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Glycerol hydrogenolysis over a Pt–Ni bimetallic catalyst with hydrogen generated *in situ*

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Using hydrogen generated *in situ* from aqueous phase reforming provides an efficient and economic route for glycerol hydrogenolysis. A Pt–Ni bimetallic catalyst supported on γ - Al_2O_3 has been prepared to catalyze the selective hydrogenolysis of glycerol to 1,2-propanediol, with glycerol conversion reaching 71.4% in 3 h. The significant promotion of conversion and selectivity could be explained by the formation of Pt–Ni alloy based on catalyst characterization. The effects of Pt/Ni ratio, reaction temperature and reaction time on the conversion of glycerol as well as product selectivity were also investigated.

1 Introduction

With its renewability, biodegradability and carbon neutrality, biodiesel is becoming an attractive energy resource as an alternative to fossil fuels.¹ The past decade has seen the rapid development of the biodiesel industry, in which a great deal of glycerol is generated as a by-product from transesterification during biodiesel production (roughly 10 wt% of the feed oil or fat), but the demand for glycerol is so limited that extensive amounts of crude glycerol are disposed of by burning, which is a waste of potential organic raw materials and releases huge amounts of CO_2 .^{2,3} Developing an economically attractive route to convert glycerol into high value-added chemicals, not only helps solve the glycerol surplus and cut down the production cost of the whole biodiesel industry, but also avoids wasting a carbon resource and diminishes the CO_2 emission from burning.

Recent lots of attention has been paid to glycerol hydrogenolysis into diols such as 1,2-propanediol, 1,3-propanediol and ethylene glycol, which are widely used in the synthesis of pharmaceuticals, polymers, cosmetics, *etc.*^{4–8} However, the low solubility of molecular hydrogen in aqueous glycerol solutions requires a high hydrogen pressure to attain an acceptable conversion, which brings potential risks to industrial process and raises the production cost. D'Hondt *et al.* firstly reported an *in situ* hydrogenation route to produce 1,2-propanediol from glycerol, in which they used NaY zeolite supported Pt catalyst and achieved a glycerol conversion of 85.4% and a 1,2-

propanediol selectivity of 64% at 230 °C under atmospheric conditions.⁹ Combining aqueous phase reforming and hydrogenolysis of glycerol (Fig. 1), the glycerol hydrogenolysis using hydrogen generated *in situ* no longer needs external hydrogen supply or hydrogen donor compounds, providing an efficient and economic route for glycerol hydrogenolysis.

Among various noble and base metals, Pt is the most selective catalyst for aqueous phase reforming of glycerol, but has a poor catalytic activity for glycerol hydrogenolysis.^{10,11} The addition of second metal can strongly modify the activity and selectivity for the hydrogenolysis of glycerol.^{12–14} Motivated by above considerations, in this paper a series of Pt–M (M = Fe, Co, Ni, Cu, Zn, Sn) bimetallic catalysts supported on γ - Al_2O_3 were prepared by incipient wetness impregnation technique, wherein Pt–Ni catalyst was selected because of its high catalytic activity and selectivity in glycerol hydrogenolysis. Field emission scanning electron microscope (FESEM), energy dispersive X-ray (EDX), X-ray diffraction (XRD), transmission electron microscopy (TEM), X-ray photoelectron spectroscopy (XPS), N_2 -adsorption/desorption and H_2 -temperature programmed reduction (H_2 -TPR) were employed to examine the composition,

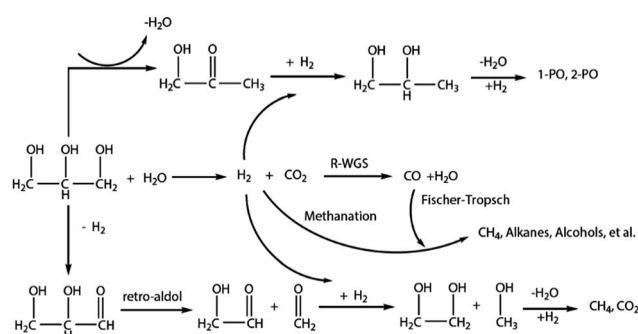


Fig. 1 The reaction network for glycerol hydrogenolysis using hydrogen generated *in situ*.

