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## Effects of anions on the underpotential deposition behavior of Cu on polycrystalline Pt†

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The process of Cu underpotential deposition (UPD) on polycrystalline Pt (pc Pt) has been investigated by cyclic voltammetry, chronoamperometry and electrochemical impedance spectroscopy techniques using (bi)sulfate and perchlorate (with/without the addition of a small amount of NaCl) as supporting electrolytes, respectively. The results showed that the adsorption capacity of the anions influences both the reversibility and charge transfer resistance ( $R_{ct}$ ) of Cu UPD reactions on pc Pt. With a negative shift of the applied potential,  $R_{ct}$  of the (bi)sulfate system decreases monotonously, whereas  $R_{ct}$  of the perchlorate system (with/without  $Cl^-$  ions) decreases at first and then increases. Cu UPD on pc Pt follows Langmuir-type adsorption and two-dimensional nucleation/growth mechanisms. The specific adsorption anions ((bi)sulfate and chloride ions) can not only enhance the Cu UPD process by decreasing  $R_{ct}$ , but also favor instantaneous 2D nucleation and subsequent grain growth. Finally, the possible deposition mechanisms of the Cu UPD process in the presence of specific adsorption anions were proposed.

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## 1. Introduction

As an opposite concept to overpotential deposition (OPD), underpotential deposition (UPD) has received extensive research interest over many years due to its theoretical and pragmatical significance.<sup>1,2</sup> Generally, the UPD process forms a (sub)monolayer of foreign species on a substrate; therefore, it is especially sensitive to the interfacial state of the electrode/solution and electrolyte composition. Many factors involved in the UPD process (such as the temperature, substrate crystallographic orientation, deposition potential, and the type and concentration of anions or other organic additives) can significantly influence the deposition behavior of UPD species. Among these factors, the effects of anions have attracted great attention and have been extensively studied.

Anions may induce an enhanced Cu UPD process ( $Cu_{UPD}$ ) or change the electrosorption valency of  $Cu_{UPD}$  ad-atoms determined by their adsorption/desorption characteristics;<sup>3</sup> also, the formation of  $Cu_{UPD}$ -anion pairs due to anion coadsorption can reduce the coulombic repulsion generated by the partially charged  $Cu_{UPD}$  ad-atoms.<sup>3,4</sup> Specific adsorption anions (such as

$Cl^-$ ,  $Br^-$  and  $SO_4^{2-}$ ) can accelerate the UPD process due to local electrostatic effects,<sup>5,6</sup> the decrease of positive potential in the dense part of the electric double layer (EDL),<sup>7</sup> and possible deformation of the highly stable  $Cu^{2+}$  hydration shell caused by the weakly hydrated (bi)sulfate and halide anions (in contrast with perchlorate anions), which can enhance the electron transfer reaction.<sup>5,8</sup> Moreover, the halide adlayer has a significant stabilizing effect on the UPD monolayer.<sup>9</sup> The density and structure of UPD copper on Pt is definitely affected or even dominated by the electrolytic environment; the presence of  $Cl^-$  in the electrolyte causes shrinkage of the Cu–Cu distance from 0.285 nm in a pure sulfuric acid environment to 0.259 nm.<sup>10</sup>

To date, considerable studies have concentrated on UPD of Cu on monocrystalline Pt substrates, especially Pt(111)<sup>4,8,11–17</sup> and Pt(110);<sup>5,11</sup> one important aspect of this process is the effects of specific adsorption anions on the structures of the  $Cu_{UPD}$  deposits (as well as the anion coadsorption layers) and on the kinetics of the  $Cu_{UPD}$  process in acid aqueous solution. In the case of Cu UPD on polycrystalline Pt (pc Pt) substrates, previous studies mainly focused on the effects induced by nonionic additives.<sup>10,18–20</sup> Some nonionic additives (such as acetonitrile and thiourea) influence the Cu UPD processes via forming a charged copper-additive complex.<sup>10,18,19</sup> At small concentrations of acetonitrile in a copper sulfate solution ( $[ACN] \leq 4$  mM), adsorbed ACN molecules promote copper underpotential deposition (UPD) on pc Pt.<sup>19</sup> Azo-heterocyclic compounds that bind primarily through a ring nitrogen atom delay UPD processes depending on the bond strength of the adsorbed layer.<sup>20</sup> However, the effect of anions on Cu UPD on pc

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Pt substrates is also an important aspect for practical applications. Therefore, this paper aims to investigate the effects of anions on  $\text{Cu}_{\text{UPD}}$  behavior on pc Pt using cyclic voltammetry (CV), chronoamperometry (CHR), and electrochemical impedance spectroscopy (EIS) techniques.

## 2. Experimental

Cu UPD on pc Pt was studied in different aqueous solutions containing (bi)sulfate and perchlorate (with/without the addition of NaCl) ions, respectively. Copper(II) oxide (Alfa Aesar, 99.9995%, metals basis),  $\text{CuSO}_4$  (Aldrich,  $\geq 99.99\%$ , trace metals basis),  $\text{H}_2\text{SO}_4$  (Sinopharm, GR),  $\text{HClO}_4$  (Sinopharm, GR), NaCl (Aladdin, 99.99%, metals basis) and ultrapure water (Millipore Water, resistivity  $\rho \geq 18.2 \text{ M}\Omega \text{ cm}$  at  $25^\circ\text{C}$ ) were used to prepare the solutions. Unless otherwise stated, all the used ultrapure water was prepared using a Millipore-Q system (Millipore-Q Academic, Millipore, USA) whose source water was doubly distilled in our lab. Immediately before each experiment, all the glassware used was soaked in a chromic mixture overnight and then rinsed with ultrapure water, and all solutions were purged by bubbling with high-purity  $\text{N}_2$  for 30 minutes to remove dissolved oxygen.

All experiments were performed in a conventional three-compartment cell at  $30 \pm 0.1^\circ\text{C}$  controlled by a thermostatic bath. A pc Pt disk (Pine Research Instrumentation Inc., USA, 99.99%) with a geometric area of  $0.1962 \text{ cm}^2$  (the diameter of the circular working area is 5.0 mm) was used as the working electrode, a large platinum foil was used as the counter electrode, and a double liquid junction saturated calomel electrode (SCE) was used as the reference electrode in order to prevent contamination of  $\text{Cl}^-$  ions. In this paper, all the potentials are referred to SCE. Before each experiment, the pc Pt working electrode was pretreated according to the following procedure: (1) the pc Pt electrode was mechanically polished with  $0.5 \mu\text{m}$  diamond polishing paste to obtain a mirror surface and was then ultrasonically cleaned for 5 min in acetone and ultrapure water, respectively. (2) The pc Pt electrode was transferred into  $0.5 \text{ M H}_2\text{SO}_4$  to carry out electrochemical polishing ( $-0.255 \text{ V}$  to

$1.160 \text{ V}$  vs. SCE) until the normal CV profile (Fig. 1) appeared. (3) Lastly, the activated pc Pt electrode with a layer of  $0.5 \text{ M H}_2\text{SO}_4$  solution covering its surface was transferred into the working solution as quickly as possible. After each experiment, the Cu UPD layer was electrochemically stripped; then, the pc Pt electrode was pretreated again according to the above procedure but without mechanical polishing.

CV and CHR measurements were carried out using a commercial model electrochemical analyzer/workstation (CHI750D, China). EIS measurements were carried out using an impedance measurement unit (PARSTAT 2273, Advanced Electrochemical System, USA) at different potential biases after the working electrode reached a steady state ( $\sim 10$  minutes). The frequency sweep was always initiated from  $100 \text{ kHz}$  to  $10 \text{ MHz}$  with a voltage amplitude of  $5.0 \text{ mV}$ .

## 3. Results and discussion

### 3.1 Cyclic voltammetry

The cleanness of the pc Pt electrode surface was examined by performing CV cycles in  $0.5 \text{ M H}_2\text{SO}_4$  (Fig. 1). The CV profile is in accordance with that in the literature,<sup>2,21</sup> indicating a clean Pt surface. According to the electric quantity of the H adsorption region ( $H_{\text{ad}}$ ) in Fig. 1 and a theoretical value of  $210 \mu\text{C cm}^{-2}$ , the electrochemical surface area (ECSA) and roughness factor (rf) of the pc Pt electrode were calculated to be  $0.3728 \text{ cm}^{-2}$  and 1.9 (all the calculations involving the electrode area refer to the apparent area unless otherwise specified), respectively.

Fig. 2 shows the voltammograms for Cu deposition on pc Pt in  $1.0 \text{ mM Cu}^{2+}$  solutions containing different anions (the CV characteristics of pc Pt in the  $5.0 \text{ mM Cu}^{2+}$  solutions showed similar behavior to those in the  $1.0 \text{ mM Cu}^{2+}$  solutions; therefore, they are not shown here). The potential scan always started in the negative direction, and the potential range was between  $0.650 \text{ V}$  and  $-0.225 \text{ V}$ . In Fig. 2, peak A and B are designated as the bulk deposition and stripping process of Cu deposits, respectively; meanwhile, the enlarged UPD peaks are shown in the insets. The different CV profiles (Fig. 2a–e) reflect significant distinctions of inter-atomic forces between the Cu–Cu and Cu–Pt bondings as well as the distinct energy states of different active sites on the pc Pt surface. From Fig. 2, the potential ranges of the OPD and UPD stripping peaks cover around  $100 \text{ mV}$  and  $500 \text{ mV}$ , respectively. Meanwhile, it can also be observed that OPD and its stripping peaks are generally unimodal, whereas UPD and its stripping peaks usually display some humps or broad curves.

