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Palladium–nickel catalysts based on ordered titanium dioxide nanorod arrays with high catalytic performance for formic acid electro-oxidation†

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Ordered titanium dioxide nanorod arrays are prepared by a hydrothermal method and applied to the catalyst supports of the palladium–nickel catalysts ($\text{Pd}_2\text{Ni}_3\text{-TiO}_2$) for formic acid oxidation. Due to the three-dimensional catalytic structure and alloying effect, the $\text{Pd}_2\text{Ni}_3\text{-TiO}_2$ exhibits superior mass activity and long-term stability than those of Pd-TiO_2 and commercial PdC catalysts. The present work opens a new approach to design catalysts with superior catalytic performance and durability for direct formic acid fuel cells with three-dimensional catalytic structure.

Introduction

Direct formic acid fuel cells (DFAFCs) have potential to serve as promising power sources for portable electronics, due to their relatively high power density, low fuel crossover, and low pollutant emission.^{1,2} However, the development of DFAFCs is hindered by the sluggish formic acid electro-oxidation (FAO) and low durability of catalysts.^{3,4} It is known that the Pt-based catalysts are not suitable as the catalysts of FAO, because the catalysts are easily poisoned by CO during the FAO. Pd-based catalysts are believed to be more suitable for FAO due to their lower adsorption of CO intermediates in catalyzing formic acid.^{5–7} Nevertheless, the electrochemical activity and stability of Pd-based catalysts should be improved. Increasing the activity of Pd-based catalysts will lead to a low dosage of Pd in practical utilization.

Previous studies have proven that controlling the sizes and morphologies of Pd-based catalysts is an effective way to improve the catalytic performance for FAO. Several Pd-based catalysts have been demonstrated, such as Pd nanowires,⁸ Pd nanorods,⁹ and the combination of Pd with transition metals (e.g., Ni, Co, Fe, Cu), Ag or P to form bimetallic compounds.^{10–16} Nevertheless, the catalytic structure and the support material also have an impact on the catalytic activity of the electrocatalysts.¹⁷ Metal oxides can be used as the support materials in fuel cells, due to their high corrosion resistance, reasonable surface area, and mechanical strength.^{18,19} Among them, Ti-based oxides has been applied as the catalyst support material

of fuel cells. Subramanian *et al.* applied anodized TiO_2 nanotubes (T_NT) as the Pt support for simultaneous FAO and photo-assisted FAO, which generates around 39-fold higher current density than that of the pure T_NT.²⁰ Xing *et al.* investigated the fine-tuned pore structured $\text{TiO}_2\text{-C}$ as the Pt or Pd catalyst supports for the electro-oxidation of methanol or formic acid, which showed a much superior catalytic performance than that of the carbon support.²¹

Based on the above considerations, we present TiO_2 NRs as the catalyst supports of Pd-based catalysts. To the best of our knowledge, the Pd-based alloy nanoparticles supported on the TiO_2 NRs are rarely reported as the catalysts toward FAO. The advantages of this approach are listed: (1) high transport rate of HCOOH ; (2) high electrochemical surface area (ECSA) and high utilization of electrocatalysts; (3) direct charge carrier transport pathways. More importantly, we combine high catalytic activity and advanced catalytic structure to show the highest electrochemical activity. Compared with the commercial PdC catalyst and pure Pd-TiO_2 catalysts, the $\text{Pd}_2\text{Ni}_3\text{-TiO}_2$ catalyst exhibited higher electrochemical activity and stability.

Experimental

Preparation of TiO_2 NRs

Oriented TiO_2 NRs were hydrothermally grown on carbon fibers by a seed-assisted method and the details of the preparation process are shown in the previous report.^{22,23} There are two key points for the formation of the oriented TiO_2 NRs, which are exactly controlling the concentration of the titanium(IV) chloride aqueous solution and tetrabutyl titanate (TBT) solution.

Preparation of the PdNi-TiO_2 and Pd-TiO_2

For the preparation of the PdNi-TiO_2 electrode, Ni and Pd catalysts were sputtered onto the TiO_2 NRs by physical vapor

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deposition (PVD) in a row and the whole sputtering time was maintained for 15 min and 6 min, respectively. After that, to increase the crystal size of the catalysts, the as-prepared samples were heat-treated at 300 °C under 5% H₂/Ar gas for 2 h. For the preparation of Pd-TiO₂ NRs, the preparation process was similar to that of PdNi-TiO₂ NRs without Ni deposition.

