

CrossMark  
click for updatesCite this: *RSC Adv.*, 2017, 7, 6345

# Quasi-reverse-emulsion-templated approach for a facile and sustainable environmental remediation for cadmium

Ruhua Zha,<sup>a</sup> Tuo Shi,<sup>b</sup> Zongwen Zhang,<sup>a</sup> Dongli Xu,<sup>a</sup> Tongwu Jiang<sup>a</sup> and Min Zhang<sup>\*c</sup>

Nanostructured hierarchical hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds and nests were fabricated by a solvothermal process at a relatively low reaction temperature using water/glycerol and water/2-propanol as the reaction solvents, respectively. This facile and green quasi-reverse-emulsion soft-templating approach can effectively tailor the monodispersity and nanostructure of the products. The BET surface areas of the chestnut buds and nests were 424.3 and 169.9 m<sup>2</sup> g<sup>-1</sup>, respectively. The maximum monolayer adsorption capacities for Cd(II) of the chestnut buds and nests were found to be 175.8 and 126.3 mg g<sup>-1</sup>, respectively. Both chestnut buds and nests could be recycled with high desorption efficiency and without any remarkable loss of adsorption capacity. Owing to the surface hydroxyl groups, which were determined by FT-IR and TG-MS measurements, and the well-defined hollow mesoporous structure (pore sizes of 5.04 and 6.85 nm, respectively), both hierarchical  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanostructures exhibited superior prospects for the removal of Cd(II) from wastewater in industrial practice.

Received 17th November 2016  
Accepted 25th December 2016

DOI: 10.1039/c6ra26949d

www.rsc.org/advances

## 1. Introduction

Issues of heavy metal pollution linked to wastewater have resulted in serious public concern, with the ever-growing levels of population density and industrialization.<sup>1,2</sup> Heavy metals, which are derived from battery manufacture, demilitarization of munitions, mineral exploitation, chemical fertilizers, pesticides, dye industries, pulping and paper-making, *etc.*, are extremely poisonous water pollutants.<sup>3,4</sup> They can lead to serious public health problems to all creatures and human beings as a result of their continual circulation *via* storage, accumulation and transfer through organisms. The advent of nanotechnology has created considerable opportunities to construct nanostructures with large specific surface areas, multiple valence states, variable electronic structures and related high reactivities, which can provide excellent affinity and removal efficiency for heavy metal ions.<sup>5-7</sup> In recent years, various nanostructured iron oxides with homogeneous sizes and well-defined morphologies have received increasing attention for the decontamination of toxic heavy metal ions in contaminated water, in virtue of the advantageous properties of natural abundance, low cost, environment-friendliness and

large-scale availability of these outstanding adsorbents.<sup>8-10</sup> Specially shaped metal oxides exerted strong effects in the uptake of trace metals. Therefore, the fabrication of nanostructured iron oxides with enhanced adsorption performance for the targeting of heavy metal ions has actively been pursued.<sup>11,12</sup> In our previously reported work, we prepared nanostructured TiO<sub>2</sub> with the shapes of dandelions and spherical flowers *via* a solvothermal method. The dandelions and spherical flowers exhibited excellent adsorption capacities for Cd(II) in aqueous solution (396 and 282 mg g<sup>-1</sup>, respectively). Both nanostructured TiO<sub>2</sub> particles could be repeatedly used without any remarkable loss of adsorption capacity.<sup>13</sup> In particular, hierarchical hollow structures with permeable backbones and large specific surface areas have emerged as fascinating material systems for rapid, efficient and economic environmental remediation.<sup>14-19</sup>

Hematite ( $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>), which is a typical n-type semiconductor with an indirect band gap of 2.1 eV, possesses the most thermodynamically stable phase among all iron oxide crystal structures.<sup>20,21</sup> In addition, it is chemically inert and environmentally friendly. Nanoscaled  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>, in particular hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoarchitectures, have recently been proved to be admirable candidates for the disposal of various inorganic/organic pollutants in contaminated water and air.<sup>22-25</sup> The primary technologies used for the synthesis of hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> include sol-gel methods,<sup>26,27</sup> template synthesis,<sup>28</sup> sonochemical synthesis<sup>29</sup> and solvothermal processes,<sup>18,30,31</sup> *etc.* Three main strategies are employed in the fabrication of hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanostructures, namely, oriented attachment, *in situ* combustion of templates or precursors and self-assembly.

<sup>a</sup>College of Chemistry and Chemical Engineering, Xinyang Normal University, Xinyang 464000, P. R. China<sup>b</sup>Laboratory of Solid State Ionics, School of Materials Science and Engineering, Huazhong University of Science and Technology, Wuhan 430074, P. R. China<sup>c</sup>Henan Collaborative Innovation Center for Energy-Saving Building Materials, Xinyang Normal University, Xinyang 464000, P. R. China. E-mail: zm201177055@sina.com; Fax: +86-376-6370639; Tel: +86-376-6370639

Despite the fact that these synthesis technologies and strategies have many advantageous properties, there are still some deficiencies in the synthesis of hierarchical hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nano-materials. First of all, these synthesis methods typically involve the use of toxic templates. Secondly, a high temperature (>200 °C) is needed for the decomposition of the precursor *via* calcination. Moreover, the majority of hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles have been prepared at elevated temperatures (>180 °C) by hydro/solvothermal processing over a long reaction time. These requirements lead to high energy consumption and impede the large-scale industrialization of the products for practical application in water treatment. Thus, it is urgently necessary to be capable of fabricating well-crystallized hierarchical hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanostructures in a facile, cost-effective and green way.

In this work, two kinds of nanostructured  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> hierarchical hollow spheres, namely, chestnut buds and nests, were synthesized by a facile solvothermal quasi-reverse-emulsion-templated solvothermal process at a relatively low reaction temperature, in which moderate solvent systems of water/2-propanol and water/glycerol mixtures were respectively employed to enable morphological tuning. The success of this approach was due to the presence of microheterogeneities in the water/alcohol soft template. The well-defined porous hollow  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> architectures that were produced exhibited a large specific surface area and a narrow pore size distribution. It is worth noting that the surface of the nanostructured  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> particles, in particular the chestnut buds, contains a large number of OH groups, which can act as effective active adsorption sites for chelating with heavy metal ions. Batch experiments on the adsorption of Cd(II) indicated that both adsorbents possessed superior adsorption capacities for Cd(II) and reusability in the remediation of wastewater.

## 2. Experimental

### 2.1. Preparation of $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles

**2.1.1. Nests.** Nano- $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nests were prepared according to the previous study of the Nanyang Technological University research group with a few modifications.<sup>19</sup> Typically, 50 mL glycerol was added to 175 mL deionized water at room temperature to form an alcohol–water mixture. The solvent mixture was magnetically stirred for 5 min. Then, 0.60 g FeSO<sub>4</sub>·7H<sub>2</sub>O (Alfa Aesar, A.R.) and 1 g CO(NH<sub>2</sub>)<sub>2</sub> (Alfa Aesar, A.R.) were dissolved in this solvent mixture and magnetically stirred for 15 min. The transparent solution that was obtained was quickly transferred into a 500 mL autoclave and solvothermally reacted at 120 °C for 15 h in an electrothermal blowing dry box. After the reaction, the autoclave was cooled naturally to room temperature. The red opaque solution was centrifuged for 10 min and washed repeatedly with deionized water and ethanol. Finally, the red precipitate was collected and dried at 60 °C for 24 h under vacuum.

**2.1.2. Chestnut buds.** Nano- $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds were prepared according to the previous literature with a few modifications.<sup>19</sup> In a typical experiment, 50 mL 2-propanol was added to 175 mL deionized water at room temperature to form an alcohol–water mixture. The solvent mixture was magnetically

stirred for 5 min. Then, 0.60 g FeSO<sub>4</sub>·7H<sub>2</sub>O (Alfa Aesar, A.R.) and 1 g CO(NH<sub>2</sub>)<sub>2</sub> (Alfa Aesar, A.R.) were dissolved in this solvent mixture and magnetically stirred for 15 min. The transparent solution that was obtained was quickly transferred into a 500 mL autoclave and solvothermally reacted at 150 °C for 20 h in an electrothermal blowing dry box. After the reaction, the autoclave was cooled naturally to room temperature. The red opaque solution was centrifuged for 10 min and washed repeatedly with deionized water and ethanol. Finally, the red precipitate was collected and dried at 60 °C for 24 h under vacuum.

### 2.2. Characterization of chestnut buds and nests

XRD patterns were obtained to study the crystal phases of the as-prepared chestnut buds and nests using a Philips diffractometer (PW 3050, 40 kV, Cu K $\alpha$ , 2 $\theta$  = 20° to 80°). XPS measurements of the chestnut buds and nests were made using a VG Multilab 2000 system with a monochromatic Al K $\alpha$  X-ray source (ThermoVG Scientific). The structure and morphology of the chestnut buds and nests were studied by SEM (Hitachi S-4800) and TEM (JEOL 2100F) experiments, in which the accelerating voltage was 200 kV. The elemental composition of the chestnut buds and nests after the adsorption of Cd(II) was determined using an energy-dispersive X-ray spectrometer (EDX) attached to a Hitachi S-4800 SEM. N<sub>2</sub> adsorption and desorption isotherms of the as-synthesized chestnut buds and nests were recorded by physisorption of N<sub>2</sub> (−196 °C, using liquid N<sub>2</sub> as the refrigerant) using a Micromeritics ASAP 2020 analyzer. The mass of the tested samples was approximately 100 mg. Before the measurements, all samples were required to be degassed in a N<sub>2</sub> atmosphere at 150 °C for 10 h. The non-local density functional theory (NLDFT) method was adopted to determine the pore size distribution (PSD) of the chestnut buds and nests. The chemical structures of the as-obtained chestnut buds and nests were studied using an FT-IR spectrometer (Bruker VERTEX 70). The thermal behavior of the chestnut buds and nests was investigated using thermogravimetric analysis (TG) with a high resolution thermogravimetric analyzer system (Netzsch STA 449F3). The thermogravimetric analyzer was purged with N<sub>2</sub> at a flow rate of 50 mL min<sup>−1</sup> and a heating rate of 10 °C min<sup>−1</sup> in the range from 50 to 700 °C. A quadrupole mass spectrometer (QMS 403) was connected to the thermogravimetric analyzer to investigate the amount of water vapour generated in the heating process.

