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Fabrication of free-standing membranes with tunable pore structures based on the combination of electrospinning and self-assembly of block copolymers†

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In this study, free-standing composite membranes with tunable pore structures are fabricated by combining electrospinning and block copolymer (BCP) self-assembly and a facile biomimetic surface modification method is employed for improvement of the interfacial interaction in the composite membranes. Firstly, polystyrene-*block*-poly(2-vinyl pyridine) (PS-*b*-P2VP) solution is drop-coated onto a electrospun PVA/SiO₂ fiber mat which provides mechanical reinforcement, fabricating symmetric (thickness, 17 ± 2 μm) and asymmetric (thickness, ~5 μm) composite membranes. The pore structures in the PS-*b*-P2VP matrix are realized by selectively swelling the P2VP block in hot ethanol and can be tuned by adjusting swelling time and swelling temperature. Moreover, pretreating the electrospun PVA/SiO₂ fibres with adhesive polydopamine (PDA) coating improves the adherence between the BCP layer and the electrospun fibres remarkably. The results of ultrafiltration performance test show the excellent performance of the composite membrane for the immobilization and capture nanoparticles (NPs).

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Introduction

Nonwoven fibrous membranes fabricated by electrospinning are promising candidates for filtration and separation because of their outstanding properties, such as excellent tensile strength, large surface area per unit volume, high porosity, interconnected porous structure, and design versatility.^{1–3} However, their drawbacks, which are attributed to the geometrical structure of their pores, wide pore size distribution, and undesirable macrovoid formation across the entire membrane thickness, result in decreased retention and poor selectivity.⁴ As a result, the practical applications of electrospun fibrous membranes are limited.

Recently, porous membranes based on block copolymers (BCPs) have attracted considerable attention due to their tunable nanoporous structures, which are achieved *via* microphase separation.^{5–7} Several studies have indicated that porous BCP membranes show great potential in ultrafiltration.^{8,9} For

example, Uehara *et al.* demonstrated that a series of flexible nanoporous membranes from PS-*b*-PMMA exhibiting a bicontinuous crystalline-amorphous phase-separation system have potential application in size-selective molecular diffusion at the nanoscale.¹⁰ However, low mechanical strength of free-standing BCP membranes is an obstruction for their ultrafiltration application. In order to enhance the mechanical properties, non-solvent induced phase separation (NIPS) process has been developed to produce integral asymmetric block copolymer membranes with ordered cylindrical nanopores on top of the disordered layer.^{11,12} By using this method, Xie *et al.* prepared membranes from polysulfone-based block copolymers which show greatly improved mechanical strength.¹³ Schacher *et al.* also obtained self-supporting porous membranes with double stimuli-responsiveness from a polystyrene-*block*-poly (N,N-dimethylaminoethyl methacrylate) (PS-*b*-PDMAEMA) block copolymer.¹⁴ However, the membranes resulting from NIPS will be expensive due to the increase of BCPs use. Therefore, fabricating nanoporous BCP membranes supported on micro/macroporous substrates, such as the commercial polysulfone,¹⁵ polyethersulfone,^{16–18} polyacrylonitrile,¹⁹ polyvinylidene fluoride²⁰ microfiltration membrane, has been gaining as an alternative. In this study, a nanoporous BCP membrane was combined with an electrospun macroporous membrane to obtain a composite membrane with enhanced mechanical stability and improved the nanoparticle (NP) entrapment efficiency of the latter.

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However, weak adhesion and even peeling at the interface results from the incompatible surface properties of the nanoporous BCP layer and the substrate. These issues further hinder the extensive application of BCPs to perfect ultrafiltration. Various surface modification techniques have been proposed to improve the interfacial interaction between the different phases of a composite membrane.^{21–25} However, the proposed methods themselves exhibit drawbacks, such as the use of complex instruments, limitations in substrate size and shape, and elaborate procedures, which restrict their widespread implementation. Messersmith *et al.* offered a solution to this problem by proposing a facile and versatile surface modification method of coating surfaces with an adhesive polydopamine (PDA) film.²⁶ The oxidant-induced auto-polymerization of dopamine to nearly any surface allows for the direct dipping of a substrate into an aqueous dopamine solution with a slightly basic pH to realize PDA coating. The ultrathin and highly hydrophilic coating exhibits a powerful adhesive ability to attach foreign objects, indicative of a favorable property for improving the interface performance of composite membrane and enhancing the adhesion between two incompatible phases.^{27–29} Compared with other surface modification methods, PDA coating is attractive because of its versatility, simplicity, low cost, and nonpolluting property.

Therefore, in this work, adhesive PDA coating was used to improve the interfacial interaction between the electrospun fibers and BCP layer in the composite membranes which are fabricated by drop-coating polystyrene-*block*-poly(2-vinyl pyridine) (PS-*b*-P2VP) onto the electrospun PVA/SiO₂ macro-porous membranes (Fig. 1). The nanopores in the PS-*b*-P2VP matrix were produced by the selective swelling of P2VP in hot ethanol. Both pore structure and pore size were adjusted by regulating swelling temperature and swelling time. The

obtained hierarchical composite membranes exhibited excellent rejection rate for Au NPs with an average diameter of ~50 nm, suggesting the considerable potential in separation.

