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# Synthesis of $\alpha$ -CaSO<sub>4</sub>·0.5H<sub>2</sub>O from flue gas desulfurization gypsum regulated by C<sub>4</sub>H<sub>4</sub>O<sub>4</sub>Na<sub>2</sub>·6H<sub>2</sub>O and NaCl in glycerol-water solution

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A brand new method to transform flue gas desulfurization gypsum (FGD gypsum) into  $\alpha$ -calcium sulfate hemihydrate ( $\alpha$ -HH) with short hexagonal prisms mediated by succinic acid disodium salt hexahydrate (C<sub>4</sub>H<sub>4</sub>O<sub>4</sub>Na<sub>2</sub>·6H<sub>2</sub>O) and NaCl in glycerol-water solution is studied, in which the appropriate reaction temperature is 90 °C. The addition of NaCl facilitates the dissolution of calcium sulfate dihydrate (DH) and creates much higher supersaturation which is a greater driving force for the phase transformation from DH to  $\alpha$ -HH. C<sub>4</sub>H<sub>4</sub>O<sub>4</sub>Na<sub>2</sub>·6H<sub>2</sub>O as the crystal modifier effectively suppresses the  $\alpha$ -HH crystal growth along the *c* axis, and the products generally change from needle-like particles to fat and short hexagonal prisms, which is attributed to the preferential adsorption of C<sub>4</sub>H<sub>4</sub>O<sub>4</sub><sup>2-</sup> on the top facets of the crystals by chelating Ca<sup>2+</sup>.

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## 1. Introduction

Flue gas desulfurization gypsum (FGD gypsum), which is mainly composed of CaSO<sub>4</sub>·2H<sub>2</sub>O (DH), is the industrial waste residue produced by the limestone-gypsum wet process of flue gas desulfurization technology. The bulk deposition of FGD gypsum not only takes up plenty space, but also results in land and water pollution. Methods to rationally utilize FGD gypsum have drawn much attention in recent years. One of the most important methods to reuse FGD gypsum is the production of calcium sulfate hemihydrate (HH), including  $\alpha$ -calcium sulfate hemihydrate ( $\alpha$ -HH) and  $\beta$ -calcium sulfate hemihydrate ( $\beta$ -HH). Indisputably,  $\alpha$ -HH is superior to  $\beta$ -HH due to its better workability and higher strength. It has been widely applied in moldings, special binder systems, dental materials, and in the construction industry.

Numerous researchers have explored methods for the production of  $\alpha$ -HH reusing FGD gypsum. One method is the autoclaving method,<sup>1</sup> which involves heating DH in an autoclave at elevated temperatures and pressure under an atmosphere of saturated vapor. Obviously, this is an expensive procedure. Another method is the salt solution process under atmospheric pressure and at mild temperature,<sup>2-5</sup> which requires high-concentration salt solutions, but evidently results in serious corrosion to equipment.

Recent scientific research has suggested that the transformation from DH to  $\alpha$ -HH can be realized in alcohol water

solution under mild conditions.<sup>6,7</sup> Compared with the autoclave and salt solution methods, this process has the advantages of mild reaction conditions and no corrosion to equipment, and is thus more favorable for continuous industrial production. Although the transition from DH to  $\alpha$ -HH is kinetically unfavorable in alcohol water solution, the addition of a small amount of salt as a phase transformation accelerator can significantly shorten the transition time.<sup>8</sup> However, few researchers have explored the preparation of  $\alpha$ -HH with a specific morphology and size using FGD gypsum in alcohol water solution. The morphology and size of  $\alpha$ -HH usually determine its properties and functionalities. For instance,  $\alpha$ -HH particles with a low aspect ratio or spherical shape possess better injectability and mechanic strength, and are preferable for use as bone cements.<sup>9,10</sup> Therefore, in order to prepare  $\alpha$ -HH products with low aspect ratios, crystal modifiers, among which carboxylic acids are highly effective,<sup>5,11,12</sup> tend to be added during the transformation process. However, in alcohol water solutions, the influence of crystal modifiers on the morphology of  $\alpha$ -HH crystals and transformation time from DH to  $\alpha$ -HH has been rarely reported.

Herein, we introduce a brand new process to prepare  $\alpha$ -HH with short hexagonal prisms by reusing FGD gypsum in glycerol-water solution. In the procedure, succinic acid disodium salt hexahydrate (C<sub>4</sub>H<sub>4</sub>O<sub>4</sub>Na<sub>2</sub>·6H<sub>2</sub>O) and NaCl are used as the crystal modifier and phase transformation accelerator, respectively, and the influence of the crystal modifier on the morphology of the  $\alpha$ -HH crystals and the transformation time in glycerol-water solution is studied.

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## 2. Experimental

### 2.1 Materials

FGD gypsum, the chemical composition of which is given in Table 1, was received from Panzhihua Iron & Steel Co., Ltd., Sichuan Province, China. Glycerol, NaCl and succinic acid disodium salt hexahydrate ( $C_4H_4O_4Na_2 \cdot 6H_2O$ ) were purchased from Sinopharm Chemical Reagent Co., Ltd., Shanghai, China.

### 2.2 Experimental procedure

Glycerol (65 wt%)-water solutions with a certain amount of NaCl (by weight of FGD gypsum) and succinic acid disodium salt hexahydrate ( $C_4H_4O_4Na_2 \cdot 6H_2O$ ) (by weight of FGD gypsum) were first added to a three-necked flask equipped with a reflux condenser on top of it, and the solution was stirred with a magnetic stirrer at a constant rate of 150 rpm and preheated to

Table 1 The chemical composition of the FGD gypsum (wt%)

CaO	SO <sub>3</sub>	H <sub>2</sub> O	SiO <sub>2</sub>	Fe <sub>2</sub> O <sub>3</sub>	Al <sub>2</sub> O <sub>3</sub>	MgO	PbO	K <sub>2</sub> O	Total
36.87	42.63	14.95	0.73	0.31	0.31	0.11	0.06	0.04	96.01

90 °C in an oil bath. Then 60 g pretreated FGD gypsum (20 wt% solid content) was added to the reactor. During the reaction, 20 mL slurry was withdrawn at certain time intervals. Half of the sample was filtrated immediately, washed three times with boiling water and then rinsed once with ethanol before it was dried at 60 °C for 2 hours in an oven. The other 10 mL of slurry was filtered through a syringe filter with a 0.2 μm cellulose membrane for Ca<sup>2+</sup> concentration determination.

