2 and N_3 samples than those of N_1 were indicative of their lower

carbonization degree. This suggested that the in-process hydrogenation method was beneficial to the formation of intermediate with high H/C atomic ratio and low SP, volatile and carbon residue. In addition, the contents of HS and QI in the intermediates N_1 , N_2 and N_3 decreased gradually, while the contents of the two middle components (HI-TS and TI-QS) increased. It implied that the molecules of the intermediates were increasingly concentrated in the two middle components with rising degree of the in-process hydrogenation. Furthermore, according to similarity-intermiscibility theory,^{30,34} the molecules which were concentrated in components HI-TS or TI-QS possessed similar molecular structures. Therefore, the molecular structure of hydrogenated intermediate was more uniform, and the uniform degree of molecular structure increased with rising degree of the in-process hydrogenation. The above demonstrated that the in-process hydrogenation method contributed to the uniform of the molecular structures. To sum up, the extracted component distribution and molecular structure of the intermediate can be regulated by the in-process hydrogenation.

3.1.2 ^1H NMR analysis. Fig. 2 present the ^1H NMR spectra of N_1 , N_2 , and N_3 . The constituent hydrogen distributions of the intermediates are listed in Table 3.

The contents of H_{ar} hydrogens in the three intermediates N_1 , N_2 , and N_3 decreased gradually (shown in Table 3), implying the decreasing condensation degrees of the intermediates and the increasing alkyl structures in the intermediates.¹⁶ The contents of H_{α} , H_{β} , H_{γ} and H_{F} in the three intermediates varied little, while the contents of H_{N} increased significantly. This indicated that the contents of alkyl chains and methylene bridges in the three intermediates were similar, but the contents of naphthenic structures increased significantly with the rising degree of the in-process hydrogenation.^{30,35} To sum up, the in-process hydrogenation was conducive to the decrease of intermediates' condensation degrees and the increase of intermediates' naphthenic structures. Given the solubility and hydrogen distribution analyses of intermediates, the increase of the naphthenic structures in intermediate was the reason for the

Table 2 Elemental compositions, SP and extracted component distribution of intermediates^a

Sample	N_1	N_2	N_3
Elemental composition/wt%			
C	93.56 \pm 0.03	93.03 \pm 0.02	92.41 \pm 0.04
H	6.36 \pm 0.04	6.91 \pm 0.03	7.53 \pm 0.04
N	0.02 \pm 0.01	0.02 \pm 0.01	0.02 \pm 0.01
S	0.03 \pm 0.01	0.02 \pm 0.01	0.02 \pm 0.01
O	0.03 \pm 0.01	0.02 \pm 0.01	0.02 \pm 0.01
SP/%C	118 \pm 3	93 \pm 2	87 \pm 2
Extracted component/wt%			
HS	31.64 \pm 0.05	27.15 \pm 0.02	26.51 \pm 0.06
HI-TS	26.26 \pm 0.03	31.89 \pm 0.04	38.28 \pm 0.02
TI-QS	31.43 \pm 0.04	34.13 \pm 0.03	31.05 \pm 0.05
QI	10.67 \pm 0.06	6.83 \pm 0.03	4.16 \pm 0.03
Volatiles/wt%	20.57 \pm 0.08	22.46 \pm 0.05	23.84 \pm 0.07
Carbon residue/wt%	31.27 \pm 0.05	28.19 \pm 0.07	25.70 \pm 0.06

^a The margins of error were obtained by calculating the average values of three parallel determination results.



