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Heavy metal ions removal from aqueous solution by xanthate-modified cross-linked magnetic chitosan/poly(vinyl alcohol) particles†

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Xanthate-modified cross-linked magnetic chitosan/poly(vinyl alcohol) particles (XCMCP) were synthesized and applied to remove Pb(II) and Cu(II) ions from aqueous solutions. To further explore the adsorption mechanisms, the complexes were characterized by Fourier transform infrared spectroscopy (FTIR), Scanning Electron Microscope (SEM), Vibrating Sample Magnetometer (VSM), X-ray Diffraction (XRD), and X-ray Photoelectron Spectroscopy (XPS). The effects of pH, contact time, and temperature on the adsorption process were investigated. The results showed that the particles were super-paramagnetic with a saturation magnetization of 34.8 emu g⁻¹, had an irregular surface, and successfully introduced xanthate groups. The adsorption capacity of XCMCP for Pb(II) or Cu(II) was better in near-neutral pH. The kinetic data were well-described by the pseudo-second-order kinetic model. The Langmuir and Freundlich isotherms fit the equilibrium data well. Based on the Langmuir isotherm model, the maximum adsorption capacities of XCMCP at 328 K were 59.855 and 139.797 mg g⁻¹ for Pb(II) and Cu(II), respectively. Meanwhile, the effect of temperature on the reaction process was not significant. XCMCP exhibited a good property for repeated use and could still retain an effective adsorption efficiency after seven cycles. The mechanism for Pb(II) and Cu(II) adsorption onto XCMCP involves the interactions of N and S atoms with heavy metals, crystal formation and surface adsorption. Thereinto, contributions of crystal formation were dominant. These properties of XCMCP make it promising for practical use, which suggests that XCMCP is a promising adsorbent for hazardous-metal-ion-contaminated water treatment.

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Introduction

Water pollution by heavy metals is a serious environmental problem because of their toxic and non-biodegradable nature.¹ The main potential sources of heavy metals in wastewater are fertilizers, fungicides, metals that are used in manufacturing, paints, pigments, and batteries.² Heavy metal ions may cause severe health problems in animals and humans, because they can bind to proteins, nucleic acids, and small metabolites in living organisms, which inhibits their functions.³ Lead and copper ions are often chosen as target metals because of their widespread use in the metal industry and their toxicity for humans and environmental health.⁴ Copper and lead pollution has occurred in many places. Ground/surface water in Osun,⁵ and surface water in cross-river states have shown a high copper concentration.⁶ Well boreholes and streams in Kogi, and ground water in Abia contain above the permissible Pb(II)

limit.^{7,8} Because they are harmful to human health, the United States Environmental Protection Agency (USEPA) has set Interim Drinking Water Health Advisory levels of 0.015 mg L⁻¹ for Pb²⁺ and 1.30 mg L⁻¹ for Cu²⁺, and the maximum dosages recommended by the World Health Organization (WHO) are 0.01 mg L⁻¹ for Pb²⁺ and 2.00 mg L⁻¹ for Cu²⁺.

Current techniques for the remediation of heavy-metal-contaminated water include chemical precipitation, ion exchange, filtration, reverse osmosis, and electrodeposition.⁹⁻¹³ Compared with these treatment methods, adsorption is more attractive because of its low cost, high removal efficiency, and easy operation. Common sorbents, which include activated carbon, atomized slag, and red mud, are limited because of their low efficiency, their sensitivity to pH and the presence of other organic materials.¹⁴⁻¹⁶ Chitosan (CS), which is the second-most-abundant biopolymer after cellulose,¹⁷ is often chosen as an effective bio-adsorbent for the removal or recovery of hazardous dyes, proteins, and heavy metals because of its non-toxicity, good biodegradability, excellent chemical resistance, and good mechanical properties.¹⁸ However, dissolved chitosan is difficult to separate from solution after adsorption of target contaminants and usually requires separation or modification.¹⁹ To solve this problem, poly(vinyl alcohol) (PVA) has been blended with chitosan to further enhance its mechanical and

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chemical properties *via* the formation of hydrogen bonds,^{20,21} which can create a three-dimensional network.²² Ngah *et al.* studied copper removal by chitosan/PVA beads, but the adsorption capacity of chitosan/PVA beads was lower than other sorbents.²¹ It is important to understand how to enhance the adsorption capacity of this adsorbent type. Sulfur compounds are efficient metal chelators because of their strong affinity for most heavy metals.²³ The xanthation of carbohydrate materials, particularly chitosan, has been reported for metal removal from aqueous solution, which occurs because the introduction of xanthate groups can enhance the metal-chelating capability of the adsorption.²⁴

Adsorbent recycling has become a key issue in practical applications, and magnetic materials are receiving increased attention. If magnetic properties can be imparted to the sorbents, it may facilitate their removal from solution. Magnetic chitosan composites are novel materials that exhibit good sorption behavior for various toxic pollutants.²⁵ However, it is necessary to establish how to improve the adsorption ability of this kind of adsorbent.

The overall goal of this research was to develop a material with a high adsorption capacity and good magnetic properties to remove Pb²⁺ and Cu²⁺ from aqueous solution. The aims of this study were to: (1) characterize the physical and chemical properties and specific sorption sites of XCMCP, (2) investigate the adsorption capacities of XCMCP for Pb²⁺ and Cu²⁺, and (3) explain the XCMCP mechanisms.

Materials and methods

Materials

Chitosan powder (average molar mass of approximately one million, deacetylation degree of 95.23%, and viscosity of 150 mPa s) and Fe₃O₄ nanopowder (purity > 99.5%, 20 nm globular particles) were supplied by Aladdin Industrial Co. (Shanghai, China). PVA-1788 (purity > 97.0%) was from Shanghai Yingjia Industrial Development Co. (Shanghai, China). Copper sulfate pentahydrate (CuSO₄·5H₂O) and lead nitrate (Pb(NO₃)₂) were from Sinopharm Chemical Reagent Co., Ltd. (Beijing, China). All other chemicals were commercially available analytical-grade reagents. All solutions were prepared with deionized water.