Under the conditions of identical  $\text{Cu}^{2+}$  concentrations, anions exert prominent impacts on both the OPD and UPD processes. With regard to OPD, peaks A and B for the (bi)sulfate supporting electrolyte (Fig. 2a) both appear at more negative potentials than that for the perchlorate supporting electrolyte (Fig. 2b), and the peak current densities of the former are smaller than the latter; this suggests that Cu bulk deposition is more facile in the perchlorate supporting electrolyte. The above phenomena can be attributed to the weaker coordination and adsorption capacity of perchlorate with respect to (bi)sulfate. With increasing  $\text{Cl}^-$  ions concentration in perchlorate

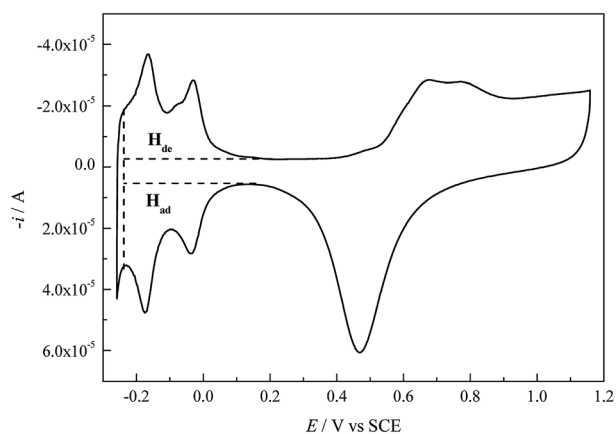
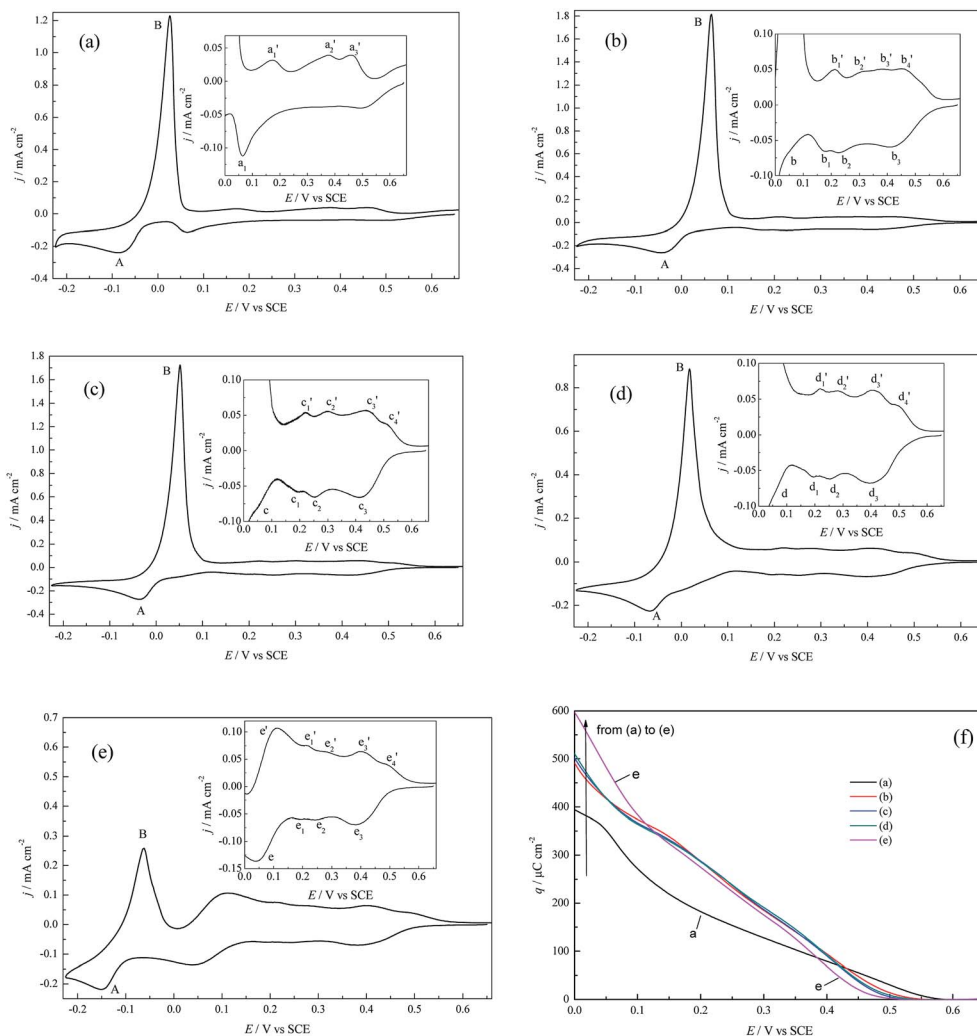


Fig. 1 CV profile obtained for the pc Pt electrode in  $0.5 \text{ M H}_2\text{SO}_4$  solution at a scan rate ( $v$ ) of  $100 \text{ mV s}^{-1}$ .





**Fig. 2** CV profiles for Cu deposition on pc Pt in (a) 0.5 M  $\text{H}_2\text{SO}_4$  + 1.0 mM  $\text{CuSO}_4$ , (b) 0.5 M  $\text{HClO}_4$  + 1.0 mM  $\text{Cu}(\text{ClO}_4)_2$ , (c) 0.5 M  $\text{HClO}_4$  + 1.0 mM  $\text{Cu}(\text{ClO}_4)_2$  + 1.0 mM NaCl, (d) 0.5 M  $\text{HClO}_4$  + 1.0 mM  $\text{Cu}(\text{ClO}_4)_2$  + 10 mM NaCl, and (e) 0.5 M  $\text{HClO}_4$  + 1.0 mM  $\text{Cu}(\text{ClO}_4)_2$  + 50 mM NaCl.  $v = 30 \text{ mV s}^{-1}$ . The insets show partial enlarged details of the UPD region. (f) The UPD charge density ( $q$ ) variation as a function of the applied potentials ( $E$ ) (the calculations refer to the ECSA), estimated by integrating the voltammograms in Fig. 2a–e.

electrolyte (Fig. 2b–e), the peak potentials of A and B shift negatively and the corresponding peak current densities decrease, whilst the peak shapes experience a gradual change. The above results can be attributed to the strong specific adsorption of  $\text{Cl}^-$  and the complexation of  $\text{Cl}^-$  with  $\text{Cu}^{2+}$  species at higher  $\text{Cl}^-$  concentrations.<sup>22</sup>

For the UPD process, the CV profiles are much more complicated than for the OPD process; this is attributed to the fact that pc Pt is composed of different crystallographic planes, crystal defects and grain boundaries, and therefore different active sites are in strikingly different energetic states.<sup>23</sup> In (bi) sulfate supporting electrolyte (Fig. 2a), there is only one UPD peak and three stripping peaks, which agrees well with the studies of Alonso *et al.*<sup>24</sup> and also indicates the irreversibility of the Cu UPD process. However, obviously different CV profiles appear in perchlorate supporting electrolyte, and at least three UPD peaks and four stripping humps/peaks appear. For example, in Fig. 2c, in the assignments of UPD and its stripping

peaks, peak  $c_1$  should correspond to  $c'_1$ , peak  $c_2$  to  $c'_2$ , and peak  $c_3$  to  $c'_3$  and  $c'_4$ . In the case of the perchlorate supporting electrolyte and  $\text{Cl}^-$  concentration  $c(\text{Cl}^-) \leq 10 \text{ mM}$  (Fig. 2b–d), the addition of  $\text{Cl}^-$  results in more distinct UPD stripping humps and shifts the UPD peak positions towards more positive potentials, suggesting that the  $\text{Cu}_{\text{UPD}}$  process tends to be more facile; however, when  $c(\text{Cl}^-)$  increases to 50 mM, the boundaries of the UPD humps become inconspicuous and peak e becomes more significant (Fig. 2e).

Fig. 2f shows the variation of the charge density ( $q$ ) as a function of the applied potential ( $E$ ). It can be observed that the UPD onset potential is *ca.* 0.56 V for (bi)sulfate electrolyte and *ca.* 0.50 V for perchlorate electrolyte containing 50 mM  $\text{Cl}^-$ ; for  $q$ , slight differences can be observed for the perchlorate electrolytes containing lower  $\text{Cl}^-$  concentrations (0 to 10 mM). In addition, it is interesting to note that the magnitude of  $q$  follows the order of  $q((\text{bi})\text{sulfate}) > q(\text{perchlorate}) > q(\text{chloride})$  in the higher potential region (0.43 V to 0.5 V), while the order is



$q(\text{chloride}) > q(\text{perchlorate}) > q(\text{(bi)sulfate})$  in the lower potential region (0.05 V to 0.0 V). Furthermore, almost a full Cu monolayer is completed prior to 0.00 V for perchlorate electrolyte with or without  $\text{Cl}^-$  according to the  $q$ - $E$  relationships (Fig. 2f) (hypothesizing the theoretical charge density needed to form a full Cu monolayer of  $420 \mu\text{C cm}^{-2}$ ), which is similar to that of Cu UPD on polycrystalline Au.<sup>25</sup> The differences in  $q$  between the (bi)sulfate and perchlorate (with or without  $\text{Cl}^-$ ) systems may synchronously result from the following factors: (1) stronger inductive effects (such as a stronger local electrostatic effect,<sup>5,6</sup> greater potential decrease in the dense part of EDL,<sup>7</sup> possible greater deformation of the hydrated  $\text{Cu}^{2+}$  hydration shell<sup>5,8</sup>), and more favorable replacement of (bi)sulfate with  $\text{Cu}_{\text{UPD}}$  ad-atoms than perchlorate.<sup>26</sup> (2) Both the different lattice structures in different supporting electrolytes and the different specific adsorption capacities of (bi)sulfate and chloride ions on pc Pt, as well as the complexation of  $\text{Cu}^{2+}$  species with  $\text{Cl}^-$  ions, especially at higher  $\text{Cl}^-$  concentrations. (3) The influence of the electrode potential on the rate and mechanisms of  $\text{Cu}^{2+}$  charge transfer as well as the desorption rate of the pre-adsorbed anions. For example, in the lower potential region, the perchlorate electrolyte system of 50 mM  $\text{Cl}^-$  shows the largest  $q$ , which may arise from the transition of charge transfer mechanisms due to the complexation of  $\text{Cl}^-$  ions with  $\text{Cu}^{2+}$ , such as the transition from single electron transfer ( $\text{Cu}^{2+} + e \rightarrow \text{Cu}^+$ ,  $\text{Cu}^+ + e \rightarrow \text{Cu}$ ) to electron transfer coupled with comproportionation ( $\text{Cu}^+ + \text{Cu}^+ \rightarrow \text{Cu} + \text{Cu}^{2+}$ ). Shao and his coworkers<sup>22</sup> also reported that the transition between two different mechanisms (direct two-step reduction and the chloride-mediated route) depends on the amount of chloride ions for Cu OPD.

