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Transient alternating current electroosmotic flow of a Jeffrey fluid through a polyelectrolyte-grafted nanochannel

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The purpose of this study is to investigate the flow of viscoelastic fluid through a slit polyelectrolyte-grafted (PE-grafted) nanochannel under applied alternating current (AC) electric field. The PE-grafted nanochannel (also called a soft nanochannel) is represented by a rigid surface coated by a polyelectrolyte layer (PEL) in a brush-like configuration. By solving linearized Poisson–Boltzmann equations and momentum equations, analytical solutions regarding electrical potentials and transient electroosmotic flow (EOF) velocities are derived under appropriate boundary conditions in the decoupled regime of the PE-grafted nanochannel, where the thickness of the PEL is independent of the electrostatic effects triggered by polyelectrolyte charges. We compare the distributions of EOF velocities between PE-grafted and rigid nanochannels. A good agreement with each other is found when the thickness of the PEL is very small. However, the velocity for PE-grafted nanochannels is larger than that for rigid ones. The influences of pertinent dimensionless parameters on the EOF velocities in PE-grafted nanochannels are discussed in detail. The results indicate that the EOF velocity amplitude for PE-grafted nanochannels increases with the thickness of the PEL. Increasing the relaxation time enhances the oscillation of the EOF velocity profiles, yet increasing the retardation time dampens the oscillation. Furthermore, increasing the oscillating Reynolds number Re results in a more obvious oscillating phenomenon of the EOF velocity, together with a weakening amplitude of oscillation. The conclusions have theoretical significance for biofluid-based microfluidic transport systems.

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1. Introduction

The theory of electrokinetics in microelectromechanical systems (MEMS) is of utmost importance in analyzing many chemical, biological and medical devices.^{1,2} Lately, the electrokinetic transport in micro-nano channels has received remarkable attention due to its variety of practical applications. Electroosmotic flow (EOF) is an important electrokinetic phenomenon and has become very attractive in the industrial and biomedical areas. When solid surfaces contact with electrolyte solution, it will cause charge exchange at the solid–liquid interface so as to form the electrical double layer (EDL). When an electric field is applied tangentially to the electrolyte solution, an electric field force acts on the excess counter-ions in the diffuse layer of the EDL. Then the excess counter-ions will migrate under the electric field force, carrying the liquid with them by viscosity, resulting in the electroosmotic flow.³

A rigid nanochannel, in which the inner walls are covered by a layer of polyelectrolyte materials in the form of polyelectrolyte brushes (PE-brushes),^{4–6} is denoted as polyelectrolyte-grafted (PE-grafted) nanochannel (or soft nanochannel). Polyelectrolyte layer

(PEL), containing both electrolyte ions and fixed charge density of ions, is also called fixed charge layer (FCL). It is assumed that electrolyte ions can penetrate into the PEL. Meanwhile, the existing of fixed charge density of ions will result in a drag force on the fluid flow within PEL. Some studies on the electrokinetic theory in soft nanochannel have been reported.^{7–13} Keh and Ding¹⁴ presented an analytical solution about the steady electrokinetic flow in a long uniform soft capillary tube or slit. The results show that the direction and the magnitudes of EOF velocity are governed by the fixed charge density inside the surface polymer layer. Chanda *et al.*¹⁵ investigated the streaming potential and electrochemomechanical energy conversion efficient in soft nanochannel and compared them with those in the rigid nanochannel under the linearization of the Poisson–Boltzmann equation. They found that energy conversion efficient and streaming potential of soft nanochannel are always upper than those of rigid nanochannel except for the particular case of large drag parameter. Chen and Das¹⁶ obtained the streaming potential and electroviscous effects in the soft nanochannel without considering Debye–Hückel approximation. Therefore, they provided a deeper and wider theory for electrokinetic phenomenon in soft nanochannel.

In the previous literatures, many investigations on EOF in microchannels have been reported.^{17–43} Oliveira and Pinho⁴⁴

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presented analytical solutions of Phan-Thien–Tanner (PTT) fluid in fully developed channel and pipe. The results indicated that the wall shear stress of PTT fluid is substantially smaller than the corresponding value of Newtonian or upper-convected Maxwell fluid. The transient behavior of electroosmotic flow under direct current (DC) or alternating current (AC) electric field in a rectangular curved microtube was discussed by Luo.⁴⁵ Chakraborty and Ray⁴⁶ obtained the analytical expression of mass flow rate in circular microchannel under the pulsating electric fields. Wang⁴⁷ presented an analytical solution for the electroosmotic flow in a semicircular microchannel under the Debye–Hückel approximation. The analytical solution of the time periodic electroosmotic flow of Maxwell fluid through a rectangular microchannel was derived by Jian *et al.*⁴⁸ under the Debye–Hückel approximation. Beyond the assumption of linearization approximation, Yang *et al.*⁴⁹ studied the time and space development of EOF in a slit channel. Time periodic electroosmotic flow of Jeffrey fluids between two micro-parallel plates was examined by Liu *et al.*,⁵⁰ semi-analytical solutions are obtained by using the method of separation of variables. Transient electroosmotic flow of Oldroyd-B fluids in a narrow capillary tube was studied by Zhao *et al.*,⁵¹ analytical solutions for electric potential and transient velocity are derived. And the effects of relaxation time and retardation time on the oscillation of the velocity are pointed out.

Recently, Matin and Ohshima⁵² presented the analysis of the flow about Newtonian fluid driven by combined electroosmotic and pressure through a soft nanochannel. Li *et al.*⁵³ investigated the time periodic electroosmotic flow (EOF) of an electrolyte solution through a slit soft nanochannel under applied AC electric field. The results indicated that oscillation of velocity is restricted within the region near the PEL–electrolyte interface for higher oscillating Reynolds number Re . The study of non-Newtonian fluids has gained great interest due to their extensive applications in industry. Materials that do not obey the Newtonian law of viscosity are non-Newtonian fluids. Complex fluids like polymer solutions, colloids, and cell suspensions, which are made of long chain molecules and behave obvious non-Newtonian characteristics, are non-Newtonian fluids. The most common and simplest model of non-Newtonian fluids is Jeffrey fluid which has time derivative instead of convected derivative in the constitutive equation. It should be noted that Jeffrey fluid model is a general viscoelastic model including relaxation time λ_1 and retardation time λ_2 . It includes the classical viscous Newtonian fluid as a special case for $\lambda_1 = 0$, $\lambda_2 = 0$, and the Maxwell fluid for $\lambda_1 \neq 0$, $\lambda_2 = 0$. In addition, Jeffrey fluid model was used to describe the blood flow through a tapered artery.^{54,55} However, there seems almost no report about the transient EOF of viscoelastic fluid through a PE-grafted nanochannel. The present paper is to investigate the transient EOF of Jeffrey fluid through a PE-grafted nanochannel under an external imposed AC electric field. We obtain the analytical solutions of EOF velocity in the PE-grafted nanochannel under Debye–Hückel approximation, and discuss the influences of pertinent dimensionless parameters on the EOF velocity.

