# **RSC Advances**



PAPER

View Article Online

View Journal | View Issue



Cite this: RSC Adv., 2017, 7, 42709

# PdZn nanoparticle electrocatalysts synthesized by solution combustion for methanol oxidation reaction in an alkaline medium†

M. A. Matin, A. Kumar, \*\* \* R. R. Bhosale, M. A. H. Saleh Saad, F. A. Almomani and M. J. Al-Marriab

Herein, we report the synthesis of PdZn nanoparticle (NP) electrocatalysts for the methanol oxidation reaction (MOR). The PdZn NPs were synthesized by solution combustion synthesis in the presence of  $Pd(NO_3)_2 \cdot xH_2O$ ,  $Zn(NO_3)_2 \cdot 6H_2O$  and glycine in  $H_2O$ , where glycine acted as a fuel. In this synthesis, the glycine amount was varied with a fixed stoichiometric ratio of Pd- and Zn-precursors at 1:1 to obtain two electrocatalysts (PdZn/C) of fuel-high (glycine to metal nitrate ratio = 1.75), PdZn/C (1.75) and fuellow (glycine to metal nitrate ratio = 0.5), PdZn/C (0.5). The NPs were characterized by X-ray diffractometry, transmission electron microscopy and scanning electron microscopy for the crystallite size, morphology and elemental composition of the electrocatalysts. High-angle annular dark-fieldscanning transmission electron microscopy coupled to energy dispersive X-ray spectroscopy was used to obtain the elemental distribution maps of the aggregated NPs, which confirmed the NPs with Pd and Zn in the alloyed state. X-ray photoelectron spectroscopy was performed to analyze the electronic structures of the elements in the samples. The NPs were then applied in the electrocatalysis for MOR in an alkaline medium. We found that PdZn/C showed an improved electrocatalytic activity by a factor of ~1.4-1.9 in comparison with Pd/C synthesized using the same method. The MOR on PdZn/C (1.75) began at an earlier onset potential and higher current density than for Pd/C and PdZn/C (0.5). Stability tests were performed by chronoamperometry on PdZn/C and Pd/C, and the results showed a higher stability of PdZn/C (1.75) compared to PdZn/C (0.5) and Pd/C. The fuel amount affected the NP sizes, reaction yield and electrocatalytic properties.

Received 23rd June 2017 Accepted 21st August 2017

DOI: 10.1039/c7ra07013f

rsc.li/rsc-advances

## Introduction

Fuel cells (FCs) are considered among the conceivable alternatives to fossil fuel energy resources as they can produce energy with fewer harmful exhausts and eventually contribute to the reduction of global warming and protection of the ecosystem. Recent research on FCs, associated with energy technologies, has shown that they could be utilized for diverse applications as a least-polluting energy source in household and commercial industries. FC energy is now expected to have a significant application in the future from the use of micro fuel cells for powering cell phones to high-powered FCs for vehicles and power stations. Among the various types of FCs, direct methanol fuel cells (DMFCs) are being intensively studied because of their low operating temperature and high energy conversion and efficiency. Furthermore, they are environment-friendly and

thus could be successfully used as a micro-power energy source. However, FCs require two types of catalysts, namely anode and cathode catalysts, to perform oxidation at the anode and reduction at the cathode, respectively.<sup>4-9</sup>

Platinum (Pt) and Pt-based electrocatalysts are the key catalyst materials for both anode and cathode of FCs in acidic media. However, a number of challenges associated with Pt such as high-cost, sluggish kinetics, scarcity and CO poisoning at the anode preclude the wider application of DMFCs at the anode side of FCs.3,9-17 Since palladium (Pd) is relatively more abundant in the earth's crust, Pd could be a better alternative for anodic electrode materials.18 In order to replace Pt completely at the anode side of FCs, many researchers have reported that Pd and Pd-based catalysts exhibit lower CO poisoning in alkaline media; their use would reduce the cost of the electrode materials as well as limit the excess utilization of Pt, which is considered a rare metal.2,19-25 The Pd catalysts are commonly synthesized by conventional methods, such as sol-gel, impregnation, solvothermal, sputtering, electrodeposition, co-deposition and coprecipitation. Some of these methods require multiple steps and the use of ancillary materials, whereas others require the use of specific techniques to attain the desired nanoparticle (NP)

<sup>&</sup>quot;Department of Chemical Engineering, Qatar University, P.O. Box 2713, Doha, Qatar. E-mail: akumar@qu.edu.qa

<sup>&</sup>lt;sup>b</sup>Gas Processing Center, Qatar University, P.O. Box 2713, Doha, Qatar

<sup>†</sup> Electronic supplementary information (ESI) available. See DOI: 10.1039/c7ra07013f

**RSC Advances** 

shape and size when these NPs are prepared at high temperature. As a result, these methods incur an increased disposable production cost and potential environmental consequences/ hazards.21,26-28 A reliable method is necessitated to reduce the production costs of the electrocatalysts and thus facilitate their widespread commercialization.

In 1967, Merzhanov et al.29 presented the concept of selfspreading high-temperature synthesis (SHS) for economically synthesizing advanced functional materials using self-sustained exothermic reactions. However, one major shortcoming of SHS was the difficulty in obtaining nanoparticles possessing a high surface area. Later, Patil et al.30 further developed this method in combination with wet chemistry and termed it as solution combustion synthesis (SCS). A wide variety of nanostructured materials has been synthesized by SCS based techniques for their applications in pigments, electronic and magnetic devices, and energy conversion and storage devices.31-34 With further recent innovations, the SCS technique has been used to synthesize a variety of nanomaterials for catalytic applications. 35-44

Previously, we used the SCS method for the synthesis of multi-component-nanostructured catalysts for hydrogen production from the reforming/decomposition of light natural gas/alcohol.31,32 In this study, we applied the SCS method for the synthesis of two PdZn NP electrocatalysts for the methanol oxidation reaction (MOR), where glycine: fuel ratio was varied maintaining a fixed ratio of Pd- and Zn-precursors at 1:1. The as-synthesized PdZn NP electrocatalysts were then applied for the electrooxidation of CH<sub>3</sub>OH. We found that PdZn electrocatalysts showed better electrocatalytic activity than a Pd NP electrocatalyst synthesized using the same method in terms of the onset potential, current density and stability with the MOR.

