



Cite this: *RSC Adv.*, 2017, 7, 23523

# Ionic liquid assisted hydrothermal synthesis of MoS<sub>2</sub> double-shell polyhedral cages with enhanced catalytic hydrogenation activities†

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MoS<sub>2</sub> double-shell polyhedral cages are synthesized *via* an ionic liquid assisted hydrothermal process, in which the polyhedral cages of organic–inorganic hybrid phosphomolybdic acid-ionic liquids (PMA-ILs) are formed *in situ* and serve as a sacrificial template. The as-synthesized MoS<sub>2</sub> hierarchical polyhedral cages have a lateral length of 0.5–1.5 μm and average shell thickness of about 150 nm. The surfaces of MoS<sub>2</sub> double-shell polyhedral cages are very rough and composed of small nanosheets. The synthesis parameters including ionic liquid dosage, crystallization time and sulfur source are investigated to clarify the growth mechanism. Polycyclic aromatic hydrocarbons including naphthalene and anthracene were used as model compounds to evaluate the catalytic hydrogenation performance of the as-synthesized MoS<sub>2</sub> sample. It turns out that MoS<sub>2</sub> double-shell polyhedral cages manifest better catalytic hydrogenation activities than MoS<sub>2</sub> nanoparticles and commercial bulk MoS<sub>2</sub>. The double-shell hollow structure and the vertical-alignment of nanosheets in the polyhedral shell are responsible for the enhanced catalytic activities of MoS<sub>2</sub> double-shell polyhedral cages.

Received 28th February 2017  
 Accepted 23rd April 2017

DOI: 10.1039/c7ra02482g

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## 1. Introduction

Over the last few decades, two-dimensional molybdenum sulfide (MoS<sub>2</sub>) materials have attracted considerable attention due to their intriguing properties and widespread applications in catalysis, optoelectronics, electrochemistry and hydrogen storage fields.<sup>1–6</sup> In particular, MoS<sub>2</sub>-based materials have been extensively studied as effective hydrogenation catalysts for hydro-processing petroleum feed stock and upgrading heavy oil.<sup>7–10</sup> Up to now, supported MoS<sub>2</sub> catalysts have been extensively utilized for hydrogenation in a fixed-bed reactor.<sup>11–13</sup> However, the catalytic activity falls rapidly because of coking and metal deposition during the reaction process.<sup>14,15</sup> An alternative technology is slurry-phase hydrogenation process with highly dispersed unsupported catalysts.<sup>9,16,17</sup> In a slurry-phase reactor filled with hydrogen, all the reactants and catalysts are well-mixed and the temperature distribution is highly homogeneous under vigorous stirring. It's worth noting that only a small amount of catalyst is added into the slurry bed reactor

owing to its one-through operation. Thus exploring highly dispersed unsupported MoS<sub>2</sub> catalysts with abundant active sites is an urgent subject.

As a typical lamellar compound, MoS<sub>2</sub> naturally exists as hexagonal structure, in which the atoms within the layer are held together by strong covalent forces while the S–Mo–S layers are loosely bound to each other by van der Waals forces. It has been demonstrated that the catalytic performance of MoS<sub>2</sub> depends on the number of exposed active edge sites.<sup>18,19</sup> Compared to bulky MoS<sub>2</sub>, micro/nano MoS<sub>2</sub> catalysts can expose more active edge sites. Unfortunately, the agglomeration of MoS<sub>2</sub> nanosheets is almost unavoidable in most cases because of the high surface energy and van der Waals attraction. In these cases, only the edge sites of the outmost nanosheets are available for catalysis while a large amount of inner nanosheets are wrapped, which means a very low density of exposed active sites.

One of the most effective solutions to solve this problem is assembling two dimensional nanosheets into hierarchical architectures with well alignment and open texture, in which most pristine nanosheets can be exposed and preserve high exposed active sites.<sup>20,21</sup> Among various hierarchical architectures, hollow micro- and nano-structures are very advantageous to increase the active edge sites since they have unique internal void, low density, high surface-to-volume ratio and shell permeability.<sup>22,23</sup> Up to now, spherical or quasi-spherical MoS<sub>2</sub> hollow particles have been easily synthesized since the interface energy of sphere is relatively low.<sup>24–28</sup> Recently, nonspherical

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† Electronic supplementary information (ESI) available. See DOI: 10.1039/c7ra02482g



MoS<sub>2</sub> hollow cages have been constructed successfully. Xie and co-workers prepared MoS<sub>2</sub> hierarchical hollow cubic cages assembled by bilayers *via* a one-step self-assembly process.<sup>29</sup> The obtained MoS<sub>2</sub> hierarchical hollow cubic cages exhibit outstanding electrochemical hydrogen storage properties due to abundant active edges exposing on the upright-standing nanoplates. Afterwards, MoS<sub>2</sub> hollow cages with abundant geometrical morphologies were controllably synthesized by varying the surfactant concentrations.<sup>30</sup> In another work, Lou and co-workers reported a facile template-assisted strategy for the synthesis of hierarchical MoS<sub>2</sub> microboxes constructed by ultrathin nanosheets.<sup>21</sup> Compared to single-shell hollow structure, double-shell structure with novel geometrical morphology may be beneficial to expose more active edge sites. However, to the best of our knowledge, there is no report on the preparation of MoS<sub>2</sub> polyhedral hollow cages with double-shell structure. Besides, most studies about hollow materials focused on the electrochemistry performance.<sup>31,32</sup> The influence of hollow structure on traditional catalytic performance of MoS<sub>2</sub> materials needs to be studied further.

