

CrossMark  
click for updatesCite this: *Chem. Sci.*, 2017, 8, 2661

# Silica-supported isolated gallium sites as highly active, selective and stable propane dehydrogenation catalysts†

Keith Searles,<sup>a</sup> Georges Siddiqi,<sup>a</sup> Olga V. Safonova<sup>b</sup> and Christophe Copéret<sup>\*a</sup>

Single-site gallium centers on the surface of silica are prepared *via* grafting of [Ga(OSi(OtBu)<sub>3</sub>)(THF)] on SiO<sub>2-700</sub> followed by a thermolysis step. The resulting surface species corresponds to well-defined tetra-coordinate gallium single-sites, [(≡SiO)<sub>3</sub>Ga(XOSi≡)] (X = -H or ≡Si) according to IR, X-ray absorption near-edge structure and extended X-ray absorption fine structure analysis. These gallium sites show high activity, selectivity and stability for propane dehydrogenation with an initial turnover frequency of 20 per h per gallium center, propylene selectivity of ≥93% and remarkable stability over 20 h. The stability of the catalyst probably results from site-isolation of the active site on a non-reducible support such as silica, diminishing facile reduction typical of Ga<sub>2</sub>O<sub>3</sub>-based catalysts.

Received 24th November 2016  
Accepted 28th December 2016

DOI: 10.1039/c6sc05178b

www.rsc.org/chemicalscience

## Introduction

The increasing propylene demand combined with the use of alternative feedstocks such as shale gas has amplified the pressure towards propene production and the development of light alkane dehydrogenation processes.<sup>1</sup> In particular, the recent conversion of cracking plants from naphtha to ethane, the second largest component of shale gas, has resulted in a decline in annual propylene production while demand continues to increase. As a result, on-site propane dehydrogenation (PDH) is of particular interest for current and future propylene production.<sup>1a,c,2</sup> While the two principal industrial processes for PDH utilize Cr-Al<sub>2</sub>O<sub>3</sub> (CATOFIN) and PtSn-Al<sub>2</sub>O<sub>3</sub> (Oleflex) supported catalysts,<sup>1,c,2</sup> other materials such as gallium-based catalysts are receiving considerable attention as alternative catalysts.

Gallium-based zeolites have already been implemented for the conversion of lightweight alkanes to aromatics and H<sub>2</sub>, a process proposed to involve a tandem dehydrogenation-aromatization process.<sup>3</sup> Ga<sub>2</sub>O<sub>3</sub> and related materials have also been investigated as catalysts for alkane conversion, specifically PDH due to the high selectivity for propylene.<sup>4</sup> In this regard it is proposed that tetra-coordinate surface sites of Ga<sub>2</sub>O<sub>3</sub> are the active sites for propane dehydrogenation. However, due to the reducibility of Ga<sub>2</sub>O<sub>3</sub>, these active sites typically suffer from facile reduction,

ultimately resulting in catalyst deactivation.<sup>1c,5</sup> This is supported by advantageous effects of co-feeding CO<sub>2</sub> or H<sub>2</sub>O during PDH, which have been attributed to the re-oxidation of inactive Ga(I) sites and removal of coke from the surface.<sup>5a,6</sup> Several computational and experimental studies have aimed at identifying these active sites,<sup>4f,h,4,7</sup> which so far remains a topic of debate. Silica-supported gallium species have been recently prepared by electrostatic adsorption methods.<sup>7a</sup> While showing promising results, the structure of the active sites is unknown.

Surface organometallic chemistry (SOMC) allows for the generation of well-defined surface species on a variety of supports *via* grafting of tailored molecular precursors on supports with isolated -OH sites.<sup>8</sup> Thus, we reasoned that the development of an appropriate molecular precursor would allow for generating well-defined isolated active sites of gallium outside of bulk Ga<sub>2</sub>O<sub>3</sub>. This would result in a material with high catalytic activity with respect to total metal loading, as inactive bulk Ga<sub>2</sub>O<sub>3</sub> would not be present. Additionally, generating isolated gallium sites on a non-reducible support such as silica could diminish reduction processes and allow for the development of a catalyst with enhanced stability under PDH conditions. A two-step approach, involving both SOMC and the thermolytic molecular precursor approach has previously been implemented to generate isolated surface sites with controlled oxidation state and nuclearity.<sup>9</sup> Herein we describe the synthesis, structural characterization of the molecular complex [Ga(OSi(OtBu)<sub>3</sub>)(THF)] (**1**)<sup>10</sup> and its utilization as a precursor for generating gallium single-sites on silica. These isolated gallium sites were achieved through grafting of **1** on silica followed by a thermolysis step at 500 °C under high vacuum. The presented gallium species display unprecedented catalytic performances, combining high activity, selectivity and stability in the dehydrogenation of propane.