2. Mathematical formulation

The unsteady EOF of the incompressible Jeffrey fluid driven by external imposed AC electric field through a PE-grafted nanochannel of height $2h$, as illustrated in Fig. 1, is investigated. We assume that the channel height $2h$ is much smaller than the channel length L and width W , *i.e.*, $2h \ll L, W$. We take a two-dimensional coordinate system where x^* -axis is placed at the middle of two plates. The bottom plate is located at $y^* = -h$, and the top plate is located at $y^* = h$. Therefore, the system only depends on y^* . It is assumed that the PE-grafted nanochannel is represented as a rigid one covered by PEL of thickness d^* , containing positively charged FCL ions, and we suppose that the thickness of PE-brushes is smaller than the half height of nanochannel. Due to the symmetry of channel and electrolyte solution, we only consider the half of the channel ($-h \leq y^* \leq 0$).

2.1 Distribution of the electrostatic potential

According to the electrostatic theory, the distribution of electrical potential ψ^* in the EDL can be described by the following Poisson–Boltzmann equations in decoupled regime^{6,56} of PE-grafted nanochannel, where the thickness of PEL is independent of the electrostatic effects triggered by polyelectrolyte charges.

$$\frac{d^2\psi^*(y^*)}{dy^{*2}} = -\frac{\rho_e}{\varepsilon}, \quad -h + d^* \leq y^* \leq 0, \quad (1a)$$

$$\frac{d^2\psi^*(y^*)}{dy^{*2}} = -\frac{\rho_e + ZeN}{\varepsilon}, \quad -h \leq y^* \leq -h + d^*, \quad (1b)$$

where $-h \leq y^* \leq -h + d^*$ denotes the PEL region, ε is the dielectric constant of the electrolyte liquid which is assumed to be identical both inside and outside PEL,¹⁶ $\rho_e = -2en_0 \sinh(ez\psi^*/(k_B T))$ is the free charge density in the electrolyte, e is the elementary electronic charge, z is the absolute value of the ionic valence, n_0 is the number concentration of electrolyte solution, k_B and T are the Boltzmann constant and temperature. Z and N are the valence and the ionic number concentration of the FCL ions. It is assumed that the electrical potential is small compared with the thermal energy of the ions, that is, $\exp[\pm(ez\psi^*)/(k_B T)]$ can be replaced by $1 \pm (ez\psi^*)/(k_B T)$, then eqn (1a) and (1b) become

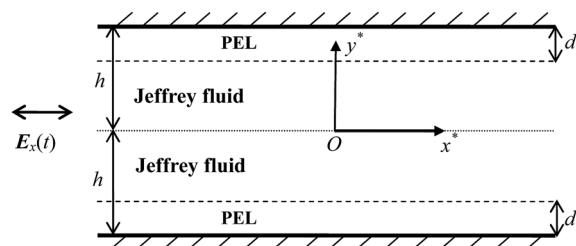


Fig. 1 Schematic of Jeffrey fluid driven by AC electric field in PE-grafted nanochannel.



$$\frac{d^2\psi^*}{dy^{*2}} = \frac{\psi^*}{\lambda^{*2}}, \quad -h + d^* \leq y^* \leq 0, \quad (2a)$$

$$\frac{d^2\psi^*}{dy^{*2}} = \frac{\psi^*}{\lambda^{*2}} - \frac{\psi_s}{\lambda_F^{*2}}, \quad -h \leq y^* \leq -h + d^*. \quad (2b)$$

In eqn (2a) and (2b), $\lambda^* = [(\epsilon k_B T)/(2n_\infty e^2 z^2)]^{1/2}$ is the EDL thickness, $\lambda_F^* = [(\epsilon k_B T)/(Ne^2 zZ)]^{1/2}$ is the equivalent EDL thickness inside PEL and $\psi_s = k_B T/ez$. The corresponding boundary conditions are

$$\left. \frac{d\psi^*}{dy^*} \right|_{y^*=0} = 0, \quad \psi^*|_{y^*=-h+d^*} = \psi^*|_{y^*=-h+d^*}^+, \quad \left. \frac{d\psi^*}{dy^*} \right|_{y^*=-h+d^*} = \left. \frac{d\psi^*}{dy^*} \right|_{y^*=-h+d^*}^+, \quad \psi^*|_{y^*=-h} = \zeta^*. \quad (3)$$

To make a direct comparison between the PE-grafted and rigid nanochannels, the last boundary condition in eqn (3) gives the wall electrical potential ζ^* at the interface of PEL and wall, which is different from previous boundary condition.^{15,16,52} Introducing the following dimensionless variations $\psi = \psi^*/\psi_s$, $y = y^*/h$, $d = d^*/h$, $\lambda = \lambda^*/h$ and $\lambda_F = \lambda_F^*/h$, we obtain the following equations and boundary conditions about the dimensionless electrical potential ψ

$$\frac{d^2\psi}{dy^2} - \frac{\psi}{\lambda^2} = 0, \quad -1 + d \leq y \leq 0, \quad (4a)$$

$$\frac{d^2\psi}{dy^2} - \frac{\psi}{\lambda^2} = -\frac{1}{\lambda^2 K^2}, \quad -1 \leq y \leq -1 + d. \quad (4b)$$

$$\left. \frac{d\psi}{dy} \right|_{y=0} = 0, \quad \psi|_{y=(-1+d)^-} = \psi|_{y=(-1+d)^+}, \quad \left. \frac{d\psi}{dy} \right|_{y=(-1+d)^-} = \left. \frac{d\psi}{dy} \right|_{y=(-1+d)^+}, \quad \psi|_{y=-1} = \zeta, \quad (5)$$

here $K = \lambda_F/\lambda$ represents the ratio of the characteristic thickness of the mobile charges in the bulk electrolyte to that in the FCL. $\zeta = \zeta^*/\psi_s$ is the dimensionless wall electrical potential at the PEL-wall interface. The solutions of eqn (4a) and (4b) under the boundary conditions (5) are

$$\psi(y) = B_1 \cosh(y/\lambda), \quad -1 + d \leq y \leq 0, \quad (6a)$$

$$\psi(y) = B_3 \cosh(y/\lambda) + B_4 \sinh(y/\lambda) + \frac{1}{K^2}, \quad -1 \leq y \leq -1 + d, \quad (6b)$$

$$B_1 = B_3 - B_4 \frac{\cosh(D)}{\sinh(D)}, \quad B_3 = \frac{1}{\cosh(1/\lambda)} \left[B_4 \sinh(1/\lambda) + \zeta - \frac{1}{K^2} \right],$$

$$B_4 = -\frac{\sinh(D)}{K^2}, \quad D = 1/\lambda - d/\lambda.$$

2.2 Distribution of the velocity field

We assume that the pressure gradient along the axial direction is ignored. When an external electric field $E_x(t)$ is applied, a pure

EOF of Jeffrey fluid through a PE-grafted nanochannel is governed by the modified momentum equations, *i.e.*,

$$\rho \frac{\partial u^*(y^*, t)}{\partial t} = \frac{\partial \tau_{yx}^*}{\partial y^*} + \rho_e E_x(t), \quad -h + d^* \leq y^* \leq 0, \quad (7a)$$

$$\rho \frac{\partial u^*(y^*, t)}{\partial t} = \frac{\partial \tau_{yx}^*}{\partial y^*} + \rho_e E_x(t) - \mu_c u^*(y^*, t), \quad -h \leq y^* \leq -h + d^*, \quad (7b)$$

where $u^*(y^*, t)$ is the axial velocity, t is time, $E_x(t)$ is the applied AC electric field, $\rho_e E_x(t)$ is the electric field force, ρ is the fluid density, μ_c is the drag coefficient within PEL, τ_{yx}^* is the stress tensor which satisfies the constitutive equation of the Jeffrey fluid.