### 2.3. Batch adsorption

Batch experiments on powder  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds and nests were employed to determine the water treatment behavior for Cd(II), which served as a typical representative of heavy metal ions in an aqueous solution. Adsorption isotherm experiments were carried out at  $T$  = 25 °C and pH = 5.0. The pH of the Cd(II) solutions was adjusted by HCl (0.1 mol L<sup>−1</sup>) and NaOH (0.1 mol L<sup>−1</sup>). To study the effect of the initial Cd(II) concentrations on the uptake capacity of the synthesized nanostructured  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>, the adsorbent (80 mg) was added to Cd(II) solutions of different concentrations (20, 50, 75, 100, 150, 200, 250, 300, 350 and



400 mg L<sup>-1</sup>) prepared using anhydrous cadmium chloride (CdCl<sub>2</sub>). The adsorption reaction was carried out on a shaking table at a shaking speed of 180 rpm. After the reaction, the mixtures were centrifuged at 18 000 rpm for 20 min to segregate the solid and liquid phases. The concentration of Cd(II) in the supernatant liquor was measured using an atomic adsorption spectrometer (AAS, Varian Spectra AA 55, USA). Continuous adsorption-desorption cycles were conducted to study the recyclability of the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> adsorbents. The adsorbed Cd(II) was desorbed with different concentrations of citric acid (0.01, 0.02, 0.1, 0.2, 0.3 and 0.4 mol L<sup>-1</sup>). The desorbed adsorbents (chestnut buds and nests) were completely cleaned with distilled water to remove any residual Cd(II) and immersed into the Cd(II) solution for the next adsorption-desorption process.

### 3. Results and discussion

#### 3.1. Characterization of chestnut buds and nests

The crystal structure and phase purity of the synthesized chestnut buds and nests were examined *via* their XRD patterns. As shown in Fig. 1, both chestnut buds and nests exhibited diffraction peaks for the (012), (104), (110), (113), (024), (116), (018), (214) and (300) planes, which were fully in agreement with those for  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> powder (JCPDS card no. 80-2377).<sup>20</sup> Besides, there is no extra diffraction peak for impurities in Fig. 1, which demonstrates that the obtained chestnut buds and nests were well crystallized. The crystallinity of chestnut buds was higher than that of nests.

SEM and TEM images of the obtained nests are shown in Fig. 2. According to Fig. 2A, the reddish brown product had a well-preserved nest-like spherical structure. The average diameter of the nest nanoparticles in this sample was approximately 400 nm. As can be seen in one high-magnification SEM image (Fig. 2B), the surface of each typical nest nanoparticle was accumulated from large numbers of fine nanosheets. Furthermore, the clear hollow interior of a single broken nest nanoparticle can be found in the other high-magnification SEM image (Fig. 2C), which demonstrates the hollow-core construction of the as-synthesized  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nests, as in the schematic diagram illustrated in Fig. 2F. It can be seen in the

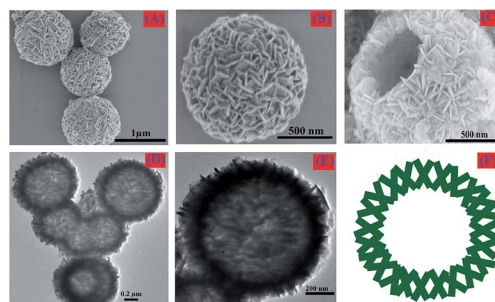


Fig. 2 (A) Low-magnification SEM image, (B, C) high-magnification SEM images, (D) TEM image, (E) HRTEM image and (F) schematic diagram of the synthesized nests.

corresponding TEM images (Fig. 2E and F) that the hollow cages possess an interlinked and uniformly stacked shell with a shell thickness of approximately 70 nm.

The above XRD results and observations of the surface and internal structure *via* SEM and TEM images indicate that there are three main stages in the formation of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nests (Fig. 3). Before the solvothermal reaction, glycerol was mixed with water to form a homogeneous quasi-reverse emulsion.<sup>32</sup> Despite the fact that these two kinds of solvent are mutually soluble and form a completely uniform aqueous system from the point of view of thermodynamic equilibrium, it has been found that such polar solutes as acetone, 2-propanol and butanol, *etc.* are liable to self-assemble in an aqueous solution because of the self-hydrophobic interactions of the alcohols, which therefore generates typical microheterogeneities in the mixed system. The quasi-reverse emulsion of water/glycerol that is formed further develops numerous emulsified spherical droplets, which act as soft templates for the construction of the shell backbone. In the solvothermal reaction, many Fe<sub>2</sub>O<sub>3</sub> nanoparticles were created and assembled on the surface of these quasi-reverse-emulsion droplets by the hydrolysis of FeSO<sub>4</sub>·7H<sub>2</sub>O at the appropriate reaction temperature (120 °C) and pH. The weakly alkaline conditions were adjusted by CO(NH<sub>2</sub>)<sub>2</sub>. As the hydrothermal treatment proceeded, these random nanoparticles gradually aggregated into sheet-like nanostructures to reduce the surface energy to the greatest extent and shape firm shells. Finally, the internal glycerol

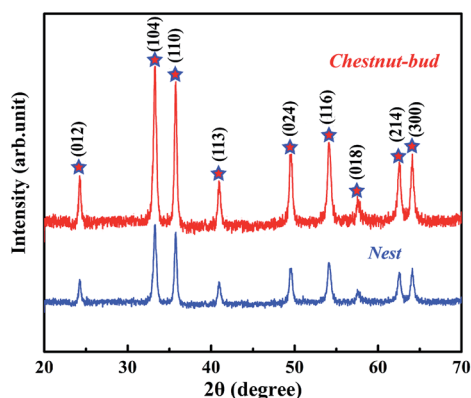


Fig. 1 XRD patterns of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds and nests.

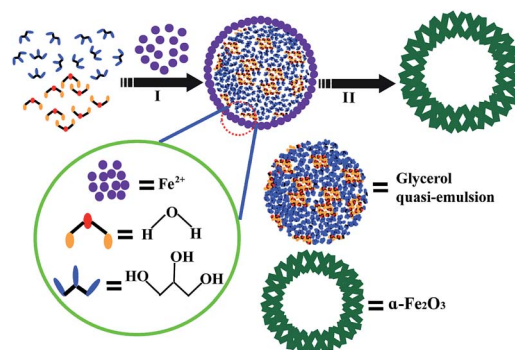


Fig. 3 Schematic illustration of the formation of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nests.





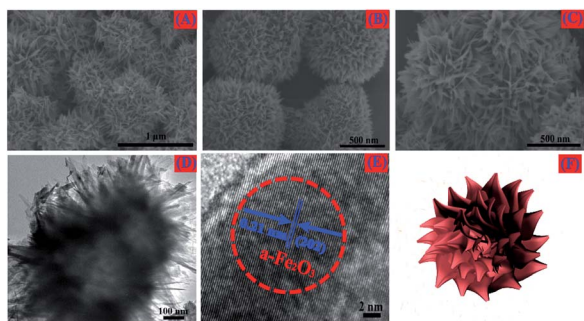


Fig. 4 (A) Low-magnification SEM image, (B, C) high-magnification SEM images, (D) TEM image, (E) HRTEM image and (F) schematic diagram of the synthesized chestnut buds.

droplets are readily removed *via* washing with ethanol while the skeleton of the outer shell retains its original form, which gives rise to the generation of a well-defined hollow sphere.

Fig. 4A–C shows typical SEM images of the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds, which are formed with a well-preserved chestnut bud-like spherical nanostructure. The  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds are approximately 5  $\mu$ m in diameter and consist of hierarchical porous spheres, which are formed from enormous neatly arranged nanorods as the basic compositional units with a typical diameter of 30 nm and a length of 100–150 nm. A TEM image (Fig. 4D) demonstrates that the spherical  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut bud has a hollow interior (as illustrated in Fig. 4F) and the outer and inner diameters of the chestnut bud-like hollow sphere are approximately 1  $\mu$ m and 500 nm, respectively. From Fig. 4E, we can observe that the distance of approximately 0.210 nm between typical adjacent lattice fringes well corresponds to the *d*-spacing value of (202) planes in the hexagonal  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> structure.