### 2.3 Characterization

The chemical compositions of FGD gypsum were investigated using X-ray fluorescence spectroscopy (XRF, Axios mAX, PANalytical B.V., Netherlands). The structures of the samples were determined by X-ray diffraction (XRD D8 Advanced, Bruker, Germany) using Cu Kα radiation ( $\lambda = 1.54178 \text{ \AA}$ ) at a scanning rate of  $5^\circ \text{ min}^{-1}$  in the  $2\theta$  range of  $5^\circ$  to  $70^\circ$ . The morphology of the samples was characterized with an optical microscope (DFC 480, Leica Microsystems Ltd., Germany). The surfaces of the crystal products were analyzed by X-ray photoelectron spectroscopy (XPS, ESCALAB 250Xi, Thermo Fisher, USA) with an.

Al Kα photon energy of 1486.6 eV. The C 1s peak at 284.8 eV, which is related to the carbon adsorbed on the surface during the exposure of the samples to ambient atmosphere, was used

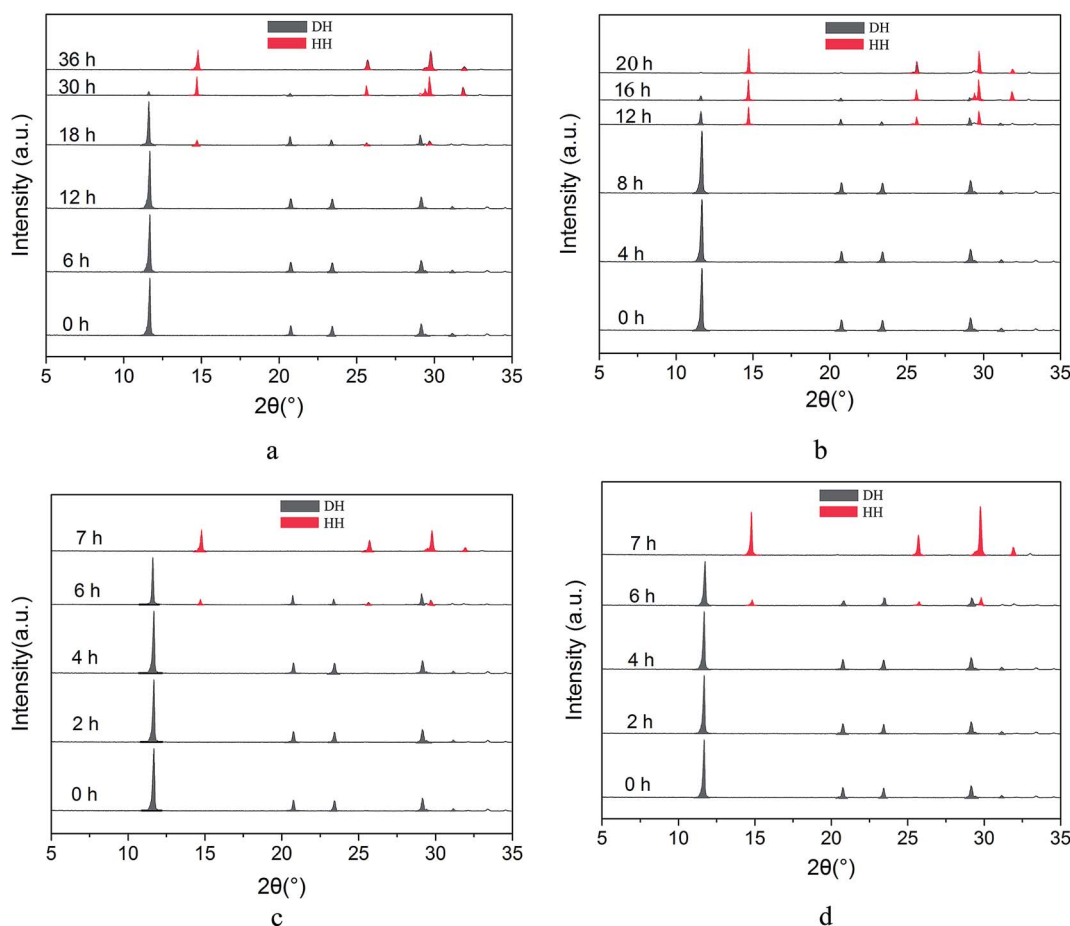


Fig. 1 XRD patterns of the crystal products at different time intervals during the phase transformation in glycerol (65 wt%)-water solution without NaCl at different reaction temperatures ((a) 80 °C; (b) 85 °C; (c) 90 °C and (d) 95 °C).



as the reference for all spectra. The interaction between the crystal modifier and the crystal surfaces was analyzed by Fourier transform infrared spectroscopy (FT-IR, IRAffinity-1, Shimadzu, Japan) at a resolution of  $4\text{ cm}^{-1}$  over the frequency range of  $400\text{--}4000\text{ cm}^{-1}$ . The concentration of  $\text{Ca}^{2+}$  in the filtrate was determined *via* inductively coupled plasma-atomic emission spectrometry (ICP-AES, PS-6, Baird, USA). The average diameters and average aspect ratios of the  $\alpha$ -HH products for each

sample were determined from about 100 crystal products using the optical images and the Image-Pro plus 6.0 software.