### 3.2 EIS measurements

With regard to the UPD process, the current density ( $j_{\text{UPD}}$ ) can be expressed as a function of the electrode potential ( $E$ ), state variables of the electrode surface ( $X_i$ ), and the surface concentration of UPD species ( $C_k^s$ ),<sup>27</sup>

$$j_{\text{upd}} = f(E, X_i, C_k^s) \quad (1)$$

where the subscripts  $i$  and  $k$  denote the number of state variables apart from the  $E$  and UPD species, respectively. At a small perturbation of the electrode potential, eqn (1) can be expanded using the Taylor series and leaving out the high-order terms,

$$\Delta j_{\text{upd}} = \left(\frac{\partial j_{\text{upd}}}{\partial E}\right)_{\text{ss}} \Delta E + \sum_{i=1}^x \left(\frac{\partial j_{\text{upd}}}{\partial X_i}\right)_{\text{ss}} \Delta X_i + \sum_{k=1}^y \left(\frac{\partial j_{\text{upd}}}{\partial C_k^s}\right)_{\text{ss}} \Delta C_k^s \quad (2)$$

where the subscript “ss” denotes “steady state”. Without considering the coadsorption of anions, there should be two state variables, namely the electrode potential ( $E$ ) and the coverage of UPD species ( $\theta$ ), *i.e.*  $i = 1$  and  $k = 1$ .

$$\Delta j_{\text{upd}} = \left(\frac{\partial j_{\text{upd}}}{\partial E}\right) \Delta E + \left(\frac{\partial j_{\text{upd}}}{\partial \theta}\right) \Delta \theta + \left(\frac{\partial j_{\text{upd}}}{\partial C_{\text{upd}}^s}\right) \Delta C_{\text{upd}}^s \quad (3)$$

Ragoisha's research group<sup>28,29</sup> elaborated several possible equivalent electric circuits (EECs) of EIS when studying the UPD process according to eqn (3). In brief, the right-hand side of eqn (3) indicates the current changes caused by the charge transfer resistance ( $R_{\text{ct}}$ ), adsorption capacitance ( $C_{\text{UPD}}$ ) and mass transfer impedance ( $Z_T$ ) of the UPD species from left to right, respectively. In view of the reversibility of the UPD process, it can be divided into two different situations. For reversible UPD, the mathematical model of interfacial impedance is expressed as<sup>29–31</sup>

$$Z = R_s + \left\{ Y_0(j\omega)^n + 1 / \left[ R_{\text{ct}} + (j\omega C_{\text{upd}})^{-1} + Z_T \right] \right\}^{-1} \quad (4)$$

For irreversible UPD, it can be expressed as<sup>29</sup>

$$Z = R_s + [Y_0(j\omega)^n + 1 / (R_{\text{ct}} + Z_T)]^{-1} \quad (5)$$

where  $R_s$  is the solution resistance. The double layer capacitance is represented by the constant phase-angle element (CPE) because of the general “dispersion effect” for solid electrodes; it is given by  $Z_{\text{dl}} = Y_0^{-1}(j\omega)^{-n}$ , where  $Y_0$  has the dimensions of capacitance related to the EDL and  $n$  is a non-dimensional parameter related to the “dispersion effect”;  $R_{\text{ct}} = -1/(\partial j_{\text{upd}}/\partial E)$  is the charge transfer resistance of the UPD process; and the adsorption capacitance  $C_{\text{UPD}}$  is given by  $C_{\text{upd}} = -q_{\text{upd}}(\partial\theta/\partial E)$ , where  $q_{\text{UPD}}$  and  $\theta$  denote the charges of the full UPD monolayer and the coverage of the Cu UPD adlayer, respectively. Supposing the coadsorption of specific adsorption anions with different time constants proceeds simultaneously with the Cu UPD process, an additional branch of anion adsorption capacitance ( $\text{CPE}_a$ ) in series with the adsorption resistance ( $R_a$ ) should be added in parallel with the double layer capacitance.<sup>29,31</sup> Then, for a reversible UPD process,

$$Z = R_s + \left\{ Y_0(j\omega)^n + 1 / \left[ R_{\text{ct}} + (j\omega C_{\text{upd}})^{-1} + Z_T \right] + 1 / \left[ R_a + (j\omega C_a)^{-1} \right] \right\}^{-1} \quad (6)$$

For an irreversible UPD process,

$$Z = R_s + \left[ Y_0(j\omega)^n + 1 / (R_{\text{ct}} + Z_T) + 1 / \left[ R_a + (j\omega C_a)^{-1} \right] \right]^{-1} \quad (7)$$

Potentiodynamic electrochemical impedance spectroscopy (PDEIS) has been applied to study UPD kinetics, of which the ac response must be confined to a limited frequency range while leaving out certain EEC elements, such as mass transfer impedance at low or infralow frequencies.<sup>29</sup> In this study, we adopted the classical EIS technique and decomposed the ac response through the whole EEC in the frequency range between 100 kHz and 10 mHz as much as possible.

**3.2.1 Cu UPD in (bi)sulfate electrolyte.** Fig. 3a–c show the EIS plots for Cu UPD on pc Pt in 1.0 mM  $\text{CuSO}_4$  + 0.5 M  $\text{H}_2\text{SO}_4$  aqueous solution at different applied potentials. The Nyquist diagram (Fig. 3a) is composed of two parts: a high-frequency capacitive arc and a low-frequency oblique line which slightly resembles a large arc. The EIS data shown in Fig. 3a–c were





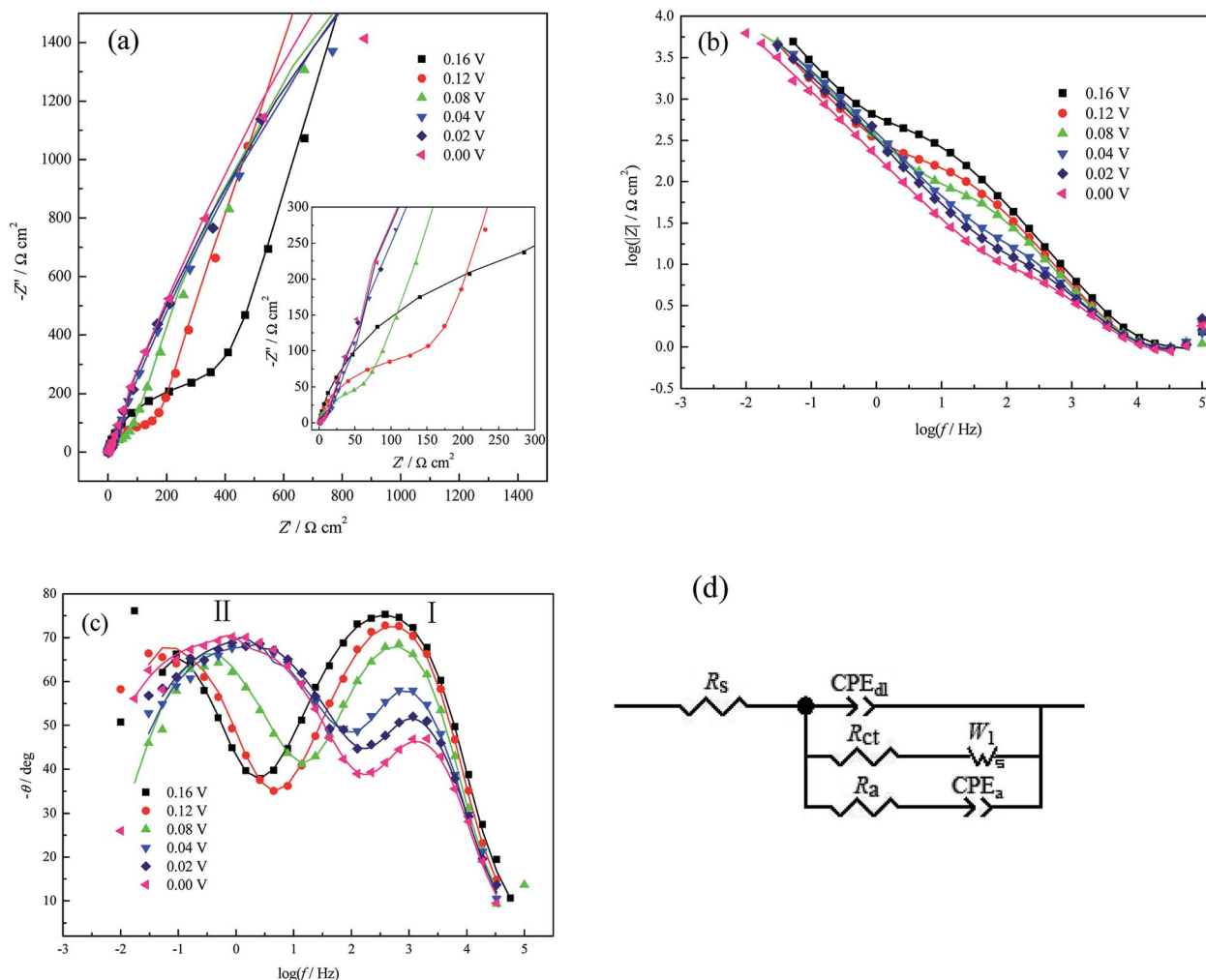


Fig. 3 EIS plots for Cu UPD on pc Pt in 1.0 mM  $\text{CuSO}_4 + 0.5 \text{ M H}_2\text{SO}_4$  at different potential bias containing both the experimental (symbols) and the fitting results (solid lines). (a) Nyquist plot (inset: enlarged details in the high frequency (HF) range), (b) and (c) Bode plots, and (d) EEC used to fit the impedance data.

