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# Co/Cu-MFF derived mesoporous ternary metal oxide microcubes for enhancing the catalytic activity of the CO oxidation reaction†

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Metal–organic framework (MOF)-based derivatives with uniform micro/mesoporous structures have attracted a great deal of interest in various research fields. Herein, we report a simple strategy to design functional mesoporous ternary metal oxides with controlled composition through direct pyrolysis of Co/Cu bimetal-formate frameworks (Co/Cu-MFFs), which were prepared by a facile one-step liquid-phase precipitation method, exhibiting uniform distribution of two different metal species and good structural integrity. The obtained mesoporous ternary metal oxide  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  ( $x = 0.5, 1$ ) microcubes exhibit much better performance for CO oxidation than pure  $\text{Co}_3\text{O}_4$ , which can be mainly attributed to their larger specific surface areas, stronger reducibility, and the synergistic effect of two active metal oxide components.

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## 1. Introduction

CO oxidation over solid catalysts has been extensively studied, not only with regard to its value as a classical probe reaction for fundamental studies but also due to its great importance in practical applications, such as air cleanup, gas sensors for detection, automotive exhaust gas treatment and CO elimination from the hydrogen feed for proton-exchange membrane fuel cells.<sup>1–5</sup> It has been reported that noble metals such as Pt, Au, and Rh are excellent CO oxidation catalysts.<sup>2,6–11</sup> Platinum group metals (PGMs) are some of the earliest catalysts and are still widely employed in automotive emission control and cleaning of gas originating from the petrochemical industry since Langmuir's pioneering work.<sup>6,7,12</sup> Haruta *et al.* discovered that oxide-supported Au catalysts prepared through a wet chemistry method exhibit an outstanding high activity for CO oxidation even at cryogenic temperatures.<sup>13</sup> Recently, a sub-nano Rh/TiO<sub>2</sub> catalyst with an unexpectedly high performance of total CO conversion at  $-50^\circ\text{C}$  was discovered by Guan *et al.*<sup>10</sup> The excellent properties of this catalyst can be ascribed to the facile formation of Rh–O–O–Ti superoxide easily reacting with the adsorbed CO species on TiO<sub>2</sub> sites.

Although these noble metals exhibit high activities for CO oxidation, the high cost and limited supply constrain their commercial applications.<sup>14</sup> Thus attention has been focused on searching for “noble metal-free” catalysts with excellent catalytic properties.<sup>15–21</sup>  $\text{Co}_3\text{O}_4$ , one kind of the less-expensive alternatives to the noble metal-based catalysts, has been reported to be one of the most efficient catalysts for carbon monoxide oxidation due to its excellent CO adsorption strength, low barrier of CO reacting with lattice O, and remarkable redox properties.<sup>14,15,18,22</sup> A pioneering work on  $\text{Co}_3\text{O}_4$  for CO oxidation reported by Xie *et al.* revealed that the  $\text{Co}_3\text{O}_4$  nanorods demonstrate a catalytic activity towards CO oxidation at a temperature of  $-77^\circ\text{C}$ .<sup>23</sup> The superior performance of the catalyst can be attributed to the predominantly exposed (110) planes with richness of active  $\text{Co}^{3+}$  sites. A recent theoretical work found that  $\text{Co}^{3+}$  has a higher activity than  $\text{Co}^{2+}$  in the  $\text{Co}_3\text{O}_4$  for CO oxidation because: (i)  $\text{Co}^{3+}$  binds CO molecule strongly compared to  $\text{Co}^{2+}$ , (ii) a high barrier exists between lattice O linked to  $\text{Co}^{2+}$  and CO adsorbed on  $\text{Co}^{2+}$ .<sup>22</sup> Therefore, many works are focusing on preparing special nano-structural  $\text{Co}_3\text{O}_4$  predominately exposing active faces with more  $\text{Co}^{3+}$  cations to enhance their catalytic activities for CO oxidation. However, these active faces still contain many  $\text{Co}^{2+}$  cations which have lower activities for CO oxidation.<sup>24–26</sup> So, replacing the inactive  $\text{Co}^{2+}$  with other active divalent cations to prepare Co-based ternary metal oxides provides an efficient way to further enhance the catalytic performance of  $\text{Co}_3\text{O}_4$ . On this point,  $\text{Cu}^{2+}$  can be a promising candidate for replacing  $\text{Co}^{2+}$  in the  $\text{Co}_3\text{O}_4$  not only due to its high activities for CO oxidation, but also owing to the similar ionic radius with  $\text{Co}^{2+}$  which allows the easy formation of Co/Cu ternary metal oxides.<sup>27–29</sup>