<sup>a</sup>Department of Chemistry and Applied Biosciences, ETH Zürich, CH-8093 Zürich, Switzerland. E-mail: coperet@inorg.chem.ethz.ch

<sup>b</sup>Paul Scherrer Institute, CH-5232 Villigen, Switzerland

† Electronic supplementary information (ESI) available: Experimental details, material characterization data, catalytic measurement details and crystallographic details. CCDC 1499756. For ESI and crystallographic data in CIF or other electronic format see DOI: 10.1039/c6sc05178b



## Results and discussion

First, we developed the synthesis of  $[\text{Ga}(\text{OSi}(\text{O}t\text{Bu})_3)_3(\text{THF})]$  (**1**) by reacting  $\text{GaCl}_3$  with  $\text{Na}(\text{OSi}(\text{O}t\text{Bu})_3)$  in THF.<sup>10</sup> A high-quality X-ray diffraction experiment provides reliable bond distances and angles for this precursor (Fig. 1). Opaque single crystals were grown from a saturated pentane solution cooled to  $-40^\circ\text{C}$ . This analysis reveals a distorted trigonal pyramidal geometry around the Ga(III) center ( $\tau_4 = 0.86$ ).<sup>11</sup> The THF ligand occupies the axial position (Ga1–O1<sub>THF</sub>, 1.963(2) Å) rendering the three siloxide ligands in the equatorial plane (Ga1–O2<sub>siloxide</sub>, 1.780(2) Å). This unusual geometry about the gallium metal center is attributed to the steric repulsion of the bulky siloxide ligands.

The next step was the reaction of a benzene solution of **1** with  $\text{SiO}_2\text{-700}$  (0.31 mmol  $-\text{OH}$  per g)<sup>12</sup> (Fig. 1). After 12 hours and subsequent washings of the material with benzene,  $^1\text{H}$  NMR spectroscopy revealed complete consumption of **1** and formation of isobutene, *tert*-butanol and THF in ratios of 4.3, 1.9, and 1.0 equivalents per consumed gallium complex. No detectable amount of  $\text{HOSi}(\text{O}t\text{Bu})_3$  was released after the grafting process, which is in sharp contrast to what was observed for similar Cr(III) or Fe(III) analogues.<sup>9b,h</sup> The aforementioned ratios indicate release of THF and thermal transformation of two  $-\text{OSi}(\text{O}t\text{Bu})_3$  ligands of **1** when contacted with the silica surface over the duration of 12 hours. The material was dried under high vacuum ( $10^{-5}$  mbar) for 12 hours and subsequent analysis by IR spectroscopy revealed

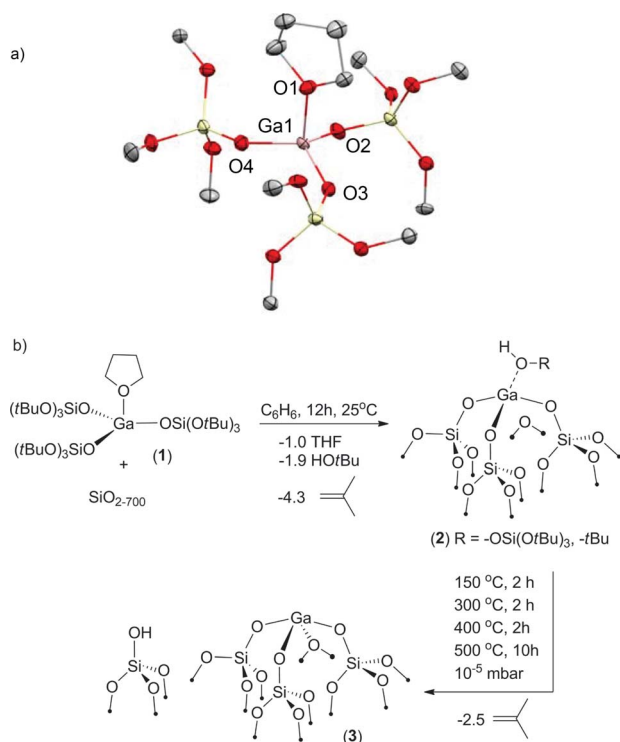


Fig. 1 (a) Molecular structure of **1** obtained from X-ray diffraction studies. Ellipsoids are at the 50% probability and all H atoms and all  $-\text{CH}_3$  groups of the  $-\text{OSi}(\text{O}t\text{Bu})_3$  ligand have been omitted for clarity. (b) Synthesis of  $[(\equiv\text{SiO})_3\text{Ga}(\text{HOR})]$ , (**2**,  $\text{R} = -\text{Si}(\text{O}t\text{Bu})_3$  or  $-t\text{Bu}$ ) and thermal transformation under high vacuum yielding  $[(\equiv\text{SiO})_3\text{Ga}(\text{XOSi}\equiv)]$  (**3**,  $\text{X} = \text{H}$  or  $\equiv\text{Si}$ ).

two  $\nu_{\text{OH}}$  bands in the range of  $3800\text{--}3100\text{ cm}^{-1}$  that are attributed to regenerated surface  $-\text{OH}$  sites and HOR ( $\text{R} = -\text{Si}(\text{O}t\text{Bu})_3$  or  $-t\text{Bu}$ ) remaining on the surface (see ESI<sup>†</sup>). Additional  $\nu_{\text{CH}}$  bands of an alkoxide ligand are observed in the range of  $3050\text{--}2860$  and  $1550\text{--}1360\text{ cm}^{-1}$ .  $^{13}\text{C}$  MAS SSNMR also revealed chemical shifts consistent with the presence of a remaining alcohol ligand on the surface of the material (see ESI<sup>†</sup>). Elemental analysis of the new material indicated a gallium loading of 1.53 weight% and 9.12 C atoms per Ga on the surface. These findings are consistent with a material possessing a remaining alcohol ligand per gallium immobilized on the support, specifically  $[(\equiv\text{SiO})_3\text{Ga}(\text{HOR})]$ , (**2**,  $\text{R} = -\text{Si}(\text{O}t\text{Bu})_3$  or  $-t\text{Bu}$ ).