Herein, we report the synthesis of MoS<sub>2</sub> double-shell polyhedral cages *via* a simple ionic liquid 1-ethyl-3-methylimidazolium bromide ([EMIM]Br) assisted hydrothermal route using phosphomolybdic acid (PMA) and glutathione (GSH) as Mo and S precursors, respectively. A possible growth mechanism of MoS<sub>2</sub> double-shell polyhedral cages is presented based on the time-dependent experiments and contrast experiments. Anthracene and naphthalene were used as model compound to test the catalytic hydrogenation performance of as-synthesized MoS<sub>2</sub> double-shell polyhedral cages, respectively. It turns out that MoS<sub>2</sub> double-shell polyhedral cages manifest better activities than MoS<sub>2</sub> nanoparticles and commercial bulk MoS<sub>2</sub> in both reactions. It's speculated that the double-shell hollow structure and the way of nanosheet arrangement are advantageous to increase the number of exposed active sites, thus enhancing catalytic activities.

## 2. Experimental

### 2.1 Synthesis of MoS<sub>2</sub> double-shell polyhedral cages

All chemicals were analytical reagents and used without further purification. In a typical procedure, 0.125 mmol of phosphomolybdic acid (PMA), 4.5 mmol of glutathione (GSH), and 7.85 mmol of [EMIM] Br were dissolved into 50 mL of deionized water. The resulting solution was transferred into a 100 ml Teflon-lined stainless steel autoclave, which was then heated at 200 °C for 24 h. After that, the autoclave was allowed to cool down to room temperature naturally. The black precipitates were filtered and washed with deionized water and absolute ethanol. The final product was dried at 70 °C overnight in a vacuum oven.

### 2.2 Characterizations of MoS<sub>2</sub> double-shell polyhedral cages

XRD analysis of the obtained samples was performed on a PANalytical X'Pert PRO diffractometer fitted with a CuK $\alpha$  radiation source ( $\lambda = 1.5418 \text{ \AA}$ ) operating at 40 mA and 40 kV. Field-emission scanning electron microscope (FESEM) images were

acquired on an FEI Quanta 200F and JSM-7800 microscope operated at 20 kV. Transmission electron microscopy (TEM) images were collected on a JEM 2100 instrument at an accelerating voltage of 200 kV. CHNS analysis was conducted on a Flash 2000 organic elemental analyzer. BET specific surface areas were measured on an ASAP 2420 instrument by nitrogen adsorption.

### 2.3 Catalytic hydrogenation activities of MoS<sub>2</sub> double-shell polyhedral cages

The evaluation of catalytic hydrogenation activity was performed in a 100 ml stirred Parr high pressure vessel. For anthracene hydrogenation, 30 g tridecane, 3 g anthracene and 0.075 g MoS<sub>2</sub> catalysts were put into the autoclave. After discharging air with hydrogen for three times, the autoclave was pressured with hydrogen to 8.0 MPa at room temperature and then heated to 350 °C at a rate of 10 °C min<sup>-1</sup>. The reaction of anthracene hydrogenation was maintained at 350 °C for 4 h with stirring rate of 300 rpm. After cooling the autoclave naturally, the reaction mixtures were filtered to obtain liquid products. The filtrate was qualitatively analyzed with an Agilent 7890B/5977A GC/MS and quantitatively analyzed with an Agilent 7890A GC system. For naphthalene hydrogenation, the initial hydrogen pressure was 6.0 MPa, and the hydrogenation reaction was maintained at 300 °C for 6 h. The experimental operation was the same as anthracene hydrogenation.

## 3. Results and discussion

### 3.1 Characterizations of MoS<sub>2</sub> double-shell polyhedral cages

XRD pattern of as-synthesized MoS<sub>2</sub> sample was shown in Fig. 1. Diffraction peaks at about  $2\theta = 32^\circ$  and  $58^\circ$  can be assigned to (100) and (110) planes of 2H-MoS<sub>2</sub> (JCPDS no. 37-1492). It is worth noting that diffraction peak of (002) plane disappears, and two new peaks appear at  $2\theta = 8.9^\circ$  and  $17.9^\circ$ , corresponding to the interlayer distances of 9.9 Å and 5.0 Å, respectively. The nearly double relationship of the interlayer distances is due to the formation of a new lamellar structure with enlarged interlayer spacing of 9.9 Å, which is similar to the results reported by Xie's group and Wang's group.<sup>33,34</sup> We speculate that some

