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A highly reduced graphene oxide/ZrO_x–MnCO₃ or –Mn₂O₃ nanocomposite as an efficient catalyst for selective aerial oxidation of benzylic alcohols†

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Highly reduced graphene oxide (HRG) nanocomposites of manganese carbonate doped with (1%) zirconia (ZrO_x) nanoparticles [ZrO_x(1%)–MnCO₃/(X%)HRG (where X = 0–7)] were prepared employing a facile co-precipitation method in which the percentage of HRG was varied. The resulting nanocomposite was calcined at 300 °C. Further calcination of the catalyst at 500 °C resulted in the conversion of manganese carbonate to manganese oxide [ZrO_x(1%)–Mn₂O₃/(X%)HRG]. The effect of the inclusion of HRG on the catalytic activity along with its comparative performance between carbonates and their respective oxides was studied for the liquid-phase selective oxidation of benzylic alcohols into corresponding aldehydes using molecular oxygen as the eco-friendly oxidizing agent without adding any external additives or bases. The influence of different parameters such as different percentages of HRG, reaction times, calcination temperatures, catalyst dosages and reaction temperatures have also been systematically studied in order to optimize the catalyst composition and reaction conditions. The inclusion of HRG as a dopant remarkably enhanced the catalytic efficiency of ZrO_x–MnCO₃ nanocatalysts for the aerobic oxidation of alcohols. The as-prepared catalysts were characterized by scanning electron microscopy (SEM), energy-dispersive X-ray spectroscopy (EDX), powder X-ray diffraction (XRD), thermal gravimetric analysis (TGA), Brunauer–Emmett–Teller (BET) surface area analysis, Raman spectroscopy and Fourier transform infrared spectroscopy (FT-IR). The catalyst with composition ZrO_x(1%)–MnCO₃/(1%)HRG obtained by calcination at 300 °C exhibited excellent specific activity (60.0 mmol g^{−1} h^{−1}) with 100% benzyl alcohol conversion and more than 99% product selectivity within an extremely short time (4 min). The same catalyst is employed for the oxidation of a wide range of substituted benzylic and aliphatic alcohols. The catalyst *i.e.* ZrO_x(1%)–MnCO₃/(1%)HRG calcined at 300 °C yielded corresponding aldehydes with complete convertibility and selectivity in short reaction times under mild conditions whereas the as-prepared catalyst exhibited high selectivity for aromatic alcohols over aliphatic alcohols. The catalyst was recycled and reused at least five times without any obvious loss in its activity or selectivity.

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Introduction

Selective oxidation of aromatic and aliphatic alcohols to corresponding aldehydes or ketones is one of the most essential organic transformations in synthetic chemistry due to their use as important precursors for different fundamental fine organic

compounds in industries such as cosmetics, pharmaceuticals, perfumery, food, insecticides, dyestuffs, agrochemicals and flavoring agents.^{1–4} In particular, benzaldehyde is considered as the second most important aromatic molecule after vanillin and is the most important industrial starting material or intermediate in numerous industries.^{5,6} With increasing environmental and economic concerns, heterogeneous catalytic reactions using molecular oxygen as an environmentally benign and low cost oxidant are developing as green processes for the selective oxidation of alcohols to their corresponding aldehydes or ketones.^{7,8} Usually, oxidation of alcohols is carried out using expensive and environmentally toxic inorganic oxidant agents such as (KMnO₄ or CrO₃). This leads to the formation of dangerous side products.⁹ In contrast, using eco-friendly low cost oxidizing agents, like molecular oxygen ends up producing water as the only by-product. Therefore, it has received

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increasing attention from the economic and environmental point of views.^{10,11} Various methods that utilize molecular oxygen for the oxidation of alcohols have been exploited using precious metals such as, gold, palladium,¹² platinum^{13,14} and ruthenium^{15,16} as heterogeneous catalysts with excellent catalytic performances and selectivities, but the high cost and lack of availability of these noble metals limits their applications. Therefore, many efforts have been carried out in order to explore environmentally friendly and low cost catalysts such as non-noble metals or transition metals like, Cu,^{17,18} Co,¹⁹ Ni,^{20,21} Fe,²² V,²³ Ag,^{24,25} Cr,^{26,27} Mo,²⁸ Re,^{29,30} and Os³¹ for aerobic oxidation of alcohols. It has been widely reported that the catalytic property of the mixed metal oxide nanoparticles as catalysts enhanced remarkably upon doping with other metals which may be owing to the metal nanoparticles having high surface area.^{32,33}

Graphene is a single layer of sp² hybridized carbon atoms in a closely packed honeycomb two-dimensional (2D) lattice. Ever since its isolation for the first time in 2004, a plethora of publications have been reported due to its amazing properties such as high electron mobility (250 000 cm² V⁻¹ s⁻¹),³⁴ extraordinary thermal conductivity (5000 W m⁻¹ K⁻¹),³⁵ an electrical conductivity of up to 6000 S cm⁻¹ (ref. 36) and an extremely high theoretical specific surface area of 2630 m² g⁻¹ (ref. 37) and wide applications.³⁸ The extraordinary catalytic, magnetic and electronic properties of metal or metal oxide based graphene nanocomposites have increased its use on industrial scale such as sensors,³⁹⁻⁴¹ drug delivery,^{42,43} water purification,⁴⁴ supercapacitor,⁴⁵⁻⁴⁷ solar cells,^{48,49} lithium ion batteries,⁵⁰ and catalysis.^{51,52}

In the field of catalysis, so far, graphene based materials *i.e.* graphene oxide (GO) or highly reduced graphene oxide (HRG) are mostly used as catalyst support for metal and/or metal oxide nanoparticles.⁵³ HRG has been used as promising material for catalyst supports in oxidation reactions due to the presence of carbon vacancies or topological defects present on the surface, which assist in enhancing the possibility of sorption and intercalation of ions and molecules⁵⁴ along with extremely high specific surface area, leads to excellent catalytic performance. The combination of metal nanoparticles with carbon supports have also been reported to be efficient catalyst's for several chemical reactions such as synthesis of aniline from nitrobenzene,⁵⁵ methanol oxidation,⁵⁶ ethylene glycol oxidation,⁵⁷ formic acid oxidation,⁵⁸ oxidation of glucose,⁵⁹ reductive amination of aldehydes,⁶⁰ reduction of benzylic alcohols⁶¹ and Suzuki coupling reaction.⁶²

In this contribution, we have developed nanostructured mixed metal oxides based nanostructured materials as heterogeneous catalysts for the aerobic oxidation of alcohols,^{24,33,63} which showed quite promising results. However, the design of such materials require better strategies leading to the formation of electrically and chemically stable systems, with high surface area and being able to transfer the charges more efficiently. The highly reduced graphene oxide (HRG) fulfils these criteria. Therefore, the present work focuses to improve the catalytic activities of mixed metal oxides based catalyst for the oxidation of benzylic alcohols by incorporating the highly reduced

graphene oxides (HRG) which helps in better transferring the electron through carbon skeleton^{64,65} and at the same time provides a very high surface area support for the catalyst.