The material **2** was then subjected to thermal treatment up to  $500^\circ\text{C}$  for 10 hours under high vacuum ( $10^{-5}$  mbar). Analysis of the volatile components from thermolysis revealed 2.5 equivalents of isobutene per gallium on the surface gauged by  $^1\text{H}$  NMR spectroscopy. Quantification of *ca.* 3  $\text{C}_4$  fragments per gallium, the absence of  $\nu_{\text{CH}}$  and the regeneration of  $\equiv\text{SiOH}$  in the IR of the new material indicates that thermal elimination of aliphatics from **2** was achieved yielding  $[(\equiv\text{SiO})_3\text{Ga}(\text{XOSi}\equiv)]$  (**3**,  $\text{X} = \text{H}$  or  $\equiv\text{Si}$ ) along with the regeneration of  $\equiv\text{SiOH}$  groups (Fig. 1).

To understand the coordination environment of gallium on the silica surface, we performed X-ray absorption spectroscopy (XAS) measurements at Ga K-edge on materials **1–3**. The edge position in the X-ray absorption near-edge structure (XANES) spectra of **2** and **3** was similar (10 374.8 and 10 374.2 eV, respectively) as well as the position of a shoulder at higher energies (10 380.8 and 10 381.2 eV, respectively), which is consistent with tetra-coordinate Ga(III) sites on the surface (Fig. 2).<sup>7a,13</sup>

Fits of the extended X-ray absorption fine structure (EXAFS) data for complexes **1–3** were fitted in *R*-space ( $1.0\text{--}3.5\text{ \AA}$ ) after a Fourier transform (**1** and **3**,  $k = 3.0\text{--}12.0\text{ \AA}^{-1}$ ; **2**,  $k = 3.0\text{--}11.0\text{ \AA}^{-1}$ ). The data are summarized in Table 1. For the molecular

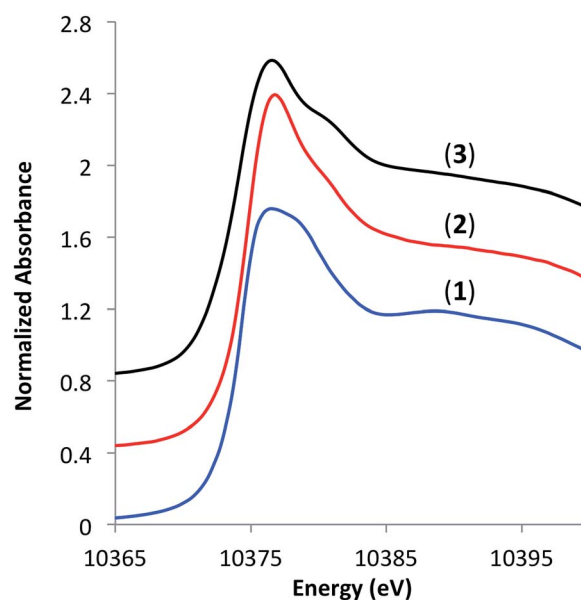


Fig. 2 XANES spectra of  $[\text{Ga}(\text{OSi}(\text{O}t\text{Bu})_3)_3(\text{THF})]$  (**1**),  $[(\equiv\text{SiO})_3\text{Ga}(\text{HOR})]$ , (**2**,  $\text{R} = -\text{Si}(\text{O}t\text{Bu})_3$  or  $-t\text{Bu}$ ) and  $[(\equiv\text{SiO})_3\text{Ga}(\text{XOSi}\equiv)]$  (**3**,  $\text{X} = \text{H}$  or  $\equiv\text{Si}$ ).



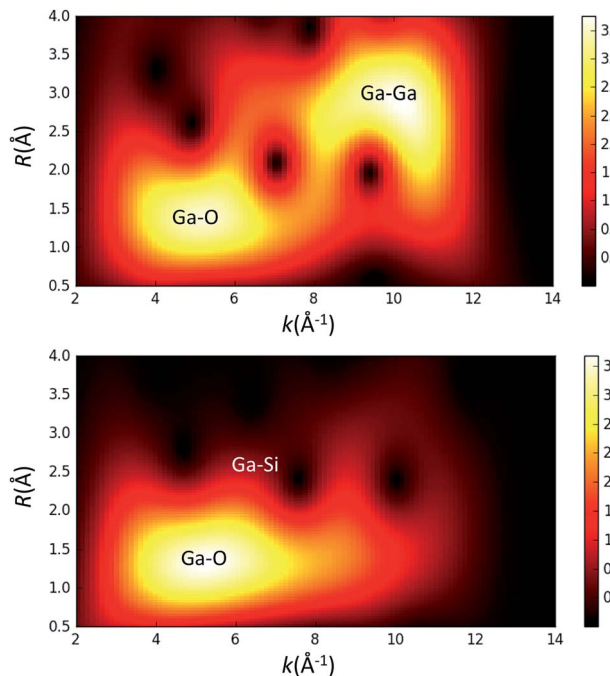
**Table 1** EXAFS fit parameters for [Ga(OSi(OtBu)<sub>3</sub>)(THF)] (**1**), [(≡SiO)<sub>3</sub>Ga(HOR)], (**2**, R = -Si(OtBu)<sub>3</sub> or -tBu) and [(≡SiO)<sub>3</sub>Ga(XOSi≡)] (**3**, X = H or ≡Si)<sup>a</sup>