MOFs are a class of porous functional materials constructed by metal ions and bridging ligands.<sup>30–33</sup> Owing to its adjustable

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cavities and flexible structures, various metal oxides with specific morphologies and interconnected pores have been fabricated by thermal decomposition of MOFs under suitable calcination conditions, expecting to improve their performance in specific applications.<sup>34–42</sup> Among them, ternary metal oxides have gained increasing considerations due to the structure merits and synergetic effect of multiple components. Therefore, bimetallic organic frameworks are considered highly desirable to facilitate synthesis of the ternary metal oxides. However such effort is still scarce because of the challenge in morphology and composition control during the incorporation of different secondary metal nodes into MOFs.<sup>39</sup> Divalent metal formate frameworks (MFFs) of  $[\text{CH}_3\text{NH}_3][\text{M}(\text{HCOO})_3]$  ( $\text{M} = \text{Mn}, \text{Fe}, \text{Ni}, \text{Co}, \text{Zn}$ ) could be promising MOFs to tackle this challenge due to the same six-connected ( $4^{12} \cdot 6^3$ ) nodes of the octahedral ( $\text{MO}_6$ ) metal ions within the framework.<sup>43</sup> Herein, we propose a facial one-step synthesis of bimetallic formate frameworks  $[\text{CH}_3\text{NH}_3][\text{M}(\text{HCOO})_3]$  ( $\text{M} = \text{Co}/\text{Cu}$ ) (Co/Cu-MFFs) and its derivation of ternary oxides  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  ( $x = 0, 0.5, 1, 1.5$ ) microcubes. The  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes are constructed by numerous interconnected nanoparticles with uniform distribution of cobalt and copper species. In addition, the Cu/Co atomic ratio can be controlled exactly through adjusting the compositions of the growth precursor solutions. Owing to its larger specific surface area, stronger reducibility and the synergistic effect of two metal oxide components, the mesoporous  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  with moderate Cu/Co atomic ratio exhibit better performance for CO oxidation reaction than pure  $\text{Co}_3\text{O}_4$ .

## 2. Experimental

### 2.1. Synthesis of Co/Cu-MFFs precursors

25 mL of ethanol was mixed with 12 mmol HCOOH, 8 mmol  $\text{CH}_3\text{NH}_2$  (30–33% in methanol) and 0.5 g polyvinylpyrrolidone (PVP K-30) to get a colorless solution. Then a transparent solution containing 1 mmol mixed salts with different Cu/Co atomic ratios (0, 1 : 5, 1 : 2, 1 : 1) and 0.5 g PVP K-30 were dropped into the above solution in 10 minutes to obtain a pink colloidal suspension. The whole reaction process was maintained at room temperature with magnetic stirring. One hour later, the colloidal suspension was aged for one day at ambient temperature without any interruption. The resulting pink precipitates were centrifuged and washed several times with ethanol, finally dried at 60 °C for 6 hours in a vacuum oven and noted as  $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$ ,  $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/6}\text{Co}_{5/6}(\text{HCOO})_3]$ ,  $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$ ,  $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/2}\text{Co}_{1/2}(\text{HCOO})_3]$  respectively.

### 2.2. Synthesis of $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ ( $x = 0, 0.5, 1, 1.5$ ) microcubes

The porous ternary metal oxides were fabricated in muffle burner by annealing these prepared Co/Cu-MFFs precursors at 350 °C for 2 hours, at a heating rate of 1 °C  $\text{min}^{-1}$  and noted as  $\text{Co}_3\text{O}_4$ ,  $\text{Cu}_{0.5}\text{Co}_{2.5}\text{O}_4$ ,  $\text{CuCo}_2\text{O}_4$ ,  $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$ , respectively.

### 2.3. Characterizations

Powder XRD patterns were recorded on a Bruker D8 advance diffractometer with  $\text{Cu K}_\alpha$  radiation over the  $2\theta$  range of 10–80°.

