



Cite this: *RSC Adv.*, 2017, 7, 47990

# Ionic liquids as efficient pretreatment solvents for lignocellulosic biomass

Fu-Ling Wang,<sup>a</sup> Shuang Li,<sup>a</sup> Yi-Xin Sun,<sup>a</sup> Hui-Ying Han,<sup>a</sup> Bi-Xian Zhang,<sup>b</sup> Bao-Zhong Hu,<sup>\*c</sup> Yun-Fei Gao<sup>b</sup> and Xiao-Mei Hu<sup>\*a</sup>

Ionic liquid (IL)-assisted pretreatment of lignocellulosic biomass has been extensively studied. Cellulose and hemicelluloses are rich resources of sugars for biofuels. Lignin is a valuable feedstock for aromatic-based platform chemicals. In this study, a series of ionic liquids (ILs) were prepared with one-step synthesis and were investigated for their activity to pretreat lignocelluloses. High yields of lignin (61.0% and 60.4%) were achieved through [Hpy]Cl and [Hmim]Cl pretreatment of poplar. Lignin yields of 51.7% and 50.3% were obtained with a [Hpy]Cl and [Hnmp]Cl pretreatment of bamboo. Improving enzymatic hydrolysis was observed from the regenerated poplar with [Hpy]Cl pretreatment and the regenerated bamboo with [Hmim]Cl pretreatment. The isolated fractions were characterized by FTIR (Fourier transform infrared) spectroscopy. SEM (Scanning electron microscopy) and XRD (X-ray diffractometry) were employed to examine the cellulose-rich materials. A 2D <sup>1</sup>H–<sup>13</sup>C heteronuclear single quantum coherence (HSQC) nuclear magnetic resonance (NMR) spectroscopy was employed to analyze lignin fraction. These ionic liquids were particularly effective to extract lignin from lignocelluloses to obtain cellulose-rich materials for biofuels.

Received 23rd July 2017

Accepted 22nd September 2017

DOI: 10.1039/c7ra08110c

rsc.li/rsc-advances

## 1. Introduction

Lignocelluloses are potentially valuable resources due to their capability of being transformed into biofuels and bioproducts. The main constituents of lignocelluloses include cellulose, hemicelluloses, and lignin. Cellulose and its derivatives are extensively used in industries such as textiles, plastics, wood and paper products, cosmetics and pharmaceuticals. There have been a number of biorefinery studies focusing on the conversion of the cellulose fraction of the biomass as a source for fuels or higher value products.<sup>1</sup> Additionally, the lignin fraction can be a valuable feedstock for the production of aromatic platform chemicals. Lignin sulfonates are used in various applications such as phenol-formaldehyde plastics, binders, adsorbents, and adhesives.<sup>2</sup> Lignin is also used to produce various polymers such as polyesters and polyurethanes. Lignin is a potential renewable source for “value-added” chemicals, such as benzene, phenol, guaiacol, vanillic acid, and methanol.

However, due to the recalcitrant structure of lignocelluloses, the pretreatment of lignocelluloses are necessary. A variety of ionic liquids (ILs), such as imidazolium-, pyridinium-, ammonium-, and phosphonium-based cations, along with alkyl or

allyl side chains coupled to various anions, such as chloride, acetate, and phosphonate, have been used in the pretreatment of lignocellulosic biomass.<sup>3–5</sup>

Ionic liquids are environmentally compatible solvents. They have high thermal stabilities and negligible vapor pressures; they do not release toxic or explosive gases when utilized.<sup>6</sup> Previous studies on ILs have focused on lignin removal from lignocellulosic biomasses to improve the saccharification efficiency of lignocelluloses. Fu and Mazza reported 29% total lignin removal from triticale straw using 1-ethyl-3-methylimidazolium acetate ([Emim]Cl) as a pretreated solvent at 150 °C for 1.5 h.<sup>7</sup> Wei *et al.* investigated 1-butyl-3-methylimidazolium chloride ([Bmim]Cl) as an IL solvent for the pretreatment of legume straw at 150 °C for 2 h; the authors observed 30% lignin removal.<sup>8</sup> Currently, more studies have been conducted regarding the lignin yield as lignin is a potential renewable source for valuable products. The pretreatment of corn stalks with [Emim]Ac at 125 °C for 1 h resulted in a 44% lignin yield.<sup>9</sup> The fractionation of bagasse was performed at 110 °C for 16 h with choline acetate, and 20% of the lignin was fractionated as lignin-rich material.<sup>10</sup>

Ionic liquids, such as [Emim]Cl, [Bmim]Cl and [Emim]Ac have been widely reported for the pretreatment of lignocelluloses, however, high pretreatment temperatures and long processing times are always required.<sup>11</sup> A ball mill was also used for 72 h before IL pretreatment.<sup>12</sup> However, lignin regeneration is not very efficient using ILs such as [Bmim]Cl and [Emim]Ac.<sup>13,14</sup> In this study, a series of ionic liquids were synthesized and

<sup>a</sup>College of Life Science, Northeast Agricultural University, Harbin, 150030, China. E-mail: huxiaomei1982@163.com

<sup>b</sup>Heilongjiang Academy of Agricultural Sciences, Harbin, 150086, China

<sup>c</sup>Harbin University, Harbin, 150086, China. E-mail: bzhu@neau.edu.cn



investigated for their activity on the pretreatment of poplar and bamboo flours.

## 2. Experimental

### 2.1 Materials

All chemicals were purchased from Aladdin Company (Shanghai, China) and used as received. Poplar flour and bamboo flour were purchased from Xingtang Xinlei Mineral Powder Factory (Shijiazhuang, China). The poplar flour and bamboo flour were ground to an average particle size of less than 40-mesh (400 $\mu$ ) and stored in an air-tight container at room temperature until used.

### 2.2 Composition of poplar and bamboo

The samples (300 mg) were hydrolyzed with 3 mL of 72% sulfuric acid and incubated for 1 h at 30 °C with stirring every 10 min. The solution was then diluted to 4% sulfuric acid by adding 84 mL of deionized water. The mixture was autoclaved for 1 h at 121 °C. After the autoclave treatment, the solution was cooled and the suspended solids were removed by filtration. The filtrate was used to determine the carbohydrate content using high-performance liquid chromatography (HPLC, Agilent 1100, America). The cellulose and xylan contents were calculated from glucose and xylose contents multiplied by conversion factors of 0.90 and 0.88, respectively.<sup>15</sup> The filtrate of the acid-soluble lignin content from poplar was estimated by measuring the absorbance at 240 nm using UV-mini-1240 spectrometer (SHIMADZU). The filtered solids were dried at 105 °C until constant weight. Then the sample was burnt at 575 °C to determine the inorganic ash content. This ash is subtracted from 105 °C dried solids weight to obtain the acid insoluble lignin.<sup>15</sup>

