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Synergistic catalysis of nano-Pd and nano rare-earth oxide/AC: complex nanostructured catalysts fabricated by a photochemical route for selective hydrogenation of phenol[†]

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Cyclohexanone is an important industrial intermediate in the manufacture of polyamides in the chemical industry, but direct selective hydrogenation of phenol to cyclohexanone under mild conditions to achieve both high conversion and selectivity is a challenge. Here we report novel complex nanostructured catalysts Pd@-CeO₂/AC and Pd@-La₂O₃/AC prepared by a photochemical route. These catalysts were characterized by XRD, BET, TEM, H₂-TPR and XPS. The results showed that Pd nanoparticles were well-dispersed on CeO₂/AC or La₂O₃/AC, and the complex nanostructured catalysts exhibit a synergistic effect between nano-Pd and nano-La₂O₃/AC or nano-CeO₂/AC. These catalysts had an excellent catalytic performance for the hydrogenation of phenol, achieved 100% conversion and a selectivity higher than 96% within 3 h at 70 °C and 0.7 MPa H₂ pressure. The results indicated that the remarkable performance may result from the synergistic effect between active component Pd and rare-earth oxide, their complex nanostructured properties and the high dispersion of Pd particles on the large surface area. Furthermore, this work revealed synergistic catalysis of nano-metal Pd and nano rare-earth oxide and opened a new direction of synergistic catalysis of nanostructured catalysts.

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1. Introduction

Cyclohexanone is an important intermediate in the production of caprolactam, which is used in the manufacture of nylon 6 and nylon 66.¹ In general, cyclohexanone can be obtained from cyclohexane oxidation or phenol hydrogenation.² The former route requires high temperatures and high pressures and generates a large number of byproducts, but low conversion and high energy consumption.³ Therefore, selective hydrogenation of phenol to cyclohexanone is an important chemical process that has been extensively studied to date.^{4,5} In the hydrogenation of phenol, cyclohexanone is generally obtained through a one-step or a two-step process. In the two-step procedure, phenol is first hydrogenated to cyclohexanol and then cyclohexanol is dehydrogenated to cyclohexanone at high temperature.⁶ In one-step, the selective hydrogenation of phenol directly into cyclohexanone,⁷ however, cyclohexanone can be further hydrogenated to cyclohexanol easily, so it is extremely necessary to prepare high selectivity and conversion catalysts. In recent years, supported Pd-based catalysts have been widely used for the selective hydrogenation of phenol to cyclohexanone,⁸ such

as Pd/C,⁹ Pd/MCM-41,¹⁰ Pd-Al₂O₃,¹¹ Pd/ZrO₂,¹² Pd/Ce-AlO_x (ref. 13) and so on. All of those catalysts indicated that Pd is an excellent metal catalyst for phenol hydrogenation. However, to achieving both excellent conversion ($\geq 80\%$) and high selectivity ($\geq 90\%$) under mild conditions is still a challenging problem.¹⁴

Notably, Han Buxing and his co-worker¹⁵ reported that a complete phenol conversion with >99.9% selectivity to cyclohexanone could be achieved on a dual-supported Pd-Lewis acid catalyst in sc-CO₂, while the conditions is so sophisticated (supercritical carbon dioxide as solvent, which requires high H₂ and CO₂ pressures >7.0 MPa). Most recently, Wang Yong and co-workers designed a kind of carbon nitride material as support to prepare Pd-based catalysts,¹⁶ which achieved both excellent conversion and selectivity in the hydrogenation of phenol in aqueous media. Nevertheless, the preparation of the mpg-C₃N₄ and/or CN-x was complicated and involved the use of NH₄HF₂ or HF which are hazardous. Zhaoyin Hou¹⁷ prepared a Amberlyst-45 palladium catalyst (Pd/A-45), achieved 89% cyclohexanone selectivity and 100% phenol conversion at 100 °C and 1 MPa H₂ pressure in water. They think the good performance of Pd/A-45 can be attributed to its strong acidity enhance the desorption of phenoxy species. On the other hand, Chen and co-workers¹⁸⁻²¹ utilized polymer-functionalized CNF, hydroxyapatite-bound and/or ionic liquid-like copolymer to stabilize Pd, and the as-prepared catalysts have been proven to be efficient for phenol hydrogenation. However, the preparation of these

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catalysts required many expensive polymers and had the disadvantage of high preparation cost. In conclusion, although a few catalysts show a decent activity under an appropriate conditions, either the harsh reaction conditions, the low cyclohexanone selectivity (<90%) or the complicated method to prepare catalysts. Therefore, it is necessary to use a facile method to prepare catalyst for high efficient selective hydrogenation of phenol.

Recently, rare earth oxide has been great interest in the use of catalytic reaction due to its unique characteristics. Especially, the CeO_2 and La_2O_3 are the most widely used.^{22,23} CeO_2 has a good performance of stockpile and release oxygen, it can not only enhance the catalytic activity but also improve thermostability.^{24,25} La_2O_3 has a lot of attractive properties for applications such as catalysts, high k gate dielectric material and optical filters.²⁶ Even so, they are low activity for used as catalyst directly. But when they combined with noble metal, it could influence the catalytic performance. Salvatore Scire²⁷ studied the gas-phase phenol hydrogenation reaction over Pd/CeO_2 (40% conversion, 92% selectivity) and $\text{Pd}/\text{La}_2\text{O}_3$ (35% conversion, 95% selectivity) at 160 °C. The groups of Inagaki²⁸ studied the reaction in the vapor phase over Pd/CeO_2 at 180 °C (80% conversion, 50% selectivity). However, the impact of the interaction between the metal oxide and noble metal on the catalytic performance of these catalysts has not been discussed. In addition, these catalysts has not achieve both excellent conversion and high selectivity simultaneously.

The utilization efficiency of noble metals (Pt, Au, Pd) in conventional supported catalysts is far less than satisfactory. Recently, research has been reported that the metal with higher dispersity, many of the metal atoms are present at a surface, available for catalysis and offer the efficiency. Flytzani-Stephanopoulos *et al.*^{29–31} showed that atomically dispersed Au or Pt cations exhibited excellent catalytic activity for water–gas shift reaction, while Au or Pt particles had no chemical action. Another solution of the significantly reducing the use of precious metal, preparation of support single-atom catalysts (SAC), was proposed by Zheng and coworkers.^{32–34} We proposed a novel strategy to utilize noble metal efficiently, and prepared a novel complex nanostructured catalyst $\text{Au}/\text{TiO}_2/\text{MCM-41}$ and $\text{Au}/\text{TiO}_2/\text{MCM-22}$ by photochemical route, these catalysts exhibited excellent activity and chemical stability for cyclohexane oxidation.^{35–37} Herein, we used a novel strategy to prepare a complex nanostructured catalyst, which combined nano-metals with nano-semiconductor to fabricate a novel nano-Pd complex nanostructured catalyst $\text{Pd}/\text{@-Me}_x\text{O}_y/\text{AC}$ (Me_xO_y : CeO_2 or La_2O_3) by photochemical route. These complex catalysts were characterized by XRD, BET, TEM and XPS, and employed in the selective hydrogenation of phenol to cyclohexanone at low temperature and H_2 pressure in the liquid phase. These catalysts exhibited a higher activity and selectivity to cyclohexanone, the remarkable catalytic performance could be ascribed to the synergistic effect between Pd nanoparticles and nano-semiconductor (CeO_2 or La_2O_3), their complex nano-structured properties and the large contact surface.

2. Experimental

2.1 Catalyst preparation

Pretreatment of activated carbon with acid. A commercial activated carbon (AC) made from coconut shells (Fujian Xinsen Carbon Co. Ltd.) was pretreated with HNO_3 (10%) under refluxing at 60 °C for 2 h. Then the AC were cooled to room temperature, washed to neutrality with distilled water. Finally, the AC were dried at 120 °C.

