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A polymer microsphere emulsion as a high-performance shale stabilizer for water-based drilling fluids

Jian-gen Xu,^{id}* Zhengsong Qiu,* Xin Zhao, Tingbo Mou, Hanyi Zhong and Weian Huang

Interest in using nanomaterials to improve shale stability during drilling operations has been increasing. Herein, a polymer microsphere emulsion (PME) as a high-performance shale stabilizer for water-based drilling fluids (WDFs) was prepared *via* emulsion polymerization. The particle sizes in PME in aqueous solution ranged from 90 to 320 nm. PME was found to exhibit excellent salt tolerance and temperature resistance. The plugging performance of PME was tested through pressure transmission tests. The results indicated that the polymer microspheres in PME could effectively plug shale pores and reduce shale permeability. In addition, rolling recovery tests were used to evaluate the shale hydration inhibition performance of PME. It was found that PME showed great performance for decreasing shale hydration potential. These factors make PME a promising shale stabilizer for WDFs used to drill shale formations.

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1. Introduction

Drilling fluids are known as “blood” in oil and gas drilling engineering. They have a variety of functions, such as transporting and suspending rock cuttings, balancing formation pressure, preventing wellbore collapse, and cooling and lubricating drilling bits.^{1–4} Based on their composition, drilling fluids are divided into three categories: water-based drilling fluids (WDFs); oil-based drilling fluids; and synthetic-based drilling fluids. Among these, WDFs are considered the drilling fluids with the most potential, because of their environmental friendliness, low cost and convenient preparation.^{5,6}

In recent years, shale gas developments have played an important role in China and received increasing interest in some other countries.^{7–10} In drilling engineering, shale instability has always been a challenging and costly issue.^{11–13} Drilling shale formations with traditional WDFs may lead to series problems, such as wellbore collapse, tight holes, stuck pipes, and lost circulation.^{14,15} In contrast to traditional reservoirs, shale reservoirs possess specific physicochemical features. They are regarded as having low porosity and ultra-low permeability because they contain numerous micro- and nano-scale pores and cracks.^{16,17} During drilling in shale formations, pressure transmission in WDFs will cause an increase in pore pressure, thus resulting in shale instability.^{18–20} Therefore, the best possible approach to maintaining shale stability is to effectively seal the micro- and nano-scale pores and cracks that develop in shale formations.^{21,22} Therefore, a plugging agent of suitable

size to obtain better sealing performance with WDFs is required. Recently, various nano-plugging materials have been introduced into WDFs, such as silica nanoparticles, graphite and polymer latex.^{18,23–25} Non-modified silica nanoparticles were first used as plugging agents in WDFs, and they could dramatically reduce the invasion of water into shale.²⁶ However, they easily aggregate and it is difficult to achieve nano-plugging performance with them. To improve the dispersion stability of pure nanoparticles, some researchers performed a series of experimental studies and the nano-plugging effects were significantly enhanced.^{27–29} But little research has related to the dispersion stability of modified nanoparticles at high salt concentrations and high temperatures, which is essential for nanoparticles being applied in the field. In addition, shale is mainly composed of clay minerals and is thus water-sensitive. Water–shale interactions may result in shale swelling and dispersion.^{30,31} Hence, improving the shale hydration inhibition of WDFs is also the goal of researchers. Consequently, hunting for a novel high-performance shale stabilizer in combination with achieving plugging and hydration inhibition properties is a more valuable research issue.

In this study, a polymer microsphere emulsion was introduced into WDFs as a high-performance shale stabilizer. A nano-polymer microsphere emulsion was prepared *via* the emulsion polymerization of styrene (St), *n*-butyl acrylate (BA) and 2-acrylamide-2-methylpropanesulfonic acid (AMPS). In this polymer, St and BA units act as hydrophobic groups. AMPS units act as hydrophilic groups to improve the dispersion stability of polymer microspheres in WDFs. In addition, the presence of emulsifiers can not only improve the dispersion stability of nanoparticles, but can also decrease the surface

School of Petroleum Engineering, China University of Petroleum (East China), Qingdao 266580, Shandong, P. R. China. E-mail: xujiangen0@163.com; qiuuzs63@sina.com



tension and thus reduce capillary effects.³² A low amount of water-intake will be also beneficial for decreasing the shale hydration potential. The novel polymer microsphere emulsion was found to exhibit high salt tolerance and temperature resistance. Furthermore, the polymer microsphere emulsion carried out the dual roles of physical plugging and shale hydration inhibition.

2. Experimental

2.1 Materials

St (99%), BA (98%), NaOH (96%), NaCl (99.5%), CaCl₂ (96%), KCl (99.5%), sodium dodecyl sulfate (SDS), and potassium persulfate (KPS, 99%) were provided by Sinopharm Chemical Corporation (Shanghai, China) and used without further purification. AMPS (98%), SiO₂ nanoparticles (99.8%, 7–40 nm), and octylphenol polyoxyethylene ether (OP-10, 99%) were purchased from Aladdin Industrial Corporation (Shanghai, China). Polymeric alcohol (JHC) was obtained from China Oilfield Services (Sanhe, China). The shale samples used for the testing of plugging properties were kindly provided by Zhejiang oilfield, and the mineral content of the shale is shown in Table 1. The shale samples used for hydration inhibition performance testing were provided by Turpan Hami Basin, China, and the average concentration of different minerals is presented in Table 2.

2.2 Preparation of the poly(St-BA-AMPS) microsphere emulsion

A poly(St-BA-AMPS) microsphere emulsion was prepared through emulsion polymerization. Fig. 1 shows a schematic diagram of the emulsion polymerization system. A 2.4 g amount of AMPS was dissolved in 55 mL of distilled water, and NaOH was used to adjust the pH value to about 6. The emulsifiers SDS (0.6 g) and OP-10 (0.6 g) were added to the solution under stirring. After the emulsifiers were dissolved in the solution, the mixture was transferred to a four-neck flask and stirred with a mechanical stirrer. The monomers St (28 g) and BA (12 g) were added into the mixture under vigorous stirring to prepare the pre-emulsion. Then, KPS was introduced into the reactor to initiate the reaction. The emulsion polymerization system was maintained at 80 °C for 4 h to obtain the polymer microsphere emulsion product, named PME.

