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# 1. Introduction

Corrosion is one of the significant sources of equipment failure and safety problems in offshore and marine operations.<sup>1,2</sup> Anticorrosive coatings are a useful approach for protecting steel structures/machinery against corrosion.<sup>2</sup> Pure zinc coatings have been widely used as sacrificial coatings to protect steel structures from corrosion. To improve the corrosion resistance properties of steel in a harsh environment, significant efforts have been made to strengthen their anti-corrosive properties.<sup>3,4</sup> One of the ways to improve the corrosion resistant properties of zinc coating is to make alloys with Fe, Cu and Ni. According to the literature,5,6 zinc alloy coatings such as Zn-Ni,79 Zn-Cu10 and Zn-Fe11 alloy films are often used to provide excellent corrosion resistance and maintain strong mechanical properties for steel equipment. They have better corrosion resistance compared to pure zinc coatings.5,6 Electrodeposition is one of the most economical and frequently used technologies for producing metallic coatings.12 The Zn alloy coatings deposited from citrate baths have been studied by Silva et al.; (2010) they deposited the Cu-Zn alloy coating on a mild steel substrate from a bath containing sodium citrate as the complexing agent, and benzotriazole and cysteine as additives. The results

# Electrochemical behaviour and analysis of Zn and Zn–Ni alloy anti-corrosive coatings deposited from citrate baths

Shams Anwar, Yahui Zhang and Faisal Khan 💷 \*

Anticorrosive coatings are a useful approach for protecting steel structures/machinery against corrosion. Electrodepositions of zinc and zinc-nickel alloy films on steel substrates under various conditions from baths containing potassium citrate were studied. The effects of electroplating variables such as bath composition and current density on the coating composition, morphology, corrosion and mechanical properties were systematically investigated. The electrochemical and mechanical behaviour of Zn-Ni deposits obtained at 60 mA cm<sup>-2</sup> from the citrate bath exhibited a lower corrosion current ( $l_{corr}$ ) and a less negative corrosion potential ( $E_{corr}$ ) compared to pure Zn and Zn-Ni alloy coatings from the non-citrate bath. The crystallite size of the Zn-Ni coating deposited from the citrate bath was 35.40 nm, and the Ni content of the coating was 8.3 wt%. The morphological properties and crystalline phase structure of the alloy coating were examined by scanning electron microscopy (SEM) and X-ray diffraction (XRD). The topographical structure of the coatings was analyzed by atomic force microscopy (AFM). The dominant  $\gamma$ -NiZn<sub>3</sub> (815) and  $\gamma$ -Ni<sub>2</sub>Zn<sub>11</sub> (330) (631) plane orientations in the zinc-nickel alloy films improved the corrosion resistance. Zn-Ni films with smaller grain size and uniform coating had an increased impedance modulus and improved corrosion resistance.

demonstrated that the coatings obtained with additives were brighter with small grain size. Cysteine, in an electrodeposition bath, increases the potential for the hydrogen evolution reaction (HER) and also prevents direct zinc deposition, and the deposited film exhibits high corrosion resistance.<sup>10</sup> It was found that citrate significantly increases the stability of the baths and denser coatings are deposited due to higher bath pH.<sup>9</sup>

Assaf *et al.* (1995) studied the effects of electroplating parameters such as bath composition, temperature and current density on the deposition of copper, zinc and brass on a steel substrate. However, they found that the zinc deposited at a low current density ( $<3 \text{ mA cm}^{-2}$ ) and low zinc content ( $<15 \text{ g dm}^{-3}$ ) in the bath affected the formation of fine grains and left some bare areas. This behaviour may be due to the low cathodic current efficiency of zinc deposition and the steady evolution of hydrogen gas.<sup>13</sup>

Rastogi and Pandey (2009) studied the electrodeposition of Zn–Mn–Mo alloy from citrate baths by investigating various parameters such as current density, temperature, pH, deposition time and the concentrations of chemical compounds. They found that the optimum conditions were 30 g L<sup>-1</sup> ZnSO<sub>4</sub>·H<sub>2</sub>O,  $60 \text{ g L}^{-1} \text{ MnSO}_4 \cdot \text{H}_2\text{O}, 4 \text{ g L}^{-1} (\text{NH}_4)_2\text{MoO}_3, 5 \text{ g L}^{-1} \text{ C}_6\text{H}_8\text{O}_7 \cdot \text{H}_2\text{O},$ pH 2.05, temperature of 25 °C, deposition time of 30 minutes, and current density of 4.0 A dm<sup>-2</sup>; semi-bright, light grey and adherent deposits were obtained.<sup>14</sup>

Nowadays, Zn–Ni alloy coatings are eco-friendly substitutes for the toxic cadmium coating<sup>7</sup> and have attracted significant

Centre for Risk, Integrity and Safety Engineering (C-RISE), Faculty of Engineering & Applied Science, Memorial University, St. John's, NL, A1B 3X5, Canada. E-mail: fikhan@mun.ca

attention due to their ability to provide better corrosion resistance and mechanical properties at higher temperatures and under severe environmental conditions, compared to pure zinc and other zinc alloy coatings.<sup>9</sup> Several analyses have been undertaken to understand the characteristics of the electrodeposition process of Zn–Ni alloys. It was found that the features of the deposited coatings depend on the current density, pH, bath composition, applied voltage, additives and temperature.<sup>6</sup> The phases and crystal structures of the surfaces of the deposited Zn–Ni alloys are significant characteristics that control the corrosion resistance and other mechanical properties.<sup>7,8</sup>