Preparation of composite support CeO_2/AC . The synthesis of CeO_2/AC was adapted from the method of El-Shall.³⁸ $\text{Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ (1.46 g) dissolved in ethanol (120 mL), while stirring, add the pre-processed AC (5 g) in it, 1 mol L^{-1} NaOH was added dropwise until the pH of the resulting solution was 10, put the solution in the microwave with the power was set 214 W for 10 min (on for 10 s, off for 20 s). After cooled down to room temperature, washed with distilled water and ethanol then left to dry at 120 °C for 12 h. The preparation of CeO_2 was same as above, just not add the AC.

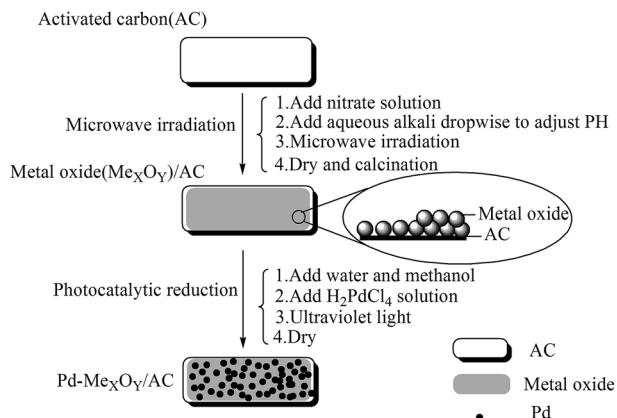
Preparation of composite support $\text{La}_2\text{O}_3/\text{AC}$. In a typical synthesis, $\text{La}(\text{NO}_3)_3 \cdot n\text{H}_2\text{O}$ (0.554 g) dissolved in distilled water (120 mL), while stirring, add the pre-processed AC (5 g) in it, 0.5 mol L^{-1} NH_4HCO_3 was added dropwise until the pH of the resulting solution was 7.0, put the solution in the microwave with the power was set 400 W for 16 min (on for 30 s, off for 30 s). After filtrating, washing and dry at 70 °C for 4 h, finally achieved composite support $\text{La}_2\text{O}_3/\text{AC}$ after calcined at 550 °C for 2 h. The preparation of La_2O_3 was same as above, just not add the AC.

The obtained CeO_2/AC and $\text{La}_2\text{O}_3/\text{AC}$ composites were denoted as $x\text{CeO}_2/\text{AC}$ and $x\text{La}_2\text{O}_3/\text{AC}$, where x represents the CeO_2/AC and $\text{La}_2\text{O}_3/\text{AC}$ loading by weight.

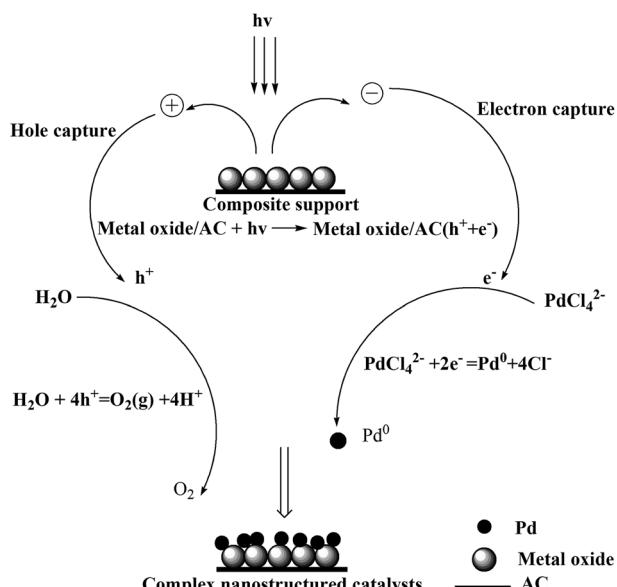
Synthesis of $\text{Pd}/\text{@-Me}_x\text{O}_y/\text{AC}$. All Pd catalysts were prepared by photochemical route with a 1–3 wt% Pd loading relative to the mass of the support. Take an example of $\text{Pd}/\text{@-CeO}_2/\text{AC}$: as-prepared CeO_2/AC (0.582 g) was added in distilled water (100 mL) and methanol (5 mL) mix solution, add the H_2PdCl_4 (1.5 mL, 0.012 g mL^{-1}) in it, ultrasonic dispersion for 30 minutes, then ultraviolet lamp for 10 h. Finally, the sample was separated by filtration, washed several times by distilled water up to pH = 7, dried in a vacuum oven at 80 °C for 10 h. The preparation of $\text{Pd}/\text{@-La}_2\text{O}_3/\text{AC}$, Pd/AC , Pd/CeO_2 and $\text{Pd}/\text{La}_2\text{O}_3$ were same as above, the only difference was to CeO_2/AC with different supports. The procedures for preparing the $\text{Pd}/\text{@-CeO}_2/\text{AC}$ or $\text{Pd}/\text{@-La}_2\text{O}_3/\text{AC}$ catalysts are graphically illustrated in Scheme 1.

Our previous work involving photocatalytic reduction of noble Au,^{35–37} the preparation process and condition was simple and mild, and the noble nanoparticles was uniform dispersed, this method is also applicable to reduction Pd. Photochemical deposition of Pd films or small particles on oxide substrates such as TiO_2 ,^{39,40} or graphene sheets/ ZnO .⁴¹ Similarly, CeO_2 is also an interesting material due to its unique redox properties as well as strong UV absorption at ~ 400 nm.⁴² La_2O_3 is also a rare earth metal oxide and has similar chemical properties to CeO_2 . It is well known that a semiconductor can be excited and then generate electrons (e^-) and holes (h^+) in the conduction





Scheme 1 Preparation of the Pd/@-CeO₂/AC and Pd/@-La₂O₃/AC catalysts.



Scheme 2 Reaction mechanism of photocatalytic reduction method.

band (CB) and valence band (VB) if the energy of the photons of the incident light is larger than that of the band gap of the semiconductor.³⁹ The reaction mechanism of photochemical route is in Scheme 2. When composite support (CeO₂/AC or La₂O₃/AC) absorbed ultraviolet, metal oxide semiconductor can be excited and then generate electrons (e⁻) and holes (h⁺), forming electron–hole pairs. In the presence of methanol, the holes were scavenged, thus leaving the electrons to accumulate on the surface of the metal oxide semiconductor, the stored electrons were then transferred to the metal ions Pd²⁺ and reduced Pd²⁺ to form Pd on the surface of composite support.

2.2 Catalyst characterization

X-ray diffraction (XRD) of samples was obtained on a Rigaku D/max-II/2500 X-ray powder diffractometer, Cu K α radiation was employed and the working voltage and current were 40 kV and 30 mA, respectively. Transmission electron microscope (TEM)

images were obtained with a JEOL JEM-2100F at an acceleration voltage of 200 kV. X-ray photoelectron spectroscopy (XPS) was performed using ESCALAB 250Xi (Thermo) with Al K α radiation. Inductively coupled plasma-atomic emission spectrometry (ICP-AES) data were obtained using an Intrepid XSP (IRIS). The specific surface areas of the samples were calculated by the BET method by N₂ adsorption–desorption with a NOVA-2200e volumetric desorption analyzer. Temperature-programmed reduction by hydrogen (H₂-TPR) was carried out on Chem Bet 3000 analyzer. All samples (0.1 g) were pretreated in the flow of Ar at 250 °C for 1 hour.

2.3 Catalytic tests

The typical procedure for hydrogenation of phenol was as follows: 0.1 g phenol, 0.353 g catalyst (0.75 mol% Pd relative to phenol), and 20 mL solvent were placed in a autoclave. The autoclave was purged with H₂ to remove the air 3 times. Then the reaction was stirred at 800 rpm under 0.7 MPa H₂ pressure until the temperature reached 70 °C. After the end of the reaction, the autoclave was cooled to room temperature, then the products were analyzed using an Agilent 6890N GC (Fig. S1†) with an HP-5 (30 m × 0.32 mm × 0.25 μ m) capillary column and FID detector. The temperature of gasify room and detector were 250 °C and 280 °C respectively. The air at a constant flow of 400 mL min⁻¹, the mixed gas H₂ and N₂ flow of 30 mL min⁻¹. The initial column temperature was fixed at 50 °C for 7 min and then increased to 180 °C at a rate of 60 °C min⁻¹. The final temperature was maintained for 2 min.