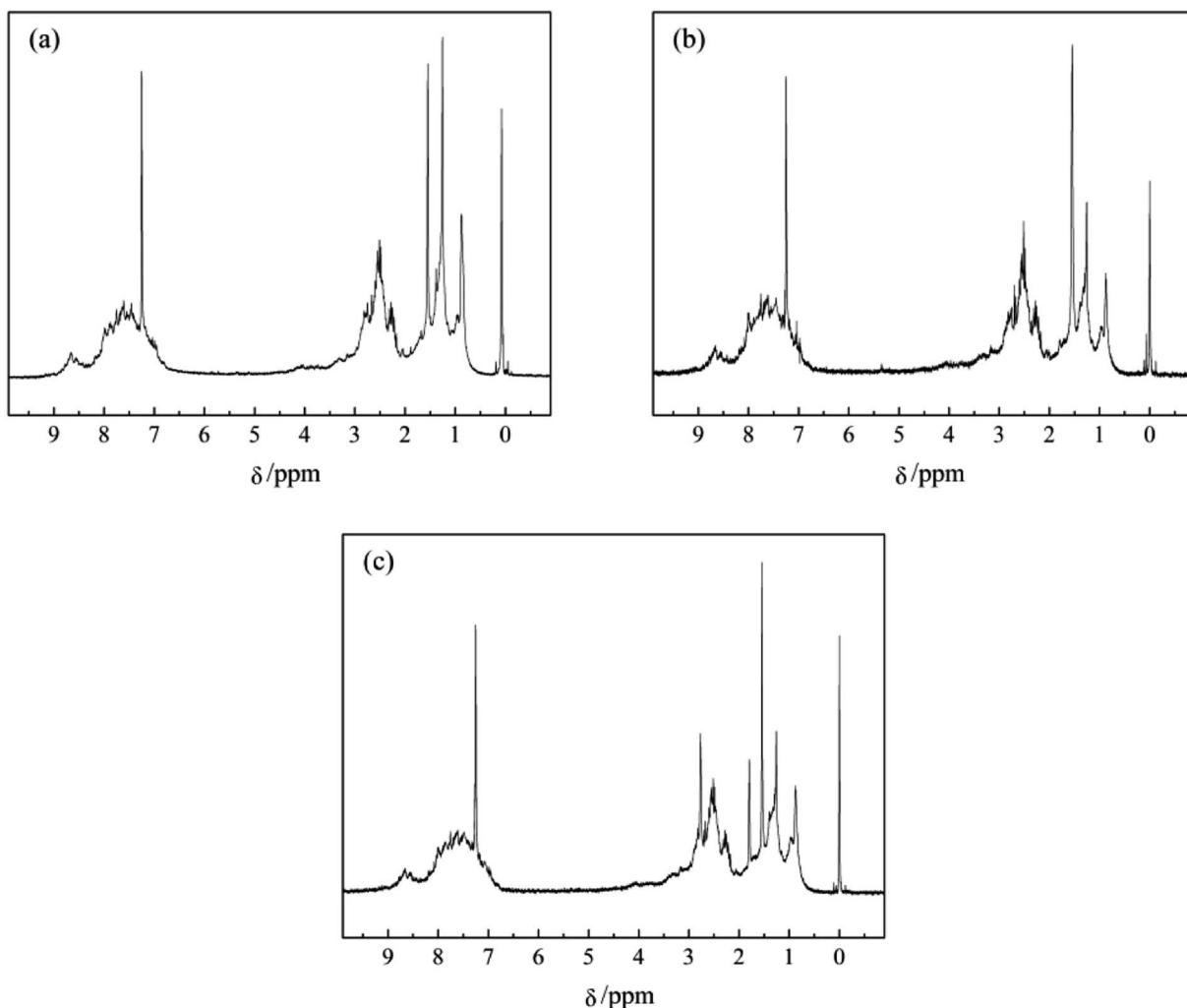


Fig. 2 ^1H NMR spectra of (a) N_1 , (b) N_2 and (c) N_3 .

Table 3 The constituent hydrogen contents of the intermediates: N_1 , N_2 and N_3^a

Sample	Hydrogen contents/%					
	H_{ar}	H_{F}	H_{α}	H_{β}	H_{γ}	H_{N}
N_1	59.97	0.91	21.52	11.06	4.47	2.07
N_2	55.03	0.93	22.57	10.39	4.84	6.24
N_3	52.46	0.98	22.33	10.18	5.08	8.97

^a H_{ar} , aromatic hydrogen (9.0–6.0 ppm); H_{F} , methylene bridge (4.5–3.3 ppm); H_{N} , naphthenic hydrogen (2.0–1.4 ppm); $\text{H}_{\alpha+\beta+\gamma}$, aliphatic hydrogen in α , β - and γ -position (3.3–2.0, 1.4–1.0 and 1.0–0.5 ppm).^{16,17}

change of the intermediates' molecular structures and extracted component distributions.

3.2 Solubility and SP analyses of products

The extracted component distributions and SP of mesophase pitches $\text{N}_1\text{-MP}$, $\text{N}_2\text{-MP}$ and $\text{N}_3\text{-MP}$ are summarized in Table 4. The contents of HS and QI components in $\text{N}_1\text{-MP}$, $\text{N}_2\text{-MP}$ and $\text{N}_3\text{-MP}$ decreased successively, while the contents of the two

middle components HI-TS and TI-QS increased obviously. This implied that the concentration degree of the extracted component distribution increased with the rising degree of the in-process hydrogenation. In addition, the SP of the three mesophase pitches decreased in sequence.