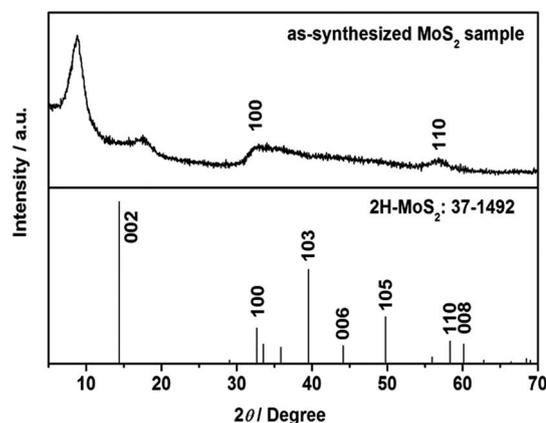


Fig. 1 XRD pattern of MoS<sub>2</sub> double-shell polyhedral cages.



groups of GSH or [EMIM] Br remained between the S–Mo–S layers, leading to the expansion of interlayer spacing. According to CHNS elemental analysis, 11.15 wt% of C, 1.67 wt% of H and 2.96 wt% of N were detected in the MoS<sub>2</sub> double-shell polyhedral cages sample, demonstrating the existence of intercalated guest species. After calcination at 350 °C under H<sub>2</sub> atmosphere for 2 h, all the diffraction peaks moved to higher angle and they can be assigned to hexagonal 2H MoS<sub>2</sub> (Fig. S1†). The reason for this shift probably is that the intercalated guest species were totally removed after the calcination, therefore, the interlayer distance returned to the standard values of 6.15 Å.

Fig. 2a indicates that the as-synthesized MoS<sub>2</sub> sample is composed of polyhedrons with side length of 0.5–1.5 micrometers. The interior space of the MoS<sub>2</sub> polyhedral cages can be observed from SEM image of a cracked MoS<sub>2</sub> polyhedral cage (Fig. 2b). The hierarchical shells of MoS<sub>2</sub> polyhedral cages have highly rough surfaces, which are constructed by nanosheets. Typical TEM image in Fig. 2c shows well-defined quadrangle and hexagon with quite a big cavity, which further confirms the polyhedral cage structure of the as-synthesized MoS<sub>2</sub> sample. It can be seen from Fig. 2c that there is a tiny gap in the middle of the shell, indicating the double-shell structure of MoS<sub>2</sub> sample. This structure is advantageous to reduce the density of MoS<sub>2</sub> catalyst and increase exposed edge sites. HRTEM image displays that the interlayer spacing of two adjacent S–Mo–S layers is about 1.0 nm while the distance between S–Mo–S layer and intercalated materials is about 0.5 nm (Fig. 2d), which is very close to the results of XRD pattern. After calcination at 350 °C under H<sub>2</sub> atmosphere for 2 h, the polyhedral cage structure of as-synthesized MoS<sub>2</sub> remained unchanged (ESI Fig. S2†), demonstrating the well structural stability of MoS<sub>2</sub> sample.

### 3.2 The effects of synthesis parameters on the growth process

It's believed that the oxidation–reduction between Mo<sub>3</sub>O<sub>10</sub><sup>2-</sup> in PMA and HS in GSH led to the formation of MoS<sub>2</sub>. The

sulfurization reagent GSH also serves as reductant. To investigate the formation mechanism of MoS<sub>2</sub> double-shell polyhedral cages, we investigated the synthesis parameters which may influence the growth process, including ionic liquid dosage, crystallization time and sulfur source.

**3.2.1 The effect of ionic liquid dosage.** Four MoS<sub>2</sub> samples were prepared by adding different dosages of ionic liquids while other reaction conditions remained the same. The samples were named as MS-ILs-*X*, in which *X* represents the mole ratio of ionic liquids and Mo atom. XRD pattern of Fig. 3 shows that the diffraction peaks of MoS<sub>2</sub> sample prepared without ILs are very weak. When the mole ratio of ionic liquids and Mo atom is 1.7, the intensities of all the diffraction peaks significantly increase, indicating a great enhancement of crystallinity. Further increasing the mole ratio of ionic liquids and Mo atom to 3.5 and 5.2 brings about little change of XRD patterns. The element composition of MoS<sub>2</sub> samples with different IL dosages was given by CHNS elemental analysis (Table 1). When no ILs were added, 13.86 wt% of carbon, 1.74 wt% of hydrogen and 2.16 wt% of nitrogen were detected in as-synthesized MoS<sub>2</sub> sample, giving a C/N atomic ratio of 7.48. C and N elements undoubtedly originate from groups of GSH, such as COOH<sup>-</sup> and NH<sub>2</sub><sup>-</sup>. After adding 2.62 mmol ILs (MS-ILs-1.7), the C/N atomic ratio decreases remarkably to 4.89. With the mole ratio of ionic liquids and Mo atom further increasing to 3.5 and 5.2, the C/N atomic ratio decreases slightly to 4.76 and 4.39, respectively. Since [EMIM]<sup>+</sup> of ILs also contains C and N elements and the C/N atomic ratio is different from that of GSH, it can be speculated that the increase of crystallinity and decrease of C/N ratio may be because of the intercalation of [EMIM]<sup>+</sup> in S–Mo–S layers. This speculation is consistent with the results of XRD (Fig. 1) and HRTEM (Fig. 2d). Overall, both XRD and CHNS analysis prove that IL influenced the crystallization process of MoS<sub>2</sub>.