Experimental

Materials and methods

Polyvinyl alcohol (PVA) was purchased from Alfa Aesar. Tetraethyl orthosilicate (TEOS) were obtained from Sinopharm Chemical Reagent Beijing Co., Ltd. Dopamine hydrochloride and trimethylaminomethane were obtained from J&K Scientific Ltd. Tetrahydrofuran (THF), phosphoric acid (H₃PO₄) and hydrochloric acid (HCl) were purchased from Beijing Chemical Reagents Company and used without any purification. Polystyrene-*block*-poly(2-vinyl pyridine) (PS-*b*-P2VP) prepared *via* reversible addition fragmentation chain transfer (RAFT) polymerization described in the ESI.†

Electrospinning of PVA/SiO₂ fibrous membrane

TEOS (4.16 g) and deionized water (3.96 g) were mixed in a small beaker and then aqueous H₃PO₄ was added by dropwise under vigorous stirring. The molar ratio of the composition was TEOS : H₂O : H₃PO₄ = 1 : 11 : 0.1. After stirring for 60 min, 10 wt% PVA (8.0 g) was gradually dropped into the resulting silica gels, then the mixture was reacted in 60 °C oil bath by magnetically stirring for 2 hours. The obtained homogeneous solution was put into a 10 mL plastic syringe with a stainless steel needle. The needle was connected to a high-voltage generator as anode while the cathode was connected to a collector covered with a piece of aluminum foil. A voltage of 16 kV and a constant flow rate of 16 μm min⁻¹ were applied to the solution with the tip-to-collector distance was 20 cm. After electrospinning for 5 hours, the collected PVA/SiO₂ fibers with certain thickness were peeled off the surface of aluminum foil and dried at 80 °C under vacuum for 12 hours to enhance crosslinking of PVA and silica. Then the PVA/SiO₂ fibrous membranes were cut into circular shapes about 25 mm of diameter for next experimental usage.

Modification of PVA/SiO₂ fibrous membrane

The PVA/SiO₂ fibers were modified with PDA by immersing the membrane into 2 mg mL⁻¹ dopamine hydrochloride solution which was prepared by dissolution of dopamine hydrochloride in Tris-HCl buffer aqueous solution (10 mM, pH 8.5).^{28,30} After coating 12 hours, the PVA/SiO₂ fibrous membranes were rinsed with deionized water and blow-dried with nitrogen.

Preparation of symmetric composite membrane

PS-*b*-P2VP synthesized in our work was dissolved in THF to yield homogeneous solutions with different concentrations. Then 1.0 mL of the solution was slowly dropped on the PVA/SiO₂ fibrous membranes or PDA-modified PVA/SiO₂ fibrous membranes. The PS-*b*-P2VP solution was absorbed by the macropores in the fibrous membranes to form composite structures. Next, confined swelling-induced pore-making strategy was used to generate nanopores in the composite

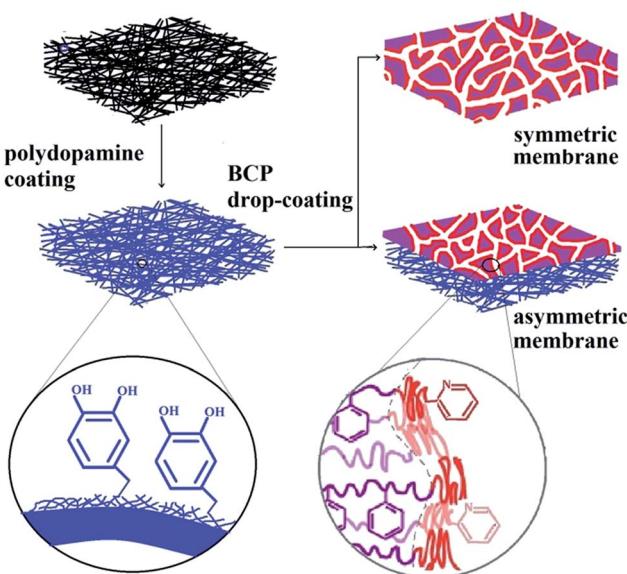


Fig. 1 Schematic illustration of free-standing composite membranes by combining electrospinning with phase-separation of block copolymer.



membranes. The composite membranes were dipped in ethanol bath for a given time at different temperature, and then placed at room temperature for 6 hours after redrawing from ethanol bath for volatilization of ethanol.

Preparation of asymmetric composite membrane

PDA-modified PVA/SiO₂ fibrous membranes were put into water for 60 min. Then the membranes saturated with water were placed at room temperature for a period time to volatilize the water on the surface. 1–3 wt% PS-*b*-P2VP/THF solution was dropped on the membranes lightly. Instantly the membranes were inclined 45° left and right to ensure the uniform spread of PS-*b*-P2VP solution. Then the pore-making strategy which was same as that of symmetric composite membranes was taken.

Ultrafiltration performance

Golden particles prepared in the laboratory with diameter of ~50 nm were dispersed in water to get a red dispersion and suspension. Then symmetric composite membrane with a thickness of 17 ± 2 μm and average nanopores of 38 nm was used to filter the golden particles in room temperature.

Characterization

The morphologies of the fabricated membranes were observed using a field emission scanning electron microscopy (FESEM) on a JEOL JSM-5400 system. The surface chemical structures of the PVA/SiO₂ electrospun fibers before and after PDA coating were characterized by Attenuated Total Reflection-Fourier Transform Infrared Spectra (ATR-FTIR) on a Perkin Elmer Spectrum GX at range of 4000–400 cm⁻¹. N₂ adsorption-desorption was measured on a Micrometrics ASAP-2020 sorption meter at 77 K. Before analysis, the samples were degassed at 323 K under a vacuum for 360 min. Brunauer–Emmett–Teller (BET) method was employed to calculate the specific surface area in the range of relative pressure from 0.05 to 0.2 and Barrett–Joyner–Halenda (BJH) model was used to calculate the pore volume and pore size distributions of the symmetric composite nanoporous membrane. Transmission electron microscope (TEM) imaging was collected on an H-7650B electron microscope operating at 120 kV by dispersing the fibers in ethanol and then drop-coating the copper grids. The wetting ability of the PVA/SiO₂ fibrous membrane before and after PDA coating was conducted with a video-based OCA 15 contact angle goniometer at 20 °C.

