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## Confinement of alcohols to enhance CO<sub>2</sub> capture in MIL-53(Al)<sup>†</sup>

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CO<sub>2</sub> capture of MIL-53(Al) was enhanced by confining MeOH and *i*-PrOH within its micropores. Compared to MIL-53(Al), results showed an approximately 1.3 fold increase in CO<sub>2</sub> capture capacity (kinetic isothermal CO<sub>2</sub> adsorption experiments), *via* confining small amounts of both alcohols. Adsorption–desorption properties are investigated for MeOH and *i*-PrOH and the enthalpy of adsorption, for MeOH and *i*-PrOH, was measured by differential scanning calorimetry (DSC):  $\Delta H = 50$  and  $56$  kJ mol<sup>-1</sup>, respectively. Regeneration (CO<sub>2</sub> adsorption–desorption cycles) of the sample MeOH@MIL-53(Al) exhibited a loss on the CO<sub>2</sub> capacity of only 6.3% after 10 cycles and the desorption is accomplished by only turning the CO<sub>2</sub> flow off. Static CO<sub>2</sub> adsorption experiments (at 196 K) demonstrated a 1.25-fold CO<sub>2</sub> capture increase (from 7.2 mmol g<sup>-1</sup>, fully activated MIL-53(Al) to 9.0 mmol g<sup>-1</sup>, MeOH@MIL-53(Al)). The CO<sub>2</sub> enthalpy of adsorption for MIL-53(Al) and Me@OHMIL-53(Al) were estimated to be  $\Delta H = 42.1$  and  $50.3$  kJ mol<sup>-1</sup>, respectively. Computational calculations demonstrated the role of the hydrogen bonds formed between CO<sub>2</sub> molecules and confined MeOH and *i*-PrOH molecules, resulting in the enhancement of the overall CO<sub>2</sub> capture.

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## Introduction

The physicochemical properties (*e.g.* dynamics and structure) in nanometre confining porous scales of condensed matter are considerably different to what is observed at the macroscopic level. Typically, gas solubility in solvents, including those confined in macroporous solid materials, is normally defined by Henry's Law, which postulates a linear relationship between the concentration of a dissolved gas and its partial pressure above the solvent.<sup>1</sup> Although, some recent investigations have shown that the confinement of solvents in porous materials, considerably enhances the gas solubility with respect to the values predicted by Henry's law. This striking improvement is known as "oversolubility".<sup>2</sup> The oversolubility of confined solvents considerably modifies their viscosity, density, dielectric constant and specific heat.<sup>3</sup> For example, Garcia-Garibay *et al.*<sup>4</sup> demonstrated in a MOF material (UCLA-R3) that the confinement of DMF molecules considerably enhanced (4 orders of

magnitude) its dynamic viscosity which was comparable to that of honey.

Focusing on gas oversolubility (or gas enhancement by confining solvents), Luzar and Bratko<sup>5</sup> showed by computational simulations (molecular dynamics, MD) an increase of N<sub>2</sub> and O<sub>2</sub> solubility in water (from 5-fold to 10-fold) under confinement conditions in hydrophobic mesopores. By confining *n*-hexane, CHCl<sub>3</sub>, EtOH and H<sub>2</sub>O in mesostructured materials (MCM-41, SBA-15 and silica aerogel), remarkable H<sub>2</sub> solubility enhancements, were reported by Pera-Titus and co-workers.<sup>1,6</sup> Pelleng<sup>7</sup> confined *N*-methyl-2-pyrrolidone (NMP) in MCM-41 and demonstrated a 6-fold increase in CO<sub>2</sub> solubility. Interestingly, Llewellyn<sup>8</sup> reported a 5-fold increase in CO<sub>2</sub> capture by confining water in a mesoporous MOF material entitled MIL-100(Fe). This striking CO<sub>2</sub> increase was achieved when approximately 40 wt% of H<sub>2</sub>O was pre-adsorbed in the mesopores of MIL-100(Fe).

In all the previous examples only mesoporous materials showed gas oversolubility properties. Interestingly, for microporous materials this phenomenon has not been observed as thoroughly demonstrated by Llewellyn and co-workers<sup>8</sup> in a MOF microporous material UiO-66. Thus, in order to referring to gas oversolubility it is necessary to incorporate (pre-adsorb) considerably high amounts of solvent (*e.g.* H<sub>2</sub>O, *n*-hexane and EtOH) prior any gas adsorption. For example, Farrusseng *et al.*<sup>9</sup> remarkably reported a 22-fold improvement on the H<sub>2</sub> uptake (at 298 K and 30 bar) on MIL-101(Cr) by confining *n*-hexane. By a solvent wet impregnation method,<sup>9</sup> they loaded *n*-hexane into the fully activated MOF material and this corresponded to the

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60% of the pore volume. In other words, 60% of the pore volume of MIL-101(Cr), was filled with *n*-hexane.

