


 Cite this: *RSC Adv.*, 2018, 8, 25725

# Porous (PVDF-HFP/PANI/GO) ternary hybrid polymer electrolyte membranes for lithium-ion batteries

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A poly(vinylidene *co*-hexafluoropropylene) (PVDF-HFP) membrane is functionalized with polyaniline (PANI) and graphene oxide (GO) nanoparticles. The obtained PVDF-HFP polymer electrolyte membranes (PEMs) have been characterized and implemented in lithium-ion batteries. As a result, the PVDF-HFP/PANI membrane shows the highest ionic conductivity (IC) of  $1.04 \times 10^{-3} \text{ mS cm}^{-1}$  compared to pristine PVDF-HFP and PVDF-HFP/PANI/GO ternary membrane; however, PANI addition decreases the tensile strength of the PVDF-HFP membrane from 4.2 MPa to 2.8 MPa. Therefore, GO is introduced to recover the reduced mechanical strength of the PVDF-HFP/PANI membrane. The obtained PVDF-HFP/PANI/GO ternary membrane shows a remarkable improvement in tensile strength of up to 8.8 MPa; however, slight reduction is observed in the ionic conductivity of  $6.64 \times 10^{-4} \text{ mS cm}^{-1}$ . Furthermore, the PVDF-HFP/PANI/GO ternary membrane exhibits outstanding thermal and mechanical stabilities, improved morphology, highest electrolyte uptake (367.5%) and an excellent porosity of around 89%. Moreover, the PVDF-HFP/PANI/GO ternary PEM has been successfully applied in a lithium-ion battery, which can retain over 95% capacity after 30 cycles. Therefore, the proposed PVDF-HFP/PANI/GO ternary membrane can be a promising candidate as a separator in future lithium-ion batteries.

 Received 8th May 2018  
Accepted 2nd July 2018

DOI: 10.1039/c8ra03918f

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## 1 Introduction

Lithium-ion batteries (LIBs) have shown remarkable potentials as energy storage devices compared to various other possible alternatives.<sup>1</sup> The high efficiency and excellent energy density of lithium-ion batteries make them a promising power source for hybrid-electronic vehicles, electric vehicles, and portable electronic devices; also, they can be used to store electrical energy from renewable sources such as wind or sun.<sup>2,3</sup> However, LIBs still need extensive research in terms of safety and performance optimization. The concepts of liquid electrolytes and solid polymer electrolytes have been recommended as solutions to some of the issues related to LIBs;<sup>4–7</sup> however, the low ionic conductivities of solid polymer electrolytes and the leakage issues associated with liquid electrolytes limit their performances in LIBs.<sup>8</sup>

Therefore, polymer electrolyte membranes or gelled polymer electrolyte membranes (PEMs) have received tremendous attention in the last few years. PEMs have shown better performances compared to their other counterparts such as solid electrolyte membranes and liquid electrolyte membranes. The use of PEMs promotes safe, lightweight and leakage proof construction of lithium batteries with improved capacity and

cycle life.<sup>9</sup> Nowadays, the focus is more on producing PEMs with enhanced room-temperature conductivity, better ion transportation and stable interfacial properties of electrolytes and electrodes.<sup>10–12</sup> In this regard, several polymers such as poly(methyl methacrylate),<sup>8</sup> poly(vinylidene fluoride) (PVDF),<sup>13</sup> polyacrylonitrile (PAN)<sup>12,14</sup> and poly(vinylidene fluoride-*co*-hexafluoropropylene) (PVDF-HFP)<sup>15,16</sup> have shown good performances when applied in lithium batteries; however, these polymers have shown limited characteristics in their pristine form. Therefore, the functionalization of host polymers either with fillers or additives or by blending pure polymer matrix with other polymers has a significant role in performance optimization. In this respect, various fillers such as ZrO<sub>2</sub>, TiO<sub>2</sub>, SiO<sub>2</sub>, graphene oxide (GO), polyaniline (PANI) and Al<sub>2</sub>O<sub>3</sub> have been used to functionalize the pure polymer matrix;<sup>17–23</sup> their addition has resulted in improved mechanical strength and reduced crystallinity, which ultimately improves the ionic transport and enhances the ionic conductivity of PEMs.<sup>4,17,24–27</sup> Among several polymers, PVDF-HFP has shown good performance and flexibility for further modifications similar to PEMs; it has amorphous HFP and a crystal VDF, which provide better ionic conductivity and improved mechanical stability to the membrane.<sup>7,28–30</sup>

Therefore, a novel PVDF-HFP/PANI/GO ternary hybrid membrane has been prepared, characterized and applied in lithium-ion batteries. Polyaniline has shown great impact on energy devices due to its flexible conductive nature, easy

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synthesis and better interaction with host polymers and fillers;<sup>31</sup> however, it has rarely been tested and verified as a separator in a lithium battery. Subsequently, GO is widely used in energy-related applications since its introduction in the last few years; it has shown great interaction with PANI due to its oxygenated functional groups.<sup>32,33</sup> Even though the PANI/GO composite has been reported in several studies, it has never been tested as a PEM or as a separator in a lithium-ion battery. Both PANI and GO have unique properties, and it will be interesting to investigate the effect of the PANI/GO composite on the performance of the PVDF-HFP separator in an LIB. Thus, the proposed PVDF-HFP/PANI/GO ternary hybrid PEM can be a promising alternative to separators in future lithium-ion batteries.

## 2 Materials and methods

### 2.1 Materials

Aniline (99%), graphene oxide powder, ammonium persulfate (99.99%), ammonium hydroxide (28%), hydrochloric acid (37%, reagent grade), *n*-butanol, poly (vinylidene *co*-hexafluoropropylene) (PVDF-HFP) pellets (99.99%), acetone (99.9%), ethanol and NMP were purchased from Sigma Aldrich.

### 2.2 Methods

The flow chart of the whole methodology is shown in Fig. 1.

**2.2.1 Synthesis of polyaniline (PANI) and PANI/GO composite material.** The simple conventional polymerization method was used to synthesize PANI/GO composite nanoparticles.<sup>34</sup> Briefly, PANI synthesis involves the addition of 10% aniline monomer to 1 M HCl solution. After that, the oxidizing agent 0.1 M ammonium persulfate (APS) was added dropwise to

the solution to initiate polymerization. After continuous stirring of the solution in an ice bath for around 2 h, the solution was kept in a refrigerator overnight. After that, the obtained green colored solution was filtered and washed with ethanol and water to remove its impurities. Subsequently, the dark-green colored residue was treated with ammonium hydroxide (NH<sub>4</sub>OH) for around 24 h until its color changed to blue; then, it was washed by ethanol and water before its further use.