Table 1 Mineral content of the shale samples used for plugging properties tests

Component	Content (wt%)	Component of clay mineral	Content (wt%)
Quartz	50	Illite	45
Pyrite	2	Chlorite	24
Siderite	2	Illite/smectite mixed layer	31
Plagioclase	15		
Clay mineral	31		

Table 2 Mineral content of the shale samples used for hydration inhibition performance tests

Component	Content (wt%)	Component of clay mineral	Content (wt%)
Quartz	20	Illite	12
Calcite	28	Chlorite	3
Plagioclase	29	Kaolinite	3
Iron dolomite	2	Illite/smectite mixed layer	82
Potassium feldspar	6		
Clay mineral	15		

2.3 Characterization

2.3.1 Instrumentation and characterization. The infrared spectrum of PME was obtained with a Fourier transform infrared spectrometer (FT-IR, Nicolet 6700, U.S.A.). The ¹H-NMR spectrum of PME was measured with nuclear magnetic resonance apparatus (¹H-NMR, Bruker AV500, Germany), and CDCl₃ was used as the solvent. The structure and morphology of PME in aqueous solution were observed using a transmission electron microscope (TEM, JEM-2100UHR, Japan). The particle size distribution of PME was determined *via* dynamic light scattering using a nanoparticle size analyzer (PSD, NanoBrook Omni, U.S.A.). Thermogravimetric analysis of PME was conducted using a TGA/DTA thermal analyzer (TGA, NETZSCH 209F3, Germany) under a N₂ atmosphere at a heating rate of 10 °C min^{−1}.

2.3.2 Salt tolerance of PME. In order to investigate the dispersion stability of PME in NaCl and CaCl₂ solutions of different concentrations, particle size distribution tests were carried out. Briefly, PME was dispersed in NaCl aqueous solutions with concentrations of 0, 5, 10, 15 and 20 wt%. After 16 h, photographs were taken to record the coagulation behaviours of PME in the aqueous solutions. In addition, the particle size distributions of PME in the solutions were also tested to further analyse the dispersion stability. The above method was also used to investigate the dispersion stability of PME in CaCl₂ solutions with concentrations of 0, 1, 2, 3 and 4 wt%.

2.3.3 Temperature resistance of PME. PME was dispersed into aqueous solutions, and the concentration of PME in solution was fixed at 1 wt%. Then, the solutions were poured into sealed tanks, and they were placed into an XGRL-4 type rolling oven (Haitongda Company, China) for 16 h at a certain temperature. In this study, hot-rolling experiments were set at temperatures of 25, 60, 90, 120, 130, 140, and 150 °C. After being hot-rolled, photographs were taken to record the coagulation behaviours of PME in the aqueous solutions. In addition, the particle size distributions of PME in the solutions were also tested to further analyse the dispersion stability.

2.4 Plugging properties of PME

Pressure transmission tests were conducted to assess the sealing performance of PME.³³ An experimental device for simulating hydro-mechanical coupling in shale was used for these tests. The shale specimens were cut into cylindrical cores (length: 6.0 mm; diameter: 25 mm), and 4% NaCl solution