SEM images of MoS<sub>2</sub> samples synthesized by adding different IL dosages are shown in Fig. 4a–d. It can be seen from Fig. 4a that MoS<sub>2</sub> sample prepared without IL consists of irregular particles which aggregate seriously. Compared to MS-ILs-0 sample, the dispersion of MS-ILs-1.7 sample becomes better and the sizes of the particles become more uniform (Fig. 4b). When the mole ratio of IL and Mo atom increases to 3.5, a few single-shell hollow cages can be observed while most of the particles are still irregular (Fig. 4c). Finally, MoS<sub>2</sub> hierarchical polyhedral cages can be obtained by increasing the mole ratio of IL and Mo atom to 5.2. By comparing the morphology of MoS<sub>2</sub> samples synthesized by adding different dosages of IL, we speculate that ILs serve as structure-directing agent in the formation of MoS<sub>2</sub> double-shell polyhedral cages.

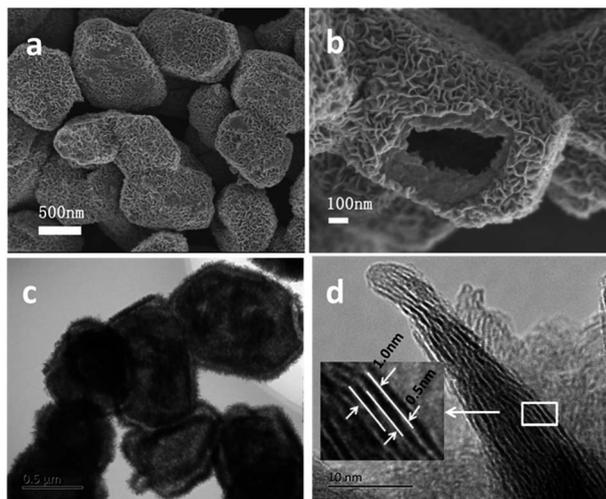


Fig. 2 (a and b) SEM, (c) TEM and (d) HRTEM images of MoS<sub>2</sub> double-shell polyhedral cages.

Table 1 CHNS analysis for MoS<sub>2</sub> samples synthesized by adding different dosages of ionic liquids

| sample     | C/wt% | N/wt% | H/wt% | S/wt% | C/N ratio |
|------------|-------|-------|-------|-------|-----------|
| MS-ILs-0   | 13.86 | 2.16  | 1.74  | 33.63 | 7.48      |
| MS-ILs-1.7 | 11.99 | 2.86  | 1.67  | 34.99 | 4.89      |
| MS-ILs-3.5 | 11.66 | 2.86  | 1.65  | 34.80 | 4.76      |
| MS-ILs-5.2 | 11.15 | 2.96  | 1.67  | 33.72 | 4.39      |



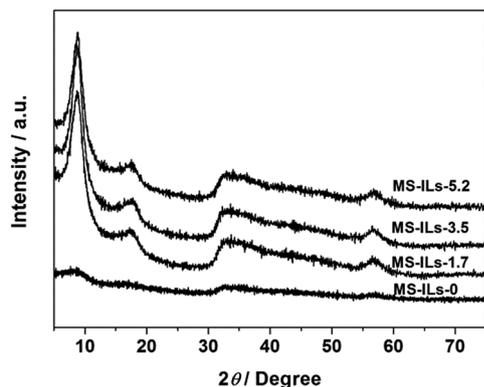


Fig. 3 XRD pattern of  $\text{MoS}_2$  samples prepared by adding different dosages of ionic liquids. X in MS-ILs-X means the mole ratio of ionic liquids and Mo atom.

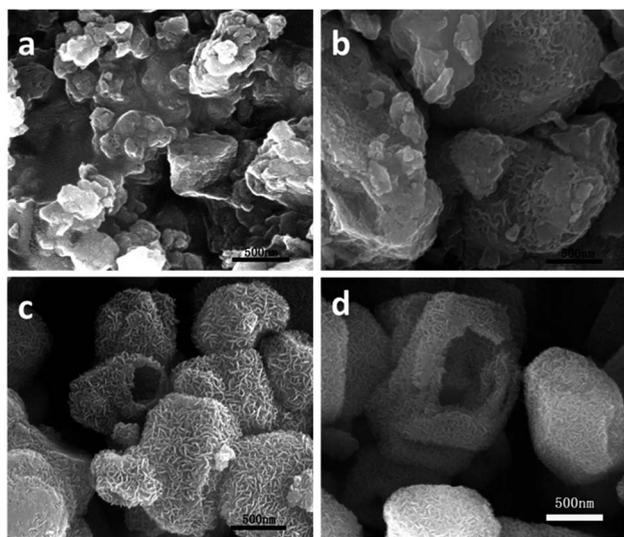


Fig. 4 SEM images of  $\text{MoS}_2$  samples prepared by adding different dosages of ionic liquid. The mole ratio of ILs and Mo atom is as follows: (a) 0, (b) 1.7, (c) 3.5 and (d) 5.2.