**2.2.2 Synthesis of PVDF-HFP and PVDF-HFP/PANI/GO ternary membranes.** The pure and modified PVDF-HFP polymer membranes were prepared through the breath figure method.<sup>35</sup> In brief, PVDF-HFP (15 wt%) pellets were dissolved in a mixture of acetone and NMP solvent with a 40 : 60 ratio and allowed to stir for 24 h; then, the mixture was kept at room temperature throughout the night for bubble removal. After that, the solution was cast on a glass substrate and allowed to dry at room temperature with around 45–60% RH. After complete solvent evaporation, the membranes were peeled off and stored in an argon glove box.

Likewise, PVDF-HFP/PANI (PANI = 2 wt%) and PVDF-HFP/PANI/GO [PANI : GO (60 : 40)] ternary hybrid membranes were prepared by the breath figure method. For PEMs, the prepared membrane samples were dipped in 1 M EC : DMC [1 : 1] lithium ion phosphate (LiPF<sub>6</sub>) solution for about 24 h before further testing.

### 2.3 Physical and electrochemical characterization

Scanning electron microscopy (SEM) analysis was performed with a FESEM, Zeiss Supra 35VP instrument to observe the morphology of the membrane. The thermal stability of different membrane samples was determined by thermogravimetric (TGA) analysis; TGA and differential scanning calorimetry (DSC)

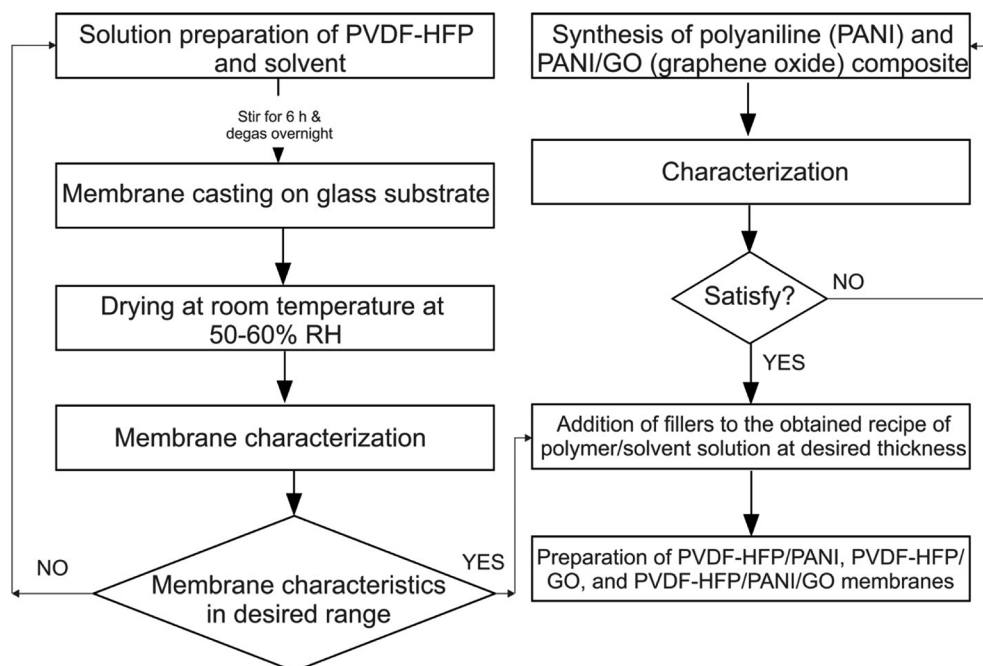


Fig. 1 Flow chart of the membrane preparation.



analyses were performed at  $10\text{ }^{\circ}\text{C min}^{-1}$  from 0 to  $400\text{ }^{\circ}\text{C}$  with Perkin Elmer STA-6000 and DSC-4000, respectively. Furthermore, Fourier transform infrared spectroscopy (FTIR) analysis was conducted within the range of  $500\text{--}4000\text{ cm}^{-1}$  with a Nicolet iS10 spectrometer by Thermoscientific. Subsequently, X-ray diffraction (XRD) analysis was performed to detect the phase of the host polymer from  $10$  to  $90^{\circ}$  using SIEMEN XRD (D5000). Moreover, the mechanical stability tests of different membrane samples were performed at  $10\text{ kN}$  as per ASTM D882-10 standards by using an Instron 3366 instrument; membrane samples with a length of  $10\text{ cm}$  and a width of  $1.5\text{ cm}$  were tested at a speed of  $2\text{ mm min}^{-1}$  through series IX software.

Different membrane samples were cut into  $2\text{ cm} \times 2\text{ cm}$  size and dipped into  $\text{LiPF}_6$  electrolyte and *n*-butanol for  $2\text{ h}$  to measure electrolyte uptake and porosity, respectively. The excess liquid was wiped off from the surface, and the weights were measured before and after immersion of the membrane samples. The following equations were used to determine electrolyte uptake and porosity:

$$\text{Porosity} = (W_f - W_i) / (V_{\text{dry}} \times \rho_b)$$

$$\text{Electrolyte uptake} = (M_f - M_i) \times 100 / M_i$$

here,  $M_i$ ,  $M_f$ , and  $W_i$ ,  $W_f$  represent the weights of the membrane samples before and after immersion in liquid electrolyte and *n*-butanol, respectively;  $\rho_b$  is the density of *n*-butanol and  $V_{\text{dry}}$  is the volume of the dry membrane samples.

The ionic conductivities of PEM samples were measured by sandwiching them between two stainless steel electrodes. Electrochemical impedance spectroscopy (EIS) analysis was performed by using a VMP3 battery analyzer and the EC-lab software at room temperature. The bulk resistances were obtained through EIS complex graphs, which were used to determine the ionic conductivity by the following relation:

$$\sigma = d / (R_b \times S)$$

here,  $d$  is the thickness and  $S$  is the surface area of different membrane samples. Chronoamperometry (CA) analysis was performed with the help of a VMP3 battery analyzer at  $5\text{ V}$  for  $30\text{ min}$  to determine the lithium ion transference number by using the following equation:

$$T_{\text{Li}^+} = I_s / I_o$$

here,  $I_s$  and  $I_o$  represent the currents at steady state and initial state, respectively.