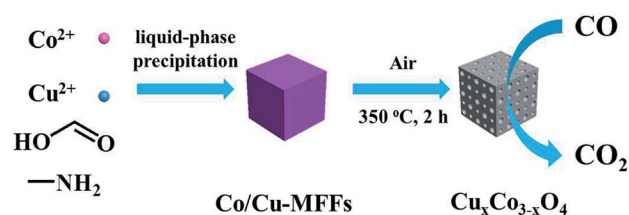
Thermogravimetric analyses (TGA) were carried out in a Netzsch SDT449F3 thermal analyzer in air atmosphere with a heating rate of 5 °C  $\text{min}^{-1}$ . The SEM and TEM images of the prepared samples were obtained through field emission scanning electron microscopy (FESEM, Hitachi S-4800 microscope) and transmission electron microscopy (TEM, JEOL, JEM-2100F). The chemical composition and elemental distribution of the prepared catalysts were examined by Energy-dispersive X-ray spectroscopy (EDX) attached to the FESEM instrument. ICP-OES was used to determine the Cu/Co atomic ratio of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ . The X-ray photoelectron spectroscopy (XPS) spectra were collected on Thermo ESCALAB 250 Xi spectrometer.  $\text{N}_2$  adsorption-desorption isotherm were obtained by a Micromeritics ASAP 2020 analyzer at 77 K.  $\text{H}_2$ -temperature-programmed reduction ( $\text{H}_2$ -TPR) experiments were performed under a 10 vol%  $\text{H}_2/\text{Ar}$  mixture with a flow rate of 50 mL  $\text{min}^{-1}$  over 60 mg of catalyst by a Micromeritics Chemisorb 2920 apparatus and the temperature was increased from ambient temperature to 800 °C at a ramp rate of 1 °C  $\text{min}^{-1}$ . Prior to each analysis, the catalysts were purged in a flow of pure argon at 200 °C for 2 hours to remove traces water.

### 2.4. Catalytic performance measurements

The catalytic tests of the  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes for CO oxidation reaction were performed in a fixed quartz tubular reactor. The reactor was charged with 50 mg of the catalysts without pretreatment. The reaction temperature was detected by a thermocouple under catalyst bed. The mixed feed gas consisted of 1 vol% CO, 20 vol%  $\text{O}_2$ , 79 vol%  $\text{N}_2$  was passed through the reactor at a flow rate of 50 mL  $\text{min}^{-1}$ , corresponding to a gas hourly space velocity (GHSV) of 60 000 mL  $\text{g}^{-1} \text{h}^{-1}$ . The components of the gas were examined by a gas chromatograph (Agilent GC7890). Two catalytic test data points at each temperature were collected and the average values of them were reported.

## 3. Results and discussion

The synthesis process of mesoporous  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes is shown in Scheme 1. Firstly, the Co/Cu-MFFs precursors with different Cu/Co atomic ratios were synthesized through a one-step liquid-phase precipitation method under room temperature. Then, the  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes with porous structure were obtained through thermal decomposition of the precursors under air. The phase and purity of the Co/Cu-MFFs precursors and  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  were examined by PXRD (Fig. 1a). All strong peaks in the XRD patterns of each Co/Cu-MFFs



Scheme 1 Schematic illustration of the synthesis of Co/Cu-MFFs precursors and its derived mesoporous  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes for CO oxidation reaction.



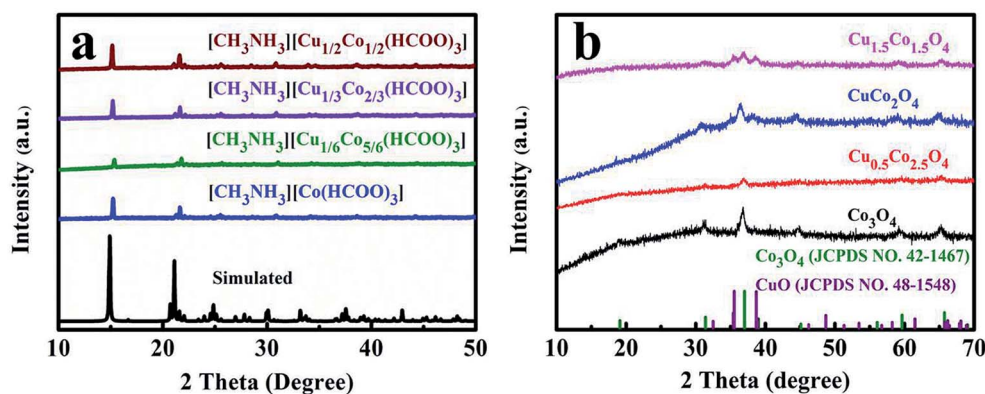


Fig. 1 XRD patterns of Co/Cu-MFFs precursors (a) and  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes (b).