3 Results and discussion

3.1 Characterization

The XRD patterns of AC, CeO₂/AC, La₂O₃/AC, Pd/@-CeO₂/AC and Pd/@-La₂O₃/AC catalysts were shown in Fig. 1. All samples present broadened peaks at about 2 θ = 25° and 42°, which could be attributed to the AC support. Due to the high dispersion and low loading of CeO₂ on the AC, just a very weak peaks at 2 θ = 56.1°. The diffraction peak at 2 θ = 31.3° was attributed to La₂O₃. Four characteristic diffraction peaks of Pd were

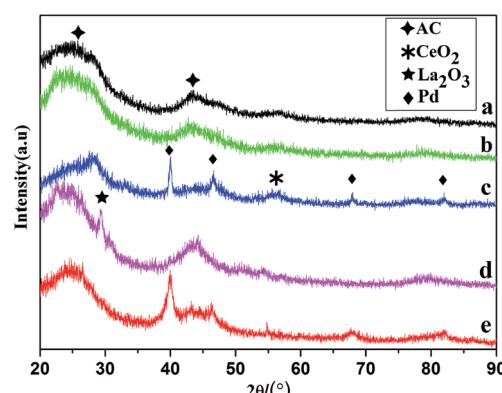


Fig. 1 XRD patterns of samples: (a) AC (b) 10% CeO₂/AC, (c) 3% Pd/@-10% CeO₂/AC, (d) 10% La₂O₃/AC (e) 3% Pd/@-10% La₂O₃/AC.

detected at $2\theta = 40.2^\circ$, 46.6° , 68.2° and 82.2° , which were attributed to the (111), (200), (220) and (311) crystalline planes. Comparison with $\text{La}_2\text{O}_3/\text{AC}$, the peaks attributed to La_2O_3 in XRD patterns of $\text{Pd}/@\text{La}_2\text{O}_3/\text{AC}$ became very weak or disappeared, which result from the uniform mixture of AC with La_2O_3 , because the strong mechanical and chemical effects of an ultrasound wave and ultraviolet lamp dispersed the precipitates immediately.

TEM and HRTEM images of 3% Pd/@-10% CeO_2/AC and 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ were recorded and shown in Fig. 2. For 3% Pd/@-10% CeO_2/AC (Fig. 2a), the Pd nanoparticles are evident as larger dark spots, while the CeO_2 substrate is smaller, it was very clear that the Pd particles were dispersed mainly on the composite support. Particles are distribution analysis in Fig. 2b, which reveals that the particles are in the range of 5–30 nm with 13 nm as an average diameter. The result was consistent with the average particle size 13.77 nm that obtained from XRD by the Scherrer equation. Fig. 2c represents the HRTEM image of 3% Pd/@-10% CeO_2/AC , the lattice fringe with a *d*-spacing of 0.312 nm corresponds to the (111) plane of CeO_2 , and the distance of 0.223 nm (measured crystal DigitalMicrograph) corresponds to the (111) plane of Pd. Fig. 2d show the EDX data of 3% Pd/@-10% CeO_2/AC , the data indicate the presence of elemental constituents within the as-synthesized samples. For 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ (Fig. 2e), the situation is different, the Pd nanoparticles was more smaller than 3% Pd/@-10% CeO_2/AC , which resulted from the interaction between Pd and La_2O_3 , because the Pd nanoparticles could be smaller when the sample contains La_2O_3 .⁴³ The image revealed highly dispersed Pd with a mean size of 5.5 nm (Fig. 2f). Fig. 2g represents the HRTEM image of 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$, the lattice fringe with a *d*-spacing of 0.297 nm corresponds to the (111) plane of La_2O_3 , and the distance of 0.225 nm corresponds to the (111) plane of Pd. In Fig. 2h, we can also observe that the presence of elemental constituents within the as-synthesized samples.

The relevant physicochemical parameters of the AC, 10% CeO_2/AC , 10% $\text{La}_2\text{O}_3/\text{AC}$, 3% Pd/@-10% CeO_2/AC and 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ were summarized in Table 1. The AC had a high specific surface area of $1418.6 \text{ m}^2 \text{ g}^{-1}$, however, the specific surface area decreased to $1309.2 \text{ m}^2 \text{ g}^{-1}$ and $1349.7 \text{ m}^2 \text{ g}^{-1}$ after doping CeO_2 and La_2O_3 , respectively. The surface area decreased gradually with further loading of Pd. Thus, the catalysts 3% Pd/@-10% CeO_2/AC and 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ exhibit the surface area of $1138.1 \text{ m}^2 \text{ g}^{-1}$ and $1349.7 \text{ m}^2 \text{ g}^{-1}$, respectively. This indicated that the loading of metal oxide and Pd within the pores, which is consistent with the reports.⁴⁴

XPS was performed on the 3% Pd/@-10% CeO_2/AC and 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ catalysts and the results were shown in Fig. 3. From Fig. 3a, Pd, Ce, C, O and Pd, La, C, O were detected in two samples, respectively. Indicated the presence of CeO_2 and La_2O_3 in $\text{Pd}/@\text{CeO}_2/\text{AC}$ and $\text{Pd}/@\text{La}_2\text{O}_3/\text{AC}$, respectively. And Pd species was loaded on the composite support by photochemical route. In Fig. 3b, the Pd 3d XPS spectra of the two catalysts show four asymmetric broad peaks. Peaks detected at around 335.9 eV and 341.1 eV can be readily assigned to the Pd 3d_{5/2} and Pd 3d_{3/2} electronic states of Pd(0),⁴⁵ respectively. Compared with standard values (335 eV and 340.3 eV), the measured values are higher than their standard values, the electron move from Pd to CeO_2 , the dissociatively chemisorbed hydrogen on Pd may diffuse from Pd surface to CeO_2 and reduce Ce^{4+} to Ce^{3+} . That means the strong metal-support interaction between nano-Pd and nano- CeO_2/AC . Peaks at 337.1 eV and 342.6 eV correspond to the Pd 3d_{5/2} and Pd 3d_{3/2} electronic states of Pd(2+)⁴⁶ species, respectively. The presence of Pd(2+) species was probably due to the interaction of Pd and surface adsorbed oxygen, which is beneficial for the enhancement of adherence of Pd on the support.⁴⁶ The Ce 3d XPS spectrum (Fig. 3c) consists of a spin orbit split doublet, the peaks located at 883.0 eV, 887.2 eV and 898.8 eV represent the Ce 3d_{5/2} and the peaks located at 901.6 eV, 907.2 eV and 917.1 eV represent the