**3.2.2 The effect of crystallization time.** A series of time-dependent experiments were performed to study the formation mechanism of  $\text{MoS}_2$  double-shell polyhedral cages. The obtained products were labelled as MS-t-Y, in which Y represents the crystallization time. XRD pattern of MS-t-1 is very close to XRD pattern of hydrothermal product of PMA and ILs (Fig. S3†), which suggests that the precursor is mainly formed by the interaction between PMA and ILs. Thus the precursor was named as PMA-ILs, which is an organic-inorganic hybrid.

SEM images of precursor PMA-IL (Fig. 5a and b) display the well-defined hollow polyhedron morphology with smooth surfaces. The side length of polyhedrons is 0.5–1.5  $\mu\text{m}$ , which is similar to that of final  $\text{MoS}_2$  product. The shape and size of the intermediate MS-t-3 remain the same with that of PMA-ILs hybrid while the surfaces of the polyhedron become rather rough (Fig. 5c). Besides, double-shell structure can be found

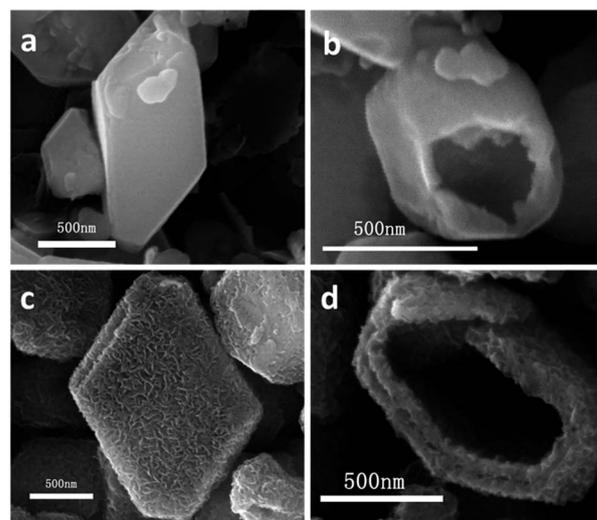


Fig. 5 SEM images of time-dependent experiments products at different time: (a and b) 1 h and (c and d) 3 h.

from the SEM image of broken particle (Fig. 5d), which is the same with that observed from TEM image in Fig. 2c.

The sulfur content of samples synthesized by different crystallization time was tested by CHNS elemental analysis. It turns out that the precursor MS-t-1 contains 5.32 wt% of sulfur. Since only small amounts of sulfur were detected, we speculate that MS-t-1 contains a small number of sulfur-contained intermediate while the major component is organic-inorganic hybrid PMA-ILs. When the hydrothermal reaction proceeds to 3 h, the mass fraction of sulfur is 24.84%. The significantly increase of sulphur content indicates the formation of sulfur-contained intermediate. With the reaction time further prolongs to 6 h, 12 h, 18 h and 24 h, the sulphur content increases to 25.25, 29.10, 32.18 and 33.72 wt%, respectively. The gradual increase of sulphur content in samples may results from the participation of some dispersive sulfur ions in the oxidation-reduction reaction, which leads to the final formation of  $\text{MoS}_2$ .

**3.2.3 The effect of sulfur source.** In order to investigate the role of GSH in the formation of  $\text{MoS}_2$  hierarchical polyhedral cages, contrast experiments were carried out without adding any sulfur source. The hydrothermal product of PMA and ILs were collected after crystallization for 1 h and 24 h. As mentioned before, the XRD patterns of the obtained products (Fig. S3†) are very close to that of MS-t-1. However, the product obtained from contrast experiments with hydrothermal time of 1 h (Fig. 6a) consisted of pebble-like solid particles with size of 100–500 nm, much smaller than the counterpart of precursor MS-t-1 (Fig. 5a and b). After hydrothermal synthesis of PMA and ILs for 24 h, as-synthesized product grows into large polyhedrons with the size of larger than ten micrometres (Fig. 6b). These polyhedrons are solid and composed by more than a dozen tetragonal and hexagonal faces. The results of contrast experiments imply that the polyhedron feature of  $\text{MoS}_2$  double-shell polyhedral cages may originate from PMA-ILs organic-inorganic hybrid while the hollow structure may originate from