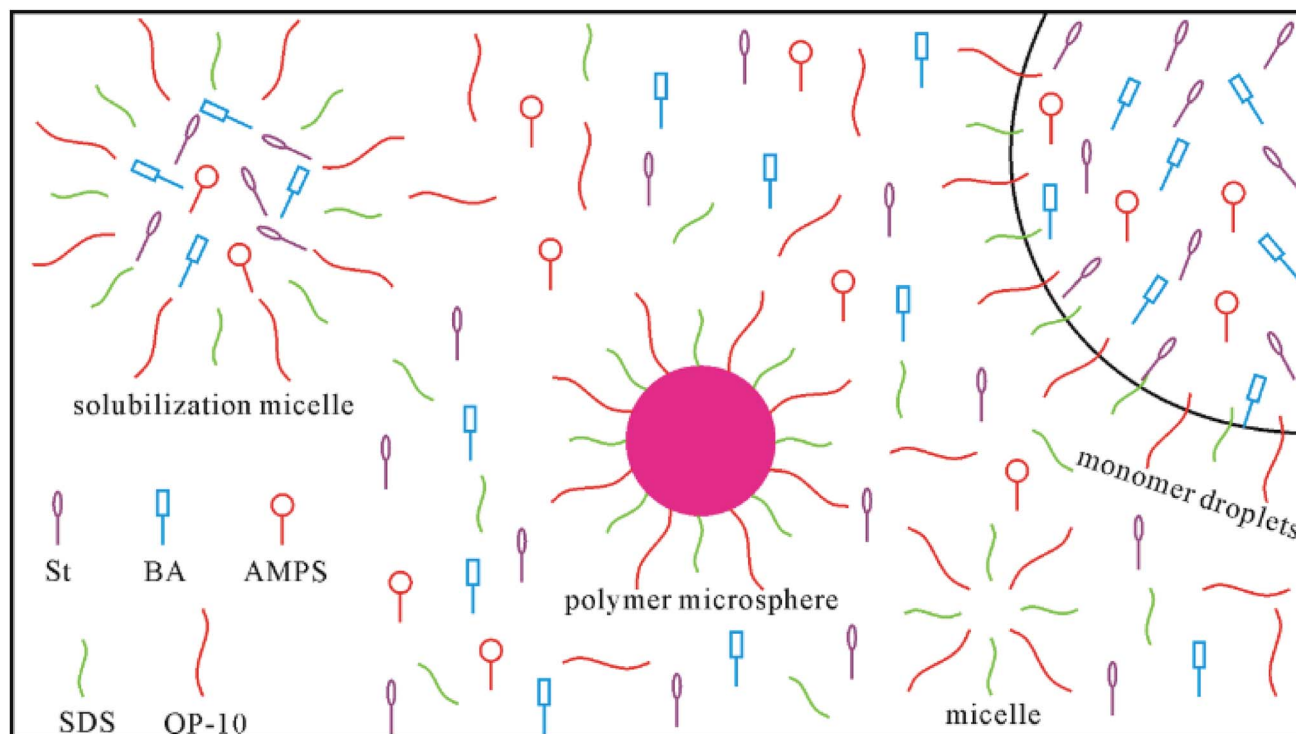


Fig. 1 A schematic diagram of the emulsion polymerization system.

served as the reservoir brine. Commonly used plugging agents, including polymeric alcohol (JHC) and nano-silica (NS), were selected for comparison with PME. During the pressure transmission tests, shale cores were placed into the sealed chamber and the testing fluids flowed across the upper part of the shale cores continuously. The upstream pressure of the shale cores was kept at 2.0 MPa at all times, and the initial downstream pressure was set at 1.0 MPa. Under the pressure difference, the downstream pressure was raised gradually over time until a balance was reached. The downstream pressure build up was recorded as a function of time, and the increasing rate of downstream pressure could be used for calculating the shale permeability. The permeability values for shale before and after interaction with the test fluids were calculated using eqn (1):³⁴

$$K = \frac{\mu\beta VL}{A} \frac{\ln\left(\frac{P_m - P_o}{P_m - P(L, t_2)}\right) - \ln\left(\frac{P_m - P_o}{P_m - P(L, t_1)}\right)}{t_2 - t_1} \quad (1)$$

where K is the permeability of the shale core, μm^2 ; μ is the fluid viscosity, mPa s; β is the fluid compressibility, MPa^{-1} ; V is the enclosed volume of the bottom chamber, cm^3 ; L is the length of the shale core, cm; A is the cross-sectional area of the shale core, cm^2 ; t is the total test time, s; P_m is the upstream pressure, MPa; P_o is the initial downstream pressure, MPa; and $P(L, t)$ is the realtime downstream pressure, MPa.

In order to further study the plugging mechanism of PME, the pore structures of shale samples before and after interacting with PME were characterized. Scanning electron microscopy (SEM, Hitachi S4800, Japan) photographs were obtained to intuitively describe the plugging properties of PME.

2.5 Hydration inhibition performance of PME

2.5.1 Rolling recovery tests. Rolling recovery tests can be used to analyse the shale hydration dispersion characteristics and assess the hydration inhibition properties of the test fluids.³⁵ Commonly used shale hydration inhibitors, including polymeric alcohol (JHC) and potassium chloride (KCl), were selected for comparison with PME. First, 50 g of shale sample (particle sizes of 2–5 mm) was dried to a constant weight and placed in an aging tank with 350 mL of test fluid. Then, the aging tank was placed into a roller oven for 16 hours of hot rolling at a temperature of 77 °C. Finally, the sample was removed from the aging tank and washed with distilled water. Then, it was filtered through a 40 mesh sieve. The filtered sample was placed in a drying oven for 4 hours at a temperature of 105 °C. The remaining shale sample was weighed to calculate the shale recovery rate.

2.5.2 Surface tension measurements. Aqueous solutions of PME at different concentrations were prepared using deionized water. Surface tension measurements were carried out using a BZY-1 surface tensiometer (Shanghai Geng Instrument Company, China) using the platinum plate method. All the solutions were tested three times and the results averaged.

2.5.3 Contact angle measurements. A contact angle tester (JC2000D5M, China) was applied to carry out contact angle measurements. First, the shale surface was polished using sandpaper to remove the oxide film. Then, shale samples were placed into beakers containing PME at different concentrations. After immersing in the solutions for 6 h, the shale samples were removed from the beaker and left to air dry. Finally, a drop of distilled water was dropped on the shale surfaces with a syringe



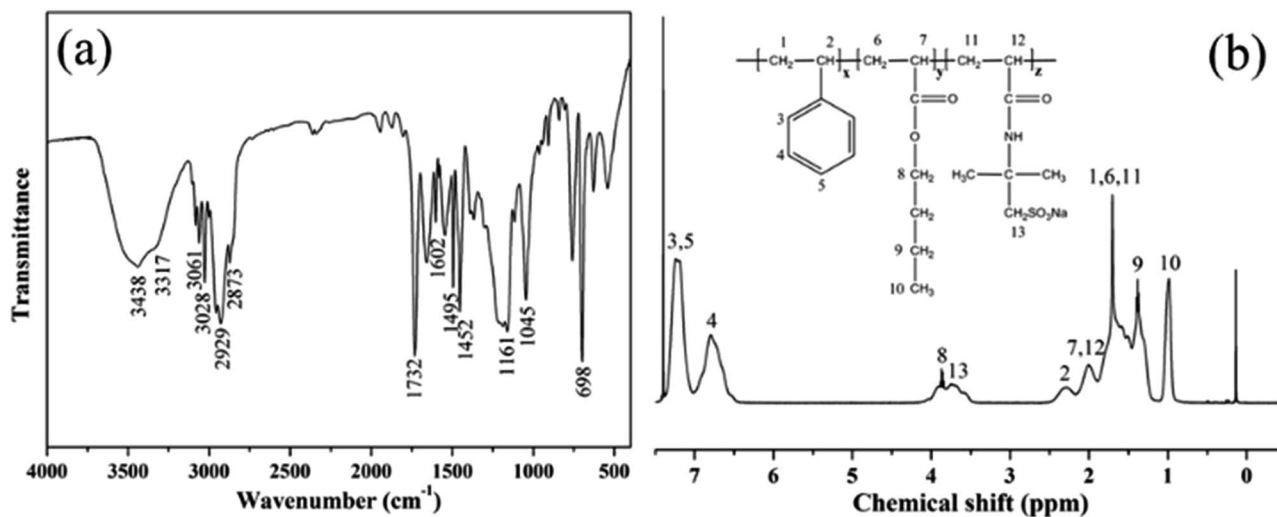


Fig. 2 (a) FT-IR spectrum of PME. (b) ^1H NMR spectrum of PME.

and pictures were captured. The contact angles were measured *via* image analysis with built-in software.