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structural and redox properties of the Pt–Ni catalyst. Then the effects of Pt/Ni ratio, reaction temperature and reaction time on the conversion of glycerol as well as product selectivity were investigated in detail.

2 Experimental

2.1 Catalyst preparation

Pt–M (M = Fe, Co, Ni, Cu, Zn, Sn) bimetallic catalysts were prepared by incipient wetness impregnation technique. $\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$ and the nitrates of the second metal were dissolved in deionized water, then $\gamma\text{-Al}_2\text{O}_3$ support was added into the liquid phase and stirred till uniform. After impregnation, the sample was aged under room temperature overnight and then dried for 12 h at 100 °C, followed by calcination in air for 4 h at 550 °C. Before use, the catalyst was reduced at 500 °C for 4 h in a hydrogen flow at a steady rate of 50 mL min^{−1}.

2.2 Catalyst characterization

The surface area and pore size were analysed by N₂-adsorption/desorption technique using a Micromeritics ASAP 2020 Physorption. Typically, 0.2 g catalyst was placed in the sample tube and pre-treated for 6 h up to 300 °C at 133 Pa to remove the moisture and impurities adsorbed on the surface, then adsorption/desorption tests were performed in liquid nitrogen at −196 °C.

The chemical composition and morphology of the samples were determined by energy dispersive X-ray (EDX) attached to field emission scanning electron microscope (FESEM, Nova NanoSEM 450).

X-Ray diffraction (XRD) patterns were obtained on a Rigaku D/max 2550 X-ray diffractometer by using the CuK α radiation (λ = 0.1544 nm) and registered in the 2θ range of 10–80° at a scan speed of 4° min^{−1}.

The morphology of the metal nanoparticles was investigated by transmission electron microscopy (TEM) using JEOL-JEM 2100 electron microscope, operated at 200 kV. The samples were prepared using ethanol as the dispersant. An EDS analysis is attached to the TEM to determine the elemental distribution of the sample. XPS measurement was conducted by using an UIVAC-PHI 5000 Versaprobe with a monochromatic Al K α radiation.

H₂-temperature programmed reduction (H₂-TPR) tests were performed with a Micromeritics AutoChemII2920 Chemisorption. A catalyst sample (50 mg) was placed in a U-shaped quartz tube and pre-heated for 2 h at 300 °C in flowing argon, followed by cooling at room temperature. After the pre-treatment, the temperature was raised from room temperature to 800 °C in a 10% H₂/Ar mixture at a flow rate of 40 mL min^{−1}, the H₂ consumption was monitored with a thermal conductivity detector (TCD).

2.3 Catalyst activity tests

Glycerol hydrogenolysis reactions were carried out in a 250 mL stainless steel autoclave equipped with an electronic temperature controller and a mechanical stirrer. After loading the

catalyst and glycerol into the autoclave, the reactor was purged with nitrogen at 2.0 MPa to remove air in it, then the system was pressurized with nitrogen to 1.0 MPa and heated up to the reaction temperature. The rotation speed of the stirrer was set constantly at 500 rpm throughout the reaction. At the end of the reaction, the reactor was cooled down to room temperature. The gas products were collected in a gas bag and analysed by gas chromatography equipped with a 3 m TDX-01 stainless column and a thermal conductivity detector. Liquid products were filtered to recover the solid catalyst powder and analysed by a gas chromatography equipped with a HP-INNOWAX column (30 m × 0.32 mm × 0.25 μm) and a flame ionization detector. The conversion of glycerol and product selectivity were calculated using the following equations:¹⁵

$$\text{Conversion} = \frac{\text{moles of glycerol consumed}}{\text{moles of glycerol initially charged}} \times 100\%$$

$$\text{Selectivity} = \frac{\text{moles of carbon in specific product}}{\text{moles of carbon in all detected products}} \times 100\%$$

3 Results and discussion

3.1 Catalyst screening

Table 1 presents the conversion and product selectivity of glycerol hydrogenolysis at 240 °C for 3 h over Pt–M (M = Fe, Co, Ni, Cu, Zn, Sn) bimetallic catalysts. Among the six bimetallic catalysts, Pt–Ni catalyst has the highest reaction conversion of 71.4%, and gives a selectivity of 52.4% and 12.9% for 1,2-propanediol (1,2-PDO) and ethylene glycol (EG) respectively.