precursor are well matched with the simulated single crystal structure of  $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$  according to the reported crystal structure data,<sup>44,45</sup> suggesting the successful incorporation of  $\text{Cu}^{2+}$  into Co/Cu-MFFs. Fig. S1† shows the TGA curves of as-prepared precursors, indicating that the weight residual of all samples becomes constant when the temperature rises to 300 °C. During the calcination, all samples exhibit similar two-step weight loss. The first weight loss could be related to the removal of amine and one formate molecule per formula unit. The second weight loss could be due to the decomposition of residual organic components. Fig. 1b shows that the corresponding diffraction profiles of prepared ternary oxides  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  are in agreement with the standard  $\text{CuCo}_2\text{O}_4$  (JCPDS no. 01-1155) or pure  $\text{Co}_3\text{O}_4$  (JCPDS no. 42-1467).  $\text{CuCo}_2\text{O}_4$  can be treated as  $\text{Co}_3\text{O}_4$  with  $\text{Co}^{2+}$  replaced by  $\text{Cu}^{2+}$  and therefore these two oxides have almost the same XRD patterns. Meanwhile, two weak peaks corresponding to  $\text{CuO}$  (002), (111) (JCPDS no. 48-1548) can be seen in the XRD patterns of  $\text{CuCo}_2\text{O}_4$  and  $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$ , suggesting that a few  $\text{Cu}^{2+}$  cations did not enter into the lattice of  $\text{Co}_3\text{O}_4$  successfully. These two peaks become obvious with the increase of Cu-doping amount, indicating that the excess amounts of  $\text{Cu}^{2+}$  cations in the Co/Cu-MFFs precursors lead to a significant phase segregation of the oxides.

The SEM images in Fig. S2a and S2b† reveal that the as-prepared  $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$  and  $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$  have similar cubic shapes with smooth surfaces and some macropores about 0.6  $\mu\text{m}$  can be observed clearly on the partial surfaces of these two precursors. Meanwhile, the size of  $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$  microcubes is about 1–2  $\mu\text{m}$ , which is smaller than that of  $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$ , mainly about 2–3  $\mu\text{m}$ . We can infer accordingly that the introduced  $\text{Cu}^{2+}$  does not have great influences on the morphology of precursors. In order to study the effect of PVP K-30 in the preparation of Co/Cu-MFFs precursors, the morphology of  $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$  prepared in the absence of PVP K-30 was also characterized. As shown in Fig. S3,† the  $[\text{CH}_3\text{NH}_3][\text{Co}(\text{HCOO})_3]$  without adding PVP K-30 still retains the cubic morphology but many microbes agglomerate together. So we can infer that PVP K-30 functions here mainly as a stabilizing agent to prevent agglomeration of the microcubes. The similar functions have been reported by many other reports.<sup>46,47</sup> The

SEM images of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  easily prepared by annealing precursors are shown in Fig. 2a–d. The cubic morphology of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  reveals that all the  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  almost preserved the original cubic morphology of as-prepared precursors. Meanwhile, a great number of small nanoparticles on the rough surface of cubic  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  can be seen clearly in the SEM images, which confirms the successful formation of porous structure. The chemical composition and elemental distribution of the microcubes were further characterized by SEM-EDX. The elemental mapping images (Fig. 2e and S4†) further confirm that all the ternary metal oxides are with similar microcubic morphologies and the uniform distribution of O, Cu and Co. The metal element ratios of Cu and Co in the oxides are similar with those ratios in the growth precursor solution as shown in Table S1 and Fig. S5,† which shows that the compositions of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  can be controlled exactly by adjusting the synthesis of  $[\text{CH}_3\text{NH}_3][\text{Cu}_{1/3}\text{Co}_{2/3}(\text{HCOO})_3]$ . The high-resolution TEM image of  $\text{CuCo}_2\text{O}_4$  microcube is shown in Fig. 2f, the interplanar distances of 0.23 nm can be indexed to the (111) plane of  $\text{CuO}$ , whereas the interplanar distance of 0.24 nm is correspondence to the (311) plane of  $\text{CuCo}_2\text{O}_4$ . The interlaced boundaries marked with white circle demonstrate the high interdispersion of the  $\text{CuO}$  and  $\text{CuCo}_2\text{O}_4$ .

