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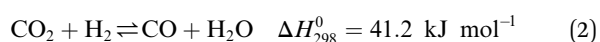
Perovskite La₂(NiCu)O₄ catalyst precursors for dry reforming of methane: effects of Cu-substitution on carbon resistance

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Exploring low-cost catalysts with low carbon deposition and high activity for dry reforming of methane (DRM) is of great importance in both industrial and academic fields. La$_2$(Ni$_{1-x}$Cu$_x$)O$_4$ (x = 0.0–0.4) perovskites were synthesized by a sol–gel self-combustion method and evaluated as catalyst precursors for DRM. The reduced La$_2$(Ni$_{0.8}$Cu$_{0.2}$)O$_4$ shows optimal performance with negligible carbon deposition, and the conversions of CH$_4$ and CO$_2$ are 73% and 80%, respectively. The remarkably improved carbon resistance of the reduced La$_2$(Ni$_{0.8}$Cu$_{0.2}$)O$_4$ is attributed to the small metallic particles obtained from the reduced perovskite and the surface segregation of Cu in the metallic Ni–Cu particles.
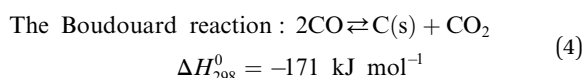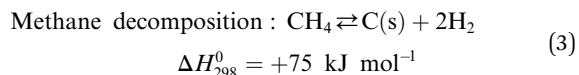
1. Introduction

Dry reforming of methane (DRM) has attracted much attention over the past decades considering its economic and environmental significance. DRM yields syngas with a H$_2$/CO ratio of 1, which is suitable for Fischer–Tropsch synthesis. This reaction consumes two greenhouse gases (CH$_4$ and CO$_2$).[1,2] The main reactions of DRM are[3]

$$CH_4 + CO_2 \rightleftharpoons 2H_2 + 2CO \quad \Delta H_{298}^0 = 247.3 \text{ kJ mol}^{-1} \quad (1)$$

$$CO_2 + H_2 \rightleftharpoons CO + H_2O \quad \Delta H_{298}^0 = 41.2 \text{ kJ mol}^{-1} \quad (2)$$

These reactions need to be operated at high temperatures due to their endothermic nature. The conversion of CO$_2$ is generally higher than that of CH$_4$ and the product ratio of H$_2$/CO is less than 1 due to the reverse water–gas reaction (RWGS, eqn (2)).

The main concern over DRM is its carbon deposition, which originates from two side reactions:[4–6]

$$\text{Methane decomposition}: CH_4 \rightleftharpoons C(s) + 2H_2$$
$$\Delta H_{298}^0 = +75 \text{ kJ mol}^{-1} \quad (3)$$

$$\text{The Boudouard reaction}: 2CO \rightleftharpoons C(s) + CO_2$$
$$\Delta H_{298}^0 = -171 \text{ kJ mol}^{-1} \quad (4)$$

Eqn (3) is favored at higher temperatures and eqn (4) is favored at lower temperatures.

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Catalysts based on noble metals are reported to be highly active towards DRM,[7] but their application is quite limited because of their high cost. Ni-based catalysts are more economical from a commercial viewpoint. However, Ni-based catalysts prepared by a conventional wet-impregnation method have large Ni particles and low resistance to carbon deposition.[8–11] Thus, developing Ni-based catalysts with high catalytic activity and carbon resistance remains an open question. It is reported that the addition of Cu to the impregnated Ni catalysts enhances the catalytic performance for DRM.[12–14] Liu *et al.*[12] reported that NiCu/Al$_2$O$_3$ shows better carbon resistance than Ni/Al$_2$O$_3$ because that Cu inhibits the dissolution of carbon in Ni. Both Chen[13] and Lee[14] reported that adding a proper amount of Cu into Ni enhanced the long-term stability for DRM.

Moreover, it is reported that a highly dispersed Ni catalyst can be prepared by the so-called "solid phase crystallization" method, where Ni is "extracted" from solids with well-defined structures (such as perovskites with Ni at the B-site) after reduction.[15] Using this method, catalysts obtained from LaNiO$_3$ and La$_2$NiO$_4$ precursors have relatively small metal particles, showing enhanced catalytic activity and carbon resistance as compared with the impregnated ones.[9,11] According to Gallego,[11] reduced La$_2$NiO$_4$ shows better catalytic performance than reduced LaNiO$_3$ due to the smaller Ni content. However, carbon deposition cannot be completely eliminated over reduced La$_2$NiO$_4$.[10] The major advantage of perovskites is that they can accommodate different elements at the A-site and/or B-site without changing their lattice structure.[16] Inspired by the improved carbon resistance of the impregnated NiCu catalysts, we substitute Ni with Cu in La$_2$NiO$_4$ to investigate the effects of Cu substitution on the catalytic performance towards DRM.

In this present work, La$_2$(Ni$_{1-x}$Cu$_x$)O$_4$ catalyst precursors were synthesized by glycine sol–gel self-combustion method.

Remarkably improved carbon resistance is observed for the reduced $La_2(Ni_{0.8}Cu_{0.2})O_4$. The effects of Cu substitution on the catalytic activity and carbon resistance for the DRM reactions are discussed.