Sample	Neighbor	N <sup>b</sup>	r <sup>c</sup> [Å]	σ <sup>2d</sup> [Å <sup>2</sup> ]
<b>1</b>	O	3*	1.788(3)	0.0035(2)
	O	1*	2.01(1)	0.0035(2)
	Si	3*	3.15(2)	0.007(2)
	O-Si	6*	3.25(3)	0.007(2)
	O	3*	3.50(2)	0.007(2)
<b>2</b>	O	4.1(4)	1.81(2)	0.008(1)
	Si	2.0(1.2)	3.17(1)	0.011(6)
<b>3</b>	O	3.6(5)	1.80(1)	0.008(1)
	Si	1.4(6)	3.08(3)	0.011*

<sup>a</sup> Samples were measured at 295 K in transmission mode. <sup>b</sup> Number of neighbors. <sup>c</sup> Distance between Ga and neighbor. <sup>d</sup> Debye-Waller factor. Set parameters are indicated by (\*).

complex **1**, two Ga-O scattering paths at distances of 1.79 Å (*N* = 3) and 2.01 Å (*N* = 1) were used for modeling of the 1<sup>st</sup> shell; a longer scattering path for Ga-Si of 3.15 Å (*N* = 3) was also employed for modeling of the 2<sup>nd</sup> shell. An additional multi-scattering path for Ga-O-Si of 3.25 Å (*N* = 6) and a long scattering path for Ga-O of 3.50 Å (*N* = 3) were required to produce a good fit. These distances match well with the X-ray single-crystal diffraction data obtained for **1**. For the grafted complex **2** and the thermally treated complex **3**, only Ga-O and Ga-Si scattering paths were used for fitting the experimental data. The fit for **2** indicates that Ga has 4.1 oxygen neighbors at 1.81 Å and 2.0 silicon neighbors at 3.17 Å. Similarly, the best fit for **3** is consistent with 3.6 oxygen neighbors at 1.80 Å and 1.4 silicon atoms at 3.08 Å.

Given the possibility of generating gallium dimers upon grafting on the surface of silica,<sup>14</sup> we have also probed the contribution of a Ga-Ga scattering path by performing a wavelet transform (WT) analysis<sup>15</sup> on the EXAFS data for thermally treated **3** (Fig. 3). This analysis provides a correlation of *R* and *k*-space and ultimately aids in the distinction between two different atoms positioned at similar distances from the gallium metal center. The WT analysis of **3** shows a predominant feature with the maximum intensity in the range of *R* = 1.2–1.6 Å and *k* = 4.5–6.2 Å<sup>-1</sup>, which is ascribed to the Ga-O scattering path. Scattering paths for Ga-Si and Ga-O-Si produce features in the range of *R* = 2.6–2.8 Å and *k* = 6.0–8.0 Å<sup>-1</sup> for complex **3**; no Ga-Ga path could be identified. Fig. 3 also shows the WT analysis of EXAFS data of a Ga<sub>2</sub>O<sub>3</sub> reference sample. This was done to evaluate the presence of a Ga-Ga scattering path in **3**. The WT analysis performed on the EXAFS data of Ga<sub>2</sub>O<sub>3</sub> shows a similar feature for a Ga-O scattering path described for **3** and an additional intense feature for a Ga-Ga scattering path in the range of *R* = 2.5–3.0 Å and *k* = 9.0–10.0 Å<sup>-1</sup>. This later feature is not observed for complex **3**, implying that a Ga-Ga scattering path is not significant for fitting of the EXAFS data, indicating that Ga<sub>2</sub>O<sub>3</sub> domains are not present at the surface. Analysis of the XAS measurements for **1–3** strongly supports the formation of well-defined and dispersed tetra-coordinate gallium single-sites on the silica surface.



**Fig. 3** Wavelet transform (WT) analysis of EXAFS data for Ga<sub>2</sub>O<sub>3</sub> (top) and [(≡SiO)<sub>3</sub>Ga(XOSi≡)] (**3**, X = H or ≡Si) (bottom).

To chemically probe the presence and accessibility of the gallium sites on the surface, pyridine adsorption studies were performed on **3** revealing three vibrational bands at 1621, 1493, 1458 cm<sup>-1</sup> (see ESI†). These vibrational bands were retained upon heating to 500 °C under high vacuum indicating the presence of strong Lewis acid sites on the surface.<sup>7a,16</sup> Additionally, no vibrational bands characteristic of the pyridinium ion were observed, indicating the absence of Brønsted acid surface sites.