Here we report on the synthesis of composites based on HRG with mixed oxides, zirconia (ZrO_x) doped manganese carbonate (MnCO₃) *i.e.* ZrO_x(1%)-MnCO₃ by varying the amount of HRG as illustrated in system (Scheme 1). These catalysts are employed for the aerobic oxidation of benzylic alcohols in order to comprehend the effect of HRG on the catalytic performance. The as-synthesized nanocomposites are evaluated as catalyst for the selective oxidation of benzylic alcohols to corresponding aldehydes in liquid-phase using green procedure, *i.e.* using molecular oxygen as an oxidizing agent. To the best of our knowledge, this is the first report on the nanocomposites involving zirconia, manganese carbonate and HRG as a catalyst for aerobic oxidation of alcohols. The nanocomposite catalyst has been characterized with various types of techniques such as scanning electron microscopy (SEM), energy-dispersive X-ray spectroscopy (EDX), powder X-ray diffraction (XRD), thermogravimetric analysis (TGA), Brunauer-Emmett-Teller (BET) surface area measurement, Raman spectroscopy and Fourier transform infrared (FT-IR) spectroscopies.

Experimental

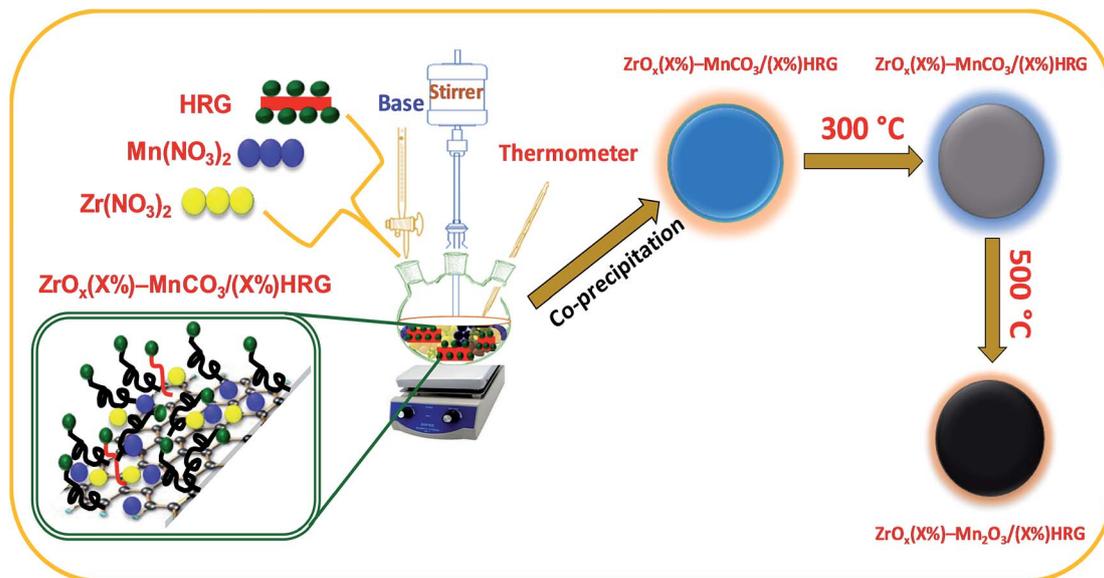
Preparation of highly reduced graphene oxide (HRG)

Firstly, graphene oxide (GO) was synthesized from graphite using Hummers method.⁶⁶ The graphene oxide (200 mg) was first dispersed in 40 mL distilled water and sonicated for 30 min. The suspension was heated to 100 °C subsequently 6 mL of hydrazine hydrate was added to the suspension. The suspension is then kept at 98 °C for 24 h. The reduced graphene was collected by filtration in the form of black powder. The obtained material was washed using distilled water several times to remove any excessive hydrazine and was subjected to sonication. The suspension was centrifuged at 4000 rpm for 3 min to remove bulk graphite. The final product was collected using vacuum filtration and dried under vacuum.

Synthesis of ZrO_x(1%)-MnCO₃/(X%)HRG nanocomposites

ZrO_x(1%)-MnCO₃/(X%)HRG nanocomposites were synthesized by co-precipitation method (where X = 0-7). In a typical synthesis stoichiometric amount of manganese(II) nitrate-tetrahydrate (Mn(NO₃)₂·4H₂O) and zirconium nitrate (Zr(NO₃)₂) and highly reduced graphene oxide (HRG) were mixed in a round bottomed flask and subjected to ultrasonication for 30 min. The resulting solution was heated to 80 °C, under vigorously stirring using a mechanical stirrer and 0.5 M solution of sodium bicarbonate (NaHCO₃) was added drop wise by using burette until the solution attained a pH 9. The solution was continued to stir at the same temperature for about 3 hours followed by stirring over night at room temperature. The solution was filtered using a Buchner funnel under vacuum and dried at 70 °C overnight in an oven. The resulting powder was calcined at various temperatures (*i.e.* 300, 400 and 500 °C).





Scheme 1 Synthetic representation of $\text{ZrO}_x(X)\text{-MnCO}_3/(X\%)\text{HRG}$ followed by calcination at $500\text{ }^\circ\text{C}$ to prepare $\text{ZrO}_x(X)\text{-Mn}_2\text{O}_3/(X\%)\text{HRG}$.

Catalyst characterization

Scanning electron microscopy (SEM) and elemental analysis (energy dispersive X-ray analysis: EDX) were carried out using Jeol SEM model JSM 6360A (Japan). This was used to determine the morphology of nanoparticles and its elemental composition. Powder X-ray diffraction studies were carried out using Altima IV [Make: Regaku] X-ray diffractometer. Fourier Transform Infrared Spectroscopy (FT-IR) spectra were recorded as KBr pellets using a Perkin-Elmer 1000 FT-IR spectrophotometer. BET surface area was measured on a NOVA 4200e surface area & pore size analyzer. Thermogravimetric analysis was carried out using Perkin-Elmer thermogravimetric analyzer 7.

General procedure for alcohol oxidation

In a typical procedure, oxidation of benzyl alcohol was carried out in glass flask equipped with a magnetic stirrer, reflux condenser, and thermometer. The mixture of the benzyl alcohol (2 mmol), toluene (10 mL), and the catalyst (0.3 g) was transferred in a three-necked round-bottomed flask (100 mL), the resulting mixture was heated to desired temperature with vigorous stirring. The oxidation experiment was started by bubbling oxygen gas at a flow rate of 20 mL min^{-1} into the reaction mixture. After the reaction, the solid catalyst was filtered off by centrifugation and the liquid products were analyzed by gas chromatography to determine the conversion of the alcohol and product selectivity by (GC, 7890A) Agilent Technologies Inc, equipped with a flame ionization detector (FID) and a 19019S-001 HP-PONA column.