Preparation of xanthate-modified cross-linked magnetic CS/PVA beads

Preparation of XCMCP included two sequential steps. First, cross-linked magnetic CS/PVA was synthesized using the momentary gelation method by dropping a composite gel-forming solution into an alkaline solution. Second, cross-linked magnetic CS/PVA was modified by introducing xanthate groups onto its backbone by treating it with carbon disulfide under alkaline conditions (the formation mechanisms was shown in ESI Fig. S1†).

Chitosan powder (6 g) was dissolved in 150 mL of 2% (v/v) aqueous acetic acid to form a solution of chitosan. PVA solution was prepared by dissolving 6 g of PVA powder in 150 mL of

deionized water. After the chitosan and PVA powder had dissolved, the two solutions were mixed together, and 6 g Fe₃O₄ was added into the mixture. The composite gel-forming solution was stirred continuously for 3 h at 303 ± 1 K. The gel-forming solution was dropped into 1.0 M sodium hydroxide, which resulted in the formation of spherical hydrogel beads. The beads were gelled for 1 h and washed several times with deionized water. Finally, the wet beads were dipped into glutaraldehyde solution (0.046 mL, 0.12 mmol) and stirred for 12 h at 303 ± 1 K to obtain cross-linked magnetic CS/PVA. After washing thoroughly with deionized water, the cross-linked magnetic CS/PVA beads were filtered and dried at 343 K for 24 h.

The CS/PVA beads (2 g) were treated with 100 mL of 14% NaOH solution and 1 mL of carbon disulfide (the amount of CS₂ used was determined by preliminary experiments and the results were shown in ESI Fig. S2†). The mixture was stirred at room temperature for 24 h. The product was washed thoroughly with distilled water and dried at 343 K for 24 h.

Batch adsorption studies

Uptake experiments were carried out by placing 0.15 g of the dried XCMCP in a series of flasks that contained 50 mL metal ions solutions. Different metal ions concentrations were used compared with similar prior studies (49.50 ± 2.70, 98.12 ± 2.02, and 192.68 ± 2.84 mg L⁻¹ of Cu²⁺ and 48.17 ± 0.21, 107.20 ± 0.82, and 211.57 ± 1.41 mg L⁻¹ of Pb²⁺). The flasks were agitated on a shaker for 12 h at 308, 318, and 328 (±1) K. In alkaline solution, precipitated heavy metal ions may interfere with the adsorption analysis, thus the effect of pH on adsorption was investigated by adjusting the pH from 2.0 to 7.0 using HCl or NaOH solutions (0.1 M). Samples were taken at predetermined time intervals to analyze the residual metal ions concentrations in solutions. All experiments were conducted in duplicate.

The amount of adsorbed metal ions at equilibrium (q_e , mg g⁻¹) was calculated as:

$$q_e = \frac{(C_0 - C_e)V}{W} \quad (1)$$

where C_0 is the initial concentration of metal ions (mg L⁻¹), C_e is the equilibrium concentration of metal ions (mg L⁻¹), V is the solution volume (L), and W is the adsorbent dry mass (g).

Analytical methods

Metal ions concentrations were determined using atomic adsorption spectroscopy (SSX-550, Shimadzu, Japan) at 283.3 nm for Pb²⁺ and 324.7 nm for Cu²⁺. The slit width was 0.4 nm.

The surface morphologies of the XCMCP were visualized using SEM (SSX-550, Shimadzu, Japan). FTIR spectra were obtained with a Fourier transform infrared spectrometer (Nexus, Nicolet, USA), and a vibrating-sample magnetometer (7303, Lake shore, USA) was used to characterize the magnetic properties of XCMCP at room temperature. The crystal structure of XCMCP was obtained by XRD (D8 Focus, Bruker, Germany), and XPS (ESCALAB 250Xi, Thermo Fisher, USA) was used to characterize the elemental compositions of the XCMCP surfaces.



Results and discussion

Adsorption material characterization

FTIR analysis. FTIR spectra were collected to investigate the transmutation of functional groups in the composite during modification and adsorption. The FTIR spectrum of a pure chitosan flake is presented in Fig. 1(line a). The basic characteristic bands of chitosan were: $3500\text{--}3200\text{ cm}^{-1}$ (O–H and N–H stretching vibrations), 2919 cm^{-1} and 2872 cm^{-1} (asymmetric and symmetric C–H stretching vibration of $-\text{CH}_2$, respectively),²⁶ 1647 cm^{-1} (C=N and C=O stretching vibration),²⁷ 1399 cm^{-1} (O–H in-plane bending vibration), 1160 cm^{-1} (C–O–C stretching vibration),²⁸ 1090 cm^{-1} (C–O stretching vibration of secondary alcohol), 895 cm^{-1} (N–H rocking vibration of $-\text{NH}_2$), and 663 cm^{-1} (O–H out-of-plane bending vibration).