However, it is possible to confine small amounts of solvents in micropores materials to enhance gas adsorption properties. Certainly, this phenomenon cannot be referred as gas over-solubility since there is not “enough” solvent to solubilise gas molecules. Walton *et al.*<sup>10</sup> exhibited that small amounts of water can enhance CO<sub>2</sub> capture in microporous MOF materials. These small amounts of H<sub>2</sub>O can interact with selected functional groups within the pores of these materials. In particular, they demonstrated that hydroxyl (–OH) functional groups act as a directing agent for water molecules inside the pores allowing a more efficient and ordered packing of H<sub>2</sub>O.<sup>11</sup> In addition, Yaghi<sup>12</sup> showed that these functional groups (–OH), significantly improve the affinity of MOF materials to water.

Previously, we have demonstrated that small amounts of pre-adsorbed H<sub>2</sub>O into microporous MOF materials considerably enhanced their CO<sub>2</sub> capture properties.<sup>13</sup> Additionally, our research group started to investigate the confinement of alcohols in MOFs to increase their CO<sub>2</sub> capture capabilities and this was exemplified with the pre-adsorption of small amounts of EtOH in InOF-1.<sup>14</sup> Therefore, we continue with the development of hybrid adsorbent MOF materials (*via* confining small amounts of alcohols within their micropores) which can contribute to new CO<sub>2</sub> capture technologies.<sup>15</sup> Among ‘the twelve principles of CO<sub>2</sub> chemistry’ that Poliakoff<sup>16</sup> proposed, CO<sub>2</sub> capture constitutes one of these challenges (maximise integration). Therefore, the search for post-synthetically modified MOFs with high structural stability, adsorption capacity, solvent stability, fast sorption kinetics and mild regeneration conditions, is nowadays a very hot research field.<sup>17,18</sup>

Herein, we report the augmented CO<sub>2</sub> capture properties of the microporous material MIL-53(Al), first reported by Serre and co-workers,<sup>19</sup> upon confining small amounts of alcohols (methanol and isopropanol), together with MeOH and *i*-PrOH adsorption–desorption properties of MIL-53(Al).

## Experimental section

### Synthetic preparations

MIL-53(Al), [Al(OH)(BDC)], was synthesised *via* a continuous flow process,<sup>20</sup> using merely water as the reaction medium. After the Al(III)-MOF material was synthesised, it went through a calcination process (extraction of terephthalic acid from within the pores of MIL-53(Al)) by heating the material up to 330 °C for 3 days. Thermogravimetric analysis (calcined MIL-53(Al)) (see Fig. S1, ESI†) and bulk powder X-ray diffraction patterns (see Fig. S2, ESI†) of the calcined MIL-53(Al) confirmed the retention of its structural integrity upon terephthalic acid removal. It is important to clarify, as previously reported,<sup>19b,c</sup> that the calcined MIL-53(Al), at room temperature, corresponds to the *lt* form (water molecules are located inside the channels of the material).<sup>19b,c</sup> When the calcined MOF sample is activated (180 °C and 10<sup>–3</sup> bar for 2 h) there is a transformation from the *lt* form to the *ht* form.<sup>19b,c</sup> This characteristic structural transformation is very well known as the breathing effect of MIL-53.<sup>19d</sup> N<sub>2</sub> adsorption isotherms for activated MIL-53(Al), *vide*

*supra*, at 77 K were used to estimate the BET surface area (0.01 <  $P/P_0$  < 0.04) of 1098 m<sup>2</sup> g<sup>–1</sup>.

### Adsorption isotherms for N<sub>2</sub>, CO<sub>2</sub>, MeOH and *i*-PrOH (isopropanol)

N<sub>2</sub> isotherms (up to 1 bar and 77 K) were recorded on a Belsorp mini II analyser under high vacuum in a clean system with a diaphragm pumping system. CO<sub>2</sub> isotherms up to 1 bar at 196 K, 212 K and 231 K, were recorded on a Belsorp HP (High Pressure) analyser. MeOH and *i*-PrOH isotherms were recorded in a DVS Advantage 1 instrument from Surface Measurement System. Ultra-pure grade (99.9995%) N<sub>2</sub> and CO<sub>2</sub> gases were purchased from PRAXAIR.

### Kinetic CO<sub>2</sub> uptake experiments

Kinetic experiments were performed by using a thermobalance (Q500 HR, from TA) at 30 °C with a constant CO<sub>2</sub> flow (60 mL min<sup>–1</sup>).

