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Co/Cu-MFF derived mesoporous ternary metal oxide microcubes for enhancing the catalytic activity of the CO oxidation reaction†

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Metal–organic framework (MOF)-based derivatives with uniform micro/mesoporous structures have attracted a great deal of interest in various research fields. Herein, we report a simple strategy to design functional mesoporous ternary metal oxides with controlled composition through direct pyrolysis of Co/Cu bimetal-formate frameworks (Co/Cu-MFFs), which were prepared by a facile one-step liquid-phase precipitation method, exhibiting uniform distribution of two different metal species and good structural integrity. The obtained mesoporous ternary metal oxide $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ ($x = 0.5, 1$) microcubes exhibit much better performance for CO oxidation than pure Co_3O_4 , which can be mainly attributed to their larger specific surface areas, stronger reducibility, and the synergistic effect of two active metal oxide components.

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1. Introduction

CO oxidation over solid catalysts has been extensively studied, not only with regard to its value as a classical probe reaction for fundamental studies but also due to its great importance in practical applications, such as air cleanup, gas sensors for detection, automotive exhaust gas treatment and CO elimination from the hydrogen feed for proton-exchange membrane fuel cells.^{1–5} It has been reported that noble metals such as Pt, Au, and Rh are excellent CO oxidation catalysts.^{2,6–11} Platinum group metals (PGMs) are some of the earliest catalysts and are still widely employed in automotive emission control and cleaning of gas originating from the petrochemical industry since Langmuir's pioneering work.^{6,7,12} Haruta *et al.* discovered that oxide-supported Au catalysts prepared through a wet chemistry method exhibit an outstanding high activity for CO oxidation even at cryogenic temperatures.¹³ Recently, a sub-nano Rh/TiO₂ catalyst with an unexpectedly high performance of total CO conversion at $-50\text{ }^\circ\text{C}$ was discovered by Guan *et al.*¹⁰ The excellent properties of this catalyst can be ascribed to the facile formation of Rh–O–O–Ti superoxide easily reacting with the adsorbed CO species on TiO₂ sites.

Although these noble metals exhibit high activities for CO oxidation, the high cost and limited supply constrain their commercial applications.¹⁴ Thus attention has been focused on searching for “noble metal-free” catalysts with excellent catalytic properties.^{15–21} Co_3O_4 , one kind of the less-expensive alternatives to the noble metal-based catalysts, has been reported to be one of the most efficient catalysts for carbon monoxide oxidation due to its excellent CO adsorption strength, low barrier of CO reacting with lattice O, and remarkable redox properties.^{14,15,18,22} A pioneering work on Co_3O_4 for CO oxidation reported by Xie *et al.* revealed that the Co_3O_4 nanorods demonstrate a catalytic activity towards CO oxidation at a temperature of $-77\text{ }^\circ\text{C}$.²³ The superior performance of the catalyst can be attributed to the predominantly exposed (110) planes with richness of active Co^{3+} sites. A recent theoretical work found that Co^{3+} has a higher activity than Co^{2+} in the Co_3O_4 for CO oxidation because: (i) Co^{3+} binds CO molecule strongly compared to Co^{2+} , (ii) a high barrier exists between lattice O linked to Co^{2+} and CO adsorbed on Co^{2+} .²² Therefore, many works are focusing on preparing special nano-structural Co_3O_4 predominately exposing active faces with more Co^{3+} cations to enhance their catalytic activities for CO oxidation. However, these active faces still contain many Co^{2+} cations which have lower activities for CO oxidation.^{24–26} So, replacing the inactive Co^{2+} with other active divalent cations to prepare Co-based ternary metal oxides provides an efficient way to further enhance the catalytic performance of Co_3O_4 . On this point, Cu^{2+} can be a promising candidate for replacing Co^{2+} in the Co_3O_4 not only due to its high activities for CO oxidation, but also owing to the similar ionic radius with Co^{2+} which allows the easy formation of Co/Cu ternary metal oxides.^{27–29}

MOFs are a class of porous functional materials constructed by metal ions and bridging ligands.^{30–33} Owing to its adjustable

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cavities and flexible structures, various metal oxides with specific morphologies and interconnected pores have been fabricated by thermal decomposition of MOFs under suitable calcination conditions, expecting to improve their performance in specific applications.^{34–42} Among them, ternary metal oxides have gained increasing considerations due to the structure merits and synergetic effect of multiple components. Therefore, bimetallic organic frameworks are considered highly desirable to facilitate synthesis of the ternary metal oxides. However such effort is still scarce because of the challenge in morphology and composition control during the incorporation of different secondary metal nodes into MOFs.³⁹ Divalent metal formate frameworks (MFFs) of $[\text{CH}_3\text{NH}_3][\text{M}(\text{HCOO})_3]$ ($\text{M} = \text{Mn}, \text{Fe}, \text{Ni}, \text{Co}, \text{Zn}$) could be promising MOFs to tackle this challenge due to the same six-connected ($4^{12} \cdot 6^3$) nodes of the octahedral (MO_6) metal ions within the framework.⁴³ Herein, we propose a facial one-step synthesis of bimetallic formate frameworks $[\text{CH}_3\text{NH}_3][\text{M}(\text{HCOO})_3]$ ($\text{M} = \text{Co}/\text{Cu}$) (Co/Cu-MFFs) and its derivation of ternary oxides $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ ($x = 0, 0.5, 1, 1.5$) microcubes. The $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes are constructed by numerous interconnected nanoparticles with uniform distribution of cobalt and copper species. In addition, the Cu/Co atomic ratio can be controlled exactly through adjusting the compositions of the growth precursor solutions. Owing to its larger specific surface area, stronger reducibility and the synergistic effect of two metal oxide components, the mesoporous $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ with moderate Cu/Co atomic ratio exhibit better performance for CO oxidation reaction than pure Co_3O_4 .