As seen from the above literature, several experimental studies have been implemented on the Zn-Ni deposited from citrate bath under various operating conditions. To the best of the authors' knowledge, there has not been a systematic study that specifically compares the pure Zn and the Zn-Ni alloy deposited from citrate and non-citrate baths, or on the optimum parameter conditions that suppress the hydrogen evolution reaction (HER) to improve the corrosion resistant properties of the coatings. Therefore, to bridge this gap, the present research is directed at investigating and analyzing the pure Zn and Zn-Ni alloy deposited under various operating conditions. Herein, we report the use of pure Zn and Zn-Ni alloy coatings on steel substrates to improve corrosion resistance, using potassium citrate as a complexing agent. The effects of plating variables such as bath composition and current density on coating composition, morphology and corrosion properties have been investigated. The XRD technique was used for structural phase analysis and to calculate the average crystal size of the coating. SEM was used for morphological analysis and AFM was used for topographical analysis. The electrochemical behaviour of the deposition bath on steel plates was studied by cyclic voltammetry (CV). Potentiodynamic polarization measurements (Tafel) and EIS were carried out to evaluate the corrosion protection performance of the Zn-Ni alloy coatings. The equivalent electrical circuits obtained from the experimental data fitted to Nyquist and Bode plots were also used to compare the Zn-Ni deposited from citrate with the pure Zn and Zn-Ni from the noncitrate bath. The effects of the optimum operating parameters on the deposition character and their corrosion behaviour have been observed and are discussed.

# Challenge: establishment of stable baths for Zn and Zn–Ni containing coatings

Due to the negative reduction potential of the Zn/Zn<sup>2+</sup> electrode, it is more challenging to electroplate Zn than hydrogen gas:<sup>16</sup>

$$Zn^{2+} (aq) + 2e^{-} \rightarrow Zn (s) E_{Zn/Zn^{2+}} = -0.762 V$$
  
 $2H^{+} (aq) + 2e^{-} \rightarrow H_2 (g) E_{2H/H_2} = 0.000 V$ 

The hydrogen ions in the electrolyte solution will be deposited before zinc since  $H^+$  ions have a more positive reduction

potential in the standard state. To overcome and modify this problem, a higher pH of the electroplating bath is preferable. Generally, a bath with a high pH (alkaline) is not stable. Therefore, most electroplating is developed in an acidic bath. The major problem with the use of an acidic bath is that the hydrogen evolution reaction occurs in the electrolyte and exhibits non-uniform coatings that are less corrosion resistant. Although the citrate bath in this work has a relatively low pH, the addition of citrate is helpful in stabilizing the plating bath during electrodeposition because the reduction of hydrogen will increase the pH around the cathode. Thus, the existence of citrate in the bath can prevent the precipitation of metal hydroxides around the cathode.

To electrodeposit Zn coatings with suitable compositions and microstructures that lead to ideal corrosion resistant and mechanical properties, the development of a stable plating bath with relatively high pH is vital. To suppress hydrogen deposition and stabilize the plating baths, alkalis and complexing agents (*e.g.*, acetate and citrate) were added to the baths for ideal Zn, Zn–Ni and Zn–Ni composite electroplating. According to the above results, the corrosion resistant properties, uniformity, thickness, and the mechanical hardness of the plated films were also improved.<sup>16–20</sup>

# 2.1 The effect of the complexing agent on the stability of the plating bath

The stability of the electroplating bath was studied using a stability diagram or Pourbaix diagram. Complexing agents such as potassium citrate were employed to stabilize the metal and alloy plating baths.

Fig. 1(a) and (b) show the Pourbaix diagrams calculated for the Zn–Ni alloy deposited from non-citrate, 0.0816 M and 0.163 M citrate baths. The dashed lines 'a' and 'b' refer to the equilibrium lines for  $H^+/H_2$  and  $(O_2 + H_2O)/OH^-$ , respectively.<sup>21</sup>

It can be seen from the figure that, thermodynamically, the stability of a Zn–Ni alloy plating bath is dominated by the precipitation of  $Zn(OH)_2$  and  $Ni(OH)_2$  at pH 6.2 and 6.8, respectively (Fig. 1(a)). The red line indicates  $Zn(OH)_2$  whereas the green line indicates  $Ni(OH)_2$ . After the addition of 0.0326 M potassium citrate, the Zn–Ni alloy plating bath was thermodynamically stable until pH 7.2 for  $Zn(OH)_2$  and pH 7.8 for  $Ni(OH)_2$  was reached with the given concentration of metal ions (Fig. 1(b)), and the formation of the stable complexing species such as  $Zn[C_6H_5O_7]^-$  and  $Ni[C_6H_5O_7]$ . Therefore, it was observed from these two Pourbaix diagrams that the  $Zn(OH)_2$  and  $Ni(OH)_2$  precipitation was extended to one pH on the pH scale, which stabilized the electrolyte bath.

