1. Introduction

With the economic globalization and the large-scale development of industrialization, water pollution of heavy metals caused by a large amount of sewage from chemical plants and mining fields, has attracted a lot of research attention. Mercury, one of the most toxic pollutants exhibiting properties of persistence, bioaccumulation and migration, can enter the human body through the food chain, causing irreversible serious damage to human body function and the nervous system.

In many countries, mercury pollution incidents occur frequently. In the 1980s in China, several serious mercury pollution incidents, occurring along the Songhua River, in the lower reaches of Tianjin Jiyun River and Jinzhou Bay in Liaoning Province, etc. greatly attracted people’s attention. So, it is imperative to solve the problem of mercury pollution in water.

To solve this issue, there are many methods developed for the recovery of mercury, such as precipitation, ion exchange, physical separation and microbiological method and so on. Nevertheless, these technologies always have shortcomings like poor removal capacity, low metal removal efficiency and the risk of secondary pollution. Hence, it is necessary to explore economic and effective technologies to treat the pollution.

Adsorption has been recognized as an economic and highly effective method used in water treatment due to its cost-effective and efficient. However, most of adsorbent materials have some issues like poor regeneration, easy to produce secondary pollution and poor selectivity. Especially after the completion of the adsorption, the material is difficult to be separated from water, which is the most difficult problem to apply on the real projects.

MFe₂O₄ (M represents metal elemental), a kind of magnetic substance with a cubic spinel structure, has well received by the people’s favorites and been widely used in many fields. Among them, CoFe₂O₄ gets more attention due to its advantages, such as large saturation magnetization and good thermal stability. Fe₃O₄ was also one of magnetic materials and got more modification and researches in recent years.

 Compared with the production process of Fe₃O₄, the synthesis method of CoFe₂O₄ is simpler and the process of reaction can underway without the need of nitrogen environment. According to the study of Zhang, the number of hydroxyl group (M–OH) on the surface of CoFe₂O₄ (38.1%) was higher than that of Fe₃O₄ (25.4%). The amount of M–OH has a significant effect on the performance of the adsorbents, and the more M–OH, the more easily material can be modified.

In addition to the above advantages, CoFe₂O₄ also has some shortcomings that cannot be overcome by itself, such as easy agglomeration, corrosion in acidic environments and so on, which is not conducive to the material adsorption and adsorption selectivity. In general, the methods of adding surfactant or...
forming silica layer outside CoFe$_2$O$_4$ through hydrolyzing tetraethyl silicate (TEOSs) can greatly improve corrosion resistance and dispersion of CoFe$_2$O$_4$ in water.$^{15,16}$

According to the Lewis acid–base interactions,$^{17}$ thiol group and mercury should have a high affinity to each other, for thiol group is characteristic of soft base and mercury is a soft acid. Thiol group is also an excellent ligand. CoFe$_2$O$_4$ can be modified with thiol group to improve the adsorption properties of materials. 3-Mercaptopropyltrimethoxysilane (MPTMS) is a silane coupling agent containing mercapto functional groups. After the inorganic layer SiO$_2$ was coated on the surface of CoFe$_2$O$_4$ and MPTMS was added, the mercapto group was successfully grafted.

During the process of modification, the contents of thiol in adsorbents are related to amount of catalysts used in the reaction, the choice of solvents, reaction temperature and reaction time.$^{18}$

Currently, most of magnetic adsorption materials were modified with Fe$_2$O$_3$. However, the research with CoFe$_2$O$_4$ modified materials to remove heavy metal was little. One aim of this paper is to explore the adsorption performance of the prepared adsorbent modified with other magnetic base material, i.e., CoFe$_2$O$_4$; another aim is to prepare CoFe$_2$O$_4$ base adsorbent with core–shell construction and investigate its adsorption performance for Hg(II) ions when the prepared adsorbent was modified by thiol group.

So, in this paper, in order to overcome the defect of easy agglomeration and corrosion of CoFe$_2$O$_4$, improve its dispersion in water and simultaneously develop a novel adsorbent with high adsorption capability, a thiol-functionalized and silica-coated magnetic nanoparticle (CoFe$_2$O$_4$@SiO$_2$–SH) was synthesized by a simple method and employed to remove Hg(II) ions from water. The characteristics and properties of materials before and after modification were discussed by various methods of characterization. To deeply comprehend the adsorption process of materials, the adsorption kinetics, isotherm and thermodynamics were employed. The effects of foreign ions on the adsorption process and the adsorption mechanism were discussed.