2. Experimental

2.1. Synthesis of Co/Cu-MFFs precursors

25 mL of ethanol was mixed with 12 mmol HCOOH, 8 mmol CH_3NH_2 (30–33% in methanol) and 0.5 g polyvinylpyrrolidone (PVP K-30) to get a colorless solution. Then a transparent solution containing 1 mmol mixed salts with different Cu/Co atomic ratios (0, 1 : 5, 1 : 2, 1 : 1) and 0.5 g PVP K-30 were dropped into the above solution in 10 minutes to obtain a pink colloidal suspension. The whole reaction process was maintained at room temperature with magnetic stirring. One hour later, the colloidal suspension was aged for one day at ambient temperature without any interruption. The resulting pink precipitates were centrifuged and washed several times with ethanol, finally dried at 60 °C for 6 hours in a vacuum oven and noted as $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$, $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/6}\text{Co}_{5/6}(\text{HCOO})_3]$, $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$, $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/2}\text{Co}_{1/2}(\text{HCOO})_3]$ respectively.

2.2. Synthesis of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ ($x = 0, 0.5, 1, 1.5$) microcubes

The porous ternary metal oxides were fabricated in muffle burner by annealing these prepared Co/Cu-MFFs precursors at 350 °C for 2 hours, at a heating rate of 1 °C min^{-1} and noted as Co_3O_4 , $\text{Cu}_{0.5}\text{Co}_{2.5}\text{O}_4$, CuCo_2O_4 , $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$, respectively.

2.3. Characterizations

Powder XRD patterns were recorded on a Bruker D8 advance diffractometer with Cu K_α radiation over the 2θ range of 10–80°.

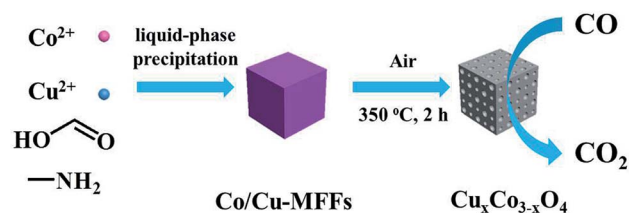
Thermogravimetric analyses (TGA) were carried out in a Netzsch SDT449F3 thermal analyzer in air atmosphere with a heating rate of 5 °C min^{-1} . The SEM and TEM images of the prepared samples were obtained through field emission scanning electron microscopy (FESEM, Hitachi S-4800 microscope) and transmission electron microscopy (TEM, JEOL, JEM-2100F). The chemical composition and elemental distribution of the prepared catalysts were examined by Energy-dispersive X-ray spectroscopy (EDX) attached to the FESEM instrument. ICP-OES was used to determine the Cu/Co atomic ratio of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$. The X-ray photoelectron spectroscopy (XPS) spectra were collected on Thermo ESCALAB 250 Xi spectrometer. N_2 adsorption-desorption isotherm were obtained by a Micromeritics ASAP 2020 analyzer at 77 K. H_2 -temperature-programmed reduction (H_2 -TPR) experiments were performed under a 10 vol% H_2/Ar mixture with a flow rate of 50 mL min^{-1} over 60 mg of catalyst by a Micromeritics Chemisorb 2920 apparatus and the temperature was increased from ambient temperature to 800 °C at a ramp rate of 1 °C min^{-1} . Prior to each analysis, the catalysts were purged in a flow of pure argon at 200 °C for 2 hours to remove traces water.

2.4. Catalytic performance measurements

The catalytic tests of the $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes for CO oxidation reaction were performed in a fixed quartz tubular reactor. The reactor was charged with 50 mg of the catalysts without pretreatment. The reaction temperature was detected by a thermocouple under catalyst bed. The mixed feed gas consisted of 1 vol% CO, 20 vol% O_2 , 79 vol% N_2 was passed through the reactor at a flow rate of 50 mL min^{-1} , corresponding to a gas hourly space velocity (GHSV) of 60 000 mL $\text{g}^{-1} \text{h}^{-1}$. The components of the gas were examined by a gas chromatograph (Agilent GC7890). Two catalytic test data points at each temperature were collected and the average values of them were reported.

3. Results and discussion

The synthesis process of mesoporous $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes is shown in Scheme 1. Firstly, the Co/Cu-MFFs precursors with different Cu/Co atomic ratios were synthesized through a one-step liquid-phase precipitation method under room temperature. Then, the $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes with porous structure were obtained through thermal decomposition of the precursors under air. The phase and purity of the Co/Cu-MFFs precursors and $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ were examined by PXRD (Fig. 1a). All strong peaks in the XRD patterns of each Co/Cu-MFFs



Scheme 1 Schematic illustration of the synthesis of Co/Cu-MFFs precursors and its derived mesoporous $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes for CO oxidation reaction.