Results and discussion

Characterization of the catalysts

X-ray diffraction (XRD). Fig. 1 shows XRD diffractograms of the graphite powder, graphene oxide (GO), highly reduced

graphene oxide (HRG), unsupported $\text{ZrO}_x(1\%)\text{-MnCO}_3$, and $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite. The XRD patterns for the pristine graphite exhibited a sharp and single reflection at $2\theta = 26.5^\circ$ with a d -spacing of 3.37 \AA .⁶⁷ However, upon oxidation the diffraction peak shifted to $2\theta = 11.8^\circ$. This shift leads to an increase in interlayer spacing from 3.37 to 6.41 \AA for graphite and graphene oxide, respectively, because of the introduction of different oxygen containing functionalities between the graphite layers during the oxidation process.⁶¹ This confirms the oxidation of graphite to graphene oxide. XRD pattern of HRG exhibits broad diffraction peak at $2\theta = 24.6^\circ$ which is a characteristic for the structure of HRG, indicating the reduction of GO.⁶⁸ As expected, in the XRD pattern of $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite, in addition to the

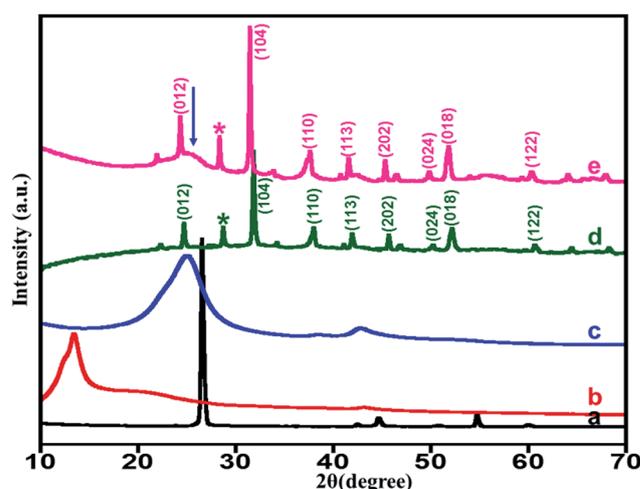


Fig. 1 XRD pattern of the (a) graphite, (b) GO, (c) HRG, (d) $\text{ZrO}_x(1\%)\text{-MnCO}_3$ and (e) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite [arrow mark indicating the presence of HRG].



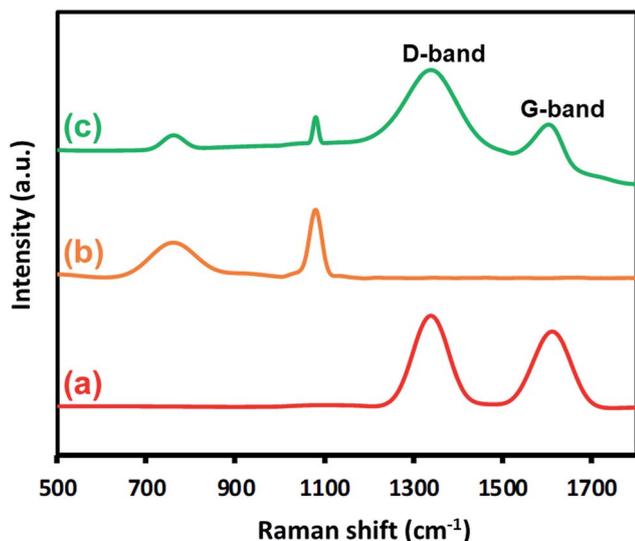


Fig. 2 Raman spectra of (a) HRG, (b) $\text{ZrO}_x(1\%)\text{-MnCO}_3$, and (c) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite.

characteristic reflections of $\text{ZrO}_x(1\%)\text{-MnCO}_3$ a broad shoulder (as indicated by arrow) at about $2\theta = 24.6^\circ$, indicating the presence of HRG in the composite.

Fourier transforms infrared spectrometer (FT-IR). The FT-IR spectra of GO, HRG, and $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ samples are shown in ESI (Fig. S1†). The FTIR spectrum of GO exhibits a broad peak at $\sim 3440\text{ cm}^{-1}$ due to stretching of hydroxyl groups (O–H) present on surface of GO, the absorption band at 1740 cm^{-1} is associated with (C=O) stretching of carboxylic groups (–COOH) on the surface,^{69,70} and the band at 1630 cm^{-1} is assigned to the stretching vibration of carbon backbone (C=C/C–C) from unoxidized in graphite lattice.⁷¹ The three absorption peaks at 1397, 1225, 1060 cm^{-1} belong to the stretching vibrations of (C–OH), (C–O–C) epoxy and (C–O) alkoxy, respectively.⁷² For HRG, the broad absorptions at 1214 cm^{-1} corresponding to (C–OH) stretching vibration and weak peak around 1634 cm^{-1} is related with (C=C) group due

to the skeletal aromatic.⁶⁹ However, by comparing the FT-IR spectrum of GO with $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite clearly displays that the complete reduction of most of oxygenated functional groups in the GO surface has occurred. The strong bands at 1740 , 1225 , and 1060 cm^{-1} related to (C=O), (C–O–C), and (C–O) stretching vibrations cannot be observed comparing with GO, indicating that the oxygen containing functional groups on GO surfaces were almost removed. The FTIR spectra of $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ is dominated by a peak at 1634 cm^{-1} corresponding to (C=C) stretching modes assigned to the skeletal aromatic vibration and wide absorption peak due to carbonate groups are observed at 1380 cm^{-1} .^{73,74} Sharp absorption peak located at approximately 590 cm^{-1} is assigned to Mn–O vibrations.⁷⁵

Raman spectra. Fig. 2 displays the Raman spectra of highly reduced graphene oxide (HRG), $\text{ZrO}_x(1\%)\text{-MnCO}_3$, and $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite. The characteristic peak at 1080 cm^{-1} is attributed to MnCO_3 and appeared in both $\text{ZrO}_x(1\%)\text{-MnCO}_3$ as well as $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite.⁷⁶ Also, the existence of highly reduced graphene oxide in the $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite is confirmed by the appearance of two main bands at ~ 1580 and 1350 cm^{-1} respectively, usually denoted as D band and G-band.⁷⁷ The D band is related to the disorder carbon structure induced by lattice defects and the G-band is associated to well-ordered structure.^{78,79} Fig. 2a shows a HRG spectrum, the G and the D bands are located at 1595 and 1360 cm^{-1} , respectively.^{80,81} Compared with HRG, the G characteristic band in $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ is shifted by $\sim 15\text{ cm}^{-1}$ from 1595 to 1580 cm^{-1} , whereas a slight shift was observed in the D-band from 1360 to 1350 cm^{-1} , indicating that the strong coupling between the MnCO_3 and highly reduced graphene oxide.^{75,82}

Scanning electron microscopy (SEM). The size and morphology of the as synthesized $\text{ZrO}_x(1\%)\text{-MnCO}_3$ and highly reduced graphene oxide supported $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ catalyst obtained by co-precipitation is monitored using scanning electron microscopy (SEM). Fig. 3 shows the SEM micrographs of the pure $\text{ZrO}_x(1\%)\text{-MnCO}_3$ after calcining at