We then investigated the catalytic performance of **3** towards PDH at 550 °C. Using a flow (10 mL per min; WHSV, 2.1 per h) consisting of 20% C<sub>3</sub>H<sub>8</sub> in Ar, selectivity for propylene after 30 min was 94.3% with a TOF of 20.4 mol C<sub>3</sub>H<sub>6</sub> per mol Ga per h and conversion of 9.3% (Fig. 4). After 20 hours of catalytic performance selectivity remained nearly constant (≥93%) with a TOF of 14.2 per h and conversion of 6.5%. The only other hydrocarbons detected during the duration of the experiment were methane and ethylene, determined to be secondary products of the reaction (see ESI†). After PDH only minimal darkening of the catalyst, as well as elemental analysis (0.18% C), suggests that coke formation is a negligible contribution to propane conversion. The initial TOF for **3** is ca. 11 times higher than recently reviewed Ga<sub>2</sub>O<sub>3</sub> based materials (highest reported TOF of 1.8 per h; WHSV, 0.97 per h)<sup>16</sup> and five times greater than isolated Ga sites prepared by electrostatic adsorption (TOF of 3.8 per h), which were tested at significantly lower space velocities.<sup>7a</sup> The higher activity of **3**, with respect to the total metal loading of the catalysts, is attributed to negligible amounts of inactive bulk gallium-material being present in **3**. Over the 20 hour experiment, **3** experiences a slow deactivation process (*k*<sub>d</sub> of 0.02 per h) which is an order of magnitude slower



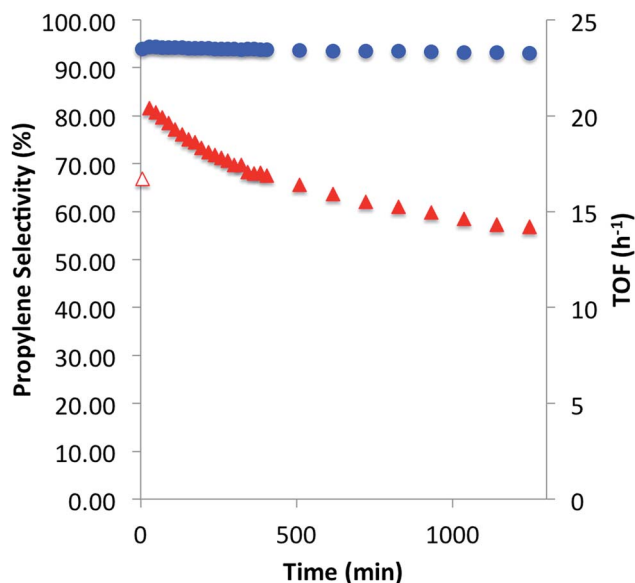


Fig. 4 Catalytic performance of  $[(\equiv\text{SiO})_3\text{Ga}(\text{XOSi}\equiv)]$  (**3**, X = H or  $\equiv\text{Si}$ ) for propane dehydrogenation at 550 °C with conversions in the range of 9.3–6.5%. Propylene selectivity (circles) and turnover frequency per hour (triangles), over a period of 20 hours.

than that observed for  $\text{Ga}_2\text{O}_3$  ( $k_d$  of 0.67 per h) and  $\beta\text{-Ga}_2\text{O}_3$  ( $k_d$  of 0.21 per h) which have a catalyst life of 4 and 6 hours, respectively.<sup>16,17</sup> An industrial-like  $\text{CrO}_x\text{-Na/Al}_2\text{O}_3$  (20 wt% Cr, 1 wt% Na) catalyst displays an initial TOF of 0.027 per h and slightly lower selectivity (80%) for propylene at 550 °C with a WHSV of 0.12 per h.<sup>16</sup> The considerably lower initial TOF in comparison to **3** highlights the effect of having significant amounts of inactive bulk metal in the catalyst. These catalytic comparisons are summarized in the ESI.†

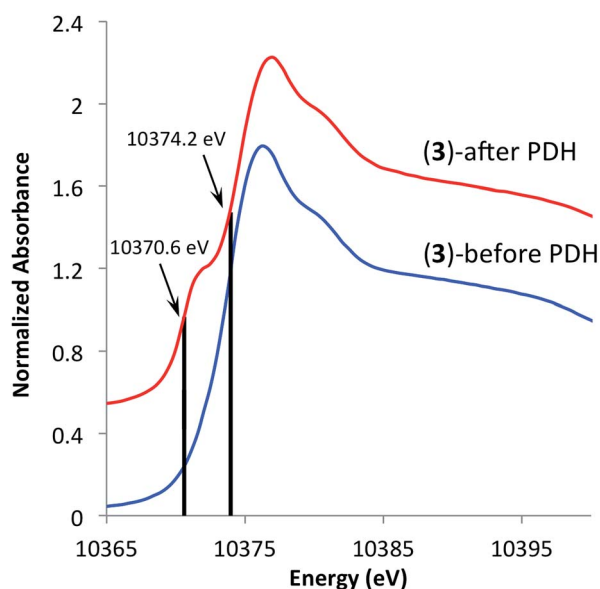


Fig. 5 XANES spectra of  $[(\equiv\text{SiO})_3\text{Ga}(\text{XOSi}\equiv)]$  (**3**, X = H or  $\equiv\text{Si}$ ) before (bottom) and after (top) propane dehydrogenation at 550 °C for 20 hours.