### 3. Results and discussion

#### 3.1 Influence of reaction temperature on the phase transition kinetics

In order to explore the influence of reaction temperature on the kinetics of phase transformation from FGD gypsum to  $\alpha$ -HH

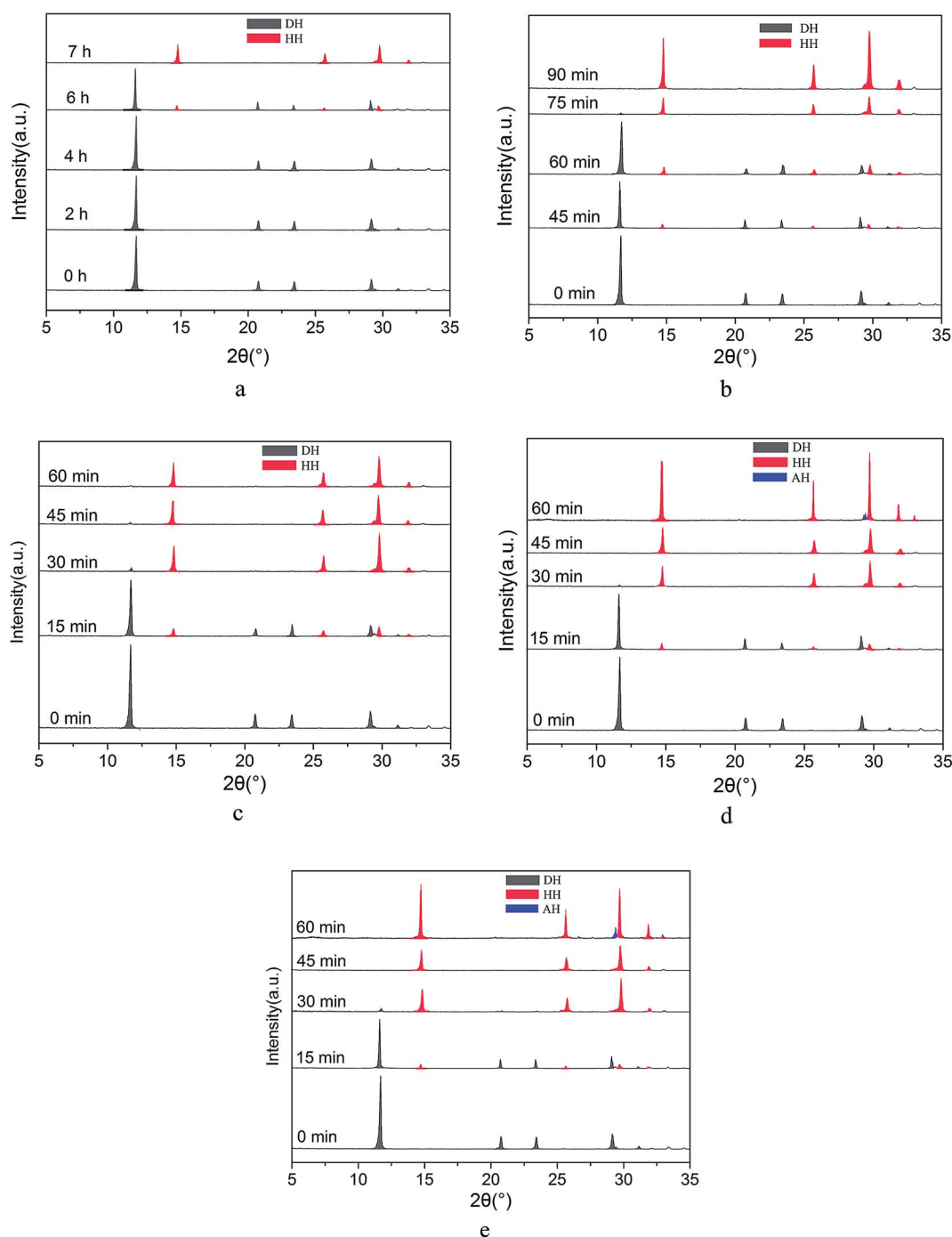


Fig. 2 XRD patterns of the crystal products at different interval times during the phase transformation in the presence of different NaCl concentrations in glycerol (65 wt%)-water solution at  $90\text{ }^{\circ}\text{C}$  ((a) 0%; (b) 1%; (c) 3%; (d) 5% and (e) 7%).



and determine the appropriate reaction temperature, we investigated the complete transformation time at different reaction temperatures using XRD, as shown in Fig. 1. The diffraction peaks of  $\alpha$ -HH appear at  $2\theta = 14.72^\circ, 25.64^\circ, 29.70^\circ, 31.86^\circ$  and FGD gypsum (DH) at  $2\theta = 11.61^\circ, 20.69^\circ, 23.35^\circ$  and  $29.08^\circ$ .

From Fig. 1a, it can be seen that at  $80^\circ\text{C}$  the diffraction peaks of  $\alpha$ -HH appear at 18 hours, which suggests that  $\alpha$ -HH crystals were formed. After that, the intensity of the DH peaks generally weakened and the  $\alpha$ -HH peaks gradually strengthened due to the gradual phase transformation from FGD gypsum to  $\alpha$ -HH. At 36 hours, the FGD gypsum was completely transformed into  $\alpha$ -HH. When the reaction temperature was increased to  $85^\circ\text{C}$ , the complete transformation time reduced sharply to 20 hours (Fig. 1b), and with an increase in the temperature to  $90^\circ\text{C}$ , the FGD gypsum was completely converted into  $\alpha$ -HH within 7 hours (Fig. 1c). Upon further increasing the temperature to  $95^\circ\text{C}$ , the complete transformation time did not significantly reduce, as shown in Fig. 1d. Therefore, considering efficiency and saving energy, the appropriate reaction temperature should be  $90^\circ\text{C}$ .

### 3.2 Influence of NaCl on the rate of phase transformation from FGD gypsum to $\alpha$ -HH

In the preparation of  $\alpha$ -HH whiskers using FGD gypsum under facile conditions,  $\text{Na}^+$  was used to accelerate the phase transformation rate.<sup>8</sup> As shown in Fig. 2, the XRD patterns of the

$$\frac{S_{\text{HH}}}{S_{\text{HH}}^0} = \frac{c_{\text{Ca}^{2+}} \times \gamma_{\text{Ca}^{2+}} \times c_{\text{SO}_4^{2-}} \times \gamma_{\text{SO}_4^{2-}} \times a_{\text{H}_2\text{O}}^{0.5}}{K_{\text{sp,HH}}} \bigg/ \frac{c_{\text{Ca}^{2+}}^0 \times \gamma_{\text{Ca}^{2+}}^0 \times c_{\text{SO}_4^{2-}}^0 \times \gamma_{\text{SO}_4^{2-}}^0 \times a_{\text{H}_2\text{O}}^{0.5}}{K_{\text{sp,HH}}^0} \approx \frac{c_{\text{Ca}^{2+}} \times c_{\text{SO}_4^{2-}}}{c_{\text{Ca}^{2+}}^0 \times c_{\text{SO}_4^{2-}}^0} = \left( \frac{c_{\text{Ca}^{2+}}}{c_{\text{Ca}^{2+}}^0} \right)^2 \quad (2)$$

crystal products withdrawn at different interval times were used to track the phase transformation process.