3.2 Catalyst characterization

The specific surface area, pore volume and average pore diameter of the samples are summarized in Table 2. With the increment of Ni amount, the surface area and pore volume decrease due to the surface coverage and plugging of the pores by NiO.¹⁶ The N₂ adsorption–desorption isotherms (Fig. 2a) reveal that all the Pt–Ni bimetallic catalysts exhibit Type V isotherms with typical H2 hysteresis loops, which are characteristic of mesoporous materials.¹⁷ The pore diameter distribution shows that higher Ni amount leads to wider pore diameter distribution (Fig. 2b).

The morphological features of fresh and used Pt–Ni bimetallic catalyst were observed from FESEM analysis (Fig. 3). The fresh Pt–Ni catalyst has a high porosity and specific surface area, which offers more active sites and larger reaction zone for glycerol molecules. For the used catalyst, we found that the porous structure collapses and filamentous carbon species deposits on the surface. EDX analysis verified the formation of coke in the reaction, which leads to an increase of carbon content in the used catalyst (Fig. 4). It is also shown that the metal content on the catalyst surface rises slightly after reaction, which is explained by the agglomeration of metal



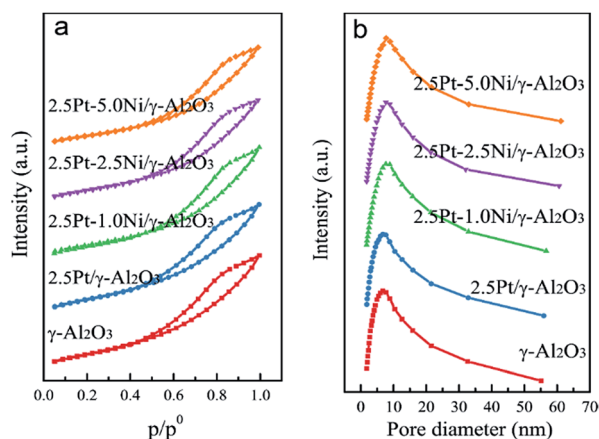
Table 1 Glycerol hydrogenolysis over Pt–M bimetallic catalysts^a

Catalyst	Conversion/%	Selectivity/%						
		1,2-PDO	EG	2-Propanol	1-Propanol	CH ₄	CO ₂	Others ^b
2.5Pt–2.5Fe	61.3	55.6	7.5	5.7	5.6	0.7	15.5	9.4
2.5Pt–2.5Co	55.6	54.4	11.7	6.7	6.8	0.5	12.8	7.1
2.5Pt–2.5Ni	71.4	52.4	12.9	7.9	1.8	3.6	16.7	1.7
2.5Pt–2.5Cu	18.2	48.4	9.8	15.9	3.9	2.4	14.5	5.1
2.5Pt–2.5Zn	52.5	52.1	8.2	7.4	5.2	1.2	11.3	2.6
2.5Pt–2.5Sn	39.1	60.5	8.6	7.4	1.2	0.1	14.5	5.7

^a Reaction conditions: 1.0 g of catalyst, 100 mL of glycerol aqueous solution (20 wt%), 1.0 MPa of N₂ pressure, 240 °C of reaction temperature, 3 h of reaction time. ^b Others contain methanol, ethanol, acetone alcohol, etc.