Some related mechanisms at the molecular level of  $\text{Co}_3\text{O}_4$  for CO oxidation suggest that gas phase CO chemisorbs preferably on the exposed  $\text{Co}^{3+}$ , then reacts with an oxygen atom linked to the active  $\text{Co}^{3+}$  site resulting in  $\text{CO}_2$  and an oxygen vacancy formation.<sup>24,48</sup> Therefore, the amount of the exposed  $\text{Co}^{3+}$  cations on the  $\text{Co}_3\text{O}_4$  surfaces is responsible for catalytic activity.<sup>49</sup> Herein, the XPS analysis was further carried out to examine the surface chemical compositions and elemental states of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes. The  $\text{Co}2\text{p}$  XPS spectra profiles (Fig. 3a) constructed with two main peaks centering at about 779.5 and 794.6 eV, corresponding to the  $\text{Co}2\text{p}_{3/2}$  and  $\text{Co}2\text{p}_{1/2}$  respectively.<sup>37,50,51</sup> The relative percentage of  $\text{Co}^{3+}$  and  $\text{Co}^{2+}$  was calculated through the fitted curves of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ , and was plotted as functions of the Cu/Co atomic ratio in the solution of preparing precursors (Fig. 3b). We can find that the ratio of  $\text{Co}^{2+}/\text{Co}^{3+}$  on the surface of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  first drastically decreases and then almost remains unchanged with the increasing Cu/Co atomic ratio. That decline of  $\text{Co}^{2+}/\text{Co}^{3+}$  atomic