2. Materials and experimental methods

2.1 Experimental materials

Cobaltous nitrate hexahydrate (Co(NO$_3$)$_2$·6H$_2$O), iron(III) acetylacetonate (Fe(acac)$_3$), ethylene glycol (EG), sodium acetate anhydrous (CH$_3$COONa), polyethylene glycol, cetyltrimethylammonium bromide (CTAB, 99 wt%), methanol (CH$_3$OH), glycerol (C$_3$H$_8$O$_3$) and ammonia water (NH$_3$·H$_2$O, 25–28 wt%) were provided by Macklin Reagent (China). (3-Mercaptopropyl)trimethoxysilane (MPTMS, 98 wt%) and TEOs were obtained from Macklin Reagent (China). All chemical materials and solvents were analytical grade.

2.2 Preparation of CoFe$_2$O$_4$@SiO$_2$–SH

2.2.1 Preparation of CoFe$_2$O$_4$. CoFe$_2$O$_4$ magnetic nanoparticles (MNP)s were obtained via using a hydrothermal technology. Briefly, Co(NO$_3$)$_2$·6H$_2$O (2.1825 g) and Fe(acac)$_3$ (5.2977 g) were dissolved in EG (90 mL), vigorous stirring for 30 min. Then, CH$_3$COONa (6.51 g) and polyethylene glycol (2.00 g) were added slowly under vigorous magnetic stirring until a uniform state was formed. The homogeneous solution was transferred into an autoclave (150 mL) and reacted in the oven at 453 K for 14 h. The resulting black mixture was washed with ultrapure water for several times after cooling, and finally dried at 333 K for 8 h and bagged for later use.

2.2.2 Preparation of CoFe$_2$O$_4$@SiO$_2$ MNPs. CTAB (0.1366 g) was dispersed in pure water (150 mL) as a surfactant by sonication for 20 min, and then CoFe$_2$O$_4$ (0.30 g) was dispersed in the above solution by vigorous mechanical stirring to form a uniform state. TEOs (1 mL) and NH$_3$·H$_2$O (1.3 mL) were added as the catalysts at the temperature of 353 K and the reaction was continued for 3 h under mechanical stirring. The synthesized CoFe$_2$O$_4$@SiO$_2$ MNPs were separated magnetically, washed with ultrapure water for three times and dried at 333 K for 8 h. The obtained powder was calcined in a muffle furnace at 673 K for 4 h, and subsequently treated with HCl (1 M) for 12 h and continued to dry for later use.

2.2.3 Preparation of CoFe$_2$O$_4$@SiO$_2$–SH MNPs. In a typical preparation (Fig. 1), the obtained CoFe$_2$O$_4$@SiO$_2$ MNPs (0.2 g), CH$_3$OH (25 mL) and CH$_3$COONa (150 mL) were added in a three-necked flask and stirred 30 min under a nitrogen atmosphere. Subsequently, the temperature was raised to 343 K and NH$_3$·H$_2$O (2 mL) was added. The ligand MPTMS (0.3 mL) dissolved in CH$_3$OH (25 mL) was added dropwise under stirring. The mixture was allowed to react for 1 h under a nitrogen atmosphere at 343 K. After that, the reaction was continued for 5 h without nitrogen. The synthesized CoFe$_2$O$_4$@SiO$_2$–SH MNPs were separated magnetically and washed with ethanol and ultrapure water for three times, separately. The obtained powders were dried in vacuum at 333 K for 8 h.

2.3 Sample characterizations

The obtained samples were characterized via Scanning Electron Microscope (SEM), Transmission Electron Microscopy (TEM), X-ray Diffraction analysis (XRD), Fourier Transform Infrared (FT-IR), Vibrating Sample Magnetometer (VSM), N$_2$ adsorption–desorption isotherms, X-ray Photoelectron Spectroscopy (XPS) and Inductively Coupled Plasma Optical Emission Spectroscopy (ICP-OES). SEM (FEI Quanta FEG250, USA) and TEM (JEM-2100F, Japan) were used to observe the morphology. XRD (D/MAX-2550-18KW, Japan) was used to analyze the phase and crystallinity of the adsorbents.

The functional groups in materials were analyzed by FT-IR (Thermo, Nicolet-6700, USA). The magnetic property of the nanocomposites was confirmed by VSM (Quantum design, MPMS3, USA). The specific surface values and the pore distributions were got on the basis of nitrogen adsorption (Quanta, Autosorb-IQZ-MP-XR-VP, USA) at 77 K through using Brunauer–Emmett–Teller (BET) equation. Chemical elements compositions were measured by XPS (Thermo Scientific, Escalab 250Xi, USA). Quantitative determination of the contents for Hg(II) ions were performed by ICP-OES.
2.4 Adsorption experiments

To prevent the hydrolysis of mercury ions, the protective solution was configured as follows: concentrated HNO₃ (10 mL) and HCl (0.1 mL) were added into ultrapure water (1000 mL). A reserve solution of Hg(II) (1 g L⁻¹) was made through dissolving HgCl₂ (0.6767 g) in a 500 mL protective solution. The protective solution was diluted with according to the desired concentration before each experiment.