2. Experimental

2.1. Preparation

$La_2(Ni_{1-x}Cu_x)O_4$ catalyst precursors were prepared by a self-combustion method.[17] The starting materials were La_2O_3, $Ni(NO_3)_2 \cdot 6H_2O$ and $Cu(NO_3)_2 \cdot 3H_2O$, which were purchased from Sinopharm Chemical Agent Company. All the chemicals were of analytical grade and used without any further purification. La_2O_3 was dissolved in distilled water by adding nitrate acid under constant stirring. $Ni(NO_3)_2 \cdot 6H_2O$ and $Cu(NO_3)_2 \cdot 3H_2O$ were added successively and a given amount of glycine ($NO_3^-/NH_2 = 1$) was added to the mixed aqueous solution of metal nitrates. The resulting solution was heated on a heating plate until self-combustion occurred. Then the powder precursors produced through combustion were calcined at 700 °C for 4 h under ambient atmosphere.

$Ni_{0.8}Cu_{0.2}/La_2O_3$ with 18 wt% metal loading, which is the same as that of $La_2(Ni_{0.8}Cu_{0.2})O_4$, was prepared by the wet-impregnation method. Stoichiometric nickel and copper nitrate were dissolved in distilled water. La_2O_3 was added and the water was evaporated at 90 °C under continuous stirring. Then the residue was dried at 120 °C overnight and calcined in air at 550 °C for 2 h.

2.2. Characterization

X-ray diffraction (XRD) analysis was performed by using an X-ray diffractometer (TTR III, Rigaku Co., Japan) with standard CuKα radiation ($\lambda = 1.5406$ Å) in the range of $2\theta = 20–80°$.

Temperature programmed oxidation (TPO) was carried out with a simultaneous thermal analyzer (STA 449 F3, NETZSCH, Germany) to determine the carbon deposition on the used samples and a temperature scheme was designed. Used catalysts of 5–15 mg were first heated to 800 °C and kept for 30 min under N_2 atmosphere to decompose $La_2O_2CO_3$. Then the sample was cooled down to room temperature under N_2 atmosphere and TPO was conducted from 30 to 1000 °C in a gas flow of air.

The temperature-programmed reduction (TPR) was conducted by the same thermal analyzer (STA 449 F3, NETZSCH, Germany). During the test, samples of 10–15 mg were placed in an alumina crucible and heated in 5% H_2/N_2 with a flow rate of 60 ml min⁻¹ and a heating rate of 5 °C min⁻¹ from 30 to 1000 °C.

Scanning electron microscopy (SEM, JSM-6301F, Hitach, Japan) and transmission electron microscopy (TEM, JEM-2011, JEOL, Japan) were employed to observe the microstructures of the samples. To identify the surface elemental composition and chemical status of the catalysts, XPS analyses were performed with monochromated Al Kα radiation using ESCALAB 250 (Thermo-VG Scientific, U.S.).

2.3. Catalytic reaction

Catalytic activity evaluation was conducted in a quartz fixed-bed reactor (i.d. = 6 mm), the catalysts were sieved to a 200–400 mesh size and charged in the reactor. The catalysts (200 mg) were reduced *in situ* in H_2 with a flow rate of 30 ml min⁻¹ at 700 °C for 1 h prior to DRM. DRM was conducted in a stream of $CH_4/CO_2 = 1$ at 750 °C for 5 h under atmospheric pressure. The flow rate of the CH_4/CO_2 stream was 60 ml min⁻¹ (GHSV = 1.8×10^4 ml g⁻¹ h⁻¹). The reaction products were analyzed by a gas chromatography (GC9790, FULI, China). The conversions of CH_4 and CO_2 are defined as:

$$\text{Conv } CH_4 = \frac{[CH_4]_{in} - [CH_4]_{out}}{[CH_4]_{in}} \times 100\%$$

$$\text{Conv } CO_2 = \frac{[CO_2]_{in} - [CO_2]_{out}}{[CO_2]_{in}} \times 100\%$$

where $[CH_4]_{in}$ and $[CO_2]_{in}$ refer to the flow rates of the introduced CH_4 and CO_2, while $[CH_4]_{out}$ and $[CO_2]_{out}$ refer to the flow rates of CH_4 and CO_2 in the tail gas.

3. Results

3.1. Catalytic performance and carbon deposition

Fig. 1(a)–(c) show the CH_4, CO_2 conversions and H_2/CO ratio as a function of reaction time during the DRM reactions over the reduced $La_2(Ni_{1-x}Cu_x)O_4$ with different x values. According to
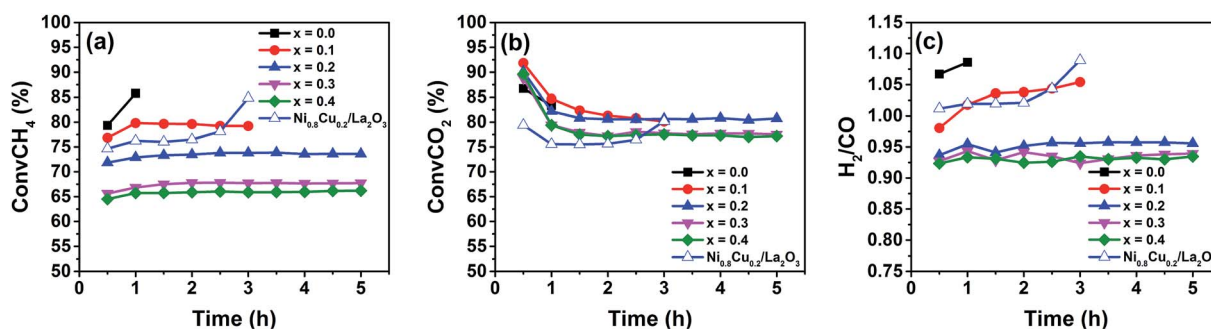