Table 2 Specific surface area, pore volume and average pore diameter

Catalysts	Surface area (m ² g ^{−1})	Pore volume (cm ³ g ^{−1})	Pore diameter (nm)
γ-Al ₂ O ₃	235.2	0.47	8.0
2.5Pt/γ-Al ₂ O ₃	220.3	0.45	8.0
2.5Pt–1.0Ni/γ-Al ₂ O ₃	203.3	0.45	8.9
2.5Pt–2.5Ni/γ-Al ₂ O ₃	200.8	0.42	8.9
2.5Pt–5.0Ni/γ-Al ₂ O ₃	185.4	0.41	8.7

Fig. 2 N₂ adsorption–desorption isotherms and pore diameter distribution.

particles.¹⁸ Both the coke formation and metal agglomeration contribute to deactivation of the catalyst.

XRD analyses were also conducted on unreduced and reduced catalysts. The peaks at 2θ values of 37.6°, 45.9° and 67.0° are assigned to γ -Al₂O₃ support. As shown in Fig. 5a, XRD did not detect any platinum or nickel species on unreduced catalysts suggesting that the fine PtO₂ and NiO particles are highly dispersed. XRD patterns of reduced catalysts are presented in Fig. 5b. Metallic Pt was observed at 39.6°, 46.2° and 67.3° in reduced 2.5Pt/γ-Al₂O₃ catalyst, which were attributed to the crystalline phases (111), (200), and (220), respectively. The peaks show a slight shift to higher 2θ value and lower intensity with an increase of Ni content after introducing Ni into the catalyst,

indicating that Ni atoms have come into the Pt lattice.¹⁹ There was no noticeable peak for Ni metals in 2.5Pt–1.0Ni/γ-Al₂O₃ catalyst and 2.5Pt–2.5Ni/γ-Al₂O₃ catalyst, which suggests a high

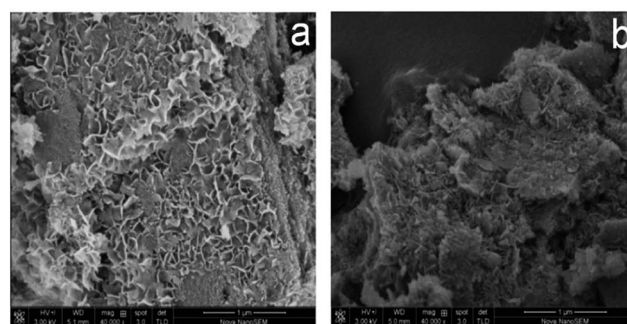
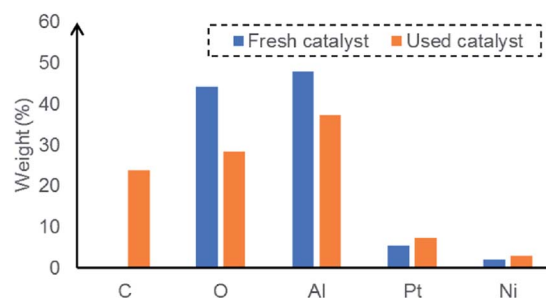
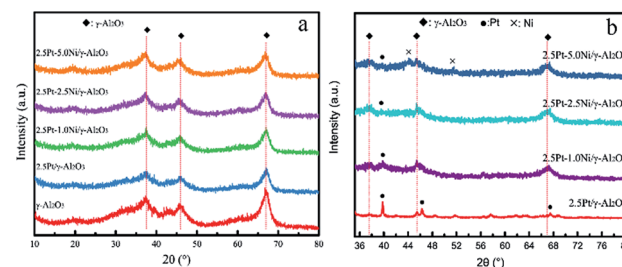
Fig. 3 FESEM images of 2.5Pt–2.5Ni/γ-Al₂O₃ catalyst. (a) Fresh catalyst. (b) Used catalyst.Fig. 4 EDX analysis of fresh and used 2.5Pt–2.5Ni/γ-Al₂O₃ catalyst.

Fig. 5 XRD patterns of catalysts. (a) Unreduced catalyst. (b) Reduced catalyst.



level of Pt–Ni alloys.²⁰ Signals of Ni were detected with 2θ values of 44.5° and 51.7° in 2.5Pt–5Ni/ γ - Al_2O_3 catalyst, which are indexed to the (111) plane and the (200) plane of face-centred cubic (fcc) Ni.