The coin cell CR2032 was prepared to evaluate the performance of the lithium-ion battery. The prepared membrane samples were used as separators, whereas lithium metal and  $\text{LiFePO}_4$  carbon were used as the anode and cathode, respectively. For the working electrode preparation, a mixture of Katzen black ( $10\text{ wt\%}$ ), PVDF binder ( $10\text{ wt\%}$ ) and  $\text{LiFePO}_4$  ( $80\text{ wt\%}$ ) was dissolved in *N*-methyl-2-pyrrolidone (NMP) solvent and pasted on a stainless steel grid. Subsequently, the mixture was vacuum dried at  $80\text{--}90\text{ }^{\circ}\text{C}$  for around  $12\text{ h}$  before its further use. The assembly was stored in an argon glove box with oxygen and moisture concentrations of less than  $0.1\text{ ppm}$ .

### 3 Results and discussion

The procedure for membrane preparation has been reported in the above-mentioned section. The real images of various prepared membranes are shown in Fig. 2. The thickness of the prepared PVDF-HFP membranes is around  $65 \pm 5\text{ }\mu\text{m}$ . As shown in Fig. 3, a significant difference can be observed in the surfaces and cross-sectional morphologies of different PVDF-HFP membranes. The GO addition results in an excellent uniform porous structure of the PVDF-HFP/PANI/GO ternary membrane as compared to those of pure and PVDF-HFP/PANI membranes; also, its incorporation in the ternary membrane remarkably improves the porosity from around  $68\%$  to  $89\%$  and EU from about  $296\%$  to  $367.5\%$  when compared to the observations for pristine PVDF-HFP membrane. Furthermore, the filler alteration to the PVDF-HFP polymer introduces some smaller pores under the larger pores of the membrane; the smaller pores can avoid dendrite formation in batteries, and larger pores can increase the electrolyte uptake by holding the electrolyte more effectively. In addition, the improved morphology of the ternary membrane is also ascribed to the breath figure method and the unique solvent mixture of NMP and acetone. NMP is an excellent solvent for both PANI and GO dispersion;<sup>31,36</sup> hence, it facilitates the interaction between fillers and improves their dispersion in the host polymer. Acetone evaporates quickly due to its lower boiling point and provides initial stability to the membrane straight after casting; also, the breath figure method favors water droplet formation on the membrane surface, which further enhances the morphology of the membrane. Overall, the proposed modified breath figure method and the addition of

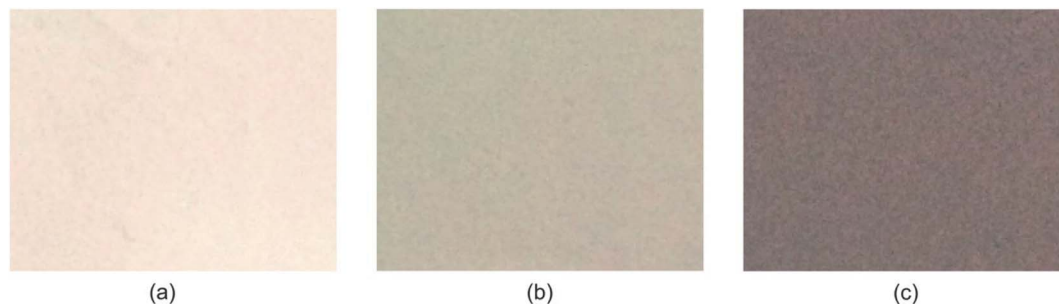


Fig. 2 Real images of (a) pristine PVDF-HFP, (b) PVDF-HFP/PANI, (c) PVDF-HFP/PANI/GO PEMs.



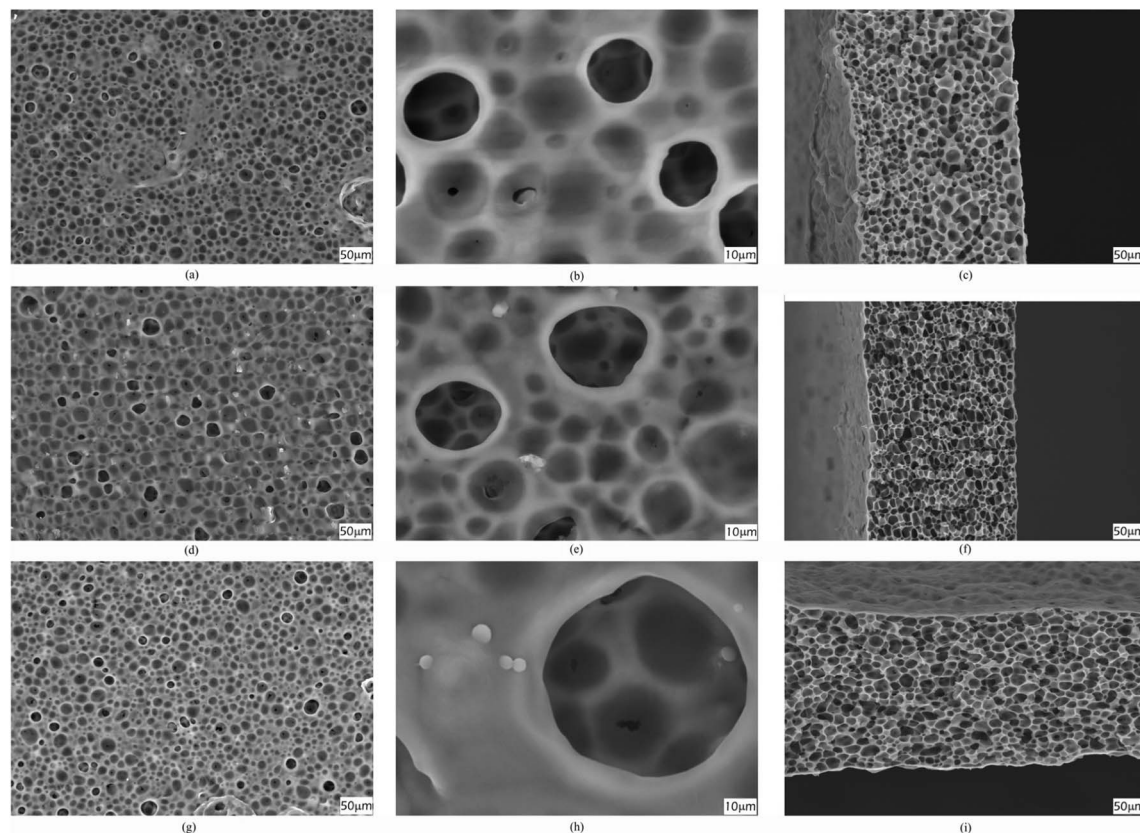


Fig. 3 SEM images of surfaces (a and b), (d and e) and (g and h); cross sections (c), (f) and (i) of pristine PVDF-HFP, PVDF-HFP/PANI and PVDF-HFP/PANI/GO membranes, respectively.

the PANI/GO composite to the host polymer result in an excellent PVDF-HFP/PANI/GO ternary hybrid membrane.

