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# *In situ* stabilizer formation from methacrylic acid macromonomers in emulsion polymerization†

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Oligomers of methacrylic acid containing a propenyl  $\omega$ -endgroup (*i.e.* MAA-macromonomers) were synthesized by cobalt-mediated catalytic chain transfer polymerization and used as precursors to stabilizers in emulsion polymerization. It was found that only in those polymerizations in which these precursors were sufficiently quickly converted into amphiphilic molecules, *via* a type of polymerization induced self-assembly (PISA) mechanism, stable emulsion polymerization could be carried out. This process was too slow in the emulsion polymerization of methyl methacrylate (MMA) and in order to obtain stable latexes, the addition of a conventional surfactant (sodium dodecyl sulphate, SDS) was necessary. In the emulsion polymerization of butyl acrylate, however, reactions with the macromonomers were faster and because of the more hydrophobic nature of BA (as compared to MMA), stabilizers were sufficiently quickly formed *in situ* and stable latexes were produced without the need for additional SDS. Also the emulsion polymerization of butyl methacrylate (BMA), which reacts *via* the same "sulfur-free RAFT" mechanism as MMA, could be carried out in the absence of SDS because of the greater hydrophobicity of the monomer. Copolymerizations of MMA with >30% of BA or 85% BMA also resulted in stable latexes without the addition of SDS. The synthesized macromonomers and *in situ* formed copolymers were characterized by means of size exclusion chromatography (SEC),  $^1\text{H}$  NMR spectroscopy and MALDI-ToF MS.

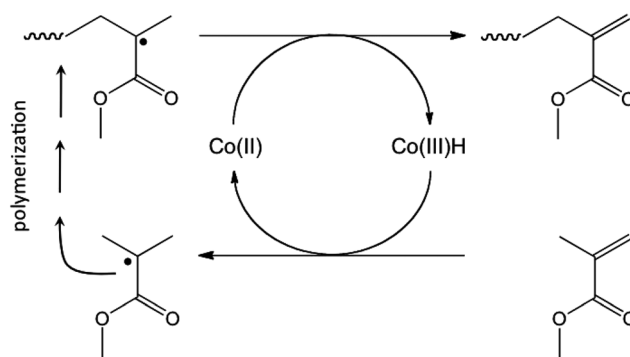
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## Introduction

Polymer latexes prepared by emulsion polymerization have found and are continuously finding applications in many fields, ranging from coatings and adhesives to biomedical applications.<sup>1–3</sup> In emulsion polymerization surfactants play an important role in controlling the particle diameter, the stability and the surface functionality of the formed latex particles. During latex film formation, surfactants can migrate from the surface of the particles towards the film interface and may have a negative effect on final film properties such as water sensitivity, gloss, adhesion and blocking.<sup>4–7</sup> A generally employed strategy used to circumvent these problems is the use of reactive surfactants which are chemically bound to the polymer particles.<sup>8–11</sup> On the one hand an ideal reactive surfactant should not be too reactive during emulsion polymerization at low monomer conversion to avoid burying of the surfactant groups inside the latex particles and/or the formation of water-soluble polymer chains that cause bridging floccula-

tion.<sup>12</sup> On the other hand, all of the surfactants should have reacted by the end of the polymerization so that a stable latex with bound surfactants is obtained.<sup>13</sup> Surfactants containing a propenyl end-group would be promising candidates displaying just the right reactivity. Oligomers containing these end-groups (called macromonomers in the remainder of this paper) are readily prepared *via* Co-mediated catalytic chain transfer (CCT)<sup>14–16</sup> (see Scheme 1) and their subsequent copolymerization behavior has been described previously.<sup>17–19</sup> In earlier



**Scheme 1** Schematic representation of the Co-mediated CCT polymerization of methacrylates.

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studies also, amphiphilic macromonomers were synthesized and subsequently used as stabilizers in emulsion polymerization.<sup>20,21</sup>

In the current study, methacrylic acid macromonomers (synthesized *via* the Co-mediated CCT polymerization of *t*-butyl methacrylate followed by acidolysis of the *t*-butyl groups) are used as precursors to stabilizing agents in the emulsion polymerization of methacrylates and acrylates. Both acrylates and methacrylates were used because it is known that methacrylic macromonomers react differently with these two classes of monomers<sup>14,22</sup> and will yield reactive surfactants with different architectures. The macromonomers will react *via* an addition–fragmentation chain transfer mechanism with methacrylates and the process will result in surface-active block copolymers. In fact it is exactly this mechanism (in combination with low monomer concentrations) that has recently been coined “sulfur-free RAFT” by Haddleton and co-workers,<sup>23,24</sup> and was recently used by Zetterlund and co-workers<sup>25</sup> in a “non-living version” of polymerization induced self-assembly (PISA).<sup>26</sup> With acrylates the macromonomers will ultimately yield graft copolymers.<sup>14</sup> The influence of the length and the added amount of macromonomers on the particle size of the latex particles and on the stability of the final latex will be examined. Also the influence of the architecture of the *in situ* formed copolymer on these properties will be discussed.