Fig. 1 Catalytic performance for the DRM reaction over the reduced $La_2(Ni_{1-x}Cu_x)O_4$ and the impregnated $Ni_{0.8}Cu_{0.2}/La_2O_3$ at 750 °C: (a) CH_4 conversion, (b) CO_2 conversion, and (c) H_2/CO ratio as a function of reaction time.
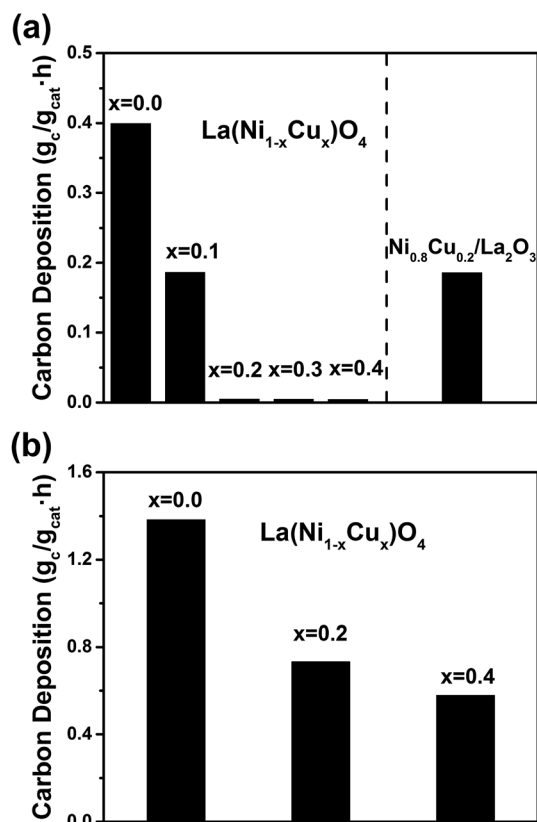
Fig. 2 Carbon deposition rates measured by TPO for (a) the DRM reaction, (b) the CH_4 decomposition reaction.

Fig. 1(a), samples with $x = 0.0$ and 0.1 show high initial CH_4 conversions but the reactions cannot proceed beyond 1 and 3 h due to the reactor blocking. When x increases to 0.2, the CH_4 conversion is stable at approximately 73% and no reactor blocking occurs during 5 h's test. Further increasing x to 0.3 and 0.4 reduces the CH_4 conversions. Fig. 1(b) shows that for the $x = 0.2–0.4$ samples, the CO_2 conversions are higher than those of CH_4; while for the $x = 0.0$ and 0.1 samples, the CO_2 conversions are lower than those of CH_4. The H_2/CO ratios for the samples with $x = 0.0$ and 0.1 are larger than unity (Fig. 1(c)), indicating that methane decomposition (eqn (3)) is predominant in side reactions. Thus, carbon deposition should be responsible for the reactor blocking. While for the samples with $x = 0.2–0.4$, the H_2/CO ratios smaller than unity indicate the predominant occurrence of RGWS reaction in the side reactions. For comparison purpose, the CH_4, CO_2 conversions and H_2/CO ratio of the impregnated $Ni_{0.8}Cu_{0.2}/La_2O_3$ are also shown in Fig. 1. It is seen that the reactor is partially blocked after 2 h and the H_2/CO ratio is larger than unity. The partial blockage raises the reactor pressure and impedes the passage of the reactants, leading to the abnormal increase in the conversions.