Physical characterization

Field-emission scanning electron microscopy (FESEM, Zeiss supra 55) and transmission electron microscopy (TEM, JEM-2000EX) are employed to observe the morphology of the as-prepared samples. High-resolution transmission electron microscopy (HRTEM, JEM-2100F) characterization and energy-dispersive X-ray (EDX) analysis were conducted using FEI Tecnai G2F30 microscopy operating at 300 kV. The crystal phases of the samples were monitored by X-ray diffraction (XRD, BrukerD8, Cu K α radiation). X-ray photoelectron spectroscopy (XPS, Thermo Scientific ESCALab 250 Xi spectrometer, Al K α in twin anode) was used to measure the chemical state of all the samples. Inductively coupled plasma-optical emission spectroscopy (ICP-OES, PerkinElmer 7300DV, USA) was applied to determine the metal loadings in the samples.

Electrochemical characterization

The electrochemical properties of all the samples were measured using a conventional three-electrode cell at room temperature. The PdNi-TiO₂ NRs, Pd-TiO₂ NRs, and a commercial PdC (BASF, 20% PdC) based electrode were used as the working electrodes. A saturated calomel electrode (SCE) and a Pt-foil served as the reference electrode and the counter electrode, respectively. The PdNi-TiO₂ NRs and Pd-TiO₂ NRs are directly used as the working electrode without additional Nafion ionomer. The commercial PdC based electrode was prepared by spraying the commercial PdC and Nafion ionomer (I/C = 0.5) on a commercial gas diffusion layer (GDL). Prior to all the experiments, the mixture was saturated with N₂ gas. Cyclic voltammetry (CV) and chronoamperometric (CA) experiments were carried out in a mixture including 0.5 M H₂SO₄ + 0.5 M HCOOH. CV curves were tested at the potential window between 0–1.0 V (vs. SCE) with the sweeping rate of 50 mV s⁻¹. CA curves were recorded at 0.55 V (vs. SCE) and maintained for 4000 s.

Results and discussion

TiO₂ NRs were directly grown on carbon paper by a hydrothermal method.^{22–24} PdNi-TiO₂ NRs and Pd-TiO₂ NRs were deposited onto the TiO₂ NRs by PVD and heat-treated in 5% H₂/Ar gas. Here the carbon paper is employed as a current collector, and the as-prepared electrodes can potentially be used as an anodic electrode of DFAFCs directly.

The XRD analysis was first applied to monitor the corresponding crystal phase of all the samples and is displayed in Fig. 1. The as-prepared products are mainly composed of rutile TiO₂ phases according to JCPDS 21-1276. The Ti 2p XPS

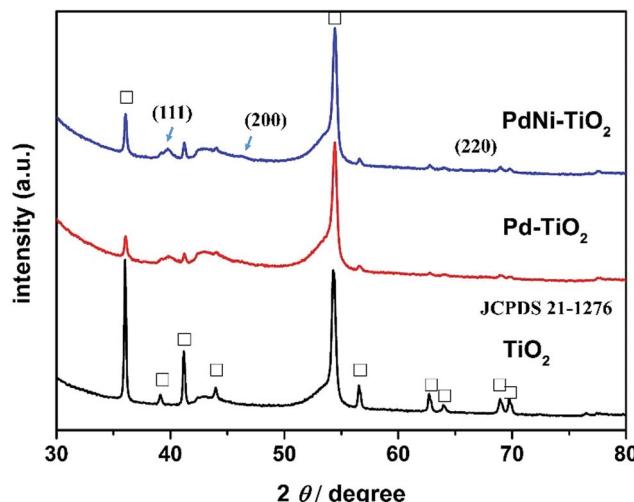


Fig. 1 XRD patterns of TiO₂, Pd-TiO₂, and PdNi-TiO₂.

spectrum of the as-prepared sample is shown in Fig. S2.[†] The binding energies of Ti 2p_{1/2} and Ti 2p_{3/2} are 458.58 eV and 464.38 eV, respectively. Since the binding energy of Ti⁴⁺ is 458.5 eV, the XPS data prove the presence of TiO₂. After deposition of the Pd and PdNi nanoparticles, the (111) peak for the Pd-TiO₂ and PdNi-TiO₂ is obviously in the XRD pattern (Fig. 1). Due to the low metal content in the products, the diffraction peaks of the (200), and (220) planes of the Pd-based catalysts are not specified in the XRD patterns.