Fig. 6a presents a typical TEM image of the 2.5Pt–2.5Ni/ γ - Al_2O_3 catalyst. As can be seen, the Pt–Ni alloy nanoparticles spread out uniformly on the surface of γ - Al_2O_3 support, and the average measured particle diameter is approximately 1.9 nm. EDS maps of Pt and Ni are presented in Fig. 6b and c, clearly revealing the locations of the nanoparticles. Although the two maps are not identical, there is a certain degree of correlation between the locations of Pt and Ni species. The loading amount of Pt : Ni obtained from spectral data is 2.05 wt% : 2.05 wt%. Fig. 7 shows the XPS spectra of Pt 4f in reduced catalysts. The Pt 4f_{7/2} has a slight negative shift due to the transfer of electrons from Ni to Pt, which lowers the density of state on the Fermi level and subsequently improves the catalytic performance.²¹

H₂-TPR profiles of calcined Pt–Ni catalysts are shown in Fig. 8. Pt monometallic catalyst showed a reduction peak at 225 °C corresponding to the $\text{PtO}_2 \rightarrow \text{Pt}$ reduction. This peak had a shift towards lower temperature for Pt–Ni bimetallic catalyst, indicating that the addition of Ni promoted the reduction of Pt species, which may be explained by the formation of Pt–Ni alloy.²² The reduction peak at the range of 600–800 °C belongs to the reduction of Ni^{2+} ions incorporated in the nickel aluminate structure.²³

3.3 The effect of Pt/Ni ratio

The effect of Pt/Ni ratio was investigated over Pt–Ni bimetallic catalysts, and the glycerol conversion as well as product selectivity were presented in Table 3. Results indicate that although

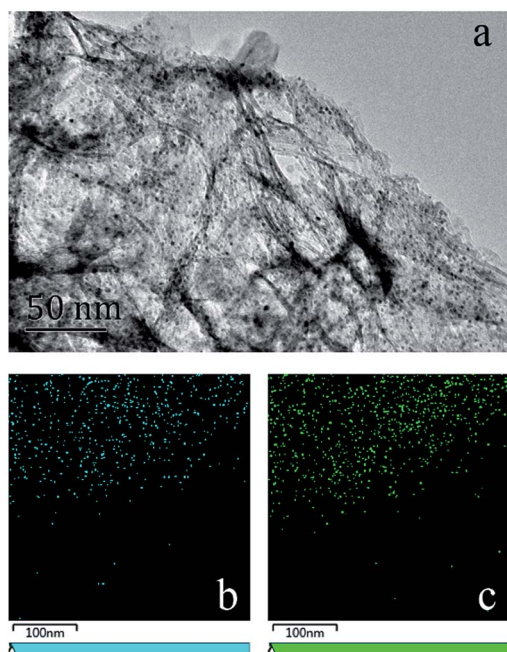


Fig. 6 (a) TEM image of 2.5Pt–2.5Ni/ γ - Al_2O_3 catalyst. (b) EDS map of Pt. (c) EDS map of Ni.

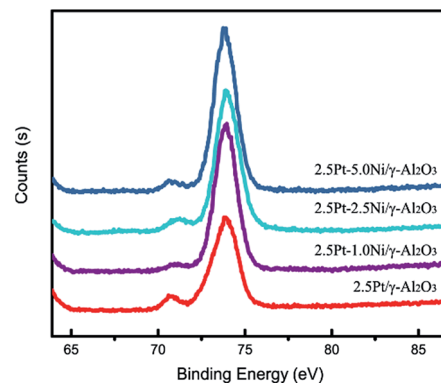


Fig. 7 XPS spectra of Pt 4f in the catalyst.