From Fig. 1(b), it is apparent that citrate has the strongest complexing power for Zn ions, followed by Ni ions. Therefore,  $Zn[C_6H_5O_7]_{(aq)}$  and  $Ni[C_6H_5O_7]_{(aq)}$  contribute to stabilizing the Zn–Ni elements in the bath solution.

The calculated stability diagrams demonstrate that, thermodynamically, citrate can effectively stabilize Zn–Ni alloy plating baths, preventing the precipitation of metal hydroxides at a higher pH. Bath stability tests on baths with and without the addition of potassium citrate were conducted.



Fig. 1 (a) Pourbaix diagram for Zn–Ni alloy plating from the non-citrate bath; (b) Zn–Ni alloy plating from the 0.0326 M citrate bath.

# 3. Experimental details

The electrodeposition experiments were carried out in a bath with a 200 mL solution at room temperature. A rectangular steel plate of 10 cm<sup>2</sup> was used as the working electrode (WE), and a graphite rod was used as the counter electrode (CE). The reference area of the coated sample was 1 cm<sup>2</sup> for the electrochemical analysis. The CE and WE were connected to the DC power supply *via* a multi-meter. There were three types of baths prepared: bath-1 (chloride bath, without potassium citrate, containing ZnCl<sub>2</sub>, SDS and NaCl); bath-2 (chloride bath, without potassium citrate, containing ZnCl<sub>2</sub>, SDS and NaCl); bath-2 (SDS and SDS and SDS) and SDS and

NaCl); and bath-3 (chloride bath, with potassium citrate, containing  $\text{ZnCl}_2$ ,  $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$ , SDS, NaCl,  $\text{K}_3(\text{C}_6\text{H}_5\text{O}_7)$  and  $\text{H}_3\text{BO}_3$ ), as shown in Table 1. They were degreased with 10 wt% sodium hydroxide solution for 5 min, then rinsed with 10% hydrochloric acid and alcohol or acetone for a few seconds. The operating conditions for electrodeposition are listed in Table 2. After deposition, the Zn and Zn–Ni alloy coatings were washed with distilled water and dried in air.

Electrochemical analyses were performed using a ZAHNER IM6 electrochemical workstation produced by ZAHNER-Elektrik GmbH & Co. KG, Germany. The electrochemical analysis experiments were carried out in a conventional three-electrode Table 1 Bath compositions for the electrodeposition of pure Zn and Zn-Ni alloy coatings

۲	a	р	e	r

	Concentrations					
Bath composition	Bath-1	Bath-2	Bath-3			
Zinc chloride (ZnCl <sub>2</sub> )	$60 (g L^{-1})$	$60 (g L^{-1})$	$60 (g L^{-1})$			
Nickel(II) chloride hexahydrate (NiCl <sub>2</sub> $\cdot$ 6H <sub>2</sub> O)	_	$20 (g L^{-1})$	$20 (g L^{-1})$			
Boric acid (H <sub>3</sub> BO <sub>3</sub> )		_	$8 (g L^{-1})$			
Sodium dodecyl sulfate (SDS)	$1.7 imes10^{-5}~{ m M}$	$1.7\times10^{-5}~{\rm M}$	$1.7 \times 10^{-5} \text{ M}$			
Potassium citrate $(K_3(C_6H_5O_7))$		_	$8 (g L^{-1})$			
Sodium chloride (NaCl)	8 (g L <sup>-1</sup> ) bath pH = 2.0	8 (g $L^{-1}$ ) bath pH = 2.0-2.5	8 (g L <sup>-1</sup> ) bath pH = 2.5-3			

Table 2	Operating	conditions	for	depositing	the	pure Zn	and	Zn–Ni
alloy coa	atings							

Operating conditions	Samples
Anode	Graphite rod
Cathode	Steel plates
Current density	$20, 40, 60 \text{ mA cm}^{-2}$
Plating time	10 minutes
Stirred speed	350 rpm
Temperature	Room

cell with a 200 mL solution. A 10 cm<sup>2</sup> rectangular steel plate was used as the cathode. A graphite rod was used as the anode. Silver/silver chloride with saturated potassium chloride as a salt bridge (Ag/AgCl/KCl<sub>sat</sub>) was used as the reference electrode. The schematic stability diagrams were plotted using OLI Analyzer Studio software. The morphology of the deposited samples was investigated using a scanning electron microscope equipped with an energy dispersive spectrometer (FEI MLA 650F). A Rigaku Ultima IV X-ray diffractometer with a copper X-ray source and a scintillation counter detector ( $\lambda = 1.5418$  Å) was used to study the crystal phase structures of the deposits, and the databases used to identify the peaks were pdf# 03-065-5310 and 00-004-0831 RDB Minerals, International Centre for Diffraction Database (ICDD).

The Debye–Scherrer equation was used to calculate the average crystallite size of the samples from the peak width at the half maximum of the crystal peaks  $(\beta)$ :<sup>22</sup>

$$t = \frac{0.94\lambda}{\beta \cos \theta}$$

where *t* is the crystallite size,  $\lambda$  is the wavelength of the X-ray radiation,  $\theta$  is the Bragg's angle of the peak and  $\beta$  is the angular width of the peak at full width at half maximum (FWHM).

The topographical structure of the coatings was analyzed by atomic force microscopy (Asylum Research MFP 3D). A Vickers Microhardness Testing machine measured the hardness of the coating.

