

Cite this: *RSC Adv.*, 2017, 7, 17311

# Fluorine substituted (Mn,Ir)O<sub>2</sub>:F high performance solid solution oxygen evolution reaction electro-catalysts for PEM water electrolysis†

Shrinath Dattatray Ghadge,<sup>‡a</sup> Prasad Prakash Patel,<sup>‡a</sup> Moni Kanchan Datta,<sup>bc</sup> Oleg I. Velikokhatnyi,<sup>bc</sup> Ramalinga Kuruba,<sup>b</sup> Pavithra M. Shanthi<sup>a</sup> and Prashant N. Kumta<sup>\*abcde</sup>

Identification and development of high performance with reduced overpotential (*i.e.* reduced operating electricity cost) oxygen evolution reaction (OER) electrocatalysts for proton exchange membrane (PEM) based water electrolysis with ultra-low noble metal content (*i.e.* reduced materials cost) is of significant interest for economic hydrogen production, thus increasing the commercialization potential of PEM water electrolysis. Accordingly, a novel electrocatalyst should exhibit low overpotential, excellent electrochemical activity and durability superior to state of the art noble metal based electro-catalysts (*e.g.* Pt, IrO<sub>2</sub>, RuO<sub>2</sub>). Herein, for the very first time to the best of our knowledge, exploiting first-principles theoretical calculations of the total energies and electronic structures, we have identified a reduced noble metal content fluorine doped solid solution of MnO<sub>2</sub> and IrO<sub>2</sub>, denoted as (Mn<sub>1-x</sub>Ir<sub>x</sub>)O<sub>2</sub>:F ( $x = 0.2, 0.3, 0.4$ ), OER electrocatalyst system exhibiting lower overpotential and higher current density than the state of the art IrO<sub>2</sub> and other previously reported systems for PEM water electrolysis. The doped solid solution displays an excellent electrochemical performance with a lowest reported onset potential to date of  $\sim 1.35$  V (*vs.* RHE),  $\sim 80$  mV lower than that of IrO<sub>2</sub> ( $\sim 1.43$  V *vs.* RHE) and  $\sim 15$  fold ( $x = 0.3$  and  $0.4$ ) higher electrochemical activity compared to pure IrO<sub>2</sub>. In addition, the system displays excellent long term electrochemical durability, similar to that of IrO<sub>2</sub> in harsh acidic OER operating conditions. Our study therefore demonstrates remarkable,  $\sim 60$ – $80\%$  reduction in noble metal content along with lower overpotential and excellent electrochemical performance clearly demonstrating the potential of the (Mn<sub>1-x</sub>Ir<sub>x</sub>)O<sub>2</sub>:F system as an OER electro-catalyst for PEM water electrolysis.

Received 26th November 2016

Accepted 6th March 2017

DOI: 10.1039/c6ra27354h

rsc.li/rsc-advances

## 1. Introduction

The inherent unceasing global energy demand, accelerating the diminution of fossil fuels and the continuing upsurge of our carbon footprint causing potentially perilous damage to the global climate are the primary thrusts for the pursuit of renewable and non-carbonaceous clean energy sources.<sup>1–4</sup> In this milieu, hydrogen has garnered immense attention for

transportation and stationary applications on the grounds of its high energy density and low carbon footprint.<sup>5–9</sup> However, the efficient and economic production of hydrogen from a non-carbonaceous clean source along with cost-effective storage and distribution are major challenges that need to be addressed before hydrogen can be commercially developed as an energy carrier for transportation at industrial scales.<sup>10,11</sup> In this direction, hydrogen production from water splitting, *via* water electrolysis is considered as a promising approach due to its non-toxic and non-carbonaceous nature.<sup>12,13</sup> In specific, water electrolysis operation in acidic media, known as proton exchange membrane (PEM) water electrolysis, is considered to be more advantageous than that in neutral and basic media due to higher efficiency, superior production rates, more compact design and increased product purity for operation in acidic media.<sup>14–16</sup> Oxygen evolution reaction (OER) for efficient hydrogen production is the major driver for water electrolysis under PEM conditions.

The slow reaction kinetics as well as the concomitant high reaction overpotential (*i.e.* high operating electricity cost) of OER electrocatalyst ( $\sim 200$  mV overpotential for IrO<sub>2</sub>) and the

<sup>a</sup>Chemical and Petroleum Engineering, Swanson School of Engineering, University of Pittsburgh, PA 15261, USA

<sup>b</sup>Department of Bioengineering, Swanson School of Engineering, University of Pittsburgh, 815C Benedum Hall, 3700 O'Hara Street, Pittsburgh, PA 15261, USA. E-mail: pkumta@pitt.edu; Fax: +1-412-624-3699; Tel: +1-412-648-0223

<sup>c</sup>Center for Complex Engineered Multifunctional Materials, University of Pittsburgh, PA 15261, USA

<sup>d</sup>Mechanical Engineering and Materials Science, University of Pittsburgh, Pittsburgh, PA 15261, USA

<sup>e</sup>School of Dental Medicine, University of Pittsburgh, PA 15217, USA

† This is an abstract presented at the AIChE Annual Meeting, San Francisco, CA, USA (November 14–18, 2016).

‡ The authors have contributed equally to this work.



high materials cost due to need of expensive and precious noble metals OER electro-catalysts (Pt, IrO<sub>2</sub>, RuO<sub>2</sub>) has thwarted the progress and commercialization of PEM based water electrolysis.<sup>17–20</sup> Therefore, the OER reaction ( $E^0 = 1.23$  V vs. NHE), which occurs at the anode of PEM water electrolysis cells, is an important, challenging and energy intensive process.<sup>12,21–23</sup> Hence, the identification and development of high performance, faster reaction kinetics, highly active and low overpotential OER electro-catalyst with ultra-low noble metal content will considerably aid in achieving high efficiency and also help reduce the materials and electricity costs of PEM based water electrolysis cells.<sup>24–26</sup>

In the pursuit of identifying low noble metal content electro-catalysts as a replacement of currently used expensive pure IrO<sub>2</sub> or RuO<sub>2</sub> electro-catalysts, one of the widely adopted approaches is mixing of robust and cheap transition metal oxides (e.g. SnO<sub>2</sub>, Ta<sub>2</sub>O<sub>5</sub>, Nb<sub>2</sub>O<sub>5</sub>, TiO<sub>2</sub>) with IrO<sub>2</sub> and/or RuO<sub>2</sub> (e.g. IrO<sub>2</sub>–SnO<sub>2</sub>, RuO<sub>2</sub>–SnO<sub>2</sub>, IrO<sub>2</sub>–Ta<sub>2</sub>O<sub>5</sub>, IrO<sub>2</sub>–SnO<sub>2</sub>–Nb<sub>2</sub>O<sub>5</sub>, etc.) maintaining the electronic conductivity and catalytic activity similar to IrO<sub>2</sub> and/or RuO<sub>2</sub> and improving the durability of IrO<sub>2</sub> and/or RuO<sub>2</sub>.<sup>12,23,27,28</sup> However, in this approach, with increase in the content of non-noble metal oxides above 50 wt%, there is deterioration in catalytic activity due to a decrease in the electrochemical active surface area and electronic conductivity.<sup>12,23,27</sup> We<sup>29,30</sup> have recently identified several F doped binary and ternary solid solution oxides [(M,M',Ir)O<sub>2</sub>:F; M,M' = Sn, Nb] with significant reduction in IrO<sub>2</sub> (~70–80 mol% reduction) content albeit exhibiting similar electrochemical performance to pure IrO<sub>2</sub> electro-catalyst, thus offering significant reduction in materials cost of the PEM water splitting process. However, all these developed [(M,M',Ir)O<sub>2</sub>:F; M,M' = Sn, Nb] electro-catalysts show similar electrochemical performance (i.e. overpotential and activity) to that of pure IrO<sub>2</sub>.<sup>29,30</sup> In addition to lowering the materials cost, a novel electro-catalyst offering lower operating electricity cost with significantly improved electrochemical performance (lower overpotential and faster kinetics) with respect to IrO<sub>2</sub> needs to be identified in order to commercialize PEM water electrolysis technology. The focus of the current work is thus not only on the identification and development of novel electro-catalyst with reduced noble metal content but more importantly, identifying reduced noble metal containing systems that exhibit faster reaction kinetics, low overpotential, superior electrochemical performance than that of pure IrO<sub>2</sub> utilizing the prudent two pronged theoretical and experimental approach.

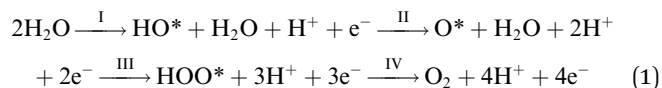
In this work, for the very first time to the best of our knowledge, exploiting first-principles theoretical calculations of the total energies and electronic structures, we have identified fluorine doped solid solution of MnO<sub>2</sub> and IrO<sub>2</sub>, denoted as (Mn<sub>1–x</sub>Ir<sub>x</sub>)O<sub>2</sub>:F electro-catalyst system exhibiting lower overpotential and higher current density than state of the art IrO<sub>2</sub> and also superior electrochemical performance as compared to other solid solution based OER electro-catalyst systems in PEM water electrolysis.<sup>25,29–32</sup> These results will portend significant reduction in noble metal content in electro-catalyst aiding in achieving significantly reduced material's cost as well as operating electricity cost. In addition, in the current study,

a thorough investigation of total energies, electronic structure and density of electronic states of the as-synthesized electro-catalysts, employing the density functional theory has been implemented. The present study also determines the free energy ( $\Delta G$ ) values of (Mn,Ir)O<sub>2</sub> electro-catalyst system which successfully shows the significant decrease in the onset potential of (Mn,Ir)O<sub>2</sub> electro-catalyst system.

In the present study, fluorine (F) is chosen as an anionic dopant for the (Mn<sub>1–x</sub>Ir<sub>x</sub>)O<sub>2</sub> solid solution due to its pivotal role in improving the electrochemical activity of [(M,M',Ir)O<sub>2</sub>:F; M,M' = Sn, Nb] for OER in acidic media as already demonstrated by us previously following experiments and first principles calculations.<sup>29,30</sup> The results of the theoretical studies are experimentally verified by synthesizing thin film architectures of (Mn<sub>1–x</sub>Ir<sub>x</sub>)O<sub>2</sub> ( $x = 0, 0.3, 1$ ) and (Mn<sub>1–x</sub>Ir<sub>x</sub>)O<sub>2</sub>:10F ( $x = 0.2, 0.3, 0.4$ ) electro-catalysts on Ti foil (substrate). Thus, for the very first time, we document the theoretical studies, synthesis, physical characteristics, and electrochemical performance of nanostructured (Mn<sub>1–x</sub>Ir<sub>x</sub>)O<sub>2</sub> ( $x = 0, 0.3, 1$ ) and (Mn<sub>1–x</sub>Ir<sub>x</sub>)O<sub>2</sub>:10F ( $x = 0.2, 0.3, 0.4$ ) thin film electro-catalysts for OER in PEM water electrolysis.

## 2. Computational methodology

The overall electro-catalytic activity and the overpotential of (Mn,Ir)O<sub>2</sub>:F OER electro-catalyst is expected to depend on the electronic structure and thermodynamics of the four elementary steps (eqn (1)) of OER under acidic conditions.



wherein \* represents an active site on the metal oxide surface.<sup>33</sup>

To study the influence of compositions on the electronic structure as well as the activity of the electro-catalyst, theoretical analysis has been performed. The computational component of the current study is to understand the electronic structure of (Mn,Ir)O<sub>2</sub>:F oxides with the following chemical compositions: (Mn<sub>1–x</sub>Ir<sub>x</sub>)O<sub>2</sub>, with  $x = 0.17, 0.33, 0.5$  and (Mn<sub>0.83</sub>Ir<sub>0.17</sub>)O<sub>1.33</sub>F<sub>0.67</sub>, corresponding approximately to 10 wt% of F. Also, for comparison purposes pure IrO<sub>2</sub> oxide has been considered as a standard electro-catalyst for PEM based water electrolysis.