## Results and discussion

### Methanol and isopropanol adsorption studies

Methanol (MeOH) and isopropanol (*i*-PrOH) adsorption properties were investigated for MIL-53(Al). First, a sample of the calcined MIL-53(Al) was placed in an analyser cell (DVS Advantage 1 instrument) and activated at 180 °C for 2 h and under a flow of N<sub>2</sub>. When the sample was fully degassed and cooled down to 30 °C, a methanol adsorption–desorption isotherm was carried out from % $P/P_0$  = 0 to 85 (Fig. 1). The adsorbed amount of MeOH gradually increased with increasing pressure up to % $P/P_0$  = 10. Then, a rapid MeOH uptake was observed in the pressure range from % $P/P_0$  = 10 to 42. Finally, from % $P/P_0$  = 12 to 85 there was a slow but gradual weight increase, and the maximum MeOH uptake was ~8.1 mmol g<sup>–1</sup> (26.1 wt%). The overall MeOH isotherm exhibited a sigmoidal shape and a strong hysteresis loop (at % $P/P_0$  = 2–12) was observed with marked stepped profiles in the desorption phase (Fig. 1, open circles). The pore dimensions of activated MIL-53(Al), *ht* form,<sup>19b,c</sup> are approximately 2.6 Å × 13.6 Å which are considerably much larger than the kinetic diameter of

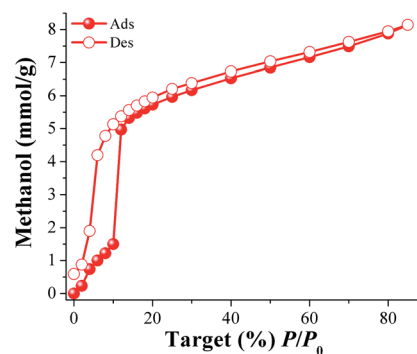


Fig. 1 Methanol adsorption isotherm at 30 °C of MIL-53(Al) from % $P/P_0$  = 0 to 85. Solid circles represent adsorption, and open circles show desorption.



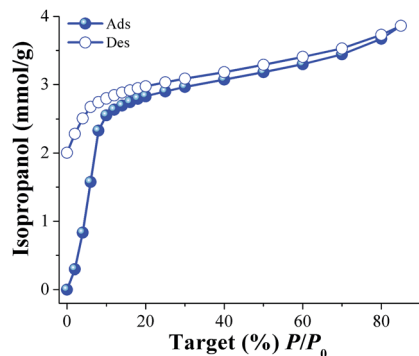


Fig. 2 Isopropanol adsorption isotherm at 30 °C of MIL-53(Al) from %  $P/P_0 = 0$  to 85. Solid circles represent adsorption, and open circles show desorption.

methanol ( $\sim 3.6$  Å). Thus, the observed hysteresis is most likely due to moderately strong host-guest interactions, which result in an enhanced affinity of MIL-53(Al) for MeOH. These interactions are the result of methanol molecules forming hydrogen bonds with the bridging hydroxo functional groups ( $\mu_2$ -OH), within the pores. This phenomenon was previously observed in a remarkable work by Maurin *et al.*<sup>19e</sup> They studied the methanol adsorption properties of MIL-53(Cr), an isostructural material to MIL-53(Al), finding a very similar MeOH adsorption-desorption isotherm and a strong and localised hydrogen bond between MeOH and the hydroxo functional group ( $\mu_2$ -OH).<sup>19e</sup>

Later, a new calcined MIL-53(Al) sample was activated (as previously described) and an isopropanol adsorption-desorption isotherm was performed from % $P/P_0 = 0$  to 85 at 30 °C (Fig. 2). To the best of our knowledge, this is the first time that the adsorption properties of isopropanol (*i*-PrOH) are described in MIL-53(Al). From 0 to 10 (% $P/P_0$ ) the uptake of *i*-PrOH was rapidly increased (indicative of favourable host-guest interactions) achieving an *i*-PrOH uptake of approximately 2.5 mmol  $g^{-1}$  (15.3 wt%). Then, from % $P/P_0 = 10$  to 85 a much slower (but constant) alcohol uptake was observed with a maximum of approximately 3.8 mmol  $g^{-1}$  (23.2 wt%). A relatively strong hysteresis was observed in the desorption phase (Fig. 2, open symbols). This hysteresis occurred mainly in the low pressure range from % $P/P_0 = 0$  to 10. As in the previous case (MeOH), the kinetic diameter of *i*-PrOH is 4.6 Å which is considerably smaller than the pore openings of activated MIL-53(Al), (2.6 Å  $\times$  13.6 Å, *ht* form),<sup>19b,c</sup> suggesting again, the formation of hydrogen bonds with the bridging hydroxo functional groups ( $\mu_2$ -OH).<sup>19e</sup>