$$\tau_{yx}^* + \lambda_1 \partial \tau_{yx}^* / \partial t = \mu (\partial u^* / \partial y^* + \lambda_2 \partial^2 u^* / \partial y^{*2} \partial t), \quad (8)$$

where λ_1 is the relaxation time, λ_2 is the retardation time, μ is the zero shear rate viscosity. Generally, the retardation time is smaller than the relaxation time.⁵⁷ When the relaxation time λ_1 and the retardation time λ_2 tend to zero, eqn (8) reduces to the constitutive equation of the Newtonian fluid. We assume that AC electric field and the EOF velocity of Jeffrey fluid can be written in the following complex forms:

$$E_x(t) = \mathcal{R}\{E_0 e^{i\omega t}\}, \quad u^*(y^*, t) = \mathcal{R}\{u_0^*(y^*) e^{i\omega t}\}, \quad (9)$$

where $\mathcal{R}\{\}$ denotes the real part of a complex number, E_0 is the amplitude of the applied AC electric field and $u_0^*(y^*)$ is the complex amplitude of EOF velocity, i is the imaginary number unit and ω is the oscillating angular frequency of the applied AC electric field. Combining eqn (7a), (7b) and (8), eliminating stress tensor τ_{yx}^* , it yields:

$$\frac{d^2 u_0^*}{dy^{*2}} - \frac{i\rho\omega}{\mu} \frac{1 + i\omega\lambda_1}{1 + i\omega\lambda_2} u_0^* = \frac{\epsilon E_0}{\mu} \frac{1 + i\omega\lambda_1}{1 + i\omega\lambda_2} \frac{\psi^*}{\lambda^{*2}}, \quad -h + d^* \leq y^* \leq 0, \quad (10a)$$

$$\frac{d^2 u_0^*}{dy^{*2}} - \left(\frac{i\rho\omega}{\mu} + \frac{\mu_c}{\mu} \right) \frac{1 + i\omega\lambda_1}{1 + i\omega\lambda_2} u_0^* = \frac{\epsilon E_0}{\mu} \frac{1 + i\omega\lambda_1}{1 + i\omega\lambda_2} \frac{\psi^*}{\lambda^{*2}}, \quad -h \leq y^* \leq -h + d^* \quad (10b)$$

Boundary conditions are given by

$$\left. \frac{du_0^*}{dy^*} \right|_{y^*=0} = 0, \quad u_0^*|_{y^*=-h+d^*} = u_0^*|_{y^*=-h+d^*}^+, \quad \left. \tau_{yx}^* \right|_{y^*=-h+d^*} = \left. \tau_{yx}^* \right|_{y^*=-h+d^*}^+, \quad u_0^*|_{y^*=-h} = 0. \quad (11)$$

In above boundary conditions, the first condition represents the symmetric velocity about x^* axis. The second and third conditions imply the continuity for the velocity and shear stress at the interface of the FCL–electrolyte. No-slip condition of the velocity is satisfied in the last condition. Notice that the continuous condition for the shear stress reduces to the condition $\left. \frac{du_0^*}{dy^*} \right|_{y^*=-h+d^*} = \left. \frac{du_0^*}{dy^*} \right|_{y^*=-h+d^*}^+$. In fact, substituting eqn (9) into (8), dividing by λ_1 , we obtain



$$\frac{\tau_{yx}^*}{\lambda_1} + \frac{d\tau_{yx}^*}{dt} = \frac{\mu}{\lambda_1} \frac{du_0^*}{dy^*} \mathcal{R} \{ (1 + i\omega\lambda_2) e^{i\omega t} \}. \quad (12)$$

Then, by integrating eqn (12) and assuming that the fluid is in unstressed state at $t = -\infty$, we get the expression of shear stress

$$\tau_{yx}^* = \mu \frac{du_0^*}{dy^*} \mathcal{R} \left\{ \frac{1 + i\omega\lambda_2}{1 + i\omega\lambda_1} e^{i\omega t} \right\}. \quad (13)$$

Dimensionless velocity is introduced by $u_0 = u_0^*/U_{eo}$, where $U_{eo} = \varepsilon E_0 \psi_s / \mu$ denotes steady Helmholtz–Smoluchowski EOF velocity of Newtonian fluid. eqn (10a) and (10b) and corresponding boundary conditions (11) in the dimensionless form are

$$\frac{d^2 u_0}{dy^2} - i\text{Re}\beta^2 u_0 = \frac{\beta^2 \psi}{\lambda^2} = \frac{\beta^2 B_1}{\lambda^2} \cosh(y/\lambda), \quad -1 + d \leq y \leq 0, \quad (14a)$$

$$\begin{aligned} \frac{d^2 u_0}{dy^2} - (\alpha^2 + i\text{Re})\beta^2 u_0 &= \frac{\beta^2 \psi}{\lambda^2} \\ &= \frac{\beta^2 B_3}{\lambda^2} \cosh(y/\lambda) + \frac{\beta^2 B_4}{\lambda^2} \sinh(y/\lambda) \\ &\quad + \frac{\beta^2}{\lambda^2 K^2}, \quad -1 \leq y \leq -1 + d, \end{aligned} \quad (14b)$$

$$\begin{aligned} \left. \frac{du_0}{dy} \right|_{y=0} &= 0, \quad u_0|_{y=(-1+d)^-} = u_0|_{y=(-1+d)^+}, \quad \left. \frac{du_0}{dy} \right|_{y=(-1+d)^-} \\ &= \left. \frac{du_0}{dy} \right|_{y=(-1+d)^+}, \quad u_0|_{y=-1} = 0, \end{aligned} \quad (15)$$

where $\text{Re} = \rho\omega h^2/\mu$ is oscillating Reynolds number, $\alpha^2 = \mu_c h^2/\mu$ is dimensionless drag parameter, and $\beta^2 = (1 + i\omega\lambda_1)/(1 + i\omega\lambda_2)$. The solutions of eqn (14a) and (14b) are

$$u_0(y) = C_1 \cosh(\sqrt{i\text{Re}\beta}y) + C_2 \cosh(y/\lambda), \quad -1 + d \leq y \leq 0, \quad (16a)$$

$$\begin{aligned} u_0(y) &= D_1 \cosh(\sqrt{\alpha^2 + i\text{Re}\beta}y) + D_2 \sinh(\sqrt{\alpha^2 + i\text{Re}\beta}y) \\ &\quad + D_3 \cosh(y/\lambda) + D_4 \sinh(y/\lambda) + D_5, \quad -1 \leq y \leq -1 + d, \end{aligned} \quad (16b)$$

where

$$\begin{aligned} C_1 &= \frac{1}{\cosh(\gamma_1)} [D_1 \cosh(\gamma_2) + D_2 \sinh(\gamma_2) + D_3 \cosh(D) \\ &\quad - D_4 \sinh(D) + D_5 - C_2 \cosh(D)], \end{aligned}$$

$$C_2 = \frac{\beta^2 B_1}{1 - i\text{Re}\beta^2 \lambda^2},$$

$$\begin{aligned} D_1 &= \frac{1}{\cosh(\sqrt{\alpha^2 + i\text{Re}\beta})} \left[D_2 \sinh(\sqrt{\alpha^2 + i\text{Re}\beta}) - D_5 \right. \\ &\quad \left. - D_3 \cosh(1/\lambda) + D_4 \sinh(1/\lambda) \right], \end{aligned}$$