The adsorption capacities of CoFe₂O₄@SiO₂–SH MNPs were evaluated at various conditions of pH, adsorbent dosages, contact time (t), initial concentration of Hg(II) and co-existing ions. Effect of pH values of 2–10 was assessed through adding 0.1 mol L⁻¹ HCl and 0.1 mol L⁻¹ NaOH solutions. Adsorption studies were carried out in 250 mL stoppered flasks with Hg(II) solution (100 mL, 40 mg L⁻¹) and 0.005 g of adsorbents. The stoppered flasks with the mixture were put in a shaker at 298 K for 12 h. The contents of Hg(II) were filtered, reserved solution of Hg(II), 0.1 mol L⁻¹ HCl and 0.1 mol L⁻¹ NaOH solutions. Adsorption separation before each experiment.

The dosage effects of adsorbents (defined as ratios of solid to liquid) were investigated at the intervals of 0.03, 0.05, 0.08, 0.1 and 0.15 g L⁻¹ with 40 mg L⁻¹ of Hg(II) at pH = 8 and 298 K. The contact time was examined at 1, 3, 5, 10, 30, 60, 180, 240, 300, 360, 420, 480, 540, 600, 660 and 720 min with 40 mg L⁻¹ of Hg(II) and 0.005 g adsorbents at pH of 8 and 298 K.

The isotherms were studied at 298, 308 and 318 K at pH = 8 and t = 12 h. The initial concentration was charged between 20 and 200 mg L⁻¹. In the research of co-existing ions, five kinds of salts with a concentration of 10 mM and 100 mM were separately added into the Hg(II) solutions, respectively. The adsorption capacities can be determined as following:

\[ q_e = \frac{(C_0 - C_e) \times V}{W} \]

where, \( q_e \) is the equilibrium capacity of Hg(II) (mg g⁻¹), \( C_0 \) and \( C_e \) are the initial and equilibrium concentration of Hg(II) (mg L⁻¹), respectively. \( V \) and \( W \) are the solution volume (L) and adsorbent dosages (mg), respectively.

3. Results and discussion

3.1 Characterization

SEM images of CoFe₂O₄, CoFe₂O₄@SiO₂ and CoFe₂O₄@SiO₂–SH MNPs are compared and shown in Fig. 2. The diameters of these adsorbents were about 50–90, 70–120, and 80–130 nm, respectively. As displayed in Fig. 2(a), the size of CoFe₂O₄ nanoparticles was small, but not uniform. Its surface was not smooth and crowded together. The observed aggregation may be due to the small size and the priority requirement for reducing the interfacial energy of nanoparticles.

As displayed in Fig. 2(b), the size of CoFe₂O₄@SiO₂ became larger and the surface got smooth, indicating that CoFe₂O₄ successfully covered the silicon shell. Fig. 2(c) shows that the dispersity of the material had been greatly improved after modified by MPTMS. Based on the data in Fig. 2(d), the black magnetic core was wrapped around the translucent polymer coating, which was the silicon shell.

Fig. 3(a) shows the XRD patterns of CoFe₂O₄, CoFe₂O₄@SiO₂ and CoFe₂O₄@SiO₂–SH. It can observe that XRD pattern of CoFe₂O₄ had the diffraction peaks that appeared at 2θ = 30.1°, 35.5°, 43.3°, 53.8°, 56.8° and 62.5°, corresponding to the JCPDS file of CoFe₂O₄ (no. 22-1086). All of the diffraction peaks of CoFe₂O₄@SiO₂ and CoFe₂O₄@SiO₂–SH were similar to those of CoFe₂O₄, and no peaks of any other phases were observed, indicating that the structure and the crystal formation of CoFe₂O₄@SiO₂ and CoFe₂O₄@SiO₂–SH MNPs remained unchanged after silicon-covering and thiol-functionalized process.

The average sizes of CoFe₂O₄, CoFe₂O₄@SiO₂ and CoFe₂O₄@SiO₂–SH were calculated using the Debye–Scherrer formula to be 18.1, 20.0 and 21.6 nm, respectively.