# Experimental

### Chemicals

The reagents palladium(II) nitrate hydrate (Pd(NO<sub>3</sub>)<sub>2</sub>, 97%), zinc(II) nitrate hexahydrate (Zn(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, 98%), glycine (99.7%) and Nafion solution (5 wt%) were purchased from Sigma-Aldrich. Potassium hydroxide (KOH, 85%) and carbon black (VXC72) were purchased from Riedel-de Haen and Cabot Corporation, respectively. Ultrapure water (Millipore, 18.2 M $\Omega$ cm) was used for the entire study. All the reagents were used without any further purification.

### **Synthesis**

Weighed amounts of Pd(NO<sub>3</sub>)<sub>2</sub>·xH<sub>2</sub>O, Zn(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O and glycine were mixed with 20 mL of de-ionized water (DIW) in a 250 mL beaker, and then the beaker was kept on a sonic vibrator until a homogeneous solution was obtained. Then, the beaker containing the reaction reagents was placed on a hotplate at 250 °C. The water evaporated overtime and after  $\sim$ 30 min, the catalysts were obtained at the end of the combustion reaction by self-ignition. The product was then ground using a mortar and a pestle to obtain uniform size of particles, and this was followed by sieving. In this way, we synthesized three catalysts in which the reaction ratios of the metal precursors of Pd(NO<sub>3</sub>)<sub>2</sub>: Zn(NO<sub>3</sub>)<sub>2</sub> were maintained at 1:1. The amount of glycine added in the mixture was calculated based on glycine to oxidizer ratio ( $\phi$ ) as defined in literature.31,32,38,41,45 The reactant ratios in the three samples  $(Pd(NO_3)_2 : Zn(NO_3)_2 : glycine (\phi))$  were 1:1:1.75 for PdZn (1.75), 1:1:0.5 for PdZn (0.5) and 1:0:1.75 for Pd, respectively. Then, 40% of the obtained catalyst powder was added to 60% of carbon support, dispersed in 7 mL DIW in a 50 mL beaker and then this mixture was heated to 125 °C until the water evaporated and the sample became completely dry. The schematic for the synthesis is shown in Fig. 1.

### Characterization techniques

X-ray diffraction (XRD) patterns were obtained using a powder X-ray diffractometer (Rigaku MiniFlexII Desktop, Cu-Kα radiation ( $\lambda = 1.54056 \text{ Å}$ )). To perform the morphological study of the samples by transmission electron microscopy (TEM, TECNAI G<sup>2</sup>, F20 FEI), a small amount of the sample was ultrasonically dispersed in ethanol, and then a few drops of the NPs-dispersed solution were deposited onto carbon-coated Cu-grids, followed by drying under ambient conditions. In order to obtain the elemental distribution in NPs, high angle annular dark field (HAADF)-scanning transmission electron microscopy (FEI Talos F200X STEM) coupled to energy dispersive X-ray spectroscopy (FEI SuperX EDS system) was conducted. The elemental compositions and morphology of the particles in the samples were obtained using an energy dispersive X-ray spectroscopy analyzer coupled to a field-emission scanning electron microscope (SEM, Nova Nano 450, FEI). X-ray photoelectron spectroscopy (XPS, Kratos AXIS Ultra DLD) was conducted to analyze the oxidation state of the elements in the samples, and the reported binding energies (BEs) obtained from the XPS data were calibrated with respect to C 1s at 284.8 eV.

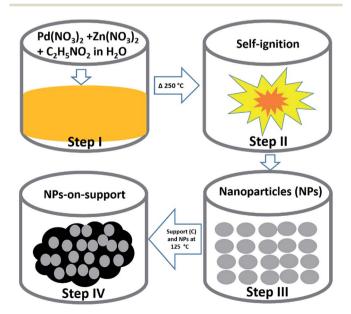


Fig. 1 A schematic of the SCS technique.

Paper **RSC Advances** 

### **Electrode fabrication**

A homogeneous dispersion of 15 mg of a sample in 5 g of distilled water was obtained with the help of a sonicator. Furthermore, 20 µL of the dispersion was added dropwise by a calibrated micro-pipette onto the surface of a glassy carbon rotating disc electrode (RDE, d = 5.0 mm and geometric area, A = 0.196 cm<sup>2</sup>). The catalyst-coated electrode surface was dried under ambient conditions and then, 20 µL of 0.125 wt% Nafion solution was added on top of it to prevent the electrode materials from coming off the RDE surface.

### **Electrochemical measurements**

For all electrochemical measurements, a Pine instruments biopotentiostat (WaveDriver 20) was used to evaluate the electrochemical activity along with a standard three-electrode electrochemical cell consisting of a glassy carbon RDE coated with the catalyst as a working electrode, a Hg/Hg<sub>2</sub>SO<sub>4</sub> in 4 M K<sub>2</sub>SO<sub>4</sub> reference electrode, and a Pt-coil counter electrode. The working electrode was electrochemically pre-treated at a scan rate of 500 mV s<sup>-1</sup> for 100 cycles prior to each measurement in the potential range from 0.1 to -0.6 V. Cyclic voltammograms (CVs) were measured in 1 M KOH aqueous solution in the potential range from 0.2 to -1.3 V at a scan rate of 50 mV s<sup>-1</sup> under an  $N_2$  atmosphere. The electrocatalytic activity for the MOR was investigated by CVs in 1 M KOH containing 2 M CH<sub>3</sub>OH at a scan rate of 50 mV s<sup>-1</sup> in the potential range from 0.5 to -0.8 V. Chronoamperometry was performed for the stability tests at 0.325 V using the same electrolyte with RDE (350 rpm) under an N2-ambient for 2 h.

