

Cite this: *RSC Adv.*, 2017, 7, 51142

# An $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$ core-shell heterogeneous catalyst for aerobic oxidation of alcohols and benzylic oxidation reaction†

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A novel magnetic  $\text{Fe}_3\text{O}_4@\text{P4VP}(\text{poly}(4\text{-vinylpyridine}))@\text{FeCl}_3$  core-shell structure was successfully synthesized. Its  $\text{Fe}_3\text{O}_4@\text{P4VP}$  core was initially prepared via polymerization of 4-vinyl pyridine on the surface of  $\text{Fe}_3\text{O}_4$  microspheres. The successful introduction of the  $\text{FeCl}_3$  moiety as a catalytic active site was achieved through coordination interaction between P4VP and  $\text{FeCl}_3$ . The obtained  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  catalyst was applied in the selective oxidation of alcohols using molecular oxygen as the oxidant. It was shown that a variety of alcohol substrates is tolerated under optimized reaction conditions. Additionally, benzylic oxidation of hydrocarbon compounds was also evaluated using  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  as the catalyst and *t*BuOOH as the oxidant, achieving high yields and very good selectivities. The heterogeneity of the  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  core-shell catalyst was tested and the initial activity was maintained after five reuses.

Received 15th August 2017  
Accepted 29th October 2017

DOI: 10.1039/c7ra09005f

rsc.li/rsc-advances

## 1. Introduction

The catalytic selective oxidation of alcohols to the corresponding carbonyl compounds is one of the most industrially significant reactions in fine and industrial organic chemistry.<sup>1</sup> The use of transition metal-based homogeneous<sup>2</sup> and heterogeneous<sup>3</sup> catalysts is a good strategy as the use of stoichiometric oxidants such as chromate or permanganate is replaced by atom-economical clean oxidants. However, heterogeneous processes are preferable for oxidation, as they display several advantages during the purification and recovery steps of products and catalysts.<sup>4</sup> Oxidizing alcohols heterogeneously using molecular oxygen is an ideal reaction process, since it produces  $\text{H}_2\text{O}$  as the sole by-product.<sup>5</sup> Recently, aerobic oxidations received much attention because of their use of inexpensive oxidants and controllable selectivities. Studies about homogeneous catalysts for aerobic oxidation reactions are abundant in the literature.<sup>6</sup> Several successful noble metal catalytic systems, such as gold,<sup>7</sup> palladium,<sup>8</sup> platinum,<sup>9</sup> rhodium,<sup>10</sup> ruthenium,<sup>11</sup> *etc.* were reported for having achieved efficient oxidation of alcohols.

Over the years, the utilization of relatively inexpensive transitional metals like copper or iron have been considered an approach towards the replacement of such expensive precious metal catalysts. Although copper derived catalysts have been studied thoroughly over the years as an alternative to platinum-based ones in the oxidation of alcohols,<sup>12</sup> iron derived ones remain relatively underexplored. Iron is less expensive and more naturally abundant than copper and other transitional metals. Since the first iron-promoted oxidation of alcohols was reported in 2002,<sup>13</sup> this field witnessed an increase in iron use for the promotion of oxidation reactions. Wang and coworkers reported a  $\text{FeCl}_3\text{-TEMPO-NaNO}_2$  system,<sup>14</sup> while Ma and colleagues have published an  $\text{Fe}(\text{NO}_3)_3\text{-TEMPO-NaCl}$  system<sup>15</sup> for oxidation reactions. However, homogeneous iron catalytic systems make the recovery of the catalyst extremely difficult, which might pose limitations to industrial scale applications. Thus, in recent years, numerous heterogeneous supports, such as molecular sieves,<sup>16</sup> aluminosilicates,<sup>17</sup> graphene-oxide<sup>18</sup> polymer<sup>19</sup> and inorganic microspheres, have been developed and applied to the alcohol oxidation reaction.<sup>20</sup>

Although heterogeneous iron catalysts were achieved in a stable and reusable manner, they commonly showed lower efficiency and metal leaching compared to their homogeneous counterparts. Among these heterogeneous catalysts, core-shell structures have been considered highly practical as they take advantage of their unique physicochemical and multi-functional properties.<sup>21</sup> Magnetic core-shell structures are of particular interest as an effective separation method since they could easily and quickly respond to an external magnetic field.<sup>22</sup> Many magnetic core-shell composites have been developed

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† Electronic supplementary information (ESI) available. See DOI: 10.1039/c7ra09005f

utilizing different coatings, such as silica, carbon, polymeric and porous materials on a  $\text{Fe}_3\text{O}_4$  core.<sup>23</sup> Several hybrid magnetic core-shell nanocatalysts have been utilized in reductions, oxidations, epoxidations, coupling reactions and photo-catalytic reactions.<sup>24</sup> To the best of our knowledge, the combination of magnetic functionality and iron catalytic sites have not been reported in the literature yet. In this work, a core-shell  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  catalyst was synthesized and it was characterized by transmission electron microscopy (TEM), powder X-ray diffraction (PXRD), FTIR spectroscopy, thermogravimetric analysis (TGA) and vibrating sample magnetometry (VSM). Numerous pyridine functional groups provided multi-dentate coordination to the iron(III) ion, which helps stabilizing the metal center. The aerobic oxidation of alcohols and benzylic carbons were both investigated using our synthesized  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  catalyst. High chemical stability and low metal leaching were observed for the oxidation catalysis using our core-shell catalyst.

## 2. Experimental section

### 2.1 General information

All reaction substrates and solvents were purchased from Sigma-Aldrich, Alfa Aesar or Aladdin. Ferric chloride hexahydrate ( $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ ), polyvinyl pyrrolidone (PVP;  $M_r = 58\,000$ ), divinylbenzene (DVB, 80%), potassium persulfate (KPS, 99%) were purchased from Alfa Aesar and were used as received. Poly(acrylic acid) (PAA;  $M_r = 1800$ ) and 2,2'-azobis (2-methylpropionamidine) dihydrochloride (97%) were purchased from Sigma-Aldrich. Anhydrous sodium acetate (99%) was supplied by Aladdin. 4-Vinylpyridine monomer (96%, 4VP; Aldrich) was stabilized with 100 ppm hydroquinone and used after distillation.