## 3. Methods

### 3.1 Synthesis of ionic liquids

Pyridine (0.3 mol) and hydrochloric acid (0.3 mol) were added into a 100 mL round bottom flask and stirred under mechanical agitation at room temperature for 24 h. The resulting mixture was washed with diethyl ether (20 mL  $\times$  3). Solvent residue was then evaporated using a rotary evaporator at 50 °C for 30 min. The resulting product was further vacuum-dried at 60 °C for 24 h to give [Hpy]Cl. The synthesis of 1-*H*-3-methylimidazolium chloride ([Hmim]Cl) and *N*-methyl-2-pyrrolidonium chloride ([Hnmp]Cl) followed protocols similar to those used for [Hpy]Cl.<sup>16</sup>

### 3.2 Pretreatment of lignocellulose

Poplar or bamboo flour (0.4 g) was added to 8 g of the ionic liquid. The mixture was stirred at 90 °C or 100 °C for 30 min. An acetone/deionized water (1/1, v/v) solution (30 mL) was then added into the ionic liquid mixture. The resulting solid was filtered, washed with 30 mL of acetone/deionized water (1/1, v/v), and dried under a vacuum at 60 °C for 24 h to yield cellulose-rich materials. Acetone was then removed from the filtrate by

rotary evaporation. The resulting product was filtered, further washed with 20 mL of deionized water, and vacuum-dried at 60 °C for 24 h to yield regenerated lignin. The yields of the cellulose-rich materials and extracted lignin were calculated according to eqn (1) and (2), respectively. The ionic liquid was recycled and concentrated for reuse.

$$\text{Cellulose-rich materials yield (\%)} = \frac{\text{cellulose-rich materials (mg)}}{\text{biomass (mg)}} \times 100\% \quad (1)$$

$$\text{Lignin content yield (\%)} = \frac{\text{recover lignin (mg)}}{\text{original content of lignin (mg)}} \times 100\% \quad (2)$$

### 3.3 Fourier transform infrared (FTIR) analysis

FTIR analysis was performed on a FTIR spectrophotometer (Bruker ALPHA-T, Karlsruhe, Germany). The operating system used was Spectrum software (OPUS 6.5, Bruker Optics, Karlsruhe, Germany). Approximately 0.5 mg of the sample was mixed with KBr. The sample was then placed in a press and pressed with 16 tons of pressure for 2 min. The FTIR spectra were recorded for the pellets over the 4000 cm<sup>-1</sup> to 400 cm<sup>-1</sup> region, with a total of 16 scans and a resolution of 4 cm<sup>-1</sup>. The FTIR spectra were recorded using a blank KBr pellet as the background.

### 3.4 Scanning electron microscopy (SEM)

SEM images were taken for both untreated and pretreated poplar and bamboo solids using a Hitachi S-3400N microscope. Prior to acquiring images, the samples were mounted with double sided carbon tape on precut brass sample stubs and sputter coated with approximately 30 angstrom of Au/Pd. The representative images of ionic liquid-pretreated poplar and bamboo were acquired with a 5 kV accelerating voltage.

### 3.5 X-ray diffractometry

X-ray diffractometry was conducted on D/max-2500PC diffractometer (Japan) equipped with Cu K $\alpha$  radiation over the range of 5–60° with a step of 4° at 40 kV and 100 mA. The crystallinity, as expressed by the crystallinity index (CrI), was determined by Segal method.<sup>17</sup> The following empirical equation was adopted to estimate the crystallinity index:

$$\text{CrI (\%)} = 100 \times \frac{I_{\text{total}} - I_{\text{am}}}{I_{\text{total}}} \quad (3)$$

In which  $I_{\text{total}}$  is the scattered intensity at the main peaks, whereas  $I_{\text{am}}$  is the scattered intensity due to the amorphous portion.<sup>18</sup>

### 3.6 Enzymatic hydrolysis

Enzymatic hydrolysis was performed with a biomass loading of 1% (g mL<sup>-1</sup>) and 0.02 g of cellulase in 0.1 M sodium citrate buffer (pH 4.8) on a shaker at 150 rpm, 50 °C for 72 h. After that time, the mixture was heated at 100 °C for 10 min. The reducing



sugars were measured by the DNS method.<sup>19</sup> The yields of glucose, xylose and cellobiose were measured by HPLC and calculated according to eqn (4).

$$\text{Sugar (\%)} = \frac{\text{glucose, cellobiose, xylose (mg)}}{\text{cellulose-rich materials subjected to enzymatic hydrolysis (mg)}} \times 100\% \quad (4)$$

### 3.7 Nuclear magnetic resonance (NMR) analysis

<sup>1</sup>H-<sup>13</sup>C correlation 2D NMR heteronuclear single quantum correlation spectra were recorded on a Bruker AV-III 400 MHz spectrometer (ShangHai, China) at 25 °C. A mixture of DMSO-d<sub>6</sub>/pyrimidine (4 : 1, v/v) was used as the solvent for sample handling.<sup>20</sup>

## 4. Results and discussion

The composition of the poplar and bamboo was analyzed using the National Renewable Energy Laboratory standard procedure.<sup>15</sup> Poplar consisted of 42.5% cellulose, 10.0% hemicelluloses, and 23.5% lignin. Bamboo contained 36.3% cellulose, 12.6% hemicelluloses, and 30.6% lignin.

### 4.1 Determination of lignin

Higher pretreatment temperatures accelerated the swelling and dissolution rates of lignocelluloses in ILs.<sup>21,22</sup> Higher temperatures could effectively disrupt the recalcitrant structure of lignocelluloses to release lignin. Vo *et al.*<sup>23</sup> demonstrated that milled poplar could be dissolved in 1-ethyl-3-methylimidazolium acetate ([Bmim]Ac) at 130 °C for 12 h; the procedure yielded 31.9% of the original lignin. With lower pretreatment temperatures, longer times were required for efficient lignin extractions of biomasses. Xu *et al.*<sup>24</sup> reported that rice straw pretreated with 1-ethyl-3-methylimidazolium phosphinate ([Emim][H<sub>2</sub>PO<sub>2</sub>]), [Emim]Ac, and [Emim]Cl at 110 °C for 24 h resulted in lignin extraction rates of 55.6%, 47.8%, and 14.6%, respectively, when determined from the UV-vis absorbance at 280 nm. Compared with current studies

(Table 1), a low pretreatment temperature and a short time were used in this work.

In this study, the yield of the lignin extracted was calculated according to eqn (2). As the temperature increased from 90 °C to 100 °C (Fig. 1), lignin regeneration improved from 51.3% to 61.0% with [Hpy]Cl-treatment. Lignin yield improved from 49.3% to 60.4% with [Hmim]Cl-treatment, and the yield improved from 38.7% to 47.9% with [Hnmp]Cl-treatment. Thus, high lignin yields of 61.0% and 60.4% were achieved when the poplar was pretreated at 100 °C for 30 min with [Hpy]Cl and [Hmim]Cl, respectively.

In addition, as the temperature increased from 90 °C to 100 °C, lignin regeneration improved from 42.6% to 51.7% with [Hpy]Cl-treatment. Lignin yield improved from 26.6% to 50.3% with [Hnmp]Cl-treatment, and the yield improved from 39.9% to 43.7% with [Hmim]Cl-treatment. Thus, high lignin yields of 51.7% and 50.3% were obtained from bamboo treated with [Hpy]Cl and [Hnmp]Cl, respectively (Fig. 2).