In order to determine the electric potentials at which a certain specific reaction would occur, the free energies ( $\Delta G$ ) of all the four anodic intermediate reactions (I–IV) have been considered. Therefore, a methodical analysis of all the calculated free energies may explain the rate determining step of the oxygen evolution reaction. This systematic analysis is essential for the knowledge of electro-catalytic activity of the specific material used as an electro-catalyst in water electrolysis reaction.

For comparison purposes two different materials have been chosen for calculation of the OER elementary steps: pure IrO<sub>2</sub> and IrO<sub>2</sub> doped with small amount of Mn as a substituent of Ir at the corresponding Ir-type lattice sites. For calculations of the total energies and electronic structure of the above mentioned oxides bulk and (110) surface rutile structure with a tetragonal



unit cell and space group  $P4_2/mnm$  have been utilized. The rutile structure of  $\text{IrO}_2$  and  $(\text{Mn},\text{Ir})\text{O}_2\text{:F}$  have been experimentally confirmed from XRD analysis which will be presented in the Experimental results section to follow.

For bulk calculations  $[1 \times 1 \times 3]$  supercell containing three elementary unit cells stacked in  $c$  direction has been chosen as the basis for construction of different Ir, Mn, and F concentrations of the oxide solid solution. Such a supercell contains 6 transition metal atoms and 12 atoms of oxygen/fluorine. Thus, for convenience of calculations the basic composition has been chosen *i.e.* several different atomic ratios of Mn/Ir, such as 5/1 corresponds to  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_2$  formula unit, while 4/2 and 3/3 correspond to  $(\text{Mn}_{0.67}\text{Ir}_{0.33})\text{O}_2$  and  $(\text{Mn}_{0.5}\text{Ir}_{0.5})\text{O}_2$  formula units, respectively. For simulation of 10 wt% of fluorine, 4 atoms of oxygen were randomly replaced with corresponding number of fluorine atoms generating the following formula unit:  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_{1.33}\text{F}_{0.67}$ . Such composition has been chosen for smaller representative super-cells for all the calculation of bulk and surface electronic structures employed in the present study.

For calculation of the (110) surface electronic properties of the materials, a two-dimensional slab repeated in  $[1, -1, 0]$  direction with 24 atom unit cell containing four oxygen layers with three oxygen–metal mixed layers in between them. A vacuum distance  $\sim 12$  Å between adjacent images of the slab was selected.

Following the previous studies,<sup>33,34</sup> for the calculation of the free energies of all the elementary reactions *i.e.* (I)–(IV) for  $\text{IrO}_2$  with and without Mn atoms located at the surface, the rutile type (110) preferred surface which is covered with oxygen has been selected. The  $2 \times 2$  surface unit cell for a symmetric 7-layer slab of  $\sim 10.3$  Å thickness which is separated between its images perpendicular to the surface direction by vacuum space of  $\sim 20$  Å has been taken which will prevent the interaction between the slab and its adjacent images. On the coordinated unsaturated sites of both sides of the chosen slab, all intermediate species involved in the OER *i.e.*  $\text{O}^*$ ,  $\text{OH}^*$ , and  $\text{OOH}^*$  have been attached. Three middle layers of the slab were fixed with the lattice parameter corresponding to the bulk  $\text{IrO}_2$ . Apart from these three middle layers, all other layers of the slab together with the intermediate species were fully relaxed and therefore, all the mathematical data obtained from such model should be divided by two.

A unit cell chosen for the calculations in the present study has been shown in Fig. 1. Two different atomic positions of Mn as a replacement of Ir in the unit cell have been considered to investigate the difference between the electronic structures of pure and doped  $\text{IrO}_2$  compounds as well as to assess the role of Mn on lowering of the overpotential of the  $(\text{Mn},\text{Ir})\text{O}_2$ . The first Mn-atomic distribution consists of one Mn-atom located in place of Ir just below the coordinatively unsaturated site (CUS) with an oxygen vacancy shown on Fig. 1a. The second distribution is characterized by introduction of Mn-atom at the lower part of the unit cell while the CUS locates above the Ir atom [Fig. 1b]. In order to calculate the free energies of all the four elementary reaction steps discussed above, such two different unit cells which have been covered by adsorbed oxygen monolayers in conjunction with intermediate species at the surface have been used.

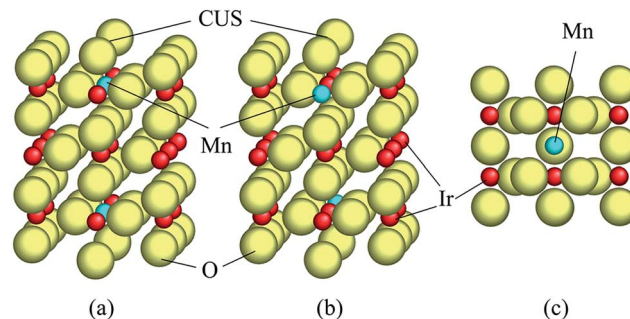


Fig. 1 Angle and top view of the elementary unit cell of the (110) rutile surface slab used in the present study: red – Ir, blue – Mn, yellow – oxygen (a) represents Mn at the center of the unit cell, (b) represents Mn at the side, (c) top view of the unit cell with Mn at the center. A coordinatively unsaturated site (CUS) is indicated by black lines.

For calculating the total energies, electronic structure and density of electronic states of the studied materials, the density functional theory implemented in Vienna Ab initio Simulation Package (VASP) was used within the projector-augmented wave (PAW) method<sup>35–37</sup> and the spin-polarized generalized gradient approximation (GGA) for the exchange–correlation energy functional in a form described by Perdew and Yue.<sup>38</sup> This computational package analyses the electronic structure and *via* Hellmann–Feynman theorem, the inter-atomic forces are determined from first-principles. The standard PAW potentials were utilized for the elemental components and the Ir, Mn, O and F potentials thus contained nine, seven, six and seven valence electrons, respectively. In the present theoretical analysis, to maintain the high precision for total energy calculations for all the electro-catalyst compositions, the plane wave cutoff energy of 520 eV has been chosen. By employing the double relaxation procedure, the internal positions as well as the lattice parameters of atoms have been completely optimized.

Moreover, the minima of the total energies with respect to the lattice parameters and internal ionic positions have been determined. Also, by minimizing the Hellman–Feynman forces *via* a conjugate gradient method, the geometry optimization was achieved. This will cause the net forces applied on every ion in the lattice close to zero. The total electronic energies were converged within  $10^{-5}$  (*i.e.* 0.00001) eV per unit cell which result into the residual force components on each atom to be lower than 0.01 eV per Å per atom. This allows the accurate determination of the internal structural parameters. Herein, the Monkhorst–Pack scheme has been used to sample the Brillouin Zone (BZ) and create the  $k$ -point grid for the solids and the different isolated atoms used in the current study. The selection of an appropriate number of  $k$ -points in the irreducible part of the BZ was made on the grounds of the convergence of the total energy to 0.1 meV per atom.

It is noteworthy to mention that, for Mn–Ir–O–F compositions, the corresponding atomic distributions are uncertain and thus, different spatial configurations can be used for exemplification of the atomic distributions. This uncertainty has been eliminated by assembling the various atomic configurations for each selected composition and the configurations which



correspond to the minimum total energy, have been selected for conducting further numerical analysis of these specific compositions of the binary oxides.

### 3. Experimental methodology

#### 3.1. Synthesis of $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$ ( $x = 0, 0.3, 1$ ) and $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_{2:10}\text{wt}\% \text{F}$ ( $x = 0.2, 0.3, 0.4$ )

Iridium tetrachloride ( $\text{IrCl}_4$ , 99.5%, Alfa Aesar), manganese chloride ( $\text{MnCl}_2$ , 99.5%, Aldrich) and ammonium fluoride ( $\text{NH}_4\text{F}$ , 98%, Alfa Aesar) were used as the sources for Ir, Mn and F respectively. Stock solutions of  $\text{IrCl}_4$ ,  $\text{MnCl}_2$  and  $\text{NH}_4\text{F}$  of the desired compositions were prepared in deionized (D.I.) water (18 M $\Omega$  cm, MilliQ Academic, Millipore). These stock solutions were mixed together according to the desired composition of the electro-catalyst material and then spin coated onto titanium foils (Alfa Aesar) of  $\sim 1\text{ cm}^2$  area ( $0.5\text{ cm} \times 2\text{ cm}$ ) (used as a substrate). The spin coating (Speciality coating Systems Inc., Model P6712) was performed employing a rotating speed of 500 rpm for 10 s with suitable amount of the precursors selected to achieve a desired total loading of  $\sim 0.3\text{ mg cm}^{-2}$  of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_{2:10}\text{F}$  oxide electro-catalyst. The precursors spin coated on Ti foil were then thermally treated at  $400^\circ\text{C}$  for 4 h in air to initiate decomposition and adequate reaction of the precursors to form  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_{2:10}\text{F}$  solid solutions on the Ti foil to achieve a total electro-catalyst loading of  $\sim 0.3\text{ mg cm}^{-2}$ . It should be noted that the same chemical approach was used to generate  $\text{IrO}_2$  thin films on the Ti foil serving as the control for comparing the electrochemical activity of the Mn substituted  $\text{IrO}_2$  solid solutions and F-doped Mn substituted  $\text{IrO}_2$  solid solutions.

#### 3.2. Electro-catalyst materials characterization

**3.2.1. Structural characterization.** X-ray diffraction (XRD) analysis has been performed to obtain qualitative phase information of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_{2:10}\text{F}$  electro-catalyst materials. XRD has been performed using the Philips XPERT PRO system employing  $\text{CuK}_\alpha$  radiation source ( $\lambda = 0.15406\text{ nm}$ ) at an operating current and voltage of 40 mA and 45 kV, respectively. The least square refinement techniques have been utilized to determine the molar volume and lattice parameters of the electro-catalyst materials of different compositions.<sup>7,39</sup> Scanning electron microscopy (SEM) has been conducted to investigate the microstructure of electro-catalysts. Quantitative elemental analysis and elemental X-ray mapping of elements have been performed by utilizing the energy dispersive X-ray spectroscopy (EDX) analyzer attached with the SEM machine. Philips XL-30FEG equipped with an EDX detector system comprising of an ultrathin beryllium window and Si(Li) detector operating at 20 kV was used for obtaining information on the microstructure as well as conducting elemental and X-ray mapping analysis of the electro-catalyst.

X-ray photoelectron spectroscopy (XPS) was used to investigate the oxidation states of Mn and Ir in  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_{2:10}\text{F}$  electro-catalysts. XPS analysis was carried out using the ESCALAB 250 Xi system (Thermo Scientific) equipped

with a monochromated Al  $K\alpha$  X-ray source. The standard analysis spot of  $400 \times 400\text{ }\mu\text{m}^2$  was defined by the micro-focused X-ray source. The system is operated at a room temperature in an ultra-high vacuum chamber with a base pressure less than  $5 \times 10^{-10}$  mbar. The binding energy (BE) scale of the analyzer was calibrated to produce  $<50\text{ meV}$  deviations of the three standard peaks from their standard values. The aliphatic C 1s peak was observed at 284.6 eV. High-resolution elemental XPS data in C 2p, S 2p, Mg 2p, and Zn 2p regions were acquired with the analyzer pass energy set to 20 eV (corresponding to energy resolution of 0.36 eV) and the step size set to 0.1 eV. The Advantage software package (Thermo Fisher Scientific) was used to fit the elemental spectra based on the calibrated analyzer transmission functions, Scofield sensitivity factors, and effective attenuation lengths for photoelectrons from the standard TPP-2M formalism.