As shown in Fig. 4, FTIR analysis was performed for different particles and membranes to investigate the interactions among them. The characteristic peaks originated at  $1380\text{ cm}^{-1}$  (benzenoid (B) ring stretching),  $1644\text{ cm}^{-1}$  (quinonoid (Q) ring stretching),  $1272\text{ cm}^{-1}$  (C–N stretching),  $876\text{ cm}^{-1}$  (aromatic C–H vibration) and  $1083\text{ cm}^{-1}$  (N=Q=N stretching) confirmed the presence of PANI particles. Likewise, the peaks obtained at  $1185\text{ cm}^{-1}$  (C–O stretching),  $1714\text{ cm}^{-1}$  (C=O stretching), and  $3852\text{ cm}^{-1}$  (O–H stretching) were assigned to GO particles. The PANI/GO composite spectrum showed characteristic peaks at  $1160\text{ cm}^{-1}$  (C–H deformation),  $1582\text{ cm}^{-1}$  (quinoid vibrations),  $1377\text{ cm}^{-1}$  (absorption band) and  $3260\text{ cm}^{-1}$  (O–H stretching). Also, the peak obtained at  $1382\text{ cm}^{-1}$  (benzenoid) for PANI slightly shifted to  $1308\text{ cm}^{-1}$  for the PANI/GO composite possibly due to the interaction of H-bonding and  $\pi$ – $\pi$  bonding between PANI and GO structure. Subsequently, different spectra were observed for different PVDF-HFP PEMs. The characteristic peaks at  $835\text{ cm}^{-1}$  (CF<sub>3</sub> stretching),  $870$ – $880\text{ cm}^{-1}$  (vinylidene group),  $1170\text{ cm}^{-1}$  (CF<sub>2</sub> group) and  $1398\text{ cm}^{-1}$  (CH=CF skeleton) affirmed the existence of the PVDF-HFP polymer. In another spectrum, a few different peaks such as  $790$ – $800\text{ cm}^{-1}$  (phenyl group),  $1173\text{ cm}^{-1}$  (C–N stretching),  $1615\text{ cm}^{-1}$  (C=C stretching) and  $3278\text{ cm}^{-1}$  (N–H stretching) were observed for the PVDF-HFP/PANI membrane. Furthermore, a significant

difference could be seen in the spectra of the PVDF-HFP/PANI/GO ternary membrane. The peaks obtained at  $839\text{ cm}^{-1}$  (CF<sub>3</sub> stretching),  $1050\text{ cm}^{-1}$  (C–C skeleton),  $1400\text{ cm}^{-1}$  (C=N stretching),  $2300$ – $2500\text{ cm}^{-1}$  (aromatic C–H stretching),  $3852\text{ cm}^{-1}$  (O–H stretching), and  $3332\text{ cm}^{-1}$  (N–H stretching) all suggested the successful incorporation of the PANI/GO composite into the PVDF-HFP polymer matrix.<sup>37–39</sup>

PEMs must have good thermal stability to perform well in energy devices. Thus, TGA analysis was used to analyze the thermal stability of different membranes. As shown in Fig. 5 and reported in Table 1, there was remarkable improvement from pure to nanoparticle-modified PVDF-HFP PEMs. The PVDF-HFP/PANI/GO ternary membrane had the highest thermal degradation temperature ( $T_d$ ) at around  $498\text{ }^{\circ}\text{C}$  possibly due to the effective interaction of the PANI/GO composite with the PVDF-HFP polymer matrix, and the  $T_d$  values were about  $470\text{ }^{\circ}\text{C}$  and  $484\text{ }^{\circ}\text{C}$  for pristine PVDF-HFP and PVDF-HFP/PANI membranes, respectively. Furthermore, only around 14% mass loss was noticed for the PVDF-HFP/PANI/GO membrane between  $440\text{ }^{\circ}\text{C}$  and  $480\text{ }^{\circ}\text{C}$ , whereas the values were about 49% and 31% for pristine PVDF-HFP and PVDF-HFP/PANI membranes, respectively. As shown in the inner graph of Fig. 3(a), the PVDF-HFP/PANI/GO ternary membrane was found to be the most stable up to  $400\text{ }^{\circ}\text{C}$  compared to others; however, the pristine PVDF-HFP and PVDF-HFP/PANI membranes also showed good stabilities with only slight phase degradations at  $250\text{ }^{\circ}\text{C}$  and  $200\text{ }^{\circ}\text{C}$ , respectively.