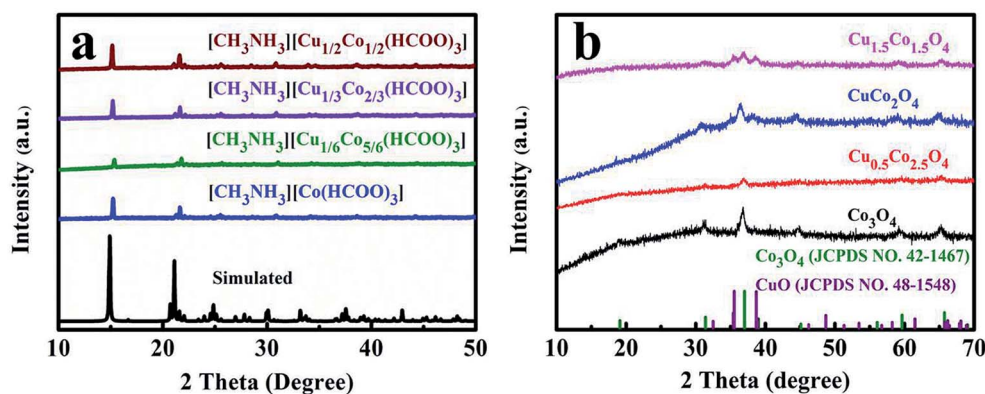


Fig. 1 XRD patterns of Co/Cu-MFFs precursors (a) and $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes (b).

precursor are well matched with the simulated single crystal structure of $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$ according to the reported crystal structure data,^{44,45} suggesting the successful incorporation of Cu^{2+} into Co/Cu-MFFs. Fig. S1† shows the TGA curves of as-prepared precursors, indicating that the weight residual of all samples becomes constant when the temperature rises to 300 °C. During the calcination, all samples exhibit similar two-step weight loss. The first weight loss could be related to the removal of amine and one formate molecule per formula unit. The second weight loss could be due to the decomposition of residual organic components. Fig. 1b shows that the corresponding diffraction profiles of prepared ternary oxides $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ are in agreement with the standard CuCo_2O_4 (JCPDS no. 01-1155) or pure Co_3O_4 (JCPDS no. 42-1467). CuCo_2O_4 can be treated as Co_3O_4 with Co^{2+} replaced by Cu^{2+} and therefore these two oxides have almost the same XRD patterns. Meanwhile, two weak peaks corresponding to CuO (002), (111) (JCPDS no. 48-1548) can be seen in the XRD patterns of CuCo_2O_4 and $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$, suggesting that a few Cu^{2+} cations did not enter into the lattice of Co_3O_4 successfully. These two peaks become obvious with the increase of Cu-doping amount, indicating that the excess amounts of Cu^{2+} cations in the Co/Cu-MFFs precursors lead to a significant phase segregation of the oxides.

The SEM images in Fig. S2a and S2b† reveal that the as-prepared $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$ and $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$ have similar cubic shapes with smooth surfaces and some macropores about 0.6 μm can be observed clearly on the partial surfaces of these two precursors. Meanwhile, the size of $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$ microcubes is about 1–2 μm , which is smaller than that of $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$, mainly about 2–3 μm . We can infer accordingly that the introduced Cu^{2+} does not have great influences on the morphology of precursors. In order to study the effect of PVP K-30 in the preparation of Co/Cu-MFFs precursors, the morphology of $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$ prepared in the absence of PVP K-30 was also characterized. As shown in Fig. S3,† the $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$ without adding PVP K-30 still retains the cubic morphology but many microbes agglomerate together. So we can infer that PVP K-30 functions here mainly as a stabilizing agent to prevent agglomeration of the microcubes. The similar functions have been reported by many other reports.^{46,47} The

SEM images of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ easily prepared by annealing precursors are shown in Fig. 2a–d. The cubic morphology of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ reveals that all the $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ almost preserved the original cubic morphology of as-prepared precursors. Meanwhile, a great number of small nanoparticles on the rough surface of cubic $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ can be seen clearly in the SEM images, which confirms the successful formation of porous structure. The chemical composition and elemental distribution of the microcubes were further characterized by SEM-EDX. The elemental mapping images (Fig. 2e and S4†) further confirm that all the ternary metal oxides are with similar microcubic morphologies and the uniform distribution of O, Cu and Co. The metal element ratios of Cu and Co in the oxides are similar with those ratios in the growth precursor solution as shown in Table S1 and Fig. S5,† which shows that the compositions of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ can be controlled exactly by adjusting the synthesis of $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$. The high-resolution TEM image of CuCo_2O_4 microcube is shown in Fig. 2f, the interplanar distances of 0.23 nm can be indexed to the (111) plane of CuO , whereas the interplanar distance of 0.24 nm is correspondence to the (311) plane of CuCo_2O_4 . The interlaced boundaries marked with white circle demonstrate the high interdispersion of the CuO and CuCo_2O_4 .