The FTIR spectrum of XCMCP is presented in Fig. 1(line b). Compared with the spectrum of pure chitosan, most basic characteristic peaks were weakened in the spectrum of XCMCP, which was attributed to the addition of PVA and Fe_3O_4 . After modification, the band at 1071 cm^{-1} could be assigned to C=S and S–C–S.²³ A new peak appeared at 562 cm^{-1} , which is related to Fe–O bond vibration, and demonstrates the existence of Fe_3O_4 .²⁹ The peak at 633 cm^{-1} disappeared because of the mixture of chitosan with PVA, which resulted in the formation of hydrogen bonds. After Pb^{2+} and Cu^{2+} adsorption (Fig. 1(line c); Fig. 1(line d)), the adsorption band at 1071 cm^{-1} shifted to 1091 cm^{-1} and 1110 cm^{-1} , respectively. Thus, it could be concluded that the xanthate group participated in the adsorption process. A peak that is attributed to the stretching vibration of the S–O of SO_4^{2-} appeared at 599 cm^{-1} , and new bands at $500\text{--}400\text{ cm}^{-1}$ revealed that SO_4^{2-} took part in the coordination rather than existed as free ions in the complexes.^{30,31} Based on FTIR analysis, Laus *et al.* and Zang *et al.* reported that the $-\text{NH}_2$ group of chitosan was involved in metal ions adsorption.^{2,17} However, a significant change in $-\text{NH}_2$ was not observed in this study, possibly because $-\text{NH}_2$ less effect on metal ions adsorption, or because the change was too weak to be observed.

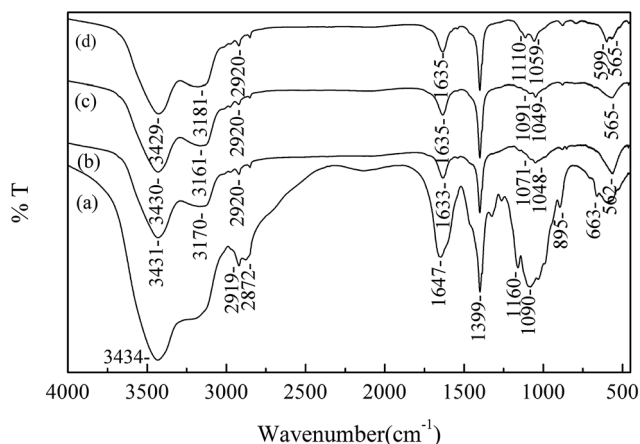


Fig. 1 FTIR spectra of chitosan flake (line a), XCMCP (line b), XCMCP loaded with Pb^{2+} (line c) and XCMCP loaded with Cu^{2+} (line d).

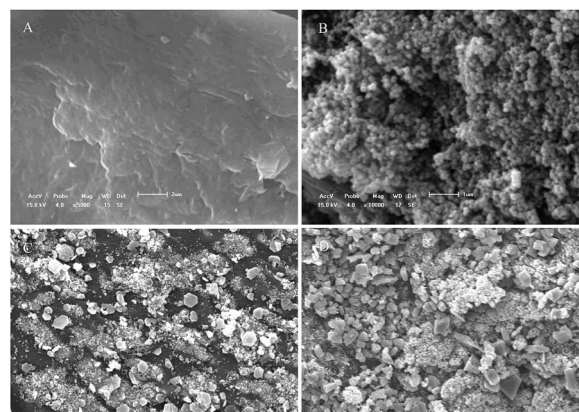


Fig. 2 SEM images of chitosan flake (A), XCMCP (B), XCMCP loaded with Pb^{2+} (C) and XCMCP loaded with Cu^{2+} (D).

SEM analysis. The XCMCP surface exhibited a microporous and irregular structure, as shown in the SEM images (Fig. 2). Cubic-shaped particles that were attributed to Fe_3O_4 were observed on the material surfaces. The XCMCP surface (Fig. 2B) was more rugged than that of chitosan (Fig. 2A), poly(vinyl alcohol) (results not shown), and Fe_3O_4 (results not shown). The irregular surface enhanced the adsorption capability of XCMCP. After Pb^{2+} adsorption (Fig. 2C), the surface morphology changed significantly, some initial pores were filled in, and hexagonal particles appeared on the surface. Similarly, crystalline particles were observed on the surface after Cu^{2+} adsorption (Fig. 2D), although these crystals were irregular compared with those that were observed after Pb^{2+} adsorption. These particles likely formed as a result of the transformation of Pb^{2+} and Cu^{2+} . XRD analyses were used to investigate these particles further.

XRD analysis. XRD is an effective method for determining the crystal structure of XCMCP and can provide useful information on the physical and chemical forms of magnetic particles that are embedded in chitosan/PVA. Fig. 3 shows the XRD patterns of pure Fe_3O_4 (line a), XCMCP before (line b) and after Pb^{2+} sorption (line c), and XCMCP after Cu^{2+} sorption (line d).

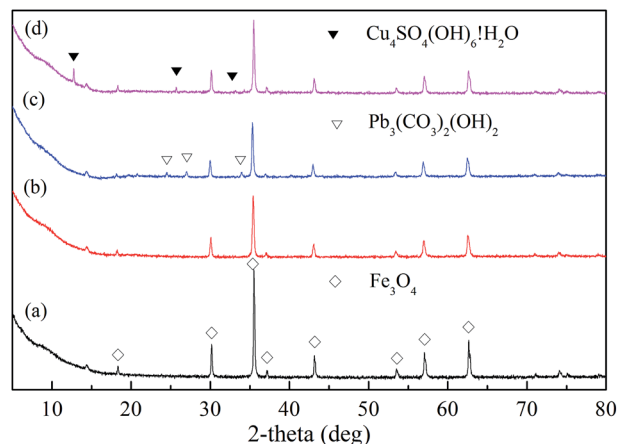


Fig. 3 XRD spectra of Fe_3O_4 (line a), XCMCP (line b), XCMCP loaded with Pb^{2+} (line c) and XCMCP loaded with Cu^{2+} (line d).