The degree of biomass recalcitrance varies among the biomass species. Fort *et al.*<sup>25</sup> proposed that wood type and species affected the dissolution ability. In this study, lignin yields of 38.7% to 61.0% were obtained from poplar, and lignin yields of 26.6% to 51.7% were extracted from bamboo. A lower lignin yield was recovered from bamboo due to its recalcitrant structure. Although ball milling of bamboo for 72 h before IL-pretreatment was required,<sup>12</sup> the milling process was not employed when using these ILs in this work.

When compared to contemporary studies, a low pretreatment temperature and a short processing time were employed using these ionic liquids, they resulted in obtaining high lignin yield (Table 1). For example, 31.90% of the lignin was extracted from poplar in [Emim]Ac at 130 °C for 12 h.<sup>26</sup> Poplar pretreated with [Emim]Ac for 1 h at 125 °C resulted in 10.1% lignin removal.<sup>27</sup> In this work, more than 60% lignin removal was achieved from poplar with [Hpy]Cl and [Hmim]Cl at 100 °C for 30 min.

### 4.2 Determination of cellulose-rich materials

The yields of cellulose-rich materials were calculated according to eqn (1). As shown in Fig. 3 and 4, when the temperature increased from 90 °C to 100 °C, the yield of cellulose-rich

Table 1 Comparison of lignin extraction in various ILs

Ionic liquid	Biomass	Temp. (°C)	Time (h)	Biomass mass/ILs mass (%)	Lignin extraction yield (%)	Ref.
[Emim]Cl	Triticale straw	150	1.5	5 (w/w)	29	28
[C <sub>4</sub> C <sub>1</sub> im]Cl	Legume straw	150	2	5 (w/w)	30	8
[Emim]Ac	Triticale straw	130	1.5	5 (w/w)	41	7
[Emim]Ac	Poplar	130	12	5 (w/w)	31.90	26
[Emim]Ac	Poplar	125	1	33.3 (w/w)	10.1	27
[Bmim]Ac/H <sub>2</sub> O	Willow	120	22	10 (w/v)	46.7	29
[Emim]Ac	Southern yellow pine	110	16	5 (w/w)	31.4	30
[Emim]Ac	Maple wood flour	90	24	5 (w/w)	37	31
[Hpy]Cl	Poplar	100	0.5	5 (w/w)	61.0	
[Hmim]Cl	Poplar	100	0.5	5 (w/w)	60.4	
[Hpy]Cl	Bamboo	100	0.5	5 (w/w)	51.7	
[Hnmp]Cl	Bamboo	100	0.5	5 (w/w)	50.3	



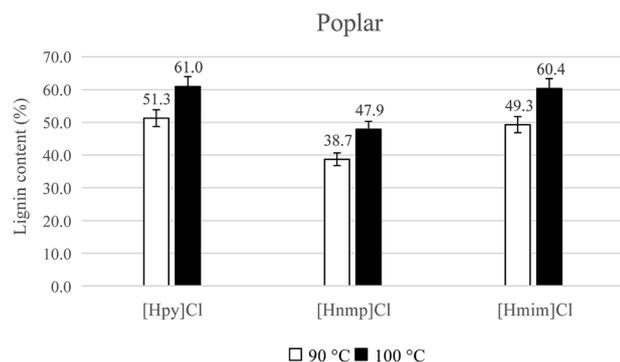


Fig. 1 The extracted lignin content from poplar.

materials decreased from 59.7% to 37.1% for poplar with [Hpy]Cl-treatment (Fig. 3). When the temperature increased from 90 °C to 100 °C, the yield of cellulose-rich materials decreased from 76.1% to 53.0% for bamboo with [Hnmp]Cl-pretreatment (Fig. 4). Increased temperatures resulted in the efficient lignin extraction and the reduced yields of cellulose-rich materials.

#### 4.3 FTIR analysis of cellulose-rich materials from lignocelluloses

The FTIR spectra of cellulose-rich materials from poplar are illustrated in Fig. 5. The absorbances at 3427, 2923, 1433, 1378, 1334, 1163, 1108, 1057, and 889  $\text{cm}^{-1}$  are associated with cellulose. Typically, the absorption at 3427  $\text{cm}^{-1}$  is associated with the O–H stretching. The peak at 2923  $\text{cm}^{-1}$  is attributed to C–H stretching. A peak at 1433  $\text{cm}^{-1}$  is related to  $\text{CH}_2$  symmetric bending. The absorbance at 1378  $\text{cm}^{-1}$  is related to CH bending. The peak at 1334  $\text{cm}^{-1}$  is related to the  $\text{CH}_2$  bending of the carbohydrates, whereas the 1163  $\text{cm}^{-1}$  peak is attributed to C–O antisymmetric stretching. The absorbance at 1111  $\text{cm}^{-1}$  is related to C–OH skeletal vibration, and the absorbance at 1053  $\text{cm}^{-1}$  is due to the C–O–C pyranose ring skeletal vibration. The peak at 889  $\text{cm}^{-1}$  corresponds to the glycosidic  $\text{C}_1$ –H deformation with ring vibration contribution, which is a characteristic of the  $\beta$ -glycosidic linkages between glucose monomers in cellulose.

The FTIR spectra of cellulose-rich materials from bamboo are illustrated in Fig. 6. The absorbance at 3442, 2912, 1458,

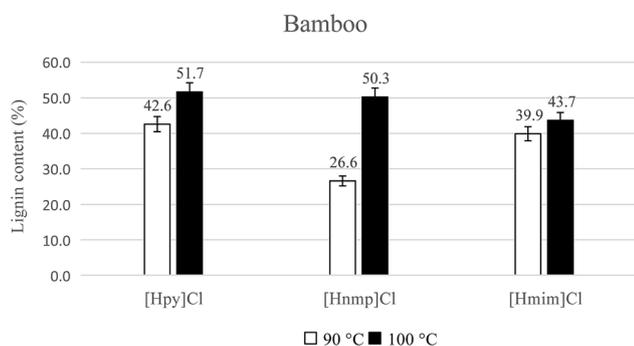


Fig. 2 The extracted lignin content from bamboo.

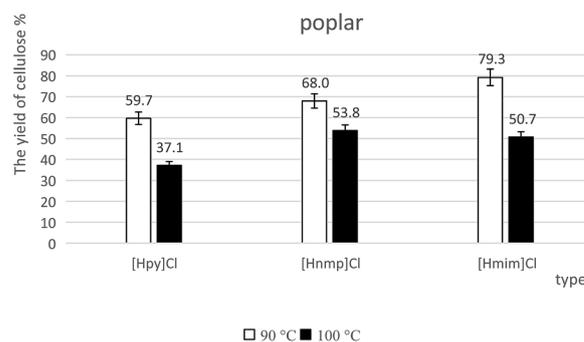


Fig. 3 The yields of cellulose-rich materials from poplar.