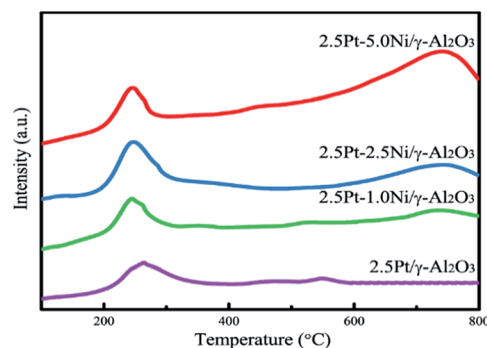


Fig. 8 H₂-TPR profiles of calcined Pt–Ni catalysts.

glycerol hydrogenolysis reaction using hydrogen *in situ* generated is able to proceed over Pt– Al_2O_3 catalyst, both the conversion and selectivity of 1,2-propanediol are relatively low. The addition of Ni significantly improves both the catalyst activity and selectivity for the hydrogenolysis of glycerol, which is associated with the strong interaction between Pt and Ni in the Pt–Ni catalyst, as evidenced in H₂-TPR analysis. A maximum conversion was obtained at a Pt/Ni ratio of 2.5 : 2.5. The surface area and pore diameter drop considerably with higher Ni content due to the plugging of Ni species, leading to a decline of catalyst activity. The selectivity of 1,2-propanediol also decreases owing to over-cracking of hydrogenolysis products into CH_4 and CO_2 .

3.4 The effect of reaction temperature

The effect of reaction temperature on activity and selectivity was studied at a temperature range of 220–260 °C, and the results are presented in Fig. 9. The glycerol conversion has an increasing trend with reaction temperature suggesting that temperature increment favours the reaction activity. The selectivity of 1,2-propanediol decreases from 61.7% at 220 °C to 37.3% at 260 °C, caused by excessive hydro-deoxygenation of 1,2-propanediol (C–O and C–C bond cleavage) to propanol and lower alcohols (*i.e.* methanol, ethanol).^{24–27} The selectivity of ethylene glycol also shows a decreasing trend, but the decrease is not significant. Lahr *et al.* found that ethylene glycol is considerably stable under hydrogenation reaction conditions,



Table 3 Effect of Pt/Ni ratio on glycerol conversion and product selectivity^a

Catalysts	Conversion/%	Selectivity/%						
		1,2-PDO	EG	2-Propanol	1-Propanol	CH ₄	CO ₂	Others ^b
2.5Pt	45.3	47.3	10.0	8.2	6.5	1.1	14.6	2.3
2.5Pt–1.0Ni	65.0	56.9	10.6	7.8	5.2	1.3	15.9	2.3
2.5Pt–2.5Ni	71.4	52.4	10.9	7.9	1.8	1.6	16.7	1.7
2.5Pt–5.0Ni	66.2	50.9	13.1	9.2	4.0	1.9	15.8	2.1

^a Reaction conditions: 1.0 g of catalyst, 100 mL of glycerol aqueous solution (20 wt%), 1.0 MPa of N₂ pressure, 240 °C of reaction temperature, 3 h of reaction time. ^b Others contain methanol, ethanol, acetone alcohol, etc.

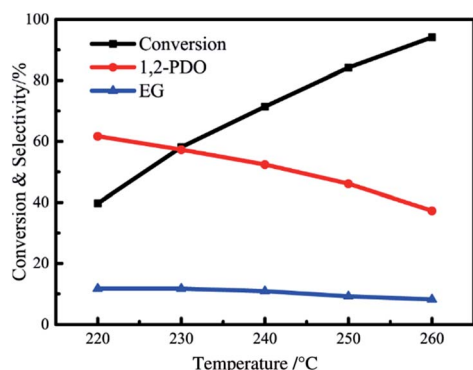


Fig. 9 Effect of reaction temperature on glycerol conversion and the selectivity of 1,2-PDO and EG over 2.5Pt–2.5Ni/γ-Al₂O₃ catalyst. Reaction conditions: 1.0 g of catalyst, 100 mL of glycerol aqueous solution (20 wt%), 1.0 MPa of N₂ pressure, 3 h of reaction time.

so the degradation of ethylene glycol is difficult to proceed in this reaction.²⁸ Besides, the selectivity of gaseous product, CH₄ and CO₂, increases significantly with reaction temperature for aqueous phase reforming of glycerol is an endothermic reaction which favours a higher reaction temperature.¹⁰

3.5 Reaction evolution with time

The effect of reaction time was investigated over Pt–Ni catalyst, and the conversion of glycerol as well as product selectivity are