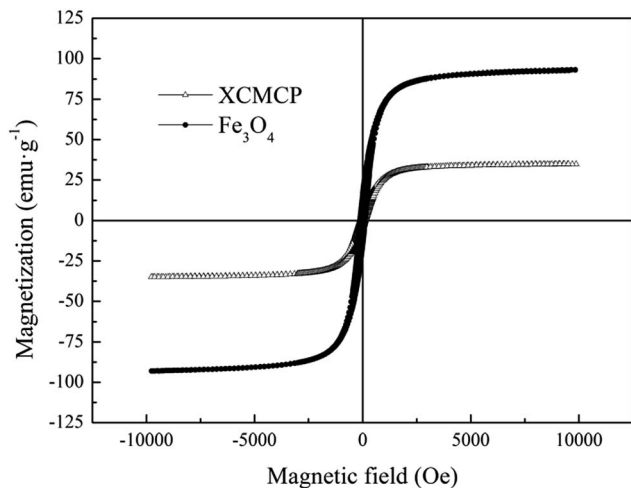


Fig. 4 Magnetization curves of XCMCP and pure Fe_3O_4 .

The patterns confirm the existence of ferroferric oxide with magnetic properties that can be used for magnetic separation.²⁶ Compared with the peak data in the JCPDS (Joint Committee on Powder Diffraction Standards) file (PDF no. 65-3107), eight characteristic peaks for Fe_3O_4 as marked by their indices [(1 1 1), (2 2 0), (3 1 1), (4 0 0), (4 2 2), (5 1 1), (4 4 0), and (5 3 3)] were observed in the spectra of all samples, which indicates that the crystal structure of Fe_3O_4 was not destroyed after metal ions adsorption. Fe_3O_4 was not involved in the adsorption process. It was demonstrated the main function of Fe_3O_4 was to provide the magnetic properties, which could facilitate materials removal from aqueous solutions. Some new peaks (24.51° , 27.00° , 33.91° , 12.78° , 25.67° , and 33.17°) appeared in the XRD patterns after Pb^{2+} and Cu^{2+} adsorption, which demonstrates that new crystals were generated. A comparison with the peak data in the JCPDS file (PDF no. 13-131 and PDF no. 20-364) suggests that these new crystals were $\text{Pb}_3(\text{CO}_3)_2(\text{OH})_2$ and $\text{Cu}_4\text{-SO}_4(\text{OH})_6 \cdot \text{H}_2\text{O}$. The results clarify the particles observed that were in the SEM images (Fig. 2C and D).

VSM analysis. VSM was used to measure the magnetic properties of XCMCP. Hysteresis loops of pure Fe_3O_4 and XCMCP were observed between ± 10 kOe at 299 K (Fig. 4). The saturation magnetization (M_s) of XCMCP was ~ 34.8 emu g^{-1} , which corresponds to 37.5% pure Fe_3O_4 nanoparticles with $M_s = 92.7$ emu g^{-1} . Obviously, the saturation magnetization of XCMCP was lower than that of pure Fe_3O_4 because of the introduction of chitosan and PVA. The saturation magnetization of XCMCP was close to the previously reported values for magnetic chitosan bioadsorbents.^{18,22,32} There was no remanence and a near-zero coercivity, which indicates that XCMCP was a superparamagnetic material.²² The saturation magnetization of XCMCP was sufficient for its rapid response to an external magnetic field. XCMCP was attracted rapidly to the side of the glass bottle from aqueous solution, and the solution became almost colorless. Although the saturation magnetization of XCMCP was lower than that of Fe_3O_4 , XCMCP could be recovered easily from the liquid phase after adsorption, which would facilitate its practical use.

Effect of pH on metal ions adsorption

Solution pH is one of the most important parameters that affects the adsorption process,³³ because it affects metal ions speciation, adsorbent surface charge, and the degree of sorbent ionization.³⁴ The effect of pH on Pb^{2+} and Cu^{2+} adsorption are shown in Fig. 5. Based on calculations that were performed using Visual MINTEQ, Pb exists as Pb^{2+} , PbNO_3^+ , $\text{Pb}(\text{NO}_3)_2(\text{aq})$, $\text{Pb}_2\text{OH}^{3+}$, and $\text{Pb}_4(\text{OH})_4^{4+}$ in aqueous solutions at pH 2.0–7.0. The adsorption capacity increased with an increasing pH. In the pH range 2.0–7.0, the maximum adsorption capacity of Pb^{2+} was 36.93 mg L^{-1} at pH 6.88. At a lower pH, the adsorption capacity was lower because the Pb species were mainly Pb^{2+} and PbNO_3^+ , which competed with the excessive amounts of H^+ or H_3O^+ . Meanwhile, the protonation of $-\text{NH}_2$ to form $-\text{NH}_3^+$ also affected the adsorption. The result is consistent with previous studies such as those by He *et al.*, Li *et al.*, and Li *et al.*, where they reported that heavy metal ions compete with H^+ in solutions with a low pH.^{1,35,36}

In aqueous solutions at pH 2.0–7.0, Cu may exist as $\text{CuSO}_4(\text{aq})$, CuHSO_4^+ , and $\text{Cu}_3(\text{OH})_4^{2+}$. As the pH increases, the adsorption capacity of Cu^{2+} increases gradually. The maximum adsorption capacity of Cu^{2+} was 22.59 mg L^{-1} at pH 6.03. When the pH was increased to 7.0, the adsorption capacity decreased to 15.96 mg g^{-1} , which agrees with the study of Laus *et al.*, who observed that Cu(II) adsorption as determined by the chitosan-epichlorohydrin-triphosphate decreased significantly when the pH increased from 6.0 to 7.0.² This phenomenon may result because of the hydrolytic properties of the copper ions.

No obvious leakage or change in XCMCP characteristics was observed during the reaction, which indicates that XCMCP was insoluble in acidic and alkaline media. XCMCP did not show any observable mass loss at low pH, which shows that XCMCP was more resistant to low-pH conditions compared with pure chitosan.³⁷ In practical applications, the pH of most heavy-metal-containing wastewater, such as electroplating wastewater, mine wastewater, battery production wastewater is acidic. If XCMCP exhibited a good durability in acidic wastewater, it would be a suitable adsorbent for wastewater treatment.