FESEM images of Pd-TiO₂ NRs and PdNi-TiO₂ NRs grown on carbon paper are shown in Fig. 2a and b (inset). The oriented TiO₂ nanorods grew on the surface of carbon fibres, and the mean diameters of the TiO₂ nanorods are about 120 nm (Fig. S1[†]). After deposition of the Pd-based catalysts onto the TiO₂ NRs, the resulting samples are heat-treated in 5% H₂/Ar gas at 300 °C for 2 h. The morphology and structure of the as-prepared samples are not obviously changed compared with that of TiO₂ NRs. The TEM image of a TiO₂ nanorod shows that the surface of the TiO₂ nanorod is smooth (Fig. 2c). The Pd nanoparticles and PdNi nanoparticles are dispersed on the TiO₂ nanorod (Fig. 2d and e) and the size distributions of the Pd and PdNi nanoparticles are shown in Fig. 2d and e (inset) and S3.[†] Fig. 2d and e show that the mean sizes of the Pd and PdNi catalysts are about 3.52 nm and 4.24 nm, respectively. However, the sizes of some other PdNi particles are about 20 nm (Fig. S3[†]), which are larger than Pd nanoparticles. The average sizes of the Pd and PdNi catalysts according to XRD are 6.09 nm and 7.53 nm, respectively, which are larger than the particle sizes of the Pd-based catalysts. Since the general detection depth of XRD measurements is around 10 nm, the composition detected by XRD indicates both surface and bulk atoms of the Pd-based catalysts.

The HR-TEM image reveals that the PdNi particles are crystalline and the lattice structure is clear (Fig. 2f). The (111) lattice spacing of the PdNi nanoparticles was measured to be 0.219 nm, which is between that of Pd (0.223 nm) and Ni (0.20 nm), confirming the formation of PdNi alloy in the as-prepared

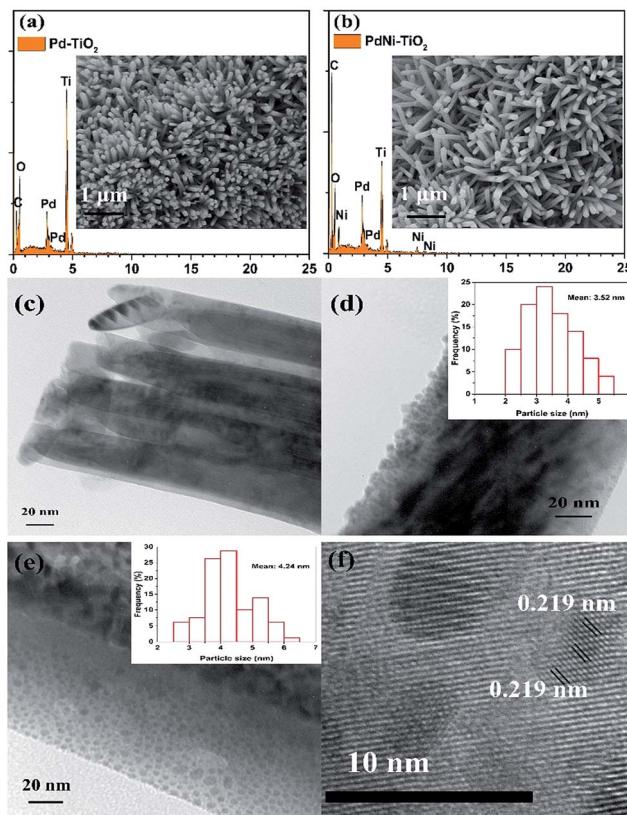


Fig. 2 FESEM images and EDX spectra of Pd-TiO₂ NRs (a) and PdNi-TiO₂ NRs (b); TEM images of TiO₂ (c), Pd-TiO₂ (d) and PdNi-TiO₂ (e); and HRTEM image of PdNi-TiO₂. The inset pictures in (d) and (e) are the size distributions of Pd and PdNi catalysts, respectively.