$$D_2 = \frac{1}{M_5} (C_2 M_3 + D_3 M_6 - D_4 M_7 + D_5 M_8),$$

$$D_3 = \frac{\beta^2 B_3}{1 - (\alpha^2 + i\text{Re})\beta^2 \lambda^2}, \quad D_4 = \frac{\beta^2 B_4}{1 - (\alpha^2 + i\text{Re})\beta^2 \lambda^2},$$

$$D_5 = -\frac{1}{(\alpha^2 + i\text{Re})K^2 \lambda^2}.$$

We use the following notations in the above coefficients:

$$\gamma_1 = \sqrt{i\text{Re}\beta}(-1 + d), \quad \gamma_2 = \sqrt{\alpha^2 + i\text{Re}\beta}(-1 + d),$$

$$M_1 = \sqrt{i\text{Re}\beta} \sinh(\gamma_1) \cosh(\gamma_2) - \sqrt{\alpha^2 + i\text{Re}\beta} \cosh(\gamma_1) \sinh(\gamma_2),$$

$$M_2 = \sqrt{i\text{Re}\beta} \sinh(\gamma_1) \sinh(\gamma_2) - \sqrt{\alpha^2 + i\text{Re}\beta} \cosh(\gamma_1) \cosh(\gamma_2),$$

$$M_3 = \sqrt{i\text{Re}\beta} \sinh(\gamma_1) \cosh(D) + \frac{1}{\lambda} \cosh(\gamma_1) \sinh(D),$$

$$M_4 = \sqrt{i\text{Re}\beta} \sinh(\gamma_1) \sinh(D) + \frac{1}{\lambda} \cosh(\gamma_1) \cosh(D),$$

$$M_5 = \frac{\sinh(\sqrt{\alpha^2 + i\text{Re}\beta})}{\cosh(\sqrt{\alpha^2 + i\text{Re}\beta})} M_1 + M_2,$$

$$M_6 = \frac{\cosh(1/\lambda) M_1}{\cosh(\sqrt{\alpha^2 + i\text{Re}\beta})} - M_3,$$

$$M_7 = \frac{\sinh(1/\lambda) M_1}{\cosh(\sqrt{\alpha^2 + i\text{Re}\beta})} - M_4,$$

$$M_8 = \frac{M_1}{\cosh(\sqrt{\alpha^2 + i\text{Re}\beta})} - \sqrt{i\text{Re}\beta} \sinh(\gamma_1).$$

3. Results and discussions

Analytical solutions are derived for the transient EOF of Jeffrey fluid through a PE-grafted nanochannel. Next, we will discuss the influences of pertinent parameters (d , K , λ , Re , $\lambda_1\omega$, $\lambda_2\omega$, ωt) on the EOF velocity. In practical engineering problems, typical parameters are taken as follows: the half height of the channel is $h \sim 100$ nm, $\rho \sim 1.06 \times 10^3$ kg m⁻³, $\mu \sim 10^{-3}$ kg (m⁻¹ s⁻¹), the AC electric field frequency changes from 0 to 400 MHz, then the angle frequency ω is from 0 to 2.5×10^9 s⁻¹. The oscillating



Reynolds number Re varies from 0 to 25 due to $Re = \rho\omega h^2/\mu$. In addition, according to the previous studies,^{15,16,52} we let $\alpha = 1$, $d/\lambda \leq 1$. Generally speaking, the retardation time λ_2 is smaller than the relaxation time λ_1 , and λ_1 should be smaller than the oscillating period of the electric field,⁵⁰ that is, $\lambda_2\omega < \lambda_1\omega \leq 2\pi$. In the following figures, letters S and R represent the PE-grafted and rigid nanochannels, respectively. The meanings of all symbols in the present paper are listed in Table 1.

Fig. 2 provides the variation of the dimensionless electrical potential ψ with dimensionless distance y for different values of the K , d and ζ when $\lambda = 0.1$. In Fig. 2a, $K = 0.1, 1$ and 10 , $d = 0.1$ and 0.05 , $\zeta = 1$. It is shown that the parameter $K = \lambda_F/\lambda$ should be taken larger than 1 to ensure the validity of Debye–Hückel linearization. In the following discussion, we always let $K \geq 1$. If the thickness of PEL in the PE-grafted nanochannel is very small ($d = 0.01$), Fig. 2b compares the electrical potential in PE-grafted and rigid nanochannels when $K = 1, 10$ and $\zeta = 1, 0.8$. It is observed that coincident profiles of electrical potential for PE-grafted and rigid nanochannels are plotted under the same wall electrical potential.

Fig. 3 compares the velocity amplitude $u_0(y)$ for Newtonian, Jeffrey and Maxwell fluids in PE-grafted and rigid nanochannels at different values of PEL thickness d when $\lambda = 0.1, K = 1, \zeta = 1, Re = 8$ ($d = 0.01$ in Fig. 3a and $d = 0.1$ in Fig. 3b). Noted that $\lambda_1\omega = 0, \lambda_2\omega = 0$; $\lambda_1\omega = 2\pi, \lambda_2\omega = 0.5\pi$ and $\lambda_1\omega = 2\pi, \lambda_2\omega = 0$ correspond to Newtonian fluid; Jeffrey fluid and Maxwell fluid,

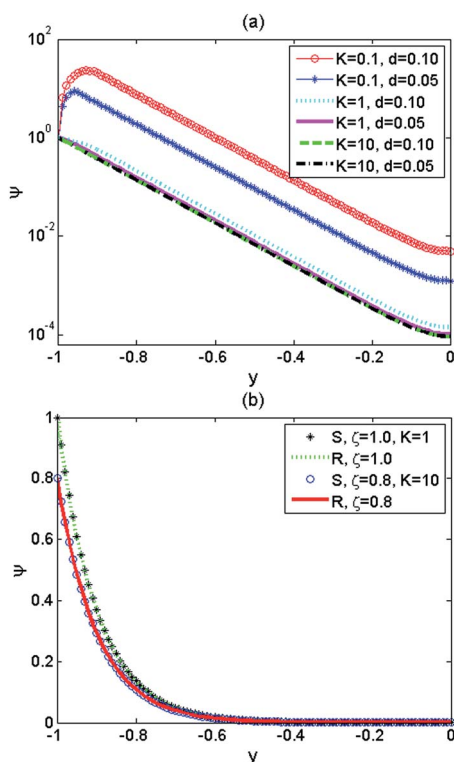


Fig. 2 Variation of the dimensionless electrical potential ψ with dimensionless distance y for different values of the d and K when $\lambda = 0.1$ (a) in the PE-grafted nanochannel ($d = 0.10, 0.05, \zeta = 1$), (b) the comparison between PE-grafted and rigid nanochannel ($d = 0.01, \zeta = 1.0, 0.8, K = 1, 10$).