fitted with ZView software based on the principle of nonlinear least squares (NLLS fit). The EEC used to fit the impedance data (Fig. 3d) was proposed according to the following considerations: (1) due to the irreversibility of Cu UPD (according to the CV features in Fig. 2a) and the oblique line in the low-frequency region of the Nyquist diagram (Fig. 3a), a branch of charge transfer resistance in series with semi-infinite diffusion impedance was added in parallel with the double layer capacitance. (2) The strong coadsorption of (bi)sulfate in the Cu UPD process is well known. Additionally, the deviation of the

inclination angles of the oblique line (Fig. 3a), symbolizing diffusion impedance from  $\pi/4$ , also demonstrated that the UPD process was affected by other surface state variables (for example, the coverage of the Cu UPD adlayer and (bi)sulfate) in addition to the applied potentials.<sup>27</sup> Thus, an additional branch of adsorption resistance in series with the adsorption capacitance of (bi)sulfate was added in parallel with the double layer capacitance (Fig. 3d). The best fitting parameters are shown in Table 1.

Table 1 EIS fitting results for Cu UPD on pc Pt in 1.0 mM  $\text{CuSO}_4 + 0.5 \text{ M H}_2\text{SO}_4$  solution

$E$ (V)	$R_s$ ( $\Omega \text{ cm}^2$ )	$CPE_{dl} \cdot T$ ( $\mu\text{F cm}^{-2}$ )	$CPE_{dl} \cdot P$	$R_{ct}$ ( $\Omega \text{ cm}^2$ )	$W_1 \cdot R$ ( $\Omega \text{ cm}^2$ )	$R_a$ ( $\Omega \text{ cm}^2$ )	$CPE_a \cdot T$ ( $\mu\text{F cm}^{-2}$ )	$CPE_a \cdot P$
0.16 V	0.921	51.779	0.906	377.881	15 915.744	738.104	337.151	0.912
0.12 V	0.846	58.588	0.916	143.069	15 685.405	265.459	595.158	0.884
0.08 V	0.922	55.708	0.927	23.878	9705.425	95.844	565.240	0.802
0.04 V	0.895	60.112	0.927	13.134	11 956.428	19.973	548.012	0.769
0.02 V	0.890	40.004	0.962	6.530	11 519.294	11.256	673.853	0.778
0.00 V	0.852	42.203	0.967	6.263	17 243.233	7.913	1098.012	0.778



With the negative shift of the applied potentials from 0.16 V to 0.0 V, the diameters of both the high-frequency arc (Fig. 3a) and the impedance module (Fig. 3b) decrease. The frequency of peak I in the Bode plot (Fig. 3c) shifts towards the higher frequency region and the analyzed  $R_{ct}$  decreases monotonously (Table 1), which is similar to H UPD in 0.1 M  $H_2SO_4$  solution;<sup>32</sup> this indicates that the UPD process (nucleation/growth) is accelerated and that the formation of  $Cu_{UPD}$ -anion pairs due to (bi)sulfate coadsorption decreases the coulombic repulsion caused by the partially charged  $Cu_{UPD}$  ad-atoms.<sup>3,4</sup> Meanwhile, two phase angle peaks obviously exist in the Bode plot (Fig. 3c) at all applied potentials, which cannot be observed in PDEIS measurements to a large extent due to its limited sweep frequency range.<sup>28,33–35</sup>

The phase angle value of peak I (Fig. 3c) decreases as the applied potential bias increases (vs. open circuit potential (OCP), approximately 0.65 V), which proves that the UPD process becomes more and more nonuniform or inhomogeneous<sup>36</sup> due to the dispersive surface energetic states of pc Pt and the increasing potential bias. The increasing

inhomogeneity can also be proved by the decrease of the surface fractal dimensions  $D_f$  ( $D_f = 3 - n$  or  $D_f = 1/n + 1$ , where  $n$  is the power exponent of the constant phase element, which is  $CPE_{dl}^{-P}$  here)<sup>37,38</sup> as the applied potential bias increases. The UPD process caused a slight decrease of the  $Cu^{2+}$  concentration (or a slight concentration polarization) based on Faraday's law and the electric quantity consumed by forming a  $Cu_{UPD}$  monolayer; meanwhile, the electrode surface should be rationally composed of more  $Cu_{UPD}$  and fewer Pt atoms at a higher potential bias (vs. OCP) (Fig. 2f). In this case, because both the specific resistance and the area of Pt were smaller than those of the  $Cu_{UPD}$  layer, the activity of the residual nude Pt increased gradually with decreasing applied potential; this would certainly accelerate the diffusion process of the UPD species and consequently result in a shift of the low frequency phase angle peak II related to the diffusion process towards the higher frequency region (Fig. 3c). The EIS measurements results at 0.00 V present no sign of inductive components (the shrinkage phenomenon of the real part) in the entire frequency range, which suggests that the H UPD process (or hydrogen evolution

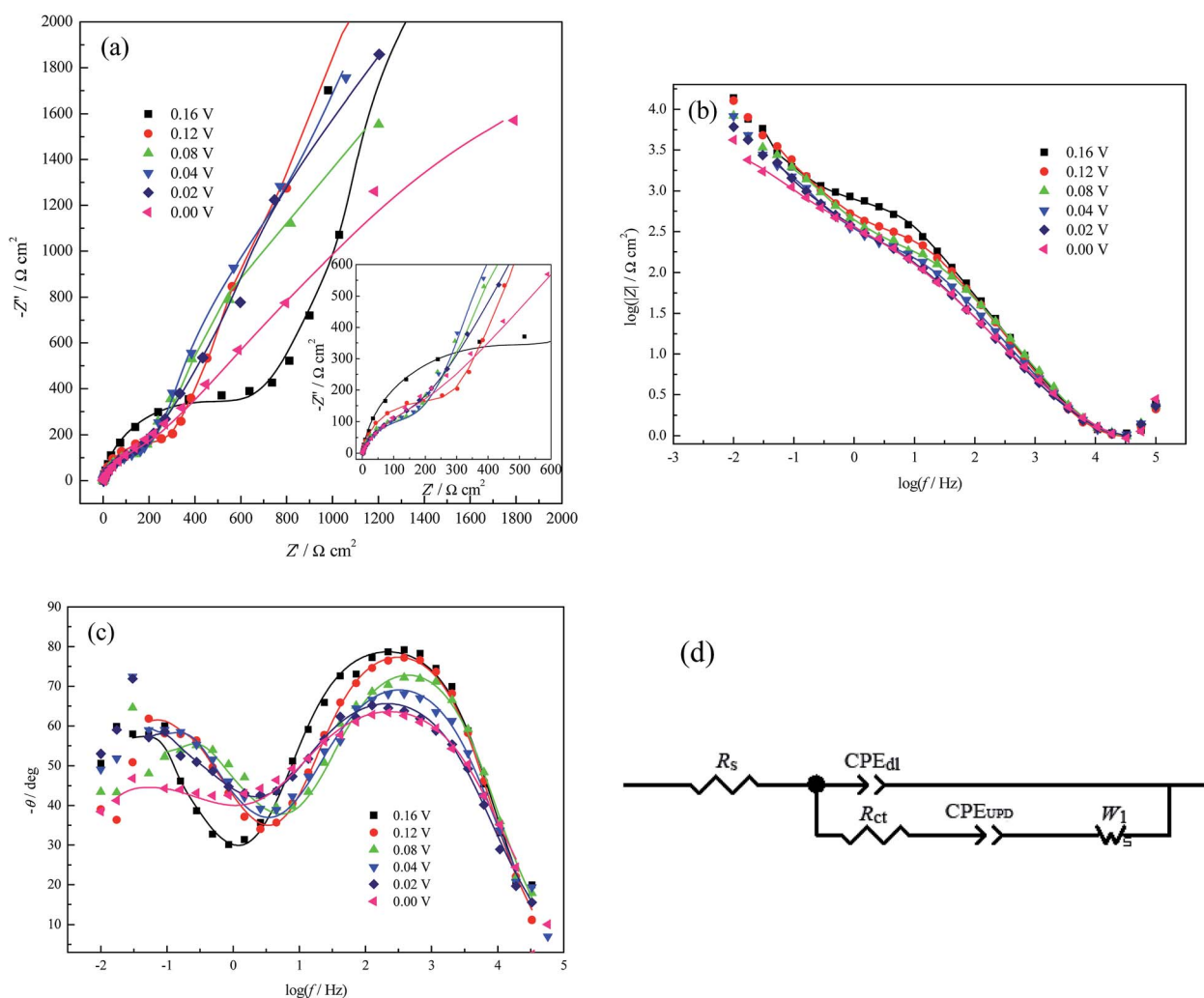


Fig. 4 EIS plots for Cu UPD at pc Pt in 1.0 mM  $Cu(ClO_4)_2 + 0.5 \text{ M } HClO_4$  at different potential biases containing both the experimental (symbols) and the fitting results (solid lines). (a) Nyquist plot (inset: enlarged details at HF), (b) and (c) Bode plots, and (d) EEC used to fit the impedance data.