The carbon deposition rates for DRM were measured by TPO and shown in Fig. 2(a). The $x = 0.0$ sample suffers severe carbon deposition ($0.4\ g_c\ g_{cat}^{-1}\ h^{-1}$), while the carbon deposition rate of the $x = 0.1$ sample is approximately half of that of the $x = 0.0$ sample. When x increases to 0.2–0.4, the carbon deposition is trivial, indicating the addition of Cu remarkably improves the carbon resistance of the reduced $La_2(Ni_{1-x}Cu_x)O_4$. Although the
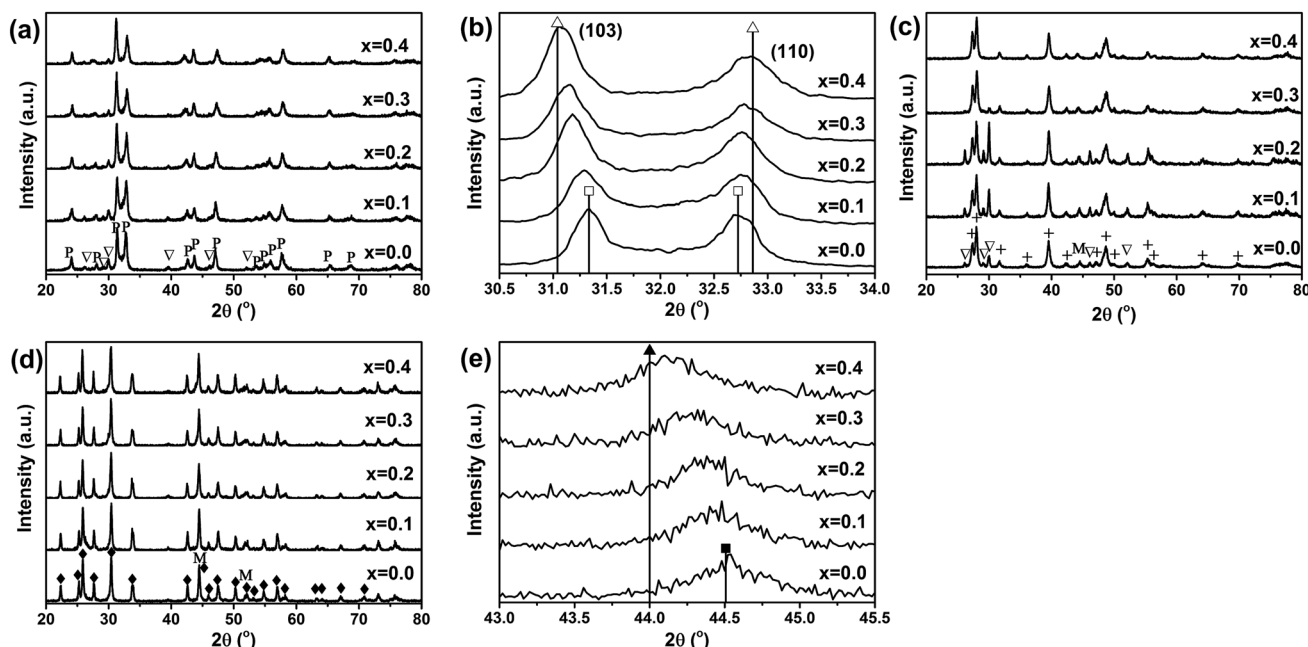

Fig. 3 (a) XRD patterns of fresh $La_2(Ni_{1-x}Cu_x)O_4$, (b) magnified (103) and (110) peaks of the perovskite $La_2(Ni_{1-x}Cu_x)O_4$ phase, (c) XRD patterns of as-reduced $La_2(Ni_{1-x}Cu_x)O_4$, (d) XRD patterns of used $La_2(Ni_{1-x}Cu_x)O_4$, and (e) magnified Ni (111) peaks of the as-reduced $La_2(Ni_{1-x}Cu_x)O_4$ (P – perovskite phase referring to JCPDS 76-0055, ▽ – La_2O_3 referring to JCPDS 73-2141, + – $La(OH)_3$ referring to JCPDS 36-1481, M – the Ni phase referring to JCPDS 04-0850, ◆ – $La_2O_2CO_3$ referring to JCPDS 84-1963, □ – standard La_2NiO_4 peak position from JCPDS 76-0055, △ – standard $La_2Ni_{0.5}Cu_{0.5}O_4$ peak position from JCPDS 80-1075, ■ – standard Ni peak position from JCPDS 04-0850 and ▲ – standard NiCu peak position from JCPDS 65-7246).

Table 1 The lattice parameters of the tetragonal $La_2(Ni_{1-x}Cu_x)O_4$ unit cell

	Unit cell parameter (Å)	
	$a = b$	c
$x = 0.0$	3.869	12.716
$x = 0.1$	3.863	12.742
$x = 0.2$	3.858	12.803
$x = 0.3$	3.852	12.936
$x = 0.4$	3.849	12.955
La_2NiO_4 [a]	3.868	12.697
$La_2Ni_{0.5}Cu_{0.5}O_4$ [b]	3.851	13.001

[a] Cell parameters of La_2NiO_4 (JCPDS 76-0055). [b] Cell parameters of $La_2Ni_{0.5}Cu_{0.5}O_4$ (JCPDS 80-1075).
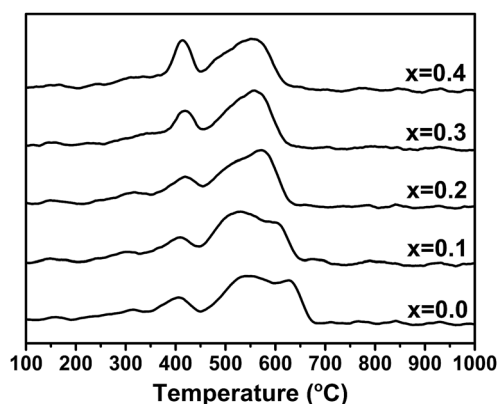
Fig. 4 TPR profiles of the fresh $La_2(Ni_{1-x}Cu_x)O_4$.

impregnated $Ni_{0.8}Cu_{0.2}/La_2O_3$ has the same metal loading and Ni : Cu ratio as the reduced $La_2(Ni_{0.8}Cu_{0.2})O_4$, it shows very severe carbon deposition. To further test the carbon resistance of the reduced perovskites, the decomposition of pure CH_4 (eqn (3)) was conducted on the $x = 0.0$, 0.2 and 0.4 samples. The reaction was performed in a fixed-bed reactor under identical conditions to DRM. Complete deactivation due to carbon deposition occurs at 25, 60 and 75 min for the $x = 0.0$, 0.2 and 0.4 samples, respectively. Fig. 2(b) shows the carbon deposition

rates of the CH_4 decomposition reaction measured by TPO. It is seen that the addition of Cu reduces the carbon deposition rate significantly even for the decomposition of pure CH_4. Thus, we conclude that the $La_2(Ni_{0.8}Cu_{0.2})O_4$ perovskite is a better catalyst precursor for DRM, which shows high carbon resistance with stable and high catalytic activity.