### 4. Results and discussion

#### 4.1 Chemical compositions and surface morphology

The surface morphologies of the electrodeposited pure Zn and Zn–Ni coatings deposited from the citrate bath and the

non-citrate bath were investigated using SEM, as shown in Fig. 2. The deposited Zn-Ni alloy coating was developed, in terms of its uniformity, porosity and grain size, by varying the bath compositions and current density. As the current density increased, the over-potential increased, leading to an increase in the nucleation rate and reduction in the grain size of the coating. This was investigated and reported by El-Sherik et al.23 and Feng et al.24 Sample (a), which is the pure Zn coating deposited from the non-citrate bath at same current density, exhibited a larger grain size and a rough structure with some cracks and holes, as also shown in Fig. 3 using AFM analysis. Sample (b), deposited from the citrate bath, showed a uniform surface with smaller grain sizes; sample (c), deposited from the non-citrate bath under the same conditions, revealed non-uniformity and swelling with larger and coarser grain sizes found due to the HER, and the bath was not stable. Therefore, sample (b) showed uniformity with an adherent and dense Zn-Ni coating surface (Fig. 2(b)). The incorporation of Ni into the Zn matrices slightly modified the morphology of the Zn-Ni coatings. The Zn coating is composed of hemispherical structures; however, after incorporation, the structure changed.<sup>24,25</sup> A similar result was demonstrated by Feng et al. (2015) on adding the complexing agents; a significant decrease in the grain size was observed, and the deposits were smooth, homogeneous, uniform, compact and fine-grained without any pores or pinholes at the surface,<sup>26</sup> as shown in Fig. 2(b). The optimum value of the plating current density was 60 mA cm<sup>-2</sup>, with smaller grain size and denser coating. The coatings shown in Fig. 2 and 3 were plated at 60 mA cm<sup>-2</sup>. Rahman et al. (2009) reported that from 40–60 mA cm<sup>-2</sup>, the plating current density grain of the deposit was smaller and more uniform and no porosity was found; whereas, with increased plating, current densities after 60 mA cm<sup>-2</sup> produced non-uniform crystals and coarsegrained coatings.15

The surface morphologies of the corroded pure Zn and Zn– Ni alloy coatings immersed in sodium chloride solution are shown in Fig. 3. All the images are at the same magnification but the image shown in the inset is at a higher magnification. It can be seen that the corrosion products were formed on the Zn and Zn–Ni alloy coatings. Sample (a), the pure Zn coating and sample (c), the Zn–Ni deposited from non-citrate, demonstrated the formation of the uniformly distributed voids and porous structures on the surface of the coating. When tensile and



Fig. 2 The SEM images of pure Zn and Zn–Ni alloy coatings: (a) pure Zn deposited from the non-citrate bath, (b) Zn–Ni deposited from the citrate bath, (c) Zn–Ni deposited from the non-citrate bath.

compressive stress were applied to the porous corroded samples, the samples cracked after prolonged exposure times.<sup>27</sup> Sample (b) deposited from the citrate bath had less of this effect on the surface of the coating. Moreover, after the immersion test, uniform and compact corrosion products appeared on the sample (b) and attained higher corrosion resistant properties. As per the above results, after the immersion in 3.5% NaCl solution, the corrosion product was formed on the coated surface; therefore, the wettability of the coated surface had a significant effect on the corrosion prevention on the Zn and Zn–Ni deposits.<sup>28</sup>

#### 4.2 Atomic force microscopy (AFM) analysis

The topographical 2D and 3D images of the surfaces of the pure Zn and Zn–Ni alloy coated samples, (a), (b) and (c), obtained by AFM measurement deposited from citrate bath and non-citrate bath are shown in Fig. 4. In the case of sample (a), the cathodic deposition was non-uniform, heterogeneous and had a large peak with bigger grains in comparison to the other samples. Samples (b) and (c) were less coarse and were uniform in texture. Sample (b) was uniform, homogeneous, and compact and exhibited small peaks with regular grain size, leading to higher mechanical and corrosion resistant properties. The additives or complexing agents were preferentially adsorbed on the Zn–Ni matrix and inhibited the Zn–Ni alloy depositions, resulting in the smaller reduction of Zn<sup>2+</sup> and Ni<sup>2+</sup> on these matrices, and therefore, smooth and homogeneous deposits were observed.<sup>29</sup> The roughness factor illustrates the initial surface irregularities, non-uniformity and heterogeneity; therefore an irregular surface demonstrates a higher dissolution rate, especially in the presence of a corrosive environment.<sup>30</sup> This surface factor suggests the non-linear dependence of the uniformity of the coating<sup>26,31</sup> deposited from a citrate or non-citrate bath.