Table 2 EIS fitting results for Cu UPD on pc Pt in 1.0 mM Cu(ClO<sub>4</sub>)<sub>2</sub> + 0.5 M HClO<sub>4</sub> solution

<i>E</i> (V)	<i>R</i> <sub>s</sub> (Ω cm <sup>2</sup> )	CPE <sub>dl</sub> - <i>T</i> (μF cm <sup>-2</sup> )	CPE <sub>dl</sub> - <i>P</i>	<i>R</i> <sub>ct</sub> (Ω cm <sup>2</sup> )	CPE <sub>UPD</sub> - <i>T</i> (μF cm <sup>-2</sup> )	CPE <sub>UPD</sub> - <i>P</i>	<i>W</i> <sub>1</sub> - <i>R</i> (Ω cm <sup>2</sup> )
0.16 V	0.922	49.878	0.921	718.681	843.629	0.746	275.072
0.12 V	0.914	50.177	0.929	322.749	693.323	0.761	755.174
0.08 V	0.900	60.810	0.895	197.573	1045.056	0.774	618.030
0.04 V	0.872	113.216	0.848	206.206	1595.872	0.905	790.294
0.02 V	0.873	203.252	0.797	272.129	1381.244	0.693	1132.663
0.00 V	0.783	242.243	0.769	275.465	1222.477	0.571	2811.546

reaction, HER) is suppressed by Cu UPD. This type of inhibiting phenomenon was also observed for low Cu ad-atoms coverage by Machado and his coworkers.<sup>39</sup>

The fitting results (Table 1) also show that the magnitude of CPE<sub>dl</sub>-*T* (*i.e.* *Y*<sub>0</sub> in eqn (4)) fluctuates within the measurement uncertainties and is much smaller than that of CPE<sub>a</sub>-*T*. This result agrees well with the fact that the former process takes place at the whole electrode/solution interface, while the latter may prefer some active sites for easier adsorption/desorption of (bi)sulfate. Due to the above reasons, it can also be observed that the dispersion index CPE<sub>dl</sub>-*P* (*i.e.* *n* in eqn (4)) is slightly larger than CPE<sub>a</sub>-*P*, and the former is closer to the behavior of pure capacitance. Moreover, the simultaneous increase of CPE<sub>a</sub>-*T* and the applied potential bias (Table 1) further suggests the occurrence of (bi)sulfate adsorption/desorption onto the Cu<sub>UPD</sub> surface.

**3.2.2 Cu UPD in pure perchlorate electrolyte.** Fig. 4a–c show the EIS plots for Cu UPD on pc Pt in 1.0 mM Cu(ClO<sub>4</sub>)<sub>2</sub> + 0.5 M HClO<sub>4</sub> aqueous solutions at different potential biases. Similar to the EIS plots of the (bi)sulfate system (Fig. 3), the Nyquist diagram (Fig. 4a) is also composed of a high-frequency capacitive arc and an oblique line (larger arc) appearing in the low or infralow frequency region. Meanwhile, with increasing applied potential bias, both the impedance module (Fig. 4b) and the peak height of the phase angle (Fig. 4c) decrease due to the increasingly inhomogeneous electrode surface.<sup>36</sup> Additionally, the H UPD process (or HER) is also suppressed by the Cu UPD process.

However, for pure the perchlorate electrolyte system, with increasing applied potential bias, the peak frequency of the phase angle (Fig. 4c) initially shows a tendency of a very small shift towards a higher frequency (0.08 V ≤ *E* ≤ 0.16 V), then to a lower frequency (0.00 V ≤ *E* ≤ 0.08 V); this indicates that the Cu UPD process becomes easier in the range of 0.08 V ≤ *E* ≤ 0.16 V and more difficult in the range of 0.00 V ≤ *E* ≤ 0.08 V, similar to a recent report.<sup>31</sup> The more difficult UPD process at a larger potential bias may be caused by strong lateral interactions among the partially charged Cu ad-atoms; this can be verified by the *q*-*E* dependence (Fig. 2f), where Cu ad-atoms have already reached a relatively large coverage at 0.08 V (~0.926 monolayer).

The deviation of the inclination angles of the diffusion impedance (Fig. 4a) from π/4 suggests that the Cu UPD process is affected by other surface state variables in addition to the applied potentials.<sup>27</sup> However, due to the weak adsorption capacity of perchlorate depicted above, the deviation should be

mainly attributed to the coverage of the Cu UPD adlayer. Therefore, when simultaneously considering the weak adsorption capacity of perchlorate and the relative reversibility of Cu UPD in the range of 0.00 V ≤ *E* ≤ 0.50 V (Fig. 2b, according to the potential difference between the reduction and oxidation peaks<sup>40</sup>), the EEC model (Fig. 4d) proposed by Huang and his coworkers for Cu UPD on polycrystalline Pd<sup>30</sup> was adopted to analyze the EIS data in Fig. 4a–c; the best fitting results are listed in Table 2.

From Table 2, *R*<sub>ct</sub> initially decreases and then increases with increasing applied potential bias, which is consistent with the variation of the peak frequency of the phase angle (Fig. 4c). Higher values of *R*<sub>ct</sub> are observed in HClO<sub>4</sub> solution than in H<sub>2</sub>SO<sub>4</sub> solution (Tables 1 and 2), which indicates that the Cu UPD rate in HClO<sub>4</sub> solution is slower. This phenomenon is consistent with that observed by Łosiewicz and his coworkers;<sup>32</sup> they also found that H UPD in H<sub>2</sub>SO<sub>4</sub> solutions is faster than that in HClO<sub>4</sub> solutions. CPE<sub>dl</sub>-*T* is much smaller than CPE<sub>UPD</sub>-*T*, whilst both CPE<sub>dl</sub>-*T* and CPE<sub>UPD</sub>-*T* (the fluctuations of their values are within the measurement uncertainties) increase with increasing applied potential bias. The former may be caused by the following synergistic effects: (1) the adsorption capacity of perchlorate is much weaker than that of (bi)sulfate, as proved by the *q*-*E* dependence (Fig. 2f), so the Cu UPD process occurs more readily in the perchlorate system with increasing applied potential bias; (2) the strong lateral interactions between the partially charged Cu ad-atoms in the perchlorate system (depicted above) result in a more inhomogeneous (or rougher) electrode surface than the (bi)sulfate system, which can be verified by the decrease of CPE<sub>dl</sub>-*P* (Table 2). Meanwhile, CPE<sub>dl</sub>-*T* may also be interpreted as the charge–discharge process of the whole electrode/solution interface; however, CPE<sub>UPD</sub>-*T* only represents the faradaic pseudo-capacitance occurring at the active sites of the pc Pt surface.

It should be mentioned that the EEC model in Fig. 4d omitting CPE<sub>UPD</sub> and *W*<sub>1</sub> was used to fit the PDEIS data<sup>31</sup> when using PDEIS to study Cu UPD on Pt. The obtained *R*<sub>ct</sub> values are much larger than those in this paper. The above discrepancies may result from both the dynamic potential scan in the PDEIS measurements and the Cu<sup>2+</sup> concentration difference.

**3.2.3 Cu UPD in perchlorate electrolyte with the addition of Cl<sup>−</sup> ions.** Fig. 5a–c show the EIS plots for Cu UPD on pc Pt in 1.0 mM Cu(ClO<sub>4</sub>)<sub>2</sub> + 0.5 M HClO<sub>4</sub> + 1.0 mM NaCl aqueous solution at different potential biases; the characteristics (including the evolution features of the EIS plots with the applied potential bias) are very similar to those of the pure