**3.2.2. Electrochemical characterization.** Electrochemical characterization of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_{2:10}\text{F}$  electro-catalysts was performed in a three electrode configuration at  $40^\circ\text{C}$  (maintained using a Fisher Scientific 910 Isotemp refrigerator circulator) on a VersaSTAT 3 (Princeton Applied Research) electrochemical workstation. 1 N sulfuric acid ( $\text{H}_2\text{SO}_4$ ) was used as the electrolyte solution and also, as a proton source for OER. Prior to electrochemical testing, oxygen from the electrolyte solution was expelled by purging the electrolyte solution with ultra-high pure (UHP) argon gas (Matheson) for  $\sim 15\text{ min}$ .<sup>40,41</sup> The thin film electrodes of the various electro-catalyst materials were used as the working electrode, Pt wire (Alfa Aesar, 0.25 mm thick, 99.95%) was used as the counter electrode and mercury/mercurous sulfate ( $\text{Hg}/\text{Hg}_2\text{SO}_4$ ) electrode (XR-200, Hach) having a potential of +0.65 V with respect to normal hydrogen electrode (NHE) was used as the reference electrode. All the potential values reported in this study are determined with respect to reversible hydrogen electrode (RHE), calculated from the formula:<sup>6,42</sup>

$$E_{\text{RHE}} = E_{\text{Hg}/\text{Hg}_2\text{SO}_4} + E_{\text{Hg}/\text{Hg}_2\text{SO}_4}^0 + 0.059\text{pH}.$$

Where,  $E_{\text{RHE}}$  is the potential *versus* RHE.  $E_{\text{Hg}/\text{Hg}_2\text{SO}_4}$  is the potential measured against the  $\text{Hg}/\text{Hg}_2\text{SO}_4$  reference electrode.  $E_{\text{Hg}/\text{Hg}_2\text{SO}_4}^0$  is the standard electrode potential of  $\text{Hg}/\text{Hg}_2\text{SO}_4$  reference electrode (+0.65 V *vs.* NHE).

**Electrochemical impedance spectroscopy (EIS):** The EIS was conducted to determine the solution resistance ( $R_s$ ), the electrode resistance ( $R_e$ ), the ohmic resistance ( $R_\Omega$ ) ( $R_\Omega = R_s + R_e$ ) and the charge transfer resistance ( $R_{ct}$ ) of the synthesized electro-catalyst materials.<sup>7,43</sup> The ohmic resistance ( $R_\Omega$ ) obtained from the EIS was further utilized for  $iR_\Omega$  ( $iR_s + iR_e$ ) correction<sup>7,43</sup> in the polarization curves of the electro-catalysts. The EIS was performed in the frequency range of 100 mHz to 100 kHz (amplitude = 10 mV) using the electrochemical workstation (Versa STAT 3, Princeton Applied Research) in 1 N  $\text{H}_2\text{SO}_4$  electrolyte solution at  $40^\circ\text{C}$ , at the constant applied potential of  $\sim 1.45\text{ V}$  (*vs.* RHE,  $iR_\Omega$  corrected) using a total loading of  $0.3\text{ mg cm}^{-2}$  for  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  ( $x = 0.3$  and  $1$ ) and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_{2:10}\text{F}$  ( $x = 0.2, 0.3, 0.4$ ). Impedance data for OER has been modeled by using the ZView software from Scribner Associates employing





the  $R_s(R_e Q_1)(R_{ct} Q_{dl})$  equivalent circuit model. In the present circuit model (similar to that of used in earlier reports<sup>25,29</sup>)  $R_s$  is in series with the parallel combination of the  $R_e$  and  $Q_1$  and further in series with the parallel combination of the  $R_{ct}$  and  $Q_{dl}$ . The components of this model are given as below:<sup>7,43</sup>

$R_s$  = solution resistance faced at high frequency due to charge transfer in the electrolyte solution.

$R_e$  = electrode resistance for electron transfer from the electrode to current collector (Ti foil).

$R_{ct}$  = charge transfer resistance (*i.e.*, polarization resistance).

$Q_1$  = constant phase element.

$Q_{dl}$  = contribution from both double layer capacitance and pseudocapacitance.

**Linear scan polarization:** The electrochemical activity of the electro-catalysts for OER was determined by conducting linear scan polarization in 1 N  $H_2SO_4$  electrolyte solution employing a scan rate of  $10\text{ mV s}^{-1}$  at  $40^\circ\text{C}$ . Polarization curves of different electro-catalysts were  $iR_\Omega$  corrected ( $R_\Omega$ , the ohmic resistance was determined from electrochemical impedance spectroscopy analysis). The current density at  $\sim 1.45\text{ V}$  (vs. RHE, which is the typical potential used for assessing the electrochemical activity of the electro-catalyst for OER<sup>44</sup>) in  $iR_\Omega$  corrected polarization curves was used for comparison of the electrochemical performance of the different electro-catalyst materials. The Tafel plot after  $iR_\Omega$  correction given by the equation  $\eta = a + b \log i$  (plot of overpotential  $\eta$  vs.  $\log$  current,  $\log i$ ) was used to determine the Tafel slope ( $b$ ), which was further used to study the reaction kinetics for all the synthesized electro-catalysts.

**Electrochemical stability test:** The electrochemical stability of  $(Mn_{1-x}Ir_x)O_2:10F$  electro-catalyst for possible long term operation in an electrolyzer was studied by conducting chronoamperometry (CA) test (current vs. time), wherein, the electrode was maintained for 24 h in the electrolyte solution of 1 N  $H_2SO_4$  at  $40^\circ\text{C}$  under a constant potential of  $\sim 1.45\text{ V}$  (vs. RHE,  $iR_\Omega$  corrected). For comparison, the CA test was also conducted for the in-house synthesized  $IrO_2$  electro-catalyst used as the control.

## 4. Results and discussion

### 4.1. Computational study to predict the high electrochemical activity of $(Mn_{1-x}Ir_x)O_2$ and $(Mn_{1-x}Ir_x)O_2:10F$

In the present study, we have continued to adopt the concept proposed by J. K. Nørskov and his group<sup>45,46</sup> and accordingly, we have used it for qualitative evaluation of the electrochemical activity of  $(Mn, Ir)O_2$  and  $(Mn, Ir)O_2:10F$ . The concept shows the existence of a simple descriptor for determining the surface catalytic activity of the two electro-catalyst systems. This descriptor has been defined as a gravity center of the transition metal d-band  $\epsilon_d$  usually located in the vicinity of the Fermi level. An optimal position of the d-band center thus, provides an optimal interaction between the catalytic surface and various species participating in the catalytic reactions predominantly occurring on the surface leading to the expected maximum catalytic activity. Thus, such an interaction should be considered optimal allowing the reactants and products to both adsorb at the surface and desorb most efficiently. Hence, an

adjustment of the d-band center position with respect to the Fermi level may likely play a critical role in designing the novel highly active and electrochemically stable electro-catalysts discussed herein. As mentioned earlier in the present study, the electronic structure of the stable surfaces for all the electro-catalysts have been calculated and the positions of the corresponding d-band centers have been obtained as a first moment

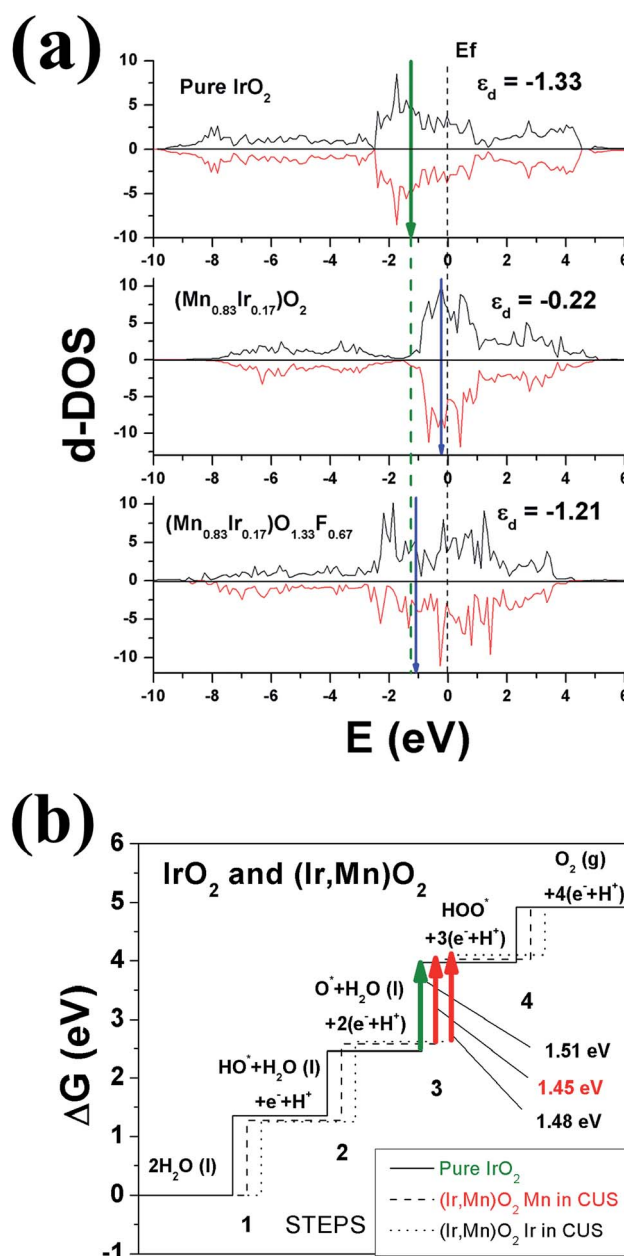


Fig. 2 (a) Projected d-band density of electronic states calculated for pure  $IrO_2$ ,  $(Mn_{0.83}Ir_{0.17})O_2$ , and  $(Mn_{0.83}Ir_{0.17})O_{1.33}F_{0.67}$ . Fermi level is set to zero, a vertical dashed line represents d-band centers for pure  $IrO_2$ , while arrows denote corresponding d-band centers for  $(Mn_{0.83}Ir_{0.17})O_2$ , and  $(Mn_{0.83}Ir_{0.17})O_{1.33}F_{0.67}$ . (b) Free energies of the intermediate reactions for pure  $IrO_2$  and  $(Mn_{0.83}Ir_{0.17})O_2$  with two different Mn configurations.



of  $n_d(E)$ :  $\varepsilon_d = \int n_d(E)E dE / \int n_d(E) dE$ , where  $n_d(E)$  is the projected d-band density of states of the corresponding materials.

Fig. 2a thus accordingly shows the projected d-band densities of states together with the corresponding centers of these zones marked with vertical arrows on the graphs for pure  $\text{IrO}_2$ , Ir substituted  $\text{MnO}_2$ ,  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_2$ , as well as F doped Mn substituted  $\text{MnO}_2$ ,  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_{1.33}\text{F}_{0.67}$ . Since,  $\text{IrO}_2$  is a recognized OER electro-catalyst, the d-band positions for  $\text{IrO}_2$ , marked with a dashed vertical line throughout the whole graph, could serve as a reference point or a benchmark attesting to the optimal catalytic activity for the designed electro-catalysts. Our calculations have showed that  $\text{IrO}_2$  is characterized by the d-band centers located at  $\sim(-1.33 \text{ eV})$ . The closer the corresponding d-band center of the solid solution electro-catalyst studied herein to  $\text{IrO}_2$  d-band center position, it can be considered as the likely indication of the substituted solid solution exhibiting electrochemical activity matching that of  $\text{IrO}_2$  and thus, an indicator of expected improvement in overall catalytic activity of the electro-catalyst. Such an approach can thus help in understanding the effect of fluorine on the electro-catalytic activity of  $(\text{Mn},\text{Ir})\text{O}_2\text{:F}$ .