The formation mechanism of the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds is shown in Fig. 5. The formation process of chestnut buds was the same as that of nests. The main differences involved the alcohol used as the starting material, the temperature of the solvothermal reaction and the reaction time. The growth pattern of chestnut buds and nests was in agreement with the report by Yang and Zeng.<sup>32</sup> It was indicated that the structure and morphology of the shell skeleton were affected by the alcohol

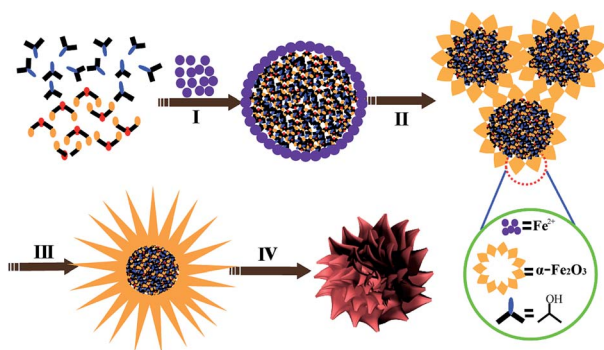


Fig. 5 Schematic illustration of the formation of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds.

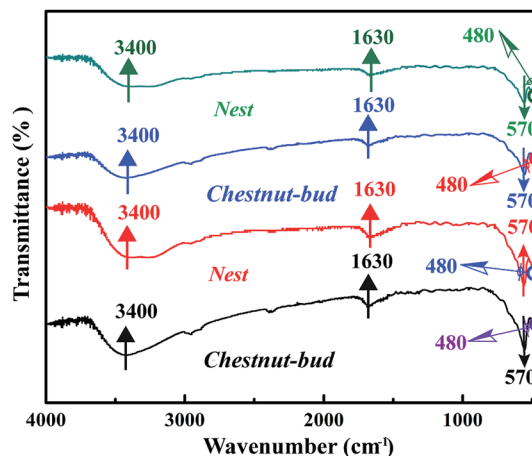


Fig. 6 FT-IR spectra of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> samples annealed at different temperatures: (a) chestnut buds: 80 °C, (b) nests: 80 °C, (c) chestnut buds: 170 °C and (d) nests: 170 °C.

used and the reaction temperature. On the one hand, the hydrophobicity of glycerol is higher than that of 2-propanol. The stronger hydrophobic interactions of glycerol would give rise to larger “micelles”, which generated a larger hollow interior structure in the chestnut buds. On the other hand, both the reaction temperature (150 °C *vs.* 120 °C) and the reaction time (20 h *vs.* 15 h) in the solvothermal treatment process for chestnut buds were higher than those for nests and gave rise to rougher, smoother and sharper edges and corners. All these factors led to the formation of chestnut bud-like nanostructures.

Fig. 6 shows the FT-IR spectra of the chestnut buds and nests. The broad band situated at 3400 cm<sup>−1</sup> is assigned to the asymmetrical and symmetrical O–H stretching vibrations of surface OH groups and lattice water molecules.<sup>33,34</sup> The strong peaks in the regions of 480 and 570 cm<sup>−1</sup> correspond to the Fe–O stretching vibrational mode in crystalline  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>.<sup>35</sup> The presence of the peak near 1630 cm<sup>−1</sup> is attributed to the bending vibrations of Fe–OH. The broad band at 3400 cm<sup>−1</sup> disappeared upon annealing at 170 °C, which indicates that the

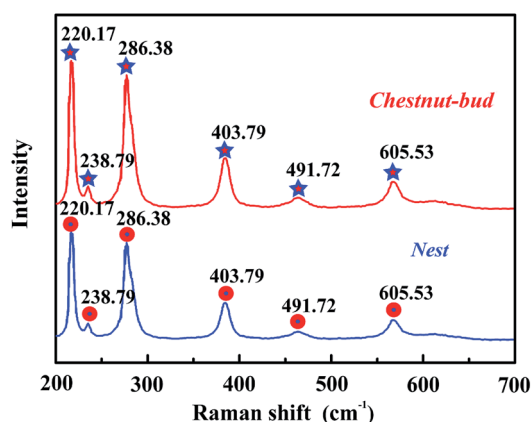


Fig. 7 Raman spectra of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds and nests.



adsorbed water on the surface of the chestnut buds and nests was dislodged by heating, but the peak at  $1630\text{ cm}^{-1}$  corresponding to the bending vibrations of Fe–OH was still present, which would guarantee the effective adsorption of Cd(II).

Fig. 7 shows the Raman spectra of chestnut buds and nests, which may reflect the microstructure of the obtained nanoparticles. Obviously, there are six strong resonance peaks at positions of 220.17, 238.79, 286.38, 403.79, 491.72 and  $605.53\text{ cm}^{-1}$  in the range from 200 to  $700\text{ cm}^{-1}$ , which are in good agreement with the typical characteristic bands observed for  $\alpha\text{-Fe}_2\text{O}_3$ . The resonance peaks situated at 220.17 and  $491.72\text{ cm}^{-1}$  correspond to the  $A_{1g}$  Raman modes, and the characteristic peaks at 238.79, 286.38, 403.79 and  $605.53\text{ cm}^{-1}$  are assigned to the  $E_{2g}$  Raman modes.<sup>36</sup> It is clear that the Raman data match well with the FT-IR results.

Analysis of the  $\text{N}_2$  adsorption–desorption isotherms (Fig. 8) was performed to determine the specific surface area and structural characteristics of pores of the produced  $\alpha\text{-Fe}_2\text{O}_3$  chestnut buds and nests. The curves exhibit hysteresis loops in the range of relative pressures of 0.80–0.98, which indicates the presence of mesopores and micropores in the chestnut buds and nests. Both samples display type II isotherms and their BET surface areas were calculated to be 424.3 and  $169.9\text{ m}^2\text{ g}^{-1}$ , respectively. Their average pore volumes are 1.09 and  $0.38\text{ cm}^3\text{ g}^{-1}$ , respectively, and their average pore sizes are 5.04 and 6.85 nm, respectively. The narrow pore size distribution for both samples, in particular the chestnut buds, relates to their homogeneous morphologies. The meso/micropores and large specific surface areas of the hollow spherical nanostructures would provide fast ion transportation and exchange for the adsorption/desorption of heavy metal ions in the process of wastewater treatment.

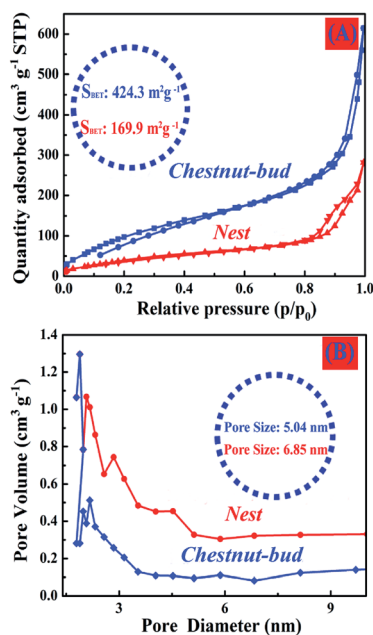


Fig. 8 (A)  $\text{N}_2$  adsorption–desorption isotherms and (B) pore size distributions of the as-synthesized hollow spherical  $\alpha\text{-Fe}_2\text{O}_3$  nanoparticles.

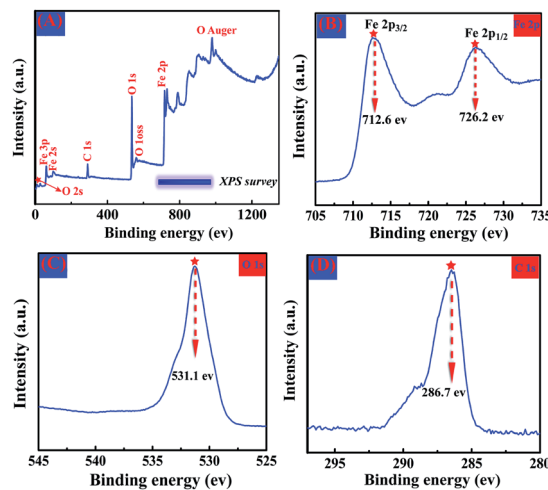


Fig. 9 Wide-scan XPS survey spectrum (A), Fe 2p XPS spectrum (B), O 1s XPS spectrum (C) and C 1s XPS spectrum (D) of the  $\alpha\text{-Fe}_2\text{O}_3$  sample.

XPS measurements were used to perform a fundamental analysis of the elemental composition and chemical state of the produced  $\alpha\text{-Fe}_2\text{O}_3$  samples, and the results are displayed in Fig. 9, as exemplified by chestnut buds. Fig. 9A illustrates the wide-scan survey spectrum of  $\alpha\text{-Fe}_2\text{O}_3$  chestnut buds, which clearly indicates the presence of Fe, O and C elements. Fig. 9B shows the XPS spectrum of Fe, which includes peaks for  $\text{Fe } 2p_{1/2}$  and  $\text{Fe } 2p_{3/2}$  with binding energies located around 726.2 eV and 712.6 eV, respectively. This indicates that the oxidation state of Fe is in the form of Fe(III) in the produced compound.<sup>37</sup> Fig. 9C illustrates the XPS spectrum of O. Only a single peak for O 1s located around 531.1 eV is observed. This suggests that there were no impurity species in the produced sample within the sensitivity of the technique. Only a C 1s peak of surface adsorbed carbon located around 286.7 eV (Fig. 9D) was present.<sup>38</sup> The above results agree well with the XRD results, namely, that the obtained samples are a pure  $\alpha\text{-Fe}_2\text{O}_3$  phase.