All the electrochemical measurements were performed at room temperature under ambient pressure, and a fresh electrolyte bubbled by N2-purging for 1 h was used for each measurement. The current densities obtained from the CVs were normalized with respect to the geometric surface area of the RDE, while the current densities obtained from the CVs for the MOR along with the chronoamperometric curves were normalized with respect to the amount of Pd used in the electrocatalytic activity.

# Results and discussion

### Structural characterization

PdZn/C electrocatalysts were synthesized by the SCS method in the presence of Pd(NO<sub>3</sub>)<sub>2</sub>·xH<sub>2</sub>O, Zn(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O and glycine in H<sub>2</sub>O, where glycine acted as a fuel. In each reaction, the ratios of weighed amounts of Pd- and Zn-precursors were fixed at 1:1 for the two electrocatalysts, in which the glycine amount was varied according to the fuel to oxidizer ratio parameter  $(\phi)^{31,32,38,41,45}$ with a ratio of 1.75 for Pd: Zn: glycine (1:1:1.75) and 0.5 for Pd: Zn: glycine (1:1:0.5), respectively. These two electrocatalysts were termed here as PdZn/C (1.75) and PdZn/C (0.5) based on the glycine amount on the addition of the carbon support into them. In order to compare the electrocatalytic activity of the two PdZn/C NP electrocatalysts, we synthesized a Pd/C NP sample using the same method in which the ratio of the Pd-precursor : glycine-fuel  $(\phi)$  was 1 : 1.75. We also

synthesized Zn NPs using the same method in which the ratio of the Zn-precursor and glycine-fuel ( $\phi$ ) was 1:1.75 for comparison with the XRD patterns of Zn in PdZn/C. In this study, we aimed to observe the effect of the fuel amount on the synthesis of the two PdZn/C electrocatalysts to tune their physiochemical properties and NP size for improving their electrochemical properties.

Fig. 1 shows a schematic of the SCS technique. SCS is a redox based reaction that takes place in a homogeneous aqueous solution of oxidizing agents such as metal nitrates, and reducing agents such as glycine. Step I in Fig. 1 involves obtaining a homogeneous solution of starting materials. Then, the beaker is placed on a hotplate where the temperature is maintained at ~250 °C in an open-air atmosphere until selfignition occurs in step II. The solution becomes concentrated overtime. Once self-ignition occurs, energy is produced simultaneously because the reaction takes place exothermically. 31,32,34 The energy produced by the system is sufficient to synthesize crystalline materials. This is how NPs are obtained in SCS. In step III, the particle size is uniformly obtained by sieving. For the application of MOR, a physical mixture of NPs and support (carbon black) is proposed at step IV.

We obtained a mixture of 40% of each synthesized sample with 60% carbon support in 7 mL DIW via use of a sonic vibrator and then heated the mixture to 125 °C with the help of a hotplate for complete drying. We carried out elemental analysis of the carbon-supported samples by SEM. The elemental compositions of Pd/C and PdZn/C were averaged from three measurements at different regions of each sample. The compositions analyzed by SEM showed that the reaction yield was almost quantitative (83.32-92.45%) based on the total weight of Pd and Zn (Table S1†), and the atomic ratios of Pd and Zn in the samples were 1: 1.54 for PdZn/C (1.75) and 1: 1.73 for PdZn/C (0.5), respectively. The SEM analysis for the compositions suggested that the electrocatalysts were Zn-enriched, where the fuel amount in the synthesis played a key role in the distribution of a Zn-high/low content in the samples. One image and its spectrum from each sample are shown in Fig. 2.

Fig. 3 shows the XRD patterns for Pd/C, PdZn/C (1.75) and PdZn/C (0.5). The peak positions at  $2\theta$  of  $39.5^{\circ}$ ,  $46.1^{\circ}$ , and  $67^{\circ}$ are attributed to the planes corresponding to (111), (200), and (220) of the face centered cubic structure (fcc) of Pd, respectively. The peak position at  $2\theta$  of  $\sim 24.9^{\circ}$  was assigned to the carbon support corresponding to the C (002) plane. XRD patterns of the two bimetallic PdZn/C electrocatalysts showed similar characteristic patterns with Pd/C but the peak positions at  $2\theta$  for PdZn/C were shifted positively by 0.28 for PdZn/C (1.75) and 0.03 for PdZn/C (0.5) compared to those for Pd/C. The presence of other detectable peaks in the PdZn/C patterns at  $2\theta$ values of  $31.2^{\circ}$ ,  $33.8^{\circ}$ ,  $35.7^{\circ}$ ,  $55.7^{\circ}$  and  $61.8^{\circ}$  were attributed to the (100), (002), (101), (110) and (103) planes of ZnO NP, respectively. These XRD patterns were confirmed by comparing them with the XRD patterns (Fig. S1†) of the synthesized ZnO obtained in the same manner as shown in literature.45 The shift of XRD patterns towards the positive direction indicates that the Zn element is incorporated into the Pd lattice to form an alloy, in accordance with reports on Pd alloyed with 3d transition

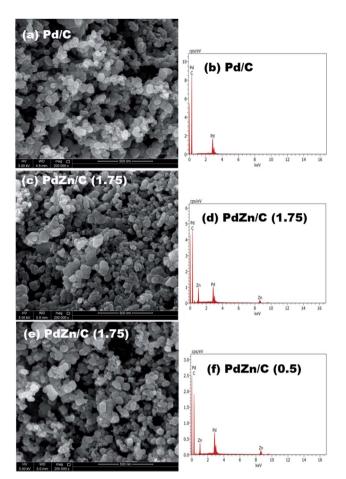


Fig. 2 Compositional analysis with SEM, and the images and spectra on (a) and (d) Pd/C, (b) and (e) PdZn/C (1.75), and (c) and (f) PdZn/C (0.5).