Results and discussion

Electrospun PVA/SiO₂ fibrous membrane

In the current work, a PVA/SiO₂ fibrous membrane prepared by electrospinning following methods described in previous report³¹ was selected as the macroporous skeleton of the composite membrane. Aside from sufficient mechanical strength, which is necessary for membrane filters, solvent resistance is required for an electrospun fibrous support given that the BCP coating dissolves in organic solvent. The enhanced stability in water or organic solvents and the improved mechanical properties of the

PVA/SiO₂ fibers can be achieved by modulating the ratio of TEOS and PVA because of the crosslinking of PVA chains with the silica network *via* Si–O–C–O–Si bridges.^{32,33} For the preparation of the PVA/SiO₂ fibrous membrane, the collection distance, the solvents and some other parameters have effects on the morphology and diameter of the obtained fibers. In general, increasing the collection distance will reduce the electric field intensity but facilitate the volatilization of solvents, which ultimately have a combined effect on the diameter of fibers. The surface tension of the precursor solution and the volatility of the solvent also play an important role in the morphology of the fibers. For example, higher surface tension may result in fibers with bead defects. One of the most common solvents for electrospinning is water, which is also the benign solvent for the PVA. Thus, in our work, the spinning solution was prepared by dissolve the precursor in H₂O and the collection distance of 15 cm was applied. The SEM images and optical photo of the PVA/SiO₂ fibrous membrane are presented in Fig. 2. Smooth-surfaced fibers with regular morphologies and diameters of approximately 1000 nm are randomly distributed in the membrane. A three-dimensional framework with a pore size ranging from several microns to tens of microns was formed. The TEM image of the original electrospun fibers is shown in Fig. 2d, which confirms that the fibers are homogeneous and have no extra shells. The fibrous membrane was briefly heated to 80 °C to further crosslink PVA and TEOS to improve the mechanical strength and solvent resistance of the membrane.

Modification of PVA/SiO₂ fibrous membrane

After coating with PDA, the morphology and integrity of the membrane and fibers were retained (Fig. 3a). However, it can be

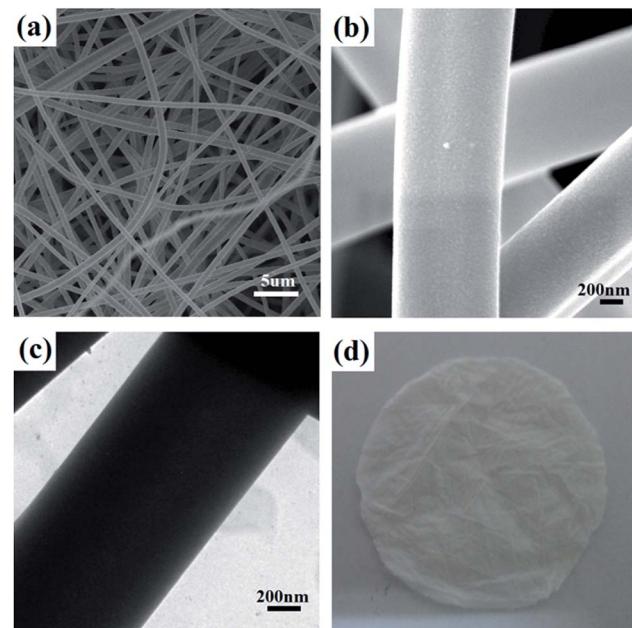


Fig. 2 (a and b) SEM images of the as-prepared PVA/SiO₂ fibrous membrane at different level of magnification; (c) TEM image of the as-prepared PVA/SiO₂ fibers; (d) optical photo of the as-prepared PVA/SiO₂ fibrous membrane.



seen from the SEM image at higher magnification that the surface of the fibers are rough after PDA coating (Fig. 3b), which results from the formation of a thin layer with densely dispersed PDA dots. The thickness of the PDA layer is approximately 30 nm, as shown in the TEM image in Fig. 3c. The color of the PVA/SiO₂ membrane changed from white to dark brown (Fig. 3d), also providing evidence of the formation of the PDA layer.^{26,34}

The ATR-FTIR spectra of the as-prepared PVA/SiO₂ fibrous membrane and PDA-coated PVA/SiO₂ fibrous membrane were recorded to determine the surface chemical composition, and the results are shown in Fig. 4a. The characteristic peaks at 1445–1610 cm⁻¹ of the ATR-FTIR spectrum of the PDA-coated PVA/SiO₂ fibrous membrane are assigned to the C–C vibration of benzene ring moiety and the N–H bending vibration of the dopamine molecules, directly proving the formation of PDA on the surfaces of the fibers.

Static water contact angle measurements were conducted to study the surface wettability of the as-prepared PVA/SiO₂ fibrous membrane before and after PDA coating. As shown in Fig. 4b, after coated with a layer of PDA, the water contact angle of PVA/SiO₂ fibrous membrane decreased from 132° to 119° owing to the hydrophilic groups such as imino and benzene hydroxyl groups in the PDA chains.