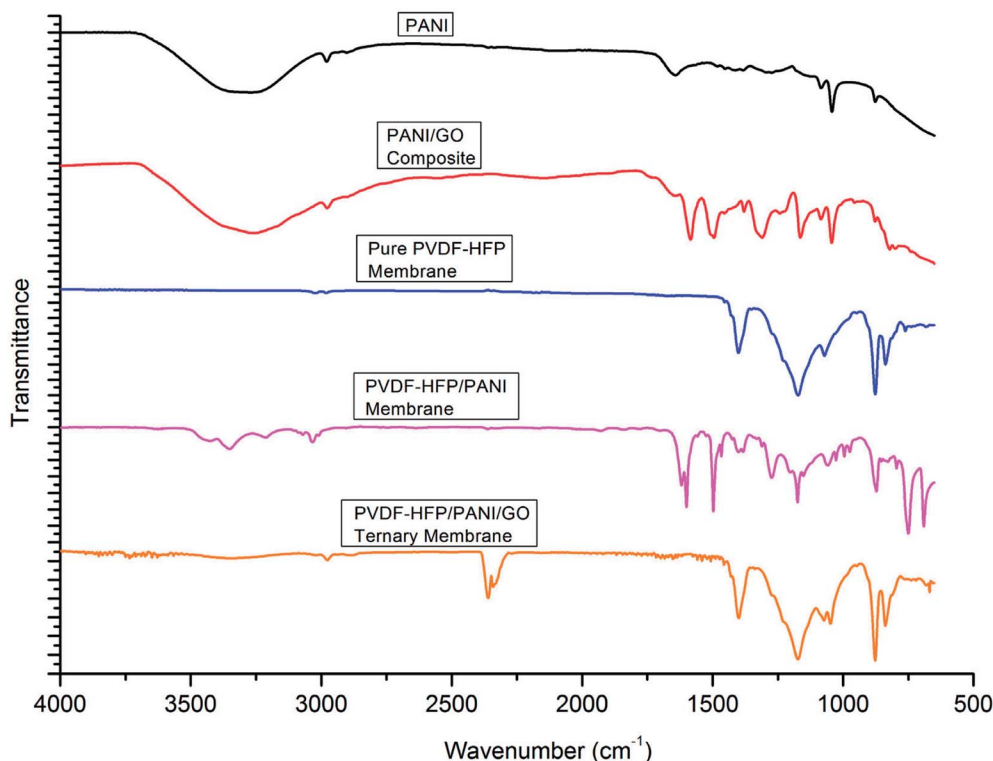


Fig. 4 FTIR analysis of PANI, PANI/GO composite, pristine PVDF-HFP, PVDF-HFP/PANI and PVDF-HFP/PANI/GO ternary membranes.

Subsequently, DSC and XRD analyses were performed to investigate the effects of nanoparticle addition on the semi-crystalline nature of the PVDF-HFP membrane. As shown in Fig. 6, first, XRD analysis affirmed the semi-crystalline nature of the PVDF-HFP membrane with characteristic peaks observed at  $2\theta = 18.4, 20,$  and  $36^\circ$ . Interestingly, the highest crystallinity reduction was found for the PVDF-HFP/PANI membrane; however, the PVDF-HFP/PANI/GO ternary membrane showed better reduction as compared to the pristine PVDF-HFP membrane. Both the GO and PANI fillers are amorphous in nature; hence, both showed reduced peak intensities compared

to the pristine PVDF-HFP membrane. Also, their combination, *i.e.*, the PANI/GO composite material, produced almost similar results to those obtained with the PVDF-HFP/PANI membrane; however, PANI alone was found to be the most effective in terms of crystallinity reduction in PVDF-HFP PEM. Additionally, higher amorphous region facilitated lithium ion transport through the membrane, which eventually enhanced the ionic conductivity. Therefore, the filler-modified membranes have more potential to perform compared to the pristine PVDF-HFP membrane in lithium-ion batteries.

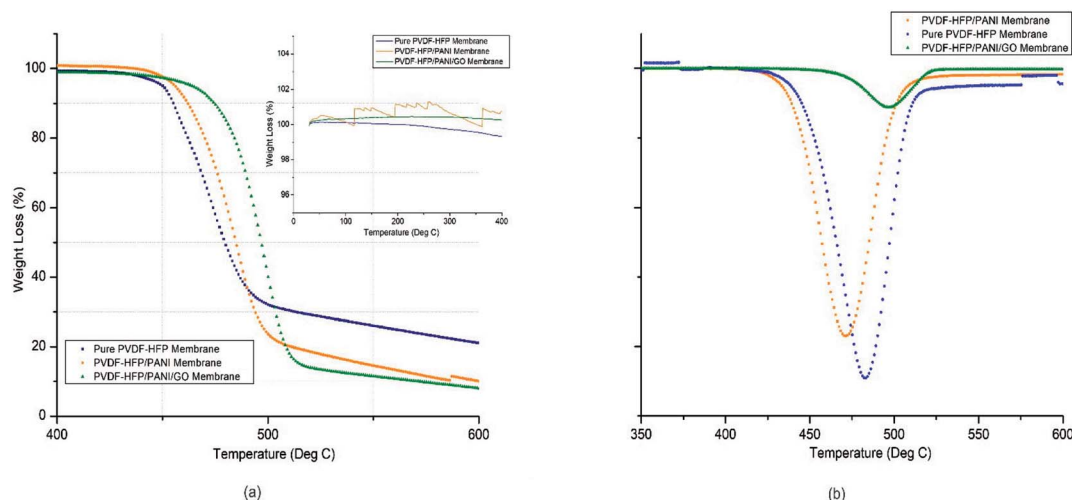
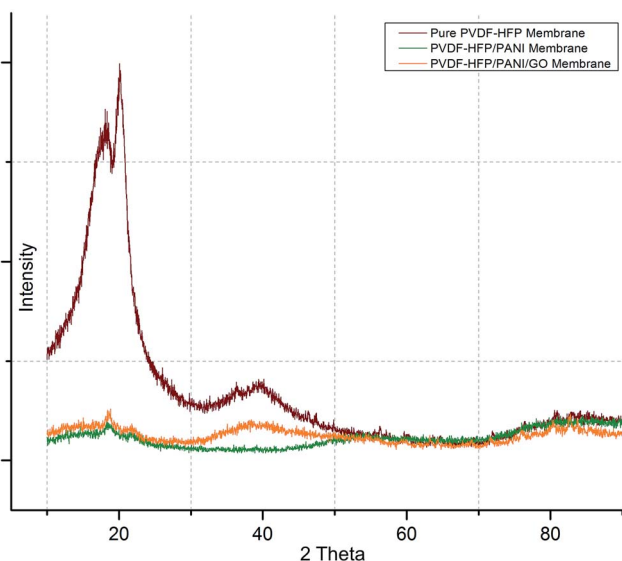


Fig. 5 Thermogravimetric (TGA) analysis of different PVDF-HFP membranes.