Some related mechanisms at the molecular level of Co_3O_4 for CO oxidation suggest that gas phase CO chemisorbs preferably on the exposed Co^{3+} , then reacts with an oxygen atom linked to the active Co^{3+} site resulting in CO_2 and an oxygen vacancy formation.^{24,48} Therefore, the amount of the exposed Co^{3+} cations on the Co_3O_4 surfaces is responsible for catalytic activity.⁴⁹ Herein, the XPS analysis was further carried out to examine the surface chemical compositions and elemental states of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes. The $\text{Co}2\text{p}$ XPS spectra profiles (Fig. 3a) constructed with two main peaks centering at about 779.5 and 794.6 eV, corresponding to the $\text{Co}2\text{p}_{3/2}$ and $\text{Co}2\text{p}_{1/2}$ respectively.^{37,50,51} The relative percentage of Co^{3+} and Co^{2+} was calculated through the fitted curves of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$, and was plotted as functions of the Cu/Co atomic ratio in the solution of preparing precursors (Fig. 3b). We can find that the ratio of $\text{Co}^{2+}/\text{Co}^{3+}$ on the surface of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ first drastically decreases and then almost remains unchanged with the increasing Cu/Co atomic ratio. That decline of $\text{Co}^{2+}/\text{Co}^{3+}$ atomic



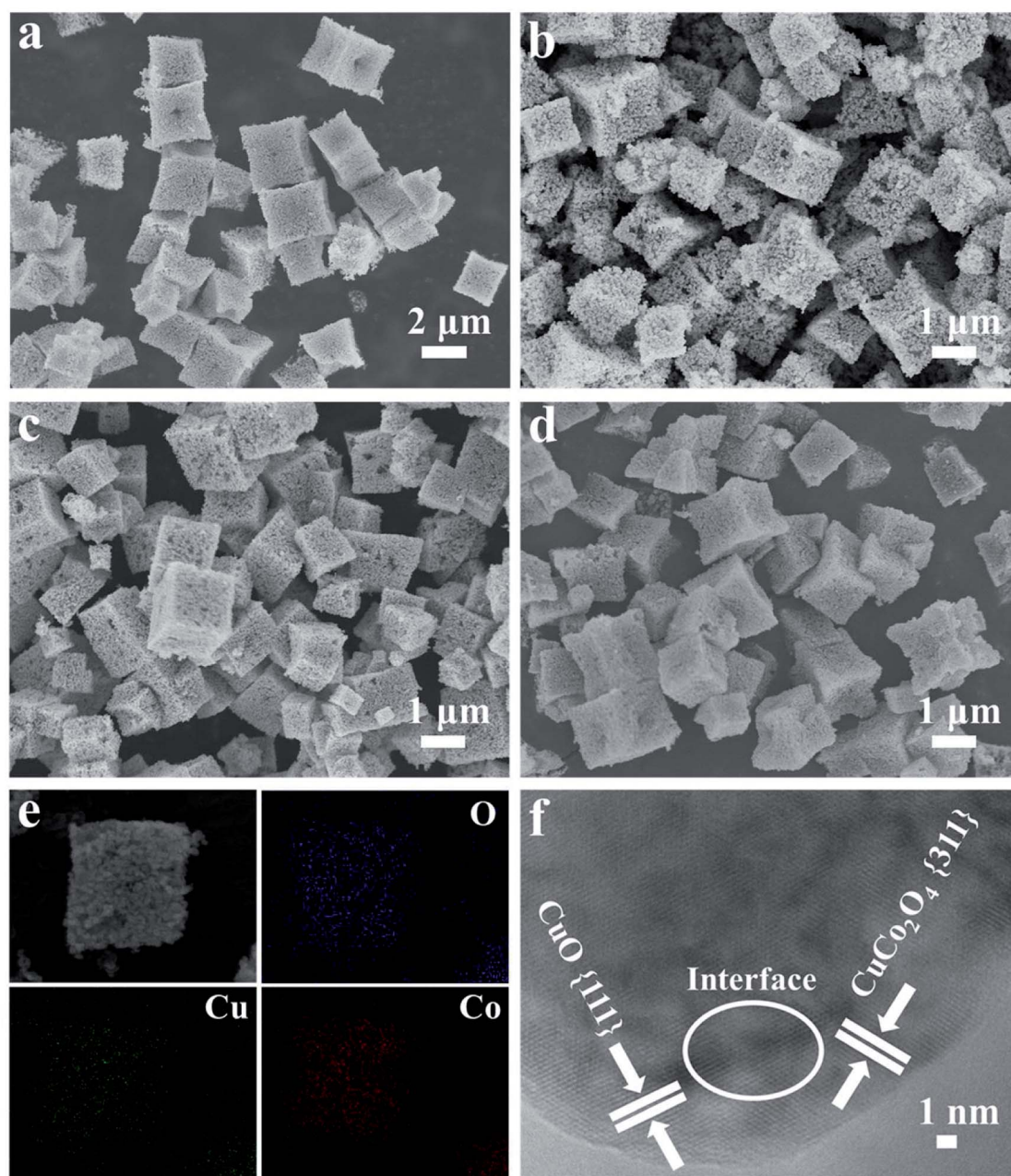


Fig. 2 SEM images of Co_3O_4 (a), $\text{Cu}_{0.5}\text{Co}_{2.5}\text{O}_4$ (b), CuCo_2O_4 (c), $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$ (d), SEM-EDX mapping images of CuCo_2O_4 (e), TEM images of CuCo_2O_4 (f).

ratio should be originated from the Cu^{2+} substitution for Co^{2+} in $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$. The further steadiness might be ascribed to many Cu^{2+} leading to the formation of CuO rather than substitution for Co^{2+} , which can also be inferred from the XRD results.