3. Results and discussion

3.1 Characterization of PME

Fig. 2a shows the FT-IR spectrum of PME. The peaks appearing at 3061 cm^{-1} , 3028 cm^{-1} and 2929 cm^{-1} correspond to the absorption peaks of C–H in a benzene ring. The peaks at 1602 cm^{-1} , 1495 cm^{-1} and 1452 cm^{-1} are ascribed to stretching vibrations of a benzene skeleton, indicating that the product contained St chain segments. In addition, the peak appearing at 1732 cm^{-1} corresponds to a stretching vibration of C=O. The peak at 1161 cm^{-1} is ascribed to a stretching vibration of a C–O–C bond, indicating that the product contains BA chain segments. Furthermore, the peaks appearing at 3438 cm^{-1} and 3317 cm^{-1} correspond to a stretching vibration of –NH. The peak at 1045 cm^{-1} is ascribed to a stretching vibration of an S=O bond, indicating that the product contains AMPS chain

segments. The above discussion indicates that the newly-prepared PME is a copolymer of St, BA and AMPS.

The chemical structure of PME was further analysed *via* ^1H NMR measurements, and the results are presented in Fig. 2b. The ^1H chemical shifts of the copolymer are presented in the ^1H NMR spectrum, and the corresponding peaks are marked. The results exhibit that the three monomers all successfully participated in the polymerization reaction. Therefore, the FT-IR and ^1H NMR results show that PME was successfully prepared.

A typical TEM micrograph of a diluted PME sample is shown in Fig. 3a. The polymer nanoparticles were mainly spherical and they were well dispersed in aqueous solution. Through the TEM image, it can be seen that the average size of the polymer microspheres was about 180 nm and the particle sizes ranged from 110 nm to 270 nm. Fig. 3b demonstrates the particle size distribution of PME. The particle sizes of the polymer microspheres ranged from 90 nm to 320 nm with a D50 value (medium particle size) of 175 nm. The PSD measurement results basically coincide with the TEM characterization results. Large polymer microspheres (particle sizes larger than 270 nm)

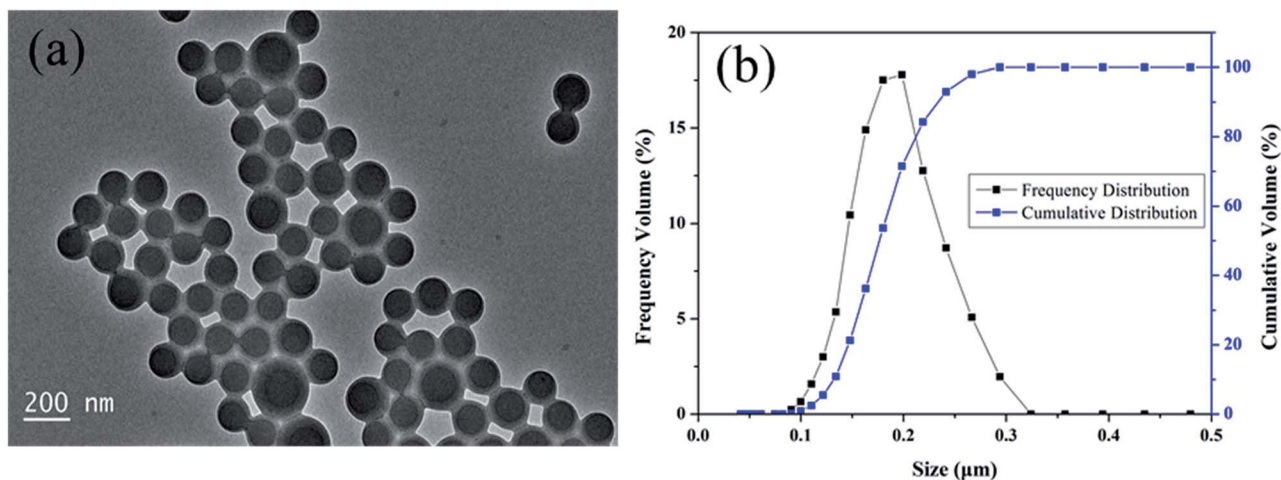


Fig. 3 (a) TEM image of PME. (b) Particle size distribution of PME.



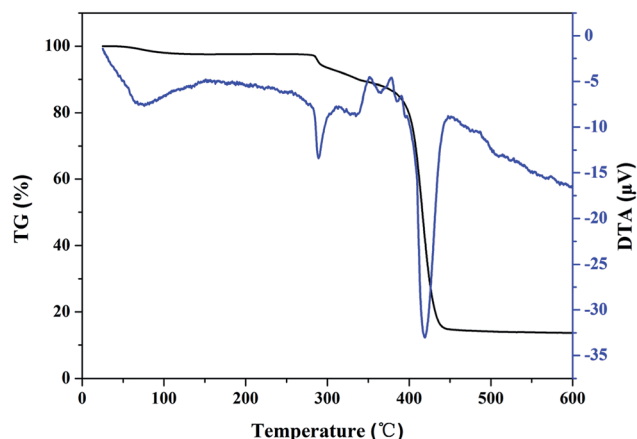


Fig. 4 TGA and DTA curves of PME.

were not observed in the TEM image due to the small number present in PME.