The chestnut buds and nests were further investigated by TG-MS. The gas detected in this procedure was  $\text{H}_2\text{O}$ . The profiles of the evolution of  $\text{H}_2\text{O}$  upon heating for chestnut buds and nests are displayed in Fig. 10. It can be observed that the signals of water are different between chestnut buds and nests. Fig. 10A shows the profiles of the evolution of  $\text{H}_2\text{O}$  ( $m/z = 18$ ) during the degradation of the chestnut buds. The first signal of weight loss is located at  $95.3^\circ\text{C}$ , and the peak in the temperature region below  $95.3^\circ\text{C}$  is related to the release of moisture adsorbed on the samples. The major weight loss above  $200^\circ\text{C}$  can be assigned to the dehydration of Fe–OH groups. The decomposition profiles of  $\text{H}_2\text{O}$  ( $m/z = 18$ ) for nests are displayed in Fig. 10B. The peak at below  $92.2^\circ\text{C}$  is associated with the evolution of moisture in the samples. Obviously, the peak signal was broader and less intense in the temperature region above  $200^\circ\text{C}$ , which demonstrated that the dehydration of Fe–OH groups in nests was much less extensive than that in chestnut buds. The FT-IR and TG-MS results are in good agreement with each other, all of which indicate the presence of Fe–OH groups in the produced  $\alpha\text{-Fe}_2\text{O}_3$  nanostructures.



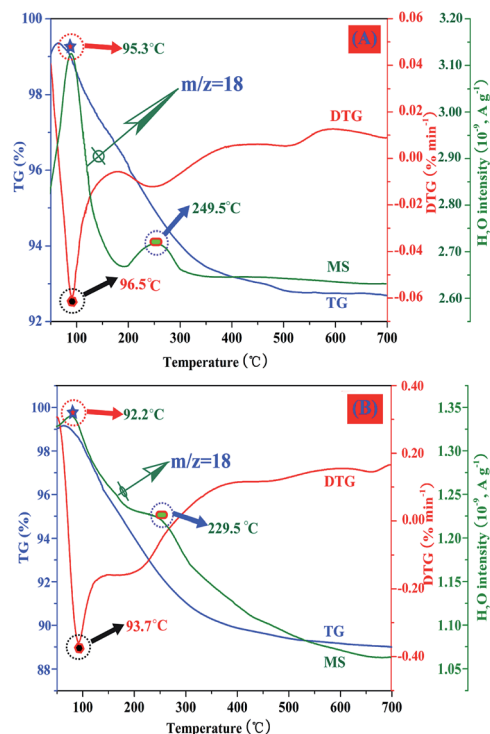


Fig. 10 Characteristic TG-MS curves for (A) chestnut buds and (B) nests.

### 3.2. Cd(II) adsorption studies

Cd(II), as one of the commonest heavy metal ions, is highly toxic in industrial effluents, and the effective removal of Cd(II) from water is significantly important for environmental remediation. Here, we examined the application of the as-synthesized  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds and nests in the control of environmental pollution. Fig. 11 clearly illustrates the procedure of wastewater treatment by the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles, which has the advantages of being facile, environment-friendly and applicable on a large scale.

The removal percentage  $R$  (%), the adsorption capacity  $q_t$  (mg g<sup>-1</sup>) for Cd(II) at a time  $t$ , and the equilibrium adsorption capacity  $q_e$  (mg g<sup>-1</sup>) for Cd(II) adsorbed onto the chestnut buds and nests from aqueous media at 25 °C were calculated using the following equations:

$$R = \frac{C_0 - C_t}{C_0} \times 100, \quad (1)$$

$$q_t = \frac{(C_0 - C_t)V}{m}, \quad (2)$$

$$q_e = \frac{(C_0 - C_e)V}{m}, \quad (3)$$

where  $C_0$  (mg L<sup>-1</sup>),  $C_t$  (mg L<sup>-1</sup>) and  $C_e$  (mg L<sup>-1</sup>) represent the initial concentration, concentration at a time  $t$  and equilibrium concentration, respectively, of the Cd(II) solution,  $V$  (L) is the volume of the Cd(II) solution and  $m$  (g) represents the mass of the adsorbent used in the batch adsorption procedure.

**3.2.1. Effect of contact time.** The effect of the contact time on the uptake of Cd(II) by chestnut buds and nests was studied to ascertain the time required to reach equilibrium in the adsorption reaction (Fig. 12). (The initial concentration of the Cd(II) solutions was 300 mg L<sup>-1</sup>, the initial pH was 5 and the adsorption reactions were conducted at 25 °C.) At the initial stage (30 min), it is clearly observed from Fig. 12A that the rate of adsorption of Cd(II) onto chestnut buds was very rapid. When the adsorption reaction was continued for 60–80 min, the relative adsorption capacity for Cd(II) underwent no significant increase, which indicated that adsorption equilibrium was established within 100 min. During this period, the chestnut buds displayed superior capability for the removal of Cd(II); almost 93.7% of Cd(II) was removed. The rapid adsorption of Cd(II) by chestnut buds may indicate that most of their active sites are exposed for the adsorption of Cd(II). Hence, a contact time of 100 min is suitable for the maximum adsorption of Cd(II) by chestnut buds.

As shown in Fig. 12B, the rate of removal of Cd(II) for nests was lower than that for chestnut buds. The appropriate contact

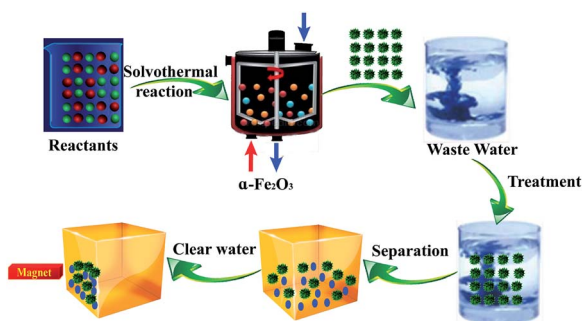


Fig. 11 Use of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles for wastewater treatment.

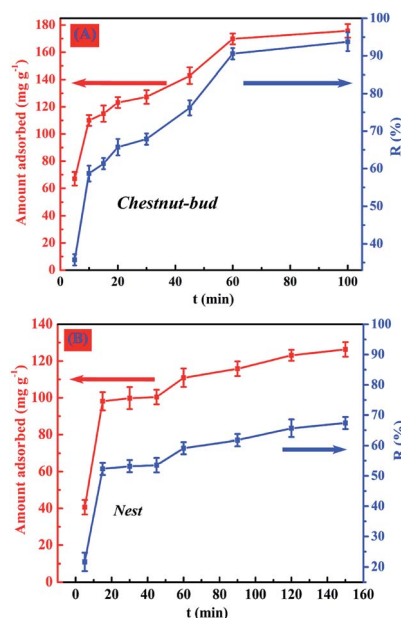


Fig. 12 Effect of contact time on adsorption capacity for Cd(II) of (A) chestnut buds and (B) nests.





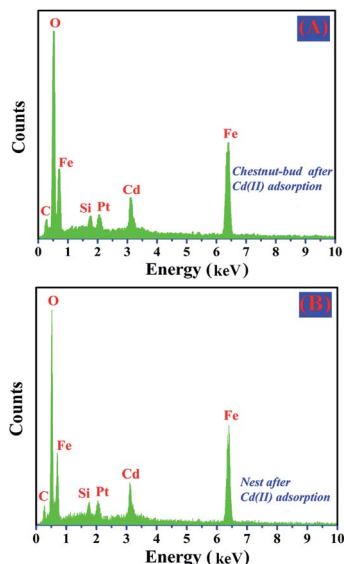


Fig. 13 EDX spectra of (A) chestnut buds after adsorption of Cd(II) and (B) nests after adsorption of Cd(II).

time taken for nests to reach adsorption equilibrium was 150 min, which was longer than that for chestnut buds. Furthermore, only 67.4% of Cd(II) was removed by the nests after 150 min. The difference in the rate of adsorption for the uptake of Cd(II) between the chestnut buds and nests was potentially due to the different numbers of available active adsorption sites. With an increase in the contact time the adsorption sites gradually became exhausted, and afterwards the adsorption rate declined as a result of the slow pore diffusion of Cd(II) into the bulk of the chestnut buds and nests.

After the adsorption of Cd(II), EDX and XPS analyses were performed to determine the elemental compositions of chestnut buds and nests. As shown in Fig. 13, the EDX results indicate the presence of Fe, O and Cd elements in the chestnut

buds and nests after the adsorption of Cd(II). The average atomic weight percentage ratios of Fe : O : Cd for the tested chestnut buds and nests were 31.8 : 59.9 : 8.6 and 35.4 : 56.5 : 8.1, respectively.

Fig. 14A and C show the wide-scan survey spectra of chestnut buds and nests after the adsorption of Cd(II). They also clearly indicate the presence of Fe, O and Cd elements. Peaks for Cd 3d<sub>3/2</sub> and Cd 3d<sub>5/2</sub> had binding energies located around 412.09 eV and 405.07 eV, respectively (Fig. 14B and D). They indicate that the oxidation state of Cd is in the form of Cd(II) in the produced compound.<sup>39</sup> The above XPS results are in good agreement with the EDX results, namely, that the heavy metal ion Cd(II) has been adsorbed onto the as-synthesized chestnut buds and nests.