3.2. XRD analysis of the fresh, as-reduced and used catalysts

Fig. 3(a) shows the XRD diffraction patterns of fresh La_2-$(Ni_{1-x}Cu_x)O_4$ catalysts with different x values. All the fresh catalysts consist of a dominant amount of tetragonal $La_2(NiCu)O_4$ and a small amount of La_2O_3. The lattice parameters of the tetragonal $La_2(Ni_{1-x}Cu_x)O_4$ unit cell determined from the XRD patterns are listed in Table 1. To further confirm the incorporation of Cu in the perovskite lattice and the formation of $La_2(Ni_{1-x}Cu_x)O_4$, the (103) and (110) XRD peaks of the perovskite phase are magnified and shown in Fig. 3(b). The standard XRD peak positions of La_2NiO_4 ((JCPDS 76-0055)) and $La_2Ni_{0.5}Cu_{0.5}O_4$ (JCPDS 80-1075) are shown in Fig. 3(b) for reference purpose. The (103) peak shifts to lower angles while the (110) peak shifts to higher angles with the increase of x. This shift is due to the change in the lattice parameters of the tetragonal $La_2(Ni_{1-x}Cu_x)O_4$ unit cell, which is in agreement with the previous report.[18] It is seen that as x increases from 0.0 to 0.4, both the lattice parameters and the peak positions of the $La_2(Ni_{1-x}Cu_x)O_4$ perovskite phase approach to those of the $La_2Ni_{0.5}Cu_{0.5}O_4$ (JCPDS 80-1075), indicating Cu has been incorporated into the B-site of the perovskite. Fig. 3(c) shows the XRD diffraction patterns of the as-reduced $La_2(Ni_{1-x}Cu_x)O_4$ catalysts, which are reduced by H_2 at 700 °C for 1 h. All the perovskites decompose completely after the reduction. Metallic Ni phase, together with La_2O_3 and $La(OH)_3$, is identified in the XRD patterns of the as-reduced catalysts. The formation of $La(OH)_3$ may be due to the reaction between La_2O_3 and moisture. Fig. 3(d) shows the XRD patterns of the used catalysts. After DRM, La_2O_3 and $La(OH)_3$ turn into $La_2O_2CO_3$ due to the reaction between La_2O_3 and CO_2. According to Gallego et al.,[9,11,19] the La_2O_3 support also participates in DRM by reacting with CO_2 to form $La_2O_2CO_3$, and $La_2O_2CO_3$ may react with the surface carbon species formed on the Ni particles to produce CO. Fig. 3(e) shows
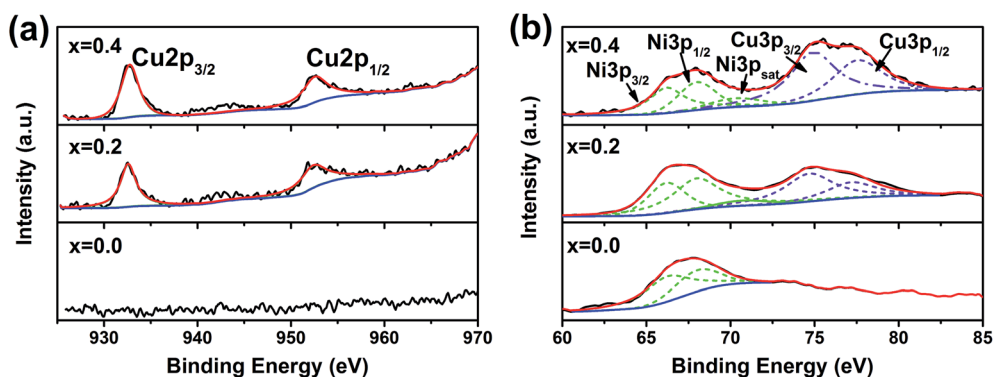
Fig. 5 XPS profiles of the used $La_2(Ni_{1-x}Cu_x)O_4$ with $x = 0.0$, 0.2 and 0.4: (a) Cu2p, (b) Ni3p and Cu3p.

Table 2 Surface composition of the Ni–Cu particles determined by XPS for the used $La_2(Ni_{1-x}Cu_x)O_4$ with x = 0.0, 0.2 and 0.4

x in $La_2(Ni_{1-x}Cu_x)O_4$ (stoichiometry)	x in $Ni_{1-x}Cu_x$ (by XPS)
0.0	0.0000
0.2	0.4554
0.4	0.6486

the magnified XRD peaks of Ni (111) of the as-reduced catalysts with different x values. The Ni (111) peak shifts to lower angles and the lattice parameter decreases from 3.5235 to 3.5553 Å when x increases from 0.0 to 0.4. Thus, the formation of Ni–Cu alloy is confirmed in the x = 0.1–0.4 samples by comparing the lattice parameters with standard ones of Ni

(111) (3.5238 Å, JCPDS 04-0850) and NiCu (111) (3.5615 Å, JCPDS 65-7246).