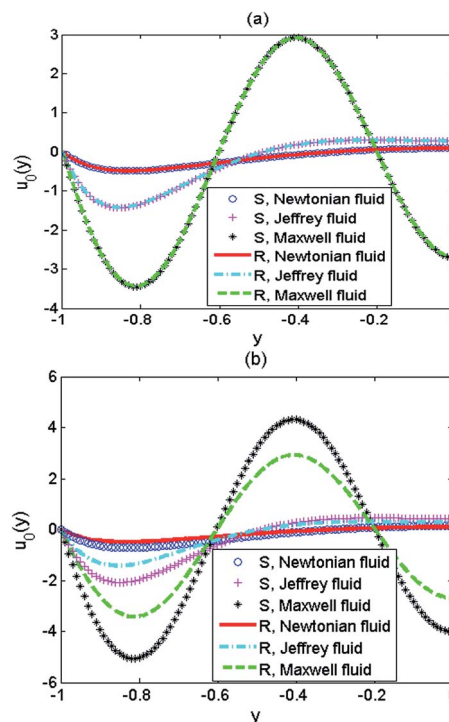


Fig. 3 Comparison of the velocity amplitude for Newtonian, Maxwell and Jeffrey fluids in PE-grafted and rigid nanochannels ($\lambda = 0.1, K = 1, \zeta = 1, Re = 8$) at different values of d : (a) $d = 0.01$, (b) $d = 0.1$. For Newtonian fluid $\lambda_1\omega = 0, \lambda_2\omega = 0$; for Jeffrey fluid $\lambda_1\omega = 2\pi, \lambda_2\omega = 0.5\pi$; for Maxwell fluid $\lambda_1\omega = 2\pi, \lambda_2\omega = 0$.

respectively. When the thickness of PEL in the PE-grafted nanochannel is very thin ($d = 0.01$), the profiles of velocity amplitude for the PE-grafted nanochannel agree very well with those for the rigid nanochannel (see Fig. 3a). However, for thick PEL thickness ($d = 0.1$), the velocity in the PE-grafted nanochannel is substantially larger than that in the rigid nanochannel whenever the values of $\lambda_1\omega$ and $\lambda_2\omega$ (see Fig. 3b). Among them, the increment of velocity for Maxwell fluid ($\lambda_1\omega = 2\pi, \lambda_2\omega = 0$) is more obvious than Newtonian and Jeffrey fluids. Under the influence of AC electric field, negative values maybe emerge in the EOF velocity profile, which mean the backflow of the fluid.

Fig. 4 illustrates the velocity amplitude $u_0(y)$ at different values of d, λ and K when $Re = 1, \zeta = 1, \lambda_1\omega = 2\pi, \lambda_2\omega = 0.5\pi$. In Fig. 4a, $d = 0.01, 0.05$ and $0.10, \lambda = 0.10, K = 1$; in Fig. 4b, $d = 0.10, \lambda = 0.10, 0.15, 0.20, K = 1, 10$. As shown in the figure, the velocity amplitude increases with d , but decreases with λ and K . Physically, in the PE-grafted nanochannel, PEL is a layer comprising polyelectrolyte materials, which contains both electrolyte ions and fixed charge density of positive ions. Under the action of an applied electric field, an increase in the thickness of the PEL (d) accompanies the increment of the cations, and therefore promotes the fluid flow. The increase of the EDL thickness (λ) means the augmentation of ionic density inside the EDL, which indicates the accumulation of the ions and leads to a high resistance in the fluid flow, together with the decline of the velocity. The increase of parameter K ($K = \lambda_F/\lambda$)



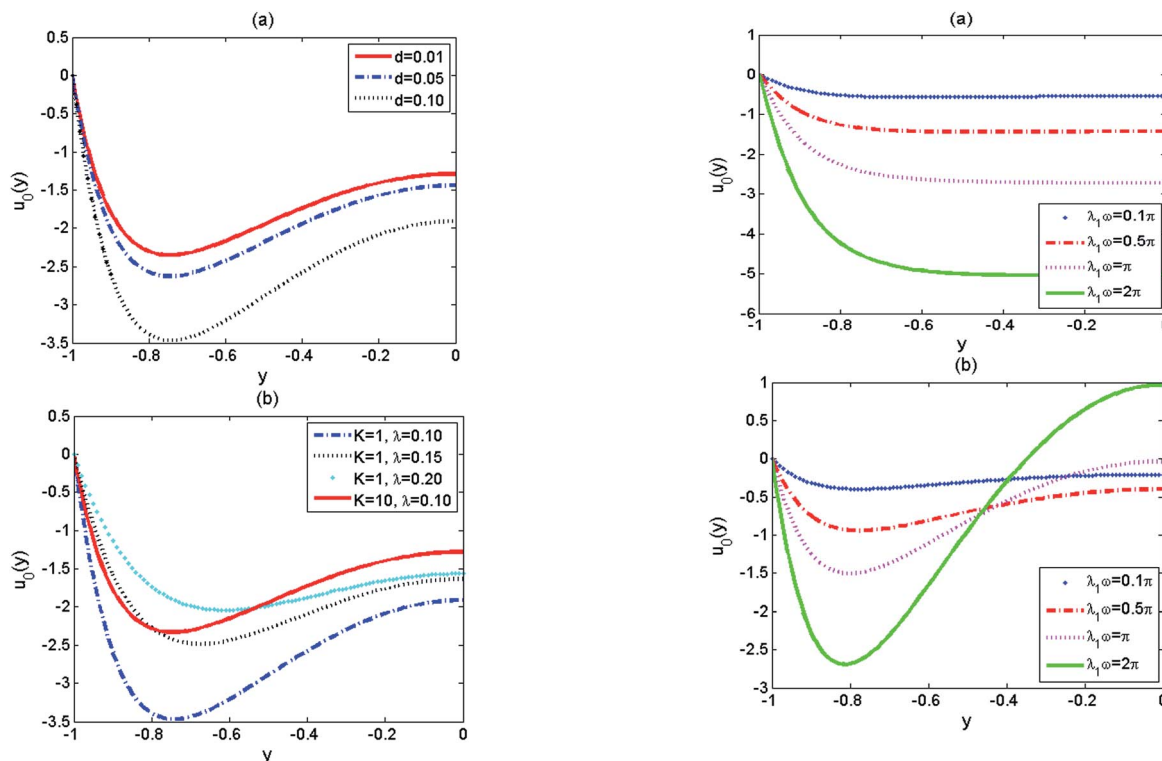


Fig. 4 Dimensionless velocity amplitude $u_0(y)$ at different values of d , λ and K when $Re = 1$, $\zeta = 1$, $\lambda_1\omega = 2\pi$, $\lambda_2\omega = 0.5\pi$ (a) $d = 0.01, 0.05, 0.10$, $\lambda = 0.10$, $K = 1$, (b) $d = 0.10$, $\lambda = 0.10, 0.15, 0.20$, $K = 1, 10$.

corresponds to the decrease of electrical potential ψ due to low ionic concentration inside the PEL, therefore, the velocity would decrease with K according to the dimensionless momentum eqn (14a) and (14b).