When both alcohols (MeOH and *i*-PrOH) uptakes in MIL-53(Al) are compared at low loadings (% $P/P_0 = 0$  to 10), there is a clear preference for *i*-PrOH over MeOH (2.5 vs. 1.4 mmol  $g^{-1}$ , respectively) which can be attributed to a stronger interaction of *i*-PrOH with the material. In order to confirm this, the enthalpy of adsorption ( $\Delta H$ ) for *i*-PrOH was experimentally measured by differential scanning calorimetry (DSC) from room temperature to 600 °C (with a ramp of 5 °C  $min^{-1}$ ). The  $\Delta H$  value was equal to 56 kJ  $mol^{-1}$  (see Fig. S3 ESI†). When the same experimental determination was performed for MeOH, the  $\Delta H$  value was equal to 50 kJ  $mol^{-1}$  (see Fig. S4 ESI†), in good

correlation with the alcohol uptakes (low loadings). When the total uptake of these alcohols is compared (MeOH = 8.1 mmol  $g^{-1}$  and *i*-PrOH = 3.8 mmol  $g^{-1}$ ), MIL-53(Al) can adsorb considerably more MeOH than *i*-PrOH, presumably, due to the size of the alcohol molecules (methanol is smaller than isopropanol; kinetic diameters = 3.6 Å and 4.6 Å, respectively).

### CO<sub>2</sub> capture studies

Isothermal and dynamic CO<sub>2</sub> adsorption experiments (kinetic) were performed on desolvated MIL-53(Al). First, a sample of the calcined MIL-53(Al) was placed inside a thermobalance (Q500 HR) and activated by heating from room temperature to 180 °C for 2 h and under a flow of pure N<sub>2</sub> gas flow. Then, the sample was cooled down to 30 °C under N<sub>2</sub> flow. After the sample had reached 30 °C, the N<sub>2</sub> purge flow was switched to 60 mL  $min^{-1}$  of CO<sub>2</sub>. Fig. 3 (MIL-53(Al)) exhibits the kinetic CO<sub>2</sub> uptake experiment at 30 °C. At this temperature, the material showed the maximum weight percentage gain, which indicates the maximum amount of CO<sub>2</sub> captured. This amount corresponds to 3.5 wt%, which was rapidly reached after only 4 min remains constant until the end of the experiment (12 min), Fig. 3 (MIL-53(Al)).

Later, a calcined sample of MIL-53(Al) was activated (180 °C for 2 h and under a flow of N<sub>2</sub>), cooled down to 30 °C (under N<sub>2</sub>) and saturated with MeOH (see ESI†). After an activation protocol (see ESI†) the residual amount of MeOH was equal to 2 wt%. The reproducibility of this protocol was confirmed by performing 5 independent experiment (see ESI†). Hereinafter, this sample will be referred as MeOH@MIL-53(Al), [Al(OH)(BDC)]·MeOH<sub>0.08</sub>. Similar procedure was carried out for sample *i*-PrOH@MIL-53(Al), [Al(OH)(BDC)]·*i*PrOH<sub>0.05</sub>, as it is described in the ESI.†

It was decided to only pre-adsorbed small amounts of alcohols (MeOH and *i*-PrOH) in MIL-53(Al) samples, based on the investigation of confined H<sub>2</sub>O in the micropores of MIL-53(Cr),<sup>21</sup> (a MOF material which is isostructural to MIL-53(Al)). Then, Paesani and co-workers<sup>21</sup> demonstrated by computational infrared spectroscopy that at low water loadings, these water molecules interact strongly with the hydroxo ( $\mu_2$ -OH)

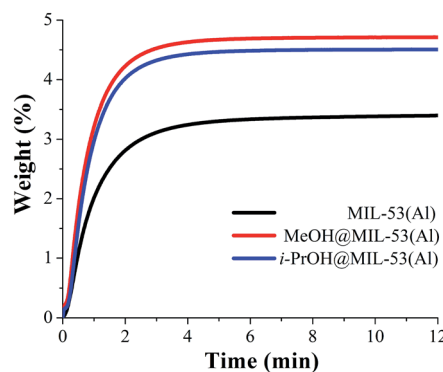


Fig. 3 Kinetic CO<sub>2</sub> uptake experiments performed at 30 °C with a CO<sub>2</sub> flow of 60 mL  $min^{-1}$  in MIL-53(Al), (black curve); MeOH@MIL-53(Al), (red curve) and *i*-PrOH@MIL-53(Al), (blue curve).



functional groups, *via* hydrogen bonding, which are located inside the pore walls of MIL-53(Cr). Continuing with the investigation of MIL-53, by different calculation methodologies, Haigis<sup>22</sup> employed molecular dynamics (MD), to show that H<sub>2</sub>O molecules can form strong hydrogen bonds with the  $\mu_2$ -OH functional groups, in MIL-53(Cr), as a function of water loading. In addition, Maurin *et al.*<sup>23</sup> corroborated by GCMC computational simulations, in MIL-53(Cr), that at low water loadings, these H<sub>2</sub>O molecules are regularly accommodated inside all the pores of the material.