TGA and DTA curves of PME are presented in Fig. 4. It can be seen that the initial weight loss (around 2.57 wt%), from room temperature to 120 °C, can be ascribed to the evaporation of adsorbed water. The weight loss in the range of 275–385 °C could be due to the decomposition of AMPS.³⁶ A sharp weight

loss was observed at around 400 °C, which was attributed to the thermal decomposition of the polymer backbone. Therefore, PME showed good thermal stability.

3.2 Salt tolerance of PME

Photographs of PME in NaCl and CaCl₂ solutions of different concentrations are shown in Fig. 5a and b, respectively. After being dispersed in salt solution for 16 h, it can be seen that the polymer microsphere emulsion remained stably dispersed and no precipitation appeared in the solutions. This proves that PME possessed strong dispersion stability in salt solutions. In addition, particle size distribution measurements were conducted to further analyze the dispersion stability of PME in NaCl and CaCl₂ solutions, the results of which are depicted in Fig. 5c and d, respectively. The salt solutions only created slight variations in the particle size distribution curves, which were only in the form of a little widening. It can be concluded that only a few nanoparticles in PME agglomerated, and the high salt tolerance of PME in NaCl and CaCl₂ solutions was further confirmed. This can be explained through the adsorption of emulsifiers onto the polymer microspheres, which can greatly enhance the effects of steric hindrance and electrostatic repulsion in salt solutions of high concentration.³²

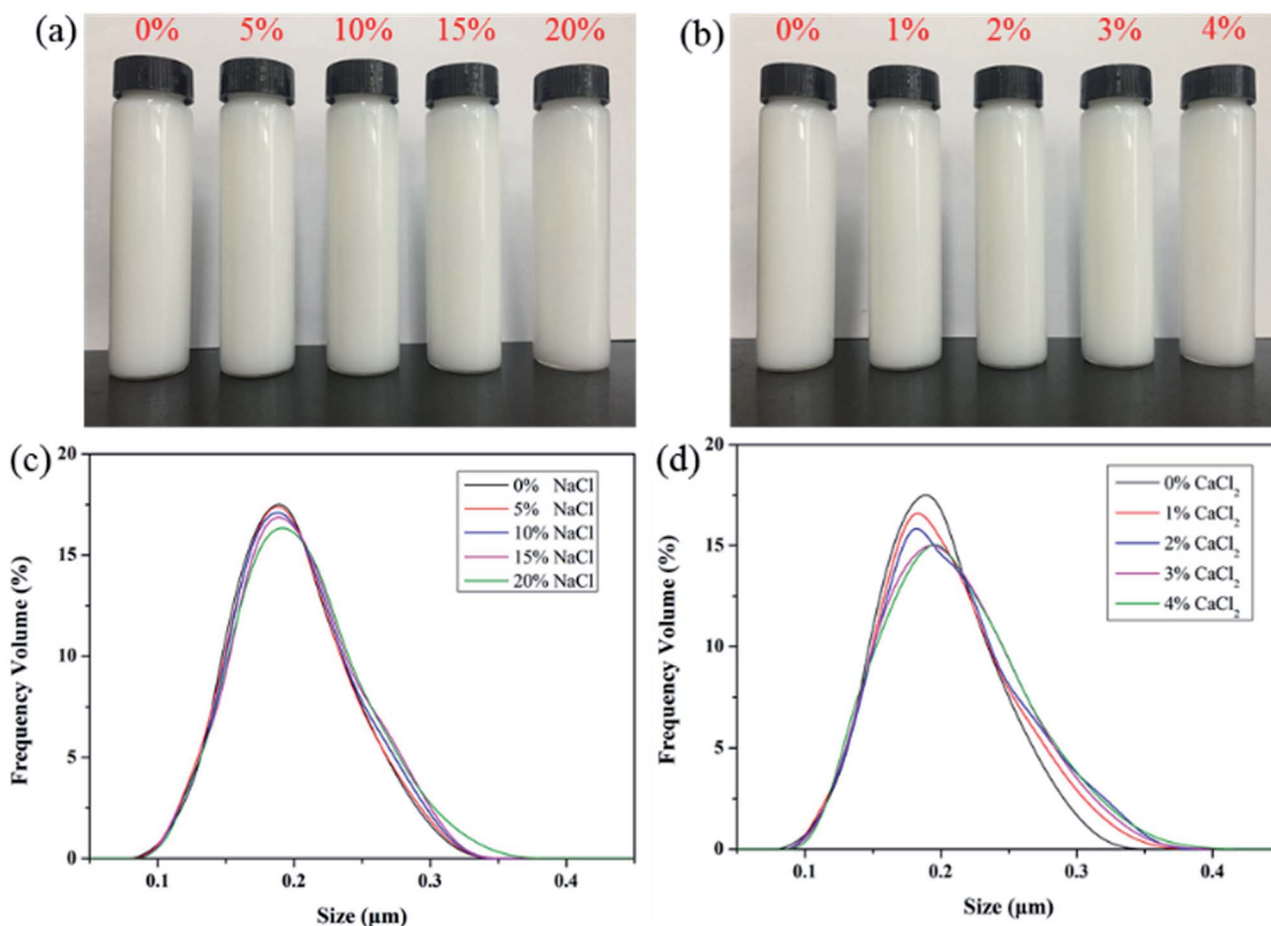


Fig. 5 Photographs of PME in (a) NaCl solutions and (b) CaCl₂ solutions of different concentrations. Particle size distributions of PME in (c) NaCl solutions and (d) CaCl₂ solutions of different concentrations.