#### 4.3 Cyclic voltammetry studies

Cyclic voltammetry (CV) is used to characterize the electrochemical behaviour and kinetics of electrochemical reactions.<sup>32</sup> Fig. 5 shows the CV behaviour and the influence of citrate and non-citrate bath on the pure Zn and Zn-Ni electroplated on steel plates at room temperature. The CVs under the given conditions were characterized by the presence of two peaks in an anodic scan and one peak in a cathodic scan. The anodic peaks seen in the anodic scan during the electrochemical oxidation of the alloy were attributed to the dissolution of the coating in the alloy from different intermetallic phases.<sup>33</sup> The two anodic peaks at 293 mV for the Zn–Ni alloy deposited from citrate and non-citrate correspond to the dissolution of Ni from their phases.<sup>8,34,35</sup> Therefore, the voltammetric behaviour of the Zn–Ni



Fig. 3 The SEM images of the corroded pure Zn and Zn–Ni alloy coatings, (a) pure Zn deposited from the non-citrate bath, (b) Zn–Ni deposited from the citrate bath, (c) Zn–Ni deposited from the non-citrate bath.

alloy indicates the properties of its structure and components in the deposited phase. The anodic current density of the pure Zn coating was high in comparison to the Zn–Ni coating, leading to an increase in the dissolution rate of pure Zn.

#### 4.4 X-ray diffraction (XRD) analysis

The distinct crystalline phase and orientations of the pure Zn and Zn-Ni coated XRD patterns were observed under different conditions. Fig. 6 shows that the coatings contain three dominant diffraction peaks: Zn (101),  $\gamma$ -NiZn<sub>3</sub> (831) and  $\gamma$ - $Ni_2Zn_{11}$  (330). The critical peaks of pure Zn coating at 36°, 43° and 54° match Zn (002), Zn (101) and Zn (102), respectively. The peaks at about  $38^\circ$ ,  $43^\circ$  and  $73^\circ$  correspond to  $\gamma$ -NiZn<sub>3</sub> (831) and  $\gamma$ -Ni<sub>2</sub>Zn<sub>11</sub> (330) and (631) phases of the Zn-Ni alloy, respectively. The other peaks at 51°, 69° and 82° match the Zn-Ni (111) and Zn (110) (200) phases, respectively. The Zn-Ni coating deposited from the citrate bath had the highest intensity of the  $\gamma$ -phase ( $\gamma$ -Ni<sub>2</sub>Zn<sub>11</sub>) with (330) plane orientation, whereas for the pure Zn coating it was Zn (101) as shown in Fig. 6(a) and (b). Moreover, the peak value of the  $\gamma$ -phase with the (330) plane orientation was higher than that of other  $\gamma$ -phase orientations such as  $\gamma$ -NiZn<sub>3</sub>, demonstrating that the  $\gamma$ -phase with the (330) plane orientation plays an assertive role in the Zn–Ni alloy coatings.<sup>28,31,36</sup> The intensity of the  $\gamma$ -phase  $(\gamma - Ni_2 Zn_{11})$  of sample (b) was high in comparison to sample (c). The crystal peaks intensities illustrated the information on the number of phases and also the relative amounts of Zn-Ni

in the deposits.<sup>37</sup> Therefore, the coating with high-intensity  $\gamma$ -phase with (330) (831) plane orientation exhibited better corrosion resistance.

#### 4.5 Potentiodynamic polarization analysis

The potentiodynamic polarization curves of the pure Zn and Zn-Ni alloy films deposited from citrate and non-citrate baths at three different plating current densities ranging from 20-60 mA cm<sup>-2</sup> were studied. The polarization analysis was performed in an aerated 3.5% NaCl solution at room temperature, and the scan rate was 10 mV s<sup>-1</sup> as tabulated in Table 3. The polarization curves of different coatings were measured at their open circuit potential (OCP), and corrosion current densities (Icorr) and corrosion potentials  $(E_{corr})$  were calculated from the intercepts on the Tafel slopes by extrapolation, obtained with reference to the silver and silver chloride electrode with saturated potassium chloride as the salt bridge (Ag/AgCl/KCl<sub>sat</sub>). The corrosive activity of the Zn-Ni alloy coating in corrosive media is directly related to the corrosion potentials. The corrosion resistance of the coating is mainly related to the structural morphologies, chemical compositions and phase compositions.37

It has been shown that the principal cathodic reduction of pure Zn and Zn alloy is oxygen reduction, which is the rate controlling step for the corrosion.<sup>38</sup> However, the superior corrosion resistance of the deposits corresponds to the more positive corrosion potential ( $E_{\rm corr}$ ) values or lower corrosion



Fig. 4 2D and 3D images of Zn and Zn–Ni alloy electrodeposited coatings: (a) pure Zn coating from non-citrate, (b) Zn–Ni coating deposited from citrate, (c) Zn–Ni coating deposited from non-citrate.

current  $(I_{\rm corr})$ .<sup>39</sup> Table 3 shows that the  $E_{\rm corr}$  of the pure Zn coating at 40 mA cm<sup>-2</sup> deposited from the non-citrate bath is less negative in comparison to the Zn plated at 20 and 60 mA cm<sup>-2</sup>. However,  $I_{\rm corr}$  for the pure Zn coating plated at 60 mA cm<sup>-2</sup> exhibits a lower value (4.76 mA cm<sup>-2</sup>). Therefore, the increase in plating current density leads to less corrosion resistance properties for the Zn coating. Moreover, for the Zn-

Ni alloy coatings deposited from citrate and non-citrate baths, as the plating current density increased, the  $I_{\rm corr}$  decreased, and less negative  $E_{\rm corr}$  were recorded. Assaf *et al.* obtained similar results.<sup>40</sup> Moreover, Abou-Krisha<sup>41</sup> found that increasing the plating current density improved Ni content in the coating and shifted the  $E_{\rm corr}$  toward more positive potential, which led to higher corrosion resistance properties.