It can be seen from Fig. 2a that the projected density of d-electronic states for  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_2$  can be presented as a sum of Mn 3d and Ir 5d electrons characterized by the d-band center position located at  $-0.22 \text{ eV}$  vs. the Fermi level. However, an introduction of F into  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_2$  changes the overall electronic structure in such a way that formation of the hybridized F 2p–Mn 3d and F 2p–Ir 5d electronic states shifts the d-band center downward to  $-1.21 \text{ eV}$  very close to that of  $\text{IrO}_2$  ( $-1.33 \text{ eV}$ ). Of course, it should be noted that this approach is very qualitative and does not provide exact chemical compositions demonstrating the optimal catalytic activity of the material. Nevertheless, it provides a basic understanding of the effect of F doping and its likely influence on the electro-catalytic activity of  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_2\text{:F}$ . An identical effect of F on the electronic structure has also been seen earlier and reported by us in the study of  $(\text{Sn},\text{Ir})\text{O}_2\text{:F}$  electro-catalysts.<sup>29</sup> Similar to  $(\text{Mn}_{0.83}\text{Ir}_{0.17})\text{O}_2\text{:F}$ , formation of F 2p–Ir 5d hybridized electronic states shifts the d-band center of  $(\text{Ir},\text{Sn})\text{O}_2\text{:F}$  down towards the optimal position, and thus, improves the overall catalytic activity of  $(\text{Ir},\text{Sn})\text{O}_2\text{:F}$  with

substantial reduction of  $\sim 70\text{--}80\%$  in the noble metal content.<sup>29</sup> The theoretical calculations were also validated experimentally and reported by us in the corresponding reports.<sup>29</sup>

Although the d-band center concept can provide a qualitative explanation of the basic origins of high catalytic activity of  $(\text{Mn},\text{Ir})\text{O}_2\text{:F}$ , it does not provide insights to elucidate effect of Mn introduction into the  $\text{IrO}_2$  lattice on the overpotential of the  $(\text{Ir},\text{Mn})\text{O}_2$  solid solution oxide. To study this effect, it is imperative to consider all the four elementary steps involved in the oxygen evolution reaction discussed in Fig. 2b and also outlined in the earlier section (eqn (1)).

Fig. 2b demonstrates the free energies of all the four elementary steps of OER calculated for pure  $\text{IrO}_2$  and the two different Ir–Mn atomic configurations discussed above and illustrated in Fig. 1. Also, some of the data used for plotting these graphs are collected in the Table 1. One can see that the most energetically challenging step for all the three materials is step 3, resulting in the formation of the hydroperoxide  $\text{HOO}^*$  from the second water molecule. This step determines the major overpotential that is required to be overcome to meet the four steps outlined in Fig. 2b, leading to the evolution of oxygen. For pure  $\text{IrO}_2$  the overpotential is  $1.51\text{--}1.23 = 0.28 \text{ V}$ , while for  $(\text{Ir},\text{Mn})\text{O}_2$  it is  $0.22 \text{ V}$  and  $0.25 \text{ V}$  for the two different positions of Mn in the unit cell, thus indicating that the presence of Mn is critical to lower the overpotential for the electrolysis reaction in comparison with pure  $\text{IrO}_2$ . Such a decrease in the energy difference for the third elementary step in the case of Mn-doped  $\text{IrO}_2$  is due to the stronger interaction between the adsorbed oxygen  $\text{O}^*$  and the surface resulting in a decrease in the total energy of the system in comparison with pure  $\text{IrO}_2$ ; making it more feasible for the species to adsorb at the surface and thus, resulting in a reduction in the overpotential of the overall OER for  $(\text{Mn},\text{Ir})\text{O}_2$  oxide. From Table 1, it can also be seen that the  $\Delta G$  values for all the intermediates in the case of both the Mn-configurations of  $(\text{Mn},\text{Ir})\text{O}_2$  are consistently lower than those for pure  $\text{IrO}_2$  indicating a stronger binding of the intermediates to the Mn-containing surface. Such an enhancement in adsorption is indirectly confirmed by the d-band calculations discussed above, when the introduction of Mn shifts the resulted d-band center upward towards the Fermi level, thus making the effective interactions between the intermediate

**Table 1** Computational data obtained from the present study. ( $\Delta ZPE - T\Delta S$  data taken from previously published study<sup>33</sup>)

Configuration	$E_{\text{tot slab}}$ (eV) for pure $\text{IrO}_2$	$\Delta ZPE - T\Delta S$ (eV)	$\Delta G$ (eV)		
			Pure $\text{IrO}_2$	Mn at the center	Mn at the side
Vac + $2\text{H}_2\text{O}$	−259.47	—	0	0	0
$\text{HO}^* + \text{H}_2\text{O} + \frac{1}{2}\text{H}_2$	−279.21	0.35	1.36	1.16	1.17
$\text{O}^* + \text{H}_2\text{O} + \text{H}_2$	−270.31	0.05	2.46	2.31	2.28
$\text{HOO}^* + \frac{3}{2}\text{H}_2$	−289.85	0.40	3.97	3.75	3.66
Vac + $\text{O}_2 + 2\text{H}_2$	−259.47	—	4.92	4.92	4.92
$\Delta G$ of step 3 (eV), (over-potential in V)			1.51, (0.28)	1.45, (0.22)	1.48, (0.25)



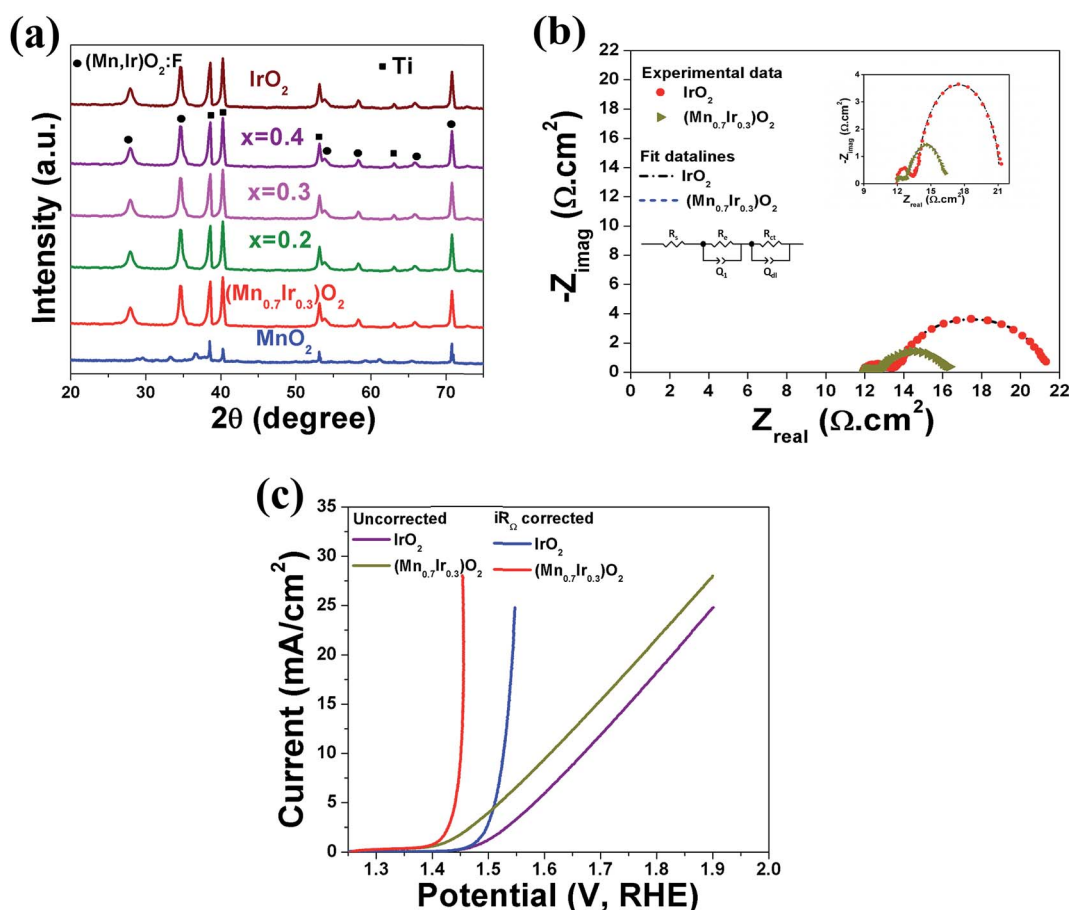
species and the catalytic surface stronger in comparison to pure  $\text{IrO}_2$ . The more close the d-band center to the Fermi level of the material, the larger is the overlap between the d-orbitals of the surface and oxygen s,p-orbitals in  $\text{O}^*$ ,  $\text{HO}^*$ , and  $\text{HOO}^*$  intermediate species leading to a stronger overall interaction between the surface and the adsorbed species. These results clearly demonstrate that the coordinatively unsaturated sites (CUS) on the oxidized surface could serve as the main active sites for water oxidation regardless of the local distribution of the Mn-ions with the difference in the over-potential of 0.03 V for the different surface configurations (see Fig. 2b).

As demonstrated in various previous studies, introduction of F into the different solid solutions of  $\text{IrO}_2$  with  $\text{SnO}_2$  and/or  $\text{NbO}_2$  oxides did not result in decreasing the overpotential for OER.<sup>29,30</sup> The onset potential remained the same for all the materials  $\sim 1.43$  V (the corresponding overpotential was  $\sim 0.20$  V), while the kinetic properties (e.g. exchange current density) strongly depended on the F-content of the material.<sup>29,30</sup> In light of this, computational investigation into the effect of F on the overpotential of  $(\text{Mn},\text{Ir})\text{O}_2$  oxide was therefore deemed redundant and hence, has not been conducted in the current study.

Thus, the present theoretical study has demonstrated different effects of introduction of Mn and F into the  $\text{IrO}_2$  lattice: an introduction of Mn makes interactions between the surface and intermediate species more strong thus decreasing the overpotential and increasing the propensity for the overall OER, while F-doping modifies the electronic structure of the material in a such way, that the d-band center moves towards the ideal position corresponding to the optimal electro-catalytic activity. Also, fluorine introduces more free electrons into the system resulting in improving the overall electronic conductivity of  $(\text{Mn},\text{Ir})\text{O}_2:\text{F}$  and, in turn, the overall catalytic activity. These theoretical findings correlate very well with experimental observations discussed in the present study.

## 4.2. Experimental characterization of $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}$ ( $x = 0, 0.3, 1$ ) electro-catalyst

**4.2.1. Structural characterization of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  ( $x = 0, 0.3, 1$ ).** The XRD patterns of pure  $\text{IrO}_2$  ( $x = 1$ ) and pure  $\text{MnO}_2$  ( $x = 0$ ) electro-catalyst produced by the thermal decomposition of  $\text{IrCl}_4$  and  $\text{MnCl}_2$  solutions (deposited on Ti foil) respectively



**Fig. 3** (a) The XRD patterns of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  ( $x = 0.3$ ) and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2, 0.3$  and  $0.4$ ), electro-catalysts coated on Ti foil, (b) EIS spectra of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  and pure  $\text{IrO}_2$  (total loading of  $0.3 \text{ mg cm}^{-2}$ ) performed at  $\sim 1.45$  V (vs. RHE,  $iR_\Omega$  corrected) in  $1 \text{ N H}_2\text{SO}_4$  at  $40^\circ\text{C}$  in the frequency range of  $100 \text{ mHz}$  to  $100 \text{ kHz}$  (inset: EIS equivalent circuit and magnified view of EIS), (c) the polarization curve of pure  $\text{IrO}_2$  and  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  electro-catalyst using total loading of  $0.3 \text{ mg cm}^{-2}$  obtained in  $1 \text{ N H}_2\text{SO}_4$  solution at  $40^\circ\text{C}$  with scan rate of  $10 \text{ mV s}^{-1}$  before and after  $iR_\Omega$  correction.



**Table 2** The lattice parameters and molar volume of  $\text{MnO}_2$ ,  $\text{IrO}_2$ ,  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  ( $x = 0.3$ ) and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$  ( $x = 0.2, 0.3, 0.4$ )

Composition	Lattice parameter ( $\text{\AA}$ )		Molar volume ( $\text{cm}^3 \text{mol}^{-1}$ )
	$a = b$	$c$	
$\text{MnO}_2$	$9.88 \pm 0.07$	$2.82 \pm 0.02$	20.72
$(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$	$4.64 \pm 0.04$	$3.07 \pm 0.03$	19.77
$(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2 \cdot 10\text{F}$	$4.63 \pm 0.06$	$3.06 \pm 0.04$	19.75
$(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2 \cdot 10\text{F}$	$4.64 \pm 0.06$	$3.08 \pm 0.04$	19.96
$(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2 \cdot 10\text{F}$	$4.65 \pm 0.06$	$3.06 \pm 0.04$	19.92
$\text{IrO}_2$	$4.63 \pm 0.06$	$3.06 \pm 0.04$	19.75

at  $400^\circ\text{C}$  for 4 h in air are shown in Fig. 3a. Both  $\text{IrO}_2$  and  $\text{MnO}_2$  exhibit tetragonal structure similar to earlier reports.<sup>24,47,48</sup> The calculated lattice parameters of pure  $\text{IrO}_2$  are  $a = b = 4.63 \pm 0.06 \text{ \AA}$  and  $c = 3.06 \pm 0.04 \text{ \AA}$ , with molar volume of  $19.75 \text{ cm}^3 \text{mol}^{-1}$  which is consistent with the reported literature values.<sup>29,49</sup> Similarly, the calculated lattice parameters of  $\text{MnO}_2$  are  $a = b = 9.88 \pm 0.07 \text{ \AA}$  and  $c = 2.82 \pm 0.02 \text{ \AA}$  with molar volume of  $\sim 20.72 \text{ cm}^3 \text{mol}^{-1}$  is similar to the earlier reported results.<sup>50–52</sup> On the other hand, the XRD patterns of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  electro-catalyst, shown in Fig. 3a, represent tetragonal structure with a lattice parameter of  $a = b = 4.64 \pm 0.04 \text{ \AA}$  and  $c = 3.07 \pm 0.03 \text{ \AA}$ , with a molar volume of  $\sim 19.77 \text{ cm}^3 \text{mol}^{-1}$  (Table 2). The XRD patterns of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  electro-catalyst show no other peaks of Ir or Mn based compounds thus confirming the formation of homogeneous single phase solid solution of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  ( $x = 0.3$ ).