1371, 1327, 1166, 1049, and 900  $\text{cm}^{-1}$  are associated with cellulose. Typically, the absorption at 3427  $\text{cm}^{-1}$  is associated with the O–H stretching. The 2912  $\text{cm}^{-1}$  peak is attributed to C–H stretching. A peak at 1422  $\text{cm}^{-1}$  is related to  $\text{CH}_2$  symmetric bending, whereas the 1371  $\text{cm}^{-1}$  peak is related to CH bending. The absorbance at 1327  $\text{cm}^{-1}$  is related to  $\text{CH}_2$  bending of carbohydrates. The 1166  $\text{cm}^{-1}$  peak is attributed to C–O antisymmetric stretching. The 1111  $\text{cm}^{-1}$  absorbance is related to C–OH skeletal vibration, whereas the 1049  $\text{cm}^{-1}$  absorbance is attributed to the C–O–C pyranose ring skeletal vibration. The peak at 900  $\text{cm}^{-1}$  is related to the glycosidic  $\text{C}_1$ –H deformation with ring vibration contribution.

#### 4.4 FTIR analysis of lignin from poplar

The peaks at 3423, 2938, 1710, 1601, 1510, 1462, 1426, 1331, 1272, 1225, 1126, 1035, and 830  $\text{cm}^{-1}$  are associated with IL-extracted lignin from poplar (Fig. 7). Typically, the peaks at 1601  $\text{cm}^{-1}$  and 1510  $\text{cm}^{-1}$  are attributed to the aromatic skeletal vibrations. The peak at 1462  $\text{cm}^{-1}$  is related to C–H deformations. The peak at 1426  $\text{cm}^{-1}$  is associated with aromatic skeletal vibrations combined with C–H in-plane deformation. The peak at 1331  $\text{cm}^{-1}$  is related to syringyl unit (S) vibration breathing with C=O stretching and to condensed guaiacyl unit (G) rings. The peak at 1272  $\text{cm}^{-1}$  is related to G ring breathing with carbonyl stretching. The peak at 1225  $\text{cm}^{-1}$  is associated with C–C, C–O, and C=O stretching. The peak at 1126  $\text{cm}^{-1}$  is attributed to ether. The peak at 1035  $\text{cm}^{-1}$  is associated with aromatic C–H in-plane deformation and with C–O deformation

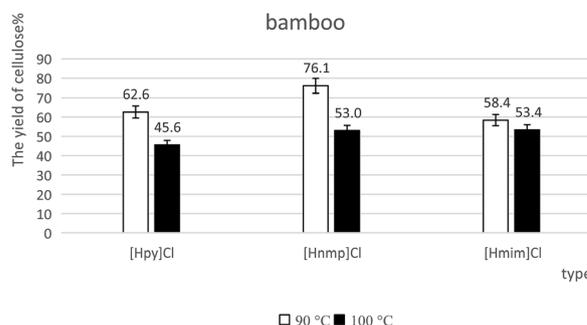


Fig. 4 The yields of cellulose-rich materials from bamboo.



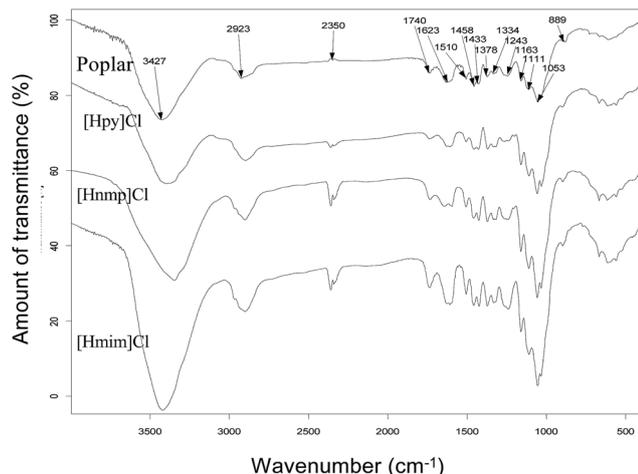


Fig. 5 FTIR spectra of cellulose-rich materials from poplar at 90 °C.

in primary alcohols, as well as C=O stretching. The peak at 830  $\text{cm}^{-1}$  is C-H out-of-plane deformation of S rings.<sup>32</sup>

#### 4.5 FTIR analysis of lignin from bamboo

The peaks at 3431, 2938, 1703, 1605, 1513, 1462, 1426, 1331, 1225, 1166, 1126, 1035, and 834  $\text{cm}^{-1}$  are attributed to alkali lignin (Fig. 8). Typically, the peaks at 1605  $\text{cm}^{-1}$ , 1513  $\text{cm}^{-1}$ , and 1426  $\text{cm}^{-1}$  are attributed to aromatic skeletal vibrations. Similarly, the peak at 1462  $\text{cm}^{-1}$  is the result of C-H deformations. The peak at 1331  $\text{cm}^{-1}$  is related to syringyl unit (S) vibrations. The peak at 1225  $\text{cm}^{-1}$  is from C-C, C-O, and C=O stretching.<sup>33</sup> The peak at 1125  $\text{cm}^{-1}$  is attributed to ether-O-. The peak at 1035  $\text{cm}^{-1}$  is associated with aromatic C-H in-plane deformation. The peak at 834  $\text{cm}^{-1}$  is associated with C-H out-of-plane deformation of S rings.

Furthermore, the intensity of the peak at 1710  $\text{cm}^{-1}$  was strong in the spectra with [Hpy]Cl and [Hmim]Cl pretreatments for bamboo, but weak in the spectra with [Hnmp]Cl pretreatment. This peak was associated with C=O stretching that

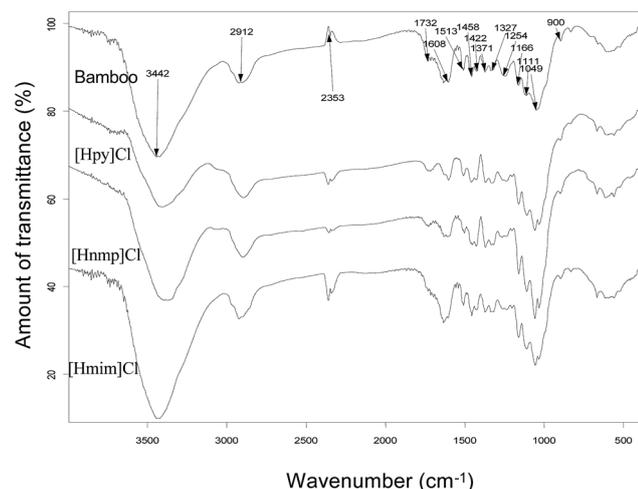


Fig. 6 FTIR spectra of cellulose-rich materials from bamboo at 90 °C.