### 2.2 Characterization

The morphology and size of the as-obtained samples were characterized on a ZEISS SUPRA55 scanning electron microscopy (FESEM). High-resolution transmission electron microscopy (HRTEM) studies were carried out on a JEOL JEM 2010 transmission electron microscope with an accelerating voltage of 200 kV. The phase structure was determined by powder X-ray diffraction (p-XRD) experiments on a DADVANCE diffractometer with  $\text{Cu K}\alpha$  radiation scanning from  $10^\circ$  to  $80^\circ$ . Fourier-transformed infrared spectra (FTIR) were recorded using a NICOLET 6700 infrared spectrophotometer using KBr pellet samples. The magnetization curves of samples were measured by a MPMS-XL superconducting quantum interference device (SQUID) at room temperature. The thermogravimetric analysis (TGA) was carried out on a NETZSCH STA409 at a heating rate of  $10^\circ\text{C min}^{-1}$  under nitrogen. X-ray photoelectron spectroscopy data were obtained with a PHI Quantera SXM. Gas chromatography-mass spectrum was recorded using Agilent 7890A/5975C. Products were determined by GC-MS using internal standard technique, and nitrobenzene was used as an internal standard.

### 2.3 Synthesis of the $\text{Fe}_3\text{O}_4@\text{P4VP}$ materials

The PAA-modified  $\text{Fe}_3\text{O}_4$  nanoparticles were prepared through an improved one-step solvothermal method reported in the

literature.<sup>25</sup> In a typical procedure,  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  (1.08 g), PAA (0.108 g), and sodium acetate (9 g) were all dissolved in ethylene glycol (40 mL) to form a homogeneous solution. Then, the solution was transferred to a 50 mL Teflon-lined stainless-steel autoclave and maintained at  $200^\circ\text{C}$  for 12 h. After being cooled to room temperature, the obtained black products were washed with deionized water and ethanol several times, and then dried in a vacuum for 12 h. The core-shell  $\text{Fe}_3\text{O}_4@\text{P4VP}$  microspheres were prepared as follows: PAA-modified  $\text{Fe}_3\text{O}_4$  (0.1 g) was dispersed with PVP (0.15 g) in 100 mL deionized water under ultrasonication. After being transferred into a 250 mL four-necked flask, an emulsion contained PVP (0.05 g), 4-VP (0.125 g), DVB (0.125 g), and deionized water (20 mL) were added. All of the solution was bubbled with nitrogen for 12 h under stirring. When the temperature was raised to  $70^\circ\text{C}$ , a KPS solution (0.25 mL,  $0.04\text{ g mL}^{-1}$ ) was added into the reaction system. After 4 h of polymerization, the obtained products were washed with ethanol several times and dried under vacuum for 12 h.

### 2.4 Synthesis of the $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$

5.0 g  $\text{Fe}_3\text{O}_4@\text{P4VP}$  nanoparticles were dispersed in 100 mL of  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  ethanol solution (0.2 M). The solution was stirred for 12 h at  $70^\circ\text{C}$  in an oil bath. The sample was recovered using a permanent magnet and washed with ethanol, and dried under vacuum at  $80^\circ\text{C}$ . The amount of iron was analyzed by inductively coupled plasma-atomic emission spectrometry (ICP-AES); the contents of iron in  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  was determined to be 4.36 wt%.

### 2.5 General procedure for the aerobic oxidation of alcohol

In general, the catalytic reaction was carried out under the following conditions: 2 mol%  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  core-shell catalyst (mole percent was based on iron), 0.1 mmol  $\text{NaNO}_2$ , 0.2 mmol of 2,2,6,6-tetramethylpiperidine-*N*-oxyl (TEMPO) and 1.0 mmol alcohol were mixed in 2.5 mL of  $\text{CH}_3\text{CN}$ . The air in the catalytic reaction system was evacuated and oxygen gas was supplied through an  $\text{O}_2$  balloon. After each catalytic cycle, the solution was magnetically separated and the filtered liquid solution was analysed *via* gas chromatography-mass spectrometry using nitrobenzene as the internal standard.

### 2.6 General procedure for the oxidation of hydrocarbon compounds

In general, a mixture of 2 mol%  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  core-shell catalyst (mole percent was based on iron), 1.0 mmol of diphenylmethane, *tert*-butyl hydroperoxide (TBHP, 5.0–6.0 M in decane, 545.0  $\mu\text{L}$ , 3.0 mmol) and 1.0 mL acetonitrile was mixed in a 25 mL single-necked flask fitted with a reflux condenser. The mixture was heated at  $80^\circ\text{C}$  for 24 h under air atmosphere in an oil bath. After each catalytic cycle, the solution was magnetically separated and the filtered liquid solution was analysed *via* gas chromatography-mass spectrometry using nitrobenzene as the internal standard.



## 2.7 Leaching test

The  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  core-shell catalyst was magnetically separated after 4 h reaction time, the conversion of benzyl alcohol and selectivity of benzaldehyde was tested by GC/MS using nitrobenzene as the internal standard. The mixture was further stirred for an additional 8 hours. After the reaction, products were again analysed by GC/MS using nitrobenzene as the internal standard.