Fig. 5 Cyclic voltammogram for pure Zn and Zn–Ni coating from electrolytic baths at a scan rate of 5 mV s<sup>-1</sup>.

The  $E_{\rm corr}$  of the Zn coating deposited from the non-citrate bath at 60 mA cm<sup>-2</sup> exhibited a more negative potential (-0.810 V), whereas, those of Zn–Ni alloy coatings deposited from the non-citrate bath and citrate bath were -0.790 V and

-0.760 V, respectively. It is also noticeable from Table 3 that the  $E_{\rm corr}$  shifted to more positive values as the plating current density increased, and the Zn–Ni alloy coating deposited from citrate bath improved the corrosion resistant properties of the steel.

The  $I_{\rm corr}$  of sample (b) at 60 mA cm<sup>-2</sup> was 2.98 mA, whereas for sample (a), it was 4.76 mA and for sample (c) it was 5.93 mA. The sample (b) coating possessed a lower  $I_{\rm corr}$  value than the other coated samples. The least  $I_{\rm corr}$  is due to the stable citrate bath Zn–Ni coated samples with decreased HER, which exhibited uniform and high anti-corrosive coating and is also shown on the SEM images for sample (b), which has small grain size, and compact, bright and uniform Zn–Ni coating. The sample (c) coated film had swelling and non-uniformity on the surface due to hydrogen evolution. Moreover, as the current density of the Zn–Ni plated sample increased, it led to



Fig. 6 XRD patterns for the pure Zn and Zn–Ni alloy coatings using different baths: (a) pure Zn coating deposited from non-citrate, (b) deposited with citrate, (c) deposited from non-citrate.

Samples	Deposition current density, (mA cm <sup>-2</sup> )	Corrosion potential, <i>E</i> <sub>corr</sub> (mV)	Corrosion current, $I_{\rm corr}$ (mA cm <sup>-2</sup> )	Corrosion rate (µmpy)
(a) Pure Zn from non-citrate	20	-820	7.39	40.51
	40	-810	6.22	38.58
	60	-814	4.76	41.54
(b) Zn–Ni from citrate	20	-798	7.15	29.8
	40	-780	5.91	36.13
	60	-760	2.98	27.28
(c) Zn–Ni from non-citrate	20	-800	8.51	35.27
	40	-812	8.90	38.29
	60	-790	5.93	32.64

#### Paper



**Fig. 7** Polarization curve for the pure Zn and Zn–Ni alloy coatings deposited from citrate and non-citrate baths.

a decrease in the corrosion rate of the coated sample, whereas for pure Zn plating, it increased (Table 3).

The optimal results of the Zn and Zn–Ni coated samples deposited from citrate and non-citrate baths at 60 mA cm<sup>-2</sup> current density are shown in Fig. 7, illustrating that the Zn–Ni alloy coating from the citrate bath exhibited less  $I_{corr}$  and more positive  $E_{corr}$  in comparison to the pure Zn and Zn–Ni alloy coatings deposited from the non-citrate bath, which led to the enhanced corrosion–resistant properties of the coating. Zn–Ni alloy was deposited at lower and higher concentrations of citrate. However, the coated sample was non-uniform and exhibited minimum corrosion resistance properties to the bare steel. Therefore, after the exploration test, these concentrations were selected and used in this paper.

As observed from Table 4, that the corrosion potential of the pure Zn coated samples are more harmful than the Zn-Ni alloy coating. This implies that all of the electrodeposited Zn-Ni samples offer more corrosion protection to the bare steel substrate. The corrosion rate of Zn-Ni deposited from citrate and non-citrate was 27.28 µmpy and 41.54 µmpy, whereas for pure Zn, it was 32.64 µmpy; this implies that the Zn-Ni deposited from citrate exhibited higher corrosion resistant properties in comparison to Zn-Ni from non-citrate and pure Zn coatings. On the other hand, Table 4 indicates that the Ni content in the Zn-Ni coating deposited from citrate bath is 8.3 wt%, whereas Zn-Ni without citrate is 4.3 wt%. This can be attributed to the higher surface activity of Zn ions in comparison to nickel ions. The average crystal size of the pure Zn coating is 80.92 nm, whereas the Zn-Ni coating deposited from the citrate bath is 35.40 nm (Table 4).

#### 4.6 Electrochemical impedance spectroscopy (EIS) analysis

The Electrochemical Impedance Spectroscopy (EIS) measurement is used as a corrosion resistance technique to evaluate the characteristics and kinetics of the electrochemical process prevailing at the electrode/solution interface in corrosive solutions.42,43 The EIS measurements were carried out by the deposition of citrate and non-citrate baths in a 3.5% NaCl solution to calculate the corrosion resistance behaviour of Zn-Ni coatings. The OCP's range of frequency was 100 kHz to 100 mHz, the amplitude was 10 mV, and the scan rate was 10 mV  $s^{-1}$ . The measured EIS data are displayed as Nyquist plots and typical Bode plots in Fig. 8–10. In the Nyquist plots, the polarization resistance resembles the shape of a semicircle.8,37 All the impedance obtained at different current densities are shown in Fig. 8. The EIS measurement of the pure Zn coating deposited from the non-citrate bath exhibited a smaller impedance modulus. However, the Zn-Ni alloy coating deposited from the citrate bath showed a higher impedance modulus than the Zn-Ni alloy deposited from the non-citrate bath at 20 mA  $\text{cm}^{-2}$ . The best coating with the maximum impedance modulus was found at 60 mA  $cm^{-2}$  for sample (b), as shown in Fig. 2(b). The worst coating with the least impedance modulus was found at 20 mA cm<sup>-2</sup> for the pure Zn coating as shown in Fig. 8(a), and it is related to a little arc at high frequencies, forming the oxide film in air.44