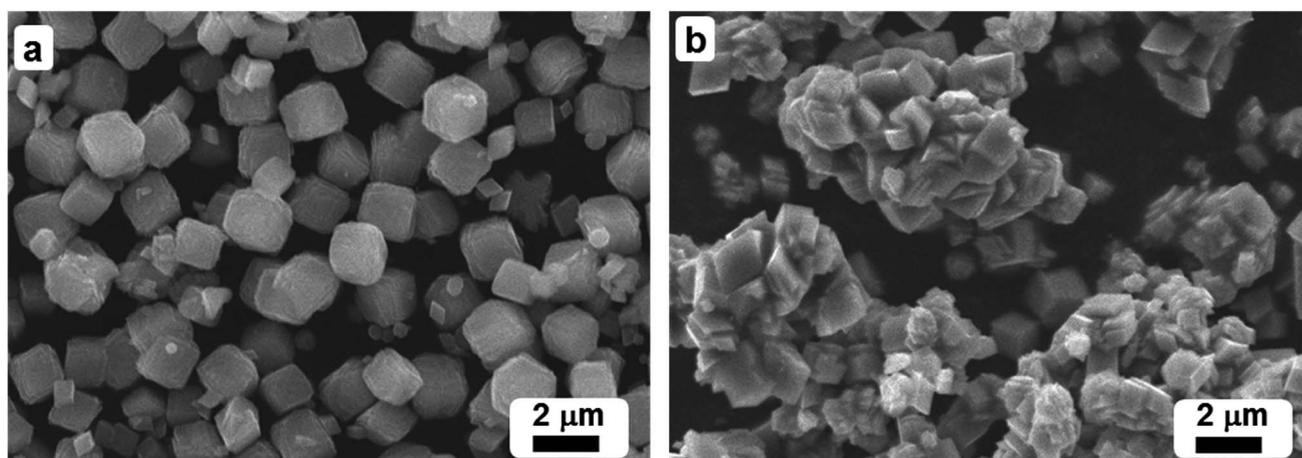


Fig. 3 SEM images of (a) $\text{ZrO}_x(1\%)\text{-MnCO}_3$, and (b) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite.



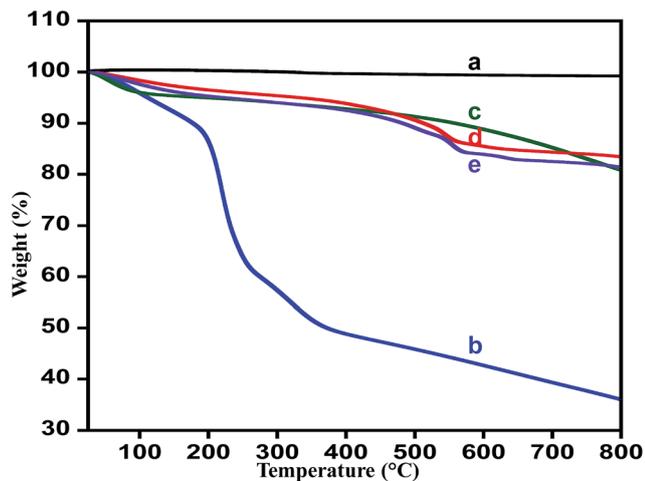


Fig. 4 TGA curves of (a) graphite, (b) graphene oxide (GO), (c) highly reduced graphene oxide (HRG), (d) $ZrO_x(1\%)-MnCO_3$, and (e) $ZrO_x(1\%)-MnCO_3/(1\%)HRG$.

temperatures 300 °C (Fig. 3a) and HRG supported $ZrO_x(1\%)-MnCO_3/(1\%)HRG$ (Fig. 3b). The pure $ZrO_x(1\%)-MnCO_3$ catalyst show well-defined cuboidal shape particles with size of particles in the micron meter but interestingly HRG supported $ZrO_x(1\%)-MnCO_3/(1\%)HRG$ (Fig. 3b), shows aggregation of rather smaller size crystals which looks like grown on the surface through surface nucleation/growth process. The composition of the catalyst is determined using EDX and stays within experimental error to the theoretical composition given in ESI (Table S1†).

Thermal stability. Thermogravimetric analysis (TGA) confirms the complete conversion of graphene oxide to HRG nano-sheets with hydrazine hydrate as reductant and thermal stability of the prepared catalyst. Fig. 4 displays the TGA patterns for the graphite, graphene oxide, highly reduced graphene oxide, $ZrO_x(1\%)-MnCO_3$ and $ZrO_x(1\%)-MnCO_3/(1\%)HRG$ nanocomposite respectively. The thermal stability of graphene oxide is much lower than the pristine graphite.⁸³ The thermogram obtained for pristine graphite shows that it undergoes a total weight loss of ~1%,⁸⁴ while graphene oxide undergoes a weight loss of ~65% within the experimental temperature range, which is very much in accordance with the previously reported literature.^{71,85} The TGA curve of highly reduced graphene oxide (HRG) exhibited overall weight loss of

around 20% at the same temperature range due to the reduction of the oxygen containing functional groups. The $ZrO_x(1\%)-MnCO_3/(1\%)HRG$ nanocomposite displayed total weight loss less than 18% in the identical temperature range (Fig. 4e), which is slightly more than the weight loss evident from the degradation pattern of $ZrO_x(1\%)-MnCO_3$ indicating that effective reduction of graphene oxide to HRG by eliminating most of the oxygen carrying functionalities like hydroxyl, carboxyl, epoxy, and carbonyl groups.⁸⁶

Surface-area measurements. To understand the relationship between the effectiveness of surface area of the synthesized catalyst and the catalytic activity for oxidation process, the BET analysis is carried out as shown in the Table 1. From the results obtained, it is found that the specific surface area of the catalyst $ZrO_x(1\%)-MnCO_3$ calcined at 300 °C was about $133.6 \text{ m}^2 \text{ g}^{-1}$, while the catalyst having (1%)HRG *i.e.* $ZrO_x(1\%)-MnCO_3/(1\%)HRG$ has surface area $211.03 \text{ m}^2 \text{ g}^{-1}$. The effect of HRG had explicit impact on the surface area of the catalyst, which in turn had an impact on the catalytic performance of catalyst, which will be discussed later.

Catalytic tests. The prepared material is explored for its catalytic performance as an oxidation catalyst using oxidation of benzyl alcohol to benzaldehyde as model reaction. Different catalysts are prepared by varying the percentage of HRG in the catalyst and calcination temperature. In addition, the influence of amount of catalyst, reaction time, and the reaction temperature is explored in detail.

Role of HRG on the catalytic performance. The catalytic performance of the catalyst can be fine-tuned using appropriate support or promoter.^{87–92} From our previously reported study, it was found that ZrO_x was found to be a very good promoter to the catalyst $MnCO_3$, and $ZrO_x(1\%)-MnCO_3$ was found to be the best catalyst for the oxidation of benzyl alcohol to benzaldehyde. In this study the catalyst $ZrO_x(1\%)-MnCO_3$ was selected and is further modified by addition of HRG in order to further fine-tune its catalytic performance. In the first place, efforts were directed towards identifying the appropriate amount of HRG (%) support/promoter in the catalyst. The catalytic studies revealed that the catalytic performance of the catalyst decreased drastically upon increasing the amount of HRG as support. Therefore, another attempt was made to use HRG as promoter. Various catalysts with varying the percentage of HRG, *i.e.* 1%, 3%, 5%, 7% HRG in the catalytic system were prepared and tested for their catalytic performance as oxidation catalyst. The catalyst $ZrO_x(1\%)-MnCO_3$ modified with addition of 1% HRG,