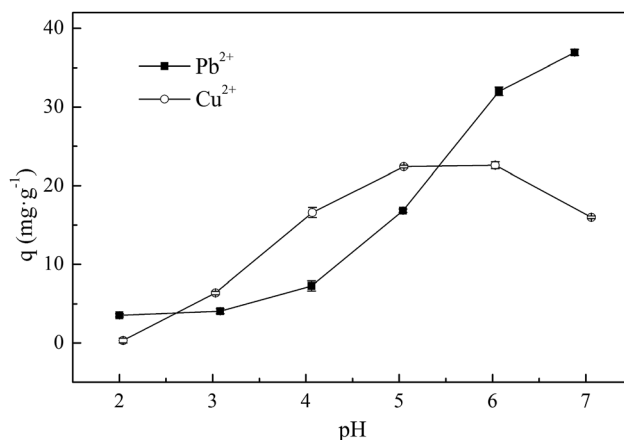


Fig. 5 Effect of pH on adsorption of Pb^{2+} and Cu^{2+} onto XCMCP. Experimental conditions: initial concentration was 100 mg L^{-1} , dosage of XCMCP was 0.1 g, and temperature was 303 K.



Table 1 Kinetic model constants and correlation coefficients for the adsorption of metal ions onto XCMCP

Metal ions	C_0 (mg L ⁻¹)	Pseudo-first-order		Pseudo-second-order		Intra-particle diffusion			
		K_1 (h ⁻¹)	R^2	K_2 (g mg ⁻¹ h ⁻¹)	R^2	$k_{p,1}$ (mg g ⁻¹ h ^{-1/2})	R^2	$k_{p,2}$ (mg g ⁻¹ h ^{-1/2})	R^2
Pb(II)	48.17	3.700	0.951	0.368	0.972	12.67	0.984	0.069	0.951
	107.20	0.688	0.990	0.024	0.985	17.39	0.995	0.604	0.994
	211.57	0.748	0.963	0.024	0.971	20.42	0.945	1.476	0.543
Cu(II)	49.50	0.903	0.977	0.081	0.988	7.970	0.987	0.714	0.747
	98.12	1.511	0.902	0.088	0.963	10.40	0.817	1.684	0.764
	192.68	0.883	0.833	0.039	0.912	9.769	0.907	1.685	0.850

Adsorption kinetics

To investigate the adsorption mechanisms and potential rate-controlling step, pseudo-first-order and pseudo-second-order kinetic models and intraparticle diffusion were used to interpret the experimental data. The pseudo-first-order and pseudo-second-order kinetic equation models are expressed as:³⁸

$$q_t = q_e - q_e e^{-k_1 t} \quad (2)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \left(\frac{1}{q_e}\right)t, \quad (3)$$

where k_1 is the pseudo-first-order rate constant of adsorption (h⁻¹); k_2 is the pseudo-second-order rate constant of adsorption (g mg⁻¹ h⁻¹); and q_e and q_t are the ion adsorption amounts at equilibrium and at any time, respectively (mg g⁻¹). k_1 and k_2 can be calculated from the slopes of the linear equations.

The intraparticle diffusion model was used to investigate the diffusion mechanisms:³⁹

$$q_t = k_{p,i} t^{1/2} + C_i \quad (4)$$

where $k_{p,i}$ ($i = 1-2$) is the intraparticle diffusion rate constant (mg g⁻¹ h^{-1/2}); that is, $k_{p,1}$ is the constant in the first stage (external surface adsorption), and $k_{p,2}$ is the constant in the second stage (inner bore adsorption). The rate constants of the kinetic models along with the corresponding regression coefficients (R^2) are listed in Table 1.

At a low initial concentration (~50 mg L⁻¹), the correlation coefficients of the pseudo-first-order and pseudo-second-order models were 0.951 and 0.972 for Pb(II) and 0.977 and 0.988 for Cu(II), respectively, which indicates that both models fit the experimental data well. However, higher correlation coefficients were obtained from the pseudo-second-order model, which suggests that chemical sorption may be a rate-determining step in Pb²⁺ and Cu²⁺ adsorption,⁴⁰ whereas the role of mass transfer in solution was more limited.⁴¹ Physical sorption was important in the adsorption process. As the initial concentration increased, the correlation coefficients for the pseudo-first-order and pseudo-second-order models decreased, especially for Cu²⁺, which demonstrates that the two kinetic models did not describe the adsorption process well at high initial concentrations. This is attributed to the increased complexity of adsorption (*i.e.*, adsorption could no longer be attributed only to simple chemical and

physical sorption) because of metal ions hydrolysis at high initial concentrations.

The parameters of intraparticle diffusion are presented in Table 1. The external surface adsorption stage of Pb²⁺ adsorption was completed within 2 h, whereas Cu²⁺ adsorption took longer. As the initial concentration increased, $k_{p,1}$ increased significantly because of an enhancement of the concentration gradient force.⁴² The linear portions of the second stage did not pass through the origin (results not shown), which indicates that intra-particle diffusion was not the rate-limiting step in the adsorption process.⁴³ $k_{p,1}$ was much greater than $k_{p,2}$, which suggests that external surface adsorption was the main rate-determining step.