3.3. TPR profiles of the fresh catalysts

The TPR profiles of the fresh $La_2(Ni_{1-x}Cu_x)O_4$ catalysts with different x values are shown in Fig. 4. All the catalysts are completely reduced below 700 °C, which is in agreement with the above XRD analyses. The TPR profile of La_2NiO_4 agrees well with that reported by Liu *et al.*,[10] in which the peak centered at about 400 °C is attributed to the reduction of NiO and the peak in the range of 450–680 °C is assigned to the reduction of La_2NiO_4. As we can see, the peak related to the reduction of perovskites shifts to lower temperatures as the substitution degree of Cu increases, indicating that the incorporation of Cu increases the reducibility of the perovskites.
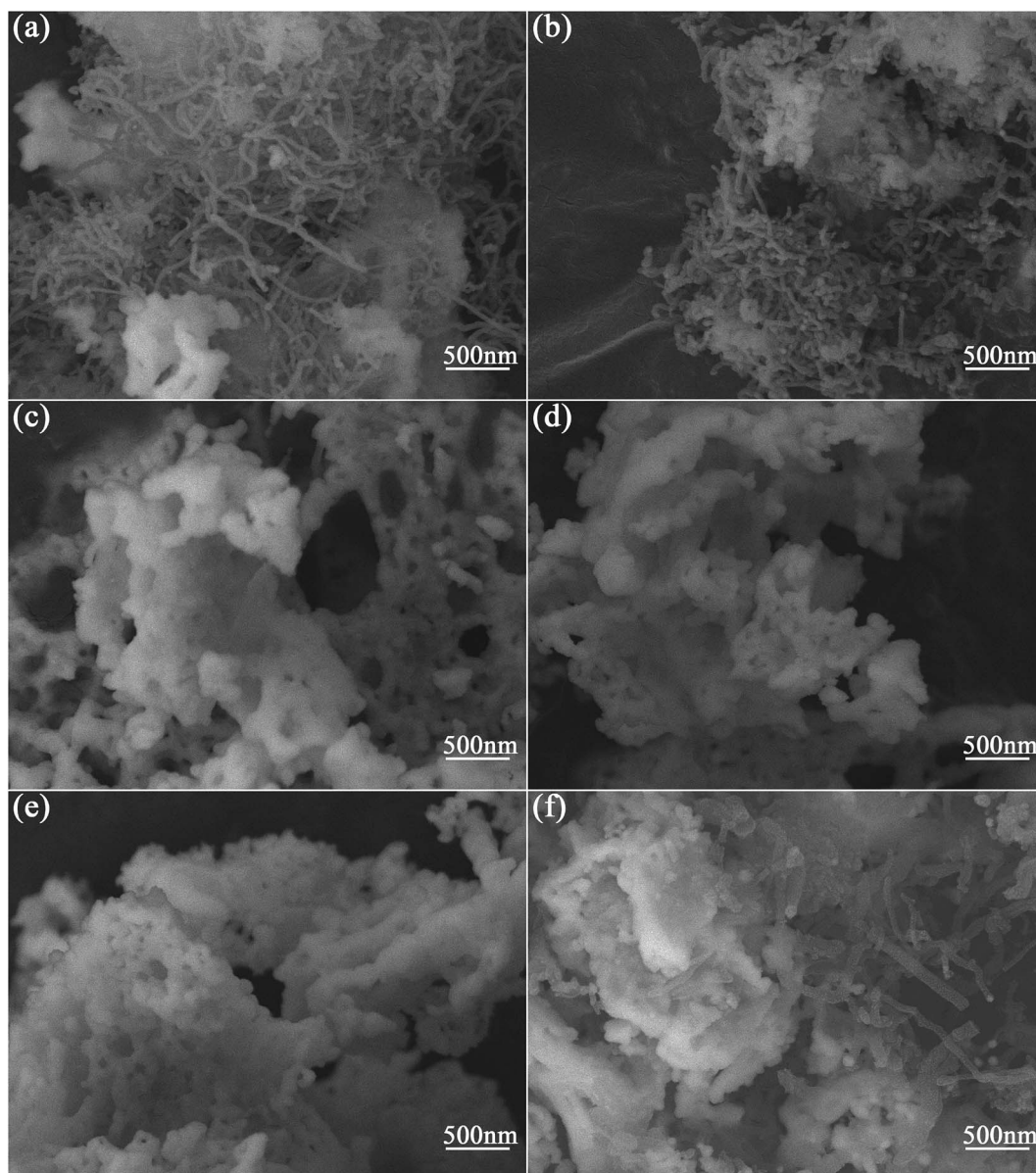
Fig. 6 SEM images of the used $La_2(Ni_{1-x}Cu_x)O_4$ with x = (a) 0.0, (b) 0.1, (c) 0.2, (d) 0.3, (e) 0.4, and (f) $Ni_{0.8}Cu_{0.2}/La_2O_3$.