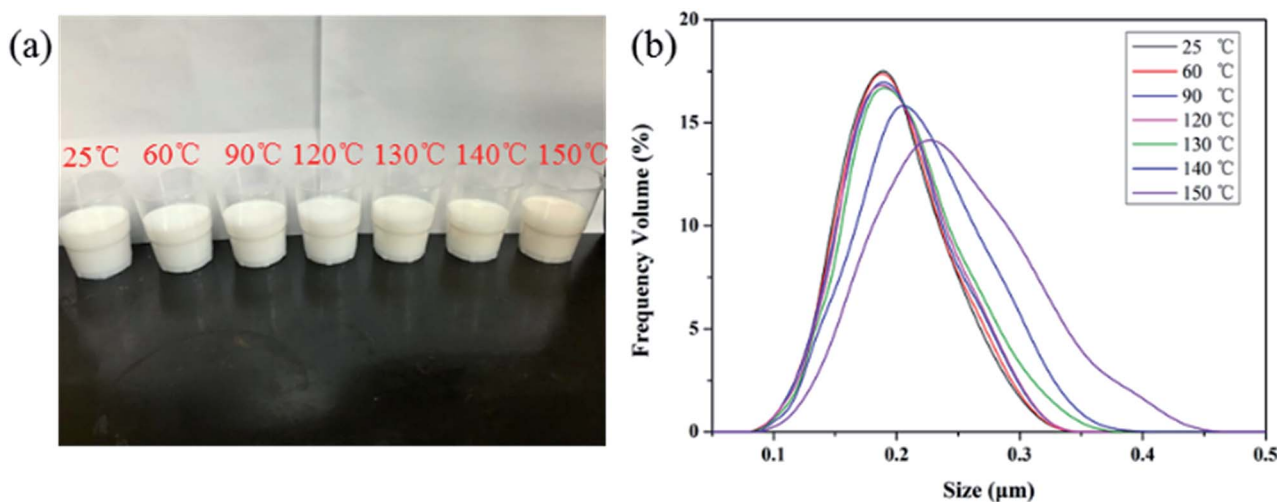


Fig. 6 (a) A photograph of PME after hot-rolling for 16 h at different temperatures. (b) Particle size distributions of PME after hot-rolling for 16 h at different temperatures.

3.3 Temperature resistance of PME

Fig. 6a presents a photograph of PME in aqueous solutions after being hot-rolled at different temperatures. No precipitation appeared in the solutions after hot-rolling at different temperatures. But after the temperature increased to 130 °C, the solutions began to turn yellow, indicating that the polymer microsphere emulsion gradually deteriorates. In addition, particle size distribution measurements were conducted to further analyse the dispersion stability of PME after hot-rolling at different temperatures.

As depicted in Fig. 6b, when the temperature was lower than 130 °C, an increase in temperature created little change in the particle size distribution curves. But after the temperature rose above 130 °C, the particle size distribution curves gradually widened, indicating that after hot-rolling, some polymer nanoparticles in PME agglomerated and the dispersion stability of PME was decreased. These results show that PME exhibited excellent temperature resistance from 25 to 130 °C.

3.4 Plugging properties of PME

Pressure transmission curves are presented in Fig. 7, and the permeability values for shale cores after interacting with different testing fluids were calculated using eqn (1), and are illustrated in Table 3. It took only around 45 min for the downstream pressure to reach a balance when interacting with PT-1, and the permeability of the shale core was $6.08 \times 10^{-7} \mu\text{m}^2$. The pressure transmission rate slowed down when interacting with PT-2, PT-3 and PT-4, and the time for the downstream pressure to reach a balance was delayed to 84, 103 and 188 min, respectively. After interacting with PT-2, PT-3 and PT-4, the permeability values of the shale cores were decreased to 2.04×10^{-7} , 1.61×10^{-7} , and $8.07 \times 10^{-8} \mu\text{m}^2$, respectively. These results showed that PME exhibited excellent plugging performance to slow down pressure transmission rates and reduce the permeability of shale cores. The plugging performance of PME was significantly better than that of JHC and NS, and thus the outstanding plugging performance of PME was further confirmed.

Based on the above results, a possible mechanism was concluded. Under the drilling pressure difference, the polymer microspheres were tightly embedded into the micro- and nano-scale pores and cracks in the shale cores, resulting in dense-plugging. This can be seen from the SEM images presented in Fig. 8. A lot of natural micro- and nano-scale pores and cracks develop in shale formations. After interacting with PME, the pores and cracks were effectively plugged by the polymer microspheres. Thus, the pressure transmission rate was slowed

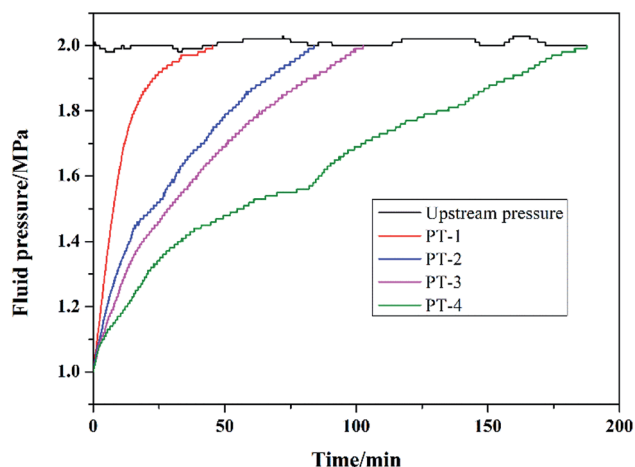


Fig. 7 Pressure transmission test curves.