Without NaCl (Fig. 2a), the transformation from FGD gypsum to  $\alpha$ -HH began at 360 min and was completed within 420 min. When 1% NaCl (by weight of FGD gypsum) (Fig. 2b) was added to the glycerol (65 wt%)-water solutions, the transformation started at 45 min and at 90 min the FGD gypsum was completely converted into  $\alpha$ -HH. When the NaCl concentration was increased to 3% (Fig. 2c), the gypsum began to dehydrate at 15 min and the phase transformation was completed within 1 h. Upon further increasing the NaCl concentration to 5% (Fig. 2d) and 7% (Fig. 2e), the time of complete transformation from FGD gypsum to  $\alpha$ -HH decreased to 45 min. As the phase transition reaction proceeded,  $\alpha$ -HH generated by the FGD gypsum continued to dehydrate and was gradually transformed into anhydrous calcium sulfate (AH).

The promoting effect of NaCl on the transformation rate is attributed to the supersaturation ( $S_{\text{HH}}$ ) of  $\alpha$ -HH in the solution. A higher supersaturation provided a greater driving force for  $\alpha$ -HH nucleus formation, resulting in a shorter phase transformation time from FGD gypsum to  $\alpha$ -HH.  $S_{\text{HH}}$  is defined as:

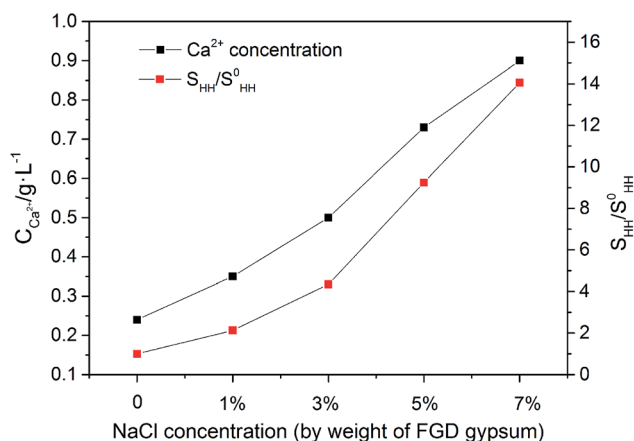


Fig. 3 Influence of NaCl on  $\text{Ca}^{2+}$  concentration and  $S_{\text{HH}}/S_{\text{HH}}^0$  in glycerol (65 wt%)-water solution at  $90^\circ\text{C}$ .

$$S_{\text{HH}} = \frac{a_{\text{Ca}^{2+}} \times a_{\text{SO}_4^{2-}} \times a_{\text{H}_2\text{O}}^{0.5}}{K_{\text{sp,HH}}} = \frac{c_{\text{Ca}^{2+}} \times \gamma_{\text{Ca}^{2+}} \times c_{\text{SO}_4^{2-}} \times \gamma_{\text{SO}_4^{2-}} \times a_{\text{H}_2\text{O}}^{0.5}}{K_{\text{sp,HH}}} \quad (1)$$

where,  $a$ ,  $c$ ,  $\gamma$  and  $K_{\text{sp,HH}}$  are the activity, ion concentration, activity coefficient and thermodynamic equilibrium constant, respectively. In this investigation, the ratio of the supersaturation with  $\text{Na}^+$  ions to that without  $\text{Na}^+$  ions is used to illustrate the influence of  $\text{Na}^+$  ions on the supersaturation of  $\alpha$ -HH:

where, 0 represents the experimental data without  $\text{Na}^+$  ions. The concentrations of  $\text{Ca}^{2+}$  and  $\text{SO}_4^{2-}$  derived from the dissolution of FGD gypsum were equal, and because the temperature was fixed at  $90^\circ\text{C}$  and the concentration of NaCl was much lower than that of the glycerol/water activity, the activity coefficient and  $K_{\text{sp,HH}}$  could be considered as constant. Therefore,  $S_{\text{HH}}/S_{\text{HH}}^0$  was a function of  $\text{Ca}^{2+}$  ion concentration.

As depicted in Fig. 3, as the NaCl concentration increased, the  $\text{Ca}^{2+}$  concentration and  $S_{\text{HH}}/S_{\text{HH}}^0$  experienced an upward trend, and when the NaCl concentration increased from 0 to 7%, the concentration of  $\text{Ca}^{2+}$  increased from 0.24 to 0.90  $\text{mg L}^{-1}$  and  $S_{\text{HH}}/S_{\text{HH}}^0$  from 1.00 to 14.06. It is clear that the addition of NaCl facilitated the dissolution of FGD gypsum and provided more available lattice ions, which created a much higher supersaturation and thus was a greater driving force for the phase transformation.