## 3. Results and discussion

The  $\text{Fe}_3\text{O}_4$  microspheres modified with PAA were synthesized by a solvothermal method reported in literature.<sup>25</sup> These microspheres were composed of tiny  $\text{Fe}_3\text{O}_4$  nanocrystals within 10 nm

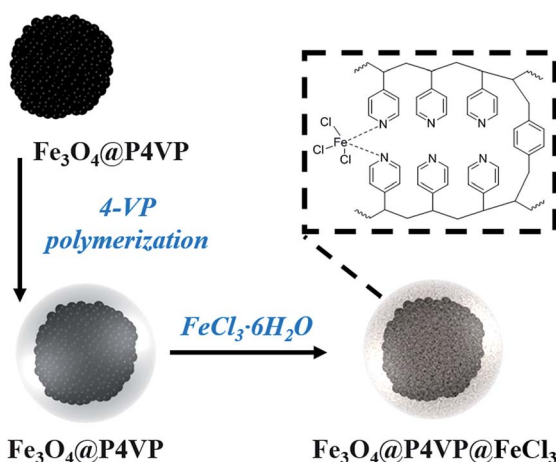


Fig. 1 Schematic illustration of the synthesis of  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$ .

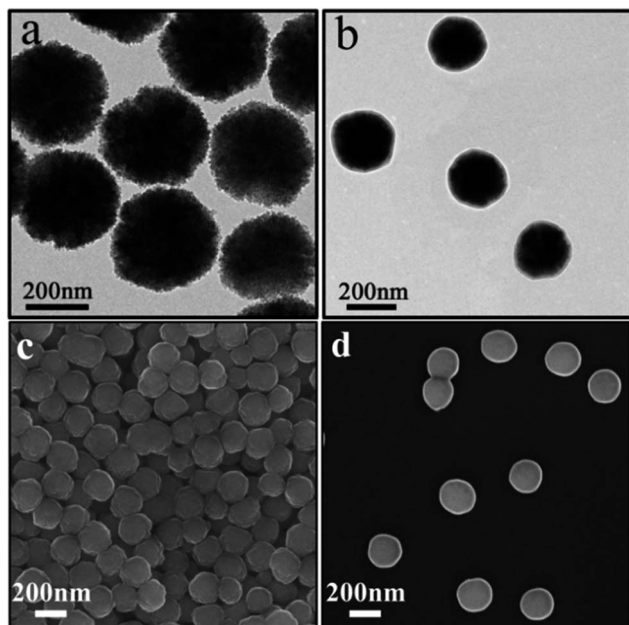


Fig. 2 TEM images of (a)  $\text{Fe}_3\text{O}_4$ , (b)  $\text{Fe}_3\text{O}_4@\text{P4VP}$ ; SEM images of (c)  $\text{Fe}_3\text{O}_4$ , (d)  $\text{Fe}_3\text{O}_4@\text{P4VP}$ .

(Fig. 2a). The P4VP shell was successfully grafted on  $\text{Fe}_3\text{O}_4$  to form core-shell composite microspheres held together by hydrogen bonds between carboxylic groups of PAA chains and pyridine. The diameters of the magnetic core and polymer shell were about 200 and 38 nm, respectively (Fig. 2b). Furthermore, the SEM images show that  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{P4VP}$  microspheres are monodispersed with a narrow size distribution of about 200 nm and 280 nm, respectively (Fig. 2c and d).

$\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  core-shell catalysts were successfully prepared taking advantage of the multi-dentate coordination between  $\text{FeCl}_3$  and poly(4-vinylpyridine) (Fig. 1). Several nitrogen sites on poly(4-vinylpyridine) ensures the stability of  $\text{Fe}^{3+}$  ions on the surface of the core-shell structure. The EDX elemental maps further provides the firm evidence of the synthesis of  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  (Fig. 3).  $\text{Fe}_3\text{O}_4$  nanoparticles were encapsulated into polymer shells, and the iron(III) was well grafted on the surface of  $\text{Fe}_3\text{O}_4@\text{P4VP}$ . The iron elemental maps of the  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  also demonstrated an excellent distribution of iron content on the surface. The existence of iron content in the  $\text{Fe}_3\text{O}_4$  core structure was also observed, as shown in Fig. 3.

Wide-angle p-XRD spectra of  $\text{Fe}_3\text{O}_4$  nanoparticles,  $\text{Fe}_3\text{O}_4@\text{P4VP}$  core/shell nanospheres, and  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  core-shell structure were collected and shown in Fig. 4. The diffraction peaks of  $\text{Fe}_3\text{O}_4$  (Fig. 4a) agree with standard JCPDS 75-1609.39 indicating a face-centered cubic lattice. After coating with P4VP, the peaks of the core-shell  $\text{Fe}_3\text{O}_4@\text{P4VP}$  microspheres are highly similar as those for  $\text{Fe}_3\text{O}_4$  due to the low-

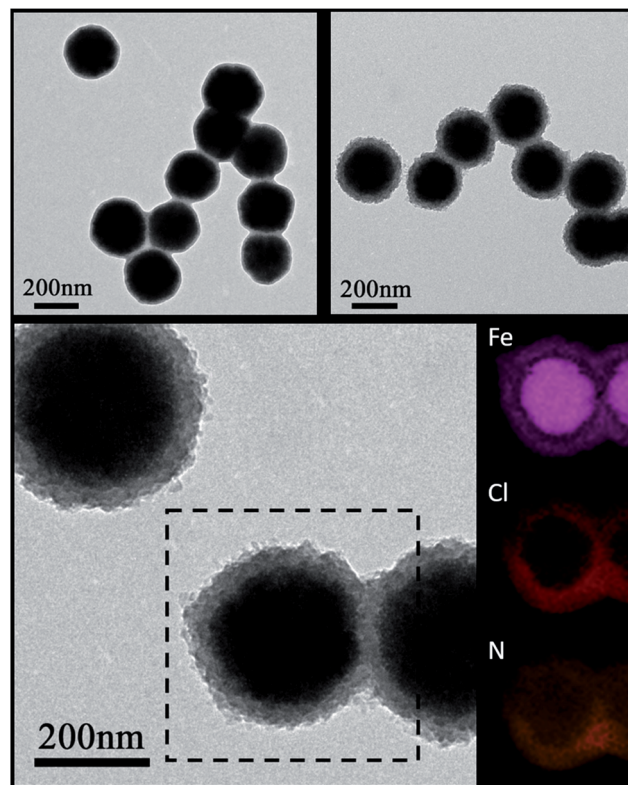


Fig. 3 HRTEM images of the  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  and EDX elemental maps of Fe, Cl and N, respectively.