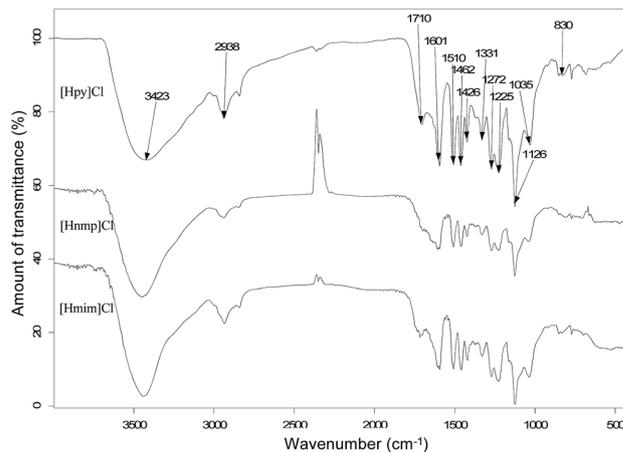


Fig. 7 FTIR spectra of IL-extracted lignin from poplar at 90 °C.

indicated hydroxycinnamates, for example, ferulate. Ferulate esterified with an arabinosyl unit in hemicelluloses was attached to lignin with an ether bond to form a carbohydrates-ferulate-lignin bridge structure. With [Hnmp]Cl pretreatment, lignin containing the bridge structure could not be dissolved in acetone/water, resulting in the decreased content of ferulate in lignin fraction.<sup>33</sup>

Comparisons of the FTIR spectra of poplar with that of bamboo showed some slight differences, for instance, the peak at 1272  $\text{cm}^{-1}$  that was associated with G ring breathing with carbonyl stretching. This peak was prominent in poplar lignin indicating more G unit than bamboo lignin.

#### 4.6 Scanning electron microscopy analysis

The structural changes in morphology of the lignocellulosic biomass before and after IL-pretreatment were analyzed by SEM. As shown in Fig. 9, the original untreated lignocelluloses had the compact ordered and rigid fibril structures, however, the significant morphological modification for both of the bamboo and poplar was observed after ionic liquids pretreatment. Specifically, for poplar, the structure was loosened and

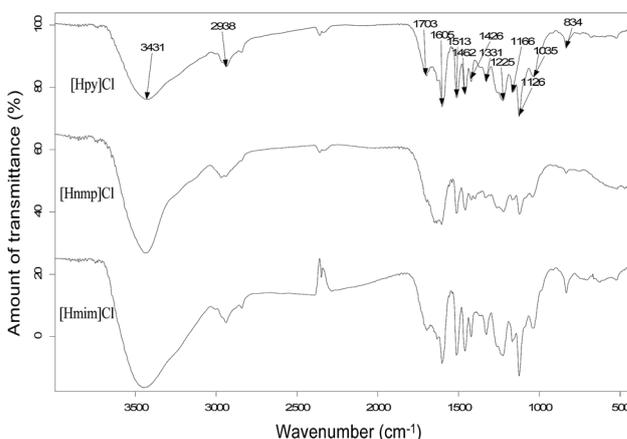


Fig. 8 FTIR spectra of IL-extracted lignin from bamboo at 90 °C.



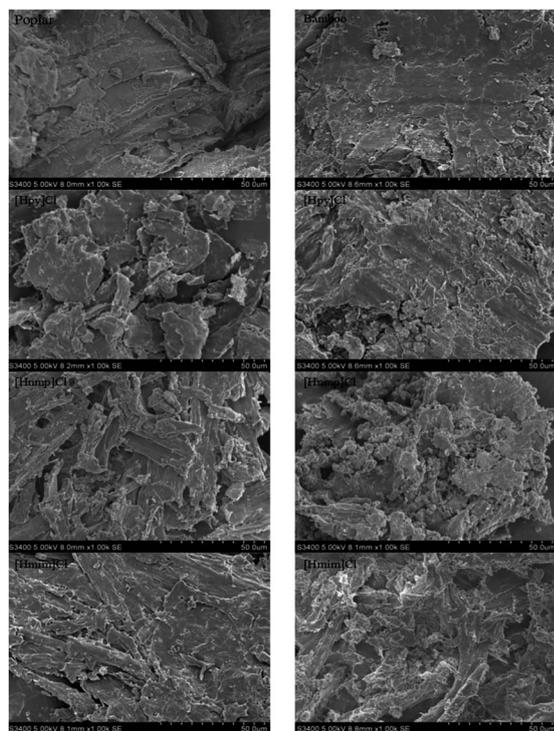


Fig. 9 SEM analysis of untreated and IL-pretreated poplar and bamboo.

less compact after [Hpy]Cl pretreatment. For bamboo, the surface of the residue become irregular after [Hmim]Cl treatment. The alteration of morphology indicated the disruption of linkages in lignocellulose during IL-pretreatment, providing a more accessible surface to cellulose, leading to enhanced enzymatic digestibility.<sup>8</sup>

#### 4.7 X-ray diffraction analysis

The untreated and pretreated cellulose-rich materials of poplar and bamboo were determined by X-ray diffraction and the results were shown in Fig. 10 and 11.

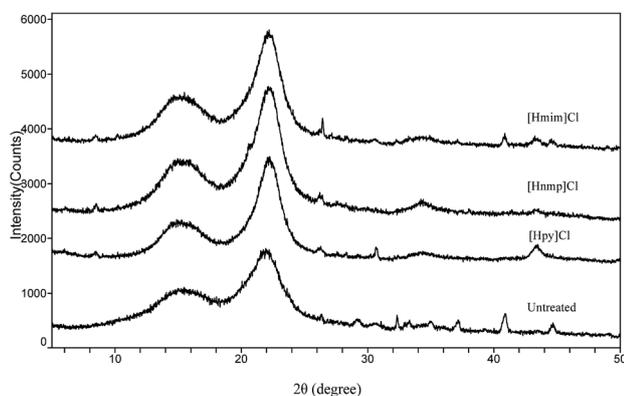


Fig. 10 XRD analysis of untreated poplar and the cellulose-rich materials.

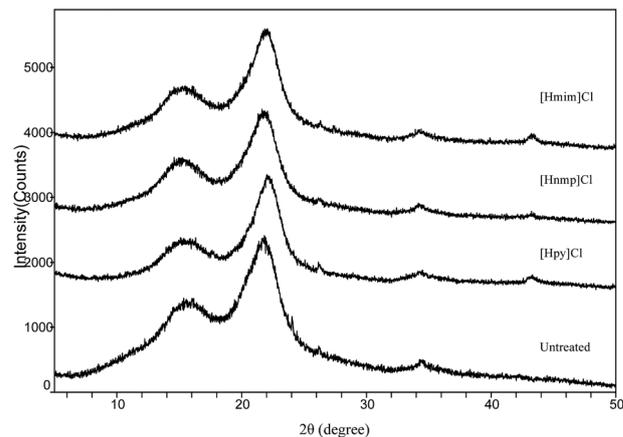


Fig. 11 XRD analysis of untreated bamboo and the cellulose-rich material.