### 3.3 Influence of $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$ on the morphology of the crystal products

Fig. 4 and 5 show the morphological images and crystal size distribution of crystal products prepared with different concentrations of  $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$ . Without the crystal



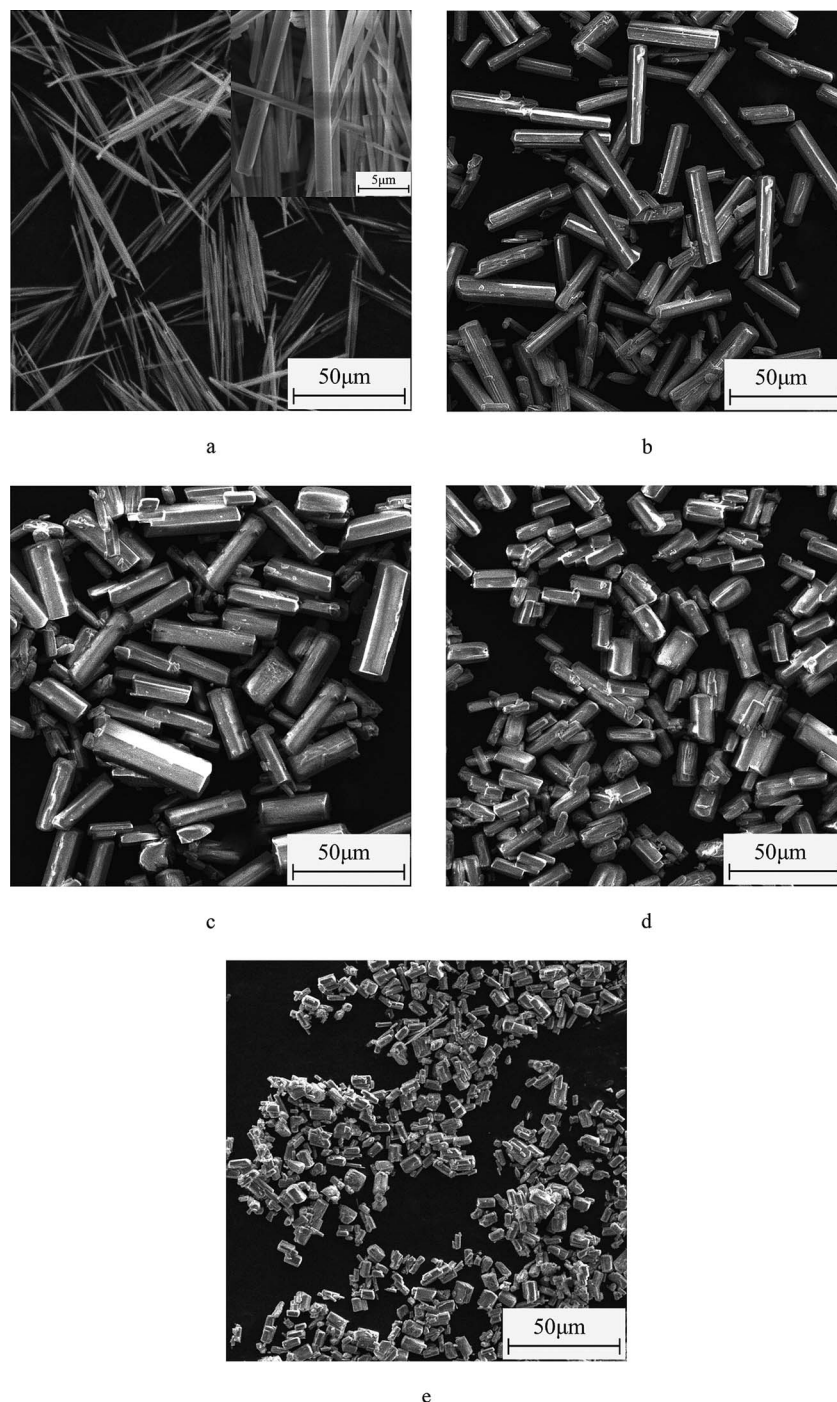


Fig. 4 Influence of  $C_4H_4O_4Na_2 \cdot 6H_2O$  on the morphology of the  $\alpha$ -HH products prepared in glycerol (65 wt%)-water solution with 5% NaCl (by weight of FGD gypsum) at 90 °C ((a) 0%; (b) 0.03%; (c) 0.06%; (d) 0.09% and (e) 0.12%).

modifier, the  $\alpha$ -HH products tended to be acicular in shape owing to their preferential 1-D growth along the  $c$  axis.<sup>13–15</sup> As shown in Fig. 4a, acicular crystals with an average aspect ratio of 28.60 were formed in the absence of the crystal modifier. When 0.03%  $C_4H_4O_4Na_2 \cdot 6H_2O$  (by weight of FGD gypsum) was added to the crystallization reaction system, the average length of the  $\alpha$ -HH crystals decreased sharply from 53.79 to 32.23  $\mu\text{m}$  and the average diameter increased from 1.89 to 7.84  $\mu\text{m}$ , which

resulted in a significant decline in the average aspect ratio to 4.15. With an increase in  $C_4H_4O_4Na_2 \cdot 6H_2O$  concentration from 0.03% to 0.06%, the average length of the crystals remained nearly unchanged, but their average diameter underwent a remarkable increase from 7.84 to 11.85  $\mu\text{m}$ , leading to a decrease in the average aspect ratio from 4.15 to 2.72. From Fig. 4b and c, it can be seen that the  $\alpha$ -HH products were transformed gradually from rod-like crystals into fat hexagonal



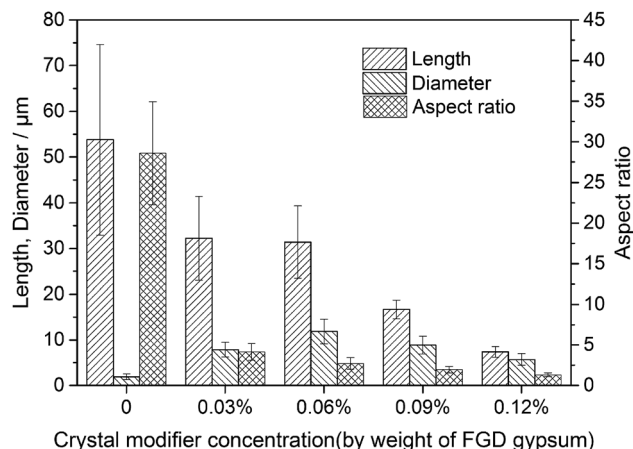


Fig. 5 Average lengths, diameters and aspect ratios of the  $\alpha$ -HH products prepared with different  $C_4H_4O_4Na_2 \cdot 6H_2O$  concentrations in glycerol (65 wt%)-water solution with 5% NaCl (by weight of FGD gypsum) at 90 °C.

prismatic crystals. With a further increase in the crystal modifier concentration to 0.09% (Fig. 4d), the crystal products appeared as shorter columns with an average diameter of 8.84  $\mu\text{m}$  and aspect ratio of 1.96. As the concentration of  $C_4H_4O_4Na_2 \cdot 6H_2O$  increased to 0.12% (Fig. 4e), fat and short hexagonal prisms with a 7.36  $\mu\text{m}$  average length, 5.70  $\mu\text{m}$  average diameter and 1.32 average aspect ratio were acquired. From Fig. 4, 5 and the above discussion, it can be concluded that  $C_4H_4O_4Na_2 \cdot 6H_2O$  effectively tuned the size and morphology of the  $\alpha$ -HH crystals.