3.4. XPS analysis of the used catalysts

Fig. 5(a) shows the XPS spectra of Cu2p for the used La_2 $(Ni_{1-x}Cu_x)O_4$ samples with $x = 0.0$, 0.2 and 0.4. As expected, we cannot observe any Cu peaks for the Cu-absent $x = 0.0$ sample. For the Cu-present $x = 0.2$ and 0.4 samples, $Cu2p_{3/2}$ (932.7 eV) and $Cu2p_{1/2}$ (952.5 eV) are clearly identified. The absence of large satellite peaks indicates the absence of CuO.[20] Thus, we conclude that Cu exists in its metallic form. Fig. 5(b) shows the spectra of Ni3p (together with Cu3p). For all three samples, Ni3p can be deconvoluted into $Ni3p_{3/2}$ (66.2 eV), $Ni3p_{1/2}$ (68.0 eV) and a satellite peak, indicating the Ni element exists as metallic Ni.[21] Both Ni and Cu exist in their metallic forms, indicating that the perovskite precursors decompose completely under the reducing DRM conditions. The composition of the Ni–Cu alloy is determined by the XPS analysis and the results are listed in Table 2. It is worth noting that the atomic ratio of Cu in the Ni–Cu alloy is much larger than the stoichiometric ratio of the $La_2(Ni_{1-x}Cu_x)O_4$ precursors. This is because the penetration depth of XPS is very small (1–5 nm).[22] Thus, the composition determined by XPS reflects the surface composition of the alloy. The larger surface Cu : Ni atomic ratio indicates an aggressive surface segregation of Cu in the Ni–Cu alloy.

3.5. Microstructures of the used catalysts

Fig. 6 shows the SEM images of the used catalysts. Large amount of filamentous carbon can be observed for the La_2 $(Ni_{1-x}Cu_x)O_4$ samples with $x = 0.0$, 0.1 and $Ni_{0.8}Cu_{0.2}/La_2O_3$, while no carbon can be seen for the $x = 0.2$–0.4 samples. This is in agreement with Fig. 2(a).

To gain further microstructural information of the used catalysts, TEM analyses were performed and the TEM images are shown in Fig. 7. Metallic particles dispersed on the support can be observed for all the samples. Carbon is present for the x
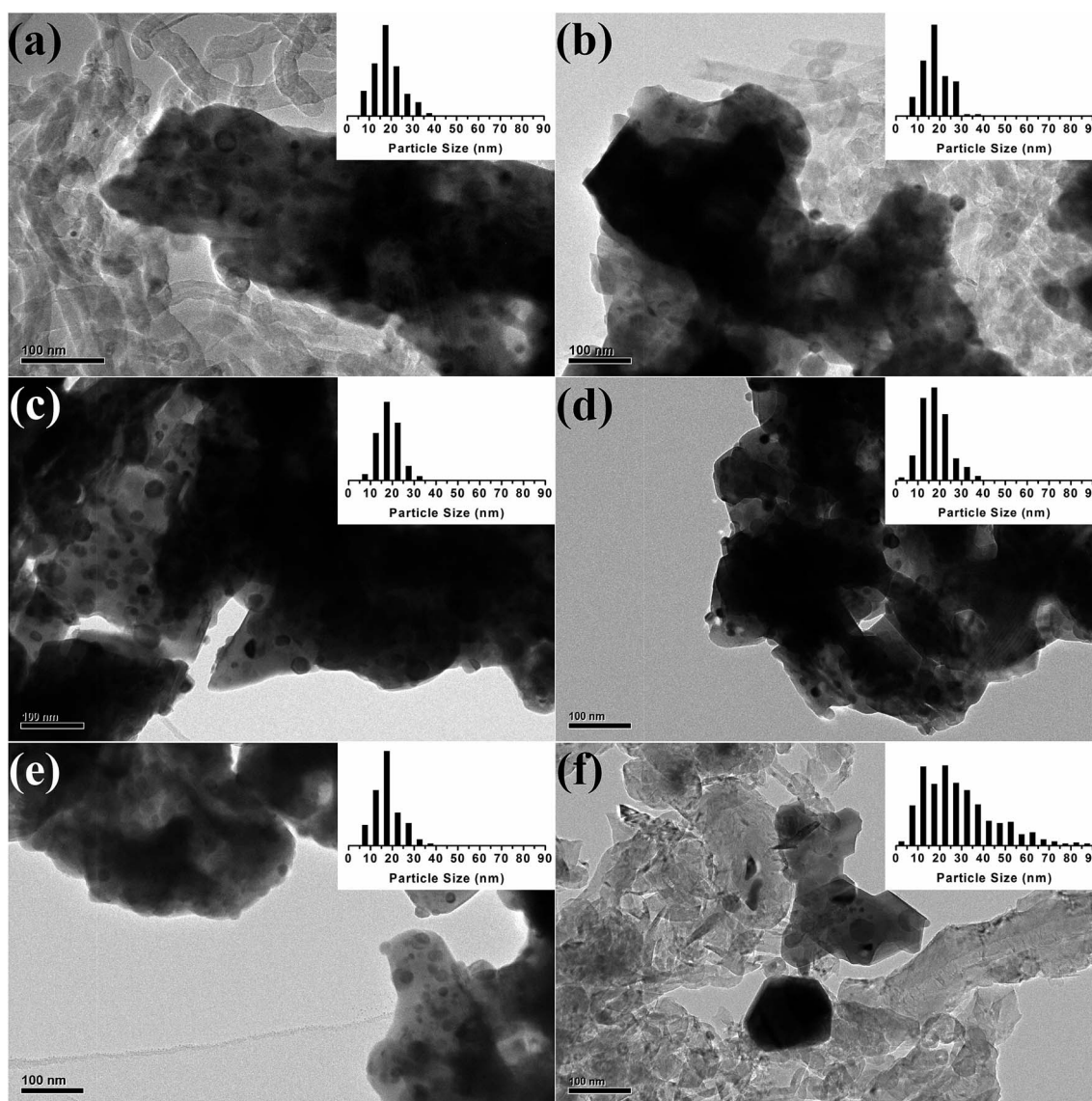