Table 3 Permeability values for the shale cores

Label	Testing fluid	Shale permeability (μm^2)
PT-1	4% NaCl	6.08×10^{-7}
PT-2	4% NaCl + 2% JHC	2.04×10^{-7}
PT-3	4% NaCl + 2% NS	1.61×10^{-7}
PT-4	4% NaCl + 2% PME	8.07×10^{-8}



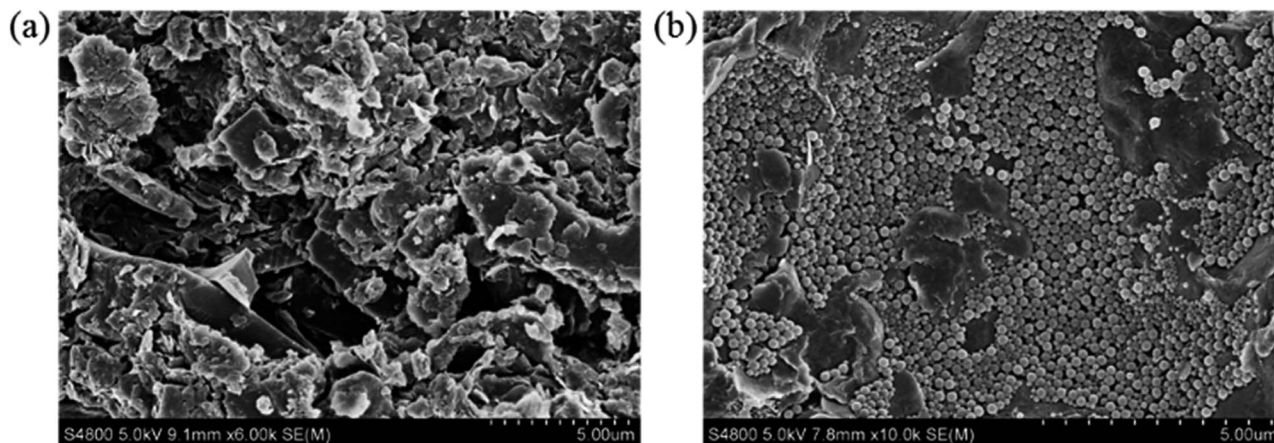


Fig. 8 SEM photographs of (a) the shale core before testing and (b) the shale core after interaction with PT-4.

down and the permeability of the shale core was reduced. Therefore, water-based fluids containing PME were proven to show excellent physical plugging performance, and PME is expected to be an effective plugging agent for WDFs used to drill shale formations.

3.5 Hydration inhibition performance of PME

Fig. 9 presents the recovery rates of shale cuttings when interacting with different testing fluids. A higher recovery rate is a symbol of better shale hydration inhibition performance. As shown in Fig. 9, a high dispersion tendency was observed when interacting with deionized water, where around 59.8% of the shale cuttings were dispersed. The solutions containing 0.5% PME, 1.0% PME, and 2.0% PME could enhance the shale recovery rate from 40.2% to 67.2%, 75.6%, and 88.4%, respectively, indicating the great shale hydration inhibition performance of PME. In addition, compared with KCl and JHC, PME showed better performance with regards to inhibiting shale dispersion at the same concentrations.

To further investigate the mechanism of how PME inhibits shale hydration, surface tension and contact angle measurements were obtained. The shale surface is usually hydrophilic, and capillary suction pressure is one of the driving forces for water molecules invading shale formations.^{37,38} Reducing the surface tension of WDFs would effectively decrease the capillary pressure, resulting in a reduced intake of WDFs, thus weakening the shale hydration effect. The variation in surface tension as a function of PME concentration is shown in Fig. 10a. The surface tension continuously decreases with an increase in PME concentration. In this work, a significant reduction in surface tension at low concentrations was observed. When the concentration was 0.1%, the surface tension decreased to as low as 36.9 mN m^{-1} , indicating that PME could effectively decrease the surface tension, even at low concentrations. This is due to the existence of surfactants in PME, resulting in lower surface tension. Therefore, the addition of PME was beneficial in decreasing the capillary pressure, and thus effectively inhibiting shale hydration *via* diminishing the intake of water into shale formations.

The effects of PME on the shale wettability are shown in Fig. 10b. The contact angle of pristine shale was around 22.6° , demonstrating favorable hydrophilicity. After interacting with PME, the contact angle of the shale surface increased rapidly. When the concentration was 0.2%, the contact angle increased to 42.5° , indicating a significant increase in contact angle after soaking with PME solution. In particular, when the concentration was 2.0%, the contact angle of the shale sample could be increased to 82.6° , nearing 90.0° . It could be inferred that PME was capable of significantly changing the shale surface to be more hydrophobic after interacting with PME. Moreover, a more hydrophobic shale surface would create less affinity towards water, and thus reduce the shale hydration potential.

3.6 Wellbore stabilizing mechanism of PME

Based on above research results and some literature, a probable mechanism for how PME improves shale stability can be summed up. An intuitive model describing the wellbore stabilizing mechanism of PME is suggested in Fig. 11. A lot of micro- and nano-scale pores and fractures develop in shale formations. Under a drilling pressure difference and capillary pressure, the

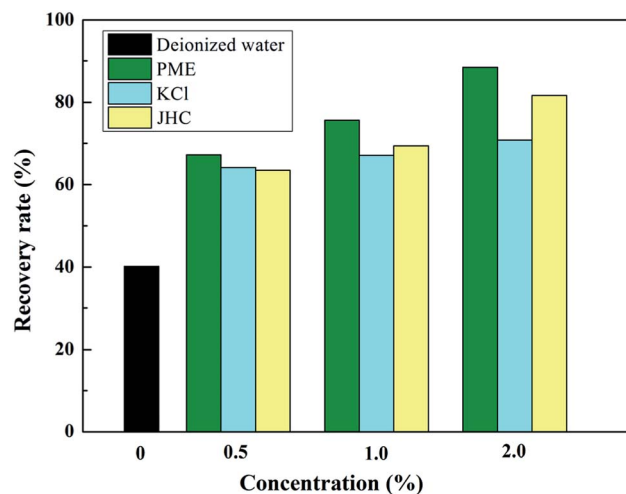


Fig. 9 The results of rolling recovery tests.