To confirm the interactions between the crystal modifier and the crystal surfaces of the  $\alpha$ -HH crystals, FT-IR spectra were explored, as shown in Fig. 6. As shown in spectrum a, the peaks at 3612, 3564 and 1620  $\text{cm}^{-1}$  are assigned to the O-H vibration of the crystal water molecules in the  $\alpha$ -HH crystals. The three peaks at 1156, 1115, and 1097  $\text{cm}^{-1}$  are assigned to the

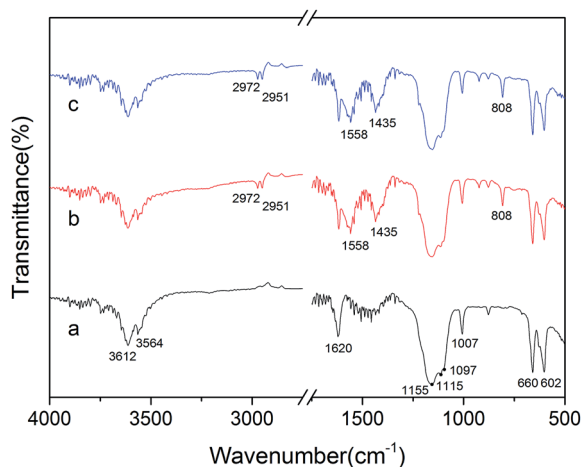


Fig. 6 FT-IR spectra of the  $\alpha$ -HH crystals prepared with different  $C_4H_4Na_2 \cdot 6H_2O$  concentrations in glycerol (65 wt%)-water solution with 5% NaCl (by weight of FGD gypsum) at 90 °C ((a) 0%; (b) 0.06% and (c) 0.12%).

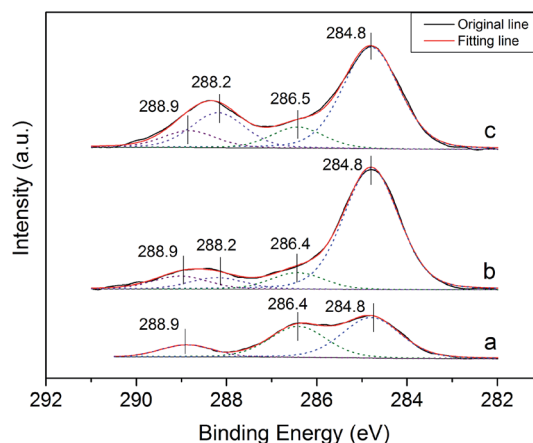


Fig. 7 C 1s XPS spectra of  $\alpha$ -HH crystals prepared with different concentrations of  $C_4H_4Na_2 \cdot 6H_2O$  in glycerol (65 wt%)-water solution with 5% NaCl (by weight of FGD gypsum) ((a) 0%; (b) 0.06% and (c) 0.12%).

asymmetric stretching vibration of  $\nu_3 \text{SO}_4^{2-}$ , and the peak at 1007  $\text{cm}^{-1}$  is assigned to the distorted symmetric stretching vibration of  $\nu_1 \text{SO}_4^{2-}$ . Also, the peaks at 660 and 602  $\text{cm}^{-1}$  are indexed to the  $\nu_4 \text{SO}_4^{2-}$  stretching.<sup>16,17</sup>

As depicted in spectra b and c, the peaks at 2972 and 2951  $\text{cm}^{-1}$  are attributed to the asymmetric and symmetric stretching vibrations of methylene ( $-\text{CH}_2-$ ), and the peaks at 1558 and 1435  $\text{cm}^{-1}$  are derived from the asymmetric and symmetric stretching vibrations of the ester group ( $-\text{COO}^-$ ), which all demonstrate the adsorption of  $C_4H_4O_4Na_2 \cdot 6H_2O$  on the  $\alpha$ -HH crystal surfaces.<sup>18</sup> Additionally, the peak at 808  $\text{cm}^{-1}$  might be due to the distorted vibration of methylene ( $-\text{CH}_2-$ ).

Fig. 7 depicts the C 1s XPS spectra of the crystal products formed in the presence of different  $C_4H_4O_4Na_2 \cdot 6H_2O$  concentrations. As shown in the C 1s spectra (Fig. 7), the most intense C 1s peak observed in all the samples is at 284.8 eV, which is associated with carbon impurity<sup>19</sup> or the C-(C, H) species in the crystal modifier.<sup>20,21</sup> Without the crystal modifier (Fig. 7a), the C 1s spectra of the  $\alpha$ -HH crystals prepared could be fitted with three components. Besides the major component at 284.8 eV, the component located at 286.5 eV is associated with the C-O in glycerol,<sup>19,20,22,23</sup> which implies the adsorption of a trace amount of glycerol on the crystal surfaces.<sup>24-26</sup> The high binding energy component of C 1s at 288.9 eV is derived from the carbonate species ( $\text{CO}_3^{2-}$ ) of the limestone existing in FGD gypsum.<sup>27,28</sup> As depicted in Fig. 7b and c, when a certain amount of crystal modifier was added to the crystallization reaction system, another C 1s component appeared at 288.2 eV, which is assigned to the carboxylic or carboxylate group ( $\text{COO}^-$ ),<sup>29-31</sup> and with an increase in the crystal modifier concentration, the intensity of the peak at 288.2 eV improved gradually, implying the adsorption of  $C_4H_4Na_2 \cdot 6H_2O$  on the surfaces of the crystal products.