**3.2.2. Effect of initial pH.** The pH value of the external Cd(II) solution affects the activity of functional groups on the surface of adsorbents. The adsorption capacity for Cd(II) of chestnut buds and nests as a function of the initial pH is illustrated in Fig. 15. (The initial concentration of the Cd(II) solutions was 300 mg L<sup>-1</sup> and the adsorption reactions were conducted at 25 °C. The contact times for chestnut buds and nests were 100 and 150 min, respectively.) As can be seen in Fig. 15, the adsorption capacity for Cd(II) of both adsorbents is critically dependent upon the pH of the Cd(II) solution. In addition, the adsorption capacity for Cd(II) of the chestnut buds is much higher than that of the nests at all pH values (1.0, 2.0, 3.0, 4.0, 5.0 and 6.0). With an increase in pH in the range from 1.0 to 6.0, the adsorption capacity for Cd(II) of chestnut buds increased from 54.1 to 175.8 mg g<sup>-1</sup>, and from 25.2 to 126.3 mg g<sup>-1</sup> for nests. The adsorption capacity for Cd(II) of both chestnut buds and nests underwent a prompt increase when the solution pH was 1.0–3.0, followed by a slow increase at pH values of 3.0–5.0 to an almost constant level at a pH of 5.0–6.0. These results indicated that the optimum adsorption capacities for Cd(II) of chestnut buds and nests can be obtained in the pH range of 5.0–6.0.

The change in adsorption capacity for Cd(II) with the change in pH can be explained by considering the point of zero charge (PZC) of the adsorbents. The pH<sub>PZC</sub> values of chestnut buds and nests are 4.9 and 5.2, respectively, which were determined from

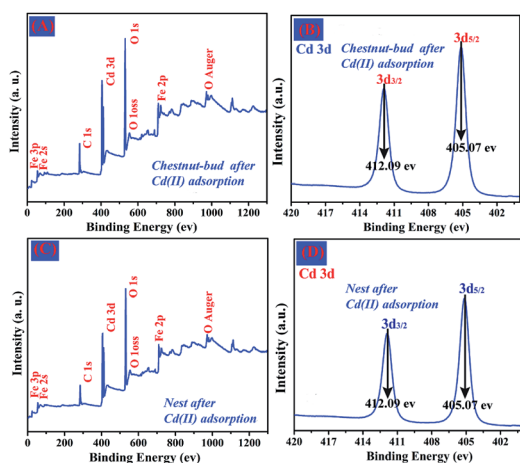


Fig. 14 (A) Wide-scan XPS survey spectrum of chestnut buds after adsorption of Cd(II), (B) the corresponding Cd 3d XPS spectrum, (C) wide-scan XPS survey spectrum of nests after adsorption of Cd(II), (D) the corresponding Cd 3d XPS spectrum.

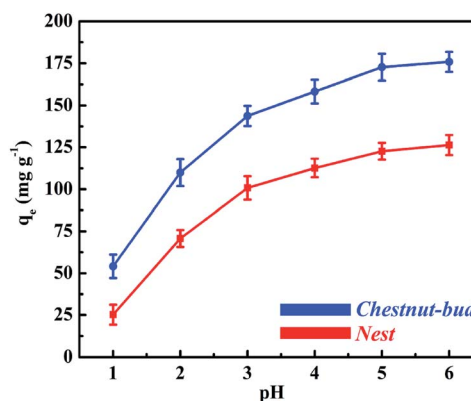


Fig. 15 Effect of initial pH value on adsorption capacity for Cd(II) of chestnut buds and nests.



measurements of the zeta potential. The available active sites on the adsorbents for the efficient removal of heavy metals are derived from hydrogen ions in hydroxyl groups.<sup>40</sup> Determination of the form in which Cd(II) is present in solutions with different pH values is complex, because there are multiple Cd(II) species present in solutions. When the adsorption process takes place, each divalent Cd(II) ion displaces one proton from -OH groups *via* electrostatic attraction (ion exchange) to generate Cd(OH)<sup>+</sup> species. At a pH below the PZC, the presence of large amounts of H<sup>+</sup> ions increases the repulsive forces that exist between the positively charged Cd(II) species and the adsorption sites of the adsorbents. They can be adsorbed on the negatively charged active sites on the surface of chestnut buds and nests *via* the protonation effect. Thus, at lower pH values (1.0–2.0) the adsorption capacity for Cd(II) was relatively low. After a further increase in the solution pH, the adsorbed Cd(OH)<sup>+</sup> species on chestnut buds and nests continued to displace one proton to produce soluble Cd(OH)<sub>2</sub>. Then, the amount of adsorbed Cd(II) rose rapidly in the pH range from 2.0 to 3.0, and rose gradually in the pH range from 3.0 to 5.0. At a pH above the PZC, negatively charged OH<sup>-</sup> ions exhibit strong coordinative affinity towards positively charged Cd(II) ions. The electrostatic attractive forces cause OH<sup>-</sup> ions to capture Cd(II) species *via* surface complexation. The level of surface complexation can be enhanced as the pH value increases. If the pH value of the solution exceeded 6.0, fewer H<sup>+</sup> ions would be able to compete with Cd(II) ions for active adsorption sites. Thus, soluble Cd(OH)<sub>2</sub> species would become supersaturated and a precipitate of Cd(OH)<sub>2</sub> would be generated. Thereafter, Cd(II) in the solution is taken up not only by adsorption but also by precipitation. Consequently, all subsequent adsorption experiments were conducted at the optimum initial pH of 5.0 to achieve the maximum adsorption capacity. At this pH value, ion exchange and surface complexation are the predominant mechanisms for the removal of metal ions from solution.

**3.2.3. Effect of initial Cd(II) concentration.** Fig. 16 shows the removal performance for Cd(II) with different initial concentrations of the chestnut buds and nests. (The initial pH of the Cd(II) solutions was 5.0 and the adsorption reactions were

conducted at 25 °C. The contact times for chestnut buds and nests were 100 and 150 min, respectively.) It is demonstrated that the adsorption capacity of chestnut buds when reaching an equilibrium state increased rapidly as the initial concentration of Cd(II) increased from 20 to 300 mg L<sup>-1</sup>, which indicates that the removal behavior for Cd(II) did not achieve adsorption saturation in this initial concentration range. The adsorption capacity remained nearly stable as the Cd(II) concentration continued to increase (300–400 mg L<sup>-1</sup>), which indicated that the active adsorption sites were not sufficient for the adsorption reaction. A similar isotherm curve is also observed for the nests, but the curve for the chestnut buds is much higher and steeper. For the chestnut buds, the removal capacity for Cd(II) increased from 97 to 175.8 mg g<sup>-1</sup> when the initial Cd(II) concentration increased from 20 to 400 mg L<sup>-1</sup>, whereas it increased from 80 to 126.3 mg g<sup>-1</sup> for the nests. The maximum adsorption capacity of the chestnut buds for Cd(II) was found to be 175.8 mg g<sup>-1</sup> in comparison to 126.3 mg g<sup>-1</sup> for the nests. The surfaces of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles can afford large amounts of active adsorption sites and are beneficial for the transportation and complexation of Cd(II). The different structures of the chestnut buds and nests and their different specific surface areas (424.3 and 169.9 m<sup>2</sup> g<sup>-1</sup>, respectively) led to different numbers of active adsorption sites.

**3.2.4. Effect of other coexisting metal ions.** To investigate the selectivity behavior for heavy metal ions in a multi-component system, the removal percentages of chestnut buds for three different heavy metal ions, *i.e.*, Cd(II), Zn(II) and Ni(II), in single-component, binary and ternary solutions were examined (Fig. 17). The concentration of each metal was 300 mg L<sup>-1</sup> and the amount of the adsorbents was 80 mg. The initial pH of the metal ion solution was 5.0 and the adsorption reactions were conducted at 25 °C. The contact time was 240 min. As illustrated in Fig. 17, the removal percentages for Cd(II), Ni(II) and Zn(II) in single-component systems were 93.7%, 76.8% and 38.3%, respectively. In binary systems (Cd(II)–Zn(II) and Cd(II)–Ni(II)), the removal percentages for Cd(II) of chestnut buds were

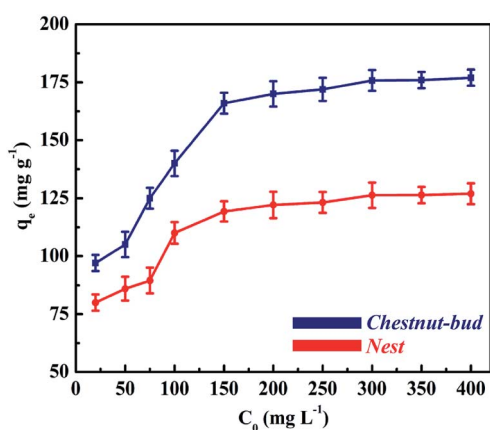


Fig. 16 Adsorption capacity for Cd(II) with different initial Cd(II) concentrations of the chestnut buds and nests.

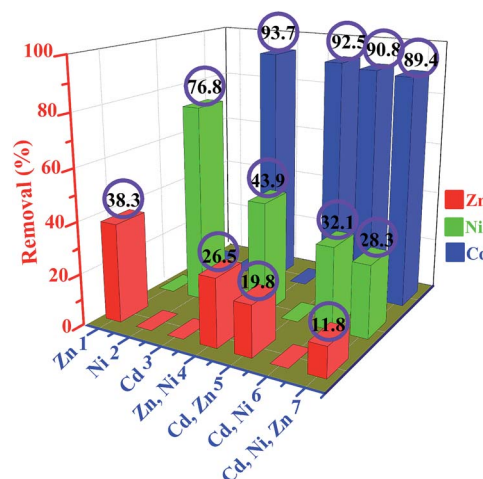


Fig. 17 Removal percentages for Cd(II), Zn(II) and Ni(II) from single-component, binary and ternary ion solutions.