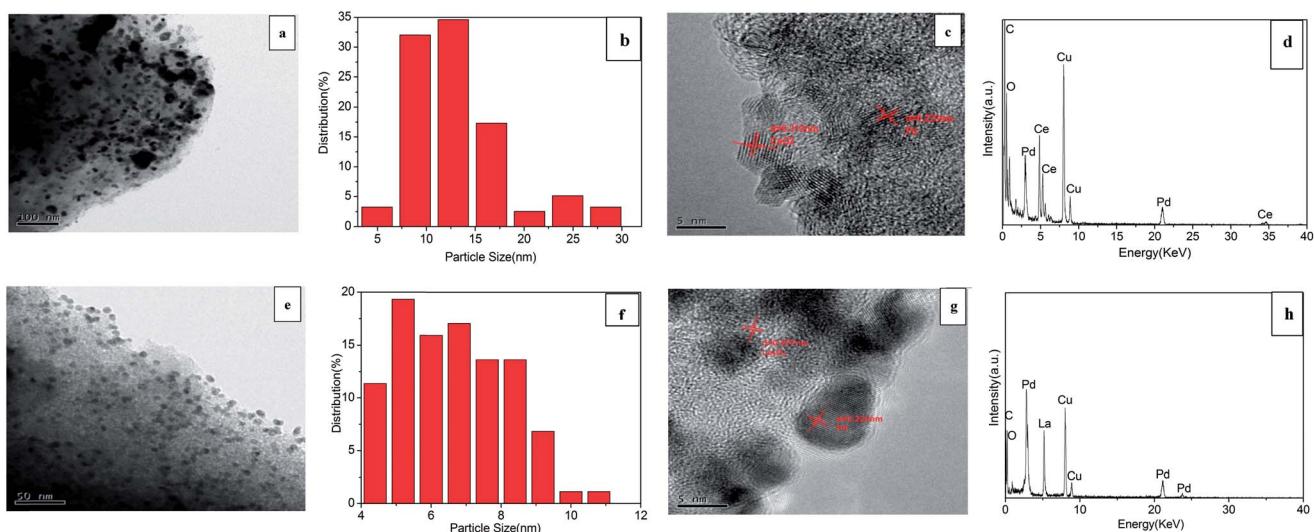


Fig. 2 (a) TEM image of 3% Pd/@-10% CeO_2/AC , (b) size distribution of Pd on 3% Pd/@-10% CeO_2/AC , (c) HRTEM image of 3% Pd/@-10% CeO_2/AC , (d) EDX spectrum of 3% Pd/@-10% CeO_2/AC , (e) TEM image of 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$, (f) size distribution of Pd on 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$, (g) HRTEM image of 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$, (h) EDX spectrum of 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$.

Table 1 Relevant physicochemical parameters of supports and Pd catalysts

Entry	Catalysts	Surface area ^a (m ² g ⁻¹)	Pd loading (wt%)		
			Theoretical	Experimental ^b	Pd particle size ^c (nm)
1	AC	1418.6	—	—	—
2	10% CeO ₂ /AC	1309.2	—	—	—
3	3% Pd/@-10% CeO ₂ /AC	1138.1	3	2.985	5–30
4	10% La ₂ O ₃ /AC	1410.4	—	—	—
5	3% Pd/@-10% La ₂ O ₃ /AC	1349.7	3	2.977	4–12

^a BET surface area. ^b Determined by ICP. ^c Observed from TEM images.

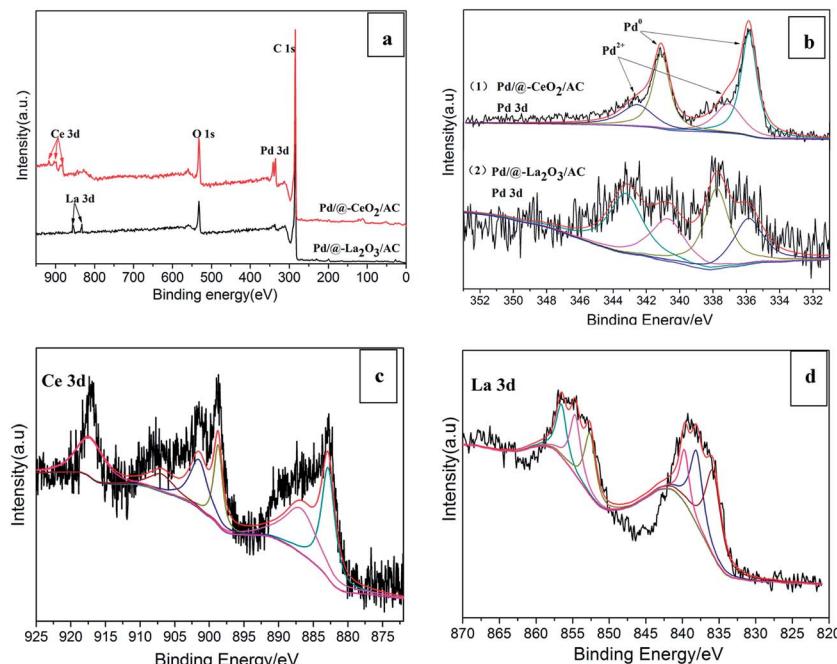


Fig. 3 (a) XPS scans survey for 3% Pd/@-10% CeO₂/AC and 3% Pd/@-10% La₂O₃/AC, (b) Pd 3d XPS spectra of 3% Pd/@-10% CeO₂/AC and 3% Pd/@-10% La₂O₃/AC, (c) Ce 3d XPS spectra, (d) La 3d XPS spectra.

Ce 3d_{3/2} peaks. The peaks at 883.0 eV, 898.8 eV, 907.2 eV and 917.1 eV could be attributed to Ce⁴⁺ oxidation states while the peaks at 887.2 eV and 901.6 eV emanate from Ce³⁺ oxidation states of cerium.^{47,48} Hence, from the XPS spectrum it was confirmed that the sample contains mixed oxidation states (Ce⁴⁺ and Ce³⁺). The La 3d XPS spectrum was shown in Fig. 3d, the peaks located at 835.8 eV, 838.2 eV and 839.8 eV represent the La 3d_{5/2} and the peaks located at 852.6 eV, 854.6 eV and 856.5 eV represent the La 3d_{3/2} peaks. And the peaks at 835.8 eV and 838.2 eV could be attributed to La³⁺.⁴⁹

3.2 Hydrogenation of phenol

The Pd complex nanostructured catalysts Pd/@-CeO₂/AC and Pd/@-La₂O₃/AC were first applied to selective hydrogenation of phenol. For comparison, the CeO₂/AC, La₂O₃/AC, Pd/AC, Pd/La₂O₃ and Pd/CeO₂ were also used as reference catalysts, the results are shown in Table 2. As we can see, only metal oxide supported on AC samples CeO₂/AC or La₂O₃/AC have no

catalytic activity (Table 2, entry 5 and 6). Obviously, the Pd played a major role in reaction. Whereas these reference catalysts 3% Pd/CeO₂ (Table 2, entry 3) and 3% Pd/La₂O₃ (Table 2, entry 4) almost no catalytic activity, with a phenol conversion of less than 10%, the selectivity of cyclohexanone were over than 99%. The 3% Pd/AC (Table 2, entry 1) catalyst have a better catalytic activity for selective hydrogenation of phenol, conversion of phenol could achieve to 76.6%. Wang Yong *et al.*⁴⁹ have reported that hydrogenation of phenol to cyclohexanone can achieve 2% phenol conversion and 100% cyclohexanone selectivity at 65 °C and 6 h in water with commercial Pd@CeO₂ catalyst. Chen Jinzhu *et al.*¹⁸ achieve 55% phenol conversion and 89% cyclohexanone selectivity with 10% Pd/AC catalyst at 80 °C and 9 h. Obviously, the activity of Pd/metal oxide and Pd/AC catalysts were far less than satisfactory. See the complex nanostructured catalysts 3% Pd/@-10% CeO₂/AC and 3% Pd/@-10% La₂O₃/AC catalysts (Table 2, entry 9 and 15), they exhibited remarkable catalytic performance for selective