Fig. 8 shows the Ca 2p XPS spectra of the  $\alpha$ -HH crystals prepared in the presence of different  $C_4H_4O_4Na_2 \cdot 6H_2O$  concentrations. As shown in Fig. 8a, in the absence of the crystal modifier, the Ca 2p spectra of  $\alpha$ -HH could be fitted with two



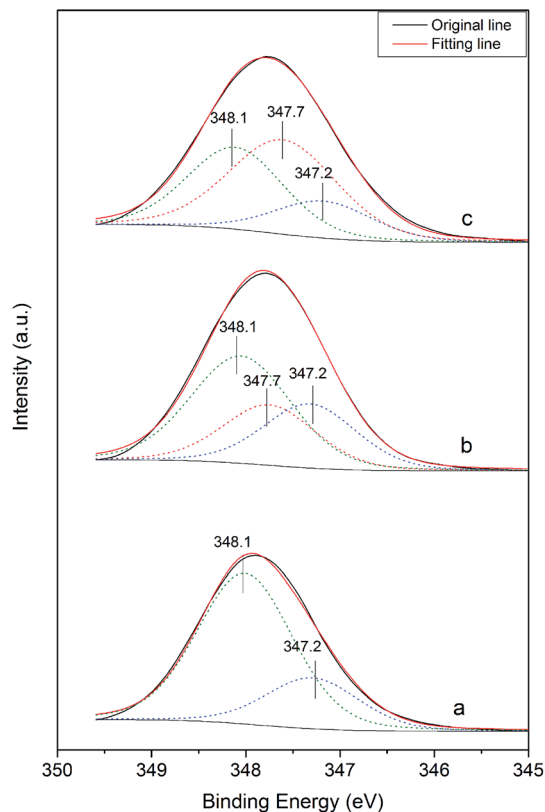


Fig. 8 Ca 2p XPS spectra of the  $\alpha$ -HH crystals prepared with different concentrations of  $C_4H_4O_4Na_2 \cdot 6H_2O$  in glycerol (65 wt%)-water solution with 5% NaCl (by weight of FGD gypsum) (a) 0%; (b) 0.06% and (c) 0.12%.

Table 2 Surface atomic concentration of the  $\alpha$ -HH crystals prepared with different  $C_4H_4O_4Na_2 \cdot 6H_2O$  concentrations in glycerol (65 wt%)-water solution with 5% NaCl (by weight of FGD gypsum) at 90 °C

$C_4H_4O_4Na_2 \cdot 6H_2O$ concentration (by weight of FGD)	Ca/%	S/%	O/%	C/%
0	15.30	16.80	64.92	2.98
0.06%	14.31	15.48	65.91	4.30
0.12%	11.56	12.72	66.32	9.40

components. The component at 347.2 eV is attributed to the calcium of limestone existing in FGD gypsum, and the other is derived from the calcium of  $\alpha$ -HH. When the crystal modifier was added to the reaction system, a third peak appeared at 347.7 eV, which is associated with the calcium chelated by the carboxyl group of the crystal modifier, as shown in Fig. 8b and c.<sup>32</sup> With an increase in the modifier concentration, the strength of the peak at 347.7 eV enhanced correspondingly. These results demonstrate the chelating reaction between the calcium on the crystal surface of  $\alpha$ -HH and the carboxyl group of the crystal modifier.

Table 2 shows the surface atomic distribution of the  $\alpha$ -HH crystals formed in the presence of different concentrations of the crystal modifier. The surface carbon concentration of the  $\alpha$ -

HH products prepared without the crystal modifier might be mainly derived from carbon impurities or glycerol adsorbed on the crystal surfaces. From Table 2, it can be seen that with an increase in  $C_4H_4O_4Na_2 \cdot 6H_2O$  concentration, the surface oxygen and carbon concentrations of the  $\alpha$ -HH products were generally enhanced, which implies the adsorption of  $C_4H_4O_4Na_2 \cdot 6H_2O$  on the  $\alpha$ -HH crystal surfaces. However, the adsorption of the crystal modifier on the  $\alpha$ -HH surfaces was much less than the amount added, and a certain amount of carboxylate ions (from the crystal modifier) could reduce water-gypsum ratio and improve the product strength to some extent. Therefore, there was no need to remove the crystal modifier from the produced  $\alpha$ -HH crystals.

As shown in Fig. 9, the  $\alpha$ -HH lattices are composed of repeating, ionically bonded Ca and  $SO_4$  atoms in chains of  $-Ca-SO_4-Ca-SO_4-$ , and  $SO_4$  is a tetrahedral structure in which each S atom is covalently bonded to four O atoms.<sup>14,15</sup> The structure of the chains may account for the fact that  $\alpha$ -HH tended to grow in a 1D shape. These chains are hexagonally and symmetrically arranged and form a framework parallel to the  $c$  axis, and along the  $c$  axis continuous channels exist with a diameter of about 4.5 Å, where one water molecule is attached to every two calcium sulfate molecules.<sup>33</sup> This crystal structure causes the distribution of  $Ca^{2+}$  to be denser on the 111 top facets and the distribution of  $SO_4^{2-}$  denser on the 110 and 100 side facets, which makes the 111 facets positively charged and the 110 and 100 facets negatively charged.<sup>14,33</sup> Therefore, when  $C_4H_4O_4Na_2 \cdot 6H_2O$  was added to the reaction system,  $C_4H_4O_4^{2-}$  preferentially absorbed on the top facets by chelating  $Ca^{2+}$  and inhibited the  $\alpha$ -HH crystal growth along the  $c$  axis, as shown in Fig. 10.<sup>34</sup>

Although succinic acid disodium salt hexahydrate ( $C_4H_4O_4Na_2 \cdot 6H_2O$ ) as the crystal modifier could effectively tune the morphology of the  $\alpha$ -HH products, it suppressed the nucleation and crystal growth of  $\alpha$ -HH and prolonged the time for the complete transformation from FGD gypsum to  $\alpha$ -HH. As shown in Fig. 11, with an increase in the crystal modifier concentration from 0 to 0.12%, the complete transformation time was extended from 25 min to 17 h. The formation of  $\alpha$ -HH can be divided into three processes: dissolution of DH,  $\alpha$ -HH

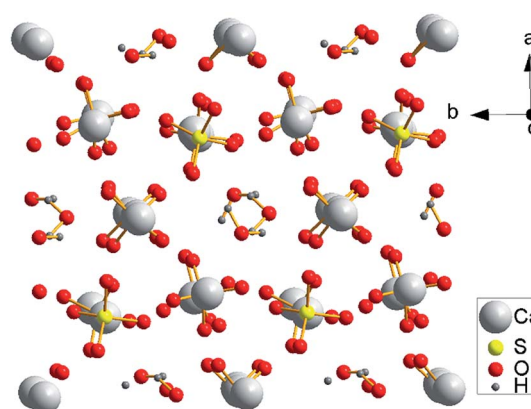


Fig. 9 Crystal structure of the  $\alpha$ - $CaSO_4 \cdot 0.5H_2O$  lattice along the  $c$  axis.