Adsorption isotherms

Adsorption equilibrium isotherms can express the surface properties and affinities of adsorbents using certain constants.⁴⁴ The initial Pb²⁺ and Cu²⁺ concentrations were adjusted to 1–500 mg L⁻¹ for adsorption on XCMCP at 308, 318, and 328 K. Langmuir theory is based on the assumption that metal ions adsorption occurs on a homogenous surface by monolayer adsorption without any interaction among adsorbed ions.⁴⁵ The Freundlich isotherm describes adsorption on a heterogeneous surface and is not restricted to monolayer formation, and the amount of adsorbate adsorbed increases infinitely with increasing concentration.⁴⁶

The Langmuir and Freundlich models were applied to interpret the adsorption process. Their linear forms are given as:^{43,47}

$$\frac{C_e}{q_e} = \frac{1}{Q_0 b} + \frac{C_e}{Q_0} \quad (5)$$

$$\lg q_e = \lg K_f + \frac{1}{n} \lg C_e \quad (6)$$

where C_e is the equilibrium concentration of metal ions (mg L⁻¹); q_e is the amount of metal ions adsorbed by a unit of adsorbent at equilibrium (mg g⁻¹); Q_0 is the amount of adsorbate at complete coverage (mg g⁻¹), which gives the maximum adsorption capacity; b (L mg⁻¹) is the Langmuir constant that reflects the energy of adsorption; K_f is the Freundlich constant, which describes adsorption capability; and $1/n$ is the adsorption intensity.

The correlation coefficients (R^2) for the two models are listed in Table 2. The Langmuir and Freundlich isotherms were fitted



Table 2 Langmuir and Freundlich isotherm model constants and correlation coefficients for adsorption of metal ions onto XCMCP

Metal ions	T (K)	Langmuir isotherm				Freundlich isotherm		
		Q_0 (mg g ⁻¹)	b (L mg ⁻¹)	R^2	R_L	K_F (mg ^(1-1/n) L ^{1/n} g ⁻¹)	1/n	R^2
Pb(II)	308	57.979	9.450×10^{-3}	0.987	0.987–0.173	3.036	0.453	0.930
	318	58.126	7.500×10^{-3}	0.967	0.989–0.207	2.263	0.494	0.958
	328	59.855	6.400×10^{-3}	0.977	0.991–0.234	1.987	0.513	0.976
Cu(II)	308	123.725	1.770×10^{-3}	0.979	0.998–0.536	0.798	0.692	0.989
	318	136.042	1.820×10^{-3}	0.982	0.998–0.529	0.831	0.705	0.988
	328	139.797	1.920×10^{-3}	0.988	0.998–0.516	0.859	0.708	0.987

Table 3 Comparison of adsorption capacities of various magnetic adsorbents for Pb(II) and Cu(II)

Adsorbent name	Saturation magnetization (emu g ⁻¹)	Q_m (mg g ⁻¹)		Conditions	References
		Pb ²⁺	Cu ²⁺		
Magnetic chitosan nanoparticles	36.0	—	35.5	308.15 K, pH = 5.0	26
EDCMS	18.2	123.5	44.4	298.0 K, pH = 5.0	50
CS/ χ OREC-Fe ₃ O ₄	6.5	—	61.0	298.0 K, pH = 5.0	51
MCCM	10.5	45.8	88.2	303.0 K	52
The magnetically modified peanut husks	2.14	28.3	—	Laboratory temperature	53
Mesoporous CoFe ₂ O ₄ nanoparticles	46.71	32.1	—	293.0 K, pH = 5.0	54
XCMCP	34.8	59.9	139.8	318.00 K, pH = 6.0	This work

well to the equilibrium data, with R^2 exceeding 0.90 at different temperatures. These results indicate that the reaction process was a combination of homogeneous and heterogeneous adsorption, and the effect of adsorbate and adsorbent interactions on the adsorption process was finite. The maximum adsorption capacity that was obtained by the Langmuir isotherm changed only slightly with increasing temperature, which showed that the effect of temperature on the reaction process was insignificant. In the study of Lu *et al.*,⁴⁸ the adsorption capacity of Pb(II) imprinted chitosan for Pb(II) was controlled by temperature. Thus, the application of this adsorbent was limited by temperature in a practical application. The stable adsorption capacity of XCMCP for heavy metals at different temperatures made it a promising material for water treatment.

The essential characteristics of the Langmuir isotherm can be expressed by a dimensionless constant, the equilibrium parameter R_L , which is calculated from the following equation:⁴⁹

$$R_L = \frac{1}{(1 + bC_0)} \quad (7)$$

where b (L mg⁻¹) is the Langmuir constant and C_0 is the initial concentration of metal ions (mg L⁻¹). R_L indicates whether the adsorption is irreversible ($R_L = 0$), favorable ($0 < R_L < 1$), linear ($R_L = 1$), or unfavorable ($R_L > 1$). R_L was between 0 and 1 (Table 2), which indicates that metal ions adsorption on the adsorbent was favorable at all temperatures.

The results of heavy metal ions adsorption onto magnetic materials from various previous studies are shown in Table 3.

The maximum adsorption capacities of XCMCP for Pb²⁺ and Cu²⁺ were comparable to or higher than those of other magnetic adsorbents. XCMCP performed better in the separation process because of its higher saturation magnetization.

Regeneration ability

The adsorbent regeneration ability is important for its reuse, which could reduce the processing costs and allow for the recycling of useful materials. The exhausted adsorbent was eluted by using 0.1 M HCl solution. Seven consecutive metal

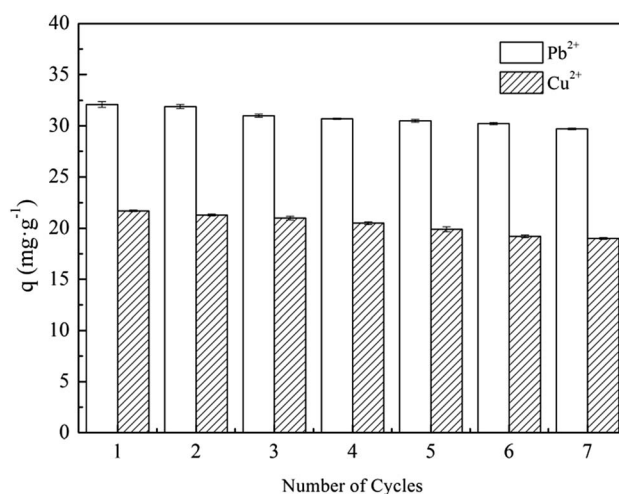


Fig. 6 Adsorption capacity of Pb²⁺ and Cu²⁺ onto XCMCP with seven adsorption-desorption cycles.