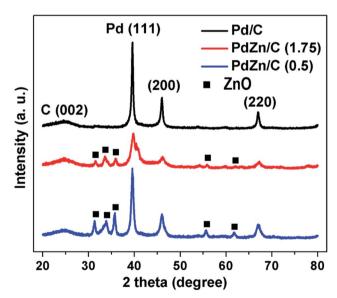


Fig. 3 XRD patterns of Pd/C, PdZn/C (1.75) and PdZn/C (0.5).

metals. $^{23,46-51}$  The presence of other crystal phases suggests that the alloy elements are not uniformly distributed within the PdZn NPs. Iwasa  $et\ al.$ , $^{46}$  Tew  $et\ al.$  $^{47}$  and Chin  $et\ al.$ 

independently reported on PdZn alloy formation with XRD observations at 200 °C, 250 °C and 350 °C, respectively, and the composition of the alloys varied with increasing temperature. In the SCS process, the combustion temperature goes up to  $\sim\!600$  °C in an open-air atmosphere. Based on the phase-diagram, <sup>52</sup> the elements of Pd and Zn could form an alloy in a wide range of compositions ( $\sim\!32\text{--}85\%$  of Zn with Pd) at a broader temperature range. The atomic ratios (61–63% of Zn with Pd (Table S1†)) of our samples and the synthetic temperature are in line with another report. <sup>52</sup> Chen *et al.* <sup>53</sup> carried out a study on PtZn and PdZn alloy formation to assess their surface structures and stabilities using density functional model theory (DFMT) and obtained an fcc structure with lattice parameters of a=3.89 Å and 3.92 Å and an hcp structure with lattice

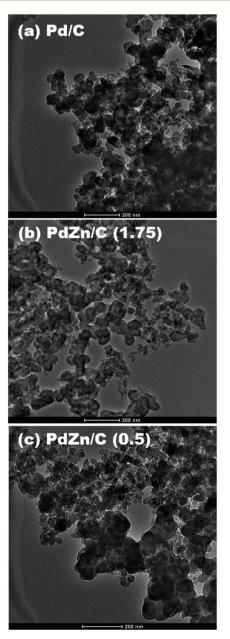


Fig. 4 TEM images of (a) Pd/C, (b) PdZn/C (1.75) and (c) PdZn/C (0.5).

Paper

(a) PdZn/C (1.75) STEM-HAADF (b) Pd (c) Zn (c) Pd+Zn

Fig. 5 (a) STEM-HAADF image, and EDS elemental maps of (b) Pd, (c) Zn, (d) Pd + Zn on PdZn/C (1.75).

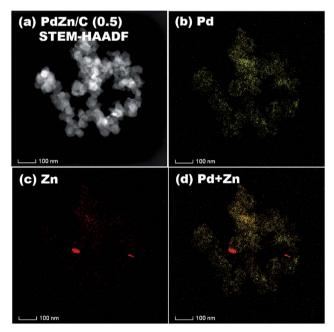


Fig. 6 (a) STEM-HAADF image and EDS elemental maps of (b) Pd, (c) Zn, (d) Pd + Zn on PdZn/C (0.5).

constants, a=2.6649 Å and c=4.9468 Å for Pd and Pt, and Zn, respectively. According to the DFMT, Pd and Zn are readily miscible and form alloys in a broad range of compositions, where different compositions produce different structures. Later, their DFMT was experimentally implemented and verified by other groups. 54–56 In addition, Penner *et al.* 51 studied the growth and structural stability of PdZn alloy formation on SiO<sub>2</sub> using TEM along with selected area electron diffraction patterns

at high resolution, and they found that the alloy, PdZn NPs, was well ordered.

Literature studies indicate that Pd and Zn could form alloys under different conditions with different synthesis methods for a broad range of compositions and temperatures. We believe that the macroscopic-phase-segregation observed using XRD for the PdZn/C samples is dependent on the formation of an orderly alloy and the Zn-content in samples. The crystallite sizes of the samples calculated at the (111) plane using Scherrer's equation<sup>49</sup> are shown in Table S1.† The trend of crystallite sizes (Table S1†) was Pd/C > PdZn/C (0.5) > PdZn/C (1.75). It is noted that the fuel-amount could affect the particle size.

Fig. 4 shows the TEM images of the three samples. It could be observed that NPs of the samples are well distributed on the carbon support, but NPs aggregation was present on all the samples with spherical shapes. Agglomeration is one of the inherent properties of NPs synthesized by SCS. Herein, the NPs of PdZn/C (1.75) show less agglomeration when a higher fuel-amount is used in the synthesis.

STEM-HAADF coupled to EDS was conducted for analysis of the elemental distribution in the NPs of both bimetallic electrocatalysts, and the results are shown in Fig. 5 for PdZn/C (1.75) and Fig. 6 for PdZn/C (0.5), respectively. The EDS elemental distribution shown in Fig. 5 indicates that the Pd element is fairly alloyed with the Zn element in the aggregated NPs. However, there are additional Zn signals detected outside of the NPs on the carbon support. These signals on the carbon support outside of the aggregated NPs correspond to ZnO and are seen in both bimetallic electrocatalysts in the XRD observations. The elemental distribution map of C in both electrocatalysts is shown in Fig. S2 and S3† as well as in the images shown in Fig. 5 and 6 for a clearer observation. In the case of PdZn/C (0.5), an almost similar observation was seen in the EDS elemental distribution of Pd and Zn throughout the aggregated NPs on the carbon support (Fig. 6). There are highly intensified Zn signals

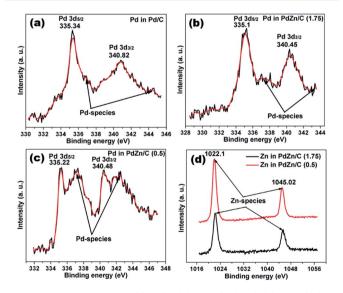


Fig. 7 XPS data spectra of (a) Pd/C, (b) PdZn/C (1.75), (c) PdZn/C (0.5) and (d) Zn in PdZn/C (1.75) and PdZn/C (0.5).