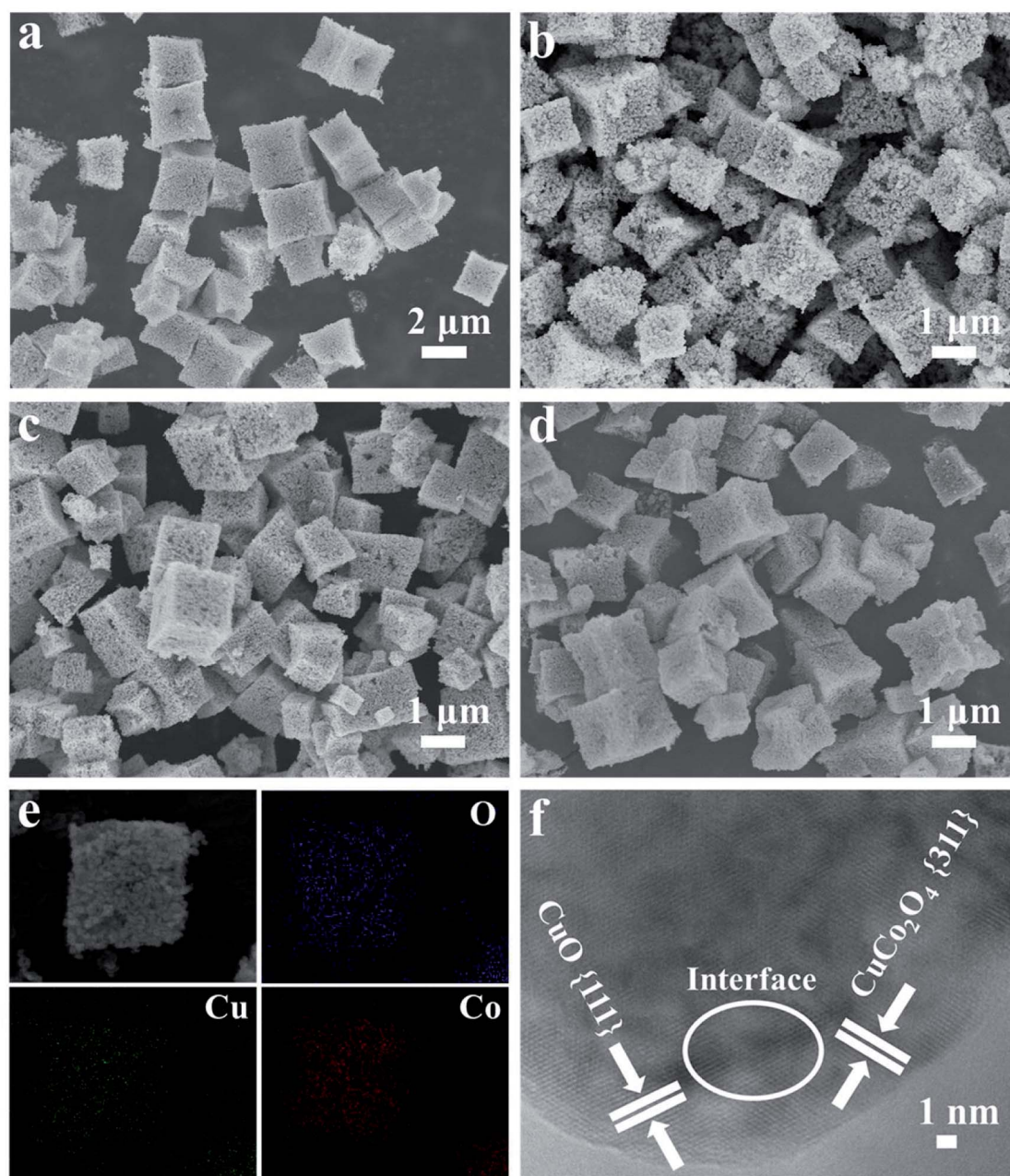


Fig. 2 SEM images of  $\text{Co}_3\text{O}_4$  (a),  $\text{Cu}_{0.5}\text{Co}_{2.5}\text{O}_4$  (b),  $\text{CuCo}_2\text{O}_4$  (c),  $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$  (d), SEM-EDX mapping images of  $\text{CuCo}_2\text{O}_4$  (e), TEM images of  $\text{CuCo}_2\text{O}_4$  (f).

ratio should be originated from the  $\text{Cu}^{2+}$  substitution for  $\text{Co}^{2+}$  in  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$ . The further steadiness might be ascribed to many  $\text{Cu}^{2+}$  leading to the formation of  $\text{CuO}$  rather than substitution for  $\text{Co}^{2+}$ , which can also be inferred from the XRD results.

The porous structures of Co/Cu-MFFs derived  $\text{CuCo}_2\text{O}_4$  and pure  $\text{Co}_3\text{O}_4$  were further examined by measuring sorption isotherms of nitrogen at 77 K. It can be observed in Fig. 4a that both of the oxides present a type-IV adsorption isotherm with a significant hysteresis loop, denoting that they are mesoporous solids. The specific surface areas of  $\text{Co}_3\text{O}_4$  and  $\text{CuCo}_2\text{O}_4$  microcubes were calculated to be  $25.59$  and  $29.47$   $\text{m}^2$   $\text{g}^{-1}$  through Brunauer-Emmett-Teller (BET) method. In addition,

the corresponding Barrett-Joyner-Halenda (BJH) pore size distribution plots (Fig. S6<sup>†</sup>) show the main pore size distribution of  $\text{Co}_3\text{O}_4$  and  $\text{CuCo}_2\text{O}_4$  are  $0.71$ – $1.58$  nm and  $16.15$ – $20.73$  nm, respectively.

To directly evaluate the catalytic performance of the Co/Cu-MFFs derived ternary oxides for CO oxidation reaction, 50 mg of the mesoporous  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes without any pre-treatments were put into a fixed quartz glass reactor respectively. As shown in Fig. 4b, with the increasing amount of Cu/Co atomic ratio in the catalysts, the catalytic activities of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  for CO oxidation reaction firstly increase and then decrease. Among them,  $\text{CuCo}_2\text{O}_4$  exhibits the highest activity