Certainly, all the previous computational approaches indicated the role of the  $\mu_2$ -OH functional groups (inside the micropores of MIL-53(Cr)) to “pin” small amounts of water *via* hydrogen bonding. Complementing to these calculations, we experimentally demonstrated that small amounts of EtOH (2.6 wt%), confined within the micropores of InOF-1 (ref. 14) can: (i) hydrogen-bond to the similar hydroxo functional (In<sub>2</sub>( $\mu_2$ -OH)) which was visualised by single crystal X-ray diffraction; and (ii) significantly enhance CO<sub>2</sub> capture (2.7 fold).

Therefore, we rationalised the hypothesis of low MeOH and *i*-PrOH loadings where the micro-porous channels of MIL-53(Al) could efficiently accommodate these alcohols molecules. As a result of this very well ordered positioning of MeOH and *i*-PrOH, these confined alcohol molecules could help to pack more efficiently CO<sub>2</sub> molecules and finally enhance the total CO<sub>2</sub> capture.

Then, a kinetic CO<sub>2</sub> experiment, at 30 °C, was carried out on the MeOH@MIL-53(Al) sample. The maximum amount of CO<sub>2</sub> captured corresponded to 4.7 wt%, which was reached at approximately 4 min and it was constant until the end of the experiment (12 min), Fig. 3 (MeOH@MIL-53). It is important to mention that samples of MeOH@MIL-53(Al) were prepared with anhydrous methanol (<0.005% water) and methanol (reagent alcohol, 95%). The kinetic CO<sub>2</sub> experiments showed no difference in the maximum amount of CO<sub>2</sub> captured. Additionally, we also tried different small residual-amounts of MeOH: 3%, 4% and 5% and the best result was obtained with 2 wt% of MeOH.

Therefore, the CO<sub>2</sub> capture was approximately 1.3-fold improved (from 3.5 wt% to 4.7 wt%), when small amounts of MeOH were pre-adsorbed in MIL-53(Al). Moreover, the 1.3-fold increase was reached at the same time (~4 min) than the MIL-53(Al) sample, showing that the CO<sub>2</sub> adsorption kinetics were highly improved due to the MeOH presence.

Later, the sample *i*-PrOH@MIL-53(Al) was prepared as previously described (*vide supra* and see ESI<sup>†</sup>) where the amount of pre-adsorbed isopropanol was equal to 2 wt%. Fig. 3 exhibits the kinetic CO<sub>2</sub> experiment performed on *i*-PrOH@MIL-53(Al) and the maximum amount of adsorbed CO<sub>2</sub> (captured) was equal to 4.5 wt%. This value is slightly smaller to the one observed for sample MeOH@MIL-53(Al), indicating that the pre-adsorption of MeOH in MIL-53(Al) favours the overall capture of CO<sub>2</sub>. It is worth to emphasise that the confinement of small amounts of both alcohols (2 wt%) enhances the CO<sub>2</sub> capture properties of this MOF material.

Long-term regeneration capacity is a fundamental parameter for any CO<sub>2</sub> capture material and it is desirable to show very low energy requirements for CO<sub>2</sub> release.<sup>24</sup> In industrial separation

processes this step is typically very expensive and complicated.<sup>25</sup> Among many current methodologies to this target, perhaps, the most common is the use of vacuum and temperature swing adsorption. For example, Long and co-workers<sup>26</sup> reported a working CO<sub>2</sub> capacity (total CO<sub>2</sub> adsorption) of ~7 wt% at room temperature (25 °C) on mmen-CuBTTri. This MOF material was regenerated by switching the flow (15% CO<sub>2</sub> in N<sub>2</sub>) to a pure N<sub>2</sub> stream followed by increasing the temperature up to 60 °C. Denayer and co-workers<sup>27</sup> reported a total CO<sub>2</sub> adsorption of 3.7 wt% for NH<sub>2</sub>-MIL-53 and the regeneration of this material was performed under purge flow at 159 °C.