**RSC Advances** 

seen in two areas in Fig. 6(c) that are assigned to the aggregation of ZnO NPs. It is noted that one can see that there are some signals in Fig. S2 and S3† for each element map where there is no carbon support. These signals correspond to the background noise detected by the instrument.

### Oxidation state of the elements

The XPS spectra of Pd/C and PdZn/C are depicted in Fig. 7. The peaks of Pd 3d<sub>5/2</sub> and Pd 3d<sub>3/2</sub> on the Pd/C sample appear at 335.34 and 340.82 eV, respectively, which are in good agreement with those reported in literature. 57,58 The numerical values of the XPS spectra peaks are listed in Table S2.† These XPS peaks in the PdZn/C samples (Table S2†) are shifted towards lower BEs by 0.12-0.24 eV, which can be ascribed to the charge-transfer from Zn to Pd because of difference in their electronegativity (Zn (1.6) and Pd (2.2)). Hammer and Norskov<sup>59</sup> reported on dband model theory, in which the charge-transfer to Pd can induce a down-shift of the Pd d-band center, thus influencing the Pd-adsorbate interaction. As a result, the charge transfer

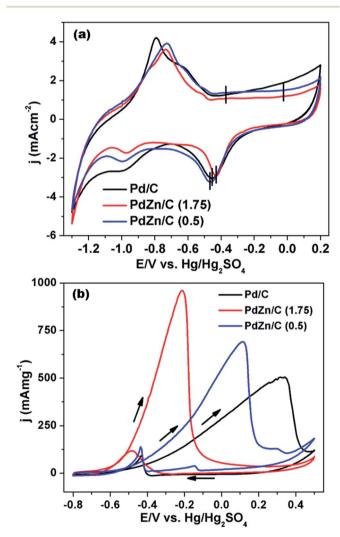


Fig. 8 CVs of (a) Pd/C, PdZn/C (1.75) and PdZn/C (0.5) in 1 M KOH at 50 mV s $^{-1}$  and (b) MOR on Pd/C, PdZn/C (1.75) and PdZn/C (0.5) in 1 M KOH containing 2 M  $\rm CH_3OH$  at 50 mV  $\rm s^{-1}$  under a  $\rm N_2$  environment.

process can weaken the interaction between Pd and the intermediate species produced during the MOR. Kibler et al. 60 and Zhang et al.61 individually studied that the down-shift of the dband center enhances the electrocatalysis on small organic molecules. The XPS peaks appearing at 336.91-337.23 eV and 342.43-344.39 eV BEs on Pd/C and PdZn/C correspond to the Pd-species of PdO and Pd(OH)2,62 respectively. The XPS spectra analysis shows the presence of Zn-species at 1021.93 eV and 1045.02 eV for PdZn/C (0.5) and 1022.3 eV and 1045.3 eV for PdZn/C (1.75), which are assigned to ZnO and agree with those reported in literature. 63 These BEs on the Pd-species and Znspecies vary with the nature of the samples and the magnitude of the charge transfer from Zn to Pd. The elements of PdZn/C (1.75) show relatively more metallic character than PdZn/C (0.5) based on the SCS method, but the XPS peaks on Zn in PdZn/C (1.75) show higher BEs because of the higher electronic interaction between Pd and Zn.

## Electrocatalysis

Fig. 8(a) compares the CVs among the Pd/C and PdZn/C electrocatalysts. The CVs were measured in an electrolyte of 1 M KOH at 50 mV s<sup>-1</sup> under a N<sub>2</sub>-ambient condition. As shown in Fig. 8(a), the CVs of Pd/C and PdZn/C exhibit the typical characteristics of Pd containing electrocatalysts. The CV peaks of Pd/ C at about -0.795 V and -0.628 V match with the hydrogen desorption as reported in the literature<sup>64</sup> on the (100) and (111) planes, respectively. The CV peak at about -0.368 V of Pd/C in the forward scan is assigned to oxide formation and that at -0.454 V in the backward scan to decomposition. The CV peaks of PdZn/C at about -0.728 V and -0.515 V are attributed to hydrogen-adsorption in the forward scan. The hydrogen adsorption/desorption and oxide formation/decomposition peaks for Pd/C are not similar to PdZn/C, suggesting that the electrocatalysts are composed of bimetallic NPs. The CV peaks of PdZn/C are shifted positively by about -341 mV for oxideformation on PdZn/C, -35 mV for that on PdZn/C (1.75), and -15 mV for that on PdZn/C (0.5) as compared to those for the decomposition from Pd/C. The onset potentials of oxideformation and decomposition for PdZn/C to a higher positive potential are evidence of the bimetallic electrocatalysts preventing the chemisorption of the hydroxyl species on the catalyst surface, which correlates with the down-shift of the Pd dband center. The adsorbed hydroxyl species on the catalyst surface hinder small molecules (formic acid/methanol/ethanol) oxidation reactions.65 The suppression of hydroxyl formation on the PdZn/C surface is observed in the CVs, and it is found to enhance the electrocatalytic activity of MOR. The electrochemical surface areas (ECSAs) calculated from the hydrogendesorption regions (2nd cycle of 3 in Fig. S4†) are shown in Table S1.† The trend for the ECSAs (Table S1†) is Pd/C > PdZn/C (0.5) > PdZn/C (1.75), and this trend does not follow the crystallite size obtained using XRD data. Upon the formation of an alloy with Pd and Zn in PdZn, the NPs can affect the ECSAs and the down-shift of the Pd d-band center may weaken the binding energy of the Pd atoms.