The porous structures of Co/Cu-MFFs derived CuCo_2O_4 and pure Co_3O_4 were further examined by measuring sorption isotherms of nitrogen at 77 K. It can be observed in Fig. 4a that both of the oxides present a type-IV adsorption isotherm with a significant hysteresis loop, denoting that they are mesoporous solids. The specific surface areas of Co_3O_4 and CuCo_2O_4 microcubes were calculated to be 25.59 and 29.47 m^2 g^{-1} through Brunauer-Emmett-Teller (BET) method. In addition,

the corresponding Barrett-Joyner-Halenda (BJH) pore size distribution plots (Fig. S6[†]) show the main pore size distribution of Co_3O_4 and CuCo_2O_4 are 0.71 – 1.58 nm and 16.15 – 20.73 nm, respectively.

To directly evaluate the catalytic performance of the Co/Cu-MFFs derived ternary oxides for CO oxidation reaction, 50 mg of the mesoporous $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes without any pre-treatments were put into a fixed quartz glass reactor respectively. As shown in Fig. 4b, with the increasing amount of Cu/Co atomic ratio in the catalysts, the catalytic activities of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ for CO oxidation reaction firstly increase and then decrease. Among them, CuCo_2O_4 exhibits the highest activity



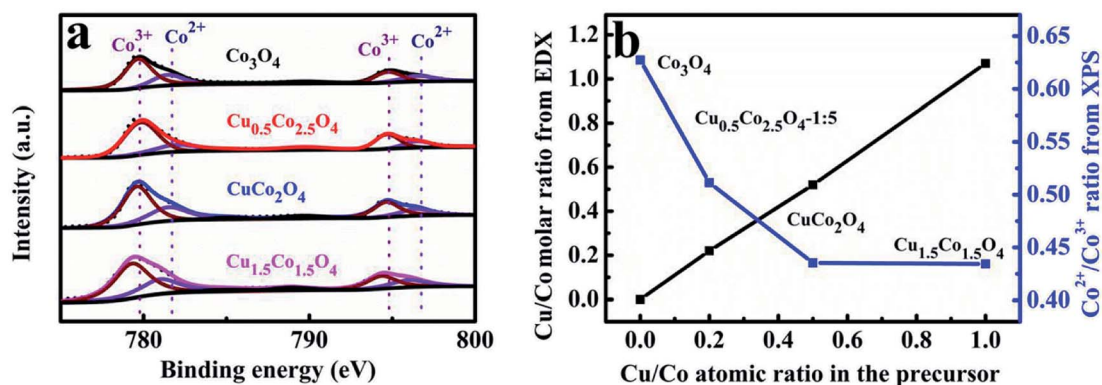


Fig. 3 XPS spectra of the $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes (a), the measured Cu/Co atomic ratio and $\text{Co}^{2+}/\text{Co}^{3+}$ atomic ratio on the surface of the $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes as functions of the Cu/Co atomic ratio in the solution of preparing precursors (b).

with 100% CO conversion rate at 120 °C, superior or comparable to other transition oxides as CO oxidation catalysts (Table S2†). These results indicate that using more active Cu^{2+} to replace the inactive Co^{2+} in the lattice of Co_3O_4 could be a novel way to enhance the catalytic performance for CO oxidation. Meanwhile, the $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$ has the lowest activity and the temperature of CO complete conversion is as high as 170 °C, which might be due to the richness of less-active CuO phase. The CO oxidation conversions of without materials and with 50 mg of precursors performed under different temperatures were shown

in Fig. S7,† the results indicated that there was no catalytic activity in the absence of catalyst and the Co/Cu-MFFs exhibited extremely low catalytic activity of CO oxidation. We also investigated the stabilities of pure Co_3O_4 and CuCo_2O_4 under the similar conditions at 140 and 130 °C, respectively (Fig. 4c). Both samples exhibit good stable performance that retains CO complete conversion within 30 hours. Based on these results, we can infer that the enhanced catalytic activity of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ can be attributed to the structure and component merits achieved through the incorporation of new secondary copper nodes