Preparation of symmetric composite membrane

Firstly, the as-prepared electrospun PVA/SiO₂ fibrous membrane without prior surface modification was used to prepare the free-standing composite membrane by drop coating a 2 wt% solution of PS-*b*-P2VP (Mn (PS) = 62, 400 mol kg⁻¹; Mn (P2VP) = 24, 150 mol kg⁻¹) in THF. The macropores in the

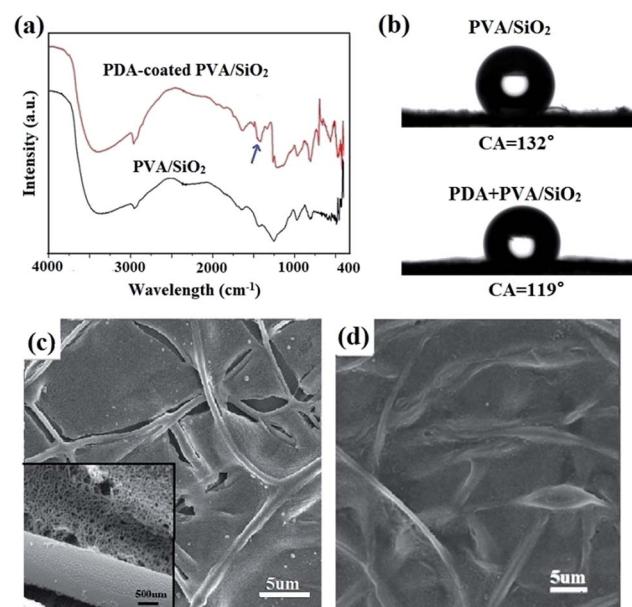


Fig. 4 (a) ATR-FTIR spectra and (b) static contact angle images of as-prepared PVA/SiO₂ fibrous membrane before and after PDA coating; SEM images of (c) PS-*b*-P2VP/electrospun PVA/SiO₂ fibers composite membrane (inset is the SEM image at higher magnification level) and (d) PS-*b*-P2VP/PDA-coated electrospun PVA/SiO₂ fibers composite membrane after swelling in 70 °C ethanol for 6 hours.

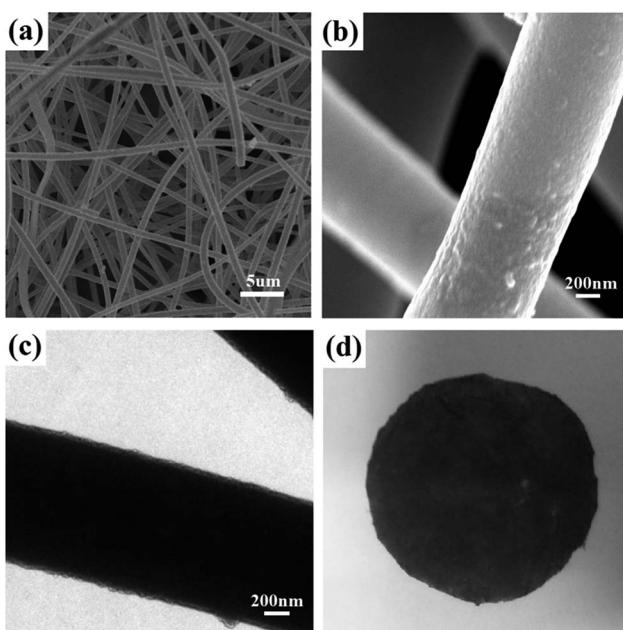


Fig. 3 (a and b) SEM images of the PDA-coated PVA/SiO₂ fibrous membrane at different magnification levels; (c) TEM image of the PDA-coated fibers; (d) optical photo of the PDA-coated PVA/SiO₂ fibrous membrane.

fibrous membrane were filled by the PS-*b*-P2VP filler (Fig. S1a†). The skeleton of the fibrous membrane in the surface was visible, and the fibers were tightly in contact with the PS-*b*-P2VP matrix. However, as shown in Fig. 4c, cracking and separation occurred at the interface of the as-prepared PVA/SiO₂ fibers and coating layer after swelling in ethanol at 70 °C. This phenomenon may be attributed to the absence of the hydrogen bonding between the –OH group on PVA and the pyridine ring in the PS-*b*-P2VP matrix for the crosslinking of the silica precursor and PVA. The very smooth surfaces of the electrospun PVA/SiO₂ fibers also result in the weak physical interaction between the fibers and PS-*b*-P2VP matrix. In this study, the PVA/SiO₂ fibers were modified with a PDA layer to solve this problem and improve the interfacial adhesion.

PDA surface modification was proved to be effective and efficient for improving the interfacial adhesion of fiber-matrix composites in recent years.^{35–37} As illustrated in Fig. 4d, the interfacial nature between the PDA-coated electrospun PVA/SiO₂ fibers and PS-*b*-P2VP matrix was remarkably improved by PDA layer; thus, the PS-*b*-P2VP matrix could maintain contact with PDA-coated fibers even after swelling in hot ethanol of 70 °C. This result could be ascribed to the hydrogen bonding interaction between pyridine groups in PS-*b*-P2VP and benzene hydroxyl groups or amine groups in PDA layer. Moreover, the PVA/SiO₂ fibers are rougher after modified with PDA, which also affected the interfacial adhesion between the fibers and the BCP matrix.

The nanopores in PS-*b*-P2VP were formed by a confined swelling induced pore generation mechanism.^{7,38} By this



mechanism, the P2VP chains are swollen and confined in the continuous phase of the glassy PS component in hot ethanol while a slight and local plastic deformation of the PS matrix is induced. Subsequently, the ethanol is air-dried at room temperature to allow the expanded P2VP domains to shrink and the PS domains to freeze with unrecoverable deformation to produce the pores. The SEM images of the obtained nanoporous membranes swollen in hot ethanol for different times show in Fig. 5. Before swelling, no nanopores were observed (Fig. S1b†). After swelling for 10 min, small cylindrical nanopores with disordered morphology formed. After swelling for 30 min, a morphology intermediate between the disordered cylindrical structure and bicontinuous structure emerged. After 1 hour, the bicontinuous morphology completely developed with uniform nanopores with a diameter of ~ 50 nm. The nanopores slightly coarsened after swelling for a longer time.