Table 1 Influence of calcination temperature on the catalytic performance^a

Entry	Catalyst	T (°C)	SA ($\text{m}^2 \text{ g}^{-1}$)	Conv. (%)	Sp. activity ($\text{mmol g}^{-1} \text{ h}^{-1}$)	Sel. (%)
1	$ZrO_x(1\%)-MnCO_3$	300	133.6	74.2	32.97	<99
2	$ZrO_x(1\%)-MnCO_3/(1\%)HRG$	300	211.0	100.0	44.44	<99
3	$ZrO_x(1\%)-Mn_2O_3$	500	17.5	17.1	2.87	<99
4	$ZrO_x(1\%)-Mn_2O_3/(1\%)HRG$	500	60.51	59.24	26.33	<99

^a Reaction conditions: 2 mmol of benzyl alcohol, 300 mg of catalyst, oxygen with rate 20 mL min^{-1} , reaction temperature at 100 °C, 10 mL of toluene, and 9 min of reaction time.



i.e. $\text{ZrO}_x(1\%)\text{-MnCO}_3/\text{HRG}(1\%)$ composites improved the catalytic activity drastically. The $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ composite was able to yield a 100% conversion product of benzaldehyde within 9 min of reaction time with very high specific activity $44.44 \text{ mmol g}^{-1} \text{ h}^{-1}$ given in ESI (Table S2,† entry 3). Further modifications were carried out by increasing the amount (wt%) of HRG with 3%, 5% and 7% of HRG. However, increasing the amount of HRG, led to a slight decrease in the catalytic performance, which resulted in the decrease of the oxidation product formed *i.e.* 93.3%, 84.1% and 67.3% benzaldehyde conversion product respectively (Table S2,† entries 4–6). It can be concluded that the highest yields of conversion product is obtained using 1 wt% of HRG as promoter for ZrO_x nanoparticles doped MnCO_3 within 9 min (Table S2,† entry 3) and also confirm that the HRG plays an important role as promoter in the enhancement of catalytic efficiency for the oxidation of benzyl alcohol. The plausible mechanism for catalytic enhancement could be the role of highly reduced graphene to increase the lifetime of charge carriers, which ultimately reacts with molecular oxygen to create reactive oxygen species to enhance the catalytic oxidation reaction. In order to understand that the HRG is just playing a role of a promoter and is not a catalyst, the catalytic activity of pure HRG (300 mg) for the aerobic oxidation of benzyl alcohol under similar conditions is studied. It is found that HRG yields only ~3% conversion product *i.e.* benzaldehyde, which indicates that it is not an active catalyst for the oxidation of benzyl alcohol. The obtained results are plotted in Fig. 5 and tabulated in Table S2.† Hence, from the results obtained it can be concluded that the catalyst $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ was the best among the all synthesized catalysts and based on these findings it is selected for the optimization of various other parameters.⁸⁵

Effect of calcination temperature on the catalytic performance. Calcination has a profound effect on the composition of the material prepared, with its such as changes in the oxide composition, surface morphology and surface area. These factors in turn, effects the catalytic performance of the material. Therefore, as synthesized composites are subjected to calcination process under atmospheric air at 300, and 500 °C. The calcined product are tested for their catalytic performance as oxidation catalyst. The results revealing the effect of calcination temperature are plotted in Fig. 6 and tabulated in the Table 1. The results obtained revealed that the calcination treatments of the nanocomposites has an inhibiting effect on the catalytic performance *i.e.* oxidation process with a decrease in the conversion of the oxidation product.⁹³ The catalyst calcined at 300 °C *i.e.* $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ exhibited the highest catalytic performance which yielded a 100% of benzaldehyde from the oxidation of benzyl alcohol within a reaction time of 9 min. While, the catalysts calcined at 500 °C, yielded a 59% conversion of benzyl alcohol within the same reaction time under similar circumstances. The specific activity in case of catalyst calcined at 300 °C *i.e.* $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ was determined to be $44.44 \text{ mmol g}^{-1} \text{ h}^{-1}$, whereas in case of catalysts calcined at 500 °C *i.e.* $\text{ZrO}_x(1\%)\text{-Mn}_2\text{O}_3/(1\%)\text{HRG}$ was found to decrease to $26.33 \text{ mmol g}^{-1} \text{ h}^{-1}$. When the results

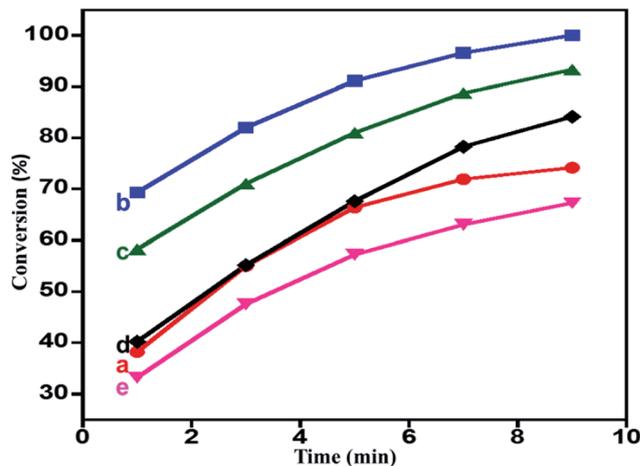


Fig. 5 Graphical representation of benzyl alcohol oxidation catalyzed by (a) $\text{ZrO}_x(1\%)\text{-MnCO}_3$, (b) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$, (c) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(3\%)\text{HRG}$, (d) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(5\%)\text{HRG}$, and (e) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(7\%)\text{HRG}$.

obtained are compared to the catalyst without HRG *i.e.* $\text{ZrO}_x(1\%)\text{-MnCO}_3$, it was found that under similar reaction conditions and within 9 min of reaction time, the conversion product obtained was only 74%. The specific activity of the catalyst *i.e.* $\text{ZrO}_x(1\%)\text{-MnCO}_3$, was found to be $32.97 \text{ mmol g}^{-1} \text{ h}^{-1}$, which was 1.35 times lesser than specific activity of the catalyst containing HRG. Interestingly, the results obtained from the catalytic evaluation can be correlated to the surface area values (BET measurements) of the prepared catalyst as well. Nevertheless, the selectivity towards benzaldehyde was almost independent of surface area. The obtained results include benzyl alcohol conversion, surface area, specific activity and selectivity over the catalyst are listed in Table 1.