The functional groups and chemical bonds in the materials were analyzed by means of FT-IR. Fig. 3(b) indicates FT-IR spectra of CoFe₂O₄, CoFe₂O₄@SiO₂ and CoFe₂O₄@SiO₂–SH (CoFe₂O₄@SiO₂–SH-1 was the fresh original sample and CoFe₂O₄@SiO₂–SH-2 was prepared one month ago). Broad FT-IR peaks around at 3439 and 1636 cm⁻¹ observed should be
attributed to stretching vibration of –OH in surface adsorbed water.\(^\text{22}\)

A broad adsorption band at 1092 cm\(^{-1}\) can be attributed to Si–O–Si.\(^\text{23}\) As reported, typical adsorption bands of thiol group should be at about 2550 cm\(^{-1}\). However, the two very weak peaks of –SH can be found at round 2360 cm\(^{-1}\). It may be owing to the aggregation of –SH group and the effect of –H bonds. The phenomenon has also been reported by other scholars.\(^\text{24,25}\) A bend at 2928 cm\(^{-1}\) was the C–H stretching of methylene from alkyl chain,\(^\text{26}\) which can indirectly indicate that MPTMS had been successfully grafted onto CoFe\(_2\)O\(_4\)@SiO\(_2\).

Moreover, the material of CoFe\(_2\)O\(_4\)@SiO\(_2\)–SH-2 had a similar FT-IR picture compared to the CoFe\(_2\)O\(_4\)@SiO\(_2\)–SH-1, shown in Fig. 3(b), which indicated that the prepared nanocomposite of CoFe\(_2\)O\(_4\)@SiO\(_2\)–SH had a good stability.

Fig. 4 shows the magnetic hysteresis loops of the three synthesized nanoparticles. The results show that saturation magnetization values for the three synthesized nanoparticles
were 56.03, 44.68 and 11.61 μemu g⁻¹ at 20 kOe, respectively. It can be clearly seen that the saturation magnetization values were decreased after modified by MPTMS, which indirectly proved that the surface of CoFe₂O₄@SiO₂ formed a non-magnetic thiol functional layer. After modified with MPTMS, the magnetic properties of the materials reduced obviously, but still can be easily separated from water via a magnetic field. It is conducive to the solid–liquid separation, making the whole adsorption process more environmentally friendly.

Based on the data in Fig. 5, the BET values, pore volumes and pore diameters of the three synthesized materials can be determined and exhibited in Table 1. From Table 1, the pore diameters and total pore volumes of CoFe₂O₄@SiO₂ changed little under the addition of surfactant CTAB and introduction of silicone shell TEOs. However, the BET value of CoFe₂O₄@SiO₂ is four times more than that of CoFe₂O₄, which may be the structure change of porous fluffy state of CoFe₂O₄@SiO₂ and the removal of CTAB after calcination at high temperature.

After the introduction of mercapto groups by MPTMS, the BET value returned to the original value, which may be due to the existence of large amount of organic mercapto groups grafted into CoFe₂O₄@SiO₂ mesopores. On one hand, it shows the successful grafting of -SH; on the other hand, it indicates that the BET value was not the main factor affecting the adsorption performance of CoFe₂O₄@SiO₂–SH.

The wide-scan XPS spectra of the three synthesized materials are shown in Fig. 6. The elements of Fe, Co, O and C on the surface of CoFe₂O₄ were detected. For CoFe₂O₄@SiO₂, the peaks of Fe and Co elements almost disappeared, and the peaks of Si and S appeared, indicating that the silicon shell has completely wrapped the magnetic core CoFe₂O₄.

After modification with MPTMS, the peaks of Si became weak and a new peak of S appeared. Through high resolution scans of CoFe₂O₄@SiO₂–SH shown in Fig. 6(b)–(f), it can be known that the peaks of Fe 2p, Co 2p, C 1s, Si 2p and O 1s were at 724.59 eV, 781.86 eV, 284.33 eV, 101.73 eV and 531.92 eV, respectively, which directly indicated that the –SH was introduced onto the material successfully by MPTMS modification. The results agreed well with the FT-IR analysis of the sorbents.

### 3.2 Adsorption experiments

#### 3.2.1 Effect of MPTMS

The addition of MPTMS had an obvious effect on the morphological and adsorption properties of CoFe₂O₄@SiO₂–SH. The relationship between the addition of MPTMS and the effects of adsorbents on mercury adsorption is shown in Fig. 7.