The swelling degree of the P2VP chains and the mobility of the PS chains in ethanol depend on temperature and determine the final pore sizes to a certain extent. The influence of swelling temperature on the morphology of the final porous membrane is clearly demonstrated in Fig. 6. At a low temperature, *i.e.*, 20 °C, the swelling degree of the P2VP minor blocks in the PS-*b*-P2VP micelles and the mobility of the glassy nonswollen PS were hardly enhanced, and almost no pores emerged in the membrane. As the temperature increased, the swelling degree of P2VP increased. Small and nonuniform nanopores appeared in the membrane surface at 30 °C and 40 °C (Fig. 6b and c). The pores enlarged and deepened at 50 °C but remained randomly distributed. At 60 °C, a bicontinuous nanostructure with extremely small pore diameter began to form. Fig. 6 suggests that 70 °C is an appropriate swelling temperature for PS-*b*-P2VP to form uniform and continuous nanopores.

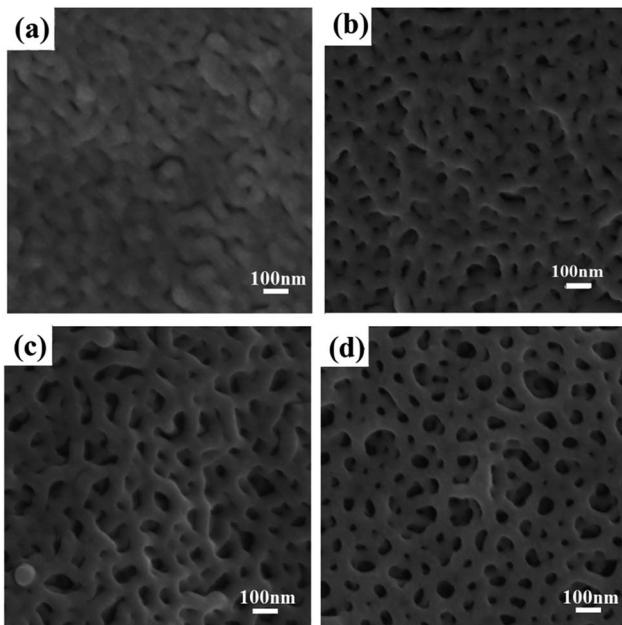


Fig. 5 SEM images of PS-*b*-P2VP membranes swollen with 70 °C ethanol for different time (a) 5 min; (b) 10 min; (c) 30 min; (d) 1 hour.

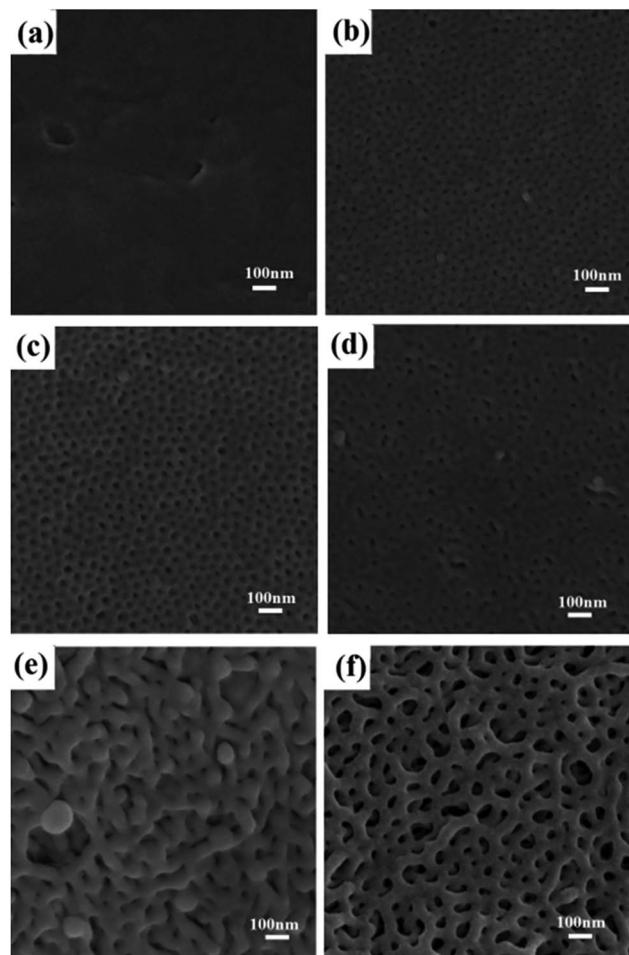


Fig. 6 SEM images of PS-*b*-P2VP membranes swollen with ethanol at different temperature (a) 20 °C; (b) 30 °C; (c) 40 °C; (d) 50 °C; (e) 60 °C; (f) 70 °C.

In the first series of experiments, the composite membranes prepared were drop-coated with 2 wt% PS-*b*-P2VP. We increased the concentration of PS-*b*-P2VP to 3 wt% with the same casting solution volume, a membrane with all the fibers on the surface completely covered by the coating matrix was obtained, with the top surface being very smooth. The magnified top view of the composite membrane is shown in Fig. 7a. Twisted and interconnected cylinders were distributed over the entire surface of the composite membrane, whose nanopores were below 100 nm in size. A cross-sectional view in Fig. 7b shows that the thickness of the composite membrane is 17 ± 2 μm . When the concentration of PS-*b*-P2VP casting solution decreased to 1 wt%, the macropores of the electrospun fibrous membrane could not be covered by the BCP matrix completely. After producing nanopores in the BCP filler, a hierarchical pore structure of macropores and nanopores formed (Fig. 7c and d).