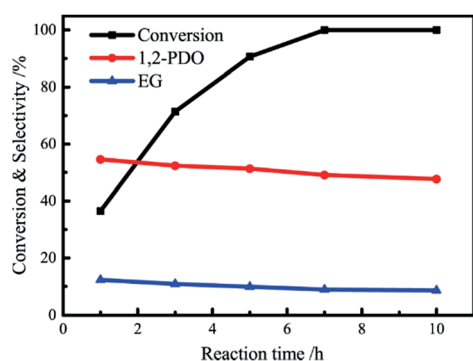


Fig. 10 Effect of reaction time on glycerol conversion and the selectivity of 1,2-PDO and EG over 2.5Pt–2.5Ni/γ-Al₂O₃ catalyst. Reaction conditions: 1.0 g of catalyst, 100 mL of glycerol aqueous solution (20 wt%), 1.0 MPa of N₂ pressure, 240 °C of reaction temperature.

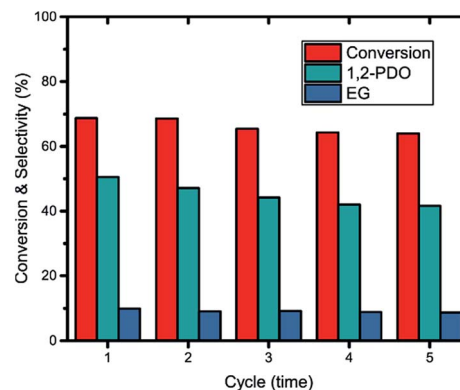


Fig. 11 Reusability tests over 2.5Pt–2.5Ni/γ-Al₂O₃ catalyst. Reaction conditions: 1.0 g of catalyst, 100 mL of glycerol aqueous solution (20 wt%), 1.0 MPa of N₂ pressure, 240 °C of reaction temperature, 3 h of reaction time.

illustrated in Fig. 10. Glycerol conversion grows rapidly in the beginning, reaching a high glycerol conversion of 71.4% at 3 h of reaction time, then it increases at a lower rate till a complete reaction for 7 h. 1,2-Propanediol is formed with a high selectivity of 54.6% at 1 h, which indicates the promotion on hydrogenation over Pt–Ni catalyst. The selectivity of 1,2-propanediol and ethylene glycol has a slight decrement with time due to catalytic cracking of 1,2-propanediol and ethylene into C1.

3.6 Reusability of Pt–Ni catalyst

Reusability tests were performed over 2.5Pt–2.5Ni/γ-Al₂O₃ catalyst, wherein the catalyst was washed and recycled after each cycle. As can be seen in Fig. 11, both the conversion and the selectivity of 1,2-propanediol has a slight decrease after each cycle, which was caused mainly by the coke formation and metal agglomeration. The conversion of glycerol and the selectivity of 1,2-propanediol decreased by only 4.77% and 8.96% after 5 cycles, suggesting the good stability and reusability of the catalyst.

4 Conclusions

This paper demonstrates a hydrogenolysis process of glycerol using hydrogen generated from aqueous phase reforming *in*



situ, which could proceed at a lower pressure and no longer need external hydrogen supply or hydrogen donor compounds. A series of Pt–M (M = Fe, Co, Ni, Cu, Zn, Sn) bimetallic catalysts supported on γ -Al₂O₃ have been synthesized, wherein the Pt–Ni catalyst was studied in detail owing to its high catalytic activity and selectivity.

The presence of Pt–Ni alloy was revealed by our catalyst characterization results, leading to a significant promotion of the conversion and selectivity over Pt–Ni bimetallic catalyst. A maximum conversion reached at a Pt/Ni ratio of 2.5 : 2.5. Higher reaction temperature favours the reaction activity increase, but the selectivity of 1,2-propanediol decreases significantly caused by excessive hydro-deoxygenation of 1,2-propanediol to propanol and lower alcohols. Glycerol conversion grows rapidly with reaction time initially, reaching 71.4% in 3 h. The reusability tests examined the good stability of the catalyst.

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