Table 2 Hydrogenation of phenol with the different catalysts^a

Entry	Catalyst	Phenol conversion (%)	Selectivity ^b (%)	
			C=O	C-OH
1	3% Pd/AC	76.62	96.21	3.79
2 ^c	10% Pd/AC	55	89	11
3	3% Pd/CeO ₂	4.50	99.20	0.8
4	3% Pd/La ₂ O ₃	8.15	100	0
5	10% CeO ₂ /AC	—	—	—
6	10% La ₂ O ₃ /AC	—	—	—
7	1% Pd/@-10% CeO ₂ /AC	32.6	96.30	3.70
8	2% Pd/@-10% CeO ₂ /AC	70.00	95.80	4.20
9	3% Pd/@-10% CeO ₂ /AC	97.22	96.32	3.68
10	3% Pd/@-5% CeO ₂ /AC	72.12	96.91	3.09
11	3% Pd/@-2% CeO ₂ /AC	66.73	97.14	2.86
12	3% Pd/@-1% CeO ₂ /AC	60.90	96.93	3.07
13	1% Pd/@-10% La ₂ O ₃ /AC	10.98	100	0
14	2% Pd/@-10% La ₂ O ₃ /AC	49.24	97.12	2.88
15	3% Pd/@-10% La ₂ O ₃ /AC	100	96.82	3.18
16	3% Pd/@-5% La ₂ O ₃ /AC	96.52	97.07	2.93
17	3% Pd/@-2% La ₂ O ₃ /AC	88.08	97.16	2.84
18	3% Pd/@-1% La ₂ O ₃ /AC	79.69	97.35	2.65

^a Reaction conditions: phenol (0.1 g), $n(\text{Pd}) : n(\text{phenol}) = 0.75\%$, CH_2Cl_2 (20 mL), 70 °C, 3 h, 0.7 MPa H_2 . ^b C=O indicates cyclohexanone and C-OH indicates cyclohexanol. ^c Reaction conditions: phenol (40 mg), 5 mol% Pd relative to phenol, H_2O (3 mL), 80 °C, 9 h, 0.1 MPa H_2 .¹⁸

hydrogenation of phenol, conversion of phenol were achieved up to 100%, selectivity of cyclohexanone were higher than 96%. According to the above results, the complex nanostructured catalysts showed a high activity because of the synergistic effect between metal nanoparticles and nano-semiconductors support, which enhanced effect of electronic promote the excellent charge transfer, promoted the synthesis of cyclohexanone and increase its selectivity. Then, the nature of the support plays an important role on activity and selectivity of Pd catalysts, because it has a large specific surface area and the add of Ce or La could increase the alkaline of catalyst,^{27,50-52} which provided a large enough place for the hydrogenation of phenol and avoid the co-planar adsorption of phenol, thus improved the selectivity of cyclohexanone. These results indicated that the Pd complex nanostructured catalysts have superiority catalytic activity.

The loading of metal oxide has a great influence on the structure and catalytic performances of the complex nanostructured catalyst. Only Pd nanoparticles have been equally anchored on the nano-CeO₂ or nano-La₂O₃ film layer, which was spread on the high specific surface AC, these complex nanostructured Pd catalysts exhibit synergistic catalysis and remarkable catalytic performances for the hydrogenation reaction of phenol. According to principles of the spontaneous monolayer distribution, metal oxide would disperse on the support at the state of the spontaneous monolayer distribution, when the content of metal oxide is less than a certain threshold and surface area of the support is large enough, so an appropriate amount of CeO₂ or La₂O₃ can form a single or multi-layer nano-semiconductor layer on AC. From Table 2, when the loading of metal oxide was 10%, the conversion of phenol was achieved 100% and 97.22% by using 3% Pd/@-10% La₂O₃/AC and 3% Pd/@-10% CeO₂/AC as catalyst, respectively. The conversion of phenol was 72.12% when the loading of CeO₂ was 5% (Table 2, entry 10), while the conversion decreased to 60.9% when CeO₂ content was 1% (Table 2, entry 12). The 3% Pd/@-xLa₂O₃/AC catalyst was observed same result, the lower loading of La₂O₃, the lower conversion (Table 2, entry 15-18). Compared the 3% Pd/@-1% La₂O₃/AC (Table 2, entry 18) with the 3% Pd/AC (Table 2, entry 1), it shown that add a few La₂O₃ could enhanced catalytic performance. The reason was that the nano-La₂O₃ improve the dispersity of the Pd particles, consistent with the result from the TEM images (Fig. 2e). But a few loading of La₂O₃ could not formed the rare-earth oxide layer, therefore Pd nanoparticles may be mostly supported on activated carbon directly rather than loaded on composite support with metal oxides. Moreover, Table 2 was also confirmed that a low loading of Pd was unfavorable for the formation of cyclohexanone. For Pd/@-CeO₂/AC catalyst, the phenol conversion decreased quickly from 97.22% (Table 2, entry 9) to 32.6% (Table 2, entry 7) when the loading of Pd from 3% to 1%. For Pd/@-La₂O₃/AC catalyst, the phenol conversion decreased from 100% (Table 2, entry 15) to 10.98% (Table 2, entry 13) when the loading of Pd from 3% to 1%.

These results also shown that the catalytic performance difference between 3% Pd/@-10% La₂O₃/AC and 3% Pd/@-10% CeO₂/AC, the possible reason could be attribute to the specific surface area. The specific surface area of 3% Pd/@-10% La₂O₃/

Table 3 Performance of 3% Pd/@-10% La₂O₃/AC and 3% Pd/@-10% CeO₂/AC at different times, temperatures and H₂ pressures^a

Entry	Time (h)	Temperature (°C)	H ₂ pressure (MPa)	Pd/@-La ₂ O ₃ /AC		Pd/@-CeO ₂ /AC	
				Conversion (%)	Selectivity (%)	Conversion (%)	Selectivity (%)
1	3	50	0.7	52.26	96.79	42.62	95.35
2	3	60	0.7	95.16	97.11	46.48	95.75
3	1	70	0.7	55.34	98.11	43.25	96.51
4	2	70	0.7	92.59	97.61	71.70	95.60
5	3	70	0.7	100	96.82	98.28	96.33
6	3	70	0.6	85.6	96.77	58.10	96.67
7	3	70	0.5	79.14	97.3	45.32	96.70

^a Reaction conditions: phenol (0.1 g), catalyst (0.353 g), $n(\text{Pd})/n(\text{phenol}) = 0.75\%$, CH_2Cl_2 (20 mL).



Table 4 Performance of 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ and 3% Pd/@-10% CeO_2/AC at different solvents^a

Time (h)	Solvent	Pd/@- $\text{La}_2\text{O}_3/\text{AC}$		Pd/@- CeO_2/AC		
		Conversion (%)	Selectivity (%)	TOF (h ⁻¹)	Conversion (%)	Selectivity (%)
3	CH_2Cl_2	100	96.82	44.35	98.28	96.33
3	H_2O	54.13	96.29	24.01	35.27	96.70
5	H_2O	100	94.88	26.61	54.36	97.60

^a Reaction conditions: phenol (0.1 g), catalyst (0.353 g), $n(\text{Pd})/n(\text{phenol}) = 0.75\%$, 70 °C, 0.7 MPa H_2 . Turnover frequency (TOF) defined as (mole of product/(moles of Pd × reaction time)).

AC (1349.667 m² g⁻¹) was more than 3% Pd/@-10% CeO_2/AC (1138.102 m² g⁻¹), so it was more beneficial to material transfer. The other reason can be find in TEM, the Pd particles of 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ was more uniformly dispersed and more smaller than 3% Pd/@-10% CeO_2/AC . As we all know, the high dispersed noble metal catalyst often exhibit high catalytic performances.

In order to fully illustrate the superiority catalytic performance of the complex nanostructured catalysts, the catalytic performance of Pd/@- CeO_2/AC and Pd/@- $\text{La}_2\text{O}_3/\text{AC}$ were investigated under various reaction conditions (Table 3). When reaction temperature increased from 50 °C, 60 °C to 70 °C, the conversion of phenol increased quickly (Table 3, entry 1, 2, 5). Increasing reaction temperature could made the reactant molecular energy increased and the activated molecule number continually increased, and accelerated the reaction rate. At the same time, it was indicated that a high H_2 pressure was more favorable for the formation of cyclohexanone, the selectivity only declined slightly (Table 3, entry 5, 6, 7). Considered that the higher H_2 pressure, the more H_2 participated in reaction, the cyclohexanone could not quickly out of active site, then lead to further hydrogenation for cyclohexanol. Also, the results showed that phenol conversion increased quickly as the reaction time was extended from 1 h to 3 h (Table 3, entry 3–5).