During the in-process hydrogenation, the hydrogen donor THN gave preference to provide hydrogen for the polycyclic aromatic compounds with high condensation degree,²⁶ which could reduce the condensation degree of aromatic compounds and restrain the formation of coke at some extent. So the content of QI component in mesophase pitch decreased with the rising degree of the in-process hydrogenation. Additionally, the decrease of aromatic compounds with high condensation degree was conducive to the maintenance of low systematic viscosity,³⁴ which could promote the conversion of HS component to HI component sufficiently. Therefore, the content of HS component in mesophase pitch also decreased with raising the degree of the in-process hydrogenation. Naturally, molecules in mesophase products were increasing concentrated in the middle extracted components. As mentioned above, the hydrogen-transfer reactions triggered by the abundant

Table 4 Extracted component distributions and SP of N₁-MP, N₂-MP and N₃-MP^a

Sample	Extracted component/wt%					SP/°C
	HS	HI-TS	TI-QS	QI		
N ₁ -MP	9.28 ± 0.04	13.77 ± 0.06	23.59 ± 0.07	53.36 ± 0.03	297 ± 3	
N ₂ -MP	6.10 ± 0.03	15.92 ± 0.06	30.12 ± 0.05	47.86 ± 0.04	253 ± 4	
N ₃ -MP	4.37 ± 0.07	16.76 ± 0.04	36.54 ± 0.06	42.33 ± 0.05	239 ± 2	

^a The margins of error were obtained by calculating the average values of three parallel determination results.

naphthenic groups in the intermediates (N₂ and N₃) were benefit for the improvement of the mesophase pitches' rheological property. This could prevent the excessive reaction and prolong the coking-induction period.^{26,30} So the softening points of N₂-MP and N₃-MP were lower than that of N₁-MP. The above demonstrated that in-process hydrogenation method contributed to the preparation of mesophase product with concentrated extracted component distribution and low softening point.

3.3 Optical structure analysis of products

The polarized micrographs of mesophase pitches N₁-MP, N₂-MP and N₃-MP are presented in Fig. 3. The mesophase pitch N₁-MP possessed medium domain structure, while N₂-MP and N₃-MP had large domain structure. Compared with N₂-MP, the size of the anisotropic structure of N₃-MP was larger. This was attributed to the differences of extracted component distributions and molecular structures among their intermediates N₁, N₂ and N₃. During the thermal treatments of intermediates, the present of QI component with polycyclic aromatic compounds was able to promote the formation of anisotropic phase as initial nucleus at the initial stage of thermal reaction.^{4,26} Then the system viscosity increased fast and the macromolecular layers were not able to move directionally and be orientated rearranged.³³ Hence, the high content of QI in intermediate N₁ resulted in a coarse mosaic structure formed in N₁-MP. In addition, the abundant naphthenic structures in intermediates N₂ and N₃ was the reason for the formation of large domain structure in N₂-MP and N₃-MP. During the preparation of N₂-MP and N₃-MP, the existence of naphthenic structures in N₂ and N₃ could effectively alleviate the carbonization, decrease the viscosity of reaction system and improve the systematic rheological property through hydrogen-transfer reactions.^{9,10} This contributed to the rearrangement of mesophase molecular layers. As a result,

the large domain structure was naturally formed in mesophase pitches N₂-MP and N₃-MP. Furthermore, compared with N₂-MP, N₃-MP possessed more ordered domain structure due to its higher content of naphthenic structures. The above indicated that the optical structure of mesophase product was improved by the in-process hydrogenation *via* decreasing the QI component content and increasing naphthenic structure content of intermediate.

3.4 ¹H NMR analysis of products

Fig. 4 illustrates the ¹H NMR spectra of PS component of N₁-MP, N₂-MP and N₃-MP (labeled as N₁-MP-PS, N₂-MP-PS and N₃-MP-PS, separately). Table 5 listed the corresponding hydrogen distributions.