92.5% and 90.8%, respectively, in the presence of Zn(II) or Ni(II). In comparison, the removal percentages for Zn(II) and Ni(II) displayed sharp declines (to 19.8% and 32.1%, respectively) in the same binary solutions. This clearly suggests that Cd(II) was preferentially adsorbed onto the surface of chestnut buds in comparison to Ni(II) or Zn(II). In the case of the binary Ni(II)–Zn(II) system, it was observed that the removal percentages for Ni(II) and Zn(II) were also reduced to 43.9% and 26.5%, respectively, which indicates the competitiveness of the two metal ions. As can be seen in the case of the ternary ion solutions, the removal percentages for Cd(II), Ni(II) and Zn(II) were 89.4%, 43.9% and 26.5%, respectively. In compared with the cases of single-component or binary ion solutions, the removal efficiency for Cd(II) maintained a relatively stable level. Nevertheless, the removal efficiency for Ni(II) and Zn(II) was much less than that in the single-component or binary systems. According to the comparative results from the single-component, binary and ternary systems, it is revealed that the influence of the coexistence of Ni(II) and/or Zn(II) on the adsorption of Cd(II) by chestnut buds was negligible, whereas the removal efficiencies for Zn(II) and Ni(II) greatly decreased when in a competitive metal ion environment. Thus, the removal efficiencies for the three metal ions follow the order of Cd(II) > Ni(II) > Zn(II), which suggests a stronger affinity of the chestnut buds for Cd(II) than for Ni(II) and Zn(II).

### 3.3. Adsorption mechanism and kinetics

The as-synthesized nanostructured  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> particles, in particular the chestnut buds, exhibited high adsorption performance with a maximum adsorption capacity of 175.8 mg g<sup>-1</sup> and a removal percentage of 93.7% within 100 min of the adsorption reaction. Their superior properties strictly depend on their microstructure. Fig. 18 illustrates the structural characteristics of the hollow spheres of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles, which can be summarized as follows. First of all, both adsorbents possess hierarchically porous hollow structures with an average pore size of 5.04 and 6.85 nm, respectively, as investigated by N<sub>2</sub> adsorption and desorption isotherms, which indicates that micropores and mesopores constituted the major pore components. The mesopores in the hollow spherical shell are

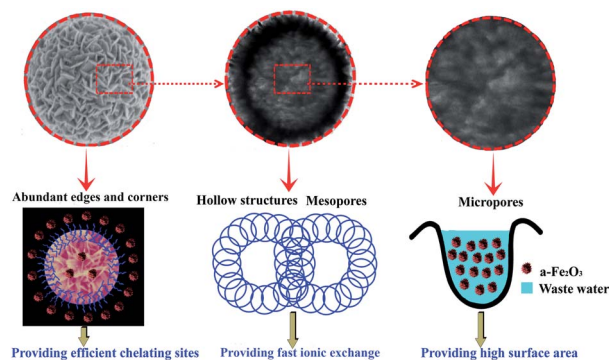


Fig. 18 Schematic illustration of the structural characteristics of the hollow spheres of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles.

beneficial for providing rapid ion exchange and a high complexation rate because of the easy permeation and transportation of Cd(II) into the surface and interior of the hollow spheres. Moreover, the micropores can provide a large surface area, namely, large amounts of active adsorption sites. Finally, the abundant edges and corners on the surfaces of the hollow spheres can provide efficient chelating sites to ensure the effective adsorption of Cd(II).

Fig. 19 illustrates the process of the adsorption of Cd(II) by nanostructured  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> adsorbents. The mechanism of the removal of Cd(II) included surface complexation and ion exchange between the surface OH groups of the adsorbents and the heavy metal ions of the adsorbates in the aqueous solution, in which bonding of Cd(II) *via* coordination by the OH groups played an indispensable role.<sup>9</sup> The well-defined morphology of the chestnut buds led to a larger BET specific surface area and pore volume (424.3 cm<sup>2</sup> g<sup>-1</sup> and 1.09 cm<sup>3</sup> g<sup>-1</sup>, respectively), which were 2.50 and 2.87 times higher, respectively, than those of the nests. The homogeneous channels inside and outside the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles could provide abundant active adsorption sites and are thus convenient for the movement and transport of Cd(II) in the adsorption reaction.

The adsorption kinetics behavior, which governs the rate of removal of Cd(II) and the adsorption mechanisms in the adsorption process, is a significant factor in evaluating the efficiency of the removal of Cd(II). As shown in Fig. 12, an apparent adsorption equilibrium was reached within 100 min and 150 min for chestnut buds and nests, respectively. Three kinetics models, *i.e.*, pseudo-first-order and pseudo-second-order rate equations and the intraparticle diffusion model, were selected to analyze the adsorption kinetics data.<sup>41,42</sup>

The expression for the pseudo-first-order kinetics model is as follows:

$$\log(q_e - q_t) = \log q_e - \frac{k_1}{2.303} t, \quad (4)$$

The expression for the pseudo-second-order kinetics model is as follows:

$$\frac{t}{q_e} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t, \quad (5)$$

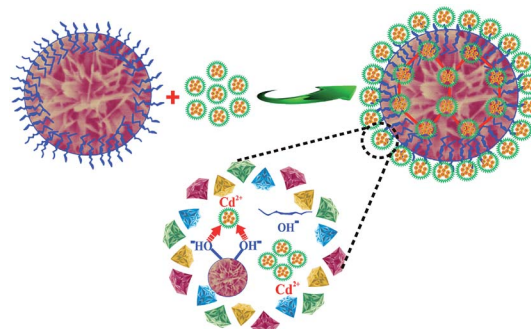


Fig. 19 Proposed mechanism of adsorption of Cd(II) on  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles.



**Table 1** Kinetic fitting parameters for adsorption of Cd(II) on the chestnut buds and nests

Sample	$q_e$ (exp)	Pseudo-first-order			Pseudo-second-order		
		$k_1$ (min <sup>-1</sup> )	$q_e$ (cal)	$R^2$	$k_2$ (g mg <sup>-1</sup> min <sup>-1</sup> )	$q_e$ (cal)	$R^2$
Chestnut buds	175.8	$3.68 \times 10^{-2}$	118.5	0.893	$4.84 \times 10^{-4}$	191.5	0.992
Nests	126.3	$1.91 \times 10^{-2}$	56.1	0.858	$7.25 \times 10^{-4}$	132.1	0.996

The expression of the intraparticle diffusion model is as follows:

$$q_t = K_3 t_{1/2} + C, \quad (6)$$

where  $q_e$  (mg g<sup>-1</sup>) is the equilibrium adsorption capacity,  $q_t$  (mg g<sup>-1</sup>) is the adsorption capacity at a time  $t$  (min),  $k_1$  (min<sup>-1</sup>) and  $k_2$  (g mg<sup>-1</sup> min<sup>-1</sup>) are the pseudo-first-order and pseudo-second-order rate constants, respectively,  $K_3$  (g mg<sup>-1</sup> min<sup>-1</sup>) is the intraparticle diffusion rate constant and  $C$  is the intercept.

The parameters calculated from the pseudo-second-order and pseudo-first-order kinetics models are presented in Table 1. The linear correlation coefficients  $R^2$  (0.893 and 0.858 for the chestnut buds and nests, respectively) that were determined from the pseudo-first-order model were not very satisfactory, which suggests that the pseudo-first-order model is not appropriate for fitting the experimental data as a result of a deviation from linear behavior. In comparison with the pseudo-first-order model, the pseudo-second-order model yields excellent results with higher correlation coefficients ( $R^2 > 0.99$ ). Therefore, it can be concluded that the adsorption of Cd(II) onto both adsorbents displays the best agreement with the pseudo-second-order kinetics model, which revealed that the rate-controlling step might be chemisorption.

In the intraparticle diffusion model, the rate-limiting step is diffusion-controlled. In other words, the rate of adsorption relies on the speed of diffusion of the adsorbate towards the adsorbent. The intraparticle diffusion model, as fitted with the experimental data, is shown in Fig. 20 and the parameters are listed in Table 2. The linear correlation coefficients calculated from the intraparticle diffusion model for both adsorbents are

**Table 2** Experimental conditions and kinetic fitting parameters of intraparticle diffusion model for adsorption of Cd(II) on the chestnut buds and nests

Sample	$C_0$ (mg L <sup>-1</sup> )	Intraparticle diffusion model	
		$K_3$ (g mg <sup>-1</sup> min <sup>-1</sup> )	$R^2$
Chestnut buds	300	12.7686	0.9089
Nests	300	4.5552	0.9027

higher than 0.9, which reveals that the rate-controlling step might be pore diffusion. Comparing all the results of the three kinetics models, it is indicated that the rate-controlling step is a combination of chemisorption and pore diffusion.

### 3.4. Adsorption isotherms

The Langmuir and Freundlich models were employed to analyze the adsorption isotherm of Cd(II).<sup>43</sup> The Langmuir model considers that strong monolayer surface sorption takes place on specific homogeneous sites and no interaction occurs among the adsorbates. The expression of the Langmuir isotherm is as follows:

$$\frac{C_e}{q_e} = \frac{1}{K_L Q} + \frac{1}{Q} C_e, \quad (7)$$

where  $C_e$  (mg L<sup>-1</sup>) represents the equilibrium concentration of Cd(II),  $q_e$  (mg g<sup>-1</sup>) represents the equilibrium adsorption capacity for Cd(II),  $Q$  (mg g<sup>-1</sup>) represents the maximum monolayer adsorption capacity of Cd(II), and  $K_L$  (L mg<sup>-1</sup>) represents the Langmuir adsorption constant.