Preparation of asymmetric composite membrane

Although the free-standing symmetric BCP-electrospun fiber composite membrane was obtained, its thickness reached approximately 20 μm . It is well known that flux performance is

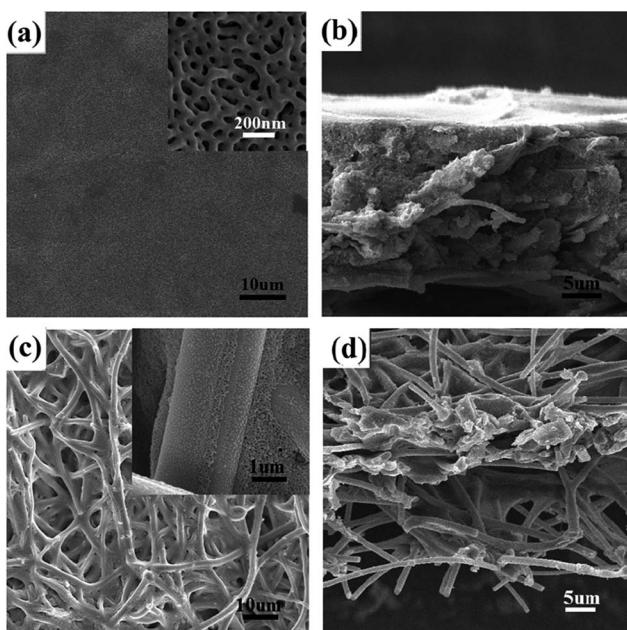


Fig. 7 SEM images of (a) the top view and (b) cross-sectional view of PS-*b*-P2VP/electrospun fibers composite membranes drop-coated with 3 wt% PS-*b*-P2VP; SEM images of (c) the top view and (d) cross-sectional view of PS-*b*-P2VP/electrospun fibers composite membranes drop-coated with 1 wt% PS-*b*-P2VP.

inversely proportional to thickness and costs are directly related to the amount of material used. Therefore, asymmetric membranes containing thin, selective BCP layers on macroporous supports are desirable. Kim *et al.* used commercially available micro-filtration membranes with a broad pore size distribution as mechanical support and a BCP coating film as a selective layer to obtain an asymmetric membrane.^{39,40} However, a sacrificial silicon oxide layer was required in the method, which was time consuming and impractical for large-scale preparation. Hillmyer *et al.* simplified the preparation by casting PS-PLA onto poly(ether sulfone) support directly without using a sacrificial thin film,¹⁷ but the water flow experiments demonstrated that flux was reduced significantly because of the low void fraction of PES and the perpendicular-parallel cylinder orientation deep inside the selective layer.

In the current study, we used a PDA-coated electrospun PVA/SiO₂ fibrous membrane as the macroporous support and a bicontinuous nanoporous membrane self-assembled with PS-*b*-P2VP as a selective layer to prepare an asymmetric membrane. The PDA-modified PVA/SiO₂ fibers were immersed in water before PS-*b*-P2VP/THF solution drop-casting. When the solution was cast onto the surface of the water-wetted electrospun fibrous membrane, the casting solution permeated the water because of the intermiscibility between THF and water. However, the strong volatility of THF prevented the solution from permeating deeply. The SEM images of the top and cross sectional views of the asymmetric composite membrane drop-coated with 2 wt% PS-*b*-P2VP/THF solution are shown in Fig. 8. The macropores in the top surface of the electrospun membrane were uniformly covered by a layer of BCP

nanoporous membrane, which was swollen in ethanol at 70 °C for 6 hours (Fig. 8a and c). Fig. 8b and d show that the thickness of the membrane was approximately 5 μm, which was significantly reduced compared with that of the symmetric composite membrane. The fibers in the surface layer were encased by the BCP matrix; as a result, the adhesion between the electrospun fibers and separation layer increased. The thickness of the BCP layer was adjusted by changing the concentration of BCP solution. As demonstrated in Fig. S2a–c,† the thickness of the separation layer increased with increasing concentration and was 7, 4, and 2 μm respectively achieved with 3 wt%, 2 wt%, and 1 wt% BCP/THF solution. However, the BCP layer with the thickness of 2 μm was torn by tensile force upon swelling in hot ethanol due to its thinness (Fig. S2d†). A thickness of 4 μm was sufficient to maintain the integrity of the separation layer and increased to ~5 μm after swelling in hot ethanol (Fig. 8).

Ultrafiltration performance evaluation

The 17 ± 2 μm-thick symmetric BCP–electrospun fiber composite membrane with a specific area of 12.08 m² g⁻¹ and an average pore diameter of 38 nm (Fig. 9a) was used for the evaluation of ultrafiltration performance. The result was compared with that of the as-prepared electrospun PVA/SiO₂ fibrous membrane with the same thickness. Fig. 9b and c show the SEM images of the top view of the composite nanoporous membrane and as-prepared electrospun fibers mat after the filtration of the Au NP dispersion. The composite membrane surface was covered with a layer of Au NPs. By contrast, the Au NPs were hardly rejected by the as-prepared electrospun fibrous membrane because of the large pore size. Only a small amount of Au NPs were absorbed on the surfaces of the fibers by the chelation effect due to the -OH

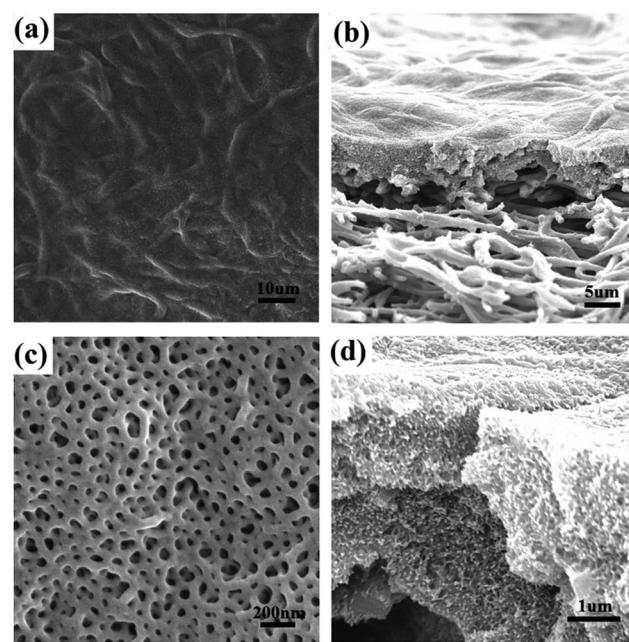


Fig. 8 SEM images of (a and c) the top view and (b and d) cross-sectional view of asymmetric membrane swelling with ethanol at 70 °C for 6 hours.