Consider the environmental impact of the solvent, we also select H_2O as a solvent, compared the performance of both Pd/@- CeO_2/AC and Pd/@- $\text{La}_2\text{O}_3/\text{AC}$ under the same conditions, the results were shown in Table 4. The phenol hydrogenation

reaction used CH_2Cl_2 as a solvent was so much better than that of in H_2O . The conversion of phenol were only 54.13% and 35.27% in water within 3 h by Pd/@- $\text{La}_2\text{O}_3/\text{AC}$ and Pd/@- CeO_2/AC catalyst, respectively. When the reaction time extends to 5 h, the Pd/@- $\text{La}_2\text{O}_3/\text{AC}$ catalyst catalyzed phenol totally conversion, we can inferred that phenol hydrogenation reaction in water instead of organic solvent should not be affected by mass transfer resistance and the phenol conversion will achieve 100% in water when the reaction time was enough long. But whether Pd/@- $\text{La}_2\text{O}_3/\text{AC}$ or Pd/@- CeO_2/AC , the turnover frequency (TOF) in H_2O was lower than it in CH_2Cl_2 . The TOF of the Pd/@- $\text{La}_2\text{O}_3/\text{AC}$ catalyst in CH_2Cl_2 could reach 44.35 h⁻¹, and is higher than that of in H_2O (24.01 h⁻¹). For Pd/@- CeO_2/AC catalyst, the TOF in CH_2Cl_2 (36.98 h⁻¹) is also higher than that of in H_2O (15.64 h⁻¹). Because the catalysts were dispersed in CH_2Cl_2 preferably, and H_2 had a better solubility, so phenol was easier adsorbed on the surface of catalysts for hydrogenate to cyclohexanone.

Fig. 4 illustrates the TOF obtained in the hydrogenation of phenol with the different catalysts (include different metal oxide loading) in CH_2Cl_2 . The TOF of the Pd/@- $\text{La}_2\text{O}_3/\text{AC}$ catalysts was higher than Pd/@- CeO_2/AC catalyst with different loading of rare-earth oxide as a whole. When the loading of rare-earth oxide achieved 10%, the TOF reached maximum, 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ catalyst is 44.35 h⁻¹ and 3% Pd/@-10% CeO_2/AC is 36.98 h⁻¹. For 3% $\text{Pd/La}_2\text{O}_3$ and 3% Pd/CeO_2 , only 3.59 h⁻¹ and 1.99 h⁻¹ TOF were obtained under the same conditions, respectively. Less than one-tenth of the complex nanostructured catalysts. The TOF of 3% Pd/AC was 33.98 h⁻¹, less than the 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ or 3% Pd/@-10% CeO_2/AC . This result indicated that these novel nano-Pd complex catalysts were high efficient selective hydrogenation of phenol.

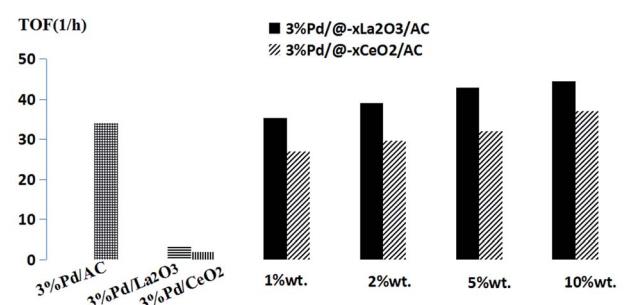


Fig. 4 The TOF of hydrogenation of phenol with the different catalysts. The x represents the CeO_2/AC and $\text{La}_2\text{O}_3/\text{AC}$ loading by weight. The conditions are as follows: $n(\text{Pd})/n(\text{phenol}) = 0.75\%$, 20 mL CH_2Cl_2 , 70 °C, 0.7 MPa H_2 , 3 h. Turnover frequency (TOF) defined as (mole of product/(moles of Pd × reaction time)).

3.3 Catalytic activity

In Table 2, it was clear that the 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$ and 3% Pd/@-10% CeO_2/AC catalysts exhibited high efficient catalytic activity for hydrogenation of phenol to cyclohexanone. To further understand the catalytic performance of the complex nanostructured catalysts, $\text{H}_2\text{-TPR}$ of the catalysts and AC, 10% CeO_2/AC , 10% $\text{La}_2\text{O}_3/\text{AC}$, 3% Pd/@-10% $\text{La}_2\text{O}_3/\text{AC}$, 3% Pd/@-10% CeO_2/AC were carried out. The results are shown in Fig. 5. Two peaks at 462.1 °C and 663.5 °C in the AC sample could be attributed to the oxygen-containing functional groups like $-\text{COOH}$, $-\text{OH}$, $=\text{O}$, which is a feature of carbon, etc.⁵¹ The reduction peak was observed at 556.2 °C over CeO_2/AC . For



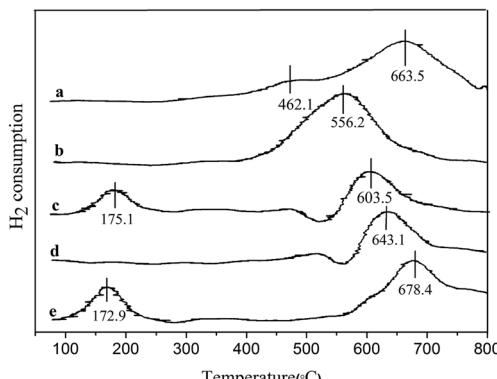


Fig. 5 TPR profiles of catalysts. (a) AC, (b) CeO_2/AC , (c) $\text{Pd}/@\text{-CeO}_2/\text{AC}$, (d) $\text{La}_2\text{O}_3/\text{AC}$, (e) $\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$.

CeO_2/AC , the low temperature peak at 400–600 °C was due to the reduction of surface oxygen species attached to surface Ce^{4+} ions in an octahedral coordination.²² H_2 -TPR of $\text{La}_2\text{O}_3/\text{AC}$ show one reduction peak at 643.1 °C that may be ascribed to the reduction of La_2O_3 .

The TPR profiles of the CeO_2/AC and $\text{La}_2\text{O}_3/\text{AC}$ supported Pd catalysts changed significantly compared with those of CeO_2/AC and $\text{La}_2\text{O}_3/\text{AC}$. For $\text{Pd}/@\text{-CeO}_2/\text{AC}$, there were two other reduction peaks at 175.1 °C and 603.5 °C. The latter was ascribed to the reduction of the bulk oxygen of CeO_2 . The peak at 175.1 °C was assigned to the reduction of the species related to the $\text{PdO}-\text{CeO}_2$ interaction, which suggests that PdO is well-dispersed on the support and CeO_2 interacts with PdO .⁵² For $\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$, there were two other reduction peaks at 172.9 °C and 678.4 °C. The latter was ascribed to the reduction of the La_2O_3 . The former was considered the reduction of PdO which was affected by La_2O_3 . Such results are also shown that the reduction temperature of PdO in $\text{Pd}/@\text{-CeO}_2/\text{AC}$ or $\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$ shifts to a higher value compared with the individual PdO (50 °C). It is further demonstrated that the complex nanostructured catalysts exhibit synergistic effect of both nano-Pd and nano- $\text{La}_2\text{O}_3/\text{AC}$ or nano- CeO_2/AC .