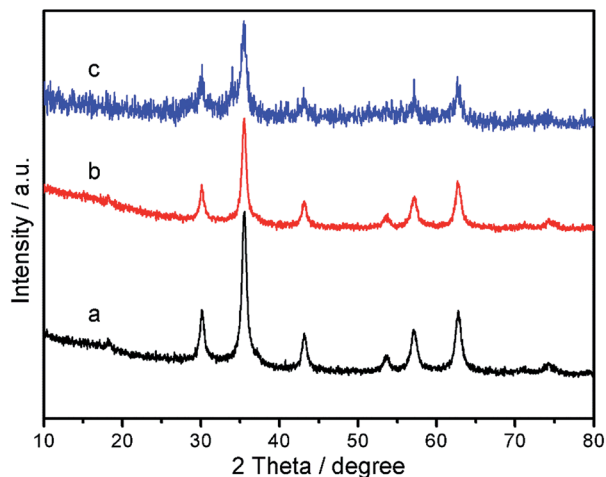


Fig. 4 PXRD patterns of (a)  $\text{Fe}_3\text{O}_4$ , (b)  $\text{Fe}_3\text{O}_4@\text{P4VP}$  and (c)  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$ .

crystalline nature of the polymeric shell (Fig. 4b). As expected, the introduction of the  $\text{FeCl}_3$  to the  $\text{Fe}_3\text{O}_4@\text{P4VP}$  nanostructure did not affect the crystalline structures of  $\text{Fe}_3\text{O}_4@\text{P4VP}$  significantly. The high chemical stability of  $\text{Fe}_3\text{O}_4$  and P4VP ensures the structure integration in presence of acidic  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ .

The FTIR spectrum of the product is shown in Fig. 5. The relatively high intensity of the band at  $592\text{ cm}^{-1}$  is characteristic of the Fe–O vibrations. The characteristic absorption of the band at  $1707$  and  $1165\text{ cm}^{-1}$  corresponds to the C=O stretching of the carboxylic acid group and in-plane deformation of C–O–H stretching, which proves that –COOH functional groups are located on the surface of  $\text{Fe}_3\text{O}_4$  nanoparticles (Fig. 5a). In the FTIR spectrum of  $\text{Fe}_3\text{O}_4@\text{P4VP}$  microspheres, the characteristic absorptions at  $1603$ ,  $1562$ , and  $1417\text{ cm}^{-1}$  are attributed to the vibration of the pyridine ring. The band at  $1603\text{ cm}^{-1}$  corresponds to the stretching vibration absorption of the C–N bond, and the bands at around  $1562$  and  $1417\text{ cm}^{-1}$  are attributed to

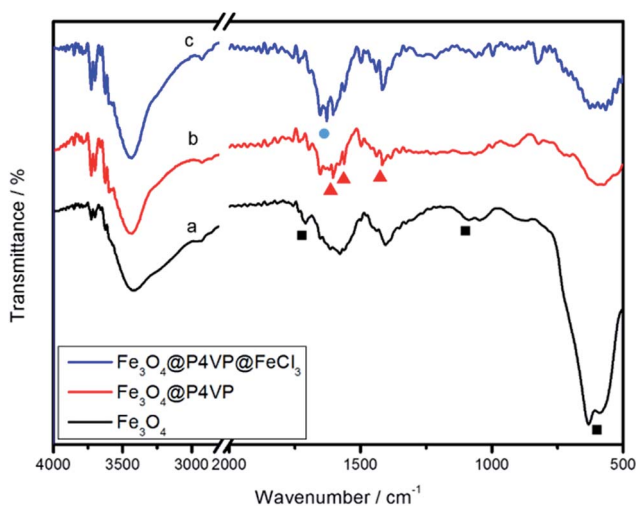


Fig. 5 FTIR spectra of (a)  $\text{Fe}_3\text{O}_4$ , (b)  $\text{Fe}_3\text{O}_4@\text{P4VP}$  and (c)  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$ .

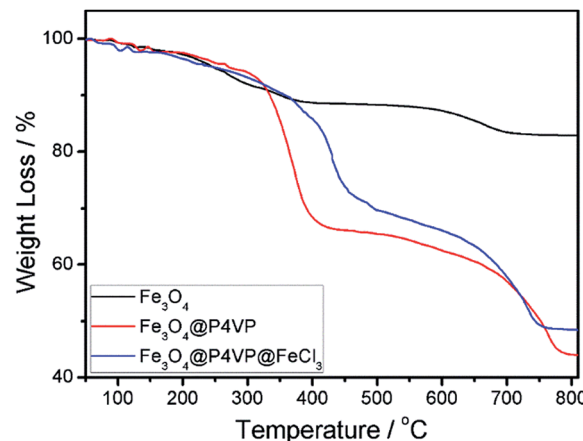


Fig. 6 TGA of (a)  $\text{Fe}_3\text{O}_4$ , (b)  $\text{Fe}_3\text{O}_4@\text{P4VP}$  and (c)  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$ .

the stretching vibration absorption of the C=C bond, which further prove the encapsulation of P4VP on the surface of the  $\text{Fe}_3\text{O}_4$  particles (Fig. 5b). Furthermore, a new peak was observed at  $1627\text{ cm}^{-1}$  after the introduction of the  $\text{FeCl}_3$  moiety, which shows chemical interaction between the iron and the polymer (Fig. 5c).