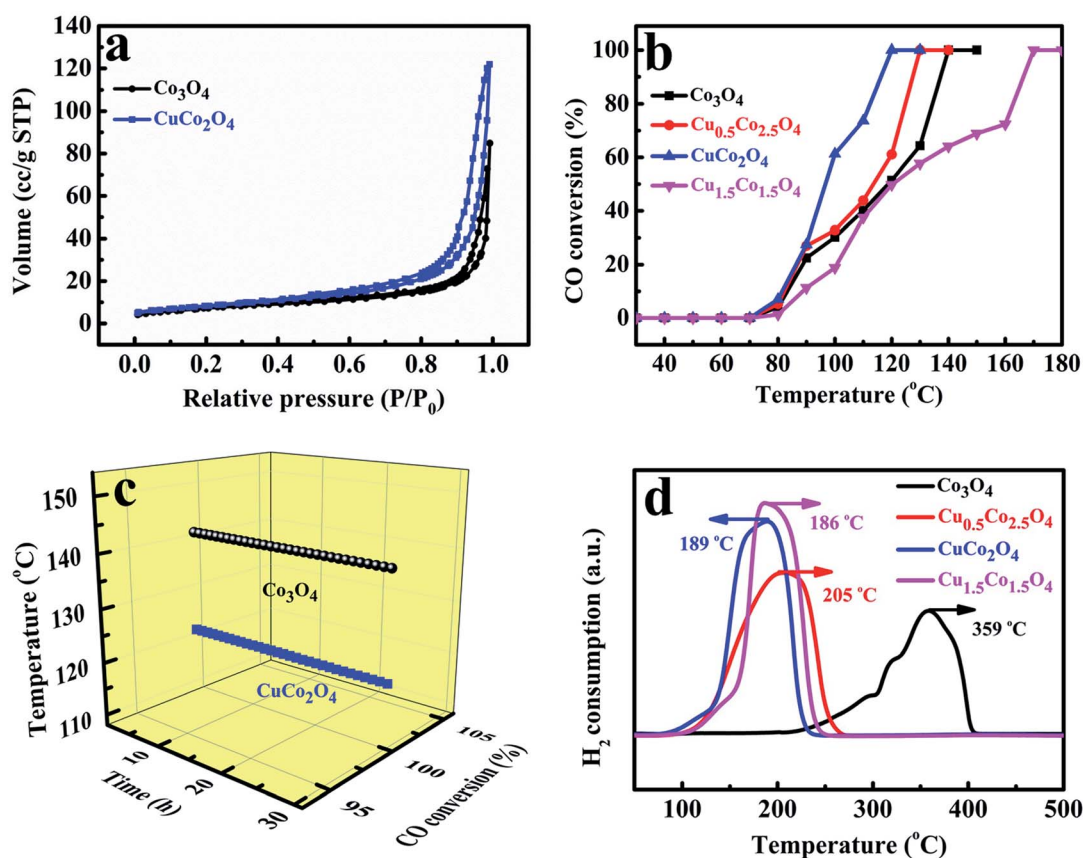


Fig. 4 Nitrogen adsorption–desorption isotherms of Co_3O_4 and CuCo_2O_4 (a), the catalytic activities of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ for CO oxidation (b), stability of Co_3O_4 at 140 °C and CuCo_2O_4 at 120 °C (c), H_2 -TPR profiles of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ (d).



in the Co/Cu-MFFs precursors. In addition, pure Co_3O_4 presents a good activity for CO oxidation with a CO complete conversion temperature of 140 °C, which is 30 °C lower than that reported by Zhang *et al.*⁵² The higher catalytic activity might be ascribed to the larger specific surface area and the lower inactive Co^{2+} concentration in the surface of Co_3O_4 according to the BET and XPS results (Table S3†).⁵²

To further investigate the synergetic effects of Cu and Co species, the temperature-programmed reductions were performed using a stream of diluted H_2 (H_2/Ar_2 , 1 : 9 v/v). As shown in Fig. 4d, only a single peak at 359 °C is observed in pure Co_3O_4 microcubes reduction profile, which can be explained by the direct reduction of cobalt ions into metallic Co in one step for the large particles of Co_3O_4 .⁵³ With the amount of Cu^{2+} increasing in catalysts, the prominent peaks of $\text{Cu}_{0.5}\text{Co}_{2.5}\text{O}_4$, CuCo_2O_4 and $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$ shift towards lower temperature to 205, 189 and 186 °C, respectively, which means that the reducibility of the catalysts was markedly promoted when the Cu/Co atomic ratio increased. Such enhanced reduction may be attributed to the strong Co–Cu interaction originated from the intimate contact and the good interdispersion of the CuO and Co_3O_4 , which possibly leads to a junction of their band levels in the solid solution or the mixed oxidations.⁵⁴ Such strong interactions also have been found for copper–zinc chromite catalysts and CuO–ZnO system.^{55,56}

4. Conclusion

In this work, we have proposed a novel and simple method to prepare Co-based ternary metal oxides $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ with cube-like morphology and studied the effect of replacing Co^{2+} with Cu^{2+} on the catalytic activity of Co_3O_4 towards CO oxidation. The $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ microcubes with controlled composition were prepared by one step pyrolysis of Co/Cu-MFFs, in which the Cu/Co atomic ratio can be tuned through adjusting the compositions of growth precursor solution. The obtained mesoporous $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ have enhanced catalytic properties for CO oxidation compared to the pure porous Co_3O_4 when the atomic ratio of Cu/Co is no more than 1/2 in the solution of preparing precursors. The larger specific surface areas and stronger reducibility resulted from the introduced new secondary Cu metal nodes into Co/Cu-MFFs which may play important roles in improving catalytic performance. We believe that the synthetic strategy can also be extended to obtain other ternary metal oxides with different structures by controlling the morphology and the compositions of the bimetal-formate frameworks, which might have a higher catalytic performance or exhibit excellent properties in other applications.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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References