The content of H_{ar} in N₁-MP-PS, N₂-MP-PS and N₃-MP-PS decreased respectively (shown in Table 5), indicating the increasing contents of alkyl structures in the three mesophase products. The contents of H_α, H_β, H_γ and H_N hydrogens in the three PS components changed little, while the content of H_F increased obviously. This implied that the proportions of alkyl chains and naphthenic structures in the three products were similar, but the contents of methylene bridges increased notably.³⁵ Given the optical structure and ¹H NMR spectra analyses of mesophase products, the increase of the methylene bridges in products was the critical reason for improving the product's properties.

3.5 Raman analysis of product

Fig. 5 presents the Raman spectra of products N₁-MP, N₂-MP and N₃-MP. The Raman parameters are shown in Table 6.

The D and G peaks (near 1350 and 1580 cm⁻¹ in Fig. 5), illustrated in the spectra of the three mesophase products, denoted the carbon with defective structure and the highly

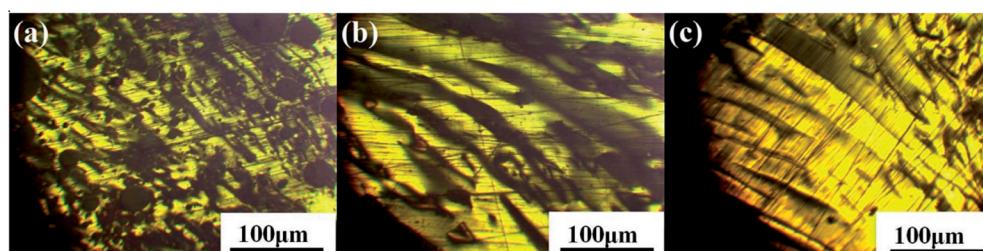


Fig. 3 Polarized micrographs of mesophase products: (a) N₁-MP, (b) N₂-MP and (c) N₃-MP.