The thermal stability of the  $\text{Fe}_3\text{O}_4$ ,  $\text{Fe}_3\text{O}_4@\text{P4VP}$  and  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  nanostructures was also examined by TGA in the temperature range of  $50\text{--}800\text{ }^\circ\text{C}$  (Fig. 6). The mass loss of  $\text{Fe}_3\text{O}_4$  was due to the decomposition of organic PAA layer on the surface of  $\text{Fe}_3\text{O}_4$  microspheres (Fig. 6a).  $\text{Fe}_3\text{O}_4@\text{P4VP}$  microspheres show two steps of mass loss. The first one, from room temperature to  $440\text{ }^\circ\text{C}$ , is related to the desorption of adsorbed water and the degradation of secondary nucleation polymer chains on the surface of microsphere. The second loss, from  $440$  to  $800\text{ }^\circ\text{C}$ , is instead correlated to the polymer shell and the PAA modification on the  $\text{Fe}_3\text{O}_4$  (Fig. 6b). For the  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  catalyst, the main decomposition stage was similar to  $\text{Fe}_3\text{O}_4@\text{P4VP}$  microspheres. The results demonstrated that the

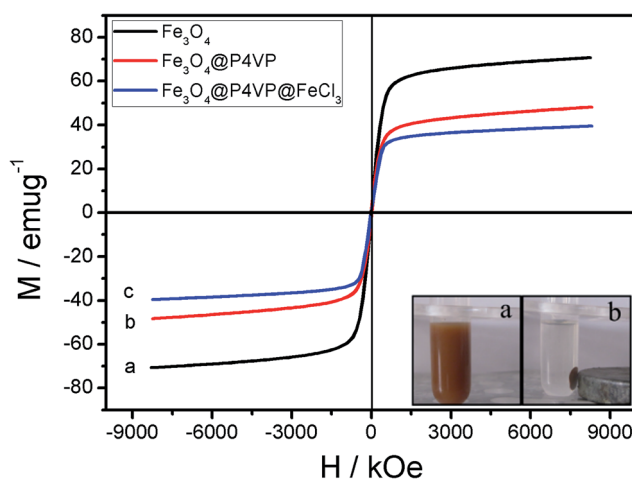


Fig. 7 Room-temperature magnetic hysteresis loops of (a)  $\text{Fe}_3\text{O}_4$ , (b)  $\text{Fe}_3\text{O}_4@\text{P4VP}$  and (c)  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$ . Photos of the insets depict magnetic recycling of  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  catalyst.



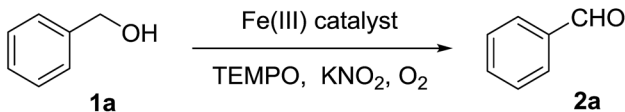
$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  catalyst is thermally stable under the conditions of the aerobic oxidation reaction.

The magnetic performance of the  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  core-shell nanostructure was investigated by SQUID at room temperature. The magnetization curves of synthesized samples are shown in Fig. 7. The magnetization curves of composite nanospheres exhibit no remanence at room temperature. Again, the results indicate their superparamagnetism, which is crucial for controllable flocculation and dispersion in solution by an external magnetic field. A saturation magnetization value of the  $\text{Fe}_3\text{O}_4@\text{P4VP}$  nanospheres of  $47.2 \text{ emu g}^{-1}$  ensures its rapid recoverability as catalyst support under an external magnetic field. The value is lower than that of  $\text{Fe}_3\text{O}_4$  nanoparticles ( $70.8 \text{ emu g}^{-1}$ ) due to the capsulation of magnetic components into the P4VP. In addition,  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  catalyst could be easily recovered by an external magnetic field as shown in Fig. 7; its saturation magnetization value is  $39.8 \text{ emu g}^{-1}$ .

The high resolution XPS spectra is obtained and the results are shown in Fig. 8, which shows the XPS spectra of the  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  core-shell structure. The strong peaks in the  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  signal are attributed to the N 1s and C 1s binding energies, respectively. The binding energies at 711 and 55 eV belong to the Fe 3p and Fe 2p<sub>2/3</sub>, respectively. The peaks at 268 and 198 eV are due to the existence of Cl 2p and Cl 2s binding, respectively. The results strongly indicate the existence of iron(III) moieties on the surface of the  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  catalyst.

The catalytic activity of the synthesized  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  toward the aerobic oxidation reaction was evaluated employing alcohol substrates and using TEMPO as the radical initiator. The control experiment showed that no benzaldehyde was detected in absence of catalyst (Table 1, entry 1). Also, the employment of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{P4VP}$  as catalysts failed to oxidize any benzyl alcohol to its corresponding aldehyde (Table 1, entries 2 and 3). Homogeneous iron catalysts were evaluated and almost quantitative conversion was observed. However, slightly lowered selectivity was observed due to overoxidation to benzoic acid (Table 1, entries 4–5). The amount of  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  added in this

Table 1 Reaction condition optimization using benzyl alcohol<sup>a</sup>

					
Entry	Catalyst	Solvent	Additive	Selec. <sup>b</sup>	Yield <sup>b</sup>
1	—	$\text{CH}_3\text{CN}$	—	—	<5%
2	$\text{Fe}_3\text{O}_4$	$\text{CH}_3\text{CN}$	$\text{KNO}_2$	—	<5%
3	$\text{Fe}_3\text{O}_4@\text{P4VP}$	$\text{CH}_3\text{CN}$	$\text{KNO}_2$	—	<5%
4	$\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$	$\text{CH}_3\text{CN}$	$\text{KNO}_2$	91%	99%
5	$\text{Fe}(\text{NO}_3)_3$	$\text{CH}_3\text{CN}$	$\text{KNO}_2$	78%	99%
6	$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$	$\text{CH}_3\text{CN}$	$\text{KNO}_2$	99%	99%
7	$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$	$\text{CH}_3\text{CN}$	$\text{NaHCO}_3$	99%	76%
8	$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$	$\text{CH}_3\text{CN}$	$\text{Na}_2\text{CO}_3$	99%	68%
9	$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$	$\text{CH}_3\text{CN}$	Pyridine	99%	43%
10	$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$	$\text{PhCH}_3$	$\text{KNO}_2$	95%	71%
11	$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$	THF	$\text{KNO}_2$	99%	55%
12	$\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$	EtOH	$\text{KNO}_2$	99%	21%