The adsorption capacity of CoFe₂O₄@SiO₂–SH increased with the increasing amount of the MPTMS under the condition of low addition of MPTMS. The optimum amount of MPTMS was found to be 0.3 mL. If the amount of MPTMS was less than 0.3 mL, the surface of the material would not be completely grafted by –SH group, therefore, the adsorption capacity cannot be maximized. When the addition amount of MPTMS was 0.3 mL, the qₑ of adsorbents reached 374.4 mg g⁻¹.

Continued to increase the amount of MPTMS, the adsorption capacity of the adsorbents had not been further improved, but slightly decreased. So, the optimal amount of MPTMS

![Fig. 4 VSM analysis of three synthesized materials.](image_url)

![Fig. 5 N₂ adsorption desorption isotherms (a) and size distribution (b) of CoFe₂O₄, CoFe₂O₄@SiO₂ and CoFe₂O₄@SiO₂–SH.](image_url)

| Table 1 Structure and chemical data of prepared mesoporous materials |
|-----------------------|----------------|-----------------|
| Samples               | BET values (m² g⁻¹) | Total pore volumes (cm³ g⁻¹) | Pore diameters (nm) |
| CoFe₂O₄               | 48.49           | 0.424           | 3.413            |
| CoFe₂O₄@SiO₂          | 225.36          | 0.552           | 3.062            |
| CoFe₂O₄@SiO₂–SH       | 48.90           | 0.348           | 3.409            |

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should be 0.3 mL. The reason may be owing to no excess active sites grafting with MPTMS on the surface of CoFe$_2$O$_4$@SiO$_2$. It also may be owing to the aggregation of magnetic core because of the uncontrolled self-condensation of trimethoxysilane groups, as Sun et al. reported.

3.2.2 Effect of pH. For the value of pH can directly influence the interaction between H$^+$/OH$^-$ and other substances, the existential morphology of mercury ions and the number of active sites on the surface of adsorbents, it is greatly important to explore the effects of solution pH on the adsorption capacity of CoFe$_2$O$_4$@SiO$_2$–SH. The pH value of solution was adjusted from 2 to 10 with $C_0$ of 40 mg L$^{-1}$ at 298 K.

Based on the data from Fig. 8, $q_e$ of CoFe$_2$O$_4$@SiO$_2$–SH for Hg$^{II}$ reached a maximum of 374.4 mg g$^{-1}$ at pH of 8. Furthermore, the CoFe$_2$O$_4$@SiO$_2$–SH exhibited better adsorption performance at pH of 2–10. The adsorption capacity had also a high value of 271.2 mg g$^{-1}$ even at pH = 2.

3.2.3 Effect of dosage. The optimum amount of adsorbents was selected by adding various amounts of adsorbents under the same adsorption conditions to test its adsorption effect. Different mass amounts of CoFe$_2$O$_4$@SiO$_2$–SH (3, 5, 8, 10 and 15 mg) were employed with 100 mL of Hg$^{II}$ ($C_0 = 40$ mg L$^{-1}$) in a water bath at pH = 8 and $T = 298$ K for 12 h.

As shown in Fig. 9, along with the increasing addition of CoFe$_2$O$_4$@SiO$_2$–SH, the adsorption capacity for Hg$^{II}$ decreased quickly and the adsorption efficiency increased remarkably. Fig. 9 shows that CoFe$_2$O$_4$@SiO$_2$–SH had great high adsorption capacities for Hg$^{II}$ even with pretty low dosage, for instance, 0.05 g L$^{-1}$.

3.3 Adsorption kinetics
The adsorption kinetic data of heavy metal ions were analyzed by testing pseudo-first-order (eqn (2)), pseudo-second-order (eqn (3)) and the intra-particle diffusion models (eqn (4)).
more Hg(II) was adsorbed onto the materials, and meanwhile, the concentration gradient between the surface of the material and the interior of solution decreased, resulting in a decreasing adsorption rate, and ultimately tending to a balance.

The goodness of fitting was estimated from the measurement coefficient $R^2$. The calculated results were listed in Table 2. The data from pseudo-first-order model in Fig. 10(b) did not show good agreement ($R^2 = 0.941$) with the experimental data, and the difference between the theoretical $q_{e,cal}$ (332.8 mg g$^{-1}$) and the experimental $q_{e,exp}$ (374.4 mg g$^{-1}$) was a little large. The data from pseudo-second-order model in Fig. 10(c) fitted well ($R^2 = 0.989$), and the theoretical $q_{e,cal}$ (392.2 mg g$^{-1}$) was close to the actual $q_{e,exp}$. Therefore, the experimental results can be well represented by pseudo-second-order model and indicated that the removal of Hg(II) with CoFe$_2$O$_4$@SiO$_2$–SH involved chemical reaction.