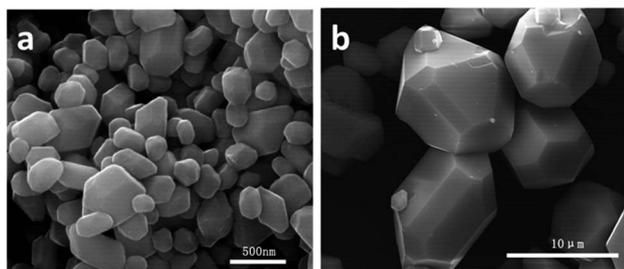


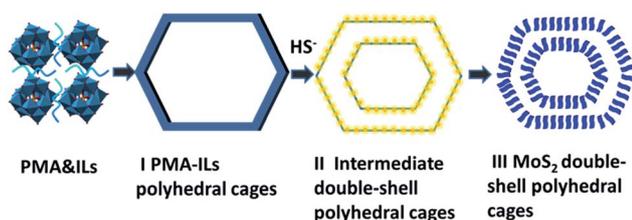
Fig. 6 SEM images of hydrothermal products of PMA and ILs at different time: (a) 1 h and (b) 24 h.

the sulfur of GSH. Furthermore, to some extent, the presence of GSH prevents the growth of organic–inorganic hybrid into big crystal.

Other sulfur sources such as thiourea, thioacetamide and elemental sulfur were adopted instead of GSH while other reaction conditions remained the same. SEM images in Fig. S4† show that all the three common sulfur sources are unable to retain the polyhedral morphology of PMA-ILs organic–inorganic hybrid. To sum up, GSH plays an important role in the formation of MoS<sub>2</sub> double-shell polyhedral cages and prevents the growth of PMA-ILs organic–inorganic hybrid into big crystals.

### 3.3 The possible growth mechanism of MoS<sub>2</sub> double-shell polyhedral cages

Based on the above discussion of ionic liquid dosage, crystallization time and sulfur source, we speculate that the growth mechanism of MoS<sub>2</sub> hierarchical polyhedral cages is as follows. First of all, Mo<sub>3</sub>O<sub>10</sub><sup>2-</sup> anion of PMA and [EMIM]<sup>+</sup> cation of ILs bind together due to the electrostatic interaction, generating PMA-ILs organic–inorganic hybrid, which is schematic as Scheme 1. PMA has a typical “Keggin” structure, in which P<sup>5+</sup> serves as central ion and four Mo<sub>3</sub>O<sub>10</sub><sup>2-</sup> anions surround P<sup>5+</sup> as ligands. Each Mo<sub>3</sub>O<sub>10</sub><sup>2-</sup> ligand contains three Mo–O tetrahedrons, which connect with each other through the corners and edges. Recently, Gao and co-workers proposed that the anisotropic molybdate anions are the main reason for oriented growth of MoO<sub>x</sub>-based organic–inorganic hybrid nanostructures.<sup>35</sup> Thus the tetrahedral building blocks of PMA provide the possibility of synthesizing polyhedral MoS<sub>2</sub> materials. In our experiments, [EMIM]<sup>+</sup> cations of ILs are considered as structure-directing agents and adsorbed on some planes of Mo–O tetrahedrons, resulting in the formation of polyhedral



Scheme 1 Illustration of the possible growth mechanism of MoS<sub>2</sub> double-shell polyhedral cages.

PMA-ILs hybrid. Meanwhile, the peptide chains of GSH are uniformly dispersed in the solution and form steric hindrance effect, hindering the agglomeration and growing up of PMA-ILs hybrid.

For the second step, PMA-ILs hybrid reacts with HS- of GSH, which are located at the inside and outside of the polyhedral shell, to generate sulfur-contained intermediate (Scheme 1-II). The tiny gap in the middle of intermediate shell (Fig. 5d) is probably due to the different diffusion rates of PMA-ILs hybrid and GSH. That is to say, the PMA-ILs hybrid diffuses into the solution in a faster rate than that of GSH movement from solution to the surface of polyhedral shell. As a result, the polyhedral shell of PMA-ILs hybrid disappears, and two new polyhedral shells of intermediate form on both sides of the original shell. This process is similar to Kirkendall effect reported by Xie and co-workers.<sup>29</sup> During this process, PMA-ILs hybrid serves as sacrifice template. At last, oxidation–reduction between the intermediate and Mo<sub>3</sub>O<sub>10</sub><sup>2-</sup> proceeds at the hydrothermal temperature, and MoS<sub>2</sub> hierarchical polyhedral cages are finally formed (Scheme 1-III).

### 3.4 Catalytic hydrogenation activities of MoS<sub>2</sub> double-shell polyhedral cages

Catalytic hydrogenation reactions of anthracene and naphthalene were performed in a slurry-phase reactor to investigate the catalytic activities of MoS<sub>2</sub> double-shell polyhedral cages (labelled as MS-PCs). For comparison, commercial MoS<sub>2</sub> (MS-Com) and MoS<sub>2</sub> nanoparticles (MS-NPs), which were hydrothermal synthesized by PMA and GSH without adding ILs, were also used as hydrogenation catalysts. Besides, the anthracene hydrogenation performance of MoS<sub>2</sub> single-shell polyhedral cages MS-ILs-3.5 (Fig. 4c) was also tested.