samples.²⁵ EDX analysis was also carried out to measure the composition of the PdNi-TiO₂ catalysts. The spectrum confirms that Pd and Ni elements exist in the PdNi nanoparticles and their atomic ratio is 1 : 1.72 (Fig. S4†). In addition, the Pd and Ni content in the as-prepared samples is estimated by ICP-OES, and the results are 40.55 $\mu\text{g cm}^{-2}$ and 14.4 $\mu\text{g cm}^{-2}$, respectively. Thus, the atomic ratio of Pd and Ni in the PdNi-TiO₂ catalysts is 1 : 1.55 according to the result of ICP-OES, which is consistent with the EDX data. Thus, the PdNi-TiO₂ catalysts can be named as Pd₂Ni₃-TiO₂ according to the data of ICP-OES. Meanwhile, the Pd loading of the Pd-TiO₂ NRs is measured as 29.7 $\mu\text{g cm}^{-2}$.

XPS was applied to analyze the chemical states and electronic states of Pd and Ni in the as-prepared samples. The Pd 3d spectra for the PdNi-TiO₂ NRs and Pd-TiO₂ NRs are shown in Fig. 3a. The Pd 3d XPS spectra of Pd-TiO₂ NRs show the binding energies of Pd⁰ 3d ($3d_{5/2} = 335.26$ eV; $3d_{3/2} = 340.53$ eV, Fig. 3a), which are slightly higher than those of bulk Pd ($3d_{5/2} = 334.90$ eV; $3d_{3/2} = 340.15$ eV).²⁶ The slight shift of binding energies of Pd⁰ to higher ones may be attributed to the significant interaction between Pd nanoparticles and TiO₂ supports. Meanwhile, after the formation of PdNi alloys, the Pd 3d binding energy of Pd₂Ni₃-TiO₂ NRs is shifted to a more negative position than that of Pd-TiO₂ NRs. This shift may be attributed to the difference of the electronegativity between Pd and Ni,

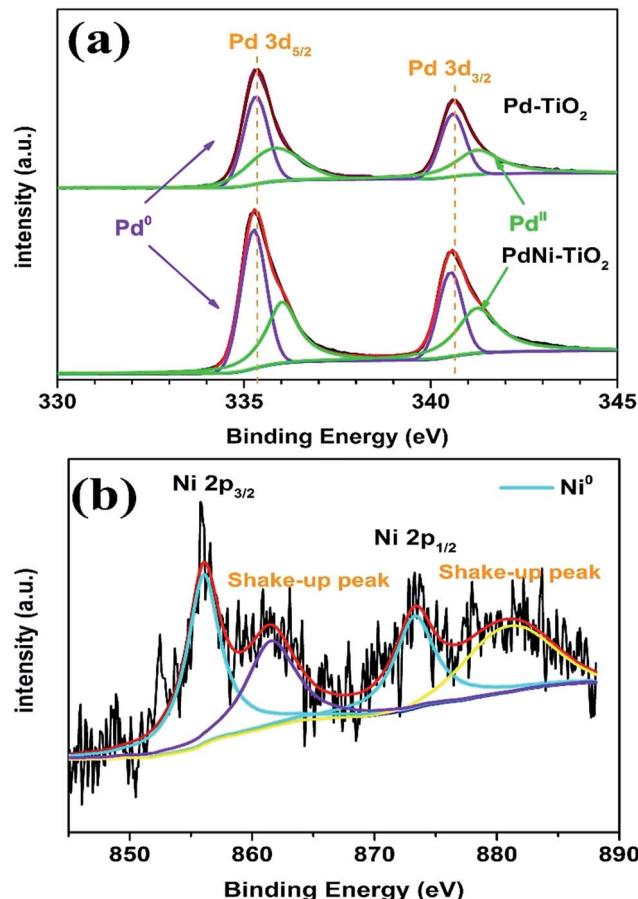


Fig. 3 XPS spectra of (a) Pd 3d carried out on the Pd-TiO₂ NRs and PdNi-TiO₂ NRs and (b) Ni 2p carried out on the PdNi-TiO₂ NRs.