In an effort to understand the stability of **3** under PDH conditions, XAS measurements at Ga K-edge of the spent catalyst were performed. This analysis revealed a partial reduction of the catalyst as evident by a new feature with an edge position at 10 370.6 eV in the XANES spectrum (Fig. 5). This shift to lower energies is attributed to partial formation of Ga(I) surface sites as no vibrational bands characteristic of surface Ga–H species were observed in the IR spectrum of the spent catalyst (see ESI†). Analysis of the EXAFS data after catalysis displayed no intense feature at higher  $R$ -values (2.2–3.5 Å) indicating that site-isolation of the gallium sites is retained after PDH. The partial reduction of the catalyst could explain the decrease in activity (*ca.* 30%) after 20 hours. The high TOF and selectivity ( $\geq 93\%$ ) maintained over 20 hours exemplifies the ability of SOMC methods to generate a stable material possessing highly active sites on the surface. It also indicates that site isolation and immobilization on a non-reducible support can diminish reduction processes that contribute to deactivation of other  $\text{Ga}_2\text{O}_3$ -based materials.

## Conclusions

In summary, we have synthesized silica-supported isolated tetra-coordinated gallium sites from a well-defined gallium-siloxide molecular precursor employing to a two-step process involving the grafting of a bulky siloxide molecular precursor **1** on highly dehydroxylated silica followed by thermolysis. XANES and EXAFS data, including a wavelet transform analysis, allowed for assignment of well-defined isolated gallium sites on the surface. Such material combines high activity towards propane dehydrogenation with high selectivity for propylene and stability over a 20 hour period. We attribute the prolonged stability of the catalyst to the generation of isolated Ga sites on a non-reducible support, thus diminishing facile reduction typical of  $\text{Ga}_2\text{O}_3$ . This study has thus opened new avenues to generate more efficient and rationally designed dehydrogenation catalysts, and we are currently exploring this area.

## Acknowledgements

The authors are grateful to the Swiss National Foundation (SNF) for financial support of this work (grant no. 200020\_149704). We thank Professor Christoph R. Müller and Paula M. Abdala (ETH Zürich) for assistance in collecting XAS data. We also thank Florian Allouche (ETH Zürich) for assistance with X-ray crystallography analysis. We thank Alexander L. Trigub (Kurchatov Institute, Moscow, Russia) for providing software for WT analysis.

## References

- (a) Z. Nawaz, *Rev. Chem. Eng.*, 2015, **31**, 413–436; (b) D. Malakoff, *Science*, 2014, **344**, 1464–1467; (c) J. J. H. B. Sattler, J. Ruiz-Martinez, E. Santillan-Jimenez and B. M. Weckhuysen, *Chem. Rev.*, 2014, **114**, 10613–10653; (d) P. C. A. Bruijninx and B. M. Weckhuysen, *Angew. Chem., Int. Ed.*, 2013, **52**, 11980–11987; (e)