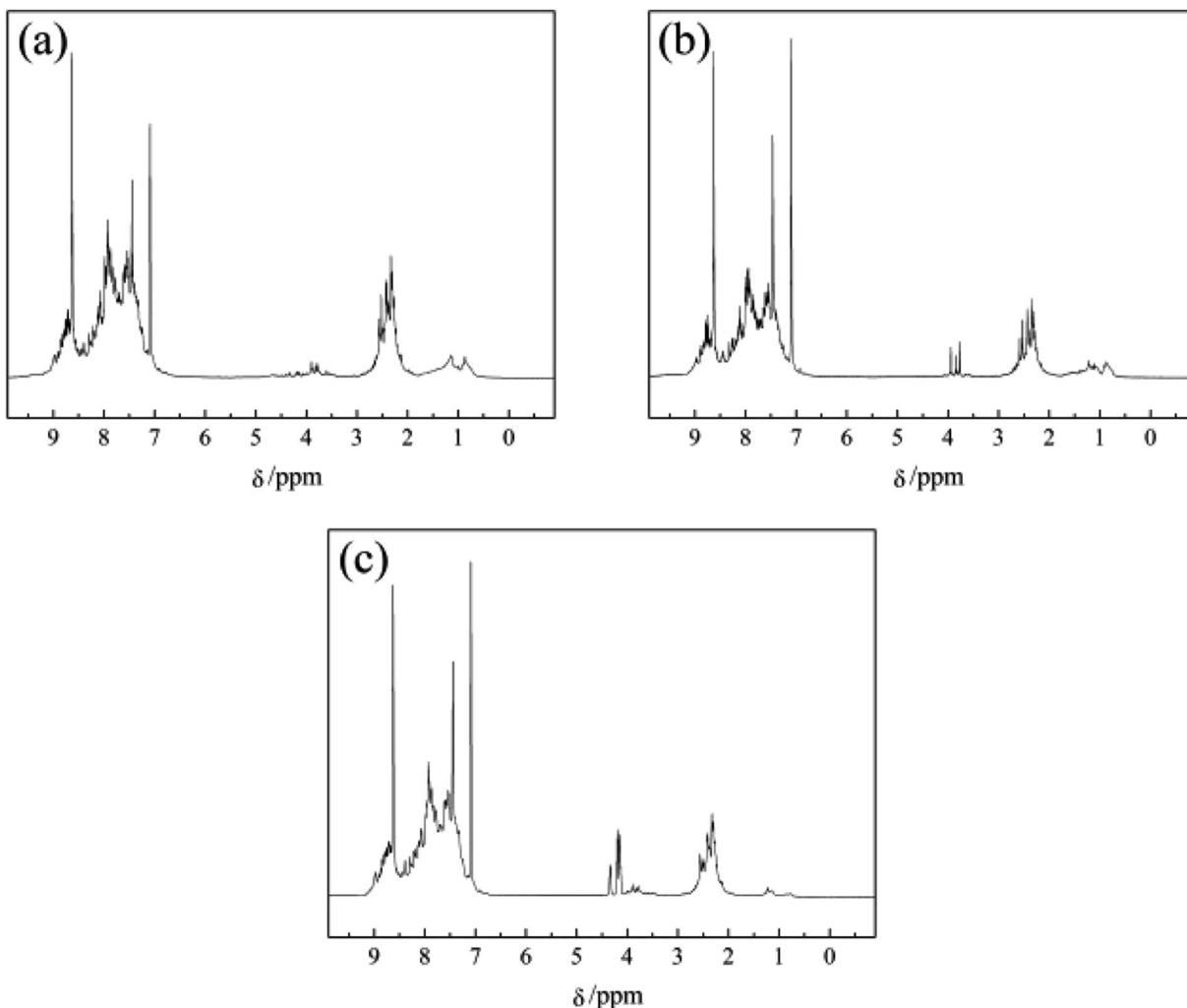


Fig. 4 ^1H NMR spectra of (a) $\text{N}_1\text{-MP-PS}$, (b) $\text{N}_2\text{-MP-PS}$ and (c) $\text{N}_3\text{-MP-PS}$.

oriented graphite crystalline.³³ The intensity ratio of D peak to G peak ($I_{\text{D}}/I_{\text{G}}$) was on behalf of the degree of crystal defect. The crystal sizes (L_{a}) which represented the incipient graphitization degrees of products were calculated according to the Shuker-Gammon equation. As shown in Table 6, the $I_{\text{D}}/I_{\text{G}}$ ratios and W_{D} of the three products increased as $\text{N}_3\text{-MP} < \text{N}_2\text{-MP} < \text{N}_1\text{-MP}$, while the L_{a} decreased in this order. This indicated that the incipient graphitization degrees of $\text{N}_2\text{-MP}$ and $\text{N}_3\text{-MP}$ were superior to those of $\text{N}_1\text{-MP}$. This was ascribed to the abundant naphthenic structures in the intermediates N_2 and N_3 . As previously explained, the increased naphthenic structures in hydrogenated intermediates could reduce the viscosity of

reaction system and improve the systematic rheological property. This was benefit for the movement and be rearrangement of mesophase molecular layers. So the mesophase products $\text{N}_2\text{-}$

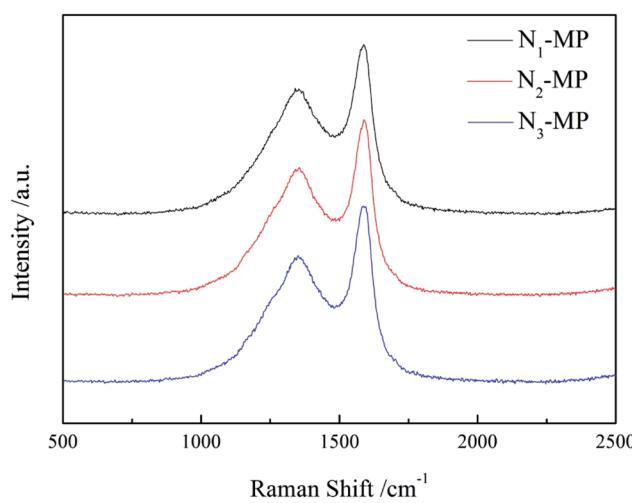


Table 5 Hydrogen distributions of $\text{N}_1\text{-MP-PS}$, $\text{N}_2\text{-MP-PS}$ and $\text{N}_3\text{-MP-PS}$

Sample	Hydrogen contents/%					
	H_{ar}	H_{F}	H_{α}	H_{β}	H_{γ}	H_{N}
$\text{N}_1\text{-MP-PS}$	78.97	1.12	14.26	2.29	3.21	0.15
$\text{N}_2\text{-MP-PS}$	74.98	5.86	13.95	2.15	2.89	0.17
$\text{N}_3\text{-MP-PS}$	72.06	9.97	13.71	1.86	2.24	0.16

Fig. 5 Raman spectra of $\text{N}_1\text{-MP}$, $\text{N}_2\text{-MP}$ and $\text{N}_3\text{-MP}$.