<sup>a</sup> Reaction conditions: 1.0 mmol of benzyl alcohol, 2 mol% of iron catalyst, 5.0 mL of solvent, 0.2 mmol of TEMPO and 0.2 mmol of additive; 60 °C, 12 h under 1 atm  $\text{O}_2$ . <sup>b</sup> Selectivities and yields were calculated by GC-MS using nitrobenzene as the internal standard.

reaction was 2 mol%, based on the same iron loading; quantitative yields were achieved using  $\text{KNO}_2$  additive (Table 1, entry 6). Several additives were tested under the same reaction conditions and  $\text{KNO}_2$  was the most optimal one. Basic inorganic additives were tested and only low to medium yields were achieved (Table 1, entries 7–8). A basic organic additive was evaluated but a poor yield was observed (Table 1, entry 9). Further solvent screening showed that  $\text{CH}_3\text{CN}$  is the most suitable solvent for the aerobic oxidation of benzyl alcohol in the presence of  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  (Table 1, entries 6, 10–12). Aromatic solvents such as toluene gave lower yields (Table 1, entry 10). Moreover, oxygen containing solvents, such as THF and ethanol, provided much lower yield, presumably due to their ability to excessively coordinate the metal (Table 1, entries 11 and 12).

With the optimal reaction conditions in hand, a variety of alcohol substrates were tested using  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  core-shell catalyst. Benzyl alcohol was transformed to the corresponding benzaldehyde in 99% yield after 12 h (Table 2, entry 1). For the aerobic oxidation of benzyl alcohol in presence of  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$  as the catalyst, the turnover number (TON) was calculated to be 50. *p*-Methyl benzyl alcohol and *p*-methoxy benzyl alcohol were reactive as electron-rich benzyl alcohols under the optimal reaction conditions, affording 99% and 95% yield, respectively (Table 2, entries 2 and 3). Alcohol substrates bearing electron-withdrawing functional groups, such as *p*-fluorobenzyl alcohol, were also tolerated. A slightly lowered yield was observed due to the reduction in electron efficiency (Table 2, entry 4). The heterocyclic alcohol pyridin-2-ylmethanol was selectively converted to its corresponding aldehyde, in the presence of the Fe derived core-shell catalyst (Table 2, entry 5). Moreover, cinnamaldehyde was obtained in good yield starting from the corresponding allylic alcohol (Table 2, entry 6). The

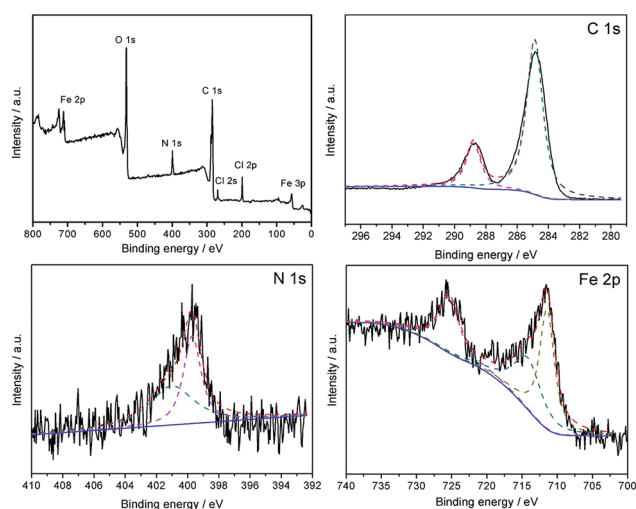
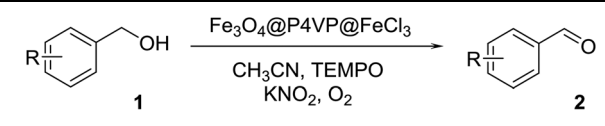


Fig. 8 XPS Spectra of  $\text{Fe}_3\text{O}_4@\text{P4VP}@ \text{FeCl}_3$ .



Table 2 Aerobic oxidation of a variety of alcohols<sup>a</sup>

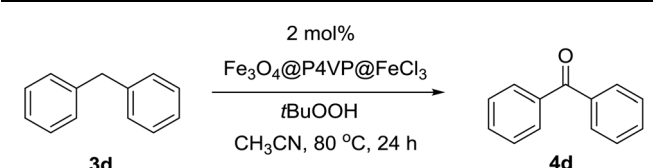
				
Entry	Alcohol	Product	Sel.	Yield
1			99%	99%
2			99%	99%
3			99%	95%
4			81%	80%
5			99%	99%
6			95%	94%
7			51%	50%
8			24%	22%

<sup>a</sup> Reaction conditions: 1.0 mmol of benzyl alcohol, 2 mol% of  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst, 5.0 mL of  $\text{CH}_3\text{CN}$ , 0.2 mmol of TEMPO and 0.2 mmol of additive; 60 °C, 12 h under 1 atm  $\text{O}_2$ .

transformation of secondary alcohols to ketones is also highly important in synthetic chemistry; 1-phenylethanol and cyclohexanol were both tested as secondary alcohols (Table 2, entries 7 and 8). Unfortunately, only 50% and 22% of acetophenone and cyclohexanone respectively were obtained.