**4.2.2. Electrochemical characterization of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  ( $x = 0.3, 1$ ).** The EIS of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  along with pure  $\text{IrO}_2$  ( $x = 1$ ), measured at  $\sim 1.45 \text{ V}$  ( $iR_\Omega$  corrected) and performed in the electrolyte solution of  $1 \text{ N H}_2\text{SO}_4$  at  $40^\circ\text{C}$ , is shown in Fig. 3b, to determine solution resistance ( $R_s$ ), electrode resistance ( $R_e$ ) and charge transfer resistance ( $R_{ct}$ ). As discussed in the Experimental section, equivalence circuit model  $R_s(R_e Q_1)(R_{ct} Q_{dl})$  has been used in which  $R_s$  is in series with the parallel combination of the  $R_e$  and  $Q_1$  and further in series with the parallel combination of the  $R_{ct}$  and  $Q_{dl}$  (shown in the inset of Fig. 3b). It is interesting to note that the charge transfer resistance ( $R_{ct}$ ), determined from the diameter of the semi-circle in the low frequency region of the EIS plot (Fig. 3b and Table 3), of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  ( $R_{ct} \sim 3.6 \Omega \text{ cm}^2$ ) is lower than pure  $\text{IrO}_2$  ( $R_{ct} \sim 8.5 \Omega \text{ cm}^2$  comparable with our earlier report).<sup>53</sup> This result clearly

suggests that the activation polarization of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  is much lower than pure  $\text{IrO}_2$  for OER, and as a result,  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  is expected to have better reaction kinetics and electrochemical activity than pure  $\text{IrO}_2$ .<sup>9,48</sup>

In order to analyze the electrochemical activity of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  electro-catalyst, linear scan polarization has also been performed in the electrolyte solution of  $1 \text{ N H}_2\text{SO}_4$  at  $40^\circ\text{C}$  with the scan rate of  $10 \text{ mV s}^{-1}$ . The electrolyte solution resistance ( $R_s$ ), electrode resistance ( $R_e$ ) and bubble resistance ( $R_{bub}$ ) are mainly responsible for the linear nature of polarization curve and non-linearity in the Tafel plot.<sup>54,55</sup> Thus, to study the inherent electrochemical activity of the electro-catalysts, ohmic resistance ( $R_\Omega$ ) correction ( $iR_\Omega = iR_s + iR_e$ )<sup>6,7,43,56</sup> has been performed in the polarization curves as well as in Tafel plots of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  and  $\text{IrO}_2$ . Fig. 3c shows the uncorrected and  $iR_\Omega$  corrected polarization curves of pure  $\text{IrO}_2$  and  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  electro-catalyst. The electrochemical activity of pure  $\text{MnO}_2$  has not been performed due to the inherent instability of  $\text{MnO}_2$  in the acidic electrolyte solution.<sup>57–59</sup> As shown in Fig. 3c and Table 3, the onset potential of OER for  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  is  $\sim 1.35 \text{ V}$  (vs. RHE) with  $\sim 120 \text{ mV}$  overpotential (w.r.t. the standard potential for OER *i.e.*  $1.23 \text{ V}$  vs. RHE) which is much lower than that of  $\text{IrO}_2$  which shows an onset potential of  $\sim 1.43 \text{ V}$  (vs. RHE) with  $\sim 200 \text{ mV}$  overpotential similar to earlier reports.<sup>29,34,60</sup> The significant decrease in the overpotential, lowest reported to date, measured for  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  electro-catalyst is in good agreement with the results of the theoretical calculation discussed in the earlier section and shown in (Fig. 2a and b, Table 1). The current density obtained at  $\sim 1.45 \text{ V}$  for  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  (total loading =  $0.3 \text{ mg cm}^{-2}$ ) is  $\sim 9.09 \text{ mA cm}^{-2}$  which is  $\sim 12$  fold higher than that of  $\text{IrO}_2$  ( $0.75 \text{ mA cm}^{-2}$  at  $1.45 \text{ V}$  with an identical loading =  $0.3 \text{ mg cm}^{-2}$ ) (Table 3). The excellent electrochemical performance (*i.e.* low over-potential and higher current density) of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  is due to the improved reaction kinetics (*i.e.* low  $R_{ct}$  as seen earlier in Fig. 3b and Table 3) for OER of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  than that of  $\text{IrO}_2$  as predicted by the theoretical calculations (Fig. 2a and b, Table 1).

In order to further improve the reaction kinetics of  $(\text{Mn},\text{Ir})\text{O}_2$  electro-catalyst,  $10 \text{ wt\% F}$  has been introduced as a dopant in the  $(\text{Mn},\text{Ir})\text{O}_2$  electro-catalyst as proposed from the theoretical studies discussed earlier (Fig. 2a and b). In addition, a higher ( $x = 0.4$ ) and lower ( $x = 0.2$ )  $\text{IrO}_2$  content solid solution electro-

**Table 3** Results of electrochemical characterization for OER of  $\text{IrO}_2$ ,  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2$  ( $x = 0.3$ ) and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) electro-catalysts, obtained in  $1 \text{ N H}_2\text{SO}_4$  electrolyte solution at  $40^\circ\text{C}$ 

Composition	Onset potential (V vs. RHE)	Current density at $\sim 1.45 \text{ V}$ (vs. RHE) ( $\text{mA cm}^{-2}$ )	$R_s$ ( $\Omega \text{ cm}^2$ )	$R_e$ ( $\Omega \text{ cm}^2$ )	$R_\Omega$ ( $\Omega \text{ cm}^2$ )	$R_{ct}$ ( $\Omega \text{ cm}^2$ )	Tafel slope ( $\text{mV dec}^{-1}$ )
$(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$	$\sim 1.35$	$\sim 9.09$	$\sim 11.73$	$\sim 1.85$	$\sim 13.58$	$\sim 3.6$	$\sim 67$
$(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2 \cdot 10\text{F}$	$\sim 1.35$	$\sim 5.45$	$\sim 11.72$	$\sim 2.4$	$\sim 14.12$	$\sim 4$	$\sim 68$
$(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2 \cdot 10\text{F}$	$\sim 1.35$	$\sim 10.65$	$\sim 11.68$	$\sim 1.78$	$\sim 13.46$	$\sim 2.6$	$\sim 65$
$(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2 \cdot 10\text{F}$	$\sim 1.35$	$\sim 11.03$	$\sim 11.71$	$\sim 1.7$	$\sim 13.41$	$\sim 2.1$	$\sim 62$
$\text{IrO}_2$	$\sim 1.43$	$\sim 0.75$	$\sim 11.73$	$\sim 2.5$	$\sim 14.23$	$\sim 8.5$	$\sim 71$





catalysts  $[(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}]$  ( $x = 0.2, 0.3, 0.4$ ) has also been explored to identify the nominal composition with an excellent electrochemical activity towards OER in PEM based water electrolysis.

#### 4.3. Characterization of $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$ ( $x = 0.2, 0.3, 0.4$ ) electro-catalyst

**4.3.1. Structural characterization of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$  electro-catalysts.** *X-ray diffraction (XRD) analysis:* The XRD patterns of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) electro-catalysts of different compositions, shown in Fig. 3a, reveal the tetragonal structure similar to that of pure  $\text{IrO}_2$  and  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  without any other peaks of Mn or Ir based compounds, suggesting the formation of complete

homogeneous single phase solid solution without any undesired phase separation for the F doped compositions containing varying amounts of Mn. The calculated lattice parameters and molar volume of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) are quite similar to that of pure  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  as shown in Table 2. The effective crystallite size of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ), calculated using the Scherrer formula from the integral breadth of the Lorentzian contribution determined from peak profile analysis using the single line approximation method after eliminating the instrumental broadening and lattice strain contribution<sup>61</sup> is  $\sim 5$  to 7 nm, indicating the nanocrystalline nature of the solid solution electro-catalyst materials of different compositions.

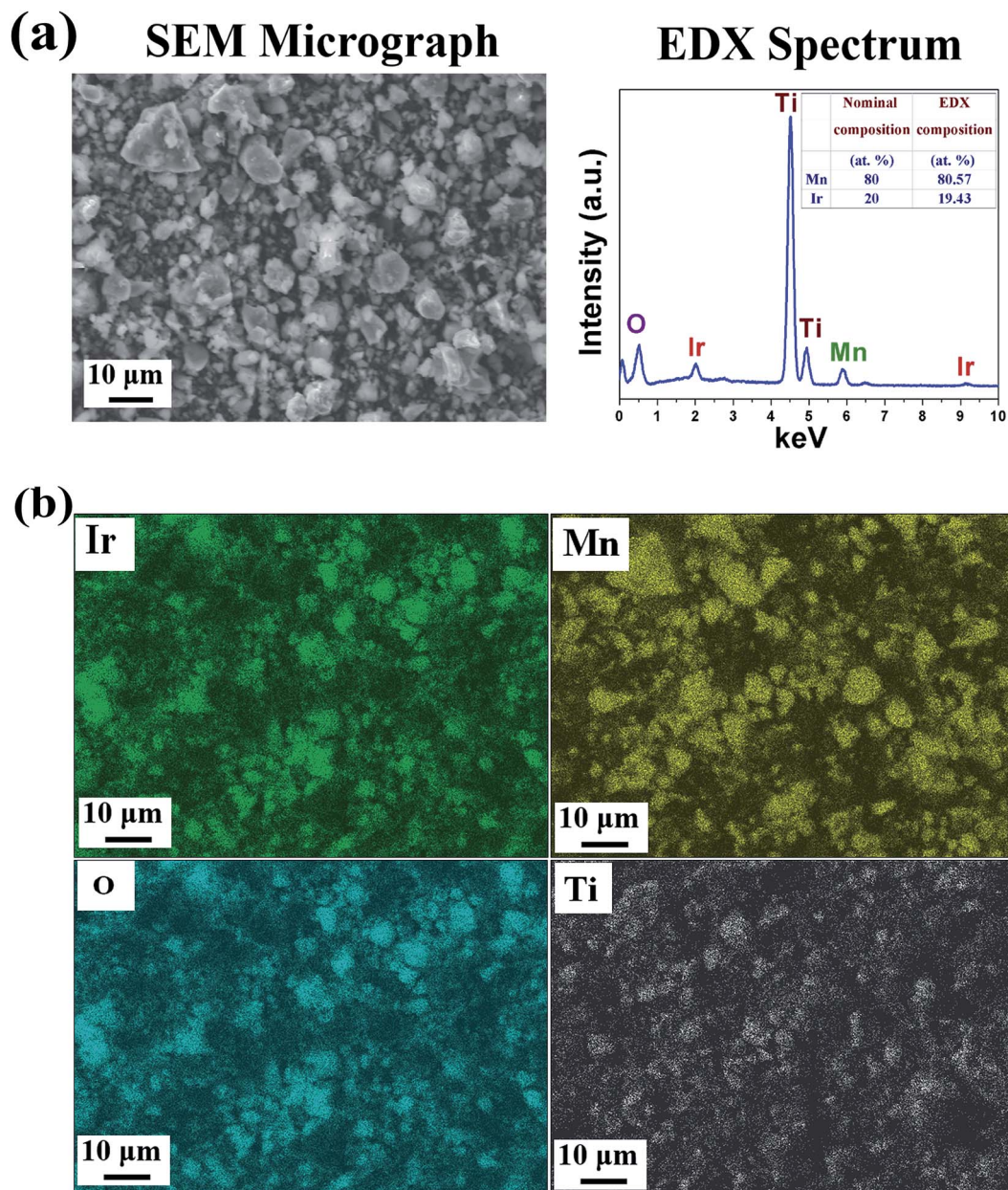


Fig. 4 (a) The SEM micrograph and EDX spectrum, (b) elemental X-ray mapping of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2 \cdot 10\text{F}$  ( $x = 0.2$ ).