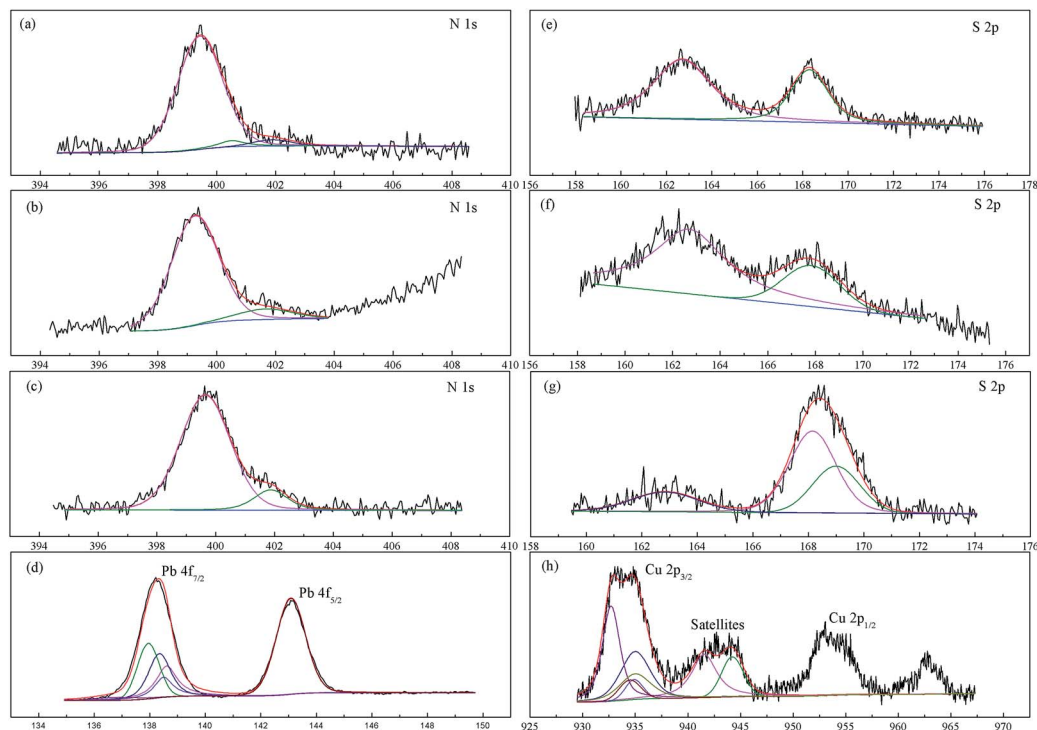


Fig. 7 N 1s spectrum of XCMCP (a), N 1s spectrum of XCMCP loaded with Pb^{2+} (b), N 1s spectrum of XCMCP loaded with Cu^{2+} (c), Pb 4f spectrum of XCMCP loaded with Pb^{2+} (d), S 2p spectrum of XCMCP (e), S 2p spectrum of XCMCP loaded with Pb^{2+} (f), S 2p spectrum of XCMCP loaded with Cu^{2+} (g), Cu 2p spectrum of XCMCP loaded with Cu^{2+} (h).

ions adsorption–desorption cycles were conducted on XCMCP under the same conditions. Compared with fresh adsorbent, the adsorption capability of the regenerated adsorbent decreased slightly after seven adsorption–desorption cycles (Fig. 6), and the adsorption capacity changed from 32.1 to 29.7 mg g^{-1} for Pb^{2+} and from 21.7 to 19.0 mg g^{-1} for Cu^{2+} . The physical properties of the regenerated adsorbent did not exhibit any obvious changes. These results indicate that elution with HCl solution regenerated the exhausted adsorbent. Therefore, XCMCP exhibits good properties for repeated use.

Adsorption mechanism

To investigate the interactions between XCMCP and heavy metals, and to elucidate the adsorption mechanisms of heavy metal ions onto particles, XPS analysis of the XCMCP surface was conducted before and after heavy metal adsorption. Survey scan results (not shown) indicated the presence of lead and copper, which demonstrates that the metal ions were adsorbed by XCMCP. The narrow C 1s, O 1s, and Fe 2p scans before and after adsorption (results not shown) did not indicate significant changes, which suggests that these atoms were not involved in the adsorption process. The narrow N 1s, S 2p, Pb 4f, and Cu 2p scans are shown in Fig. 7. The N 1s spectrum of XCMCP comprised three peaks with binding energies of 399.5, 400.5, and 401.9 eV (Fig. 7a). These peaks agreed with literature data.⁵⁵ The peak at 399.5 eV originated from $-\text{NH}_2$, which is the basic structural unit of chitosan.⁵⁶ The second peak at 400.5 eV was assigned to $\text{O}=\text{C}-\text{NH}-$ (amide) from the acetylated unit.⁵⁶ The

third peak at 401.9 eV was attributed to $-\text{NH}_3^+$ (protonated amine). The peaks of $\text{O}=\text{C}-\text{NH}-$ and $-\text{NH}_3^+$ were weak. The calculation of peak areas indicated that the total amine ($-\text{NH}_2$) and protonated amine ($-\text{NH}_3^+$) concentrations exceeded 95%, which indicates that chitosan had a high degree of deacetylation.⁵⁵ After Pb^{2+} adsorption (Fig. 7b), a new peak appeared at 399.7 eV, and the peak at 399.5 eV of XCMCP shifted slightly to 399.3 eV. After Cu^{2+} adsorption (Fig. 7c), a new peak appeared at 401.1 eV, and the peak at 399.5 eV of XCMCP shifted slightly to 399.7 eV. These phenomena are attributed to interactions of N atoms with the heavy metals (according to NIST XPS data). These results indicate the formation of complexes between the surface groups of XCMCP with heavy metal ions, where pairs of lone electrons from the N atoms were shared with Pb^{2+} or Cu^{2+} . The change in spectrum was more significant after Cu^{2+} adsorption, which suggests that N atoms were more important in the Cu^{2+} adsorption process.