The oxidation of diphenylmethane **3a** for the generation of benzophenone **4a** was carried out in 2.0 mL acetonitrile at 80 °C for 24 h (Table 3). The activation of C–H bond is difficult and *tert*-butyl hydroperoxide (TBHP) was employed as the oxidant under extended reaction time. The catalytic system has been re-optimized to adapt the benzylic oxidation reaction of hydrocarbon derivatives. In the absence of any additive,  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  and  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  failed to promote any conversion (Table 3, entries 1 and 3). The employment of basic pyridine additive strongly increased the yield of the desired benzophenone product (Table 3, entries 2 and 4). Initially, 91% conversion and 99% selectivity were obtained for  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst

Table 3 Benzylic oxidation in presence of different additives<sup>a</sup>

				
Entry	Catalyst	Additive	Selec.	Yield <sup>b</sup>
1	$\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$	None	—	<5%
2	$\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$	Pyridine	99%	91%
3	$\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$	None	—	<5%
4	$\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$	Pyridine	99%	75%
5	$\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$	None	99%	84%
6	$\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$	Pyridine	99%	99%
7 <sup>c</sup>	$\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$	Pyridine	99%	99%
8	$\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$	$\text{Et}_3\text{N}$	99%	85%
9	$\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$	HMTA	99%	87%

<sup>a</sup> Reaction conditions: 1.0 mmol **3d**, 2.0 mol%  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst, 5 mmol TBHP, 2.0 mL acetonitrile, 80 °C for 24 h. <sup>b</sup> Isolated yield. <sup>c</sup> 2 mol% pyridine.

in the absence of additive (Table 1, entry 5). The high efficiency of  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst was due to the pyridine sites on the surface of the heterogeneous iron catalyst. The addition of a small amount of homogeneous pyridine can further boost the conversion to over 99% (Table 1, entry 6). Furthermore, the amount of pyridine can be reduced to 2 mol% without affecting the yield and selectivity of the diphenylmethane oxidation (Table 1, entry 7). In addition, other basic additives were examined. However, almost no improvement was observed when triethylamine ( $\text{Et}_3\text{N}$ ) was employed (Table 3, entry 8). Hexamethylenetetramine (HMTA) failed to increase the yield as well (Table 3, entry 9). These results indicate that pyridine was the best base additive among the organic bases screened. Our  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst was designed so that the heterogeneous P4VP layer would provide large amounts of pyridine sites. These heterogeneous pyridine sites were highly helpful for the oxidation reaction process, while homogeneous  $\text{FeCl}_3$  failed to convert diphenylmethane to the desired product. Several organic solvents were screened and acetonitrile demonstrated good compatibility in the catalytic system, which resulted in 99% isolated yield (Table 3, entry 2). Other solvents showed a trend similar to the results in Table 1. Therefore the optimal catalytic system was set to be 2.0 mol%  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst, 0.02 equivalent of pyridine additive and 3.0 equivalents of TBHP in acetonitrile solvent.

The optimized reaction conditions were utilized for the oxidation of other substrates in the presence of *t*BuOOH (Table 4). C–H activation/oxidation was further extended to other hydrocarbon compounds. Ethylbenzene **3a** was oxidized to 1-phenylethanone **4a** in 91% conversion and 97% selectivity (Table 4, compound **4a**). Ethylthiophene **3b** containing a heterocyclic moiety was also employed as the substrate and over 96% yield and up to 99% selectivity were achieved (Table 3,



Table 4 Benzylic oxidation of hydrocarbon derivatives

$\text{R}'\text{-C}_6\text{H}_4\text{-CH}_2\text{-R} \xrightarrow[\text{CH}_3\text{CN}, 80^\circ\text{C}, 24\text{ h}]{\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3, \text{tBuOOH, pyridine}} \text{R}'\text{-C}_6\text{H}_4\text{-C(=O)-R}$		
<b>3</b>		<b>4</b>
<b>4a</b>	<b>4b</b>	<b>4c</b>
91% yield 97% selectivity	96% yield 99% selectivity	99% yield 99% selectivity
<b>4d</b>	<b>4f</b>	<b>4g</b>
99% yield 99% selectivity	99% yield 99% selectivity	99% yield 99% selectivity

compound **4b**). Isochromane **3c** underwent oxidation to give 4-isochromanone **4c** in high yield (Table 4, compound **4c**). The oxidation of diphenylmethane **3d** and bis(4-fluorophenyl) methanone **3f** for the generation of corresponding ketones **4d** and **4f** were smooth (Table 4, compounds **4d** and **4f**). Moreover, by oxidation of 9H-fluorene **3g**, the reaction proceeded smoothly to form the corresponding ketones in high yield and selectivity (Table 4, compound **4g**). In summary, the  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  was a versatile catalyst for benzylic methylene compounds (Table 4).

The recyclability of the catalyst was studied under the optimized conditions and utilizing 2 mol% and 0.5 mol% of  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst in acetonitrile (Fig. 9). The same batch of the  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst was reused for five catalytic cycles. Conversion and selectivity were retained at 99% and the yield of benzaldehyde was compromised only slightly

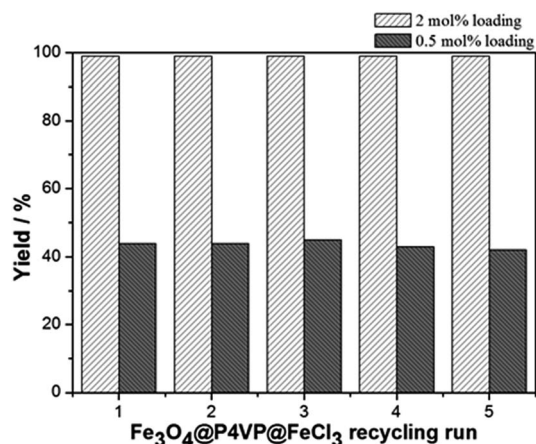


Fig. 9 Core-shell iron catalyst recyclability test at 2 mol% and 0.5 mol% catalyst loading for aerobic oxidation of benzyl alcohol.