In Fig. 10(d), the initial linear portion represented instantaneous adsorption on the surface of the material, indicating that the mass transfer in the early stage was achieved by large pore diffusion. The second stage was the gradual adsorption, indicating that mass transfer at this stage was achieved via microporous diffusion. The second stage was the main diffusion rate limitation. The third line was tending to equilibrium stage. Straight lines did not go through the origin, indicating that intra-particle diffusion was not the only rate limitation.

### 3.4 Adsorption isotherms

To further investigate the capacity of Hg(II) onto CoFe$_2$O$_4$@SiO$_2$–SH, Langmuir (eqn (5)$^{32}$ and Freundlich models (eqn (7)$^{33}$) were employed. The Langmuir model supposes the adsorption as monolayer and occurring on a homogeneous surface shown as eqn (6), whereas Freundlich model is built on the theory of multilayer adsorption shown as eqn (6).

$$\frac{C}{q_e} = \frac{C}{Q_m} + \frac{1}{Q_mK_L}$$

$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e$$

---

Fig. 7 Effect of MPTMS amount in CoFe$_2$O$_4$@SiO$_2$–SH. Conditions: pH = 8, dosage of 0.05 g L$^{-1}$, $C_0 = 40$ mg L$^{-1}$, $t = 12$ h and $T = 298$ K.

Fig. 8 Effects of pH on the removal of Hg(II) with CoFe$_2$O$_4$@SiO$_2$–SH as adsorbent. Conditions: dosage of 0.05 g L$^{-1}$, $C_0 = 40$ mg L$^{-1}$, $t = 12$ h and $T = 298$ K.

Fig. 9 Effects of dosage with CoFe$_2$O$_4$@SiO$_2$–SH as adsorbent. Conditions: pH = 8, $C_0 = 40$ mg L$^{-1}$, $t = 12$ h and $T = 298$ K.

Fig. 10(a) shows that when $t \leq 60$ min, the adsorption rate was very fast, which may be due to the surface of the material had a rich activity of adsorption sites at the beginning of the reaction. With the passage of time, more and more Hg(II) was adsorbed onto the materials, and meanwhile, the concentration gradient between the surface of the material and the interior of solution decreased, resulting in a decreasing adsorption rate, and ultimately tending to a balance.

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$$\frac{C}{q_e} = \frac{C}{Q_m} + \frac{1}{Q_mK_L}$$

$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e$$
where $Q_m$ (mg g$^{-1}$) is the maximum capacity, $K_L$ (L mg$^{-1}$), $K_F$ (mg$^{1-n}$ L$^n$ g$^{-1}$) and $n$ (unitless) are all constants related to adsorption. The separation factor ($R_L$) can be written as follows:

$$R_L = \frac{1}{1 + K_L C_0} \tag{7}$$

Fig. 11(a) and (b) show the isotherm fitting of Hg(II) on the surface of CoFe$_2$O$_4$@SiO$_2$–SH. Table 3 exhibits the isotherm parameters under three temperatures. $R^2$ (0.995) from Freundlich model was higher than that from Langmuir model (0.989),

Table 2 Parameters of adsorption kinetics for Hg(II) onto CoFe$_2$O$_4$@SiO$_2$–SH

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<td>$R^2$</td>
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Intra-particle diffusion

$k_{d1}$ $C_1$ $R_1^2$ $k_{d2}$ $C_2$ $R_2^2$ $k_{d3}$ $C_3$ $R_3^2$

74.69 $-57.21$ 0.910 10.66 97.06 0.999 5.80 228.39 0.839

Table 3 Isotherm parameters of CoFe$_2$O$_4$@SiO$_2$–SH

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<th>T (K)</th>
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</table>

Fig. 11 The Langmuir (a) and Freundlich (b) isotherm curves with CoFe$_2$O$_4$@SiO$_2$–SH ($T = 298$ K, pH = 8, dosage of 0.05 g L$^{-1}$ and t = 12 h).
indicating a better fitting with Freundlich model compared with Langmuir model. The \( n \) from Freundlich constants was greater than 1, indicating a favourable adsorption.\(^{34}\) Three \( R^2 \) from Langmuir model were all greater than 0.980, indicating a good fitting degree. So Langmuir model can be employed to simulate the removal process for Hg(II).

Langmuir also suggested a monolayer adsorption process and the \( Q_m \) from CoFe\(_2\)O\(_4@\)SiO\(_2\)–SH was 641.0 mg g\(^{-1}\). This value was much larger than the maximum adsorption capacity of many similar materials (Table 4).\(^{35,36}\) The separation factor \( R_L \) can determine if adsorbents have an ability to effectively remove contaminants. The data in Table 3 showed that \( R_L \) value changed from 0 to 1, indicating a spontaneous adsorption.