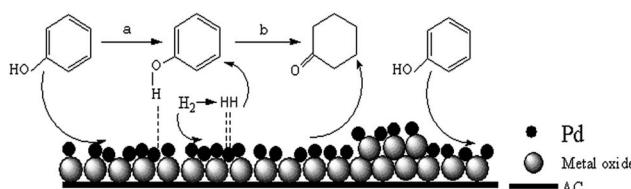
3.4 Compare with other catalyst

To unveil the underlying factors that provide the superior activity of the hydrogenation over these complex nanostructured catalysts ($\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$ and $\text{Pd}/@\text{-CeO}_2/\text{AC}$), we

compared the TOF for the hydrogenation of phenol over these complex nanostructured catalysts with other catalysts in Table 5. The result shown that the $\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$ catalyst catalytic the hydrogenation of phenol to cyclohexanone could be finished within 3 h, with a TOF reaching over 44.35 h^{-1} . TOF of the $\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$ catalyst was about an order of magnitude higher than that of traditional catalysts and 2-fold higher than that of the best reported catalyst $\text{Pd}/\text{Al}_2\text{O}_3\text{-CWE}$ (Table 5, entry 3). It is illustrated that the complex nanostructured catalyst was an efficient catalytic system and exhibited outstanding activity and selectivity for phenol hydrogenation.

3.5 Possible reaction mechanism of phenol over complex nanostructured catalysts

In our study, the main product is cyclohexanone, a small amount of cyclohexanol (very slight). Generally, phenol was adsorbed by “non-planar” on alkaline support which was more advantage for the production of cyclohexanone. Whereas, it was more tend to produce cyclohexanol that phenol was adsorbed by “co-planar” on acidity support.^{28,57} As we all know, the adding of Ce or La could increase the alkaline of catalyst, then phenol was adsorbed by non-planar, inhibited the saturated hydrogenation of phenol to cyclohexanol. According to reaction results and the discussion above, possible reaction mechanism was proposed as the following. The process is shown in Scheme 3. The strong interaction between Pd and rare-earth oxide increases the ability to attract electron of hydroxyl group on phenol by non-planar, on which the H in the excited state could react on active benzene ring. After benzene ring hydrogenated to cyclohexanone, cyclohexanone was quickly dissociation of active site, otherwise it will further hydrogenation for cyclohexanol.



Scheme 3 Mechanism of phenol hydrogenation with catalysis of $\text{Pd}/@\text{-CeO}_2/\text{AC}$ or $\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$.

Table 5 Comparison of different catalysts for phenol hydrogenation^a

Entry	Catalyst	$n(\text{Pd}) : n(\text{phenol}) (\%)$	T (°C)	Time (h)	Conversion (%)	Selectivity (%)	TOF (h^{-1})	Note
1	$\text{Pd}/@\text{-La}_2\text{O}_3/\text{AC}$	0.75	70	3	100	96.82	44.35	This work
2	$\text{Pd}/@\text{-CeO}_2/\text{AC}$	0.75	70	3	98.28	96.33	36.98	This work
3	$\text{Pd}/\text{Al}_2\text{O}_3\text{-CWE}$	2.5	100	2	100	98	20.05	Ref. 53
4	$\text{Pd}/\text{TiO}_2\text{-AC}$	1.6	50	4	47.3	96.4	15.27	Ref. 54
5	$\text{Pd}/\text{MIL-101}$	1.8	50	4	99.6	80.3	13.52	Ref. 55
6	Pd/SiO_2	2	60	7.5	99	97	6.32	Ref. 56
7	Pd-HPW	5	80	7	>99	>99	2.86	Ref. 20
8	Pd-PANI/CNT	5	80	9	>99.9	>99	2.22	Ref. 18

^a Turnover frequency defined as (mole of product/(moles of Pd \times reaction time)).



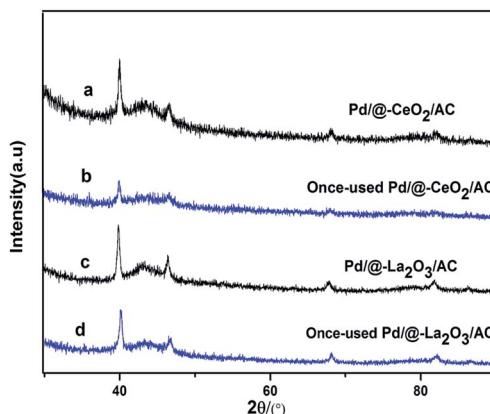


Fig. 6 The XRD patterns of catalysts, (a) Pd@-CeO₂/AC, (b) once-used Pd@-CeO₂/AC, (c) Pd@-La₂O₃/AC, (d) once-used Pd@-La₂O₃/AC.

After the reaction, the catalysts were recycled for phenol hydrogenation. The activity of Pd@-La₂O₃/AC and Pd@-CeO₂/AC were decreased. The XRD patterns of the once-used Pd@-La₂O₃/AC and once-used Pd@-CeO₂/AC were shown in Fig. 6. The Pd peaks of once-used catalysts were weakened, due to the destruction of the special structural and lost its portion activity component. Further study for the repeatability of the catalysts is still carried out.

4. Conclusions

Novel complex nanostructured catalysts Pd@-La₂O₃/AC and Pd@-CeO₂/AC have been successfully fabricated *via* a photochemical route. The prepared catalysts Pd@-La₂O₃/AC and Pd@-CeO₂/AC exhibited excellent performance of phenol hydrogenation under mild conditions. The results shown that 100% conversion of phenol and a selectivity higher than 96% were achieved within 3 h at 70 °C and 0.7 MPa H₂ pressure, and the activity of Pd complex nanostructured catalyst was better than that of supported Pd on the metal oxide or AC directly. Furthermore, H₂O was used as solvent, the prepared complex nanostructured catalysts also exhibited remarkable performance of phenol hydrogenation. It is indicated that the remarkable activity of these complex nanostructured catalysts may be ascribed to the synergistic effect of the interaction between active component nano-Pd and atom-layer rare-earth oxide, and enhance effect of electron of complex nanostructured catalysts, and formation of more contact interface due to the high dispersion of Pd particles on the large surface area support La₂O₃/AC and CeO₂/AC. This work demonstrated that novel complex nanostructured catalysts Pd@-La₂O₃/AC and Pd@-CeO₂/AC prepared *via* a photochemical route exhibited synergistic catalysis of nano-Pd and rare-earth oxide, and opened a new direction of complex nanostructured catalyst. The synergistic catalysis of complex nanostructured catalyst opened a promising direction to developing nanostructured catalyst for heterogeneous catalytic reaction.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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References