resulting in a partial electron transfer from Ni to Pd, which would change the penetration of outer electron density of Pd.²⁷ Fig. 3b shows that Ni(OH)₂ and NiOOH with obvious shake-up peaks can be seen at higher binding energies than those of the high-energy band (Ni 2p_{3/2}) and the low-energy band (Ni 2p_{1/2}).²⁵

To investigate the electronic activity of the as-prepared Pd₂Ni₃-TiO₂ NRs, we employed FAO as the model system, comparing with pure Pd-TiO₂ NRs and commercial PdC. Typical Pd electrochemical behaviours of all the Pd-based electrocatalysts and the TiO₂ sample were observed in 0.5 M H₂SO₄ (Fig. 4a and S5†). The ECSA was estimated according to the area of hydrogen adsorption peaks and the calculation equation is according to that previously reported.^{17,28,29} The CVs of Pd-TiO₂, and Pd₂Ni₃-TiO₂ are shown in Fig. 4a. The calculated ECSAs of Pd-TiO₂, Pd₂Ni₃-TiO₂, and commercial PdC are 53.6 $\text{m}^2 \text{g}^{-1}$, 43.6 $\text{m}^2 \text{g}^{-1}$, and 37.6 $\text{m}^2 \text{g}^{-1}$, respectively. Since some PdNi nanoparticles are larger than the Pd nanoparticles at the surface of the TiO₂ nanorods, the ECSA of the Pd₂Ni₃-TiO₂ NRs is smaller than that of the Pd-TiO₂.

The electrocatalytic properties of the Pd₂Ni₃-TiO₂ catalysts towards FAO were investigated in a 0.5 M H₂SO₄ + 0.5 M HCOOH mixture. The electrocatalytic properties of the Pd-TiO₂ and the commercial PdC toward FAO were measured for

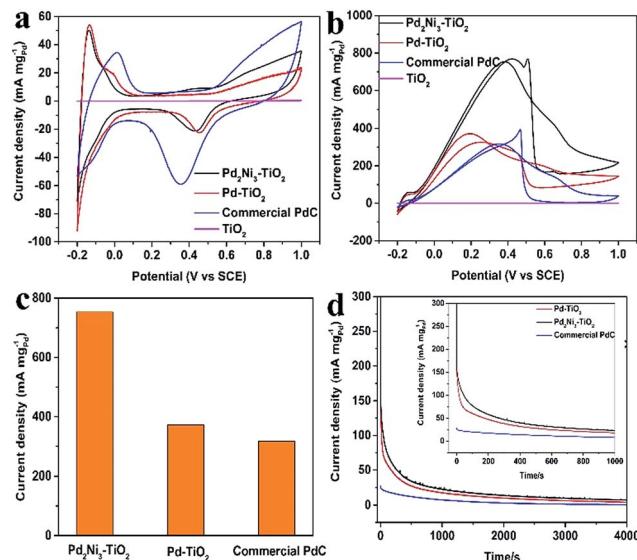
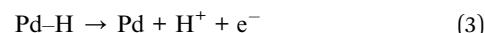


Fig. 4 (a) CVs of $\text{Pd}-\text{TiO}_2$, $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$, and commercial PdC in the $0.5 \text{ M H}_2\text{SO}_4$ solution at a sweeping rate of 50 mV s^{-1} ; (b) CVs of FAO of all samples in $0.5 \text{ M H}_2\text{SO}_4$ solution + 0.5 M HCOOH at the scan rate of 50 mV s^{-1} ; (c) the mass activity of different catalysts at the peak position; (d) CA curves of all samples in $0.5 \text{ M H}_2\text{SO}_4$ solution + 0.5 M HCOOH at 0.25 V . The unit of current density of the TiO_2 sample is mA cm^{-2} .