For poplar and bamboo, all samples showed major intensive peaks related to their crystalline structures at  $2\theta$  values of around  $15.5^\circ$  and  $22.2^\circ$ , indicating that the crystallinity of the samples were not significantly changed by IL pretreatment.<sup>34</sup> The peak intensities of the IL treated samples were slightly increased compared to those of the untreated samples, which was consistent with the current reports.<sup>35</sup> The cellulose-rich material crystal structure was unaffected by delignification, but the CrI of the biomass was increased owing to lignin removal.<sup>36</sup> In addition, the peaks around  $2\theta = 15.5^\circ$  and  $22.2^\circ$  were sharper for the IL pretreated poplar and bamboo, which were typical peak for the cellulose I.<sup>37</sup>

#### 4.8 Enzymatic hydrolysis

The results of enzymatic hydrolysis of original biomass and IL-treated biomass are summarized in Tables 2 and 3. After 72 h, high yields of glucose, cellobiose and xylose were 67.5%, 4.2% and 10.4%, respectively, pretreated by [Hpy]Cl from poplar at

Table 2 Enzymatic hydrolysis of cellulose from poplar

Biomass pretreated	Glucose (%)		Cellobiose (%)		Xylose (%)	
	Ave (%)	Std.	Ave (%)	Std.	Ave (%)	Std.
Poplar	46.4	0.37	5.5	0.89	7.3	1.24
[Hpy]Cl	67.5	1.42	4.2	1.07	10.4	0.60
[Hmp]Cl	62.3	0.86	3.6	1.23	8.1	0.77
[Hmim]Cl	62.0	0.94	3.1	0.42	8.0	1.19

Table 3 Enzymatic hydrolysis of cellulose from bamboo

Biomass pretreated	Glucose (%)		Cellobiose (%)		Xylose (%)	
	Ave (%)	Std.	Ave (%)	Std.	Ave (%)	Std.
Bamboo	42.0	0.55	4.5	0.41	8.4	0.34
[Hpy]Cl	63.5	0.94	2.2	0.73	8.0	0.68
[Hmp]Cl	60.8	0.53	2.5	1.12	8.4	0.90
[Hmim]Cl	65.5	1.03	7.1	0.41	11.8	1.09



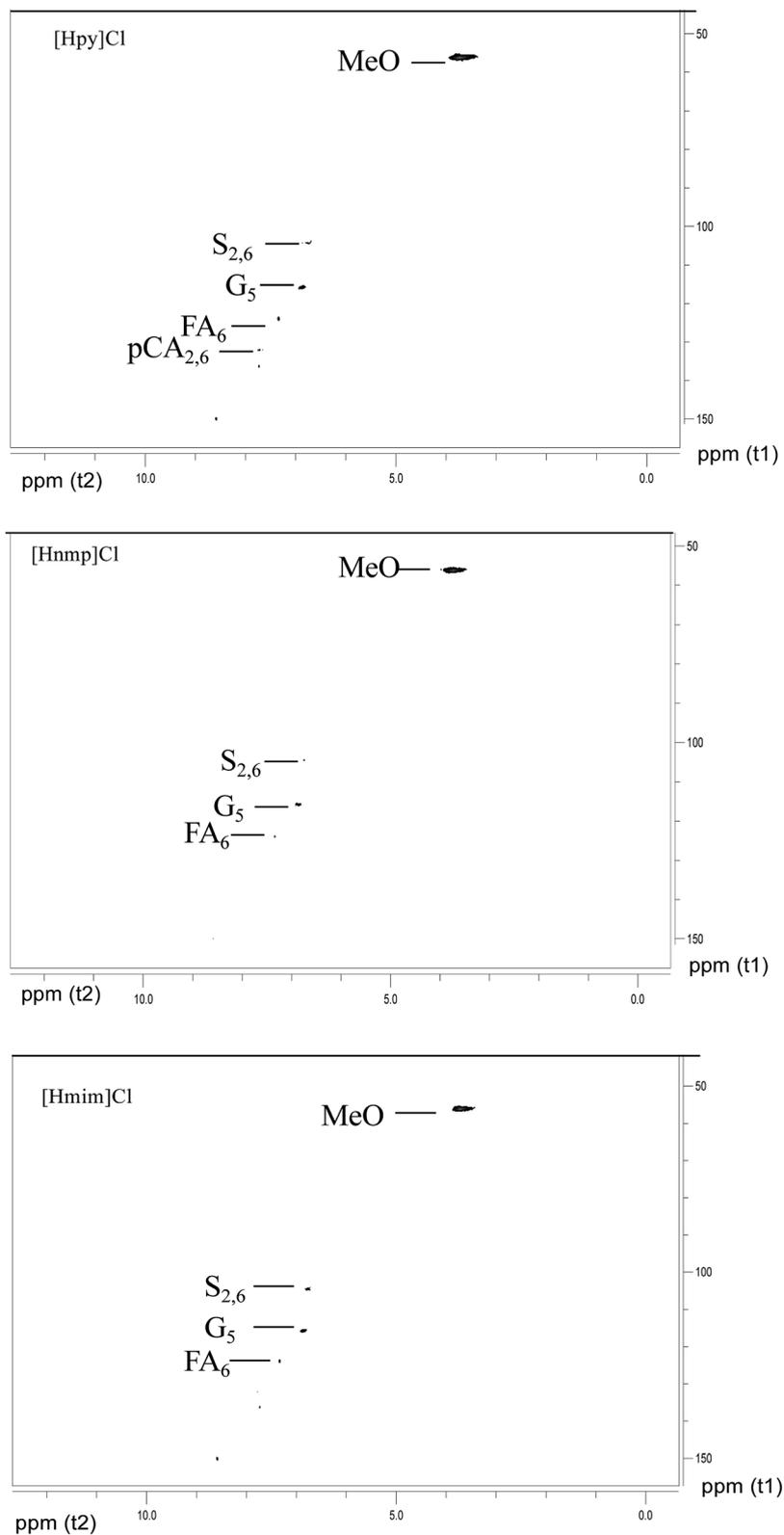


Fig. 12 2D-NMR (HSQC) spectra of IL-extracted lignin from poplar.

90 °C for 30 min. Good yields of glucose, cellobiose and xylose were 65.5%, 7.1% and 11.8% in [Hmim]Cl-treated bamboo sample at 90 °C for 30 min, respectively.

The capability of ionic liquids could destruct the link of lignocelluloses and then to remove the lignin content effectively. The significantly reduction lignin resulted in the high