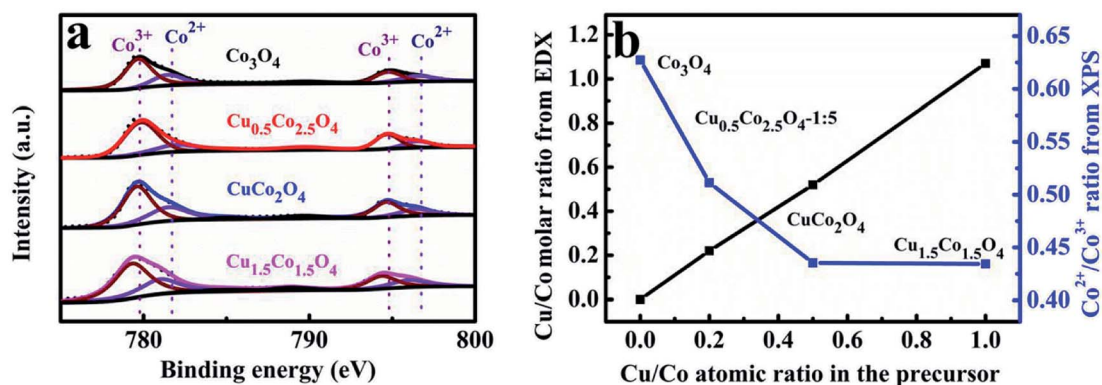


Fig. 3 XPS spectra of the  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes (a), the measured Cu/Co atomic ratio and  $\text{Co}^{2+}/\text{Co}^{3+}$  atomic ratio on the surface of the  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes as functions of the Cu/Co atomic ratio in the solution of preparing precursors (b).

with 100% CO conversion rate at 120 °C, superior or comparable to other transition oxides as CO oxidation catalysts (Table S2†). These results indicate that using more active  $\text{Cu}^{2+}$  to replace the inactive  $\text{Co}^{2+}$  in the lattice of  $\text{Co}_3\text{O}_4$  could be a novel way to enhance the catalytic performance for CO oxidation. Meanwhile, the  $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$  has the lowest activity and the temperature of CO complete conversion is as high as 170 °C, which might be due to the richness of less-active CuO phase. The CO oxidation conversions of without materials and with 50 mg of precursors performed under different temperatures were shown

in Fig. S7,† the results indicated that there was no catalytic activity in the absence of catalyst and the Co/Cu-MFFs exhibited extremely low catalytic activity of CO oxidation. We also investigated the stabilities of pure  $\text{Co}_3\text{O}_4$  and  $\text{CuCo}_2\text{O}_4$  under the similar conditions at 140 and 130 °C, respectively (Fig. 4c). Both samples exhibit good stable performance that retains CO complete conversion within 30 hours. Based on these results, we can infer that the enhanced catalytic activity of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  can be attributed to the structure and component merits achieved through the incorporation of new secondary copper nodes