**SEM/EDX analysis:** The SEM micrograph combined with the EDX pattern of the representative composition,  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  ( $x = 0.2$ ) shows the presence of Ir, Mn and O (Fig. 4a). The quantitative elemental composition analysis of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  ( $x = 0.2$ ) obtained from EDX shows the measured elemental composition of Ir and Mn close to the nominal composition. The elemental X-ray maps of Ir, Mn and O for  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  ( $x = 0.2$ ) (Fig. 4b) show the homogeneous distribution of elements within the particles indicating absence of any segregation at any specific site.

**X-ray photoelectron spectroscopy (XPS) analysis:** XPS analysis has been performed on  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  electro-catalysts with different Mn content to study the valence states of Ir and Mn. The XPS analysis has been plotted in the Fig. 5a and b for Ir and Mn, respectively. The deconvoluted XPS spectrum of Ir in pure  $\text{IrO}_2$  (Fig. 5a) shows the presence of Ir 4f doublet centered at binding energy of  $\sim 61.7$  eV and  $\sim 64.6$  eV (similar to earlier report<sup>62</sup>) which corresponds to Ir 4f<sub>7/2</sub> and Ir 4f<sub>5/2</sub> respectively,

consistent with that of pure  $\text{IrO}_2$ .<sup>48</sup> Fig. 5b shows the XPS spectra of Mn 2p doublet for  $\text{MnO}_2$  centered at  $\sim 641.6$  eV and  $\sim 653.8$  eV (similar to earlier report<sup>63–65</sup>) for Mn 2p<sub>3/2</sub> and Mn 2p<sub>1/2</sub>, respectively, which corresponds to that of pure  $\text{MnO}_2$ .<sup>63,66</sup> As can be seen in Fig. 5b, deconvoluted XPS spectra of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  (for  $x = 0.2, 0.3, 0.4$ ) exhibit an additional peak centered near  $\sim 645.5$  eV, similar to the previous studies, which may be a shake-up peak and can be referred as a satellite peak.<sup>63,64</sup> However, the positive shift in Ir 4f doublet and Mn 2p doublet positions of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  after incorporation of F in the solid solution lattice as well as with increase in Ir content (Fig. 5a and b) suggests modification of the electronic structure of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  for the different compositions upon formation of solid solution and due to the presence of fluorine in the solid solution lattice leading to stronger binding due to the higher electronegativity of fluorine.<sup>29,67</sup> The presence of F in  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  of different compositions could not be unequivocally ascertained by the XPS analysis similar to our

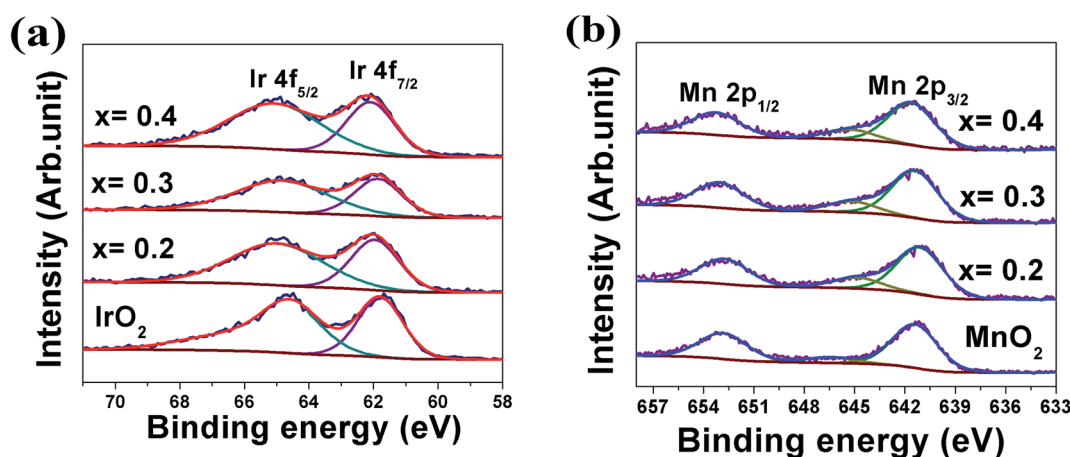


Fig. 5 The XPS and corresponding deconvoluted spectra of (a) Ir 4f<sub>7/2</sub> and 4f<sub>5/2</sub> doublet, (b) Mn 2p<sub>1/2</sub> and Mn 2p<sub>3/2</sub> doublet of pure  $\text{IrO}_2$  and pure  $\text{MnO}_2$  and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  ( $x = 0.2, 0.3$  and  $0.4$ ) electro-catalysts.

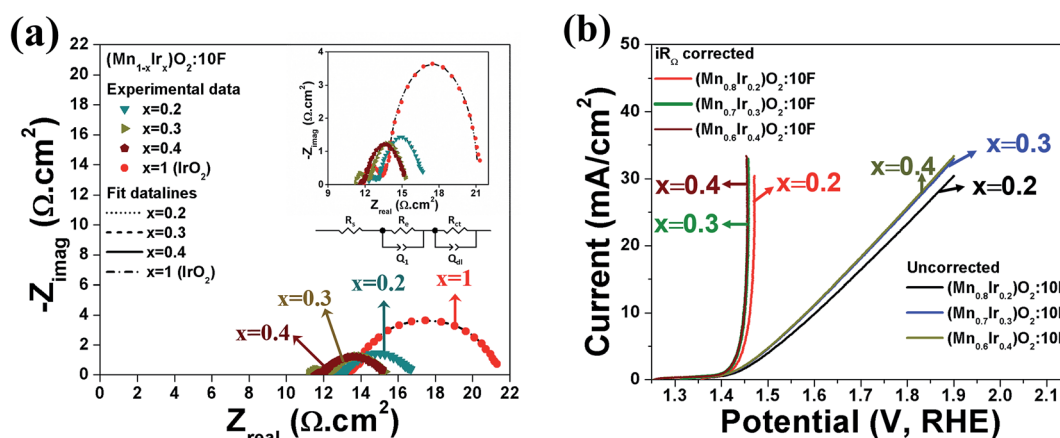


Fig. 6 (a) EIS spectra of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  for ( $x = 0.2, 0.3$  and  $0.4$ ) and pure  $\text{IrO}_2$  (total loading of  $0.3 \text{ mg cm}^{-2}$ ) performed at  $\sim 1.45 \text{ V}$  (vs. RHE,  $iR_\Omega$  corrected) in  $1 \text{ N H}_2\text{SO}_4$  at  $40^\circ \text{C}$  in the frequency range of  $100 \text{ mHz}$  to  $100 \text{ kHz}$  (inset: EIS equivalent circuit and magnified view of EIS), (b) the polarization curve of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\cdot 10\text{F}$  for ( $x = 0.2, 0.3$  and  $0.4$ ) (total loading of  $0.3 \text{ mg cm}^{-2}$ ) obtained in  $1 \text{ N H}_2\text{SO}_4$  solution at  $40^\circ \text{C}$  with scan rate of  $10 \text{ mV s}^{-1}$  before and after  $iR_\Omega$  correction.



earlier publications on Sn substituted  $\text{IrO}_2$ ,<sup>29,30</sup> probably due to the low concentration of F actually retained within the lattice. Nevertheless, F incorporation has indeed beneficial effect on the electrochemical activity (as witnessed in the polarization curve, Fig. 6b, discussed later) of  $(\text{Mn},\text{Ir})\text{O}_2\text{:F}$  solid solution most likely due to the improved electronic conductivity.<sup>29</sup>

**4.3.2. Electrochemical characterization of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  electro-catalysts.** The electrochemical performance of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  ( $x = 0.2, 0.3, 0.4$ ) has been studied by conducting EIS to determine  $R_s$ ,  $R_e$  and  $R_{ct}$  (Fig. 6a) using  $R_s(R_e - Q_1)(R_{ct}Q_{dl})$  as the equivalent circuit model (inset in Fig. 6a), as discussed in the Experimental section. It is noteworthy that the  $R_{ct}$ , determined from the diameter of the semi-circle in the low frequency region of the EIS plot (Fig. 6a and Table 3), of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2\text{:10F}$  ( $R_{ct} \sim 2.6 \Omega \text{ cm}^2$ ) and  $(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2\text{:10F}$  ( $R_{ct} \sim 2.1 \Omega \text{ cm}^2$ ) is lower than  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  ( $R_{ct} \sim 3.6 \Omega \text{ cm}^2$ ) and pure  $\text{IrO}_2$  ( $\sim 8.5 \Omega \text{ cm}^2$ ) which clearly suggests that F doping has a significant influence on the kinetics of the water splitting reaction as also predicted by the theoretical analysis (Fig. 2a and b, Table 1). These results thus indicate that the activation polarization of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  for  $x = 0.3$  and  $x = 0.4$  is significantly lower than  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  and pure  $\text{IrO}_2$  for OER. On the other hand, the  $R_{ct}$  of  $(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2\text{:10F}$  ( $R_{ct} \sim 4 \Omega \text{ cm}^2$ ) is comparable with  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  ( $R_{ct} \sim 3.6 \Omega \text{ cm}^2$ ), and much lower than pure  $\text{IrO}_2$ . In addition, it has been noticed that the  $R_e$  decreases with increase in Ir content for  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  and  $x$

$= 0.4$  shows the lowest  $R_e$  of  $\sim 1.7 \Omega \text{ cm}^2$ . The decrease in  $R_e$  with increase in Ir content for  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  can be due to an improved electronic conductivity of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  with increase in Ir content. Furthermore, the ohmic resistance, ( $R_\Omega = R_s + R_e$ ) as shown in Table 3 also decreases with increase in Ir content.