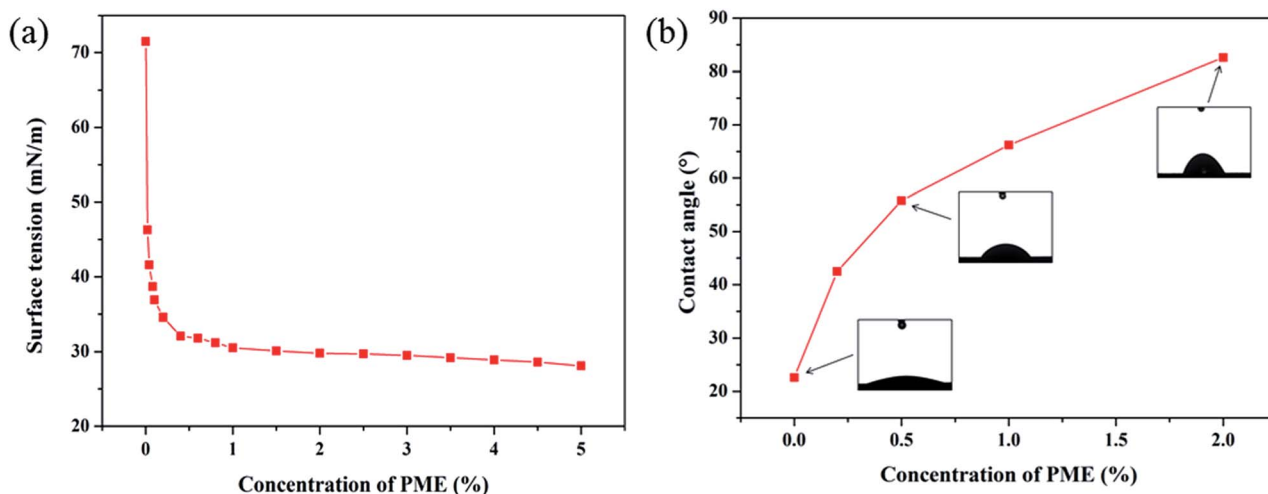


Fig. 10 Results of (a) surface tension tests and (b) contact angle tests.

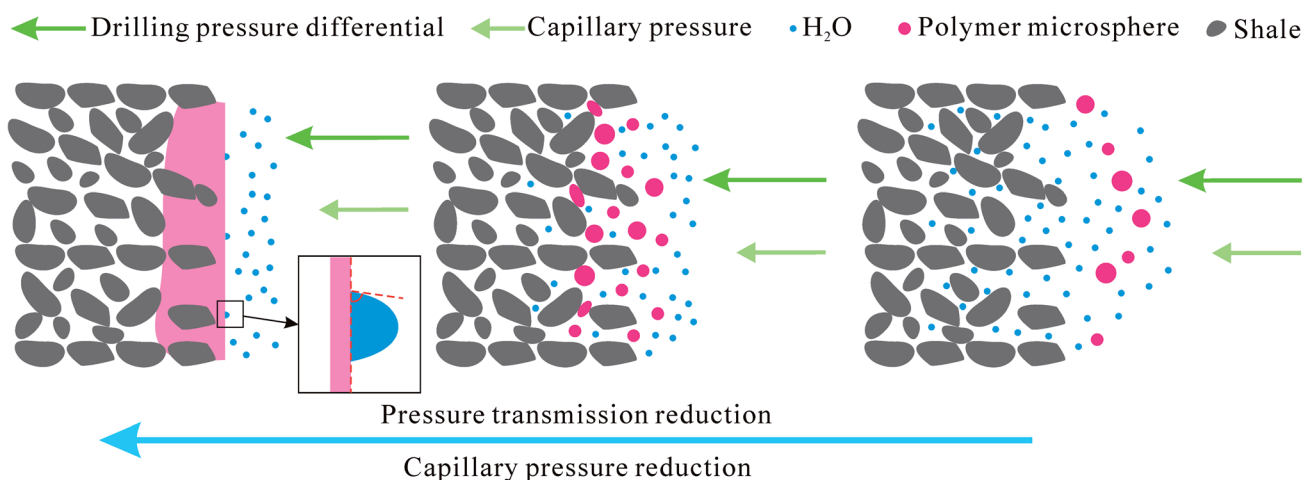


Fig. 11 The wellbore stabilizing mechanism of PME.

polymer microspheres are squeezed into the shale pores and fractures, resulting in dense-plugging. Hence, pressure transmission is retarded and the permeability of shale formations is reduced, which favor improving shale stability.³⁹ In addition, the capillary effect can be decreased *via* PME addition, thus reducing water intake into shale formations. Meanwhile, after interacting with PME, the shale surface changes to be more hydrophobic, which contributes to decreasing its affinity towards water.⁴⁰ Thus, the shale hydration potential can be effectively reduced as the invasion of water into shale formations is restricted. Therefore, PME has the potential to be an excellent shale stabilizer for WDFs used in drilling shale formations, as it undertakes the dual roles of physical plugging and shale hydration inhibition.

and 320 nm, with a D50 value of 175 nm. It was found that PME exhibited excellent salt tolerance and temperature resistance. Pressure transmission tests indicated that PME could effectively plug shale pores and reduce shale permeability. The excellent physical plugging performance of PME was further confirmed *via* SEM analysis. Rolling recovery tests showed that PME possessed better performance for inhibiting shale hydration compared with KCl and JHC. Decreasing the capillary pressure and creating a hydrophobic film could be the mechanism through which PME effectively reduces shale hydration potential. The greatest advantage of this novel shale stabilizer was that it undertook the dual roles of physical plugging and shale hydration inhibition. Based on the above research results, PME could be a promising shale stabilizer for WDFs used to drill shale formations.

4. Conclusions

In this study, a polymer microsphere emulsion (PME) as a potential shale stabilizer for WDFs was prepared and characterized. The particle size distribution of PME was between 90

Conflicts of interest

There are no conflicts to declare.



Acknowledgements

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