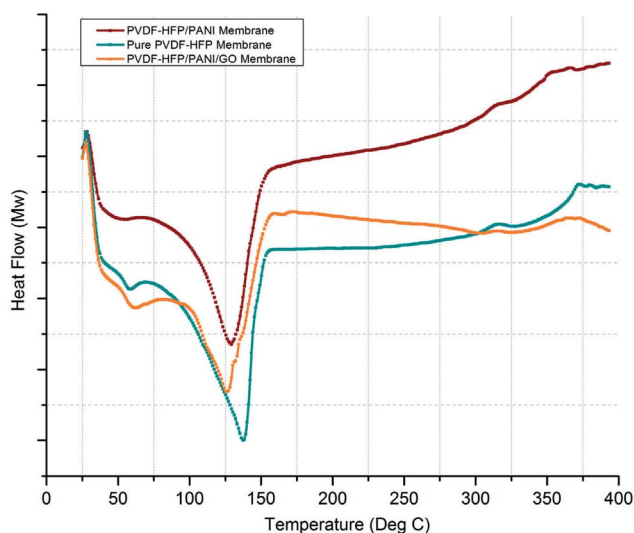


**Table 1**  $T_m$ ,  $T_d$ , degree of crystallization ( $X_c$ ), EU, porosity and ionic conductivity of different PVDF-HFP membrane samples

Sr. no.	Membrane sample	$T_d$ ( $^{\circ}\text{C}$ )	$T_m$ ( $^{\circ}\text{C}$ )	% $X_c$	Electrolyte uptake (%)	Porosity (%)	Ionic conductivity ( $\text{mS cm}^{-1}$ )
1	Pure PVDF-HFP membrane	470.34	138.37	69.2	296.4	68.8	$1.98 \times 10^{-4}$
2	PVDF-HFP/PANI membrane	483.34	129.95	48.8	340.4	77.3	$1.04 \times 10^{-3}$
3	PVDF-HFP/PANI/GO ternary membrane	497.50	125.95	51.9	367.6	88.7	$6.64 \times 10^{-4}$

**Fig. 6** XRD analysis of various PVDF-HFP membrane samples.

Similarly, DSC analysis has been performed to cross-check the XRD investigations and also to obtain the melting temperatures ( $T_m$ ) of various membranes. As shown in Fig. 7, a significant difference in  $T_m$  can be seen for pure PVDF-HFP and modified PVDF-HFP membranes. The broader endothermic

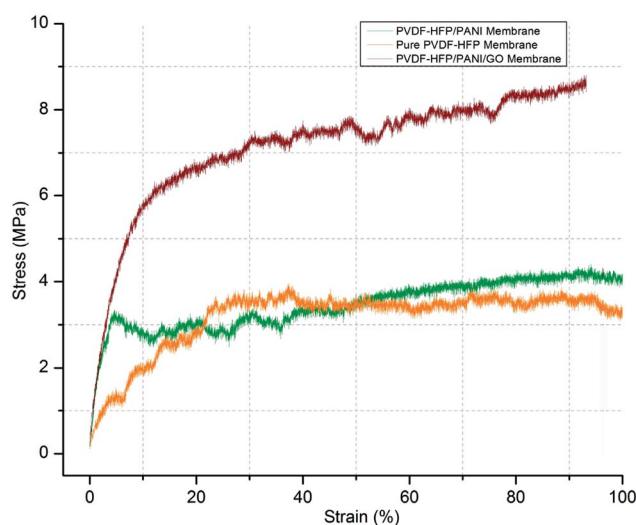
**Fig. 7** DSC analysis of different PVDF-HFP membrane samples.

peak shows a  $T_m$  value that is highest for the pure PVDF-HFP membrane at around  $139^{\circ}\text{C}$ ; however, it shifts towards the left and results in reduced  $T_m$  values for the modified PVDF-HFP membranes. The lowest  $T_m$  value is obtained at around  $125^{\circ}\text{C}$  for the PVDF-HFP/PANI/GO ternary membrane as the PANI/GO addition disturbs the crystal structure of the PVDF-HFP polymer. However, the PVDF-HFP/PANI ternary membrane also shows good reduction in  $T_m$  with a value of about  $130^{\circ}\text{C}$  due to PANI nanoparticles, which can disrupt the crystal structure of the PVDF-HFP membrane. Moreover, the crystallization degree can be calculated through the area under the  $T_m$  curve by the equation given below:

$$X_c = \Delta H_m / \Delta H_m^{\circ}$$

here,  $\Delta H_m$  and  $\Delta H_m^{\circ}$  represent the fusion enthalpy of the prepared PEMs and that of the pure PVDF-HFP polymer (*i.e.*,  $104.7 \text{ J g}^{-1}$ ), respectively.

In addition, the mechanical stability of modified and unmodified PVDF-HFP PEMs is a major concern for the separator in lithium-ion batteries. In this regard, the tensile strength test of different PVDF-HFP membranes has been performed at room temperature. As shown in Fig. 8, the PVDF-HFP/PANI/GO ternary membrane with 8.9 MPa displays much better tensile strength when compared to the pure PVDF-HFP membrane (4.2 MPa). In contrast, the tensile strength of the PVDF-HFP/PANI membrane reduces to 2.8 MPa, which can be due to the

**Fig. 8** Tensile strength of different PVDF-HFP membranes.

plasticizing effect of PANI; this decreases the flexibility and breaks it slightly earlier than that observed in other PVDF-HFP membranes. However, the PANI/GO composite responds well in the PVDF-HFP polymer matrix and forms a balanced ternary membrane. The improved tensile strength of the ternary membrane is due to the enhanced interfacial contact area between the polymer chains of PVDF-HFP and the GO particles. The polymer chains of the host polymer enwrap the GO particles and enhance the mechanical stability of the composite PEMs. Thus, GO addition to the PANI particles balances the reduced mechanical strength of PVDF-HFP/PANI PEM, which results in an improved PVDF-HFP/PANI/GO ternary hybrid PEM.