The Freundlich isotherm is an empirical equation, which usually describes heterogeneous surface adsorption. The common expression is as follows:

$$\log q_e = \log K_F + \frac{1}{n} \log C_e, \quad (8)$$

**Table 3** Isotherm fitting parameters for adsorption of Cd(II) on the chestnut buds and nests

Sample	Langmuir			Freundlich		
	$q_m$ (mg g <sup>-1</sup> )	$K_L$ (L mg <sup>-1</sup> )	$R^2$	$1/n$	$K_F$	$R^2$
Chestnut buds	184.8	$6.31 \times 10^{-2}$	0.997	0.108	91.9	0.774
Nests	131.9	$6.75 \times 10^{-2}$	0.998	0.121	62.6	0.839

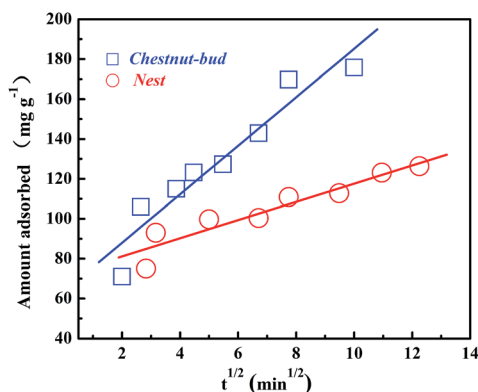
**Fig. 20** Intraparticle diffusion kinetics model for removal of Cd(II) by chestnut buds and nests.

Table 4 Maximum adsorption capacities for Cd(II) of various adsorbents

Adsorbent	BET surface area (m <sup>2</sup> g <sup>-1</sup> )	Removal efficiency (%)	Maximum capacity (mg g <sup>-1</sup> )	Reference
Chinese loess	15	90	9.4	44
Multiwalled carbon nanotubes	36	87	10.9	45
FPBS	214.1	91	38.8	46
Biogenic Fe <sub>3</sub> O <sub>4</sub> nanocomposites	11.3	96.1	49.1	47
γ-FeOOH nanowires	58	87	77.2	48
Cu <sub>3</sub> (BTC) <sub>2</sub> -SO <sub>3</sub> H	445	95	88.7	49
α-Fe <sub>2</sub> O <sub>3</sub> chestnut buds	424.3	93.7	175.8	This work

where  $K_F$  (mg g<sup>-1</sup>) and  $1/n$  represent the Freundlich constants that relate to the adsorbed amount and the adsorption intensity of the adsorbent, respectively.

The results of the Langmuir and Freundlich models, which were determined by curve fitting, are listed in Table 3. It is found that the linear correlation coefficients fitted by the Langmuir model ( $R^2 = 0.997$  and  $0.998$  for the chestnut buds and nests, respectively) are higher than those fitted by the Freundlich model, which indicates that the Langmuir model is preferable for describing the adsorption of Cd(II) on both adsorbents. The simulated Langmuir adsorption behavior shows that there are homogeneous active sites in the chestnut buds and nests and the adsorption process of Cd(II) is a monolayer adsorption reaction.

As listed in Table 4 and illustrated in Fig. 21, in comparison with other adsorbents reported in the literature it is obvious that the adsorbents, in particular the chestnut buds, studied in this work have superior adsorption capacities for Cd(II). Hence, the chestnut buds have great potential for the efficient removal of Cd(II) in the treatment of water pollution.

### 3.5. Reusability studies

An efficient recycling process for an adsorbent must possess the quality of being able to simply release the adsorbate under

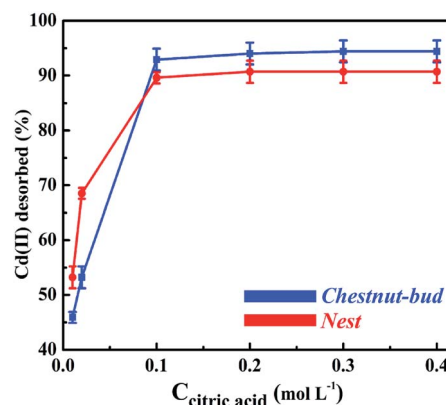


Fig. 22 Recovery of Cd(II) desorbed from the chestnut buds and nests as a function of the citric acid concentration.

mild conditions without damaging the adsorbent itself.<sup>50</sup> For the as-synthesized nanostructured  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> adsorbents, the elution of Cd(II) was performed with citric acid as the eluent. The desorption percentages for Cd(II) adsorbed on the chestnut buds and nests as a function of the citric acid concentration are illustrated in Fig. 22. Approximately 45.9, 53.2, 92.9, 94, 94.4 and 94.4% of Cd(II) adsorbed on chestnut buds was eluted when the citric acid concentration was 0.01, 0.02, 0.1, 0.2, 0.3 and 0.4 mol L<sup>-1</sup>, respectively. It is apparent that 0.2 mol L<sup>-1</sup> citric acid gives the best desorption result. The same tendency was displayed for the nests, which indicates that the best desorption result can be achieved with 0.2 mol L<sup>-1</sup> citric acid as the eluent.

Fig. 23 shows the results for the recovery of Cd(II) desorbed from the chestnut buds and nests as a function of the citric acid concentration. The adsorption capacities of the chestnut buds (Fig. 23A) and nests (Fig. 23B) did not decrease remarkably and remained at 160.0 and 115.2 mg g<sup>-1</sup>, respectively, after three repeated adsorption-desorption cycles using the same adsorbents. It could be concluded that the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles exhibit good regeneration ability, which would decrease the operational cost and expand the range of their sustainable application.

The FT-IR spectra of the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> chestnut buds and nests after three repeated adsorption-desorption cycles were examined to estimate the retention of their surface characteristics. As

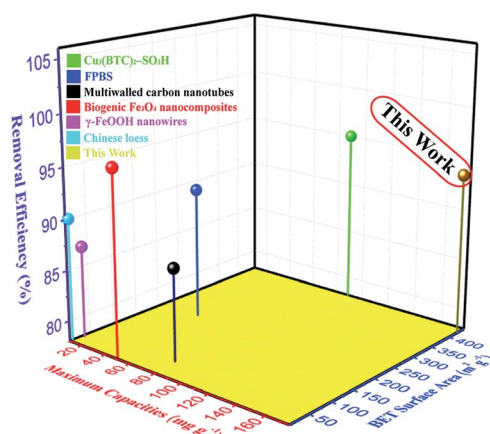


Fig. 21 Summary of adsorption capacities for Cd(II) of several typical adsorbents.



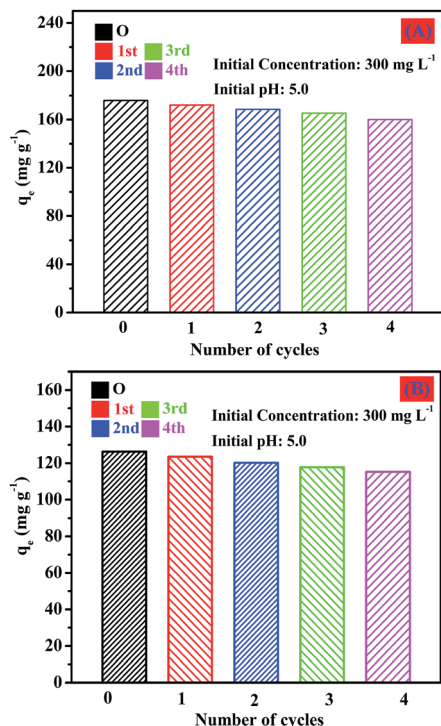


Fig. 23 Reusability of the chestnut buds and nests for adsorption of Cd(II) with 0.2 mol L<sup>-1</sup> citric acid as the eluent.

demonstrated in Fig. 24, the shapes of the peaks in the FT-IR spectra are almost the same as those shown in Fig. 6. It is clearly seen that the corresponding characteristic absorption peaks of O–H stretching vibrations of the surface OH groups (3400 cm<sup>-1</sup>), Fe–O stretching vibrations (480 and 570 cm<sup>-1</sup>) and Fe–OH bending vibrations (1630 cm<sup>-1</sup>) are still present upon repeated recycling. The above results indicate that the surface structure was not damaged during repeated processes of elution with citric acid. Therefore, both adsorbents, namely, chestnut buds and nests, possess excellent potential for sustainable application.

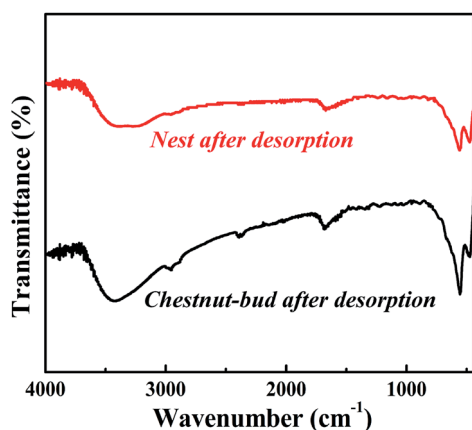


Fig. 24 FT-IR spectra of chestnut buds and nests after desorption.