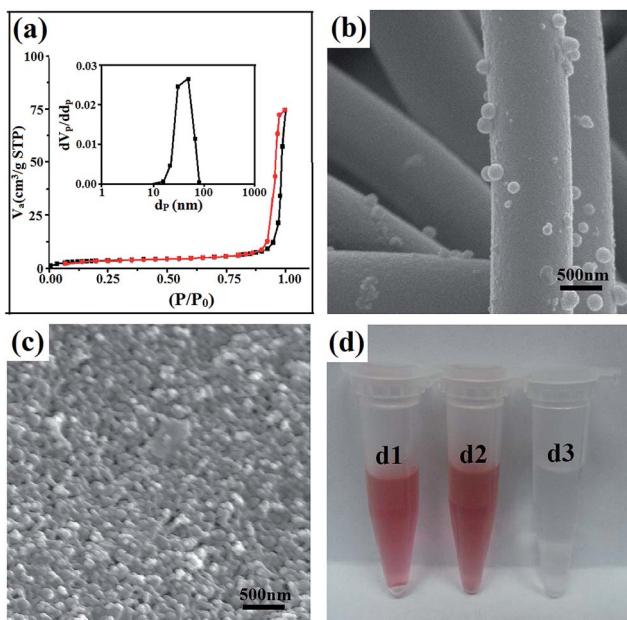


Fig. 9 (a) Nitrogen adsorption isotherm of the PDA-coated PVA/SiO₂ and PS-*b*-P2VP composite membrane swollen in 70 °C for 6 hours, the inset shows the pore size distribution. SEM of (b) the as-prepared electrospun fibers membrane and (c) the composite membrane after filtration of golden nanoparticles; (d) the digital photograph of the golden nanoparticle suspension (d1) before filtration, (d2) after filtration by the as-prepared electrospun fibers membrane, and (d3) after filtration by the composite membrane.

groups on the electrospun fibers. Fig. 9d shows the digital photographs of the Au NP dispersion before and after filtration. The color of the red Au dispersion nearly did not change after filtration with the as-prepared electrospun fibrous membrane, but the color disappeared after filtration with the nanoporous composite membrane. This result is consistent with the rejection phenomenon shown in the SEM images.

Conclusion

Symmetric and asymmetric membranes each composed of an electrospun PVA/SiO₂ fibrous membrane and a PS-*b*-P2VP BCP matrix were fabricated by combining electrospinning and BCP phase separation. The interfacial interaction between the PVA/SiO₂ electrospun fibers and PS-*b*-P2VP matrix was strengthened by the modification of PVA/SiO₂ fibers with PDA coating. The results suggest that the PDA-coated electrospun fiber mat can be tightly covered by the PS-*b*-P2VP precursor when the concentration of PS-*b*-P2VP is 3 wt%. Furthermore, the nanopores of the composite membranes can be produced by the selective swelling of P2VP cylinders surrounded by PS matrix in the membranes. The influences of the swelling temperature and swelling time on the pore size and pore structure were also comprehensively discussed. The results indicate that the pore size and pore structure are tunable by adjusting the swelling conditions. For the asymmetric membrane, the thickness of the separation layer is tunable by varying the PS-*b*-P2VP

solution concentration. A 5 μm-thick asymmetric nanoporous membrane was successfully obtained by our strategy. The result of the ultrafiltration performance evaluation indicates that the composite membrane can be used for the efficient separation of NPs, which informs that this hierarchical porous composite membrane is a promising candidate for industrial and environmental applications.

Conflicts of interest

There are no conflicts to declare.

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Notes and references

- 1 A. Greiner and J. H. Wendorff, *Angew. Chem.*, 2007, **46**, 5670–5703.
- 2 R. Sahay, P. S. Kumar, R. Sridhar, J. Sundaramurthy, J. Venugopal, S. G. Mhaisalkar and S. Ramakrishna, *J. Mater. Chem.*, 2012, **22**, 12953–12971.
- 3 S. Mohammadzadehmoghadam, Y. Dong and I. Jeffery Davies, *J. Polym. Sci., Part B: Polym. Phys.*, 2015, **53**, 1171–1212.
- 4 S. S. Homaeigohar, K. Buhr and K. Ebert, *J. Membr. Sci.*, 2010, **365**, 68–77.
- 5 P. van Rijn, M. Tütür, C. Kathrein, L. Zhu, M. Wessling, U. Schwaneberg and A. Boeker, *Chem. Soc. Rev.*, 2013, **42**, 6578–6592.
- 6 H. Ahn, S. Park, S.-W. Kim, P. J. Yoo, D. Y. Ryu and T. P. Russell, *ACS Nano*, 2014, **8**, 11745–11752.
- 7 Y. Wang, *Acc. Chem. Res.*, 2016, **49**, 1401–1408.
- 8 J. I. Clodt, V. Filiz, S. Rangou, K. Buhr, C. Abetz, D. Höche, J. Hahn, A. Jung and V. Abetz, *Adv. Funct. Mater.*, 2013, **23**, 731–738.
- 9 Z. Yi, P.-B. Zhang, C.-J. Liu and L.-P. Zhu, *Macromolecules*, 2016, **49**, 3343–3351.
- 10 H. Uehara, M. Kakiage, M. Sekiya, D. Sakuma, T. Yamonobe, N. Takano, A. Barraud, E. Meurville and P. Ryser, *ACS Nano*, 2009, **3**, 924–932.
- 11 M. Karunakaran, R. Shevate and K.-V. Peinemann, *RSC Adv.*, 2016, **6**, 29064–29071.
- 12 S. P. Nunes, *Macromolecules*, 2016, **49**, 2905–2916.
- 13 F. Schacher, M. Ulbricht and A. H. Müller, *Adv. Funct. Mater.*, 2009, **19**, 1040–1045.