### 3.5 Adsorption thermodynamics

Three thermodynamic parameters, Gibbs free energy (\( \Delta G^0 \), kJ mol\(^{-1}\)) (eqn (8)), enthalpy (\( \Delta H^0 \), kJ mol\(^{-1}\)) (eqn (9)) and entropy (\( \Delta S^0 \), kJ mol\(^{-1}\) K) (eqn (9)) of adsorption are listed as follows:

\[
\Delta G^0 = -RT \ln K_d
\]  
(8)

\[
\ln K_d = \frac{\Delta S^0}{R} - \frac{\Delta H^0}{RT}
\]  
(9)

where \( R \) is universal gas constant (8.314 J mol\(^{-1}\) K), and \( K_d \) \( (q_e/C_0) \) is a coefficient. The resulted thermodynamic data for Hg(II) removal onto CoFe\(_2\)O\(_4@\)SiO\(_2\)–SH was listed in Table 5. For \( \Delta H^0 < 0 \), the process was exothermic. The value of \( \Delta G^0 \) was less than 0, indicating that the removal process for Hg(II) was spontaneous.

### 3.6 Effect of coexisting ions

In the real application of materials, the anions and cations in the natural water may have an effect on adsorption capacity. Hence, six common types of ions, including three cations (Na\(^+\), K\(^+\) and Ca\(^{2+}\)) and three anions (Cl\(^-\), NO\(_3^-\) and SO\(_4^{2-}\)) were used to assess the removal of Hg(II) with CoFe\(_2\)O\(_4@\)SiO\(_2\)–SH.

From Fig. 12, the adsorption properties of materials are affected by the individual ions and decreased as the ionic strength increases. This may be owing to the fact that the cations in the water compete with the active adsorption sites, resulting in a descending adsorption.\(^{47}\)

Among these ions, Ca\(^{2+}\) has the greatest effect on the capacity of materials, probably because Ca\(^{2+}\) is a divalent cation with two positive charges, which will occupy two active sites.\(^{48}\) Therefore, the effect of Ca\(^{2+}\) on the performance of the material was larger than that of other monovalent cations including K\(^+\) and Na\(^+\). For anions, Cl\(^-\) has the greatest effect on the adsorption. Cl\(^-\) can complex with mercury to form HgCl\(_2\), HgCl\(_3\) and HgCl\(_4\).\(^{44}\) However, higher concentration of Cl\(^-\) can compete for the surface of the active sites with mercury, resulting in a decreased adsorption.\(^{49}\)

### 3.7 Application evaluation

In order to further reveal the performance of the material of CoFe\(_2\)O\(_4@\)SiO\(_2\)–SH in a real engineering, an application
evaluation was carried out. Firstly, desorption and regeneration experiments were made to investigate the reusable performance of the material, and the results were shown in Fig. 13. From the data in Fig. 13, it can be seen that the adsorption capacities declined slowly with the increasing cycles, and the decrease of adsorption capabilities of CoFe$_2$O$_4$@SiO$_2$–SH was about 16.2% after five cycles.

Besides, as we know, electroplating wastewater is a common and typical wastewater and contains many kinds of harmful heavy metals, such as mercury, chromium, nickel, lead, and so on. To investigate the adsorption activity of the material, a real electroplating wastewater sample was employed to be treated by the material of CoFe$_2$O$_4$@SiO$_2$–SH.

The concentrations of Hg(II), Cr(VI), Ni(II) and Pb(II) in the wastewater sample are 0.04–0.8 mg L$^{-1}$, 0.6–1.3 mg L$^{-1}$, 0.5–1.1 mg L$^{-1}$ and 0.15–0.3 mg L$^{-1}$, respectively. The COD$_{cr}$ value of wastewater is about 43.5–55.1 mg L$^{-1}$. The experiments were carried out at the conditions of dosage of 0.15 g L$^{-1}$ and pH of 8 ± 0.2.

The test shows that the removal efficiency of Hg(n) achieved over 99% after adsorption and the effluent basically met the Chinese National Standard “Emission Standard of Pollutants for Electroplating” (GB 21900-2008). The above data indicated that the as-prepared material of CoFe$_2$O$_4$@SiO$_2$–SH could be employed as a promising and efficient adsorbent in the real water treatment engineering.

### 3.8 Mechanism speculation

By comparing the XPS spectra of a wide range and individual important elements of CoFe$_2$O$_4$@SiO$_2$–SH before and after adsorption for mercury, it can further investigate the removal mechanism of materials.