Based on the above results, it is anticipated that  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  ( $x = 0.3$  and  $0.4$ ) will show enhanced reaction kinetics as well as electrochemical activity than  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  and pure  $\text{IrO}_2$ . The uncorrected and  $iR_\Omega$  corrected linear scan polarization curves of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  ( $x = 0.2, 0.3, 0.4$ ) obtained in the electrolyte solution of 1 N  $\text{H}_2\text{SO}_4$  at  $40^\circ\text{C}$  with the scan rate of  $10 \text{ mV s}^{-1}$  are shown in Fig. 6b. The onset potential of OER for  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2\text{:10F}$  ( $x = 0.2, 0.3, 0.4$ ) is  $\sim 1.35 \text{ V}$  (vs. RHE) which is comparable to  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$  with  $\sim 120 \text{ mV}$  overpotential and lower than  $\text{IrO}_2$  which shows  $\sim 200 \text{ mV}$  overpotential (Fig. 3c and Table 3). The current density obtained at  $\sim 1.45 \text{ V}$  (vs. RHE) for  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2\text{:10F}$ ,  $(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2\text{:10F}$  is  $\sim 10.65 \text{ mA cm}^{-2}$  and  $\sim 11.03 \text{ mA cm}^{-2}$  respectively (Table 3), which is  $\sim 14$  and  $\sim 15$  fold higher than that of  $\text{IrO}_2$  ( $0.75 \text{ mA cm}^{-2}$  at  $1.45 \text{ V}$ ), respectively. Although the current density obtained at  $\sim 1.45 \text{ V}$  for  $(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2\text{:10F}$  electro-catalyst (*i.e.*  $\sim 5.45 \text{ mA cm}^{-2}$ ) is lower than that of  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2\text{:10F}$ ,  $(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2\text{:10F}$  and  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2$ ,  $(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2\text{:10F}$  shows a significantly higher current density ( $\sim 7$  fold) than that of pure  $\text{IrO}_2$  observed at  $\sim 1.45 \text{ V}$  with a hallmark 80% reduction in noble metal content

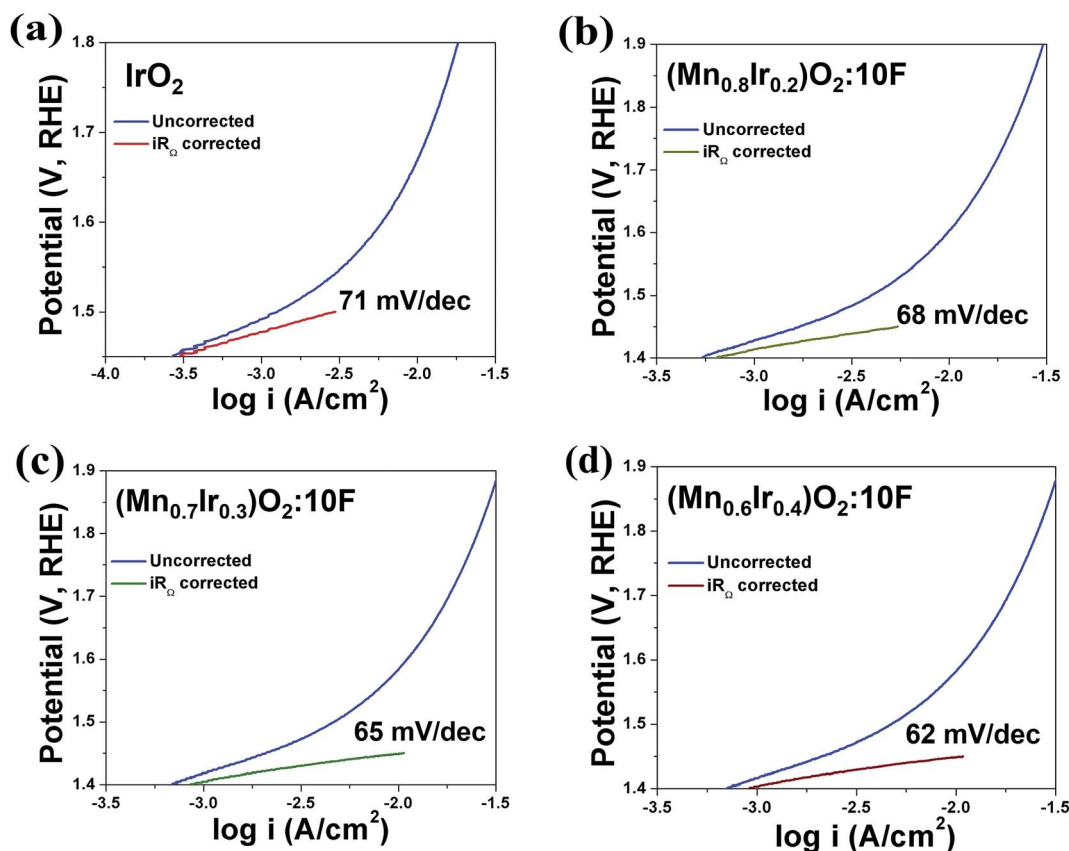


Fig. 7 The Tafel plot of (a)  $\text{IrO}_2$  (b)  $(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2\text{:10F}$  (c)  $(\text{Mn}_{0.7}\text{Ir}_{0.3})\text{O}_2\text{:10F}$  and (d)  $(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2\text{:10F}$ , before and after  $iR_\Omega$  correction.





and even  $\sim 11$  fold higher current density than  $(\text{Mn}_{0.87}\text{Ir}_{0.13})\text{O}_2$  solid solution system reported in a recent publication.<sup>32</sup> The Tafel slope of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) is  $\sim 68 \pm 0.0001 \text{ mV dec}^{-1}$ ,  $\sim 65 \pm 0.0001 \text{ mV dec}^{-1}$  and  $\sim 62 \pm 0.0001 \text{ mV dec}^{-1}$ , respectively (Fig. 7a–d). Thus, the Tafel slope of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  decreases with increase in Ir content with the lowest obtained for  $(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2:10\text{F}$  indicating increase in the reaction kinetics and higher electrochemical activity with the largest value obtained for  $(\text{Mn}_{0.6}\text{Ir}_{0.4})\text{O}_2:10\text{F}$ . In addition, the Tafel slope of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  does reflect the desired two electron pathway for OER in accordance with published reports (Table 3).<sup>13</sup>

**Electrochemical stability/durability test:** It is extremely important for electro-catalyst to exhibit excellent long term electrochemical durability in harsh acidic operating conditions of OER, which will aid in efficient continuous long term operation when implemented in PEM water electrolysis cells. Therefore, to assess the electrochemical stability/durability of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  electro-catalyst, chronoamperometry (CA) test has been performed at the constant applied potential of  $\sim 1.45 \text{ V}$  ( $iR_{\Omega}$  corrected, *i.e.*,  $\sim 1.55 \text{ V}$  in the uncorrected polarization curve) in  $1 \text{ N H}_2\text{SO}_4$  at  $40^\circ \text{C}$ . The CA curve obtained for the higher Mn content electro-catalyst  $(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2:10\text{F}$ , shown in Fig. 8, displays minimal loss in current density, indicating the superior long term electrochemical stability, similar to that of in-house synthesized  $\text{IrO}_2$ . The initial decrease in current density seen in CA curves of both in-house synthesized  $\text{IrO}_2$  and  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2$ ) can possibly be due to dissolution of irregular electro-catalyst coating and/or diffusion controlled reaction, similar to earlier reports.<sup>29,68</sup> Thus, excellent long term electrochemical stability of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2$ ) can possibly be due to good alloying of  $\text{IrO}_2$  and  $\text{MnO}_2$  and beneficial modification in the electronic structure upon formation of F-doped solid solution, resulting in unique active phase exhibiting superior electrochemical stability.

The above results clearly suggest that the incorporation of  $\text{IrO}_2$  in the framework of  $\text{MnO}_2$  along with incorporation of F in

the lattice offers a unique opportunity to tailor the electronic, physical, chemical and electro-catalytic properties of  $(\text{Mn},\text{Ir})\text{O}_2:10\text{F}$ . The formation of a single phase solid solution  $(\text{Mn},\text{Ir})\text{O}_2:10\text{F}$  offers modified electro-catalytic properties due to a change in the d-band center energy leading to change in adsorption strength of the corresponding adsorbed species on the electro-catalyst surface. Additionally, significant decrease in overpotential and improvement in electrochemical performance contributes to efficient OER electro-catalytic activity for PEM water electrolysis. The present study also demonstrates remarkable,  $\sim 60$ – $80\%$  reduction in the noble metal content along with substantial reduction in over-potential for the  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:\text{F}$  solid solution systems indicative of the excellent electrochemical performance. The study thus clearly demonstrates the potential of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:\text{F}$  system as an efficient OER electro-catalysts for PEM water electrolysis. However, it should be noted that the true potential of the electro-catalyst can only be realized when tested in a full PEM based water electrolyzer. Although electrolyzer evaluation of these electro-catalysts is beyond the scope of the current study, it can be mentioned that the present electro-catalyst system displays superior electrochemical response compared to F-doped  $\text{IrO}_2$  when evaluated in a half-cell configuration. Our evaluation of F-doped  $\text{IrO}_2$  in a full PEM electrolyzer was also reported in a previous publication.<sup>69</sup> It is therefore likely, that if the current system were tested in a full PEM based electrolyzer system, the electro-catalyst would also potentially exhibit superior electrochemical response. These studies will nevertheless, be planned in the near future and reported in subsequent publications.

## 5. Conclusions

The present study successfully demonstrates nanostructured solid solution of 10 wt% F doped  $\text{IrO}_2$  and  $\text{MnO}_2$  solid solutions denoted as  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) with thin film architecture coated on Ti foil as potential anode electro-catalysts for OER in PEM based water electrolysis. The corresponding solid solutions  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) with unique electronic/molecular structure showed excellent electrochemical activity with the lowest reported to date, onset potential of  $\sim 1.35 \text{ V}$  (*vs.* RHE) with  $\sim 120 \text{ mV}$  overpotential (*w.r.t*  $1.23 \text{ V}$  *vs.* RHE, which is the standard potential for OER), lower than that of  $\text{IrO}_2$  ( $\sim 1.43 \text{ V}$  *vs.* RHE, *i.e.*  $\sim 200 \text{ mV}$  overpotential). In addition, remarkable  $\sim 7$ ,  $\sim 14$  and  $\sim 15$  fold higher electrochemical activity was obtained for  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) than that of pure  $\text{IrO}_2$ , respectively. Additionally,  $(\text{Mn}_{0.8}\text{Ir}_{0.2})\text{O}_2:10\text{F}$  displayed excellent long term stability in acidic media, similar to that of  $\text{IrO}_2$ . Hence,  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  ( $x = 0.2, 0.3, 0.4$ ) indeed shows excellent promise for replacing state of the art OER electro-catalyst ( $\text{IrO}_2$ ) based on the excellent electrochemical performance demonstrated in this study. Moreover, this study portends significant reduction in noble metal content for OER electro-catalyst and thus, can likely lead to new electrocatalysts development with significant reduction in capital costs of water electrolysis cells for economic and efficient hydrogen production from acid based PEM water electrolysis.

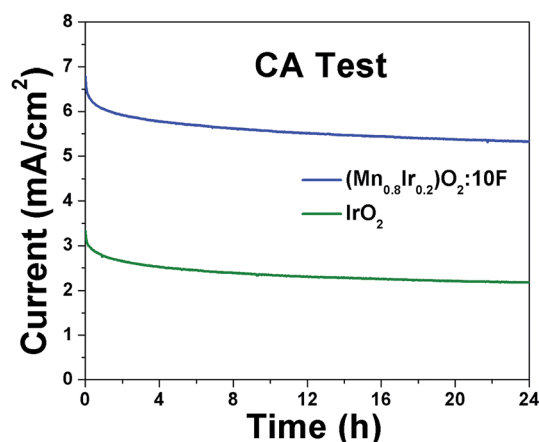


Fig. 8 The variation of current density *vs.* time in the chronoamperometry test of  $(\text{Mn}_{1-x}\text{Ir}_x)\text{O}_2:10\text{F}$  for ( $x = 0.2$ ) and pure  $\text{IrO}_2$  performed in  $1 \text{ N H}_2\text{SO}_4$  solution under a constant potential of  $\sim 1.45 \text{ V}$  (*vs.* RHE,  $iR_{\Omega}$  corrected) at  $40^\circ \text{C}$  for 24 h.





## Author contributions

The original concept of the present work is conceived by S. D. G., P. P. P. and P. N. K. based on the earlier project conceived by P. N. K. along with M. K. D. and O. I. V. S. D. G. and P. P. P. performed the synthesis, structural and electrochemical characterization and analyzed the results of structural and electrochemical characterization of electro-catalyst materials. Theoretical study is conducted by O. I. V. P. M. S. performed XPS. S. D. G. and P. P. P. performed analysis of XPS results. S. D. G., P. P. P. and R. K. performed and analyzed SEM-EDX-elemental X-ray mapping results. M. K. D. and P. N. K. made important suggestions in the draft components. S. D. G., P. P. P., M. K. D., O. I. V. and P. N. K. composed first draft of the present paper. All authors contributed extensively in the manuscript revision. The current project was conceived by P. N. K. and was prudently supervised by P. N. K., M. K. D. and O. I. V.