Fig. 5 and 6 describe the effects of the relaxation time and retardation time on the velocity amplitude $u_0(y)$ of the Jeffrey fluid for different oscillating Reynolds number Re (0.5, 3, 10, and 25) in the PE-grafted nanochannel. In Fig. 5, different values of relaxation time $\lambda_1\omega$ (0.1π , 0.5π , π , 2π) are discussed, and Fig. 6 considers different retardation time $\lambda_2\omega$ (0.1π , 0.3π , 0.5π). It can be observed from Fig. 5 and 6, with the increase of the oscillating Reynolds number Re , the velocity profiles gradually present oscillating characteristic, and the oscillating amplitude of velocity tends to be lessening whether at high or low values of relaxation time and retardation time. It is pointed out that near the region of EDL and the interface of liquid–PEL, the oscillation phenomenon of the velocity becomes particularly obvious for large oscillating Reynolds number Re . And yet, the EOF velocities are almost zero at the region far away from the EDL (see Fig. 5c and d and 6c and d). Physically, it is because that the diffusion time is much longer than the oscillating period in the case of high oscillating frequency. Therefore, the velocities near the centre of the channel are almost zero. Furthermore, according to profiles of velocity amplitude in Fig. 5 and 6, the velocity increases with $\lambda_1\omega$ due to large elastic effect. However, the profile of velocity decreases with $\lambda_2\omega$ due to large retard effect of Jeffrey fluid. Therefore, the increase of

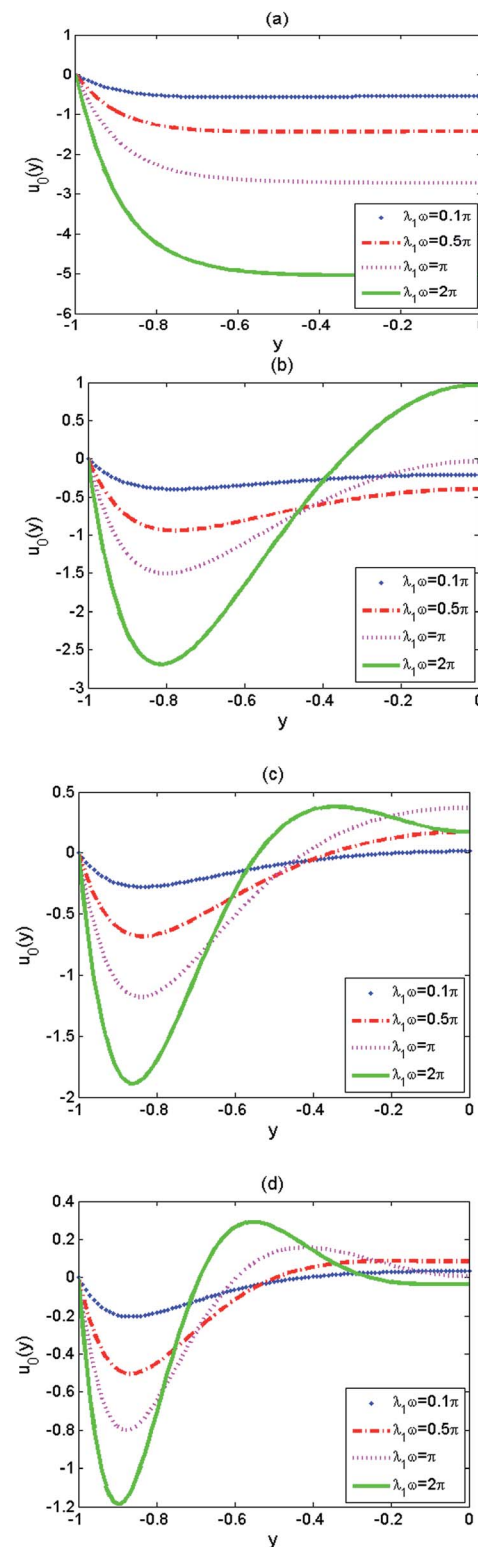


Fig. 5 Dimensionless velocity amplitude $u_0(y)$ at different values of $\lambda_1\omega$ ($\lambda_1\omega = 0.1\pi, 0.5\pi, \pi, 2\pi$) when $d = 0.1$, $\lambda = 0.1$, $K = 1$, $\zeta = 1$ and $\lambda_2\omega = 0.5\pi$ corresponding to (a) $Re = 0.5$, (b) $Re = 3$, (c) $Re = 10$, (d) $Re = 25$.

relaxation time enhances the oscillation of EOF velocity. On the contrary, the increase of retardation time dampens the oscillation.



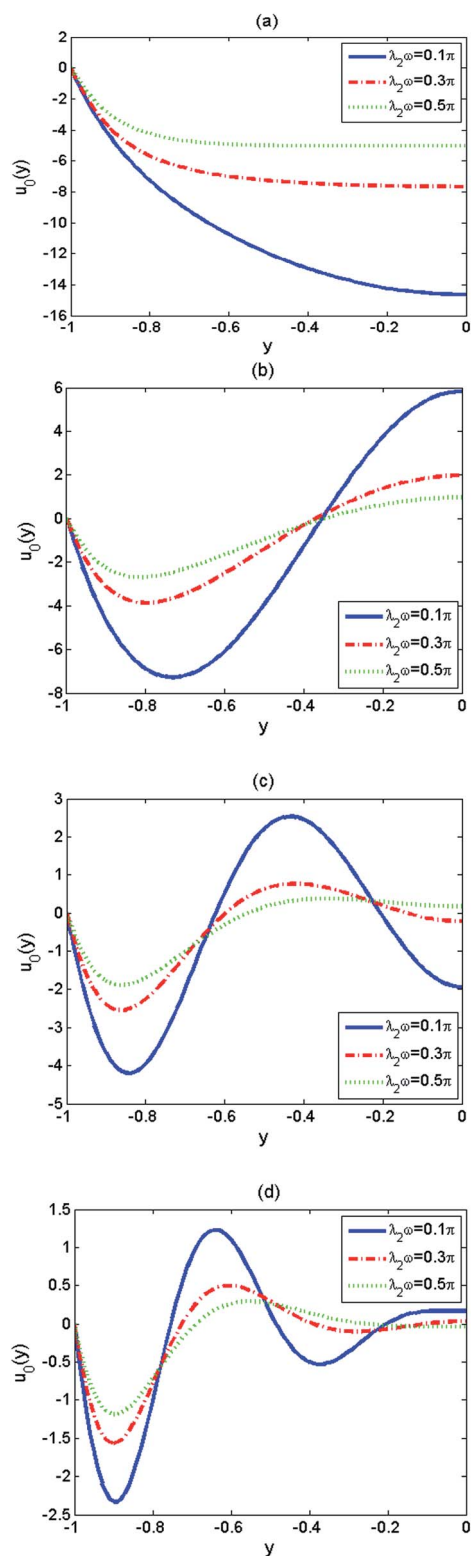


Fig. 6 Dimensionless velocity amplitude $u_0(y)$ at different values of $\lambda_2\omega$ ($\lambda_2\omega = 0.1\pi, 0.3\pi, 0.5\pi$) when $d = 0.1, \lambda = 0.1, K = 1, \zeta = 1$ and $\lambda_1\omega = 2\pi$ corresponding to (a) $Re = 0.5$, (b) $Re = 3$, (c) $Re = 10$, (d) $Re = 25$.