Effect of reaction temperature on the catalytic performance. Reaction temperature also influence catalytic performance;

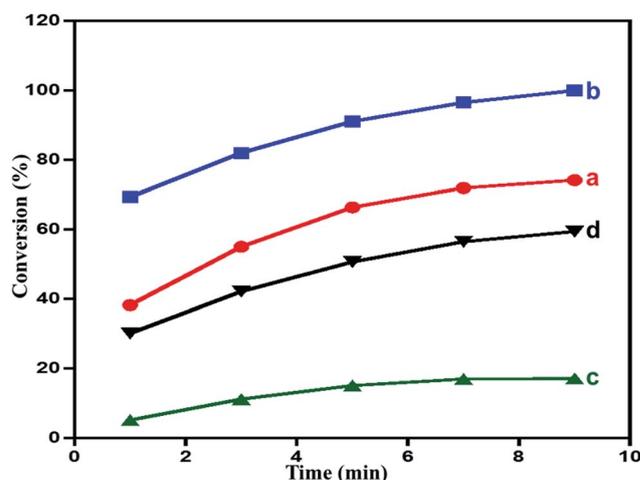


Fig. 6 Time vs. conversion plot in the aerobic oxidation of benzyl alcohol catalyzed by (a) $\text{ZrO}_x(1\%)\text{-MnCO}_3$, (b) $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$, (c) $\text{ZrO}_x(1\%)\text{-Mn}_2\text{O}_3$, and (d) $\text{ZrO}_x(1\%)\text{-Mn}_2\text{O}_3/(1\%)\text{HRG}$.



hence, a study was carried out by varying the reaction temperature from 20 °C to 100 °C, such as 20, 40, 60, 80 and 100 °C for the aerobic oxidation of benzyl alcohol over the $ZrO_x(1\%)-MnCO_3/(1\%)HRG$ under similar conditions. The results obtained are tabulated in ESI (Table S3†), the graphical representation of the conversion product (percentage) obtained is given in Fig. 7. The obtained results indicated that the temperature plays an essential role on rate of oxidation of benzyl alcohol, for example, as compared to the reaction carried out at 20 °C, (38.4%), under identical conditions a 100% conversion product and >99% selectivity towards benzaldehyde was observed at 100 °C. To our observation, best results were obtained by maintaining the reaction temperature at 100 °C to achieve an optimum activity of the catalyst $ZrO_x(1\%)-MnCO_3/(1\%)HRG$.

Effect of catalyst amount on the catalytic performance. The role of catalyst amount during the oxidation of benzyl alcohol to benzaldehyde was assessed by varying the amount of catalyst from 100 mg to 500 mg, while other optimized parameters were unchanged (Table 2). The results obtained clearly displays that as the amount of catalyst is decreased from 500 mg, which was used in all earlier studies, the conversion product formed also decreases. When 100 mg of catalyst is used the percentage of conversion product formed was about 22%, while with the 500 mg of catalyst is employed it yielded 100% conversion within extremely short reaction time (4 min) under similar set of reaction conditions. Moreover, there is no effect on the selectivity. A linear correlation is found between the amount of catalyst and conversion of benzyl alcohol as shown in Fig. 8.

In order to confirm that the oxidized product *i.e.* benzaldehyde, is actually obtained by the oxidation of benzyl alcohol and not upon oxidation of toluene (solvent), the oxidation process is performed without the substrate *i.e.* benzyl alcohol, under optimum conditions. It is found that no desired oxidation product (benzaldehyde) was detected. Accordingly, it can be deduced that the oxidation product obtained is formed because of the catalytic oxidation of benzyl alcohol and not from the oxidation of toluene. Likewise, a blank experiment was

Table 2 The influence of amount of catalyst $ZrO_x(1\%)-MnCO_3/(1\%)HRG^a$

Entry	Catalyst amount (mg)	Conv. (%)	Sp. activity (mmol g ⁻¹ h ⁻¹)	Sel. (%)
1	100	22.2	66.48	<99
2	200	42.0	63.03	<99
3	300	61.6	61.57	<99
4	400	81.4	61.06	<99
5	500	100.0	60.00	<99

^a Reaction conditions: 2 mmol of benzyl alcohol, calcination temperature at 300 °C, oxygen with rate 20 mL min⁻¹, reaction temperature at 100 °C, 10 mL of toluene, and 4 min of reaction time.

conducted in the absence of the catalyst under similar conditions to assure that the oxidation product is being obtained due to the catalytic performance of the catalyst and not due to the self-oxidation of benzyl alcohol.

The plausible mechanism based on literature, spectroscopic data available and our previous experience could involve the following steps; (i) the ZrO_x dispersed on $MnCO_3$ will provide basic sites to promote the dehydrogenation step of the alcohol^{94,95} (ii) the $MnCO_3$ in the presence of molecular oxygen oxidized easily to high-valent Mn; most likely to $\gamma-MnOOH$ ^{96,97} and organic molecule oxidizes at the expense of these high-valent Mn active sites. (iii) The HRG in this case, promotes the reaction by assisting in fast transferring the charges for the re-oxidation of the Mn^{2+} species back into its high valance state Mn^{4+} ($\gamma-MnOOH$), which is formed during the transfer of lattice oxygen to benzyl alcohol resulting in the formation of reactive carbocation species. During this process the carbocation can be rapidly deprotonated to benzaldehyde and the reduced Mn^{2+} species is oxidized to Mn^{4+} .

Oxidation of various benzylic and aliphatic alcohols. The catalyst ($ZrO_x(1\%)-MnCO_3/(1\%)HRG$) is also examined under optimized conditions for the oxidation of a wide range of derivatives of benzyl alcohol and citronellol (as an aliphatic

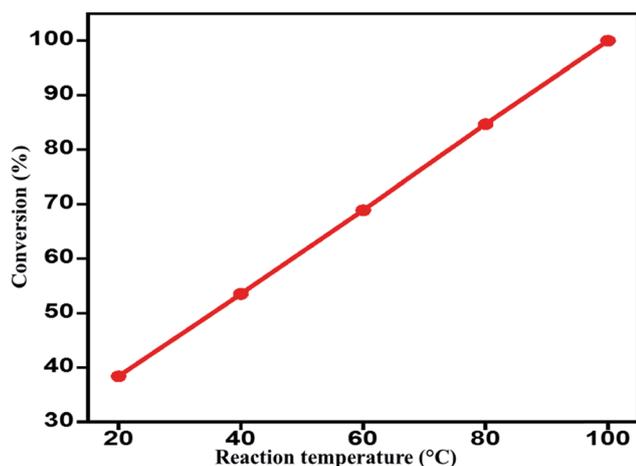


Fig. 7 Effect of reaction temperature on the oxidation of benzyl alcohol over $ZrO_x(1\%)-MnCO_3/(1\%)HRG$.

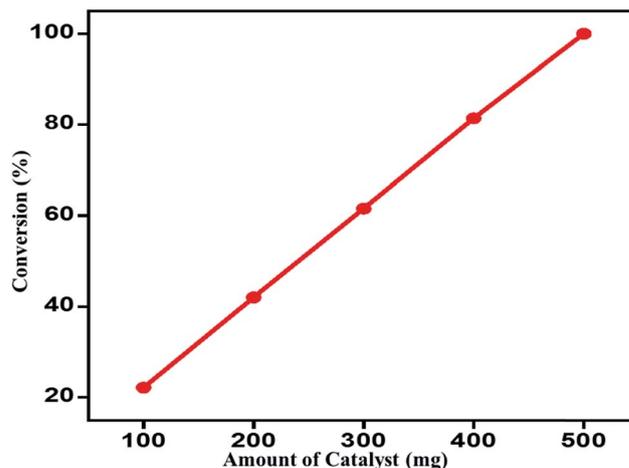


Fig. 8 Effect of catalyst amount on the benzyl alcohol conversion over $ZrO_x(1\%)-MnCO_3/(1\%)HRG$.