- J. M. Thomas and W. J. Thomas, *Principles and Practice of Heterogeneous Catalysis*, Wiley-VCH, New York, 2nd edn, 2015; (f) G. Ertl, H. Knözinger, F. Schüth and J. Weitkamp, *Handbook of Heterogeneous Catalysis*, Wiley-VCH, Weinheim, 2nd edn, 2008; (g) K. Weisermel and H. J. Arpe, *Industrial Organic Chemistry*, Wiley-VCH, Weinheim, 4th edn, 2003.
- 2 D. Sanfilippo and I. Miracca, *Catal. Today*, 2006, **111**, 133–139.
- 3 (a) R. Fricke, H. Kosslick, G. Lischke and M. Richter, *Chem. Rev.*, 2000, **100**, 2303–2406; (b) G. L. Price and V. Kanazirev, *J. Catal.*, 1990, **126**, 267–278; (c) P. Meriaudeau and C. Naccache, *J. Mol. Catal.*, 1989, **50**, L7–L10; (d) N. S. Gnep, J. Y. Doyemet, A. M. Seco, F. R. Ribeiro and M. Guisnet, *Appl. Catal.*, 1988, **43**, 155–166; (e) H. Kitagawa, Y. Sendoda and Y. Ono, *J. Catal.*, 1986, **101**, 12–18; (f) J. M. Thomas and X. S. Liu, *J. Phys. Chem.*, 1986, **90**, 4843–4847; (g) G. D. Meitzner, E. Iglesia, J. E. Baumgartner and E. S. Huang, *J. Catal.*, 1993, **140**, 209–225.
- 4 (a) S. Tan, S.-J. Kim, J. S. Moore, Y. Liu, R. S. Dixit, J. G. Pendergast, D. S. Sholl, S. Nair and C. W. Jones, *ChemCatChem*, 2016, **8**, 214–221; (b) S. Tan, L. B. Gil, N. Subramanian, D. S. Sholl, S. Nair, C. W. Jones, J. S. Moore, Y. Liu, R. S. Dixit and J. G. Pendergast, *Appl. Catal.*, A, 2015, **498**, 167–175; (c) J. J. H. B. Sattler, I. D. Gonzalez-Jimenez, L. Luo, B. A. Stears, A. Malek, D. G. Barton, B. A. Kilos, M. P. Kaminsky, T. W. G. M. Verhoeven, E. J. Koers, M. Baldus and B. M. Weckhuysen, *Angew. Chem., Int. Ed.*, 2014, **53**, 9251–9256; (d) J.-L. Wu, M. Chen, Y.-M. Liu, Y. Cao, H.-Y. He and K.-N. Fan, *Catal. Commun.*, 2013, **30**, 61–65; (e) P. Michorczyk, P. Kuśtrowski, A. Kolak and M. Zimowska, *Catal. Commun.*, 2013, **35**, 95–100; (f) M. Chen, J. Xu, F.-Z. Su, Y.-M. Liu, Y. Cao, H.-Y. He and K.-N. Fan, *J. Catal.*, 2008, **256**, 293–300; (g) H. Li, Y. Yue, C. Miao, Z. Xie, W. Hua and Z. Gao, *Catal. Commun.*, 2007, **8**, 1317–1322; (h) B. Xu, B. Zheng, W. Hua, Y. Yue and Z. Gao, *J. Catal.*, 2006, **239**, 470–477; (i) B. Zheng, W. Hua, Y. Yue and Z. Gao, *J. Catal.*, 2005, **232**, 143–151; (j) N. S. Nesterenko, O. A. Ponomoreva, V. V. Yuschenko, I. I. Ivanova, F. Testa, F. Di Renzo and F. Fajula, *Appl. Catal.*, A, 2003, **254**, 261–272; (k) K. Nakagawa, C. Kajita, K. Okumura, N.-O. Ikenaga, M. Nishitani-Gamo, T. Ando, T. Kobayashi and T. Suzuki, *J. Catal.*, 2001, **203**, 87–93; (l) K. Nakagawa, C. Kajita, Y. Ide, M. Okamura, S. Kato, H. Kasuya, N. O. Ikenaga, T. Kobayashi and T. Suzuki, *Catal. Lett.*, 2000, **64**, 215–221; (m) K. Nakagawa, M. Okamura, N. Ikenaga, T. Suzuki, K. Nakagawa, M. Okamura, T. Suzuki, T. Kobayashi and T. Kobayashi, *Chem. Commun.*, 1998, 1025–1026; (n) H. Xiao, J. Zhang, P. Wang, X. Wang, F. Pang, Z. Zhang and Y. Tan, *Catal. Sci. Technol.*, 2016, **6**, 5183–5195; (o) M. Saito, S. Watanabe, I. Takahara, M. Inaba and K. Murata, *Catal. Lett.*, 2003, **89**, 213–217.
- 5 (a) C. Copéret, *Chem. Rev.*, 2010, **110**, 656–680; (b) C. Copéret, D. P. Estes, K. Larmier and K. Searles, *Chem. Rev.*, 2016, **116**, 8463–8505.
- 6 (a) E. A. Pidko and R. A. van Santen, *J. Phys. Chem. C*, 2009, **113**, 4246–4249; (b) E. J. M. Hensen, E. A. Pidko, N. Rane and R. A. van Santen, *Angew. Chem., Int. Ed.*, 2007, **46**, 7273–7276; (c) E. A. Pidko, R. A. van Santen and E. J. M. Hensen, *Phys. Chem. Chem. Phys.*, 2009, **11**, 2893–2902.
- 7 (a) A. B. Getsoian, U. Das, J. Camacho-Bunquin, G. Zhang, J. R. Gallagher, B. Hu, S. Cheah, J. A. Schaidle, D. A. Ruddy, J. E. Hensley, T. R. Krause, L. A. Curtiss, J. T. Miller and A. S. Hock, *Catal. Sci. Technol.*, 2016, **6**, 6339–6353; (b) Y. Liu, Z. H. Li, J. Lu and K.-N. Fan, *J. Phys. Chem. C*, 2008, **112**, 20382–20392; (c) I. Takahara, M. Saito, M. Inaba and K. Murata, *Catal. Lett.*, 2004, **96**, 29–32; (d) P. Michorczyk and J. Ogonowski, *Appl. Catal.*, A, 2003, **251**, 425–433; (e) A. A. Gabrienko, S. S. Arzumanov, A. V. Toktarev and A. G. Stepanov, *Chem. Phys. Lett.*, 2010, 496; (f) V. B. Kazansky, I. R. Subbotina, A. A. Pronin, R. Schlögl and F. C. Jentoft, *J. Phys. Chem. B*, 2006, **110**, 7975–7978; (g) U. Das, G. Zhang, B. Hu, A. S. Hock, P. C. Redfern, J. T. Miller and L. A. Curtiss, *ACS Catal.*, 2015, **5**, 7177–7185.
- 8 (a) C. Copéret, A. Comas-Vives, M. P. Conley, D. P. Estes, A. Fedorov, V. Mougel, H. Nagae, F. Núñez-Zarur and P. A. Zhizhko, *Chem. Rev.*, 2016, **116**, 323–421; (b) C. Copéret, M. Chabanas, R. Petroff Saint-Arroman and J.-M. Basset, *Angew. Chem., Int. Ed.*, 2003, **42**, 156–181; (c) S. L. Wegener, T. J. Marks and P. C. Stair, *Acc. Chem. Res.*, 2012, **45**, 206–214; (d) J. D. A. Pelletier and J.-M. Basset, *Acc. Chem. Res.*, 2016, **49**, 664–677.
- 9 (a) T. D. Tilley, *J. Mol. Catal. A: Chem.*, 2002, **182–183**, 17–24; (b) C. Nozaki, C. G. Lugmair, A. T. Bell and T. D. Tilley, *J. Am. Chem. Soc.*, 2002, **124**, 13194–13203; (c) J. Jarupatrakorn and T. D. Tilley, *J. Am. Chem. Soc.*, 2002, **124**, 8380–8388; (d) K. L. Fajdala and T. D. Tilley, *J. Catal.*, 2003, **216**, 265–275; (e) K. L. Fajdala, R. L. Brutchey and T. D. Tilley, *Surface and Interfacial Organometallic Chemistry and Catalysis*, Springer, Berlin, Heidelberg, 2005; (f) A. W. Holland, G. Li, A. M. Shahin, G. J. Long, A. T. Bell and T. D. Tilley, *J. Catal.*, 2005, **235**, 150–163; (g) M. P. Conley, M. F. Delley, G. Siddiqi, G. Lapadula, S. Norsic, V. Monteil, O. V. Safonova and C. Copéret, *Angew. Chem., Int. Ed.*, 2014, **53**, 1872–1876; (h) M. F. Delley, F. Núñez-Zarur, M. P. Conley, A. Comas-Vives, G. Siddiqi, S. Norsic, V. Monteil, O. V. Safonova and C. Copéret, *Proc. Natl. Acad. Sci. U. S. A.*, 2014, **111**, 11624–11629; (i) V. Mougel, K.-W. Chan, G. Siddiqi, K. Kawakita, H. Nagae, H. Tsurugi, K. Mashima, O. Safonova and C. Copéret, *ACS Cent. Sci.*, 2016, **138**, 14987–14997; (j) D. P. Estes, G. Siddiqi, F. Allouche, K. V. Kovtunov, O. V. Safonova, A. L. Trigub, I. V. Koptuyug and C. Copéret, *J. Am. Chem. Soc.*, 2016, **2**, 569–576; (k) R. L. Brutchey, C. G. Lugmair, L. O. Schebaum and T. D. Tilley, *J. Catal.*, 2005, **229**, 72–81.
- 10 [Ga(OSi(OtBu)<sub>3</sub>)(THF)] was disclosed during the course of this study; J. P. Dombrowski, G. R. Johnson, A. T. Bell and T. D. Tilley, *Dalton Trans.*, 2016, 11025–11034.
- 11 M. H. Reineke, M. D. Sampson, A. L. Rheingold and C. P. Kubiak, *Inorg. Chem.*, 2015, **54**, 3211–3217.