Fig. 7 TEM images of the used $La_2(Ni_{1-x}Cu_x)O_4$ with x = (a) 0.0, (b) 0.1, (c) 0.2, (d) 0.3, (e) 0.4, and (f) $Ni_{0.8}Cu_{0.2}/La_2O_3$.

= 0.0, 0.1 samples and $Ni_{0.8}Cu_{0.2}/La_2O_3$ but absent for the x = 0.2–0.4 samples, which agrees with Fig. 2(a) and 6. The insets of Fig. 7 show the lateral size distributions of Ni particles which are statistically analyzed over more than 150 particles. It is interesting to note that although the reduced $La_2(Ni_{1-x}Cu_x)O_4$ catalysts show significant differences in carbon deposition, the size distributions (0–40 nm) of the metal particles are very similar. On the other hand, the impregnated $Ni_{0.8}Cu_{0.2}/La_2O_3$ shows a more disperse metal particle distribution (0–90 nm). The phenomenon that the metallic particle size of impregnated samples is larger than that of the reduced perovskites agrees with other reports.[8–11]

4. Discussion

According to our results, the reduced $La_2(Ni_{0.8}Cu_{0.2})O_4$ shows the optimal catalytic performances with high catalytic activity and significantly improved carbon resistance.

Obviously, the reduced $La_2(Ni_{0.8}Cu_{0.2})O_4$ shows better catalytic performance than the impregnated $Ni_{0.8}Cu_{0.2}/La_2O_3$. According to Fig. 7, the metallic particle size of the x = 0.2 sample is smaller than that of the impregnated $Ni_{0.8}Cu_{0.2}/La_2O_3$. It is generally accepted[4,23] that the nucleation of the CNTs is through a dissolution–precipitation mechanism. Carbon, which has a high solubility in the nickel lattice, may dissolve into the nickel crystal and precipitate after supersaturation. According to Bengaard et al.,[24] large nickel particles favor graphite nucleation, since a graphite nucleus needs to be large enough to be stable. Thus, the large metallic particles of the impregnated $Ni_{0.8}Cu_{0.2}/La_2O_3$ lead to severe carbon deposition. Similar results were reported by Gallego et al.[11]

However, it is interesting to note that although the metal particles show similar distribution (see the insets of Fig. 7), the reduced $La_2(Ni_{1-x}Cu_x)O_4$ catalysts show significant differences in carbon deposition. Thus, we cannot attribute the remarkably improved carbon resistance of the x = 0.2–0.4 samples to the size effects of the metal particles. We have confirmed the surface segregation of Cu in the Ni–Cu particles of the reduced $La_2(Ni_{1-x}Cu_x)O_4$ catalysts (see Table 2). The surface segregation of Cu in Ni–Cu has also been widely reported.[25–30] Moreover, Zhu et al. reported[25] that the distribution of Cu on the Ni–Cu particle surface is not uniform; Cu tends to segregate at corners and edges of the particle and both Ni and Cu tend to have neighbors of the same element. Thus, a cage-like structure of Cu forms on the surface of the Ni core and divides the surface of Ni ensembles into small areas. The small areas of Ni should be too small for the formation of stable graphite nucleus, thus suppresses the carbon deposition. Nevertheless, Cu is reported to be inert for CH_4 adsorption and dissociation.[31,32] Further increase of x above 0.2 leads to reduced Ni-exposure on the metal surface, resulting in reduced catalytic activity.

5. Conclusions

$La_2(Ni_{1-x}Cu_x)O_4$ catalyst precursors were synthesized by glycine sol–gel self-combustion method. The reduced $La_2(Ni_{0.8}Cu_{0.2})O_4$ shows optimal performance with negligible carbon deposition,

and the conversions of CH_4 and CO_2 are 73% and 80%, respectively. The remarkably improved carbon resistance of the reduced $La_2(Ni_{0.8}Cu_{0.2})O_4$ is attributed to: (1) the smaller metallic particles of the reduced perovskite as compared with those of the impregnated catalyst; (2) the cage-like structure of surface segregated Cu, which divides the surface of Ni ensembles into small areas and suppresses the formation of stable graphite nucleus. Thus, the perovskite $La_2(Ni_{0.8}Cu_{0.2})O_4$ is a promising catalyst precursor for DRM.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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