comparison. Fig. 4b shows the CV curves of FAO of different catalysts. All the current densities of FAO of different samples were normalized by Pd loading (mass activity). The TiO_2 samples show no catalytic performance in the $0.5 \text{ M H}_2\text{SO}_4$ and $0.5 \text{ M H}_2\text{SO}_4$ containing 0.5 M HCOOH mixture (Fig. 4a, b, S5a and S4b†). Meanwhile, after deposition of Pd nanoparticles, the as-prepared $\text{Pd}-\text{TiO}_2$ catalyst exhibits high catalytic activity as its mass density is $371.87 \text{ mA mg}^{-1}$, which is around 1.17-fold higher than that of commercial PdC (Fig. 4c). The enhancement of the onset potential of the as-prepared $\text{Pd}-\text{TiO}_2$ catalysts compared with the commercial PdC for FAO might be explained by the formation of a three-dimensional catalytic structure. The performance will be further improved by adding Ni element to Pd. Many studies shows that the highest FAO performance of a PdNi catalyst is when the atomic ratio of Pd and Ni is around $1:1$.^{10,25,30} After alloying with Ni, the catalytic activity of $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ is further improved ($753.42 \text{ mA mgPd}^{-1}$, Fig. 4b), indicating the electronic structure modification after Pd alloying with Ni, as demonstrated in the XPS analysis, which has been observed in many other Pd-based alloys.³¹ The FAO reaction occurs over the surface atom layer of the Pd-based catalysts for the test samples. With a similar amount of $\text{Pd}-\text{TiO}_2$, $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ shows better catalytic activity toward the FAO than $\text{Pd}-\text{TiO}_2$. Ni element does not catalyze the FAO reaction, thus the Ni must be improving the catalytic activity of the Pd element toward FAO in such a way that the FAO rate is increased consequently.³² One possible effect is that the Pd surface electronic structure is perturbed by Ni.³³ The d-band center of the catalysts will be altered and the electronic structure of the Pd surface layer will be affected by the formation of the PdNi

alloy.³⁴ During the FAO reaction, the HCOOad (HCOO-Pd) is formed firstly through breaking the O–H bond of HCOOH .³⁵ The possible reaction steps are listed as follows.^{35,36}



After the Pd d-band center is shifted to an optimum value, the Pd-adsorbate bond strength will be optimized.³² We believe that the Pd d-band center is shifted to an optimum value after alloying with Ni, thus $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ shows the best catalytic activity toward FAO. At the same time, the strong interactions between TiO_2 and metals (strong metal–support interaction, SMSI) have been shown in previous research,³⁷ thus the stability of the catalysts will be enhanced. Compared with the oxidation peak potential of formic acid in the literature,³⁸ $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ did not show excellent catalytic activity for FAO with a more positive oxidation peak potential, and the possible reason is the low electronic conductivity of TiO_2 though oriented TiO_2 NRs, which were hydrothermally grown on carbon fibers. Meanwhile, compared with the similar state-of-the-art Pd-based electrocatalysts, the as-prepared $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ exhibits higher mass activity than most of them (Table S1†).

To further evaluate the surface poisoning, CA curves of $\text{Pd}-\text{TiO}_2$, $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$, and commercial PdC were investigated in $0.5 \text{ M H}_2\text{SO}_4 + 0.5 \text{ M HCOOH}$ with the potential of 0.25 V for 4000 s during the measurements (Fig. 4d). It is obvious that the decrease in current density for the FAO on the $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ NRs is slower than that of the $\text{Pd}-\text{TiO}_2$ NRs and commercial PdC , which indicates its higher tolerance to the intermediaries during FAO. The improvement of the catalytic performance is possibly attributed to the alloying effect and the advanced catalytic structure.

Conclusions

In conclusion, we have designed and synthesized a three-dimensional catalytic structure based on TiO_2 NRs. We found that $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ catalysts show higher mass activity and higher durability than $\text{Pd}-\text{TiO}_2$ catalysts and commercial PdC catalysts. Moreover, the improved catalytic activity of the $\text{Pd}_2\text{Ni}_3-\text{TiO}_2$ catalyst is taking advantage of its unique three-dimensional structure and the alloying effect during FAO. In addition, this work provides a new avenue to design electrocatalysts with superior catalytic activity and stability for DFAFCs and they can be used as an electrode directly.

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