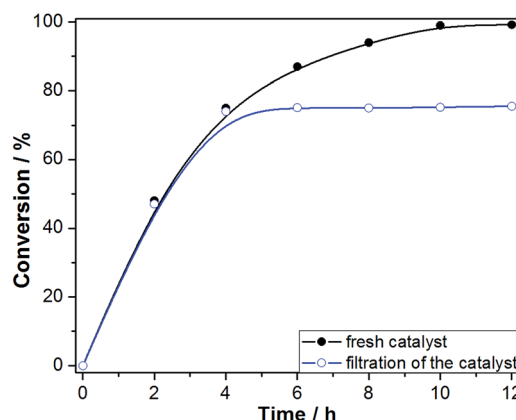
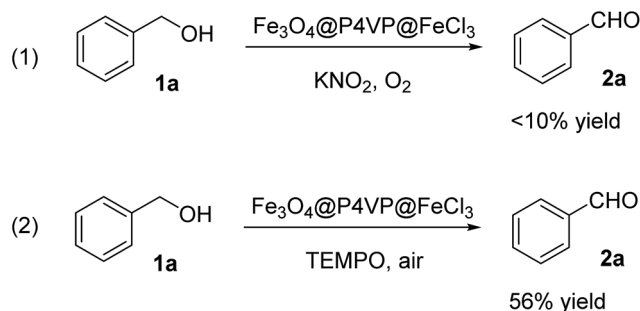


Fig. 10 Hot filtration test of  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  in aerobic oxidation of benzyl alcohol.

after five cycles (Fig. 9). At a lower catalyst loading of 0.5 mol%, 44% yield was achieved in the initial cycle. Only slight yield decrease (98%) was observed after 5 cycles of reaction (Fig. 9). The ability to retain conversion rates and selectivities after five cycles indicates that the core-shell heterogeneous catalyst is highly stable. TEM and p-XRD spectra showed no significant difference between fresh  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  and five-time reused samples (Fig. S1 and S2†).

The hot filtration test was conducted to confirm the heterogeneous nature of the catalytic aerobic oxidation and low reaction leaching (Fig. 10). The  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst was isolated using an external magnet after 4 hours of reaction and the mixture was stirred for another 8 h. Conversion of benzyl alcohol stopped after the catalyst was removed at 4 h reaction time. This result indicates that the multi-dentate  $\text{Fe}\cdots\text{N}$  bonds ensure the stability of the  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  catalyst during the liquid oxidation process. Furthermore, the reaction solution after solid catalyst removal was tested by ICP-AES, which suggested 2.3 ppm of iron content. These results demonstrated the high stability of  $\text{Fe}_3\text{O}_4\text{@P4VP@FeCl}_3$  core-shell catalyst during the oxidation reaction condition.

Several control experiments were designed and conducted in order to reveal the reaction mechanism. First of all, the oxidation reaction was carried out without TEMPO (Scheme 1, reaction 1). In the absence of radical initiator, reaction was not able to proceed. This observation suggested radical reaction



Scheme 1 Controlled experimental reaction.



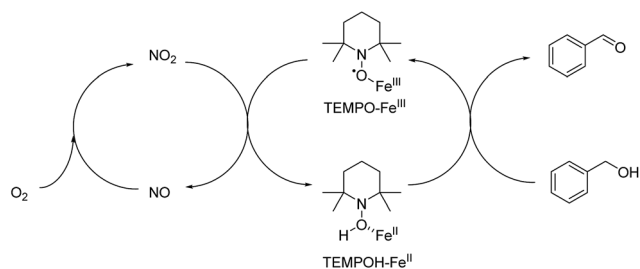


Fig. 11 Reaction mechanism of Fe(III) promoted oxidation.

pathway. Furthermore, reaction was performed under open air condition, decent yield of the desired aldehyde product was obtained (Scheme 1, reaction 2). Oxygen was crucial in the oxidation process and the certain density of oxygen ensures the high conversion of the alcohol product.

A overall mechanism of Fe(III) promoted catalytic oxidation can be described as a redox reaction involving two separated cycles in Fig. 11.  $\text{KNO}_2$  was acting as a source of  $\text{NO}_2$ . Therefore, TEMPO is envisioned to carry out the main oxidation reaction of alcohols with the help of Fe(III) that initiates a series of electron and proton transfer steps in the right cycle where TEMPO-Fe(III) is reduced to generate TEMPOH-Fe(II). The overall oxidation process involves the oxidation of Fe(II) to Fe(III) by  $\text{NO}_2$  and the oxidation of TEMPOH to TEMPO by Fe(III). The conversion of NO to  $\text{NO}_2$  was performed in the presence of molecular oxygen.

## 4. Conclusions

In summary, a novel magnetic core-shell  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  structure was designed, prepared and fully characterized. The iron(III) immobilized core-shell microspheres were composed by a magnetic  $\text{Fe}_3\text{O}_4$  core and a P4VP middle layer. Taking advantage of active iron(III) catalytic site, the magnetic composite microspheres were utilized as an efficient catalyst for the selective aerobic oxidation of alcohols. A variety of alcohol substrates were tolerated under our optimized conditions at only 2 mol% catalyst loading. In addition, benzylic oxidation of hydrocarbon compounds was also carried out using the  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  catalyst and  $t\text{BuOOH}$  oxidant. The initial catalytic activity of the  $\text{Fe}_3\text{O}_4@\text{P4VP}@\text{FeCl}_3$  catalyst was retained after at least five consecutive reaction cycles. A hot filtration test suggested low leaching of iron into the solution. Further applications of the various heterogeneous core-shell catalysts are currently under investigation.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This work is supported by Beijing Natural Science Foundation (2172037) and National Natural Science Foundation of China (No. 51503016). P. Y. thanks the State Key Laboratory of Chemical Resource Engineering and Y. L. thanks the

Fundamental Research Funds for the Central Universities (Grant No. FRF-TP-16-004A3) for funding support.

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