## Experimental

### Materials

All monomers, methyl methacrylate (MMA), *n*-butyl acrylate (BA), *n*-butyl methacrylate (BMA), ethyl acrylate (EA) and *tert*-butyl methacrylate (*t*-BMA), were obtained from Sigma-Aldrich (99%). The monomers were passed over a column of an inhibitor remover (Aldrich) to remove the inhibitor. Azobis(isobutyronitrile) (AIBN, Merck) was recrystallized from methanol. The bis-methanol complex of cobaloxime boron fluoride (COBF) was prepared as described previously<sup>27</sup> (measured  $C_T$  for MMA in bulk =  $34 \times 10^3$  at 60 °C). Toluene (AR, Biosolve), dichloromethane (DCM, AR, Biosolve) and trifluoro acetic acid (TFA, 95%, Aldrich) were all used as received. Sodium dodecyl sulfate (SDS, 99%), potassium persulfate (KPS, p.a.) and sodium carbonate (dehydrated, p.a.) were purchased from Merck and used as received.

### Synthesis of the *t*-butyl methacrylate macromonomer

For the *t*-butyl methacrylate macromonomer (*t*-BMA-MM) synthesis, *t*-BMA was polymerized with AIBN in toluene in a round-bottom flask at 60 °C.<sup>28</sup> The initially added amount of the COBF catalyst was varied to obtain macromonomers with different molecular weights. In a typical experiment the procedure is as follows: 141 g *t*-BMA (1.0 mol) and 200 g toluene (2.2 mol) were deoxygenated by purging for 30 minutes with nitrogen at 0 °C in a flask (A) sealed airtight with a septum. To a separate flask (B), fitted with a magnetic stirring bar, 600 mg

**Table 1** Characteristics of *t*-BMA and MAA macromonomers

#	[COBF]/ [ <i>t</i> -BMA]	<i>t</i> -BMA-MM			MAA-MM $DP_n^b$	Sample name
		$DP_n^a$	$D^a$	$DP_n^b$		
1	$3.0 \times 10^{-6}$	14 ± 5	1.9	17 ± 1	17 ± 3	MAA <sub>16</sub>
2	$2.4 \times 10^{-6}$	80 ± 12	2.3	70 ± 4	80 ± 8	MAA <sub>80</sub>
3	$0.9 \times 10^{-6}$	350 ± 24	2.0	330 ± 25	335 ± 25	MAA <sub>350</sub>

<sup>a</sup> Determined *via* SEC using appropriate Mark-Houwink constants to convert the polystyrene calibration curve,<sup>29</sup> for samples 1 and 2  $DP_n = M_w/(2 \times 142)$ ,<sup>30</sup> for sample 3  $DP_n = M_n/142$ . <sup>b</sup> From <sup>1</sup>H NMR.

AIBN ( $3.7 \times 10^{-3}$  mol) and 10 mg COBF ( $2.6 \times 10^{-5}$  mol) were added; the flask was consecutively evacuated and purged with nitrogen three times.

Then the monomer solution A was added to flask B *via* a cannula and the solution was heated to 60 °C. The reaction mixture was left with continuous stirring for 24 h. The *t*-BMA-MM was isolated by evaporation of toluene and residual monomer under reduced pressure and subsequently dried in a vacuum oven at 60 °C for 24 h (120 g yield, 85%). The molar mass distributions and the number-average degrees of polymerization ( $DP_n$ ) were determined by SEC and <sup>1</sup>H NMR, and the results are summarized in Table 1 (see ESI† for more details).

### Synthesis of the methacrylic acid macromonomer

For the synthesis of the MAA macromonomer (MAA-MM), *t*-BMA-MM was acidolized using trifluoroacetic acid (TFA) in dichloromethane (DCM). A typical procedure is as follows: a round-bottom flask fitted with a magnetic stirring bar was charged with *t*-BMA-MM (100 g,  $M_n^{SEC} = 2300$  g mol<sup>-1</sup>,  $D = 1.9$ ) and DCM (100 mL). The mixture was stirred until the polymer was dissolved after which TFA (100 mL, 1.3 mol) was added. Subsequently, the mixture was allowed to stir at room temperature for 48 h. DCM and excess TFA were removed by evaporation under reduced pressure and the resulting polymer was dried in a vacuum oven at 60 °C for 2 days to yield the MAA-MM (60 g yield, 100%). The number-average degrees of polymerization were determined *via* <sup>1</sup>H NMR, and the results are summarized in Table 1.

### Emulsion polymerization

Emulsion polymerizations were carried out in both batch and semi-batch operation. All experiments were carried out under argon in a jacketed and baffled glass reactor (250 mL), thermostated at 60 °C and equipped with a mechanical four-bladed turbine stirrer. The monomer conversions during and after the reaction were determined gravimetrically.

For the batch emulsion polymerizations all ingredients except the initiator solution were charged into the reactor, stirred at 350 rpm, purged with argon for 30 minutes and subsequently heated to 60 °C. Five minutes after reaching a constant temperature, an aqueous KPS solution (10 mL containing 0.08 g of KPS) was injected to initiate the polymerization.