In order to study the electrochemical activity on Pd/C and PdZn/C electrocatalysts, the MOR was conducted using CV in an electrolyte of 1 M KOH containing 2 M CH<sub>3</sub>OH at a 50 mV s<sup>-1</sup> in an N2-ambient condition. As seen in Fig. 8(b), the onset of potential for PdZn/C (1.75) is negatively shifted by about -125 mV and −92 mV compared to that of Pd/C and PdZn/C (0.5), respectively. The poison tolerance ratio (PTR) of the forward and backward currents is 8.2 on PdZn/C (1.75) and 5 on PdZn/C (0.5)  $\equiv Pd/C$ , whereas many reports on PTR provide a value of about 1.0 (ref. 22, 62 and 66) in alkaline media. In general, the backward current is assigned to carbonaceous species formed during the MOR. The PTR ratio and the intensity of the backward current for all the electrocatalysts show that the MOR is nearly complete in the forward scan. The reaction kinetics of CH<sub>3</sub>OH is greatly enhanced on PdZn/C compared to Pd/C. According to the kinetics studies reported in the literature,67,68 the dissociation of oxygenated species, such as O and OH, are the rate limiting steps for small molecules oxidation/ reduction reactions. As observed in Fig. 8(a), the CV peaks for the oxide formation/decomposition on PdZn/C are at higher potentials than those of Pd/C. This indicates that PdZn NPs are less oxophilic than Pd/C. One can expect that a less oxophilic NPs surface can get rid of oxygenated species more easily and thus refresh the catalyst surface faster than that of Pd/C. This would result in more active sites being free on a bimetallic electrode surface for further quicker adsorption of CH<sub>3</sub>OH. Since the down-shift of the Pd d-band in the PdZn/C samples is seen in the XPS analysis, it can be inferred that the intermediate species generated in the MOR are less adsorbed on the catalyst surface. This study agrees with reports in the literature. 59-61 Zn itself is an oxophilic element and can produce a synergistic effect with an electrolyte of alkaline media to release the intermediate species generated by the MOR. This is how the electrode surface can get more active sites for the adsorption of CH<sub>3</sub>OH, thereby, leading to an enhancement in electrocatalysis as well as in the MOR kinetics on the PdZn/C samples. The

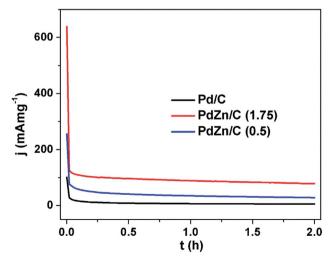


Fig. 9 Chronoamperometric curves of Pd/C, PdZn/C (1.75) and PdZn/ C (0.5) in 1 M KOH containing 2 M CH<sub>3</sub>OH at 0.325 V under a N<sub>2</sub> environment for 2 h at 350 rpm.

current densities at the forward scan of each electrocatalyst were normalized by the amount of Pd used in the measurement of the MOR activity (Table S1†). The electrocatalytic activity for MOR is ~1.9 times for PdZn/C (1.75) and ~1.4 times for PdZn/C (0.5) higher than that of Pd/C. This is a significant step ahead for application in DMFCs and meets one of the key criteria for fuel cells application that the catalyst should produce the highest current density at the lowest potential. The current densities were also normalized by ECSAs (Fig. S5(a)†). The normalization factor used for the ECSAs affects the trend of the current density normalized by the Pd amount in the samples.

The stability test is one of the key factors for assessing suitability for FCs application. Stability tests were performed on all the electrocatalysts using the chronoamperometry technique in an electrolyte of 1 M KOH containing 2 M CH<sub>3</sub>OH for a period of 2 h (Fig. 9) in a N<sub>2</sub>-ambient condition. The chronoamperometric curves in Fig. 9 demonstrate that the MOR on the PdZn/C electrocatalysts commences at high potentiostatic currents compared to Pd/C. The potentiostatic currents sharply decrease at ~62 s for Pd/C and ~85 s for PdZn/C, respectively. This phenomenon, observed on all the electrocatalysts, was due to adsorption of the reaction intermediates formed during CH<sub>3</sub>OH oxidation, hydrogen and oxygen species from the electrolyte, the dissolution/leaching of some Zn and bilayer discharge. These reasons are found in many reports 17,21,23,26,66,69,70 for explaining the significant decay of the electrochemical performance at the very beginning of the oxidation of small molecules in acidic and alkaline media. After the sharp decrease at 62-85 s, the performance of the as-synthesized electrocatalysts remained firmly stable over a period of 2 h in an electrochemical environment. PdZn/C (1.75) showed the highest stability over both Pd/C and PdZn/C (0.5) based on the current densities normalized by both the Pd amount in the samples and the ECSAs from the CVs (Fig. 5(b)).

# Conclusions

We successfully synthesized PdZn/C and Pd/C electrocatalysts by the SCS method and used them for the MOR in an alkaline medium. The NP electrocatalysts were characterized by XRD, TEM and SEM for the crystallite size, morphology and composition of the elements in the samples. The EDS elemental distribution throughout the NPs showed that the NPs were composed of Pd and Zn elements in the alloyed state. The electronic structure of Pd modified by the incorporation of Zn was proved by XPS analysis, which confirmed the down-shift of the d-band center on Pd. Agglomerated NPs observed by TEM were employed for the electrocatalysis of CH<sub>3</sub>OH. We found that PdZn/C showed better electrocatalytic performance by a factor of  $\sim$ 1.4–1.9 in comparison with Pd/C. Among the electrocatalysts, PdZn/C (1.75) showed the highest current density on the MOR at the earliest onset potential, thus meeting one of the key criteria for DMFCs application. The stability tests conducted using chronoamperometry showed that PdZn/C (1.75) was more stable in an electrochemical environment compared to Pd/C and PdZn/C (0.5). We found that the variation of the fuel

amount affected the NP sizes, electronic structure and electrochemical properties in the two samples.