The optimal results of the Nyquist plot at 60 mA cm<sup>-2</sup> current density are shown in Fig. 9. The equivalent electrical circuit can explicate the corrosion resistance of the present Zn–Ni alloy coating circuit. The electrical circuits are shown in Fig. 11, where  $R_{sol}$  represents the solution/electrolyte resistance between the reference and the working electrode (*i.e.*, Zn–Ni coated specimen).  $R_3$  and CPE<sub>3</sub> correspond to the resistance and capacitance of the formation of the thin oxide film that is reinforced by the ionic conduction through its pores.  $R_2$  and CPE<sub>2</sub> correspond to the resistance and capacitance of the pure Zn and Zn–Ni alloy films.  $R_1$  represents the charge transfer resistance associated with the reaction of zinc oxide and reduction of oxygen. CPE<sub>1</sub> corresponds to the electric double layer capacitance at the interface of the coating/electrolyte solution.<sup>28</sup>

The mathematical equation for the impedance of constant phase element (CPE) is given below:<sup>45</sup>

$$Z(Q) = y_0^{-1} (jw)^{-\alpha}$$

where  $y_0$  is the coefficient of the constant phase element,  $j^2 = -1$ , an imaginary constant, w is the frequency, and  $\alpha$  is the

Table 4	The optimized results	s for the pure Zn and Zn	<ul> <li>Ni alloy coating (</li> </ul>	deposited from citrate and non-citrate
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	Coating compositi	on (wt%)	Average crystallite	$E_{\rm corr}$ (mV vs.	I <sub>corr</sub>	Corrosion rate
Bath condition	Zn	Ni	size (nm)	Ag/AgCl)	$(mA cm^{-2})$	(µmpy)
(a) Pure Zn from non-citrate	100	_	80.92	-814	4.76	41.54
(b) Zn–Ni from citrate	91.7	8.3	35.40	-760	2.98	27.28
(c) Zn–Ni from non-citrate	95.7	4.3	40.78	-790	5.93	32.64



Fig. 8 Nyquist plot for the Zn–Ni alloy coatings at different current densities, (a) pure Zn deposited from the non-citrate bath, (b) Zn–Ni deposited from the non-citrate bath.

exponential of CPE;  $\alpha = 0$  represents the full resistor,  $\alpha = -1$  represents the inductor,  $\alpha = 1$  represents an ideal capacitor,  $\alpha = 0.5$  represents the Warburg impedance.<sup>45</sup>

All the measured impedance values were fitted using the Zahner Thales software. The calculated fit data of the electrical equivalent circuit deposited from citrate and non-citrate baths for the pure Zn and Zn–Ni alloy coating are shown in Table 5. The charge transfer resistance ( $R_1$ ) of the pure Zn coating was 55.6  $\Omega$  cm<sup>2</sup>, whereas, for the Zn–Ni coating deposited from the citrate bath, it was 3.6 k $\Omega$  cm<sup>2</sup> and for the non-citrate Zn–Ni alloy sample, the value was 688.6  $\Omega$  cm<sup>2</sup>. This illustrates that the higher oxide reduction and zinc oxide reaction occurring on the Zn–Ni coated surface deposited from citrate bath, and the lower  $R_1$  value, are due to the increase of the active surface, which is



**Fig. 9** Nyquist plot for the pure Zn and Zn–Ni alloy coatings deposited from citrate and non-citrate baths.

related to the discontinuity and porosity of the coated film. It is well known that higher polarization resistance  $(R_1)$  values indicate better corrosion resistance. The coating resistance  $(R_2)$ 



**Fig. 10** Bode plots for the pure Zn and Zn–Ni alloy coatings deposited from citrate and non-citrate baths; (a) log modulus Z vs. log f; (b) phase angle vs. log f.

 Table 5
 Electrochemical parameters determined by equivalent circuit modelling

Bath condition	$R_{\rm sol} \left(\Omega {\rm cm}^2\right)$	$R_1 \left(\Omega \ \mathrm{cm}^2\right)$	$R_2 \left(\Omega \ \mathrm{cm}^2\right)$	$R_3 \left(\Omega \ \mathrm{cm}^2\right)$	$CPE_1 (\mu F^{\alpha} cm^2)$	$CPE_2 (\mu F^{\alpha} cm^2)$	$CPE_3 (nF^{\alpha} cm^2)$
Pure Zn from non-citrate	3.06	55.6	67.65	3.5	893.3, $\alpha = 0.761$	173.5, $\alpha = 0.712$	61.3, $\alpha = 1.0$
Zn–Ni from non-citrate	2.62	688.6	264.7	3.3	105.5, $\alpha = 0.599$	63.7, $\alpha = 0.858$	104.0, $\alpha = 1.0$
Zn–Ni from citrate	3.08	3.6K	879	4.2	39.8, $\alpha = 0.626$	28.2, $\alpha = 0.766$	98.3, $\alpha = 1.0$