Fig. 14(a) exhibits the wide scans of CoFe$_2$O$_4$@SiO$_2$–SH (before adsorption) and CoFe$_2$O$_4$@SiO$_2$–SH–Hg (after adsorption). Before adsorption, the wide scan clearly shows the peaks of O 1s, C 1s, Si 2p and S 2p. After the material adsorbed Hg(n), the peak of S 2p became weak and the new peaks of Hg 4d and Hg 4f were clearly observed. The presence of Hg 4p and Hg 4f demonstrated the successful adsorption of CoFe$_2$O$_4$@SiO$_2$–SH for Hg(n) ions.

Fig. 14(b), through comparing the XPS spectra of S elements before and after adsorption for Hg(n), it can be known that the peak of S 2p after adsorption was weaker than that before adsorption, and was slightly shifted. Also, a peak of S 2p appeared at 162.91 eV before adsorption may belong to –SH.
The peak of S 2p was slightly moved to 162.82 eV after adsorption. It may be that S atoms in mercapto group donated parts of electrons to Hg during the process of adsorption.

From Fig. 14(c), the high resolution XPS spectra of Hg, there is a double-peaks, which may be the Hg 4f_{5/2} (100.8 eV) and Hg 4f_{7/2} (104.8 eV), which further demonstrates the successful adsorption of mercury onto the material.

As we know, mercury in aqueous solution exists mainly in three forms: Hg^{2+}, Hg(OH)^+ and Hg(OH)_2. In acidic solution (pH < 3), the three forms are all present. Hg^{2+} was the main form of existence, and its amount will decrease with the pH increasing, until disappearance. The amount of the other two forms of Hg(OH)^+ and Hg(OH)_2 will increase as pH increases.

In addition, the number of Hg(OH)^+ will reach the maximum at pH = 4, and Hg(OH)_2 will become the main form at pH > 6. To better understand the removal mechanism, the probable reaction processes between Hg(u) and the mercapto-modified materials are plotted in Fig. 14.

Fig. 15 shows that Hg^{2+} can form −SH−Hg^2+ with the mercapto group under electrostatic attraction, but the existence of large amount of −SH−Hg^+ might be also slightly prevent the further progress of the reaction. Hg(OH)^+ and Hg(OH)_2 in water can form complexes directly with mercapto groups with/without electrostatic attraction. In the solutions with various pH, the above three forms of mercury exist in different amounts and are adsorbed by the mercapto group by different ways.

In the aforementioned study of pH on adsorption, the gaps between adsorption performances of CoFe$_2$O$_4$@SiO$_2$−SH were not large at pH of 2–10. Coupled with results of the effect of mercapto content on the adsorption capacities, it can be concluded that the adsorption capacity of CoFe$_2$O$_4$@SiO$_2$ was greatly improved after the introduction of mercapto. CoFe$_2$O$_4$@SiO$_2$−SH had an excellent adsorption for mercury, mainly due to the affinity between −SH and mercury, apart from the electrostatic interactions between the material and mercury. Based on the Hard Soft Acid–Base theory, mercapto (soft base) and Hg (soft acid) can have a strong affinity, which is very conducive to the progress of the adsorption reaction.

4. Conclusions

In this study, a thiol-functionalized and silica-coated magnetic nanoparticle (CoFe$_2$O$_4$@SiO$_2$−SH) was successfully synthesized via a simple and cost effective method, and employed to remove Hg(u) in water.

The adsorption process showed a good performance at pH of 2–10, which implied a probable practical application. And CoFe$_2$O$_4$@SiO$_2$−SH had great high adsorption capacities for Hg(u) even with pretty low dosage of 0.05 g L$^{-1}$.

Kinetic fitting exhibited a good correlation to pseudo-second-order model and adsorption process was controlled by a chemical reaction with three diffusion stages. The isotherm data were in accord with Freundlich model with maximum capacities of 641.0 mg g$^{-1}$ at 298 K and pH of 8, substantially higher than many similar materials. Thermodynamic data displayed an exothermic and spontaneous adsorption process.

Hg$^{2+}$ can form −SH−Hg^2+ with the mercapto group or complexes with/without electrostatic attraction. Furthermore, after adsorption, CoFe$_2$O$_4$@SiO$_2$−SH MNPs can be collected from water at a low magnetic field gradient, which helps to prevent secondary pollution and reduce the costs of water treatment. In general, CoFe$_2$O$_4$@SiO$_2$−SH MNPs is an economy and efficient material with great potential to remove mercury from water.

Conflicts of interest

There are no conflicts to declare.

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