Moreover, ionic conductivity is also an important factor for the membrane separator in lithium batteries. As shown in Fig. 9 and reported in Table 1, the addition of PANI to the PVDF-HFP polymer matrix results in an excellent ionic conductivity of  $1.04 \times 10^{-3} \text{ mS cm}^{-1}$  possibly due to the improved electrostatic force of attraction in the polymer matrix. In contrast, GO insertion is not very effective in terms of ionic conductivity and produces around  $6.64 \times 10^{-4} \text{ mS cm}^{-1}$  with the PVDF-HFP/PANI/GO ternary membrane; nevertheless, this value is still better compared to those of pure and other reported PVDF-HFP membranes. Recently, an ionic conductivity of  $4.23 \times 10^{-4} \text{ mS cm}^{-1}$  has been reported for the PVDF-HFP/GO membrane.<sup>40</sup> Similarly, ionic conductivities of  $4.98 \times 10^{-3} \text{ mS cm}^{-1}$ ,<sup>41</sup>  $0.918 \times 10^{-3} \text{ mS cm}^{-1}$  (ref. 42) and  $1.31 \times 10^{-3} \text{ mS cm}^{-1}$  have been reported for PVDF-HFP/PVA/LiCF<sub>3</sub>SO<sub>3</sub>/LiAlO<sub>2</sub>, PVDF-HFP/PEMA and PVDF-HFP/PMMA membranes, respectively; membranes with ionic conductivities over  $10^{-3}$  are acceptable for lithium batteries.<sup>43</sup> Therefore, the PVDF-HFP/PANI/GO ternary hybrid membrane can be considered to be a balanced PEM as it exhibits better ionic conductivity as well as excellent mechanical strength compared to the pure PVDF-HFP membrane. Moreover, chronoamperometry analysis provides the lithium ion transference number ( $T_{\text{Li}^+}$ ) for different PVDF-HFP membranes, as shown in Fig. 10. The highest  $T_{\text{Li}^+}$  value of around 0.30 is obtained with the PVDF-HFP/PANI/GO ternary

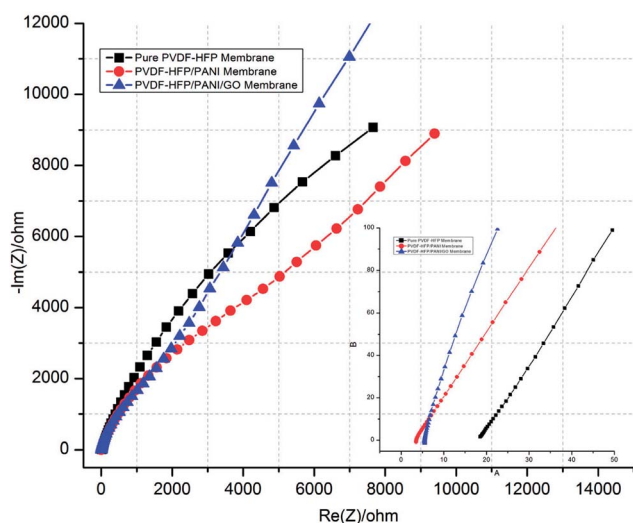


Fig. 9 EIS complex graphs of various PVDF-HFP PEMs.

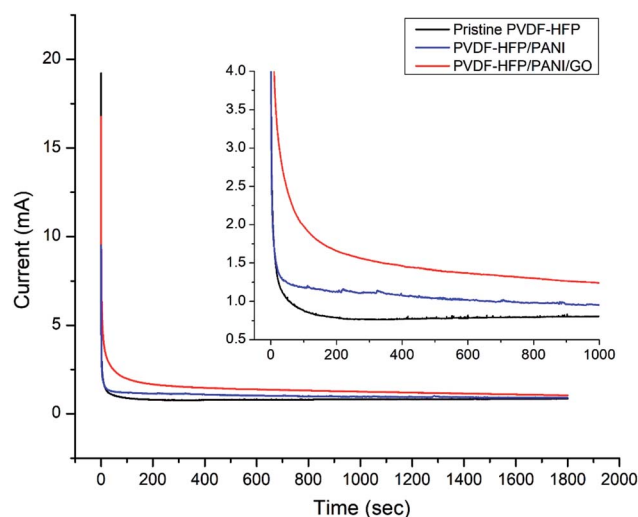


Fig. 10 Chronoamperometry profiles of various PVDF-HFP membranes.

membrane, whereas  $T_{\text{Li}^+}$  values of about 0.20 and 0.13 are obtained for PVDF-HFP/PANI and pristine PVDF-HFP membranes, respectively.

Furthermore, the coin cell CR2032 was used to test the electrochemical performances of different PEMs in lithium-ion cells. The prepared membranes were used as separators, lithium metal was used as the anode, and LiFePO<sub>4</sub> was used as the cathode in the coin cell assembly. The battery coin cells were tested at a C/20 current rate with a cut-off voltage of 2.5–4.2 V. As shown in Fig. 11(a)–(c), the charge–discharge curves of various lithium-ion coin cells with different PVDF-HFP membrane separators exhibited plateaus at around 3.4 V. In addition, the voltage difference between the charge–discharge curves was not more than 0.1 V, which can normally be obtained with commercial separators when used directly with the electrolyte.<sup>44,45</sup> A very low voltage difference between the charge–discharge curves for around 30 cycles demonstrated the capability of the PVDF-HFP/PANI/GO ternary membrane as an important energy device. Fig. 11(d) describes the obtained initial discharge capacities of pristine PVDF-HFP, PVDF-HFP/PANI, and the PVDF-HFP/PANI/GO ternary hybrid membranes, which were around 127 mA h g<sup>-1</sup>, 164 mA h g<sup>-1</sup> and 156 mA h g<sup>-1</sup>, respectively; however, the PVDF-HFP/PANI/GO ternary membrane was found to be more stable during the initial 10 cycles compared to the others. Even though the cell discharge capacity of LIBs is highly dependent on the cathode material, the morphology, ionic conductivity and electrolyte uptake of the membrane separator also have significant effects on it. Therefore, based on the overall performance, the PVDF-HFP/PANI/GO ternary membrane was subjected to the capacity retention test, and excellent results were obtained with more than 95% capacity retention after 30 cycles; this showed that with the ternary membrane, the battery could easily go up to 30 cycles without significant degradation in capacity. The electrode materials could remain wet more effectively for a longer time period due to larger electrolyte uptake, which ultimately enhanced the ionic conductivity and the cell