Hydrogenation of anthracene proceeds ring by ring *via* reversible successive steps.<sup>36</sup> First, 9,10-dihydroanthracene (AH<sub>2</sub>) is generated by hydrogenation of the middle ring of anthracene. As the reaction proceeds, tetrahydro-product (AH<sub>4</sub>), octahydro-product (AH<sub>8</sub>), and perhydroanthracene (AH<sub>14</sub>) appear in sequence. The first-ring hydrogenation reaction of anthracene is most favored kinetically. Thus it's easy to reach a high conversion of anthracene to AH<sub>2</sub>. However, the hydrogenation rates of subsequent rings tend to become slower. The hydrogenation of the last ring is most difficult. Based on the above analysis, the activity of MoS<sub>2</sub> catalysts mainly depends on the selectivity of deeply hydrogenated products (AH<sub>8</sub> and AH<sub>14</sub>).

Conversion and selectivity of anthracene hydrogenation products are displayed in Fig. 7. Conversion of anthracene hydrogenation with MS-NPs and MS-PCs catalysts is 100%, and the conversion for MS-Com is 90.9%. The high conversion is due to the easy transformation from anthracene to AH<sub>2</sub>, which is mentioned above. Selectivity of hydrogenation products differs greatly for all the catalysts. AH<sub>2</sub> was the main product when MS-Com was adopted as catalyst. The selectivity of deeply hydrogenated products AH<sub>8</sub> is highest (78.2%) with MS-PCs as catalyst. Besides, 1.38% of fully hydrogenated product AH<sub>14</sub> appeared when MS-PCs were adopted as hydrogenation catalyst. As for MS-NPs catalyst, its selectivities of AH<sub>8</sub> and AH<sub>14</sub> are



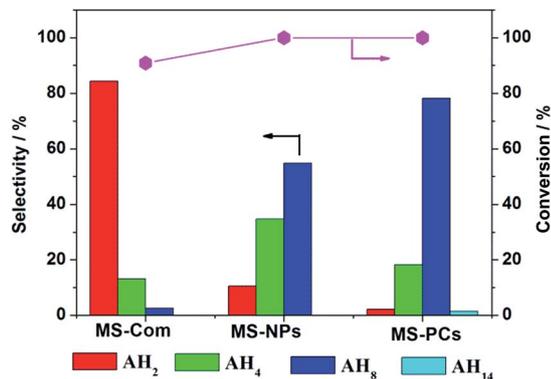


Fig. 7 Selectivity and conversion of anthracene hydrogenation reaction using MS-Com, MS-NPs and MS-PCs as catalysts. Reaction conditions:  $T = 350\text{ }^{\circ}\text{C}$ ,  $P_{\text{H}_2} = 8\text{ MPa}$ ,  $t = 4\text{ h}$ , 2.5 wt% cat.

inferior to those of MS-PCs catalyst. By comparing selectivity of deeply hydrogenated products, we can draw the conclusion that MS-PCs catalyst has the optimal hydrogenation activity, followed by MS-NPs and MS-Com. When using MoS<sub>2</sub> single-shell polyhedral cages MS-ILs-3.5 as catalyst, the conversion of anthracene is 99.46% and the selectivity of deeply hydrogenated products AH<sub>8</sub> is 69.92%. The catalytic activity of single-shell polyhedral cages is lower than that of double-shell polyhedral cages (Fig. S5†).

Tetrahydronaphthalene (NH<sub>4</sub>) is the main product of naphthalene hydrogenation. The selectivity of decalin (NH<sub>10</sub>) is very low since the generation of NH<sub>10</sub> is thermodynamics restricted. Besides, small amounts of hydrocracking products (HYC) 1,3-dimethyl benzene were detected. The conversion of naphthalene hydrogenation reaction using MS-Com catalyst is very low (2.07%). The conversion with MS-PCs is the highest, followed by MS-NPs (Fig. 8).

As we all know, the activity of MoS<sub>2</sub> catalysts is closely related to its dimension and microstructure. It can be seen from Fig. 9a and d that MS-Com is composed of micro-sized S-Mo-S layers with the stacking layer number of more than a dozen. Fig. 9b and e show that MS-NPs are aggregates of nanosheets with the

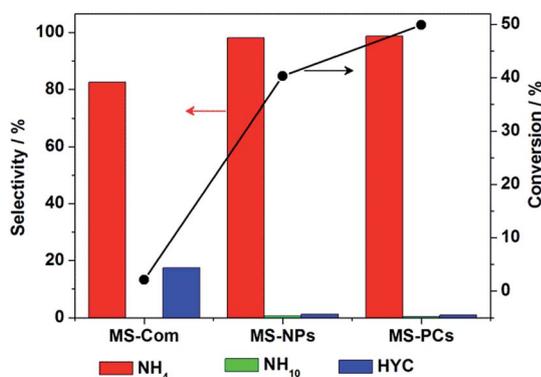


Fig. 8 Selectivity and conversion of naphthalene hydrogenation reaction using MS-Com, MS-NPs and MS-PCs as catalysts. Reaction conditions:  $T = 300\text{ }^{\circ}\text{C}$ ,  $P_{\text{H}_2} = 6\text{ MPa}$ ,  $t = 6\text{ h}$ , 2.5 wt% cat.