In order to evaluate the regeneration properties of MeOH@MIL-53(Al), a new sample was prepared (by confining 2 wt% of MeOH in MIL-53(Al)) and kinetic CO<sub>2</sub> adsorption-desorption experiments, at 30 °C, were carried on (Fig. 4). We decided to only evaluate the regeneration properties of MeOH@MIL-53(Al) since it showed the best CO<sub>2</sub> capture result. Each cycle consists of an adsorption step (15 min) and a desorption step (15 min), providing a cycling time of only 30 min without the use of N<sub>2</sub> purge nor increasing the temperature.

Simply, by turning off the CO<sub>2</sub> flow (corresponding to the desorption step) and keeping the adsorption temperature (30 °C), the total regeneration of the MeOH@MIL-53(Al) sample was accomplished. From the first cycle (4.7 wt% CO<sub>2</sub> adsorption) to the tenth cycle (4.4 wt% CO<sub>2</sub> adsorption) it was observed a loss of the CO<sub>2</sub> capacity (from 4.7 to 4.4 wt%) which represents a loss on the CO<sub>2</sub> capacity of only 6.3% (Fig. 4). Although there was a small loss in the CO<sub>2</sub> capacity, this result is noteworthy since there is no need to use a purge gas (*e.g.* N<sub>2</sub>) and more significantly no thermal re-activation of the sample is required, resulting in a very low cost separation process.

In order to describe the CO<sub>2</sub> adsorption properties of MeOH@MIL-53(Al), we performed static (increasing the partial pressure from 0 to 1 bar) and isothermal (196 K) CO<sub>2</sub> adsorption experiments on MeOH@MIL-53(Al) samples. It was decided to perform these experiments at 196 K since the adsorption of CO<sub>2</sub> at 30 °C (303 K) is problematic due to proximity to the critical temperature of CO<sub>2</sub>.<sup>28</sup> The uncertainty of the  $\delta_{\text{CO}_2}$  (density) of the CO<sub>2</sub> adsorbed, and since at that temperature the CO<sub>2</sub> saturation

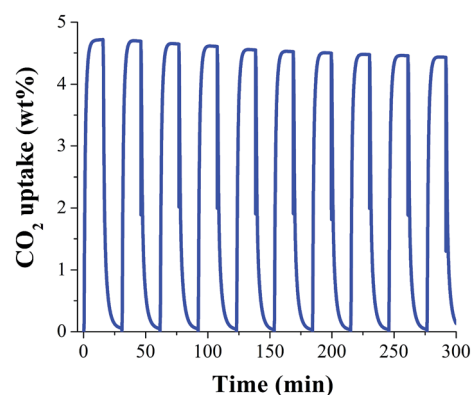


Fig. 4 Adsorption-desorption cycling for MeOH@MIL-53(Al), showing a reversible CO<sub>2</sub>.



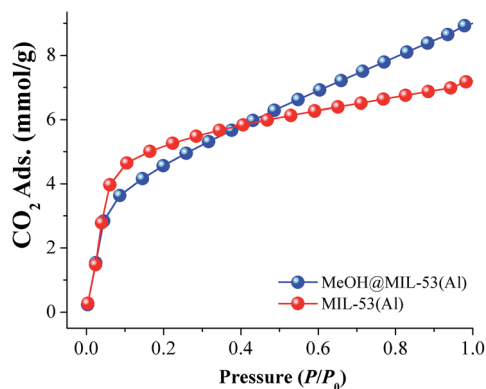


Fig. 5 Static CO<sub>2</sub> adsorption performed from 0 to 1 bar at 196 K on MIL-53(Al), (red circles) and MeOH@MIL-53(Al), (blue circles).

pressure is extremely high, the range of  $P/P_0$  is limited to 0.02 at sub-atmospheric pressures.<sup>29</sup> It has been proposed that adsorption in well-defined micropores occurs by a pore-filling mechanism rather than surface coverage.<sup>29,30</sup> As an example, N<sub>2</sub> molecules at 77 K can fill these micropores in a liquid-like fashion at very low relative pressures (below 0.01). On the other hand, CO<sub>2</sub> adsorbed at approximately ambient temperatures (298 or 303 K) can only form a monolayer on the walls of the micropores.<sup>30</sup> Therefore, to accomplish pore-filling within the micropores of MOFs and a more accurate description of the CO<sub>2</sub> adsorption properties of these microporous materials, CO<sub>2</sub> gas adsorption experiments at 196 K are preferred.<sup>31</sup>