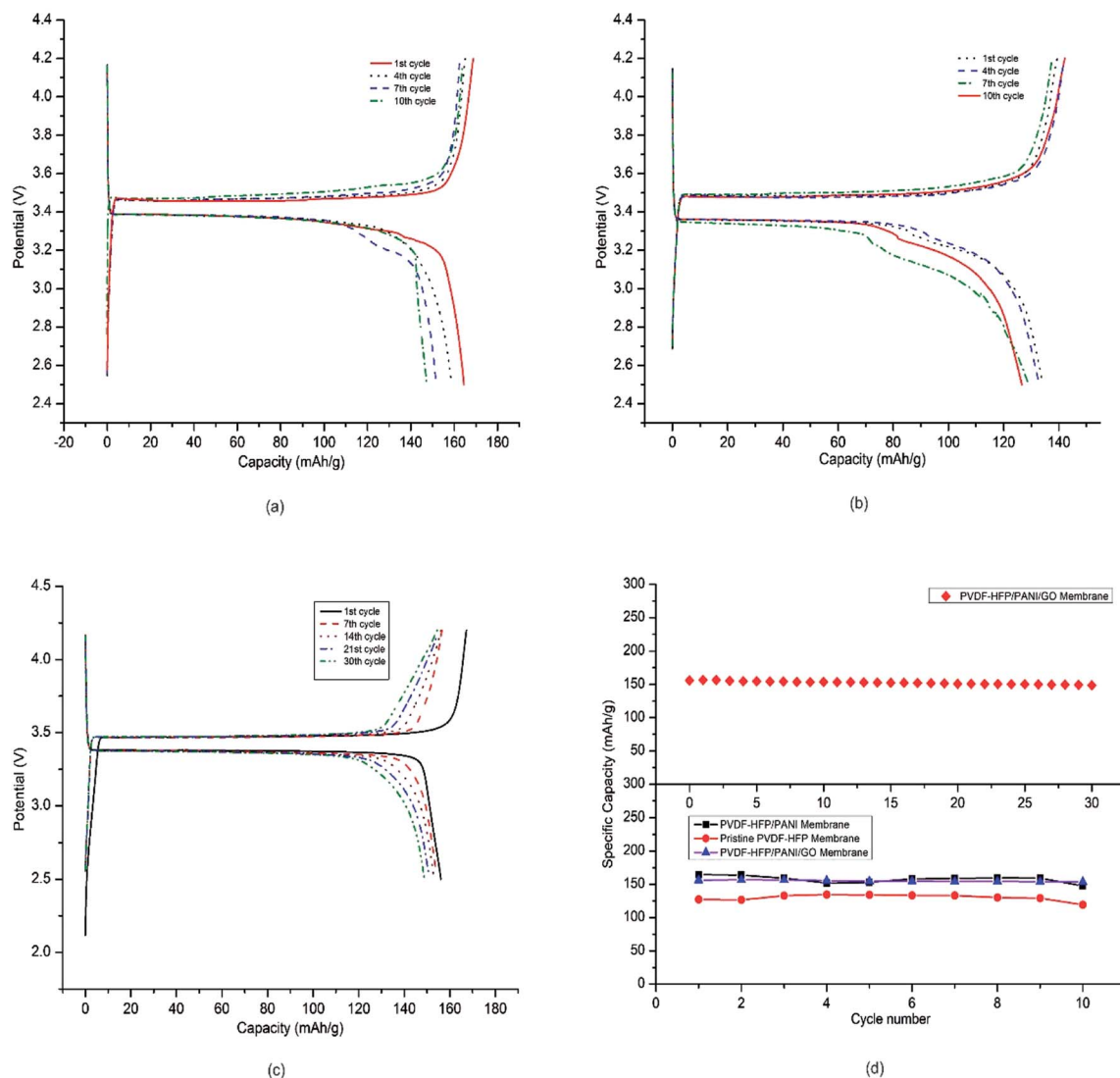


Fig. 11 Electrochemical performances of lithium ion coin cells: (a)–(c) charge–discharge curves for PVDF-HFP/PANI, pristine PVDF-HFP and PVDF-HFP/PANI/GO PEM, respectively; (d) cycling performance of various PVDF-HFP PEMs at cut off voltages of 2.5–4.2 V.

performance. Thus, the performances of all the tested membranes were satisfactory for the initial 10 cycles; however, the addition of the PANI/GO composite and its effective interaction with the host polymer resulted in a very balanced PVDF-HFP/PANI/GO ternary hybrid membrane. The improved ionic conductivity of the PVDF-HFP membrane was due to the addition of PANI, whereas the excellent mechanical stability was due to GO incorporation. Moreover, the PANI/GO composite material showed the best morphology, which enhanced the porosity and electrolyte uptake of the PVDF-HFP/PANI/GO ternary hybrid membrane. Therefore, a very stable and efficient PVDF-HFP/PANI/GO ternary hybrid membrane was obtained, and it showed great potential as a separator in lithium-ion batteries.

## 4 Conclusion

A PVDF-HFP/PANI/GO ternary hybrid membrane was successfully fabricated by the breath figure method. The obtained ternary membrane was compared to the pristine PVDF-HFP

membrane and the PVDF-HFP/PANI membrane in terms of various physical and electrochemical properties. The PVDF-HFP/PANI membrane showed the highest ionic conductivity with a value of  $1.04 \times 10^{-3} \text{ mS cm}^{-1}$ ; however, decreased tensile strength was observed from 4.2 MPa of the pure PVDF-HFP membrane to 2.8 MPa due to its plasticizing effect. Therefore, GO addition resulted in the highest tensile strength of 8.9 MPa for the PVDF-HFP/PANI/GO ternary hybrid membrane; however, GO addition exhibited negligible effect on the ionic conductivity of the PVDF-HFP/PANI membrane. Thus, the unique combination of PANI/GO composite material efficiently balanced the ionic conductivity and the mechanical strength of the PVDF-HFP polymer matrix. The new and improved PVDF-HFP/PANI/GO ternary hybrid membrane showed excellent morphology with the highest porosity of around 89% and the highest electrolyte uptake of about 367.5%. Moreover, all the PEMs were successfully tested with a battery cycler through the coin cell CR2032. Every membrane displayed good rate performance when implemented in lithium-ion batteries; also, the proposed





PVDF-HFP/PANI/GO ternary membrane displayed excellent rate performance and retained over 95% of the cell capacity after 30 cycles. Therefore, the proposed PVDF-HFP/PANI/GO ternary membrane can be a promising alternative separator for lithium-ion batteries.

## Conflicts of interest

There are no conflicts of interest.

## Acknowledgements

The Fundamental Research Grant Scheme (203.PJKIMIA.6071355 and 203.PJKIMIA.6071334) offered by the Ministry of Higher Education Malaysia and the USM Fellowship provided by Universiti Sains Malaysia provided financial support throughout this research.

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