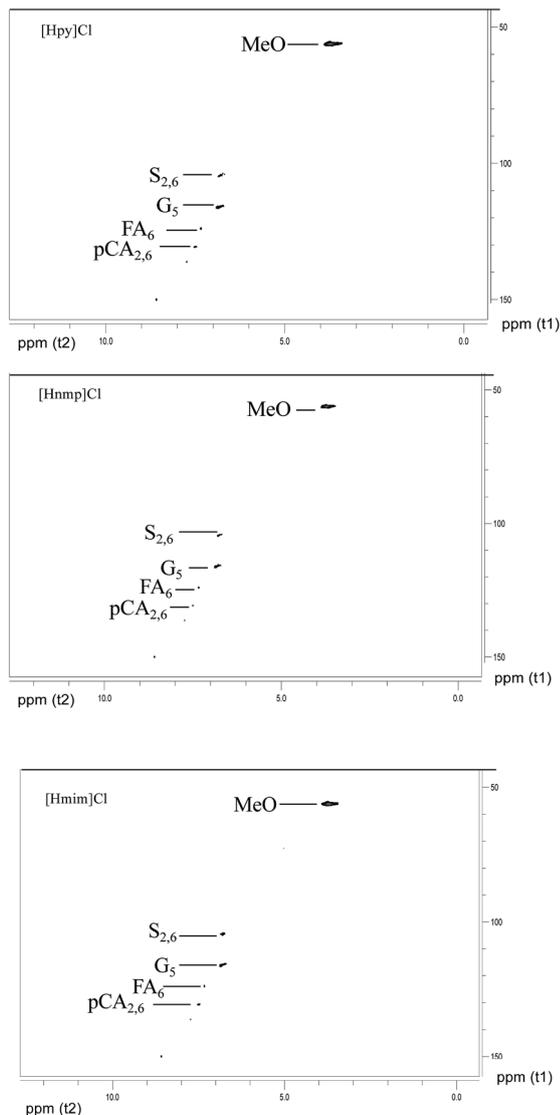


Fig. 13 2D-NMR (HSQC) spectra of IL-extracted lignin from bamboo.

enzyme digestibility of cellulose. The reduced lignin in cellulose-rich materials were also confirmed by FTIR analysis. Moreover, SEM image showed the significant structural changes in morphology, which released a large area on the fiber surface, consequently improving the accessibility of cellulose and the enzymatic efficiency. Ionic liquids pretreatment in this work contributed to achieve the high yield of IL-isolated lignin and the high enzymatic digestibility of cellulose.

#### 4.9 HSQC NMR analysis

The IL-extracted lignin was analyzed by 2D  $^1\text{H}$ - $^{13}\text{C}$  HSQC (Heteronuclear Single Quantum Correlation) NMR. As shown in Fig. 12, the signals at 56.139/3.731 ppm, 115.670/6.860 ppm, 123.920/7.342 ppm, 136.214/7.746 ppm, and 149.965/8.594 ppm are associated with poplar lignin. In general, the signal at 56.139/3.731 ppm is from methoxyl groups (MeO) in the aliphatic region. The aromatic region of lignin is from 100 ppm

to 155 ppm. Typically, a signal at 115.670/6.860 ppm is from  $\text{C}_5\text{-H}_5$  in guaiacyl units (G). A signal at 123.920/7.342 ppm is associated with ferulate groups (FA). However, no signal is observed in the region from 60 ppm to 100 ppm, which is generally associated with polysaccharides.

As shown in Fig. 13, the signals at 56.139/3.731 ppm, 104.508/6.794 ppm, 104.508/6.794 ppm, 116.155/6.860 ppm, 123.920/7.342 ppm, 130.714/7.498 ppm, 136.376/7.746 ppm, and 149.965/8.594 ppm are associated with bamboo lignin. The signal at 56.139/3.731 ppm is from methoxyl groups (MeO) in the aliphatic region.<sup>38</sup> A signal at 104.508/6.794 ppm is associated with  $\text{C}_{2/6}\text{-H}_{2/6}$  in etherified syringyl units (S). The signal at 116.155/6.860 ppm is from guaiacyl units (G). A signal at 123.920/7.342 ppm is associated with ferulate groups (FA).<sup>39</sup> A signal at 130.662/7.509 ppm is associated with p-coumarate groups (PCA).

## 5. Conclusions

In this study, ionic liquids were prepared *via* one-step synthesis as compared to other ILs reported in literature that required a two-step synthesis route. These ILs worked efficiently at a relatively low temperature of 90 °C and 100 °C and a short processing time of 30 min for the pretreatment of lignocellulosic biomass.

These ionic liquids appeared to be more efficient at disruption of inter- and intra-molecular hydrogen bonding in the biopolymers comprising these biomasses. Ionic liquids interact with and solvate the aromatic moieties of lignin through  $\pi$ - $\pi$  and  $n$ - $\pi$  interactions between the aromatic rings and the cations of the IL. Lignin extraction yields of 61.0% and 60.4% from poplar were achieved with [Hnmp]Cl and [Hmim]Cl pretreatments, respectively. Lignin extraction yields of 51.7% and 50.3% from bamboo were obtained with [Hpy]Cl and [Hmim]Cl pretreatments, respectively.

The significantly decreased lignin content resulted in the high enzyme digestibility of cellulose. Additionally, the significant structural changes in morphology increased the accessibility of cellulase and then improved the enzymatic efficiency. The original fibrous structure was significantly disorder by IL-pretreatment, which released a large area on the fiber surface, consequently improving the accessibility of cellulose and the enzymatic efficiency. Poplar with [Hpy]Cl pretreatment resulted in 67.5% glucose, 4.2% cellobiose and 10.4% xylose. Bamboo with [Hmim]Cl pretreatment resulted in 65.5% glucose, 7.1% cellobiose and 11.8% xylose after enzymatic hydrolysis.

[Hnmp]Cl, [Hpy]Cl, and [Hmim]Cl were found to be very effective at lignin extraction and enzymatic saccharification for lignocellulosic biomass.

## Supplementary data

### Pyridinium chloride ([Hpy]Cl)

$^1\text{H}$ -NMR (400 MHz,  $\text{DMSO-d}_6$ ) (ppm): 8.135 (t, 2H, pyridinium ring), 8.684 (t, 1H, pyridinium ring), 9.019 (d, 2H, pyridinium ring), and 12.357 (s, 1H, N-H).

$^{13}\text{C}$ -NMR (400 MHz,  $\text{DMSO-d}_6$ ) (ppm): 127.657 (s, 2C, pyridinium ring), 141.222 (s, 2C, pyridinium ring), and 146.803 (s, 1C, pyridinium ring).



### N-Methyl-2-pyrrolidonium chloride ([Hnmp]Cl)

<sup>1</sup>H-NMR (400 MHz, DMSO-d<sub>6</sub>) (ppm): 1.831 (q, 2H, pyrrolidonium ring), 2.147 (t, 2H, pyrrolidonium ring), 2.633 (s, 3H, -CH<sub>3</sub>), 3.255 (t, 2H, pyrrolidonium ring), and 13.511 (s, 1H, N-H).

<sup>13</sup>C-NMR (400 MHz, DMSO-d<sub>6</sub>) (ppm): 17.582 (s, 1C, pyrrolidonium ring), 29.530 (s, 1C, -CH<sub>3</sub>), 30.463 (s, 1C, pyrrolidonium ring), 49.153 (s, 1C, pyrrolidonium ring), and 174.474 (s, 1C, pyrrolidonium ring).

### 1-H-3-Methylimidazolium chloride ([Hmim]Cl)

<sup>1</sup>H-NMR (400 MHz, DMSO-d<sub>6</sub>) (ppm): 2.079 (f, 2H, -CH<sub>2</sub>-), 2.444 (t, 2H, -CH<sub>2</sub>-), 3.841 (s, 3H, -CH<sub>3</sub>), 4.290 (t, 2H, -CH<sub>2</sub>-), 7.704 (s, 1H, imidazolium ring), 7.779 (s, 1H, imidazolium ring), and 9.159 (s, 1H, imidazolium ring).