First, a CO<sub>2</sub> adsorption experiment at 196 K was carried on a fully activated (180 °C for 1 h and 10<sup>-3</sup> bar) sample of MIL-53(Al) exhibiting a total CO<sub>2</sub> uptake of 7.2 mmol g<sup>-1</sup> (31.7 wt%), (see Fig. 5, MIL-53(Al)). Later, a MeOH@MIL-53(Al) sample was placed in a high-pressure cell (Belsorp HP) and gently evacuated to remove any absorbed moisture. The CO<sub>2</sub> uptake was measured from 0 to 1 bar at 196 K and the resultant CO<sub>2</sub> adsorption exhibited a characteristic Type-I isotherm with a total CO<sub>2</sub> capture of 9.0 mmol g<sup>-1</sup> (39.6 wt%), (Fig. 5, MeOH@MIL-53(Al)). Then, at 1 bar and 196 K, the CO<sub>2</sub> capture was approximately 1.25-fold increased (from 7.2 to 9.0 mmol g<sup>-1</sup>) when small amounts of MeOH are present within the micropores of MIL-53(Al). The evaluation of the BET surface area of MeOH@MIL-53(Al) was equal to 762 m<sup>2</sup> g<sup>-1</sup> with a pore volume of 0.39 cm<sup>3</sup> g<sup>-1</sup> (lower values than for the fully activated MIL-53(Al), BET = 1096 m<sup>2</sup> g<sup>-1</sup> and pore volume = 0.56 cm<sup>3</sup> g<sup>-1</sup>). In addition, we measured CO<sub>2</sub> adsorption isotherms at 212 K (dry ice and chloroform bath) and 231 K (dry ice and acetonitrile bath), in order to calculate the enthalpy of adsorption ( $\Delta H$ ) by isosteric method for both samples: MIL-53(Al) and MeOH@MIL-53(Al), (see Fig. S5–S8 ESI†). The values were estimated to be 42.1 and 50.3 kJ mol<sup>-1</sup> for MIL-53(Al) and MeOH@MIL-53(Al), respectively. Thus,  $\Delta H$  for CO<sub>2</sub> was enhanced when small quantities of MeOH are confined within the material MIL-53(Al).

### Computational studies

In order to investigate the relationship between the presence of methanol and isopropanol (confined into MIL-53(Al)) and their

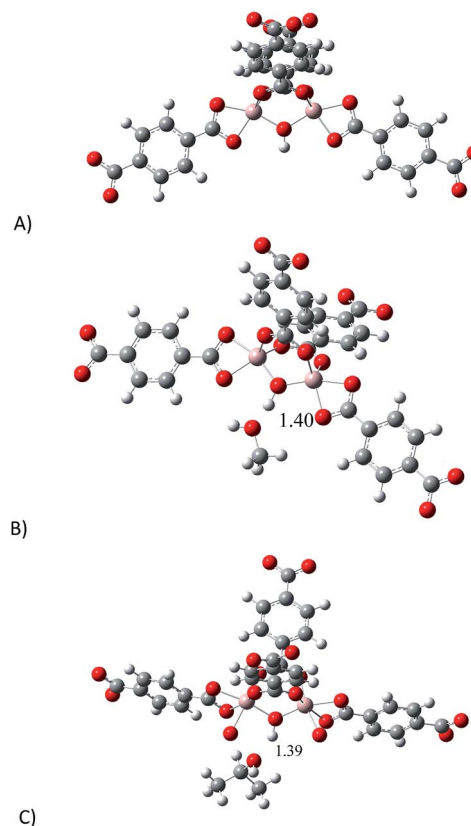


Fig. 6 Optimised structures of: (A) proposed model to represent the active site; (B) model interacting with MeOH and (C) model interacting with *i*-PrOH.

affinity towards CO<sub>2</sub>, a model of the binuclear [Al<sub>2</sub>(μ<sub>2</sub>-OH)] building block (reactive section) was taken and the geometry was optimised (see ESI,† computational details). Since the most representative section of the model is related to the μ<sub>2</sub>-OH group, we decided to study the interactions between μ<sub>2</sub>-OH and the incorporation of different analytes (MeOH, *i*-PrOH and CO<sub>2</sub>). Fig. 6 shows the optimised structure of the proposed model (A) and the optimised structures for the model interacting with MeOH (B) and *i*-PrOH (C). As it was expected, both alcohols form hydrogen bonds with the μ<sub>2</sub>-OH group. Bond distances of these hydrogen bonds are very similar (1.39 and 1.40 Å). Our computations suggest that the interaction of both alcohol molecules (MeOH and *i*-PrOH) with the μ<sub>2</sub>-OH group of the model is very similar, since the distance of the hydrogen bond is practically the same. This result correlates with the small CO<sub>2</sub> capture difference on confining small amounts of MeOH vs. *i*-PrOH within MIL-53(Al), see Fig. 3.