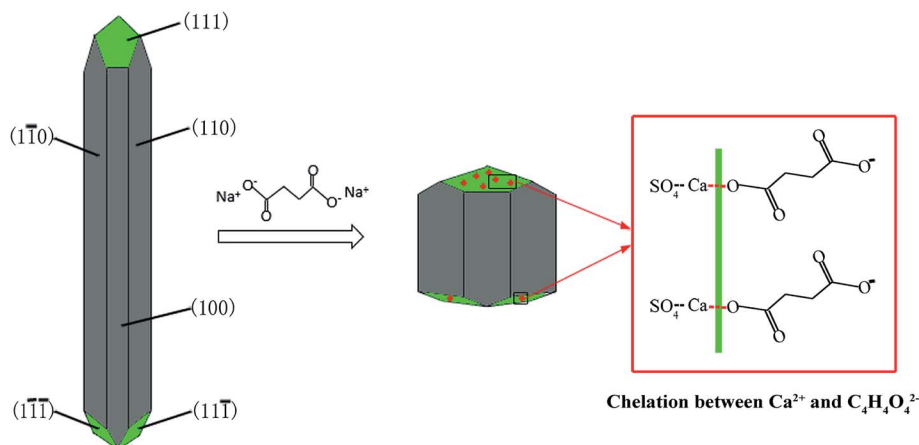


Fig. 10 Schematic illustration of the adsorption of  $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$  on the  $\alpha$ -HH crystal surfaces.

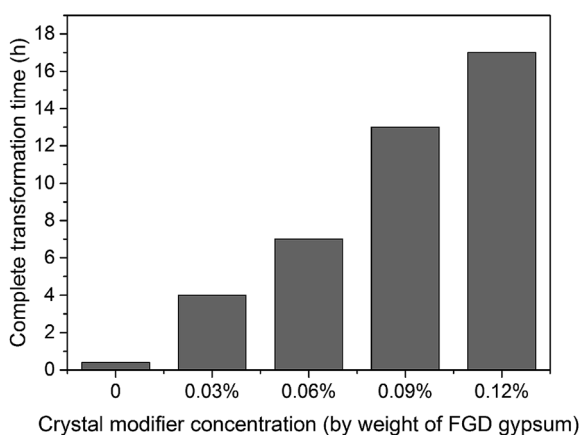


Fig. 11 Time for the complete transformation from FGD gypsum to  $\alpha$ -HH products with different  $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$  concentrations and 5% NaCl (by weight of FGD gypsum) in glycerol (65 wt%)-water solution at  $90^\circ\text{C}$ .

nucleation and  $\alpha$ -HH growth, of which nucleation is the rate-determining step.<sup>35,36</sup> When the crystal modifier was added to the reaction system,  $\text{C}_4\text{H}_4\text{O}_4^{2-}$  chelated free  $\text{Ca}^{2+}$  in the solution and lower the supersaturation for  $\alpha$ -HH, which restrained the nucleation of  $\alpha$ -HH, and thus prolonged the transformation time.<sup>12</sup>

The substitution of sodium ions in the modifier with calcium ions might have a considerable impact on the formation and properties of the  $\alpha$ -HH products. Succinate calcium does not fully dissociate, and the succinate ions dissociated from succinate calcium in the solution would much less than that from succinate sodium, which would reduce the transformation time, but increase the aspect ratio of the  $\alpha$ -HH products, in comparison with succinate sodium. However, the substitution of sodium ions in the modifier with other ions, such as potassium and magnesium, would not have a significant impact on the preparation of  $\alpha$ -HH crystals because all of them are fully dissociated.

## 4. Conclusions

A new method was created for reusing FGD gypsum by preparing  $\alpha$ -HH with short hexagonal prisms in glycerol-water solution with a small amount of succinic acid disodium salt hexahydrate ( $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$ ) and NaCl. Considering efficiency and saving energy, the appropriate reaction temperature was  $90^\circ\text{C}$ . NaCl played an important role in accelerating the transformation from DH to  $\alpha$ -HH. With an increase in NaCl concentration from 0 to 5%, the concentration of  $\text{Ca}^{2+}$  increased from 0.24 to  $0.73 \text{ g L}^{-1}$  and the corresponding  $S_{\text{HH}}/S_{\text{HH}}^0$  increased from 1.00 to 9.25, which led to a sharp decrease in the complete transformation time from 7 h to 45 min.  $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$  acted as a crystal modifier to regulate the crystal morphology, and as the concentration of  $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$  increased from 0 to 0.12%, the crystal morphology was tuned from acicular to fat and short prismatic and the corresponding average aspect ratio decreased remarkably from 28.60 to 1.32. The suppression of the  $\alpha$ -HH crystal growth along the  $c$  axis by  $\text{C}_4\text{H}_4\text{O}_4\text{Na}_2 \cdot 6\text{H}_2\text{O}$  is due to the preferential adsorption of  $\text{C}_4\text{H}_4\text{O}_4^{2-}$  on the top facets of the crystal by chelating  $\text{Ca}^{2+}$ . However,  $\text{C}_4\text{H}_4\text{O}_4^{2-}$  chelates free  $\text{Ca}^{2+}$  in the solution and lowers the supersaturation of  $\alpha$ -HH, thus restraining the nucleation of  $\alpha$ -HH, which prolongs the transformation time.

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