The narrow S 2p scan before adsorption showed two peaks at 162.7 and 168.3 eV, which correspond to the thiol group and $\text{C}=\text{S}$, respectively (Fig. 7e).²⁸ After Pb^{2+} adsorption, the peak at 168.3 eV shifted to 167.8 eV (Fig. 7f). After Cu^{2+} adsorption, the spectrum comprised three peaks. The additional peak at 168.15 eV was attributed to $\text{S}-\text{O}$ in SO_4^{2-} , and initial peaks moved to 162.8 and 169.0 eV (Fig. 7g). The significant change in binding energy (>0.5 eV) is considered to be from chemical shifts.⁵⁷ This phenomenon may occur because of the coordination of S atoms with metal ions. Thus, the XPS spectra demonstrate the binding of Pb^{2+} and Cu^{2+} to S atoms.



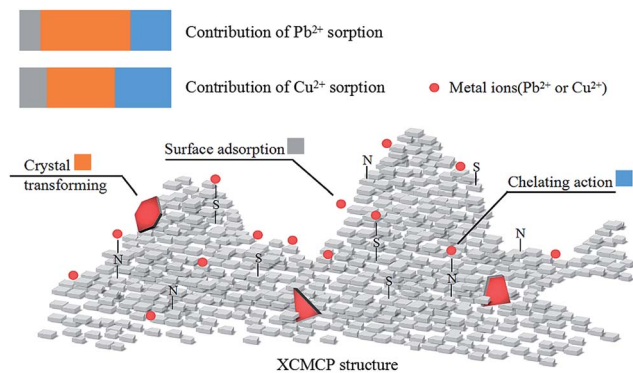


Fig. 8 Adsorption mechanism diagram and contributions of adsorption Pb^{2+} and Cu^{2+} onto XCMCP.

The Pb spectrum exhibits a doublet ($Pb\ 4f_{5/2}$ and $Pb\ 4f_{7/2}$) with symmetric peaks because of spin-orbit coupling (Fig. 7d). The area ratio of $4f_{5/2}$ to $4f_{7/2}$ was 3 : 4. The $4f_{7/2}$ peak could be decomposed into five contributions at 138.6 eV (23.78%), 137.95 eV (29.92%), 138.35 eV (29.23%), 138.5 eV (13.77%), and 136.85 eV (3.30%), which correspond to Pb-S, $Pb(OH)_2$, $PbCO_3$, $PbNO_3$, and $Pb-NH_2$, respectively (according to NIST XPS data). Chemical and physical sorption accounted for 27.08% and 72.92% of the adsorption process, respectively. Therefore, S atoms played a leading role in chemical sorption. In physical sorption, Pb^{2+} likely formed crystals and was adsorbed on the XCMCP surface. This speculation is consistent with the SEM and XRD results.

The Cu 2p XPS spectrum revealed three segments, Cu $2p_{1/2}$, Cu $2p_{3/2}$, and satellites (Fig. 7h). The appearance of satellites demonstrated the presence of Cu^{2+} ions.⁵⁸ The Cu $2p_{3/2}$ peak could be decomposed into five contributions at 935.1 eV (29.52%), 935.0 eV (17.81%), 934.9 eV (6.43%), 934.5 eV (7.69%), and 932.7 eV (38.55%), which were assigned to Cu-S, $CuCO_3$, $CuSO_4$, Cu- NH_2 , and $Cu(OH)_2$, respectively (according to NIST XPS data). Chemical and physical sorption accounted for 37.21% and 62.79% of the adsorption process, respectively. The mechanisms of Cu(II) sorption were similar to those of Pb(II).

In summary, the FTIR, SEM, and XRD analyses demonstrated that the xanthate group participated in the adsorption process, and that crystals appeared on the XCMCP surface after adsorption. These conclusions were confirmed by the XPS analysis, which indicated the following possible mechanism of heavy metal absorption by XCMCP: (1) N and S atoms interacted with heavy metals, (2) heavy metals were transformed to crystals, and (3) heavy metals adsorbed on the XCMCP surface (Fig. 8).

Conclusions

XCMCP was synthesized and tested for metal ions removal from aqueous solution. The characterization results showed that XCMCP was a rough and magnetic material with xanthate groups. The adsorption capacity of XCMCP for Pb(II) or Cu(II) was better in near-neutral pH. Chemical sorption was likely the rate-limiting step in Pb(II) and Cu(II) adsorption process.

Physical sorption was important in the adsorption process. External surface adsorption was the main rate-determining step for adsorption. Based on the isotherm models, the maximum adsorption capacities of XCMCP were 59.855 and 139.797 $mg\ g^{-1}$ for Pb(II) and Cu(II) at 328 K, respectively, and the reaction was a combination of homogeneous and heterogeneous adsorption. XCMCP exhibited a good property for repeated use and could still retain an effective adsorption efficiency after seven cycles. The mechanism for Pb(II) and Cu(II) adsorption onto XCMCP involved the interactions of N and S atoms with heavy metals, and the transformation of heavy metals to crystals followed by their adsorption on the XCMCP surface. The magnetic and reusability properties of XCMCP make it a promising adsorbent for hazardous-metal-ion-contaminated water treatment.

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