## 4. Conclusions

We have successfully synthesized two kinds of nanostructured  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> hierarchical hollow spheres, namely, chestnut buds and nests, by a facile solvothermal quasi-reverse-emulsion-templated solvothermal process. Both  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles exhibited highly porous characteristics with specific surface areas of 424.3 and 169.9 m<sup>2</sup> g<sup>-1</sup>, respectively. The pH value of the Cd(II) solution and the initial Cd(II) concentration played significant roles in the adsorption capacity for Cd(II). The adsorption kinetics of Cd(II) showed that the uptake of Cd(II) by both adsorbents was fairly rapid and was in good agreement with the pseudo-second-order model. The adsorption isotherms were well described using the Langmuir isotherm, and the maximum monolayer adsorption capacities for Cd(II) of the chestnut buds and nests were 184.8 and 131.9 mg g<sup>-1</sup>, respectively. Furthermore, the adsorption capacities of the chestnut buds and nests did not decrease markedly and remained at 160.0 and 115.2 mg g<sup>-1</sup>, respectively, after three repeated adsorption–desorption cycles using the same adsorbents. Therefore, the hierarchical  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanoparticles possess promising potential for the treatment of Cd(II) in contaminated water in engineering practice.

## Acknowledgements

This work was supported by the Henan Key Scientific Research Project (16A430026 and 17A150048) and the Nanhu Scholars Program for Young Scholars of XYNU.

## Notes and references

- 1 M. M. Khin, A. S. Nair, V. J. Babu, R. Murugan and S. Ramakrishna, *Energy Environ. Sci.*, 2012, **5**, 8075–8109.
- 2 I. Ali, *Chem. Rev.*, 2012, **112**, 5073–5091.
- 3 L. Gao, J. Chen, C. Tang, Z. Ke, J. Wang, Y. Shimizu and A. Zhu, *Environ. Sci.: Processes Impacts*, 2015, **17**, 1769–1782.
- 4 Y. Hu and H. Cheng, *Environ. Sci. Technol.*, 2013, **47**, 3752–3760.
- 5 M. H. Sun, S. Z. Huang, L. H. Chen, Y. Li, X. Y. Yang, Z. Y. Yuan and B. L. Su, *Chem. Soc. Rev.*, 2016, **45**, 3479–3563.
- 6 J. Lee, S. Mahendra and P. J. J. Alvarez, *ACS Nano*, 2010, **4**, 3580–3590.
- 7 M. Khajeh, S. Laurent and K. Dastafkan, *Chem. Rev.*, 2013, **113**, 7728–7768.
- 8 P. Z. Ray and H. J. Shipley, *RSC Adv.*, 2015, **5**, 29885–29907.
- 9 S. Huang, L. Gu, N. Zhu, K. Feng, H. Yuan, Z. Lou and A. Shan, *Green Chem.*, 2014, **16**, 2696–2705.
- 10 S. Venkateswarlu and M. Yoon, *Dalton Trans.*, 2015, **44**, 18427–18437.
- 11 J. Su, Y. Zhang, S. Xu, S. Wang, H. Ding, S. Pan and H. Zhao, *Nanoscale*, 2014, **6**, 5181–5192.
- 12 J. Chen, F. He, H. Zhang, X. Zhang, G. Zhang and G. Yuan, *Ind. Eng. Chem. Res.*, 2014, **53**, 18481–18488.
- 13 R. Zha, R. Nadimicherla and X. Guo, *J. Mater. Chem. A*, 2014, **2**, 13932–13941.





- 14 J. Qi, X. Lai, J. Wang, H. Tang, H. Ren, Y. Yang and Z. Su, *Chem. Soc. Rev.*, 2015, **44**, 6749–6773.
- 15 R. Purbia and S. Paria, *Nanoscale*, 2015, **7**, 19789–19873.
- 16 G. Tian, Y. Chen, W. Zhou, K. Pan, Y. Dong, C. Tian and H. Fu, *J. Mater. Chem.*, 2011, **21**, 887–892.
- 17 J. H. Pan, X. Zhang, A. J. Du, D. D. Sun and J. O. Leckie, *J. Am. Chem. Soc.*, 2008, **130**, 11256–11257.
- 18 Z. Wei, R. Xing, X. Zhang, S. Liu, H. Yu and P. Li, *ACS Appl. Mater. Interfaces*, 2012, **5**, 598–604.
- 19 B. Wang, H. B. Wu, L. Yu, R. Xu, T. T. Lim and X. W. Lou, *Adv. Mater.*, 2012, **24**, 1111–1116.
- 20 L. S. Zhong, J. S. Hu, H. P. Liang, A. M. Cao, W. G. Song and L. J. Wan, *Adv. Mater.*, 2006, **18**, 2426–2431.
- 21 T. J. Park and S. S. Wong, *Chem. Mater.*, 2006, **18**, 5289–5295.
- 22 K. Simeonidis, S. Mourdikoudis, E. Kaprara, M. Mitrakas and L. Polavarapu, *Environ. Sci.: Water Res. Technol.*, 2016, **2**, 43–70.
- 23 Z. Liu, R. Yu, Y. Dong, W. Li and W. Zhou, *RSC Adv.*, 2016, **6**, 82854–82861.
- 24 E. M. Verdugo, Y. Xie, J. Baltrusaitis and D. M. Cwiertny, *RSC Adv.*, 2016, **6**, 99997–100007.
- 25 X. Hu, J. C. Yu, J. Gong, Q. Li and G. Li, *Adv. Mater.*, 2007, **19**, 2324–2329.
- 26 J. Hu, M. Chen, X. Fang and L. Wu, *Chem. Soc. Rev.*, 2011, **40**, 5472–5491.
- 27 R. Sui and P. Charpentier, *Chem. Rev.*, 2012, **112**, 3057–3082.
- 28 R. Yuan, X. Fu, X. Wang, P. Liu, L. Wu, Y. Xu and Z. Wang, *Chem. Mater.*, 2006, **18**, 4700–4705.
- 29 J. H. Bang and K. S. Suslick, *J. Am. Chem. Soc.*, 2007, **129**, 2242–2243.
- 30 M. Chen, W. Li, X. Shen and G. Diao, *ACS Appl. Mater. Interfaces*, 2014, **6**, 4514–4523.
- 31 S. W. Cao and Y. J. Zhu, *J. Phys. Chem. C*, 2008, **112**, 6253–6257.
- 32 H. G. Yang and H. C. Zeng, *Angew. Chem., Int. Ed.*, 2004, **43**, 5206–5209.
- 33 Z. Ding, G. Q. Lu and P. F. Greenfield, *J. Phys. Chem. B*, 2000, **104**, 4815–4820.
- 34 Y. B. Luan, L. Q. Jing, M. Z. Xie, X. Shi, X. X. Fan, Y. Cao and Y. J. Feng, *Phys. Chem. Chem. Phys.*, 2012, **14**, 1352–1359.
- 35 H. Li, Q. Zhao, X. Li, Y. Shi and G. Chen, *Appl. Surf. Sci.*, 2012, **258**, 7099–7104.
- 36 S. Li, H. Zhang, J. Wu, X. Ma and D. Yang, *Cryst. Growth Des.*, 2006, **6**, 351–353.
- 37 L. S. Zhong, J. S. Hu, H. P. Liang, A. M. Cao, W. G. Song and L. J. Wan, *Adv. Mater.*, 2006, **18**, 2426–2431.
- 38 H. Li, Q. Zhao, X. Li, Y. Shi and G. Chen, *Appl. Surf. Sci.*, 2012, **258**, 7099–7104.
- 39 T. Abe, Y. Kashiwaba, M. Baba, J. Imai and H. Sasaki, *Appl. Surf. Sci.*, 2001, **175**, 549–554.
- 40 D. Chen, W. Shen, S. Wu, C. Chen, X. Luo and L. Guo, *Nanoscale*, 2016, **8**, 7172–7179.
- 41 Y. Pan, Z. Liu, W. Wang, C. Peng, K. Shi and X. Ji, *J. Mater. Chem. A*, 2016, **4**, 2537–2549.
- 42 V. Venkateswaran, P. Kalaamani and N. Karpagam, *Chem. Sci. Trans.*, 2015, **4**, 347–354.
- 43 J. C. Soares, A. C. Soares, P. A. R. Pereira, V. da Cruz Rodrigues, F. M. Shimizu, M. E. Melendez and O. N. Oliveira, *Phys. Chem. Chem. Phys.*, 2016, **18**, 8412–8418.
- 44 Y. Wang, X. W. Tang, Y. M. Chen, L. T. Zhan, Z. Z. Li and Q. Tang, *J. Hazard. Mater.*, 2009, **172**, 30–37.
- 45 Y. H. Li, J. Ding, Z. K. Luan, Z. C. Di, Y. F. Zhu, C. L. Xu, D. H. Wu and B. Q. Wei, *Carbon*, 2003, **41**, 2787–2792.
- 46 T. S. Anirudhan, N. B. Fernandez and M. D. Mullassery, *J. Chem. Technol. Biotechnol.*, 2012, **87**, 714–722.
- 47 S. Venkateswarlu and M. Yoon, *RSC Adv.*, 2015, **5**, 65444–65453.
- 48 L. Liu, L. Q. Yang, H. W. Liang, H. P. Cong, J. Jiang and S. H. Yu, *ACS Nano*, 2013, **7**, 1368–1378.
- 49 Y. Wang, G. Ye, H. Chen, X. Hu, N. Zheng and S. Ma, *J. Mater. Chem. A*, 2015, **3**, 15292.
- 50 L. D. Bitonto, A. Volpe, M. Pagano, G. Bagnuolo, G. Mascolo, V. L. Parola and C. Pastore, *J. Hazard. Mater.*, 2017, **324**, 168–177.