- 12 Silica (Degauss Aerosol,  $204 \text{ m}^2 \text{ g}^{-1}$ ) thermally treated at  $700 \text{ }^\circ\text{C}$  with a temperature ramp of  $5 \text{ }^\circ\text{C}$  per min under high vacuum ( $10^{-5}$  mbar) yielded  $0.31 \text{ mmol OH per g of SiO}_2$  corresponding to  $0.92$  accessible OH groups per  $\text{nm}^2$ . The slightly higher  $-\text{OH}$  density in comparison to that reported in literature for  $\text{SiO}_{2-700}$  is attributed to the slightly higher temperature ramp used during dehydroxylation (see ref. 8a).
- 13 (a) K. Nishi, K.-i. Shimizu, M. Takamatsu, H. Yoshida, A. Satsuma, T. Tanaka, S. Yoshida and T. Hattori, *J. Phys. Chem. B*, 1998, **102**, 10190–10195; (b) P. Behrens, H. Kosslick, T. Vu Anh, M. Fröba and F. Neissendorfer, *Microporous Mater.*, 1995, **3**, 433–441; (c) K. A. Al-majnouni, N. D. Hould, W. W. Lonergan, D. G. Vlachos and R. F. Lobo, *J. Phys. Chem. C*, 2010, **114**, 19395–19405; (d) R. I. Walton and D. O'Hare, *J. Phys. Chem. Solids*, 2001, **62**, 1469–1479.
- 14 (a) Z. A. Taha, E. W. Deguns, S. Chattopadhyay and S. L. Scott, *Organometallics*, 2006, **25**, 1891–1899; (b) S. D. Fleischman and S. L. Scott, *J. Am. Chem. Soc.*, 2011, **133**, 4847–4855.
- 15 H. Funke, M. Chukalina and A. C. Scheinost, *J. Synchrotron Radiat.*, 2007, **14**, 426–432.
- 16 (a) A. Vimont, J. C. Lavalley, A. Sahibed-Dine, C. Otero Areán, M. Rodríguez Delgado and M. Daturi, *J. Phys. Chem. B*, 2005, **109**, 9656–9664; (b) E. P. Parry, *J. Catal.*, 1963, **2**, 371–379.
- 17  $k_d$  is defined as  $\ln(1 - \text{conv}_{\text{end}}/\text{conv}_{\text{end}}) - \ln(1 - \text{conv}_{\text{start}}/\text{conv}_{\text{start}})/t$ , where  $\text{conv}_{\text{start}}$  is the conversion at start of experiment,  $\text{conv}_{\text{end}}$  is the conversion at end of experiment, and  $t$  is the duration of experiment in hours.