Table 3 Aerobic oxidation of benzyl alcohol derivatives using $ZrO_x(1\%)$ - $MnCO_3/(1\%)$ HRG nanocomposite^a

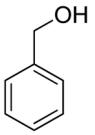
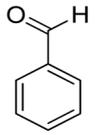
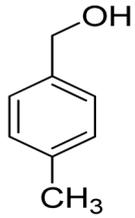
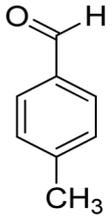
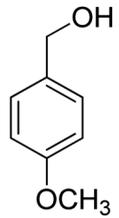
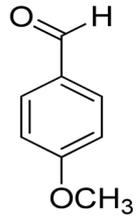
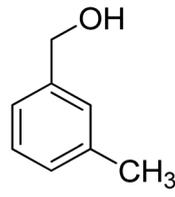
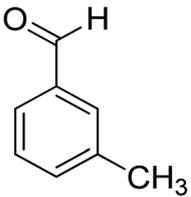
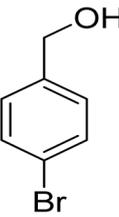
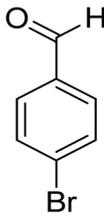
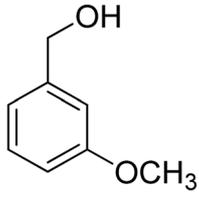
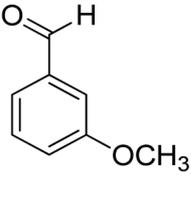
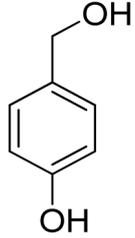
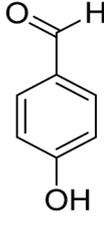
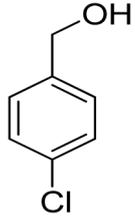
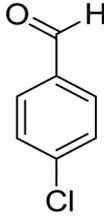
R. No.	Reactants	Products	Time (min)	Conv. (%)	Sel. (%)
1			4	100	>99
2			4	100	>99
3			4	100	>99
4			5	100	>99
5			6	100	>99
6			5	100	>99
7			5	100	>99
8			6	100	>99



Table 3 (Contd.)

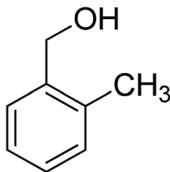
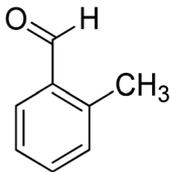
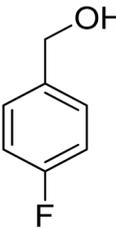
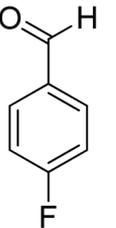
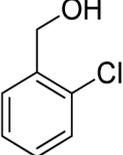
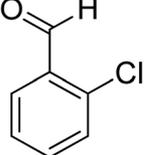
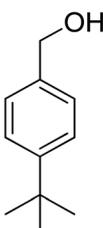
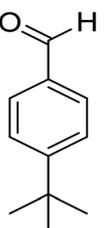
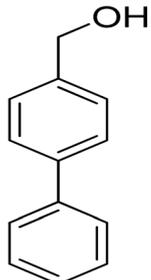
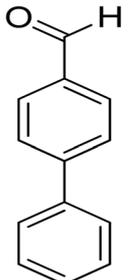
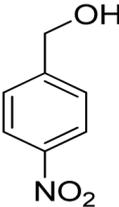
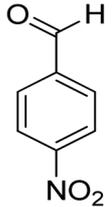
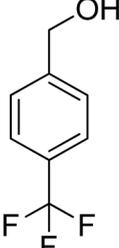
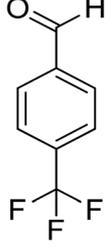
R. No.	Reactants	Products	Time (min)	Conv. (%)	Sel. (%)
9			6	100	>99
10			6	100	>99
11			6	100	>99
12			7	100	>99
13			6	100	>99
14			8	100	>99
15			7	100	>99



Table 3 (Contd.)

R. No.	Reactants	Products	Time (min)	Conv. (%)	Sel. (%)
16			7	100	>99
17			11	100	>99
18			12	100	>99
19			13	100	>99
20			15	100	>99
21			80	100	>99

^a Reaction conditions: 2 mmol of alcohol, 0.5 g of catalyst amount, calcination temperature at 300 °C, oxygen with rate 20 mL min⁻¹, reaction temperature at 100 °C, and 10 mL of toluene.

alcohol) using molecular O₂. The results were compiled in Table 3. Under the optimized reaction conditions, various benzylic alcohols (2 mmol) in toluene (10 mL) and oxygen flow rate (20 mL min⁻¹) at 100 °C reaction temperature and 500 mg of catalyst calcined at 300 °C were oxidized to their corresponding aldehydes at different reaction times. According to Table 3, all substituted benzyl alcohols are smoothly converted

into corresponding aldehydes with 100% convertibility in relatively short reactions times (Table 3, entries 1–20). In addition, more than 99% selectivity toward corresponding aldehydes is achieved in all oxidation experiments and no over-oxidation such as carboxylic acids is detected in the reaction mixture. Traditionally, the oxidation of aliphatic alcohols is much more difficult than aromatic.^{98,99} In this context, the oxidation of



aliphatic alcohol such as citronellol is a relatively slow with respect to aromatic alcohols, may be due to the absence of conjugation in the β -position of the hydroxyl group. As expected, citronellol required longer reaction time to complete conversion to citronellal (Table 3, entry 21). Therefore, it can be said that the prepared catalyst have higher activity towards oxidation of aromatic alcohols than aliphatic alcohols. The obtained results clearly showed that electronic effects play an essential role on the rate of the oxidation process. The electron-rich benzylic substrates containing electron-donating groups are found to be most reactive and exhibit shorter oxidation times, whereas times for electron-deficient benzylic alcohols are longer.^{100,101} Oxidation of derivatives of benzyl alcohol bearing electron donating groups such as ($-\text{CH}_3$, $-\text{OCH}_3$, $-\text{OH}$, and $-\text{C}(\text{CH}_3)_3$) resulted in formation of the corresponding aldehyde derivatives with complete conversions in relatively short reaction times. Whilst, the substitution with electron withdrawing groups such as ($-\text{Cl}$, $-\text{F}$, $-\text{NO}_2$, and $-\text{CF}_3$) decreases the rate of reaction and needed a longer time for a complete conversion. The increase in conversion% in case of substrates containing electron donating groups may be attributed to the adequate electron density in the active center, as compared to the benzylic alcohols with electron withdrawing groups.^{102,103} For instance, the benzylic alcohol with a *para*-electron donating group such as 4-methylbenzyl alcohol is completely oxidized to its corresponding aldehyde only in 4 min (Table 3, entry 2). Whereas, 4-(trifluoromethyl)benzyl alcohol which bearing a *para*-electron withdrawing group, require longer reaction time (7 min) (Table 3, entry 15). On the other hand, *para*-substituted alcohols give complete conversion after shorter reaction periods relative to *ortho*- and *meta*-substituent, possibly due to *para*-position has minimum steric hindrance in comparison to other derivatives.^{104,105} For instance, *para*-nitrobenzyl alcohol was completely converted to its corresponding aldehyde within only 8 min (Table 3, entry 14), while for *meta*- and *ortho*-nitrobenzyl

alcohol are completely oxidized into their corresponding aldehydes after relatively longer time 11 and 13 min, respectively as compared to the *para*-substituent (Table 3, entries 17 and 19). Steric hindrance is also a significant factor that affects the rate of the oxidation reactions, the bulky groups such as (2,3,4-Tri-Ome, $-\text{C}(\text{CH}_3)_3$, $-\text{CF}_3$, 2,4-DiCl and 2,3,4,5,6-pentafluoro) attached to the benzyl alcohol decreases the performance of oxidation reaction and required longer reaction time. This is probably due to the presence of the steric resistance that hinder the oxidation of the bulky substituents benzylic alcohols (Table 3, entries 12, 15, 16, 18, 20).¹⁰⁶ Therefore, it can be concluded that the catalytic oxidation of benzyl alcohol derivatives catalyzed using $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite is affected by two factors, electronic density and steric hindrance.