14 Y. Xie, N. Moreno, V. M. Calo, H. Cheng, P.-Y. Hong, R. Sougrat, A. R. Behzad, R. Tayouo and S. P. Nunes, *Polym. Chem.*, 2016, **7**, 3076–3089.

15 M. Seo, D. Moll, C. Silvis, A. Roy, S. Querelle and M. A. Hillmyer, *Ind. Eng. Chem. Res.*, 2014, **53**, 18575–18579.

16 S. Schoettner, H.-J. Schaffrath and M. Gallei, *Macromolecules*, 2016, **49**, 7286–7295.

17 W. A. Phillip, B. O'Neill, M. Rodwgin, M. A. Hillmyer and E. L. Cussler, *ACS Appl. Mater. Interfaces*, 2010, **2**, 847–853.

18 X. Yao, L. Guo, X. Chen, J. Huang, M. Steinhart and Y. Wang, *ACS Appl. Mater. Interfaces*, 2015, **7**, 6974–6981.

19 X. Li, C.-A. Fustin, N. Lefèvre, J.-F. Gohy, S. De Feyter, J. De Baerdemaeker, W. Egger and I. F. Vankelecom, *J. Mater. Chem.*, 2010, **20**, 4333–4339.

20 W. Sun, Z. Wang, X. Yao, L. Guo, X. Chen and Y. Wang, *J. Membr. Sci.*, 2014, **466**, 229–237.

21 H. Zhou, Y. Su, X. Chen, J. Luo, S. Tan and Y. Wan, *J. Membr. Sci.*, 2016, **520**, 779–789.

22 H. Li, L. Tuo, K. Yang, H.-K. Jeong, Y. Dai, G. He and W. Zhao, *J. Membr. Sci.*, 2016, **511**, 130–142.

23 L. Jin, M. Zhang, H. Li, M. Li, L. Shang, L. Xiao and Y. Ao, *RSC Adv.*, 2016, **6**, 80485–80492.

24 A. Abdolmaleki, S. Mallakpour and S. Borandeh, *Polym. Compos.*, 2016, **37**, 1924–1935.

25 L. Wang, Y. Shi, R. Sa, N. Ning, W. Wang, M. Tian and L. Zhang, *Ind. Eng. Chem. Res.*, 2016, **55**, 12547–12556.

26 H. Lee, S. M. Dellatore, W. M. Miller and P. B. Messersmith, *Science*, 2007, **318**, 426–430.

27 M. Hu and B. Mi, *Environ. Sci. Technol.*, 2013, **47**, 3715–3723.

28 J. Zhao, C. Fang, Y. Zhu, G. He, F. Pan, Z. Jiang, P. Zhang, X. Cao and B. Wang, *J. Mater. Chem. A*, 2015, **3**, 19980–19988.

29 Y. Li, Y. Su, J. Li, X. Zhao, R. Zhang, X. Fan, J. Zhu, Y. Ma, Y. Liu and Z. Jiang, *J. Membr. Sci.*, 2015, **476**, 10–19.

30 H. Lee, J. Rho and P. B. Messersmith, *Adv. Mater.*, 2009, **21**, 431–434.

31 C. Shao, H. Y. Kim, J. Gong, B. Ding, D. R. Lee and S. J. Park, *Mater. Lett.*, 2003, **57**, 1579–1584.

32 M. Krissanasaeranee, T. Vongsetskul, R. Rangkupan, P. Supaphol and S. Wongkasemjit, *J. Am. Ceram. Soc.*, 2008, **91**, 2830–2835.

33 T. Pirzada, S. A. Arvidson, C. D. Saquing, S. S. Shah and S. A. Khan, *Langmuir*, 2012, **28**, 5834–5844.

34 H. Yang, Y. Lan, W. Zhu, W. Li, D. Xu, J. Cui, D. Shen and G. Li, *J. Mater. Chem.*, 2012, **22**, 16994–17001.

35 W. Lee, J. U. Lee and J. H. Byun, *Compos. Sci. Tech.*, 2015, **110**, 53–61.

36 M. Yi, H. Sun, H. Zhang, X. Deng, Q. Cai and X. Yang, *Mater. Sci. Eng., C*, 2016, **58**, 742–749.

37 Y. Li, Q. Chen, M. Yi, X. Zhou, X. Wang, Q. Cai and X. Yang, *Appl. Surf. Sci.*, 2013, **274**, 248–254.

38 Y. Wang and F. Li, *Adv. Mater.*, 2011, **23**, 2134–2148.

39 S. Y. Yang, I. Ryu, H. Y. Kim, J. K. Kim, S. K. Jang and T. P. Russell, *Adv. Mater.*, 2006, **18**, 709–712.

40 S. Y. Yang, J. Park, J. Yoon, M. Ree, S. K. Jang and J. K. Kim, *Adv. Funct. Mater.*, 2008, **18**, 1371–1377.