The variation of transient velocity with time is an important characteristic of unsteady electroosmotic flow. Fig. 7 depicts the EOF velocity profiles $u(y, t)$ of the Jeffrey fluid as a function of

Table 1 List of symbols

Symbol	Meaning
d^*	Thickness of PEL (m)
d	Dimensionless thickness of PEL
$E_x(t)$	AC electric field ($V m^{-1}$)
E_0	Amplitude of AC electric field ($V m^{-1}$)
e	Elementary electronic charge (C)
h	Half height of soft nanochannel (m)
i	Imaginary number unit
K	Ratio of characteristic thickness, $K = \lambda_F/\lambda$
k_B	Boltzmann constant ($J K^{-1}$)
L	Length of the soft nanochannel (m)
N	Ionic number concentration of the FCL ions (m^{-3})
n_0	Number concentration of electrolyte solution (m^{-3})
Re	Oscillating Reynolds number, $Re = \rho\omega h^2/\mu$
R	Rigid nanochannel
S	Soft nanochannel (PE-grafted nanochannel)
T	Temperature (K)
t	Time (s)
$u^*(y^*, t)$	Axial velocity for soft nanochannel ($m s^{-1}$)
$u_0^*(y^*)$	Amplitude of velocity for soft nanochannel ($m s^{-1}$)
$u_0(y)$	Dimensionless amplitude of velocity for soft nanochannel
$u_r(y, t)$	Dimensionless axial velocity for rigid nanochannel
$u_{r0}(y)$	Dimensionless amplitude of velocity for rigid nanochannel
U_{eo}	Helmholtz–Smoluchowski velocity of Newtonian fluids ($m s^{-1}$)
W	Width of the soft nanochannel (m)
x^*, y^*	Coordinates
x, y	Dimensionless coordinates
Z	Valence of the FCL ions
z	The absolute value of the ionic valence
α	Dimensionless drag parameter, $\alpha^2 = \mu_c h^2/\mu$
β	Dimensionless parameter, $\beta^2 = (1 + i\omega\lambda_1)/(1 + i\omega\lambda_2)$
ψ^*	Electrical potential (V)
ψ	Dimensionless electrical potential
$\psi_r(y)$	Electrical potential for rigid nanochannel (V)
ψ_s	Characteristics of electrical potential (V), $\psi_s = k_B T/ez$
ε	Dielectric constant ($N m^{-1}$)
ρ_e	Free charge density ($C m^{-3}$), $\rho_e = -2ezn_0 \sinh(ez\psi^*/k_B T)$
λ^*	Thickness of EDL (m), $\lambda^* = [(\varepsilon k_B T)/(2n_\infty e^2 z^2)]^{1/2}$
λ	Dimensionless thickness of EDL
λ_F^*	Equivalent EDL thickness inside PEL (m), $\lambda_F^* = [(\varepsilon k_B T)/(N e^2 z Z)]^{1/2}$
λ_F	Dimensionless equivalent EDL thickness inside PEL
ζ^*	Wall electrical potential at the interface of PEL and wall (V)
ζ	Dimensionless wall electrical potential
ρ	Fluid density ($kg m^{-3}$)
μ_c	Drag coefficient within PEL
τ_{yx}^*	Stress tensor of Jeffrey fluid ($N m^{-2}$)
λ_1	Relaxation time (s)
λ_2	Retardation time (s)
μ	Zero shear rate viscosity ($kg m^{-1} s^{-1}$)
ω	Oscillating angular frequency of the applied AC electric field (s^{-1})



time (t) for different oscillating Reynolds number Re (0.5, 3, 10, and 25) in the PE-grafted nanochannel. From Fig. 7, it is evident that for lower oscillating Reynolds number, the flow can extend

to the whole PE-grafted nanochannel. However, with the increasing of oscillating Reynolds number, near the interface of liquid–PEL, the oscillating characteristic of velocity become obvious gradually. In the case of large oscillating Reynolds number, EOF velocity far away from the interface of liquid–PEL almost maintains zero at any time. These phenomena for Jeffrey fluid are similar to those for Newtonian fluid in the PE-grafted.⁵³

4. Conclusions

An analytical transient EOF of Jeffrey fluid under external applied AC electric field in a PE-grafted nanochannel is presented in this work. Based on the Debye–Hückel approximation, we arrive at the analytical solutions involving the momentum equations and the constitutive equation of the Jeffrey fluid. By comparing the electrical potentials and EOF velocities between PE-grafted and rigid nanochannels, it can be found that electrical potentials and EOF velocities in PE-grafted nanochannel with thin PEL are in excellent agreement with those in rigid nanochannel. In PE-grafted nanochannel, the PEL has the positive role of increasing the velocity amplitude. However, the amplitude of EOF velocity decreases with EDL thickness λ and parameter K . Moreover, with the increase of oscillating Reynolds number Re , the oscillating phenomenon of EOF velocity becomes obvious, and the weakening amplitude of oscillation is observed. In the case of high oscillating frequency, the EOF velocities are almost zero at the region far away from the interface of liquid–PEL. It is observed that relaxation time of Jeffrey fluid enhances the oscillation of velocity. However, the retardation time dampens the oscillation of velocity. The results have theoretical significance for biofluids-based microfluidic transport system.

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References

- 1 H. A. Stone, A. D. Stroock and A. Ajdari, *Annu. Rev. Fluid Mech.*, 2004, **36**, 381.
- 2 T. Bayraktar and S. B. Pidugu, *Int. J. Heat Mass Transfer*, 2006, **49**, 815.
- 3 R. J. Hunter, *Zeta potential in colloid science*, Academic Press, New York, 1981.
- 4 Y. B. Zhulina, V. A. Pryamitsyn and O. V. Borisov, *Polym. Sci. U.S.S.R.*, 1989, **31**, 205.
- 5 S. T. Milner, *Science*, 1991, **251**, 905.
- 6 S. Das, M. Banik, G. Chen, S. Sinha and R. Mukherjee, *Soft Matter*, 2015, **11**, 8550.
- 7 E. Donath and E. Voigt, *J. Colloid Interface Sci.*, 1986, **109**, 122.

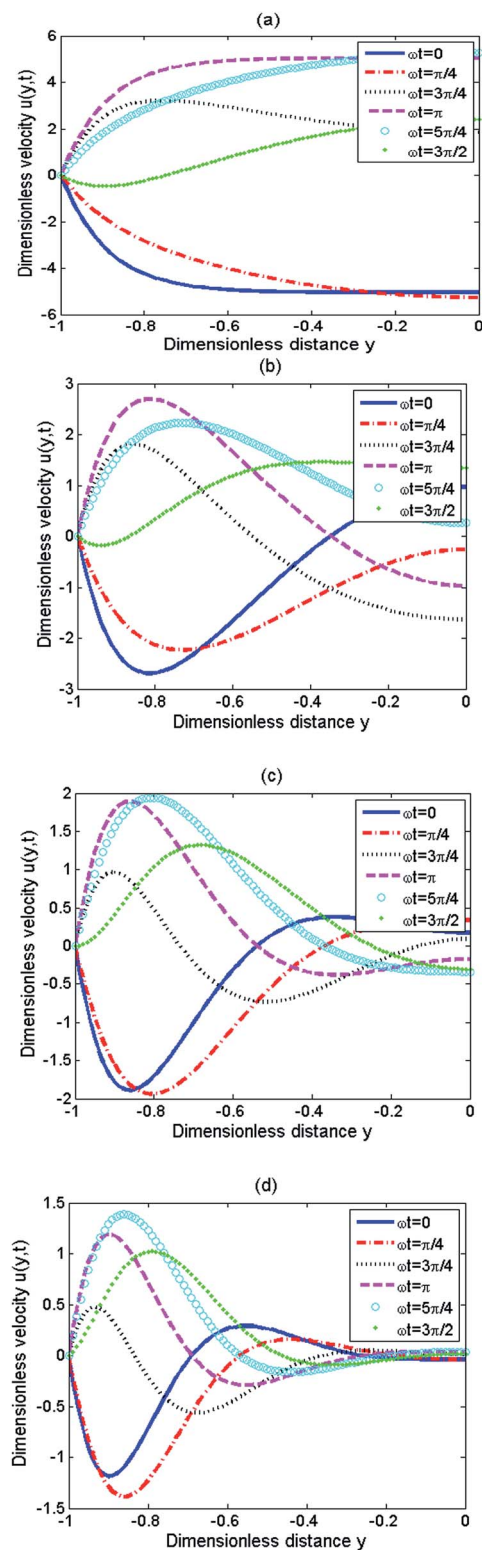


Fig. 7 Dimensionless velocity $u(y,t)$ at different values of ωt ($\omega t = 0, \pi/4, 3\pi/4, \pi, 5\pi/4, 3\pi/2$) when $d = 0.1, \lambda = 0.1, K = 1, \zeta = 1$ and $\lambda_1\omega = 2\pi, \lambda_2\omega = 0.5\pi$ corresponding to (a) $Re = 0.5$, (b) $Re = 3$, (c) $Re = 10$, (d) $Re = 25$.