## Acknowledgements

Authors gratefully acknowledge the support of the National Science Foundation, CBET – Grant 0933141 and CBET – Grant 1511390 for the current research. Acknowledgement is also due to the U.S. Department of Energy, Office of Basic Energy Sciences, Division of Materials Sciences and Engineering under Award DE-SC0001531 for supporting the early work on substituted  $\text{IrO}_2$ . PNK acknowledges the Edward R. Weidlein Chair Professorship funds, the Center for Complex Engineered Multifunctional Materials (CCEMM) for acquiring the electrochemical equipment and facilities used in the present research work and the Pittsburgh Supercomputing Center for providing the computational resources. P. N. K. and O. I. V. also gratefully acknowledge the Extreme Science and Engineering Discovery Environment (XSEDE)<sup>70</sup> supported by National Science Foundation grant number ACI-1053575, for providing the computational resources needed to complete the theoretical component of the present study.

## References

- 1 M. Ball and M. Wietschel, *Int. J. Hydrogen Energy*, 2009, **34**, 615–627.
- 2 I. Katsounaros, S. Cherevko, A. R. Zeradjanin and K. J. J. Mayrhofer, *Angew. Chem., Int. Ed.*, 2014, **53**, 102–121.
- 3 K. Zeng and D. Zhang, *Prog. Energy Combust. Sci.*, 2010, **36**, 307–326.
- 4 J. Suntivich, K. J. May, H. A. Gasteiger, J. B. Goodenough and Y. Shao-Horn, *Science*, 2011, **334**, 1383–1385.
- 5 P. P. Patel, P. J. Hanumantha, O. I. Velikokhatnyi, M. K. Datta, B. Gattu, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Mater. Sci. Eng. B*, 2016, **208**, 1–14.
- 6 P. P. Patel, P. J. Hanumantha, O. I. Velikokhatnyi, M. K. Datta, D. Hong, B. Gattu, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Power Sources*, 2015, **299**, 11–24.
- 7 P. P. Patel, M. K. Datta, O. I. Velikokhatnyi, P. Jampani, D. Hong, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Mater. Chem. A*, 2015, **3**, 14015–14032.
- 8 M. Fischer, M. Werber and P. V. Schwartz, *Energy Policy*, 2009, **37**, 2639–2641.
- 9 P. P. Patel, M. K. Datta, O. I. Velikokhatnyi, R. Kuruba, K. Damodaran, P. Jampani, B. Gattu, P. M. Shanthi, S. S. Damle and P. N. Kumta, *Sci. Rep.*, 2016, **6**, 28367.
- 10 K. Shimura and H. Yoshida, *Energy Environ. Sci.*, 2011, **4**, 2467–2481.
- 11 N. Himeshima and Y. Amao, *Green Chem.*, 2005, **7**, 742–746.
- 12 A. T. Marshall, S. Sunde, M. Tsyppkin and R. Tunold, *Int. J. Hydrogen Energy*, 2007, **32**, 2320–2324.
- 13 A. H. A. Rahim, A. S. Tijani, S. K. Kamarudin and S. Hanapi, *J. Power Sources*, 2016, **309**, 56–65.
- 14 P. Millet, N. Mbemba, S. A. Grigoriev, V. N. Fateev, A. Aukauloo and C. Etievant, *Int. J. Hydrogen Energy*, 2011, **36**, 4134–4142.
- 15 S. A. Grigoriev, V. I. Porembsky and V. N. Fateev, *Int. J. Hydrogen Energy*, 2006, **31**, 171–175.
- 16 A. S. Aricò, V. Baglio, N. Briguglio, G. Maggio and S. Siracusano, *Fuel Cells: Data, Facts and Figures*, 2016.
- 17 X. Lu and C. Zhao, *Nat. Commun.*, 2015, **6**, 6616.
- 18 J. Xu, M. Wang, G. Liu, J. Li and X. Wang, *Electrochim. Acta*, 2011, **56**, 10223–10230.
- 19 A. Skulimowska, M. Dupont, M. Zaton, S. Sunde, L. Merlo, D. J. Jones and J. Rozière, *Int. J. Hydrogen Energy*, 2014, **39**, 6307–6316.
- 20 S. A. Grigoriev, P. Millet and V. N. Fateev, *J. Power Sources*, 2008, **177**, 281–285.
- 21 Y. Matsumoto and E. Sato, *Mater. Chem. Phys.*, 1986, **14**, 397–426.
- 22 C. C. L. McCrory, S. Jung, J. C. Peters and T. F. Jaramillo, *J. Am. Chem. Soc.*, 2013, **135**, 16977–16987.
- 23 E. Mayousse, F. Maillard, F. Fouda-Onana, O. Sicardy and N. Guillet, *Int. J. Hydrogen Energy*, 2011, **36**, 10474–10481.
- 24 K. Kadakia, M. K. Datta, P. H. Jampani, S. K. Park and P. N. Kumta, *J. Power Sources*, 2013, **222**, 313–317.
- 25 K. S. Kadakia, P. Jampani, O. I. Velikokhatnyi, M. K. Datta, S. J. Chung, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Electrochem. Soc.*, 2014, **161**, F868–F875.
- 26 T. Reier, Z. Pawolek, S. Cherevko, M. Bruns, T. Jones, D. Teschner, S. R. Selve, A. Bergmann, H. N. Nong and R. Schlögl, *J. Am. Chem. Soc.*, 2015, **137**, 13031–13040.
- 27 J. M. Hu, H. M. Meng, J. Q. Zhang and C. N. Cao, *Corros. Sci.*, 2002, **44**, 1655–1668.
- 28 C. P. De Pauli and S. Trasatti, *J. Electroanal. Chem.*, 1995, **396**, 161–168.
- 29 M. K. Datta, K. Kadakia, O. I. Velikokhatnyi, P. H. Jampani, S. J. Chung, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Mater. Chem. A*, 2013, **1**, 4026–4037.
- 30 K. Kadakia, M. K. Datta, O. I. Velikokhatnyi, P. H. Jampani and P. N. Kumta, *Int. J. Hydrogen Energy*, 2014, **39**, 664–674.
- 31 R. G. Gonzalez-Huerta, G. Ramos-Sanchez and P. B. Balbuena, *J. Power Sources*, 2014, **268**, 69–76.
- 32 W. Sun, L. Cao and J. Yang, *J. Mater. Chem. A*, 2016, **4**, 12561–12570.
- 33 J. Rossmeisl, Z. W. Qu, H. Zhu, G. J. Kroes and J. K. Nørskov, *J. Electroanal. Chem.*, 2007, **607**, 83–89.
- 34 O. I. Velikokhatnyi, K. Kadakia, M. K. Datta and P. N. Kumta, *J. Phys. Chem. C*, 2013, **117**, 20542–20547.



- 35 G. Kresse and J. Furthmüller, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 1996, **54**, 11169.
- 36 G. Kresse and J. Furthmüller, *Comput. Mater. Sci.*, 1996, **6**, 15–50.
- 37 G. Kresse and D. Joubert, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 1999, **59**, 1758.
- 38 J. P. Perdew and W. Yue, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 1986, **33**, 8800–8802.
- 39 G. N. Murshudov, A. A. Vagin and E. J. Dodson, *Acta Crystallogr., Sect. D: Biol. Crystallogr.*, 1997, **53**, 240–255.
- 40 P. R. Zafred, J. T. Dederer, J. E. Gillett, R. A. Basel and A. B. Antenucci, Google Patents, 1996.
- 41 H. Hu, Y. Fan and H. Liu, *Int. J. Hydrogen Energy*, 2009, **34**, 8535–8542.
- 42 J. A. V. Butler, *Proc. R. Soc. London, Ser. A*, 1936, **157**, 423–433.
- 43 P. P. Patel, M. K. Datta, P. H. Jampani, D. Hong, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Power Sources*, 2015, **293**, 437–446.
- 44 K. S. Kadakia, P. H. Jampani, O. I. Velikokhatnyi, M. K. Datta, S. K. Park, D. H. Hong, S. J. Chung and P. N. Kumta, *J. Power Sources*, 2014, **269**, 855–865.
- 45 B. Hammer and J. K. Nørskov, *Adv. Catal.*, 2000, **45**, 71–129.
- 46 T. Bligaard and J. K. Nørskov, *Electrochim. Acta*, 2007, **52**, 5512–5516.
- 47 V. Subramanian, H. Zhu, R. Vajtai, P. M. Ajayan and B. Wei, *J. Phys. Chem. B*, 2005, **109**, 20207–20214.
- 48 P. P. Patel, P. H. Jampani, M. K. Datta, O. I. Velikokhatnyi, D. Hong, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Mater. Chem. A*, 2015, **3**, 18296–18309.
- 49 J. Xu, G. Liu, J. Li and X. Wang, *Electrochim. Acta*, 2012, **59**, 105–112.
- 50 D. J. Davis, T. N. Lambert, J. A. Vigil, M. A. Rodriguez, M. T. Brumbach, E. N. Coker and S. J. Limmer, *J. Phys. Chem. C*, 2014, **118**, 17342–17350.
- 51 M. Sugantha, P. A. Ramakrishnan, A. M. Hermann, C. P. Warmsingh and D. S. Ginley, *Int. J. Hydrogen Energy*, 2003, **28**, 597–600.
- 52 C. S. Johnson, D. W. Dees, M. F. Mansuetto, M. M. Thackeray, D. R. Vissers, D. Argyriou, C. K. Loong and L. Christensen, *J. Power Sources*, 1997, **68**, 570–577.
- 53 K. Kadakia, M. K. Datta, O. I. Velikokhatnyi, P. H. Jampani and P. N. Kumta, *Int. J. Hydrogen Energy*, 2014, **39**, 664–674.
- 54 N. Krstajic and S. Trasatti, *J. Appl. Electrochem.*, 1998, **28**, 1291–1297.
- 55 A. Minguzzi, F.-R. F. Fan, A. Vertova, S. Rondinini and A. J. Bard, *Chem. Sci.*, 2012, **3**, 217–229.
- 56 P. P. Patel, P. H. Jampani, M. K. Datta, O. I. Velikokhatnyi, D. Hong, J. A. Poston, A. Manivannan and P. N. Kumta, *J. Mater. Chem. A*, 2015, **3**, 18296–18309.
- 57 A. M. Mohammad, M. I. Awad, M. S. El-Deab, T. Okajima and T. Ohsaka, *Electrochim. Acta*, 2008, **53**, 4351–4358.
- 58 F. Cheng, Y. Su, J. Liang, Z. Tao and J. Chen, *Chem. Mater.*, 2009, **22**, 898–905.
- 59 M. Morita, C. Iwakura and H. Tamura, *Electrochim. Acta*, 1977, **22**, 325–328.
- 60 K. Kadakia, M. K. Datta, P. H. Jampani, S. K. Park and P. N. Kumta, *J. Power Sources*, 2013, **222**, 313–317.
- 61 R. H. Blessing, *Crystallogr. Rev.*, 1987, **1**, 3–58.
- 62 C. Zhao, H. Yu, Y. Li, X. Li, L. Ding and L. Fan, *J. Electroanal. Chem.*, 2013, **688**, 269–274.
- 63 H. W. Nesbitt and D. Banerjee, *Am. Mineral.*, 1998, **83**, 305–315.
- 64 X. Liang, C. Hart, Q. Pang, A. Garsuch, T. Weiss and L. F. Nazar, *Nat. Commun.*, 2015, **6**, 5682.
- 65 Z. Li, Y. Mi, X. Liu, S. Liu, S. Yang and J. Wang, *J. Mater. Chem.*, 2011, **21**, 14706–14711.
- 66 M. A. Stranick, *Surf. Sci. Spectra*, 1999, **6**, 31–38.
- 67 M. Sathish, B. Viswanathan, R. P. Viswanath and C. S. Gopinath, *Chem. Mater.*, 2005, **17**, 6349–6353.
- 68 K. Kadakia, M. K. Datta, O. I. Velikokhatnyi, P. Jampani, S. K. Park, S. J. Chung and P. N. Kumta, *J. Power Sources*, 2014, **245**, 362–370.
- 69 K. S. Kadakia, P. H. Jampani, O. I. Velikokhatnyi, M. K. Datta, S. K. Park, D. H. Hong, S. J. Chung and P. N. Kumta, *J. Power Sources*, 2014, **269**, 855–865.
- 70 J. Towns, T. Cockerill, M. Dahan, I. Foster, K. Gaither, A. Grimshaw, V. Hazlewood, S. Lathrop, D. Lifka and G. D. Peterson, *Comput. Sci. Eng.*, 2014, **16**, 62–74.