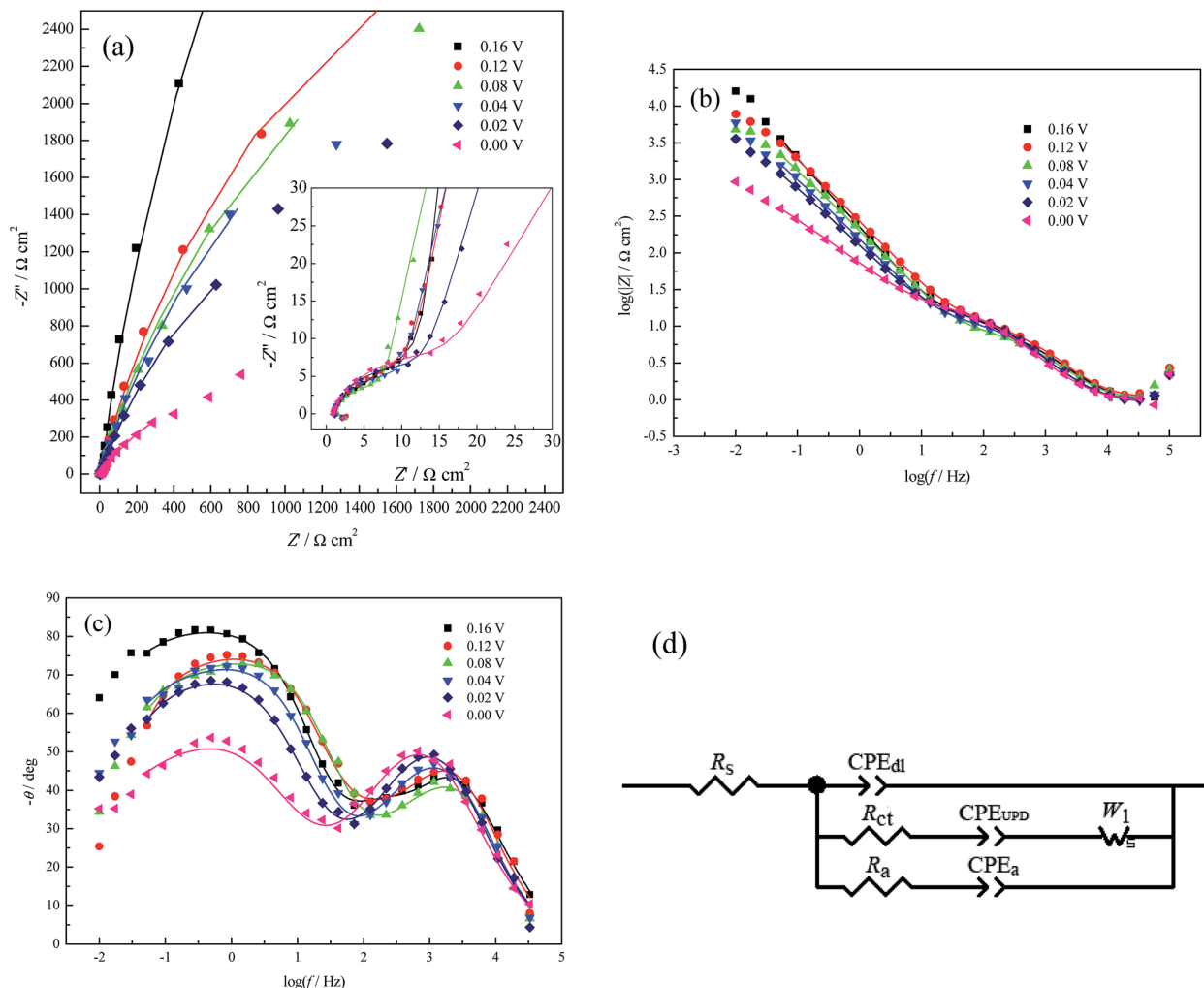


Fig. 5 EIS plots for Cu UPD on pc Pt in 1.0 mM  $\text{Cu}(\text{ClO}_4)_2$  + 0.5 M  $\text{HClO}_4$  + 1.0 mM  $\text{NaCl}$  at different potential biases containing both the experimental (symbols) and the fitting results (solid lines). (a) Nyquist plot (inset: enlarged details at HF), (b) and (c) Bode plots, and (d) EEC used to fit the impedance data.

perchlorate system, except that the inclination angles of the diffusion impedance further deviate from  $\pi/4$  (insets in Fig. 4a and 5a) due to the comparatively stronger adsorption of  $\text{Cl}^-$  (than  $\text{ClO}_4^-$ ). Markovic and his coworkers<sup>11</sup> also reported that the specific adsorption capacity of anions at the Pt surface is in the order of chloride > (bi)sulfate > perchlorate, and the bond strength follows the order of  $\text{Cl}^-$ -Pt >  $\text{SO}_4^{2-}$ -Pt >  $\text{ClO}_4^-$ -Pt. When simultaneously considering the reversibility of the Cu

UPD process (according to the potential difference between the reduction and oxidation peaks<sup>40</sup> in Fig. 2c) and the strong specific adsorption of  $\text{Cl}^-$  on pc Pt, the EEC model shown in Fig. 5d was adopted to analyze the EIS data. Table 3 lists the best fitting results.

From Table 3,  $R_{\text{ct}}$  initially decreases and then increases with increasing applied potential bias. This variation trend of  $R_{\text{ct}}$  is very similar to that in a pure perchlorate electrolyte bath (Table

Table 3 EIS fitting results for Cu UPD on pc Pt in 1.0 mM  $\text{Cu}(\text{ClO}_4)_2$  + 0.5 M  $\text{HClO}_4$  + 1.0 mM  $\text{NaCl}$  solution

$E$ (V)	$R_s$ ( $\Omega \text{ cm}^2$ )	$\text{CPE}_{\text{dl}} \cdot T$ ( $\mu\text{F cm}^{-2}$ )	$\text{CPE}_{\text{dl}} \cdot P$	$R_{\text{ct}}$ ( $\Omega \text{ cm}^2$ )	$\text{CPE}_{\text{UPD}} \cdot T$ ( $\mu\text{F cm}^{-2}$ )	$\text{CPE}_{\text{UPD}} \cdot P$	$W_1 \cdot R$ ( $\Omega \text{ cm}^2$ )	$R_a$ ( $\Omega \text{ cm}^2$ )	$\text{CPE}_a \cdot T$ ( $\mu\text{F cm}^{-2}$ )	$\text{CPE}_a \cdot P$
0.16	0.926	119.893	0.850	13.065	82.768	0.906	63 060.642	17.162	590.826	0.950
0.12	1.052	80.459	0.887	11.674	349.725	0.720	6876.810	20.424	359.516	0.938
0.08	1.055	28.836	0.997	3.588	538.481	0.666	2505.866	10.614	558.716	0.922
0.04	0.925	75.474	0.918	4.573	624.720	0.601	1235.079	13.987	811.009	0.914
0.02	0.950	142.961	0.864	14.697	605.861	0.526	1988.487	17.020	1202.548	0.866
0.00	0.929	280.133	0.810	26.153	1980.581	0.784	1146.200	36.297	2482.875	0.463





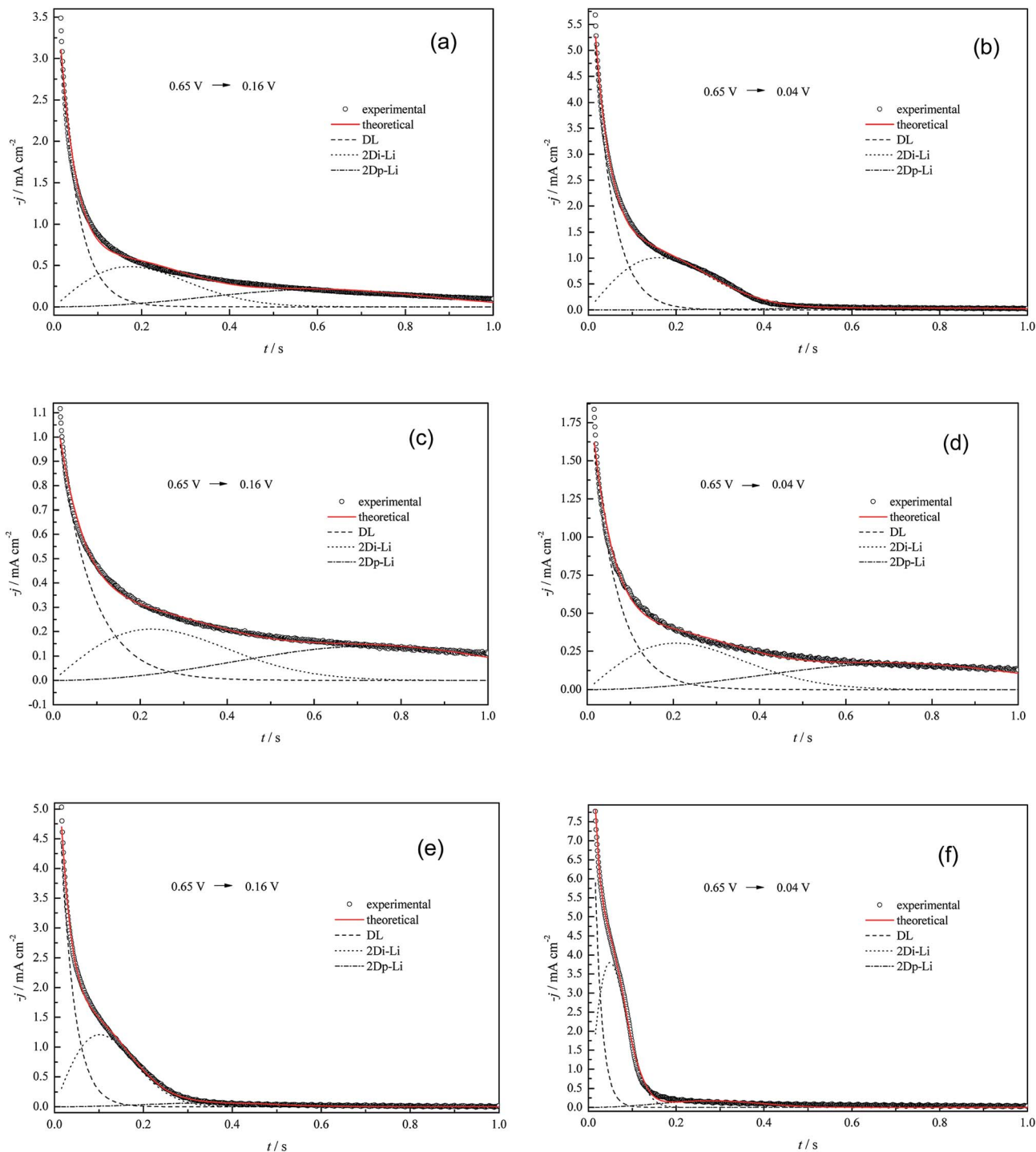


Fig. 6 Experimental current density transients recorded for Cu UPD at pc Pt in (a) and (b) 5.0 mM  $\text{CuSO}_4$  + 0.5 M  $\text{H}_2\text{SO}_4$ , (c) and (d) 5.0 mM  $\text{Cu}(\text{ClO}_4)_2$  + 0.5 M  $\text{HClO}_4$ , (e) and (f) 5.0 mM  $\text{Cu}(\text{ClO}_4)_2$  + 0.5 M  $\text{HClO}_4$  + 1.0 mM  $\text{NaCl}$ , and theoretical non-linear fitting with eqn (15) at some selected potentials. Other current density transients with non-linear fitting results shown in the ESI (Fig. S1–S3†).