<sup>13</sup>C-NMR (400 MHz, DMSO-d<sub>6</sub>) (ppm): 26.050 (s, 1C, -CH<sub>2</sub>-), 35.677 (s, 1C, -CH<sub>3</sub>), 47.309 (s, 1C, -CH<sub>2</sub>-), 47.666 (s, 1C, -CH<sub>2</sub>-), 122.246 (s, 1C, imidazolium ring), 123.538 (s, 1C, imidazolium ring), and 136.710 (s, 1C, imidazolium ring).

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This work was financially supported by the National Natural Science Foundation of China (21506030).

## References

- S. Siankevich, Z. Fei, N. Yan and P. J. Dyson, *Chimia*, 2015, **69**, 592–596.
- L. Petrus and M. A. Noordermeer, *Green Chem.*, 2007, **38**, 861–867.
- S. H. Lee, T. V. Doherty, R. J. Linhardt and J. S. Dordick, *Biotechnol. Bioeng.*, 2009, **102**, 1368–1376.
- N. I. Haykir, E. Bahcegul, N. Bicak and U. Bakir, *Ind. Crops Prod.*, 2013, **41**, 430–436.
- T. Heinze, K. Schwikal and S. Barthel, *Macromol. Biosci.*, 2005, **5**, 520–525.
- Y. Dong, J. Holm, J. Kärkkäinen, J. Nowicki and U. Lassi, *Biomass. Bioenerg.*, 2014, **70**, 461–467.
- D. Fu, G. Mazza and Y. Tamaki, *J. Agric. Food Chem.*, 2010, **58**, 2915–2992.
- L. Wei, K. Li, Y. Ma and X. Hou, *Ind. Crops Prod.*, 2012, **37**, 227–234.
- Q. Li, Y. C. He, M. Xian, G. Jun, X. Xu, J. M. Yang and L. Z. Li, *Bioresour. Technol.*, 2009, **100**, 3570–3575.
- K. Ninomiya, K. Inoue, Y. Aomori, A. Ohnishi, C. Ogino, N. Shimizu and K. Takahashi, *Chem. Eng. J.*, 2015, **259**, 323–329.
- C. Li, B. Knierim, C. Manisseri, R. Arora, H. V. Scheller, M. Auer, K. P. Vogel, B. A. Simmons and S. Singh, *Bioresour. Technol.*, 2010, **101**, 4900–4906.
- D. Yang, L. X. Zhong, T. Q. Yuan, X. W. Peng and R. C. Sun, *Ind. Crops Prod.*, 2013, **43**, 141–149.
- J. Y. Kim, E. J. Shin, I. Y. Eom, K. Won, Y. H. Kim, D. Choi, I. G. Chio and J. W. Choi, *Bioresour. Technol.*, 2011, **102**, 9020–9025.
- J. K. Xu, Y. C. Sun and R. C. Sun, *Process Biochem.*, 2015, **50**, 955–965.
- A. D. Sluiter, B. Hames, R. Ruiz, C. Scarlata, J. Sluiter, D. W. Templeton and D. Crocker, NREL/TP-510-42618, National Renewable Energy Laboratory, Golden, CO, 2012.
- B. X. Zhang, Y. F. Wang and X. M. Hu, *Ind. Crops Prod.*, 2015, **76**, 688–696.
- L. C. Segal, J. J. Creely, A. E. J. Martin and C. M. Conrad, *Text. Res. J.*, 1959, **29**, 786–794.
- G. Cheng, P. Varanasi, C. Li, H. Liu, Y. B. Melnichenko, B. A. Simmons, M. Kent and S. Singh, *Biomacromolecules*, 2011, **12**, 933–941.
- G. L. Miller, *Anal. Chem.*, 1959, **31**, 175–201.
- N. Sun, H. Liu, N. Sathitsuksanoh, V. Stavila, M. Sawant, A. Bonito, K. Tran, A. George, K. L. Sale, S. Singh, B. A. Simmons and B. A. Holmes, *Biotechnol. Biofuels*, 2013, **6**, 39–52.
- N. Sun, M. Rahman, Y. Qin, M. L. Maxim, H. Rodriguez and R. D. Rogers, *Green Chem.*, 2009, **11**, 646–655.
- X. Wang, H. Li, Y. Cao and Q. Tang, *Bioresour. Technol.*, 2011, **102**, 7959–7965.
- H. T. Vo, C. S. Kim, B. S. Ahn, H. S. Kim and H. Lee, *J. Wood Chem. Technol.*, 2011, **31**, 89–102.
- J. Xu, B. Wu, L. Hu, Z. Wu, N. Xu, B. L. Dai and J. He, *Chem. Eng. J.*, 2015, **267**, 163–169.
- D. A. Fort, R. C. Remsing, R. P. Swatloski, P. Moyna, G. Moyna and R. D. Rogers, *Green Chem.*, 2007, **9**, 63–69.
- M. Lawoko, G. Henriksson and G. Gellerstedt, *Holzforschung*, 2006, **21**, 143–165.
- H. Wu, M. Mora-Pale, J. Miao, T. V. Doherty, R. J. Linhardt and J. S. Dordick, *Biotechnol. Bioeng.*, 2011, **108**, 2865–2875.
- D. Fu and G. Mazza, *Bioresour. Technol.*, 2011, **102**, 7008–7011.
- A. Pinkert, D. Goeke, K. N. Marsh and S. Pang, *Green Chem.*, 2011, **13**, 3124–3136.
- X. Pan, D. Xie, N. Gilkes, D. J. Gregg and J. N. Saddler, *Appl. Biochem. Biotechnol.*, 2005, **124**, 1069–1079.
- A. W. King, J. Asikkala, I. Mutikainen, P. Järvi and I. Kilpeläinen, *Angew. Chem., Int. Ed.*, 2011, **50**, 6301–6305.
- A. Casas, M. V. Alonso, M. Oliet, E. Rojo and F. Rodriguez, *J. Chem. Technol. Biotechnol.*, 2012, **87**, 472–480.
- W. Lan, C. F. Liu, F. Yue, R. C. Sun and J. F. Kennedy, *Carbohydr. Polym.*, 2011, **86**, 672–677.
- X. Chen, Y. Gao, L. Wang, H. Chen and N. Yan, *ChemPlusChem*, 2015, **80**, 1565–1572.
- W. Xiao, W. Yin, S. Xia and P. Ma, *Carbohydr. Polym.*, 2012, **87**, 2019–2023.
- L. Wu, A. Kumagai, S. H. Lee and T. Endo, *Bioresour. Technol.*, 2014, **162**, 207–212.
- A. Alemdar and M. Sain, *Bioresour. Technol.*, 2008, **99**, 1664–1671.
- T. Q. Yuan, T. You, W. Wang, F. Xu and R. C. Sun, *Bioresour. Technol.*, 2013, **136**, 345–350.
- A. M. Socha, S. P. Plummer, V. Stavila, B. A. Simmons and S. Singh, *Biotechnol. Biofuels*, 2013, **6**, 61–70.