Table 6 Raman parameters of N₁-MP, N₂-MP and N₃-MP^a

Sample	I_D/I_G	W_D/cm	$L_a (\times 10^{-2})$
N ₁ -MP	0.437	57	1.259
N ₂ -MP	0.405	54	1.358
N ₃ -MP	0.384	49	1.432

^a I_D/I_G , the intensity ratio of D peak to G peak; W_D , the full width at half-maximum (FWHM) of D peak; L_a , the crystal size.

MP and N₃-MP possessed more oriented crystal structures than N₁-MP. In this sense, the crystal structure of product was able to be improved by in-process hydrogenation method *via* changing the naphthenic structure content in intermediate.

3.6 XRD analysis of products

Fig. 6 illustrates the XRD patterns of products N₁-MP, N₂-MP and N₃-MP, and Table 7 listed the corresponding crystalline parameters.

As illustrated in Fig. 6, the diffraction peaks (near 25.6 and 43.0), represented aromatic layer and crystal plane, were all displayed in spectra of N₁-MP, N₂-MP and N₃-MP. This demonstrated that the three products all possessed initial crystal forms.^{33,35} The parameters L_c , M_e and O_g of the three products increased in the order: N₁-MP < N₂-MP < N₃-MP, while the d_{002} increased in the reverse order (presented in Table 7). This suggested that crystal structures of the three products were increasingly improved. It meant that the present of naphthenic structures in intermediates was benefit for the generation of mesophase product with ordered crystal structure. This was accordant with the analysis results of mesophase pitches' polarized structures and Raman spectra.

To sum up, the in-process hydrogenation method contributed to the generation of mesophase product with concentrated extracted component distribution, low softening point, large domain structure and ordered crystal structure. Furthermore,

Table 7 Crystalline parameters of N₁-MP, N₂-MP and N₃-MP^a

Sample	$d_{002}/\text{\AA}$	L_c/nm	M_e	O_g
N ₁ -MP	3.75	2.36	7.29	0.895
N ₂ -MP	3.52	2.78	8.90	0.946
N ₃ -MP	3.46	3.09	9.93	0.972

^a d_{002} , interlayer spacing; L_c , stacking height; M_e , layer number; O_g , orientation degree.

the properties of mesophase product were improved by the in-process hydrogenation *via* increasing the naphthenic structure content in intermediate.

4. Conclusion

The in-process hydrogenation was a new method to prepare mesophase pitch, and proved to have obvious promoting effect on the formation and development of mesophase pitch with high quality. The molecular structures of feedstock have an important influence on the formation and development of mesophase pitch. The impacts of in-process hydrogenation method on the properties of intermediates and products were discussed. It was found that in-process hydrogenation contributed to the generation of intermediates with concentrated extracted component distribution and uniform molecular structure. This was ascribed to the increased naphthenic structures in hydrogenated intermediates. The characterizations of mesophase pitches showed that in-process hydrogenation method was benefit for the preparation of product with concentrated extracted component distribution, low softening point, large domain structure and ordered crystal structure. The properties of mesophase pitch were improved by the in-process hydrogenation *via* increasing the naphthenic structure content in intermediate. Moreover, the increase of methylene bridges in the product was the critical reason for improving the product's properties.

Conflicts of interest

There are no conflicts to declare.

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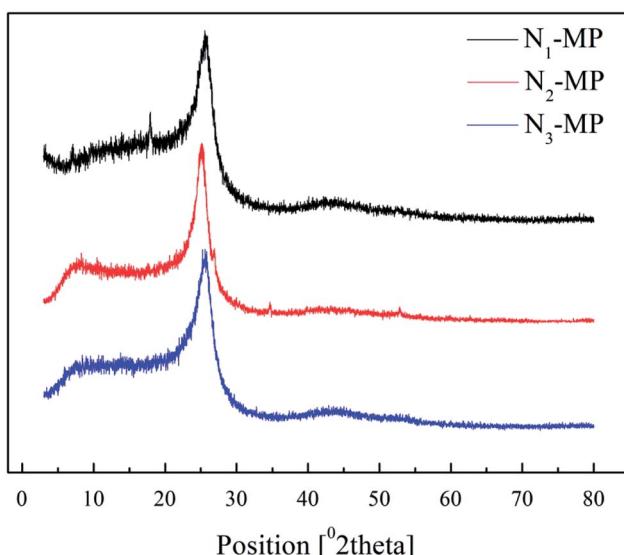


Fig. 6 XRD spectra of N₁-MP, N₂-MP and N₃-MP.



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