To compare our catalyst with the previously reported catalysts, the obtained results of the catalytic performance of $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite has been compared with previously reported catalysts possessing graphene in the catalytic system employed for the oxidation of benzyl alcohol. The comparison is made with respect to their conversions, selectivity, reaction times, specific activities, and reaction temperatures and the findings are compiled in Table 4. From the information compiled in Table 4, it can be understood that the catalyst reported in this study allowed the oxidation of benzyl alcohol derivatives in relatively short reaction times under mild reaction conditions as compared to the methods described in the literature. Among all these, the synthesized $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite (from present study) exhibited highest specific activity.

Catalyst reusability. The recycling of the catalyst has tremendous importance from industrial usage point, therefore, the reusability and stability of $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ catalyst for the selective oxidation of benzyl alcohol using molecular oxygen is examined under similar conditions. After the completion of reaction, the solvent was evaporated and

Table 4 Comparison of the $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite for the oxidation of benzyl alcohol with earlier reported catalyst with graphene support

Catalyst	Conv. (%)	Sel. (%)	Temp. (°C)	Time	Sp. activity (mmol g ⁻¹ h ⁻¹)	Ref.
$\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$	100	<99	100	4 min	60.0	This work
$\text{ZrO}_x(1\%)\text{-MnCO}_3$	100	<99	100	5 min	48.0	63
1%RGO-MnCoO	78	100	140	2 h	12.64	90
Au NPs-HRG	75	<99	130	4 h	23.15	85
Pd/GO	36.2	34.1	110	6 h	0.97	87
Ag NPs/rGO	12	8	80	24 h	1.0	107
Ag NPs/GO	33	55	80	24 h	2.75	107
Au/RGO	65	93	100	8 h	5.42	89
GO-N-PW	76	99	100	6 h	10.57	108
GO-100	100	100	80	2 h	1.11	71
$\text{CoO}_x/\text{RGO-HP}$	96	<99	110	6 h	14.8	109
$\text{FeO}_x/\text{RGO-HP}$	64	<99	110	6 h	9.87	109
$\text{NiO}_x/\text{RGO-HP}$	28	<99	110	6 h	4.32	109
$\text{Fe}_3\text{O}_4\text{-Pt/rGO}$	33.6	100	80	3 h	42.0	91
Au/NG-4.0	67	40	70	6 h	0.37	110
APTMS/GO	97	93	65	20 min	14.55	111
Pd(II)-AAPTMS@GO	96	99	60	3 h	2.13	112
$\text{TiO}_2\text{-0.1% GR}$	60	<99	<i>hv</i>	4 h	0.94	92



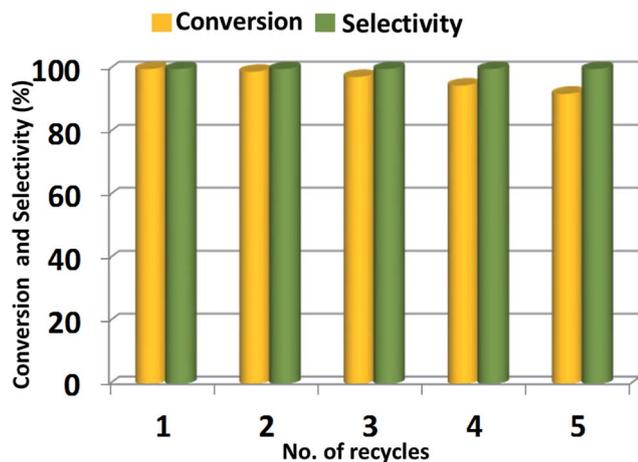


Fig. 9 Recyclability of $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite in the aerobic oxidation of benzyl alcohol. Reaction conditions: 2 mmol of benzyl alcohol, 0.5 g of catalyst, 10 mL of toluene, calcination temperature at 300 °C, oxygen with flow rate 20 mL min^{-1} at 100 °C for 4 min.

fresh toluene was added and the used catalyst is separated using centrifugation. The used catalyst is washed sequentially with toluene and dried at 100 °C for 4 h. The recovered $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ was then re-used for the same reaction under similar reaction conditions and the conversion product was monitored using GC. After five consecutive cycles, there is no appreciable loss in the catalytic activity of the recycled catalyst *i.e.* $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$. The conversion of benzyl alcohol decreases gradually from 100% to 92% after five runs while the selectivity towards benzaldehyde remains unchanged *i.e.* <99% during all recycling experiments. The decrease in the catalytic performance is partly attributed to the mass loss during the filtration method.¹¹³ Therefore, it can be said that the $\text{ZrO}_x(1\%)\text{-MnCO}_3/(1\%)\text{HRG}$ nanocomposite is a stable catalyst. The results obtained from this study are represented in Fig. 9. Moreover, the used catalyst retained its phase and crystallinity even after 5 cycles (Fig. S2†).

Conclusion

In conclusion, we present here an efficient ZrO_x doped MnCO_3 on highly reduced graphene oxide catalyst for the selective oxidation of derivatives of benzyl alcohol to corresponding aldehydes using green procedure, *i.e.* using molecular O_2 as an environmentally friendly oxidizing agent under base-free condition. A complete benzyl alcohol conversion (100%) was achieved within only 4 min along with 60.0 $\text{mmol g}^{-1} \text{h}^{-1}$ specific activity, which is higher than the specific activity of many catalysts already reported. Moreover, the selectivity obtained for corresponding aldehydes is very high *i.e.* >99%, for all the alcohols used in the present work. The performance of the catalytic protocol has remarkably improved upon addition of HRG for the selective oxidation of alcohols. Broad range of substituted benzyl alcohols were evaluated for selective oxidation to corresponding aldehydes, a 100% conversion product with >99% selectivity with short reaction times were obtained

under mild reaction conditions. The oxidation of benzylic alcohols bearing electron-donating groups required shorter reaction times than those containing electron-withdrawing or bulky groups to corresponding aldehydes. Moreover, the oxidation of aliphatic alcohols such as citronellol is more difficult than benzylic alcohols, which may be due to lack of the conjugation. The as-prepared catalyst exhibits remarkable recyclability, excellent performance for its reuse and product selectivity stayed roughly unchanged (above 99%). The apparent merits of our catalytic protocol are: (a) benign synthetic methodology; (b) environmentally friendly oxidant; (c) no additives or bases are required for the oxidation process; (d) mild reaction conditions; (e) complete convertibility; (f) complete selectivity; (g) short reaction time; and (h) reusable heterogeneous catalyst. All these superiorities will give rise to this protocol to be very much beneficial and applicable for the alcohol oxidation.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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