# Conflicts of interest

There are no conflicts of interest to declare.

# Acknowledgements

This publication was made possible by NPRP grant (NPRP8-509-2-209) from the Qatar National Research Fund (a member of Qatar Foundation). The statements made herein are solely the responsibility of the author(s). The authors also gratefully acknowledge the Gas Processing Centre (GPC), the Central Laboratory Unit (CLU) at Qatar University and Qatar Environment and Energy Research Institute (QEERI) at Qatar Foundation for services related to XPS analysis, electron microscopy and STEM-HAADF-EDS, respectively.

# Notes and references

- 1 W. Winter and R. J. Brodd, Chem. Rev., 2004, 104, 4245.
- 2 X. Li, M. Wen, D. Wu, Q. Wu and J. Li, J. Alloys Compd., 2016, 685, 42.
- 3 H. Zhao, C. Yu, H. You, S. Yang, Y. Guo, B. Ding and X. Song, I. Mater. Chem., 2012, 22, 4780.
- 4 K. Maharaju and L. Cindrella, RSC Adv., 2014, 4, 11939.
- 5 J. H. Lin, T. H. Tse and M. Y. Yen, *Energy Fuels*, 2009, 23, 4042.
- 6 J. Speder, L. Altmann, M. Baumer, J. J. K. Kirkensgaard and K. Mortasen, *RSC Adv.*, 2014, 4, 14971.
- 7 S. Y. Huang, S. M. Chan, C. L. Lin, C. H. Chen and C. T. Yeh, J. Phys. Chem. B, 2006, 110, 23300.
- 8 A. D. Moore, S. M. Holmes and E. P. L. Roberts, *RSC Adv.*, 2012, **2**, 1669.
- 9 L. Gao, W. Yue, S. Tao and L. Fan, *Langmuir*, 2013, **188**, 957.
- 10 Z. L. Liu, X. Y. Ling, B. Guo, L. Hong and J. Y. Lee, *J. Power Sources*, 2007, **167**, 272.
- 11 K. Eid, Y. H. Ahmad, S. Y. Alqaradawi and N. K. Allam, *Catal. Sci. Technol.*, 2017, 7, 2819.
- 12 X. R. Jiang, T. M. Guer, F. B. Prinz and S. B. Bent, *J. Electrochem. Soc.*, 2010, **147**, B314.
- 13 W. Wang, Q. Huang, J. Liu, Z. Zou, Z. Li and H. Yang, *Electrochem. Commun.*, 2008, **10**, 1396.
- 14 Y. C. Wei, C. W. Liu, Y. W. Chang, C. M. Lai, P. Y. Lim and L. D. Tsai, *Int. J. Hydrogen Energy*, 2010, 35, 1864.
- 15 S. K. Meher and G. R. Rao, ACS Catal., 2012, 2, 2795.
- 16 A. B. A. A. Nassr and M. Bron, ChemCatChem, 2013, 5, 1472.
- 17 M. A. Matin, E. Lee, H. Kim, W.-S. Yoon and Y.-U. Kwon, *J. Mater. Chem. A*, 2015, 3, 17154.
- 18 Z. J. Mellinger, T. G. Kelly and J. G. Chen, ACS Catal., 2012, 2, 751.
- 19 F. Kadirgan, S. Beyhan and T. Atilan, *Int. J. Hydrogen Energy*, 2009, 34, 4312.
- 20 C. T. Hsieh, Y. Y. Liu and A. K. Roy, *Electrochim. Acta*, 2012, **64**, 205.
- 21 C. T. Hsieh, P. O. Yu, D. Y. Tzou, J. P. Hsu and Y. R. Chiu, *J. Electroanal. Chem.*, 2016, **761**, 28.