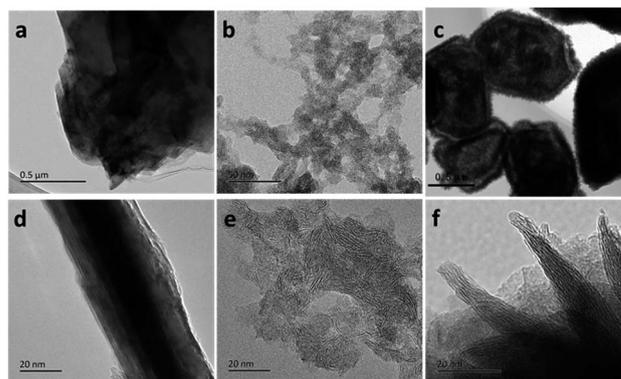


Fig. 9 TEM images of (a and d) MS-Com, (b and e) MS-NPs, (c and f) MS-PCs catalysts.

length of 5–20 nm. In the TEM images of MS-PCs, most of the nanosheets are perpendicular to the double shells of MoS<sub>2</sub> polyhedral cages, exposing abundant active edge sites (Fig. 9c and f).

The BET specific surface areas of MS-Com, MS-NPs and MS-PCs were measured N<sub>2</sub> physisorption. It turns out that MS-NPs have the largest specific surface areas, followed by MS-PCs and MS-Com. It can be concluded that the hydrogenation activity of MoS<sub>2</sub> catalysts doesn't depend on the surface area. This is similar to the results reported by Ramos *et al.*<sup>37</sup> This result is because most of the surface areas result from the basal planes of MoS<sub>2</sub> nanosheets, which are catalytic inert.

According to "Rim-edge" model proposed by M. Daage and R. R. Chianelli, active sites of MoS<sub>2</sub> for hydrogenation are rim sites which located at the top and bottom layers.<sup>18</sup> Due to its much smaller size, MS-NPs have much more rim sites than MS-Com. However, the seriously agglomeration of nanosheets in MS-NPs (Fig. 9b and e) hampers the exposure of rim sites, thus exhibits poor hydrogenation performance. This problem is greatly alleviated in the case of MS-PCs since the vertical-alignment of nanosheets in the polyhedral shell ensures the exposure of abundant rim sites. Moreover, the hollow double-shell structure reduces the density of catalyst and greatly increases the contact areas between reactant molecules and catalysts. In consequence, the as-synthesized MoS<sub>2</sub> double-shell polyhedral cages are highly active for catalytic hydrogenation of anthracene and naphthalene. The SEM images of MS-Com, MS-NPs and MS-PCs after anthracene hydrogenation reaction were displayed in Fig. S6,† showing no obvious change of morphology. Thus the structural stability of as-synthesized MoS<sub>2</sub> sample was very well.

## 4. Conclusions

MoS<sub>2</sub> double-shell polyhedral cages with lateral length of 0.5–1.5 μm and average shell thickness of 150 nm have been successfully synthesized *via* an ionic liquid assisted hydrothermal route. The growth mechanism of MoS<sub>2</sub> double-shell polyhedral cages is speculated by discussing the synthesis parameters including ionic liquid dosage, crystallization time



and sulfur source in detail. It's believed that the anisotropy of  $\text{Mo}_3\text{O}_{10}^{2-}$  in phosphomolybdic acid and structure-directing effect of ionic liquids [EMIM] Br lead to the formation of organic-inorganic hybrid PMA-ILs polyhedral cages. Afterwards, the hybrid serves as sacrifice template and interacts with glutathione to generate intermediate. Further oxidation-reduction between the intermediate and  $\text{Mo}_3\text{O}_{10}^{2-}$  produces  $\text{MoS}_2$  double-shell polyhedral cages. Furthermore, the catalytic property of  $\text{MoS}_2$  hierarchical polyhedral cages for anthracene and naphthalene hydrogenation is superior to  $\text{MoS}_2$  nanoparticles and commercial bulk  $\text{MoS}_2$ . The hollow structure and the vertical-alignment of nanosheets in the polyhedral shell are the main reasons for the enhancing catalytic hydrogenation activities of  $\text{MoS}_2$  double-shell polyhedral cages. Significantly, the strategy of synthesizing  $\text{MoS}_2$  double-shell polyhedral cages here provides new route to design novel nanostructures of other transition metal sulfides.

## Acknowledgements

This work was financially supported by the Strategic Priority Research Program of the Chinese Academy of Sciences (Grant No. XDA07020300) and the National Natural Science Foundation of China (Grant No. 21303186).

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