- H.-J. Freund, G. Meijer, M. Scheffler, R. Schlögl and M. Wolf, *Angew. Chem., Int. Ed.*, 2011, **50**, 10064–10094.
- M. Haruta, S. Tsubota, T. Kobayashi, H. Kageyama, M. J. Genet and B. Delmon, *J. Catal.*, 1993, **144**, 175–192.
- J.-C. Ding, H.-Y. Li, T.-C. Cao, Z.-X. Cai, X.-X. Wang and X. Guo, *Solid State Ionics*, 2017, **303**, 97–102.
- K. M. Adams and G. W. Graham, *Appl. Catal., B*, 2008, **80**, 343–352.
- P. Landon, J. Ferguson, B. E. Solsona, T. Garcia, A. F. Carley, A. A. Herzing, C. J. Kiely, S. E. Golunski and G. J. Hutchings, *Chem. Commun.*, 2005, 3385–3387.
- J. Lin, X. Wang and T. Zhang, *Chin. J. Catal.*, 2016, **37**, 1805–1813.
- B. Liu, Y. Liu, H. Hou, Y. Liu, Q. Wang and J. Zhang, *Catal. Sci. Technol.*, 2015, **5**, 5139–5152.
- L. W. Guo, P. P. Du, X. P. Fu, C. Ma, J. Zeng, R. Si, Y. Y. Huang, C. J. Jia, Y. W. Zhang and C. H. Yan, *Nat. Commun.*, 2016, **7**, 13481.
- B. Qiao, J. Lin, A. Wang, Y. Chen, T. Zhang and J. Liu, *Chin. J. Catal.*, 2015, **36**, 1505–1511.
- H. Guan, J. Lin, B. Qiao, X. Yang, L. Li, S. Miao, J. Liu, A. Wang, X. Wang and T. Zhang, *Angew. Chem., Int. Ed.*, 2016, **55**, 2820–2824.
- H. Guan, J. Lin, L. Li, X. Wang and T. Zhang, *Appl. Catal., B*, 2016, **184**, 299–308.
- I. Langmuir, *Trans. Faraday Soc.*, 1992, **17**, 621–654.
- M. Haruta, N. Yamada, T. Kobayashi and S. Iijima, *J. Catal.*, 1989, **115**, 301–309.
- L. F. Liotta, H. Wu, G. Pantaleo and A. M. Venezia, *Catal. Sci. Technol.*, 2013, **3**, 3085–3102.
- X. Wang, W. Zhong and Y. Li, *Catal. Sci. Technol.*, 2015, **5**, 1014–1020.
- Z. Zhao, X. Lin, R. Jin, G. Wang and T. Muhammad, *Appl. Catal., B*, 2015, **115–116**, 53–62.
- Y. Su, Z. Tang, W. Han, Y. Song and G. Lu, *Catal. Surv. Asia*, 2015, **19**, 68–77.
- C. J. Jia, M. Schwickardi, C. Weidenthaler, W. Schmidt, S. Korhonen, B. M. Weckhuysen and F. Schuth, *J. Am. Chem. Soc.*, 2011, **133**, 11279–11288.
- A. Biabani-Ravandi and M. Rezaei, *Chem. Eng. J.*, 2012, **184**, 141–146.
- T. Cwele, N. Mahadevaiah, S. Singh and H. B. Friedrich, *Appl. Catal., B*, 2016, **182**, 1–14.
- Y. Yu, T. Takei, H. Ohashi, H. He, X. Zhang and M. Haruta, *J. Catal.*, 2009, **267**, 121–128.
- H.-F. Wang, R. Kavanagh, Y.-L. Guo, Y. Guo, G. Lu and P. Hu, *J. Catal.*, 2012, **296**, 110–119.
- X. Xie, Y. Li, Z. Q. Liu, M. Haruta and W. Shen, *Nature*, 2009, **458**, 746–749.
- J. Jansson, A. E. C. Palmqvist, E. Fridell, M. Skoglundh, L. Österlund, P. Thormählen and V. Langer, *J. Catal.*, 2002, **211**, 387–397.
- P. Broqvist, I. Panas and H. Persson, *J. Catal.*, 2002, **210**, 198–206.