- 8 H. Ohshima and T. Kondo, *J. Colloid Interface Sci.*, 1990, **135**, 443.
- 9 E. Donath, P. Kuzmin, A. Krabi and A. Voigt, *Colloid Polym. Sci.*, 1993, **271**, 930.
- 10 H. J. Keh and Y. C. Liu, *J. Colloid Interface Sci.*, 1995, **172**, 222.
- 11 J. H. Wu and H. J. Keh, *Colloids Surf., A*, 2003, **212**, 27.
- 12 J. F. L. Duval and H. P. van Leeuwen, *Langmuir*, 2004, **20**, 10324.
- 13 H. C. Ma and H. J. Keh, *J. Colloid Interface Sci.*, 2007, **313**, 686.
- 14 H. J. Keh and J. M. Ding, *J. Colloid Interface Sci.*, 2003, **263**, 645.
- 15 S. Chanda, S. Sinhab and S. Das, *Soft Matter*, 2014, **10**, 7558.
- 16 G. Chen and S. Das, *J. Colloid Interface Sci.*, 2015, **445**, 357.
- 17 D. Burgreen and F. R. Nakache, *J. Phys. Chem.*, 1964, **68**, 1084.
- 18 S. Levine, J. R. Marriott, G. Neale and N. Epstein, *J. Colloid Interface Sci.*, 1975, **52**, 136.
- 19 C. Yang, D. Li and J. H. Masliyah, *Int. J. Heat Mass Transfer*, 1998, **41**, 4229.
- 20 S. Arulanandam and D. Li, *Colloids Surf., A*, 2000, **161**, 89.
- 21 S. Chakraborty, *Int. J. Heat Mass Transfer*, 2006, **49**, 810.
- 22 Y. J. Kang, C. Yang and X. Y. Huang, *J. Colloid Interface Sci.*, 2002, **253**, 285.
- 23 H. K. Tsao, *J. Colloid Interface Sci.*, 2000, **225**, 247.
- 24 A. Sharma and S. Chakraborty, *Int. J. Heat Mass Transfer*, 2008, **51**, 4875.
- 25 A. M. Afonso, M. A. Alves and F. T. Pinho, *J. Non-Newtonian Fluid Mech.*, 2009, **159**, 50.
- 26 S. Dhinakaran, A. M. Afonso, M. A. Alves and F. T. Pinho, *J. Colloid Interface Sci.*, 2010, **344**, 513.
- 27 S. Chakraborty and A. K. Srivastava, *Langmuir*, 2007, **23**, 12421.
- 28 Y. Jian, L. Yang and Q. Liu, *Phys. Fluids*, 2010, **22**, 042001.
- 29 S. Das and S. Chakraborty, *AIChE J.*, 2007, **53**, 1086.
- 30 S. Das, K. Subramanian and S. Chakraborty, *Colloids Surf., B*, 2007, **58**, 203.
- 31 C. C. Chang and C. Y. Wang, *Electrophoresis*, 2008, **29**, 2970.
- 32 N. Scales and R. N. Tait, *J. Chem. Phys.*, 2006, **125**, 094714.
- 33 D. Erickson and D. Li, *Langmuir*, 2003, **19**, 5421.
- 34 Q. Liu, Y. Jian and L. Yang, *J. Non-Newtonian Fluid Mech.*, 2011, **166**, 478.
- 35 X. X. Li, Z. Yin, Y. J. Jian, L. Chang, J. Su and Q. S. Liu, *J. Non-Newtonian Fluid Mech.*, 2012, **187–188**, 43.
- 36 P. Dutta and A. Beskok, *Anal. Chem.*, 2001, **73**, 5097.
- 37 H. J. Keh and H. C. Tseng, *J. Colloid Interface Sci.*, 2001, **242**, 450.
- 38 Y. J. Kang, C. Yang and X. Y. Huang, *Int. J. Eng. Sci.*, 2002, **40**, 2203.
- 39 W.-J. Luo, *J. Colloid Interface Sci.*, 2006, **295**, 551.
- 40 B. Gheshlaghi, H. Nazaripoor, A. Kumar and M. Sadrzadeh, *RSC Adv.*, 2016, **6**, 17632.
- 41 G. C. Shit, A. Mondal, A. Sinha and P. K. Kundu, *Colloids Surf., A*, 2016, **489**, 249.
- 42 L. Martínez, O. Bautista, J. Escandón and F. Méndez, *Colloids Surf., A*, 2016, **498**, 7.
- 43 J. Marroquin-Desentis, F. Méndez and O. Bautista, *Fluid Dynam. Res.*, 2016, **48**, 035503.
- 44 P. J. Oliveira and F. T. Pinho, *J. Fluid Mech.*, 1999, **387**, 271.
- 45 W.-J. Luo, *J. Colloid Interface Sci.*, 2004, **278**, 497.
- 46 S. Chakraborty and S. Ray, *Phys. Fluids*, 2008, **20**, 083602.
- 47 C. Y. Wang, Y. H. Liu and C. C. Chang, *Phys. Fluids*, 2008, **20**, 3105.
- 48 Y. Jian, Q. Liu and L. Yang, *J. Non-Newtonian Fluid Mech.*, 2011, **166**, 1304.
- 49 C. Yang, K. T. Ooi, T. N. Wong and J. H. Masliyah, *J. Colloid Interface Sci.*, 2004, **275**, 679.
- 50 Q. Liu, Y. Jian and L. Yang, *Phys. Fluids*, 2011, **23**, 102001.
- 51 M. Zhao, S. Wang and S. Wei, *J. Non-Newtonian Fluid Mech.*, 2013, **201**, 135.
- 52 M. H. Matin and H. Ohshima, *J. Colloid Interface Sci.*, 2015, **460**, 361.
- 53 F. Li, Y. Jian, L. Chang, G. Zhao and L. Yang, *Colloids Surf., B*, 2016, **147**, 234.
- 54 N. S. Akbar and S. Nadeem, *Commun. Theor. Phys.*, 2012, **57**, 133.
- 55 R. Ellahi, S. U. Rahman and S. Nadeem, *Phys. Lett. A*, 2014, **378**, 2973.
- 56 G. Chen and S. Das, *J. Phys. Chem. B*, 2015, **119**, 12714.
- 57 R. B. Bird, W. E. Stewart and E. N. Lightfoot, *Transport phenomena*, John Wiley & Sons, Inc., New York, 2nd edn, 2001.