Later, we introduced a single CO<sub>2</sub> molecule in all the optimised structures: proposed model (empty) and the models interacting with MeOH and *i*-PrOH. In Fig. 7 is presented the optimised structures of all the models interacting with CO<sub>2</sub>. As expected, the single CO<sub>2</sub> molecule forms hydrogen bonds in all the structures. It is very well studied that the hydrogen bond distance is an indication on the strength of the interaction between molecules.<sup>32</sup> Thus, if we compare the μ<sub>2</sub>-OH...O=C=O bond distances, it is possible to observe that the structure



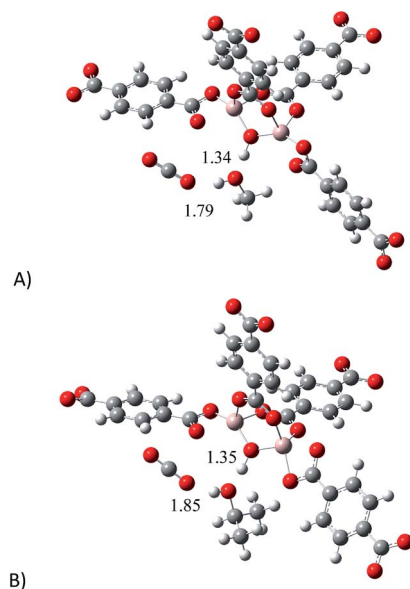


Fig. 7 Optimised structures of: (A) proposed model interacting with MeOH and CO<sub>2</sub> and (B) proposed model interacting with *i*-PrOH and CO<sub>2</sub>.

containing MeOH establishes a shorter hydrogen bond (1.79 Å, Fig. 7A) than the structure with *i*-PrOH (1.85 Å, Fig. 7B). This slight difference, in the bond length, can actually explain the small dissimilarity in the overall capture of CO<sub>2</sub> when small amounts of the alcohols are confined within the MOF material MIL-53(Al), see Fig. 3. Therefore, our computational calculations highlighted the significance of the hydrogen bonds formed between CO<sub>2</sub> molecules and confined alcohol molecules: on increasing the strength (diminishing the distance) of the hydrogen bond between the μ<sub>2</sub>-OH group and the confined alcohol, the overall ability to capture CO<sub>2</sub> increases.

## Conclusions

The microporous Al(III)-based MOF material MIL-53(Al) exhibited, by kinetic isotherm CO<sub>2</sub> experiments, a total CO<sub>2</sub> uptake of 3.5 wt%. When confining small amounts of methanol (MeOH) and isopropanol (*i*-PrOH) (2 wt%) within MIL-53(Al), the CO<sub>2</sub> capture incremented to 4.7 and 4.5 wt%, respectively, which approximately corresponds to a 1.3-fold increase. MeOH and *i*-PrOH adsorption properties were investigated for MIL-53(Al). Uptakes (at low loadings: %P/P<sub>0</sub> = 0 to 10) of both alcohols in MIL-53(Al) showed a clear preference for *i*-PrOH over MeOH (2.5 vs. 1.4 mmol g<sup>-1</sup>, respectively) which was attributed to a stronger interaction of *i*-PrOH with the material. Enthalpy of adsorption (Δ*H*) for *i*-PrOH and MeOH were experimentally measured by differential scanning calorimetry (DSC) with values of Δ*H* = 56 and 50 kJ mol<sup>-1</sup>, respectively. MeOH@MIL-53(Al) can reversibly adsorb/desorb CO<sub>2</sub> with a loss on the CO<sub>2</sub> capacity of only 6.3% after 10 cycles and the desorption is performed by turning the CO<sub>2</sub> flow off without the need to change the temperature or use inert gas. Static and isothermal CO<sub>2</sub> experiments (from 0 to 1 bar of CO<sub>2</sub> at 196 K) also demonstrated a 1.25-fold CO<sub>2</sub> capture

increase (from 7.2 mmol g<sup>-1</sup>, MIL-53(Al) fully activated to 9.0 mmol g<sup>-1</sup>, MeOH@MIL-53(Al)). The CO<sub>2</sub> enthalpy of adsorption for MIL-53(Al) and MeOH@MIL-53(Al) were calculated from CO<sub>2</sub> adsorption isotherms at 212 K and 231 K to be Δ*H* = 42.1 and 50.3 kJ mol<sup>-1</sup>, respectively. Quantum calculations demonstrated the role of the hydrogen bonds formed between CO<sub>2</sub> molecules and confined MeOH and *i*-PrOH molecules: on increasing the strength (shorting the distance) of the hydrogen bond between the hydroxyl functional group (μ<sub>2</sub>-OH) group and the confined alcohol, the overall result is the enhancement of the CO<sub>2</sub> capture. We are currently exploring other MOF materials and the confinement of different solvents (polar and non-polar) which could enhance CO<sub>2</sub> capture in MOFs.

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