**Fig. 11** Electrical equivalent circuit modelling used for the simulation of EIS data of pure Zn and Zn–Ni alloy coating deposited from citrate and non-citrate baths.

of Zn–Ni from the citrate bath is  $879 \Omega \text{ cm}^2$ , from the non-citrate bath is 264.7  $\Omega$  cm<sup>2</sup>, and pure Zn coating from the non-citrate bath is 67.65  $\Omega$  cm<sup>2</sup>. The decrease in  $R_1$  from Zn–Ni to pure Zn from the citrate to non-citrate bath indicates the easier access of the electrolyte on the pure Zn coated surface deposited from the non-citrate baths. Moreover, the pure Zn coating deposited from the non-citrate bath had the lowest  $R_1$  and  $R_2$ , which means that the electrolyte molecules that diffused into the coating surface exhibited less corrosion resistance. In the initial measurement, the low-frequency capacitive magnitude was less because there was a smaller effect of corrosive media on the working electrode and thus the obtained impedance response was purely due to the coated surface. As a result, the Zn-Ni alloy from the citrate bath had a maximum coating resistance  $(R_2)$  with a minimum capacitance  $(CPE_2)$  of 879  $\Omega$ cm<sup>2</sup> and 28.2 µF cm<sup>2</sup>. The similar electrical equivalent circuit was reported by Feng et al. (2016) who prepared a Zn-Ni alloy coating from a new DMH-based bath as a replacement for Zn and Cd coatings.24 This behaviour indicates that the addition of the complexing agent  $(K_3(C_6H_5O_7))$  in a bath is a simple and effective process to improve the corrosion resistance of the Zn-Ni alloy coating.

As seen in the Bode plot, in the view of impedance vs. frequency, the impedance value increased on adding the potassium citrate. As for Bode plots of frequency vs. phase angle, the phase angle also increased from the citrate bath, as shown in Fig. 10(a) and (b).

#### 4.7 Vickers microhardness test

The Vickers microhardness values obtained from different bath conditions of pure Zn and Zn–Ni alloy coatings electrodeposited on steel are shown in Fig. 12. The development of film microhardness showed an increase from 154 HV for the pure coating from the non-citrate (sample (a) to 223 HV sample (b)) prepared



**Fig. 12** Vickers microhardness of pure Zn and Zn–Ni alloy electrodeposited on steel from different baths.

from the citrate bath. It was concluded that the microhardness was affected by the deposition of Zn–Ni from the citrate bath. Thus, the crystallite size is a significant variable that affects the hardness value.<sup>46,47</sup> The smaller grain size suggests that there is a more substantial amount of grain boundaries that obstruct the dislocation motion and then create harder materials.

## 5. Conclusions

The electrochemical behaviour of pure Zn and Zn–Ni alloy coatings from citrate and non-citrate baths and the stability of the electrolyte baths have been studied in this work. According to the above analysis, the following conclusions can be made:

• Stabilized plating baths and complexing agents such as potassium citrate can be employed for Zn-Ni alloy electrodeposition. This extends the precipitation of  $Ni(OH)_2$  and  $Zn(OH)_2$  to a higher pH and the hydrogen evolution reaction is suppressed.

• The potentiodynamic polarization results reveal that the sample (b) coating possesses a lower  $I_{\rm corr}$  value and a more positive corrosion potential than the other two coated samples. The smallest  $I_{\rm corr}$  is due to the stable citrate bath Zn–Ni coated samples with decreased HER, which exhibited uniform and higher corrosion resistance and the SEM images showed the formation of denser and more uniform coating. The phase structure of the Zn–Ni deposits from the citrate bath had the highest intensity of the  $\gamma$ -phase ( $\gamma$ -NiZn<sub>3</sub>) (815), and the  $\gamma$ -Ni<sub>2</sub>Zn<sub>11</sub> (330) (631) plane orientation exhibited better corrosion resistance.

• The EIS measurement of the sample (b) deposited from the citrate bath showed higher impedance modulus than the other coated samples. Further EIS measurements carried out for sample (a) and sample (c) deposited in the non-citrate bath

showed lower impedance moduli in comparison to sample (b). The best coating with the maximum impedance modulus was found at 60 mA cm<sup>-2</sup> for sample (b). The electrical equivalent circuit modelling data best fit the generated Nyquist plot and demonstrated that the Zn–Ni alloy coating on a steel substrate deposited from the citrate bath had maximum coating resistance ( $R_2$ ) with minimum capacitance (CPE<sub>2</sub>). This behaviour indicates that the addition of the complexing agent ( $K_3(C_6H_5O_7)$ ) to a bath is a simple and effective process to improve the corrosion resistance of Zn–Ni alloy coating.

• Higher current density also leads to reduced grain size and provides a stronger, less coarse and more uniform coating. The development of film microhardness showed an increase in the hardness from 154 HV for pure Zn (sample (a)) and 223 HV for the Zn–Ni coating deposited from a non-citrate (sample (c)) to (sample (b)) that prepared from a citrate bath.

# Conflicts of interest

There is no conflicts to declare.

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