- 1 R. D. Patil and Y. Sasson, *Appl. Catal., A*, 2015, **499**, 227–231.
- 2 X. Xuan, L. Haoran and W. Yong, *ChemCatChem*, 2015, **6**, 3328–3332.
- 3 J. Hong, Q. Zhengyan, L. Ying, H. Jun, C. Rizhi and X. Weihong, *Chem. Eng. J.*, 2016, **284**, 724–732.
- 4 H. Shuo, Z. Xiang, Q. Zhengyan, J. Hong, L. Yefei, H. Jun, X. Weihong and C. Rizhi, *J. Ind. Eng. Chem.*, 2017, **53**, 333–340.
- 5 Z. Fengwei, C. Shuai, L. Huan, Z. Xianming and Y. Hengquan, *RSC Adv.*, 2015, **5**, 102811–102817.
- 6 M. Juan and C. Avelino, *Appl. Catal., A*, 2011, **404**, 103–112.
- 7 N. Mahata, K. V. Raghavan, V. Vishwanathan, C. Parkb and M. A. Keane, *Phys. Chem. Chem. Phys.*, 2001, **3**, 2712–2719.
- 8 G. S. Sheldon, D. Errun, P. Colin and A. K. Mark, *J. Mol. Catal. A: Chem.*, 2004, **212**, 291–300.
- 9 W. Shingo and A. Venu, *Top. Catal.*, 2010, **53**, 1150–1152.
- 10 M. Kohsuke, F. Ken, O. Shusuke and Y. Hiromi, *Chem. Commun.*, 2012, **48**, 8886–8888.
- 11 Y. Hiroshi, N. Satomi, F. Shinichiro and A. Masahiko, *J. Mol. Catal. A: Chem.*, 2013, **379**, 80–85.
- 12 M. S. Priscilla, C. R. N. Raimundo, E. P. B. Luiz, J. Gary, H. D. Burtron, M. G. Uschi, E. R. Daniel and B. N. Fabio, *ACS Catal.*, 2015, **5**, 7385–7398.
- 13 G. Qingqing, Z. Yanhua, S. Junjun, C. XinSheng, G. Junjie, M. Rongrong, L. Bin and N. Ping, *Chem. Eng. J.*, 2016, **299**, 63–73.
- 14 K. Sergey, M. Anton, Z. Anna and K. Eduard, *Catal. Commun.*, 2016, **73**, 63–68.
- 15 L. Huizhen, J. Tao, H. Buxing, L. Shuguang and Z. Yinxi, *Science*, 2009, **326**, 1250–1252.
- 16 W. Yong, Y. Jia, L. Haoran, S. Dangsheng and A. Markus, *J. Am. Chem. Soc.*, 2011, **133**, 2362–2365.
- 17 Z. Mengsi, S. Juanjuan and H. Zhaoyin, *Chin. J. Catal.*, 2016, **37**, 234–239.
- 18 C. Jinzhu, Z. Wei, C. Limin, M. Longlong, G. Hui and W. Tiejun, *ChemPlusChem*, 2013, **78**, 142–148.
- 19 C. Aibing, L. Yonglei, C. Jinzhu, Z. Guoying, M. Longlong and Y. Yifeng, *ChemPlusChem*, 2013, **78**, 1370–1378.
- 20 C. Aibing, Z. Guoying, C. Jinzhu, C. Limin and Y. Yifeng, *RSC Adv.*, 2013, **3**, 4171–4175.
- 21 X. Guangyue, G. Jianhua, Y. Zhang, Y. Fu, C. Jinzhu, M. Longlong and G. Qingxiang, *ChemCatChem*, 2015, **7**, 2485–2492.
- 22 Y. Ye, W. Zhimiao, A. Hualiang, X. Wei and W. Yanji, *Chin. J. Catal.*, 2015, **36**, 1142–1154.
- 23 L. Lianjun, C. Yuan, S. Wenjing, Y. Zhijian, L. Bin, G. Fei and D. Lin, *Catal. Today*, 2011, **175**, 48–54.



24 W. Zili, L. Meijun and H. O. Steven, *J. Catal.*, 2012, **285**, 61–73.

25 C. N. Nicholas, J. M. Sebastián, D. S. Aaron, H. O. Steven and I. S. Igor, *ACS Catal.*, 2015, **5**, 2051–2061.

26 K. SangWoo and R. ShiWoo, *J. Electrochem. Soc.*, 2002, **6**, C345–C348.

27 S. Salvatore, M. Simona and C. Carmelo, *Appl. Catal., A*, 2002, **235**, 21–31.

28 S. Velu, M. P. Kapoor, S. Inagaki and K. Suzuki, *Appl. Catal., A*, 2003, **245**, 317–331.

29 Q. Fu, H. Saltsburg and M. Flytzani-Stephanopoulos, *Science*, 2003, **301**, 935–938.

30 F. Qi, W. Deng, H. Saltsburg and M. Flytzani-Stephanopoulos, *Appl. Catal., B*, 2005, **56**, 57–68.

31 Y. Ming, L. F. Allard and F. S. Maria, *J. Am. Chem. Soc.*, 2013, **135**, 219–224.

32 Q. Botao, W. Aiqin, Y. Xiaofeng, L. F. Allard, J. Zheng, C. Yitao, L. Jingyue, L. Jun and Z. Tao, *Nat. Chem.*, 2011, **3**, 634–641.

33 L. Jian, W. Aiqin, Q. Botao, L. Xiaoyan, Y. Xiaofeng, W. Xiaodong, L. Jinxia, L. Jun, L. Jingyue and Z. Tao, *J. Am. Chem. Soc.*, 2013, **135**, 15314–15317.

34 Y. XiaoFeng, W. Aiqin, Q. Botao, L. Jun, L. Jingyue and Z. Tao, *Acc. Chem. Res.*, 2013, **46**, 1740–1748.

35 Z. Jicheng, Y. Xiaofeng, W. Yaqiong and C. Weijun, *Catal. Commun.*, 2014, **46**, 228–233.

36 L. Lin, Z. Jicheng, X. Zhibo and O. Wenbing, *Acta Pet. Sin.*, 2013, **29**, 975–983.

37 W. Yaqing, Z. Jicheng and Y. Xiaofeng, *Chin. J. Process Eng.*, 2009, **6**, 1186–1191.

38 G. Glaspell, L. Fuoco and M. S. El-Shall, *J. Phys. Chem. B*, 2005, **37**, 17350–17355.

39 S. F. Chen, J. P. Li and K. Qian, *Nano Res.*, 2010, **3**, 244–255.

40 P. Liu, Y. Zhao, R. Qin, S. Mo, G. Chen, L. Gu, D. M. Chevrier, P. Zhang, Q. Guo, D. Zang, B. Wu, G. Fu and N. Zheng, *Science*, 2016, **352**(6287), 797.

41 H. Gu, Y. Yang, J. Tian and G. Shi, *ACS Appl. Mater. Interfaces*, 2013, **5**, 6762–6768.

42 G. K. Lau, T. S. Zhang and G. K. L. Goh, *J. Nanosci. Nanotechnol.*, 2010, **10**, 4733–4737.

43 X. L. Seoane, N. S. Figoli, P. C. L'Argentiere, J. A. Gonzalez and A. Arcoya, *Catal. Lett.*, 1997, **47**, 213–220.

44 S. Zheng and L. Gao, *Mater. Chem. Phys.*, 2002, **78**, 512–517; S. A. Khan and A. Ahmad, *Mater. Res. Bull.*, 2013, **48**, 4134–4138.

45 R. V. Gulyaev, E. M. Slavinskaya, S. A. Novopashin, D. V. Smovzh, A. V. Zaikovskii, D. Y. Osadchii, O. A. Bulavchenko, S. V. Korenev and A. I. Boronin, *Appl. Catal., B*, 2014, **147**, 132–143.

46 D. Shuaishuai, Z. Chunhua, L. Yefei, J. Hong, X. Weihong and C. J. Rizhi, *Ind. Eng. Chem.*, 2017, **46**, 258–265.

47 E. A. Anumol, P. Kundu, P. A. Deshpande, G. Madras and N. Ravishankar, *ACS Nano*, 2011, **5**, 8049–8061.

48 H. Spod, M. Lucas and P. Claus, *ChemCatChem*, 2016, **8**, 1–9.

49 L. Yi, X. Xuan, Z. Pengfei, G. Yutong, L. Haoran and W. Yong, *RSC Adv.*, 2013, **3**, 10973–10982.

50 L. Hui, L. Jianliang and L. Hexing, *Mater. Lett.*, 2008, **62**, 297–300.

51 L. Hui, L. Jun, X. Songhai, Q. Minghua, D. Weilin, L. Yunfeng and L. Hexing, *Adv. Funct. Mater.*, 2008, **18**, 3235–3241.

52 S. Chandra Shekar, J. Krishna Murthy, P. Kanta Rao and K. S. Rama Rao, *J. Mol. Catal. A: Chem.*, 2003, **191**, 45–59.

53 Z. Huaqing, Q. Zhangfeng, S. Wenjuan, S. Wenjie and W. Jianguo, *J. Catal.*, 2004, **225**, 267–277.

54 Y. Pérez, M. Fajardo and A. Corma, *Catal. Commun.*, 2011, **12**, 1071–1074.

55 Z. Damin, Y. Feiyang, X. Teng, G. Yejun and W. Yi Meng, *Catal. Today*, 2014, **234**, 133–138.

56 C. Ling, D. Qiguang, L. Hua and W. Xingyi, *Catal. Commun.*, 2014, **57**, 23–28.

57 Y. Z. Chen, C. W. Liaw and L. I. Lee, *Appl. Catal., A*, 1999, **177**, 1–8.