2); the reason for this has been elucidated in Section 3.2.2. However, this variation trend of  $R_{\text{ct}}$  is very different from that in (bi)sulfate electrolyte (Table 1), which can be attributed to the different effects of perchlorate and (bi)sulfate ions on the Cu UPD process. Table 3 also clearly shows that  $R_{\text{ct}}$  is slightly smaller than  $R_{\text{a}}$ , indicating more facile adsorption of  $\text{Cu}_{\text{UPD}}$

adatoms than  $\text{Cl}^-$  ions. From Table 3,  $\text{CPE}_{\text{dl}}-T$  is much smaller than both  $\text{CPE}_{\text{UPD}}-T$  and  $\text{CPE}_{\text{a}}-T$ ; this is because  $\text{CPE}_{\text{dl}}-T$ ,  $\text{CPE}_{\text{UPD}}-T$  and  $\text{CPE}_{\text{a}}-T$  originate from the whole electrode/solution interface, the fast charge transfer reaction (*i.e.* pseudo-capacitance) and the strong adsorption/desorption of  $\text{Cl}^-$  ions at the active sites, respectively.



### 3.3 Potentiostatic current transient measurements

The aim of this section is to investigate the effects of anions ( $\text{SO}_4^{2-}$ ,  $\text{ClO}_4^-$  and  $\text{Cl}^-$ ) on the nucleation and growth features of the Cu UPD process, and solutions containing 5.0 mM  $\text{Cu}^{2+}$  with specific anions were chosen to perform chronoamperometric (CHR) experiments (Fig. 6). Additionally, in order to avoid the pre-adsorption of dissolved oxygen species and Cu UPD adatoms, the potential for the remaining CHR tests was selected as 0.65 V. Potentiostatic current density transients were obtained by voltage stepping from the rest potential to the UPD potentials.

There are two typical differences between the “ $j$ - $t$ ” curves of different electrolyte systems (Fig. 6). One is that an obvious shoulder peak always exists for all the “ $j$ - $t$ ” curves obtained in the perchlorate electrolyte system containing 1.0 mM  $\text{Cl}^-$  ions, whereas this peak does not appear in the pure perchlorate electrolyte system or only exists at higher potential biases for the (bi)sulfate electrolyte system. The other difference is that the current density (after the initial marked drop, which is simultaneously related to charging of the adsorption pseudo-capacitance, *i.e.* the discharging of copper ions in the copper electrodeposition process,<sup>41,42</sup> or the shoulder peak) is much larger than zero for the pure perchlorate electrolyte system, whereas it always levels off to zero for the perchlorate electrolyte system containing 1.0 mM  $\text{Cl}^-$  ions or for the (bi)sulfate electrolyte system at higher potential biases (the critical potential is *ca.* 0.04 V).

Currently, it is widely accepted that the UPD process generally follows the two-dimensional (2D) nucleation/growth mechanism.<sup>43,44</sup> According to the  $j_p$ - $v^{1/2}$  relationship in Fig. 7, linear fitting results reveal that the rate-controlling step of Cu UPD with diffusion control was converted to non-diffusion control as a result of the increase of the  $\text{Cu}^{2+}$  concentration from 1.0 mM to 5.0 mM. On the other hand, based on the fact that the formation of even an integrated  $\text{Cu}_{\text{UPD}}$  monolayer only consumes  $8.11 \times 10^{-7}$  mol  $\text{Cu}^{2+}$  in our experimental conditions (hypothesizing a two-electron transfer mechanism), the Cu UPD process should be mostly controlled by charge transfer.

Therefore, the theoretical models proposed by Bewick–Fleischmann–Thirsk (BFT) were adopted to analyze the current density transients shown in Fig. 6. In the BFT model, the overlapping effects between crystal nuclei are taken into consideration, and the growth of the 2D circular island nuclei proceeds with lattice incorporation of adatoms into the periphery of the growing nuclei as the rate-controlling step.<sup>45,46</sup> According to the BFT model, the nucleation/growth current densities of 2D instantaneous nucleation (2Di-Li) and 2D progressive nucleation (2Dp-Li) are given by the following equations, respectively.<sup>25,45,46</sup>

$$j_{2\text{Di-Li}}(t) = k_1 t \exp(-k_2 t^2) \quad (8)$$

$$j_{2\text{Dp-Li}}(t) = k_3 t^2 \exp(-k_4 t^3) \quad (9)$$

where  $k_1 = 2\pi z F M h N_0 k_g^2 / \rho$ ,  $k_2 = \pi N_0 M^2 k_g^2 / \rho^2$ ,  $k_3 = \pi z F M h A N_0 k_g^2 / \rho$ , and  $k_4 = \pi A N_0 M^2 k_g^2 / (3\rho^2)$ ;  $zF$  denotes the molar charge transferred during the deposition process ( $\text{C mol}^{-1}$ );  $M$  is the atomic weight ( $\text{g mol}^{-1}$ );  $h$  is the layer height ( $\text{cm}$ );  $N_0$  is the number density of active sites ( $\text{cm}^{-2}$ );  $k_g$  is the lateral growth rate constant ( $\text{mol cm}^{-2} \text{s}^{-1}$ );  $t$  is the deposition time ( $\text{s}$ );  $\rho$  is the density of the deposit ( $\text{g cm}^{-3}$ ); and  $A$  is the nucleation rate constant ( $\text{s}^{-1}$ ).

The deposition process should accompany the deposition/dissolution of metal ions/metal adatoms, namely, the copper ion discharge process. Milchev *et al.*<sup>41,42</sup> have shown that discharge of the copper ions takes place in two steps:



Meanwhile, assuming that the deposition/dissolution of a (sub)monolayer at defect sites mostly resembles a Langmuir-type adsorption/desorption process, the current density can be expressed as:<sup>41–43,45,47</sup>

$$j_{\text{ad}}(t) = k_5 \exp(-k_6 t) \quad (12)$$

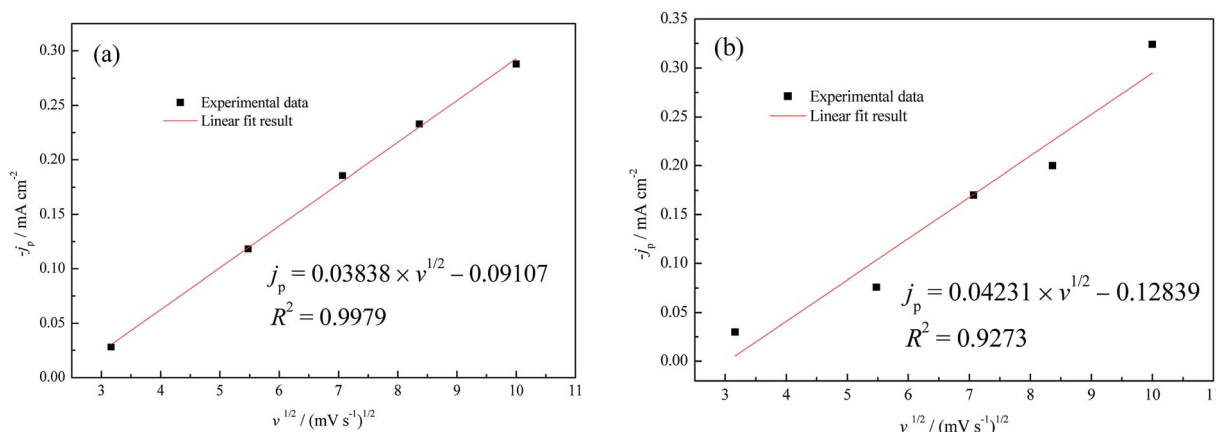


Fig. 7 UPD peak maxima  $j_p$  of CV in (a) 0.5 M  $\text{H}_2\text{SO}_4$  + 1.0 mM  $\text{CuSO}_4$ , (b) 0.5 M  $\text{H}_2\text{SO}_4$  + 5.0 mM  $\text{CuSO}_4$  as a function of the square root of the scan rate ( $v$ ).