- 22 Y. Ren, S. Zhang and H. Li, Int. J. Hydrogen Energy, 2014, 39, 288.
- 23 Y. Song, X. Zhang, S. Yang, Z. Wei and Z. Sun, *Fuel*, 2016, **181**, 269
- 24 A. I. C. Hidalgo, M. R. Aguirre, E. Valenzuela, J. Y. V. Gomez, A. C. Davila, R. S. Varma and V. H. R. Sanchez, *Int. J. Hydrogen Energy*, 2016, 41, 23329.
- 25 M. A. Alvi and M. S. Akhtar, J. Alloys Compd., 2016, 684, 524.
- 26 L. Dai and S. Zou, J. Power Sources, 2011, 196, 9369.
- 27 C. Du, M. Chen, W. Wang and G. Yin, ACS Appl. Mater. Interfaces, 2011, 3, 105.
- 28 H. Wang, Z. Sun, Y. Yang and D. Su, Nanoscale, 2013, 5, 139.
- 29 A. G. Merzhanov, Ceram. Int., 1995, 21, 371.
- 30 J. Kingsley and K. C. Patil, Mater. Lett., 1988, 6, 427.
- 31 A. Kumar, A. S. Mukasyan and E. E. Wolf, *Appl. Catal., A*, 2011, **401**, 20.
- 32 A. Cross, A. Kumar, E. E. Wolf and A. S. Mukasyan, *Ind. Eng. Chem. Res.*, 2012, **51**, 12004.
- 33 S. L. Gonzalez-Cortes and F. E. Imbert, *Appl. Catal.*, *A*, 2013, 452, 117.
- 34 F. T. Li, J. Ran, M. Jaroniec and S. Z. Qiao, *Nanoscale*, 2015, 7, 17590.
- 35 A. Kumar, E. Wolf and A. Mukasyan, *AIChE J.*, 2011, **57**, 3473.
- 36 A. Kumar, E. Wolf and A. Mukasyan, AIChE J., 2011, 57, 2207.
- 37 A. Kumar, A. S. Mukasyan and E. E. Wolf, *Ind. Eng. Chem. Res.*, 2010, 49, 11001.
- 38 A. Ashok, A. Kumar, R. R. Bhosale, M. A. H. Saleh, V. D. Broeke and J. P. Leo, RSC Adv., 2015, 5, 28703.
- 39 A. Ashok, A. Kumar, R. R. Bhosale, M. A. H. Saleh, U. K. Ghosh, M. Al-Marri, F. A. Almomani, M. M. Khader and F. Tarlochan, *Ceram. Int.*, 2016, 42, 12771.
- 40 A. Kumar, A. Ashok, R. R. Bhosale, M. A. H. Saleh, F. A. Almomani, M. Al-Marri, M. M. Khader and F. Tarlochan, *Catal. Lett.*, 2016, 146, 778.
- 41 A. Kumar, A. Mukasyan and E. Wolf, Appl. Catal., A, 2010, 372, 175.
- 42 G. Carotenuto, A. Kumar, J. Miller, A. S. Mukasyan, E. Santacesaria and E. E. Wolf, *Catal. Today*, 2013, **203**, 163.
- 43 A. Kumar, J. T. Miller, A. S. Mukasyan and E. E. Wolf, *Appl. Catal.*, *A*, 2013, **467**, 593.
- 44 A. Kumar, A. Cross, K. Manukyan, R. R. Bhosale, J. P. Leo, V. D. Broeke, J. T. Miller, A. S. Mukasyan and E. E. Wolf, *Chem. Eng. J.*, 2015, **278**, 46.
- 45 A. K. Zak, W. H. A. Majid, M. E. Abrishami and R. Yousefi, *Solid State Sci.*, 2011, 13, 251.
- 46 N. Iwasa, T. Mayanagi, S. Masuda and N. Takezawa, *React. Kinet. Catal. Lett.*, 2000, **2**, 355.
- 47 M. W. Tew, H. Emerich and J. A. Bokhoven, *J. Phys. Chem. C*, 2011, **115**, 8457.
- 48 Y.-H. Chin, R. Dagle, J. Hu, A. C. Dohnalkova and Y. Wang, *Catal. Today*, 2002, 77, 79.
- 49 M. A. Matin, J.-H. Jang and Y.-U. Kwon, *J. Power Sources*, 2014, 262, 356.
- 50 N. Tekezawa and N. Iwasa, Catal. Today, 1997, 36, 45.
- 51 S. Penner, B. Jenewein, H. Gabasch, B. Klotzer, D. Wang, A. Knop-Gericke, R. Schlogl and K. Hayek, *J. Catal.*, 2006, **241**, 14.
- 52 H. Okamoto, in *Binary Alloy Phase Diagrams*, ed. T. B. Massalski, 1990, p. 3068.

- Paper
- 53 Z. X. Chen, K. M. Neyman, A. B. Gordienko and N. Rosch, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 2003, **68**, 075417.
- 54 H. Gabasch, A. Knop-Gericke, R. Schlogl, S. Penner, B. Jenewein, K. Hayek and B. Klotzer, *J. Phys. Chem. B*, 2006, **110**, 11391.
- 55 E. Jeroro, L. Lebarbier, A. Datye, Y. Wang and J. M. Vohs, *Surf. Sci.*, 2007, **601**, 5546.
- 56 G. Weirum, M. Kratzer, H. P. Koch, A. Tamtogl, J. Killmann, I. Bako, A. Winkle, S. Surnev, F. P. Netzer and R. Schennach, J. Phys. Chem. C, 2009, 113, 9788.
- 57 L. Chen, H. Guo, T. Fjujita, A. Hirata, W. Zhang, A. Inoue and M. Chen, *Adv. Funct. Mater.*, 2011, 21, 4364.
- 58 W. Wang, S. Ji and H. Wang, Fuel Cells, 2012, 12, 1129.
- 59 B. Hammer and J. K. Norskov, Adv. Catal., 2000, 45, 71.
- 60 L. A. Kibler, A. M. El-Aziz, R. Hoyer and D. M. Kolb, *Angew. Chem., Int. Ed.*, 2005, 44, 2080.
- 61 Z. Zhang, J. Ge, L. Ma, J. Liao, T. Lu and W. Xing, *Fuel Cells*, 2009, 9, 114.

- 62 Y. Feng, D. Bin, b. Yan, Y. Du, T. Majima and W. Zhou, *J. Colloid Interface Sci.*, 2017, **493**, 190.
- 63 M. C. Biesinger, L. W. M. Lau, A. R. Gerson and R. St. C. Smart, *Appl. Surf. Sci.*, 2010, 257, 887.
- 64 M. Jin, H. Zhang, Z. Xie and Y. Xia, Energy Environ. Sci., 2012, 5, 6352.
- 65 L. Zhang, L. Wan, Y. Ma, Y. Chen, Y. Zhou, Y. Tang and T. Lu, Appl. Catal., B, 2013, 138–139, 229.
- 66 S. R. Chowdhury, S. Ghosh, S. Kumar and S. K. Bhattachrya, *Electrochim. Acta*, 2017, 225, 310.
- 67 J. X. Wang, N. M. Markovic and R. R. Adzic, J. Phys. Chem. B, 2004, 108, 4127.
- 68 J. X. Wang, J. L. Zhang and R. R. Adzic, J. Phys. Chem. A, 2007, 111, 12702.
- 69 R. Shi, J. Wang, N. Cheng, X. Sun, L. Zhang, J. Zhang and L. Wang, *Electrochim. Acta*, 2014, **148**, 1.
- 70 H. A. Gasteiger, S. S. Kocha, B. Somalli and F. T. Wagner, *Appl. Catal.*, *B*, 2005, **56**, 9.