- 26 F. Grillo, M. M. Natile and A. Glisenti, *Appl. Catal., B*, 2004, **48**, 267–274.
- 27 M. Y. Guo, F. Liu, J. Tsui, A. A. Voskanyan, A. M. C. Ng, A. B. Djurišić, W. K. Chan, K.-Y. Chan, C. Liao, K. Shih and C. Surya, *J. Mater. Chem. A*, 2015, **3**, 3627–3632.
- 28 R. Zhang, L. Hu, S. Bao, R. Li, L. Gao, R. Li and Q. Chen, *J. Mater. Chem. A*, 2016, **4**, 8412–8420.
- 29 M. Zhou, L. Cai, M. Bajdich, M. García-Melchor, H. Li, J. He, J. Wilcox, W. Wu, A. Vojvodic and X. Zheng, *ACS Catal.*, 2015, **5**, 4485–4491.
- 30 E. A. Dolgoplova, A. J. Brandt, O. A. Ejegbavwo, A. S. Duke, T. D. Maddumapatabandi, R. P. Galhenage, B. W. Larson, O. G. Reid, S. C. Ammal, A. Heyden, M. Chandrashekar, V. Stavila, D. A. Chen and N. B. Shustova, *J. Am. Chem. Soc.*, 2017, **139**, 5201–5209.
- 31 L. Chen, R. Luque and Y. Li, *Chem. Soc. Rev.*, 2017, **46**, 4614–4630.
- 32 X. Yang and Q. Xu, *Cryst. Growth Des.*, 2017, **17**, 1450–1455.
- 33 L. Zhu, X. Q. Liu, H. L. Jiang and L. B. Sun, *Chem. Rev.*, 2017, **117**, 8129–8176.
- 34 F. Wang, X. Wang, D. Liu, J. Zhen, J. Li, Y. Wang and H. Zhang, *ACS Appl. Mater. Interfaces*, 2017, **6**, 22216–22223.
- 35 Y. Zhu, C. Cao, J. Zhang and X. Xu, *J. Mater. Chem. A*, 2015, **3**, 9556–9564.
- 36 L. Shen, L. Yu, X.-Y. Yu, X. Zhang and X. W. D. Lou, *Angew. Chem., Int. Ed.*, 2015, **54**, 1868–1872.
- 37 J. Wei, Y. Feng, Y. Liu and Y. Ding, *J. Mater. Chem. A*, 2015, **3**, 22300–22310.
- 38 L. Han, X.-Y. Yu and X. W. D. Lou, *Adv. Mater.*, 2016, **28**, 4601–4605.
- 39 H. Li, M. Liang, W. Sun and Y. Wang, *Adv. Funct. Mater.*, 2016, **26**, 1098–1103.
- 40 R. R. Salunkhe, Y. V. Kaneti and Y. Yamauchi, *ACS Nano*, 2017, **11**, 5293–5308.
- 41 Z. Yu, Y. Bai, Y. Liu, S. Zhang, D. Chen, N. Zhang and K. Sun, *ACS Appl. Mater. Interfaces*, 2017, **9**, 31777–31785.
- 42 S. Zheng, X. Li, B. Yan, Q. Hu, Y. Xu, X. Xiao, H. Xue and H. Pang, *Adv. Energy Mater.*, 2017, **7**, 1602733.
- 43 Z. Wang, K. Hu, S. Gao and H. Kobayashi, *Adv. Mater.*, 2010, **22**, 1526–1533.
- 44 L. C. Gomez-Aguirre, B. Pato-Doldan, J. Mira, S. Castro-Garcia, M. A. Senaris-Rodriguez, M. Sanchez-Andujar, J. Singleton and V. S. Zapf, *J. Am. Chem. Soc.*, 2016, **138**, 1122–1125.
- 45 B. Pato-Doldan, L. C. Gomez-Aguirre, A. P. Hansen, J. Mira, S. Castro-Garcia, M. Sanchez-Andujar, M. A. Senaris-Rodriguez, V. S. Zapf and J. Singleton, *J. Mater. Chem. C*, 2016, **4**, 11164–11172.
- 46 X. Huang and N. Zheng, *J. Am. Chem. Soc.*, 2009, **131**, 4602–4603.
- 47 J. Yin, J. Wang, M. Li, C. Jin and T. Zhang, *Chem. Mater.*, 2012, **24**, 2645–2654.
- 48 Y. Xie, F. Dong, S. Heinbuch, J. J. Rocca and E. R. Bernstein, *Phys. Chem. Chem. Phys.*, 2010, **12**, 947–959.
- 49 A. Alvarez, S. Ivanova, M. A. Centeno and J. A. Odriozola, *Appl. Catal., A*, 2012, **431–432**, 9–17.
- 50 G. Li, L. Li, Y. Li and J. Shi, *New J. Chem.*, 2015, **39**, 1742–1748.
- 51 J. Zhu and Q. Gao, *Microporous Mesoporous Mater.*, 2009, **124**, 144–152.
- 52 C. Zhang, L. Zhang, G.-C. Xu, X. Ma, Y.-H. Li, C.-Y. Zhang and D.-Z. Jia, *New J. Chem.*, 2017, **41**, 1631–1636.
- 53 J.-Y. Luo, M. Meng, X. Li, X.-G. Li, Y.-Q. Zha, T.-D. Hu, Y.-N. Xie and J. Zhang, *J. Catal.*, 2008, **254**, 310–324.
- 54 G. Fierro, M. Lo Jacono, M. Inversi, R. Dragone and P. Porta, *Top. Catal.*, 2000, **10**, 39–48.
- 55 G. L. Castiglioni, A. Vaccari, G. Fierro, M. Inversi, M. Lo Jacono, G. Minelli, I. Pettiti, P. Porta and M. Gazzano, *Appl. Catal., A*, 1995, **123**, 123–144.
- 56 G. Fierro, M. Lo Jacono, M. Inversi, P. Porta, F. Cioci and R. Lavecchia, *Appl. Catal., A*, 1996, **137**, 327–348.