For the deposition of metal ions associated with a charge transfer,<sup>43</sup>

$$k_6 = k_a^0 \exp[-(1 - \beta)nFE/RT] \quad (13)$$

For the dissolution of metal adatoms,<sup>43</sup>

$$k_6 = k_d^0 \exp(\beta nFE/RT) \quad (14)$$

where  $k_6$  is assumed to follow the Butler-Volmer relation,  $\beta$  is the transfer coefficient, and  $k_a^0$  and  $k_d^0$  denote the standard rate constants of the deposition and dissolution processes, respectively. Thus, in consideration of the Langmuir-type adsorption/desorption process proceeding in parallel with the nucleation and growth process of Cu UPD on pc Pt, the total current density transient should be theoretically decomposed into three parts: double layer charging accompanied by faradaic pseudo-capacitance, two-dimensional instantaneous nucleation (2Di-Li) and two-dimensional progressive nucleation (2Dp-Li):

$$j_{\text{total}}(t) = j_{\text{ad}}(t) + j_{2\text{Di-Li}}(t) + j_{2\text{Dp-Li}}(t) \quad (15)$$

The experimental current density transients were deconvolved by non-linear fitting with eqn (15), and the fitted lines are

also shown in Fig. 6. Based on the best fitting parameters  $k_1$  to  $k_6$  (shown in the ESI of this paper, Tables S1–S3†), the electric quantities of the different contributions ( $Q_{\text{ad}}$ ,  $Q_{2\text{Di-Li}}$  and  $Q_{2\text{Dp-Li}}$ ) were calculated according to expressions (16)–(18)<sup>25</sup> and are listed in Tables 4–6

$$k_5 = Q_{\text{ad}}k_6 \quad (16)$$

$$k_1 = 2Q_{2\text{Di-Li}}k_2 \quad (17)$$

$$k_3 = 3Q_{2\text{Dp-Li}}k_4 \quad (18)$$

In eqn (16)–(18) and Tables 4–6,  $Q_{\text{ad}}$ ,  $Q_{2\text{Di-Li}}$  and  $Q_{2\text{Dp-Li}}$  are the charge densities of adsorption, 2D instantaneous nucleation/growth and progressive nucleation/growth, respectively;  $Q_{\text{nucl}} = Q_{2\text{Di-Li}} + Q_{2\text{Dp-Li}}$ ,  $Q_{\text{total}} = Q_{\text{ad}} + Q_{\text{nucl}}$ ;  $q_{\text{ad}}$  and  $q_{\text{nucl}}$  are the contributions of adsorption and nucleation to the total charge density, respectively.

For Cu UPD in the above three systems,  $Q_{\text{total}}$  always increases with increasing applied potential bias (Tables 4–6). However, comparing the values of  $Q_{\text{total}}$ ,  $Q_{\text{ad}}$  and  $q_{\text{ad}}$  of different systems, it is interesting to observe that all of them are directly related to the anionic specific adsorption capacity. Briefly, the stronger the adsorption capacity of the anions in the supporting

**Table 4** Charge density and proportion of different contributions to Cu UPD on pc Pt in 5.0 mM CuSO<sub>4</sub> + 0.5 M H<sub>2</sub>SO<sub>4</sub> in terms of eqn (16)–(18)

<i>E</i> (V)	<i>Q</i> <sub>ad</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>2Di-Li</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>2Dp-Li</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>nucl</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>total</sub> (μC cm <sup>−2</sup> )	<i>q</i> <sub>ad</sub> (%)	<i>q</i> <sub>nucl</sub> (%)
0.16	186.110	138.844	123.901	262.745	448.855	41.463	58.537
0.12	210.807	173.477	138.821	312.298	523.105	40.299	59.701
0.08	218.230	187.258	163.011	350.269	568.499	38.387	61.613
0.04	315.751	263.973	26.615	290.588	606.339	52.075	47.925
0.02	247.359	170.395	211.423	381.818	629.177	39.315	60.685
0.00	307.161	300.887	33.151	334.038	641.199	47.904	52.096

**Table 5** Charge density and proportion of different contributions to Cu UPD on pc Pt in 5.0 mM Cu(ClO<sub>4</sub>)<sub>2</sub> + 0.5 M HClO<sub>4</sub> in terms of eqn (16)–(18)

<i>E</i> (V)	<i>Q</i> <sub>ad</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>2Di-Li</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>2Dp-Li</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>nucl</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>total</sub> (μC cm <sup>−2</sup> )	<i>q</i> <sub>ad</sub> (%)	<i>q</i> <sub>nucl</sub> (%)
0.16	91.034	78.841	100.757	179.598	270.632	33.637	66.363
0.12	78.721	69.486	82.852	152.338	231.059	34.070	65.930
0.08	111.169	95.960	114.182	210.141	321.310	34.599	65.401
0.04	122.454	103.243	119.615	222.858	345.312	35.462	64.538
0.02	133.165	108.358	117.791	226.149	359.314	37.061	62.939
0.00	179.900	147.879	152.242	300.122	480.022	37.478	62.522

**Table 6** Charge density and proportion of different contributions for Cu UPD at pc Pt in 5.0 mM Cu(ClO<sub>4</sub>)<sub>2</sub> + 0.5 M HClO<sub>4</sub> + 1.0 mM NaCl in terms of eqn (16)–(18)

<i>E</i> (V)	<i>Q</i> <sub>ad</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>2Di-Li</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>2Dp-Li</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>nucl</sub> (μC cm <sup>−2</sup> )	<i>Q</i> <sub>total</sub> (μC cm <sup>−2</sup> )	<i>q</i> <sub>ad</sub> (%)	<i>q</i> <sub>nucl</sub> (%)
0.16	225.323	202.359	22.257	224.616	449.939	50.079	49.921
0.12	237.648	240.819	16.953	257.772	495.420	47.969	52.031
0.08	245.331	286.739	24.954	311.692	557.024	44.043	55.957
0.04	256.258	309.797	47.260	357.057	613.315	41.782	58.218
0.02	276.591	305.269	64.873	370.142	646.734	42.767	57.233
0.00	586.859	47.097	95.063	142.160	729.019	80.500	19.500



electrolyte, the larger the parameters ( $Q_{\text{total}}$ ,  $Q_{\text{ad}}$  and  $q_{\text{ad}}$ ). For the systems containing  $\text{SO}_4^{2-}$  (Table 4) and  $\text{Cl}^-$  (Table 6) ions with stronger adsorption capacity,  $Q_{2\text{Di-Li}}$  is generally larger than  $Q_{2\text{DP-Li}}$  (except at the potentials adjacent to the Nernst potential; the reason for this is under further investigation), and the differential of  $Q_{2\text{Di-Li}}$  and  $Q_{2\text{DP-Li}}$  increases with increasing anionic specific adsorption capacity. Meanwhile, for the pure perchlorate supporting electrolyte system (Table 5),  $Q_{2\text{Di-Li}}$  is always slightly smaller than  $Q_{2\text{DP-Li}}$ , and the differential of  $q_{\text{nuc}}$  and  $q_{\text{ad}}$  is significantly larger than that obtained in the systems containing  $\text{SO}_4^{2-}$  or  $\text{Cl}^-$  ions. The above results undoubtedly indicate that the process of Cu UPD on pc Pt is always coupled with adsorption and replacement of the used anions, and the anions with stronger adsorption capacity facilitate the process of instantaneous nucleation and subsequent growth. When simultaneously taking into account the results shown in Fig. 2, it is rational to consider that co-adsorbed  $\text{Cu}_{\text{UPD}}^{n+}$  – anions ( $n = 0$  to  $2$ ) of some specific structures should exist on the pc Pt surface and influence the deposition rate to some extent.

The UPD process is highly complicated, and the deposition mechanisms should be mainly related to both the spatial structures of the adsorbed anions and the electrostatic interactions of the anions with the substrate and UPD species. Based on the above results and the previous reports of Cu UPD on single crystal Pt concurrent with coadsorption of specific adsorption anions,<sup>5,8,12,13,48</sup> it is rational to deduce that Cu UPD on a pc Pt surface in the presence of specific adsorption anions may proceed *via* the following mechanisms. Firstly, before the onset potential of Cu UPD, the specific adsorption anions adsorb onto the Pt substrate and gradually translate into specific adlayers of certain lattice structures (the structures may transform along with the negative potential scan), which will also deform the hydration shell of the pre-adsorbed  $\text{Cu}^{2+}$  (some specific adsorption anions can even insert into the  $\text{Cu}^{2+}$  hydration shells) and cause a decrease of the positive potential in the dense part of the EDL region.<sup>7</sup> Meanwhile, the electrostatic interaction of the specific adsorption anions with  $\text{Cu}^{2+}$  ions causes the latter to gather in the dense part of the EDL. Secondly, when the UPD potential is suddenly applied, Cu UPD proceeds with simultaneous replacement of the adsorbed anions at certain active sites,<sup>26</sup> and some uniform structures of co-adsorbed  $\text{Cu}_{\text{UPD}}^{n+}$  – anion ( $n = 0$  to  $2$ ) may form at some critical potentials. Here, it should be mentioned that in the presence of halide ions, Pb UPD on pc Au may proceed *via* the reduction of  $\text{Pb}^{2+}$  adsorbed on the pre-adsorbed halide ions.<sup>49</sup> Finally, as the potential becomes more negative, the UPD process continues until the integrated Cu UPD monolayer is formed; this process is always coupled with the adsorption of specific adsorption anions onto the Cu UPD monolayer (a sandwiched structure), which may inhibit the continuous deposition of  $\text{Cu}^{2+}$  on the  $\text{Cu}_{\text{UPD}}$  layer, thereby stabilizing the UPD film.<sup>10,13</sup>

## 4. Conclusions

The CV plot of pc Pt in a (bi)sulfate system shows only one significant UPD peak and three corresponding stripping peaks;

this differs from the plots of perchlorate systems, which contain at least three UPD peaks and four stripping peaks. In contrast to the irreversibility of the Cu UPD process in the (bi)sulfate system, better reversibility was observed in the perchlorate system, and the reversibility was further improved by the addition of a small amount of  $\text{Cl}^-$  ions.

Anions with stronger adsorption capacity facilitate the process of 2D instantaneous nucleation and subsequent grain growth, and specific adsorption anions ((bi)sulfate and chloride) can enhance the Cu UPD process by decreasing the charge transfer resistance ( $R_{\text{ct}}$ ). With decreasing applied potential,  $R_{\text{ct}}$  of the (bi)sulfate system decreases monotonously, whereas  $R_{\text{ct}}$  shows a trend of initial decrease and subsequent increase for perchlorate systems with or without  $\text{Cl}^-$  ions. Finally, the possible mechanisms of Cu UPD on pc Pt in the presence of specific adsorption anions were proposed; these reveal the intrinsic relationships between specific adsorption anions and the Cu UPD process.

## Conflicts of interest

There are no conflicts to declare.

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