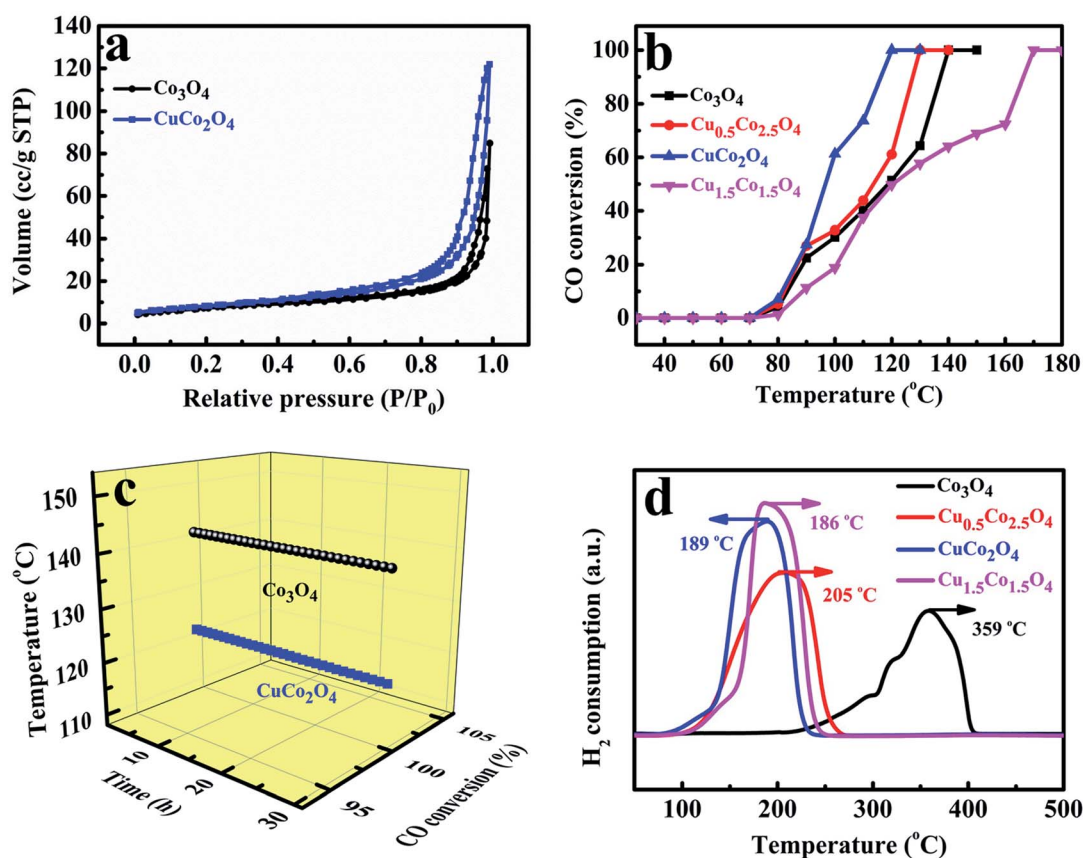


Fig. 4 Nitrogen adsorption–desorption isotherms of  $\text{Co}_3\text{O}_4$  and  $\text{CuCo}_2\text{O}_4$  (a), the catalytic activities of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  for CO oxidation (b), stability of  $\text{Co}_3\text{O}_4$  at 140 °C and  $\text{CuCo}_2\text{O}_4$  at 120 °C (c), H<sub>2</sub>-TPR profiles of  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  (d).



in the Co/Cu-MFFs precursors. In addition, pure  $\text{Co}_3\text{O}_4$  presents a good activity for CO oxidation with a CO complete conversion temperature of 140 °C, which is 30 °C lower than that reported by Zhang *et al.*<sup>52</sup> The higher catalytic activity might be ascribed to the larger specific surface area and the lower inactive  $\text{Co}^{2+}$  concentration in the surface of  $\text{Co}_3\text{O}_4$  according to the BET and XPS results (Table S3†).<sup>52</sup>

To further investigate the synergetic effects of Cu and Co species, the temperature-programmed reductions were performed using a stream of diluted  $\text{H}_2$  ( $\text{H}_2/\text{Ar}_2$ , 1 : 9 v/v). As shown in Fig. 4d, only a single peak at 359 °C is observed in pure  $\text{Co}_3\text{O}_4$  microcubes reduction profile, which can be explained by the direct reduction of cobalt ions into metallic Co in one step for the large particles of  $\text{Co}_3\text{O}_4$ .<sup>53</sup> With the amount of  $\text{Cu}^{2+}$  increasing in catalysts, the prominent peaks of  $\text{Cu}_{0.5}\text{Co}_{2.5}\text{O}_4$ ,  $\text{CuCo}_2\text{O}_4$  and  $\text{Cu}_{1.5}\text{Co}_{1.5}\text{O}_4$  shift towards lower temperature to 205, 189 and 186 °C, respectively, which means that the reducibility of the catalysts was markedly promoted when the Cu/Co atomic ratio increased. Such enhanced reduction may be attributed to the strong Co–Cu interaction originated from the intimate contact and the good interdispersion of the CuO and  $\text{Co}_3\text{O}_4$ , which possibly leads to a junction of their band levels in the solid solution or the mixed oxidations.<sup>54</sup> Such strong interactions also have been found for copper–zinc chromite catalysts and CuO–ZnO system.<sup>55,56</sup>

## 4. Conclusion

In this work, we have proposed a novel and simple method to prepare Co-based ternary metal oxides  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  with cube-like morphology and studied the effect of replacing  $\text{Co}^{2+}$  with  $\text{Cu}^{2+}$  on the catalytic activity of  $\text{Co}_3\text{O}_4$  towards CO oxidation. The  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  microcubes with controlled composition were prepared by one step pyrolysis of Co/Cu-MFFs, in which the Cu/Co atomic ratio can be tuned through adjusting the compositions of growth precursor solution. The obtained mesoporous  $\text{Cu}_x\text{Co}_{3-x}\text{O}_4$  have enhanced catalytic properties for CO oxidation compared to the pure porous  $\text{Co}_3\text{O}_4$  when the atomic ratio of Cu/Co is no more than 1/2 in the solution of preparing precursors. The larger specific surface areas and stronger reducibility resulted from the introduced new secondary Cu metal nodes into Co/Cu-MFFs which may play important roles in improving catalytic performance. We believe that the synthetic strategy can also be extended to obtain other ternary metal oxides with different structures by controlling the morphology and the compositions of the bimetal-formate frameworks, which might have a higher catalytic performance or exhibit excellent properties in other applications.

## Conflicts of interest

There are no conflicts to declare.

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