For the semi-batch emulsion polymerizations the reactor was charged with water, buffer, stabilizer(s) and 3 g of the monomer (*i.e.* 10% of the overall monomer content), stirred at 350 rpm, purged with argon for 30 minutes and subsequently heated to 60 °C. Five minutes after reaching a constant temperature, an aqueous KPS solution (10 mL containing 0.08 g of KPS) was injected to initiate the polymerization. Starting 1 h after initiation, the remaining monomer (27 g) was added at a constant feeding rate of 5 mL h<sup>-1</sup>.

Particle size distributions were determined by dynamic light scattering (DLS) and some of the latexes were examined using scanning (SEM) and transmission electron microscopy (TEM).

## Analysis

**Size exclusion chromatography.** Size exclusion chromatography (SEC) for low molecular weight macromonomers was carried out using a Waters 2695 separation module equipped with an auto-injector, a Polymer Laboratories 5.0 μm bead size guard column (50 mm × 7.5 mm), followed by two 5.0 μm bead size PL columns in series of 500 Å and 100 Å, respectively, and a Waters 2414 differential refractive index detector (40 °C). The injection volume used was 50 μL and tetrahydrofuran (Biosolve, stabilized with BHT) was used as the eluent at a flow rate of 1.0 mL min<sup>-1</sup>. The SEC system was calibrated using linear polystyrene standards (Polymer Laboratories,  $M_n = 370 \text{ g mol}^{-1} - M_n = 4 \times 10^4 \text{ g mol}^{-1}$ ).

SEC for high molecular weight macromonomers and polymers was carried out using a Waters Alliance system equipped with a Waters 2695 separation module, a Waters 2414 refractive index detector (40 °C), a Waters 2487 dual UV absorbance detector, a PSS SDV 5 μm bead size guard column along with two PSS SDV 5 μm bead size linear XL columns in series (300 × 8 mm) at 40 °C. Tetrahydrofuran (THF stabilized with BHT, Biosolve) with 1 v/v% acetic acid was used as the eluent at a flow rate of 1.0 mL min<sup>-1</sup>. The system was calibrated with polystyrene standards (Polymer Laboratories,  $M_n = 580 \text{ g mol}^{-1} - M_n = 7.1 \times 10^6 \text{ g mol}^{-1}$ ), after which correction was applied using the appropriate Mark-Houwink parameters (polystyrene:  $K_{ps} = 1.14 \times 10^{-4} \text{ dL g}^{-1}$ ,  $a_{ps} = 0.716$  and poly(*tert*-butyl methacrylate)  $K_{pL-BMA} = 5.84 \times 10^{-5} \text{ dL g}^{-1}$ ,  $a_{pL-BMA} = 0.76$ ).<sup>29</sup>

**Nuclear magnetic resonance.** <sup>1</sup>H NMR spectra were recorded on a Varian MercuryVx spectrometer at 400 MHz. Chloroform-*d*<sub>1</sub>, methanol-*d*<sub>4</sub> and tetra methyl silane were used as solvents and internal standard, respectively. For methacrylic acid macromonomers in methanol-*d*<sub>4</sub> suppression of the water peak at 4.88 ppm was applied.

**MALDI-ToF MS.** MALDI-ToF MS spectra were recorded using a PerSeptive Biosystems Voyager-DE STR MALDI-TOF MS spectrometer equipped with 2 m flight tubes for linear mode, 3 m flight tubes for reflector mode and a 337 nm nitrogen laser (3 ns pulse). All mass spectra were obtained with an accelerating potential of 20 kV in positive ion and reflector modes with delayed extraction. Data were processed using Voyager software. 2,4,6-Trihydroxyacetophenone (THAP) (80 mg mL<sup>-1</sup> THF or methanol) and di-ammonium hydrogen

citrate (DAC) (5 mg mL<sup>-1</sup> THF or methanol) were used as the matrix and cationating agent, respectively. The acrylate polymer samples were dissolved in THF and methacrylic acid containing polymer samples were dissolved in methanol at concentrations of 5 mg mL<sup>-1</sup> solvent. Analyte solutions were prepared by mixing the matrix, salt and polymer at a 4 : 1 : 4 volume ratio. Subsequently, 0.30 μL of this mixture was spotted on the sample plate, and the spots were dried at room temperature.

**Dynamic light scattering.** Dynamic light scattering (DLS) analyses were performed on a Nanotracs Ultra (Microtracs systems) system. The used laser is a gallium-aluminum-arsenide semiconductor diode laser with a wavelength of 780 nm and a power of 3–5 mW. The angle of incident-to-scattered light is 180° (backscatter). This technique uses the Brownian motion of the molecules. The cumulants algorithm was used to obtain the particle size distribution from the second order autocorrelation function. The mean diameter was evaluated from the Stokes–Einstein equation for spheres (according to International standards ISO22412<sup>31</sup> and ISO13321<sup>32</sup>).

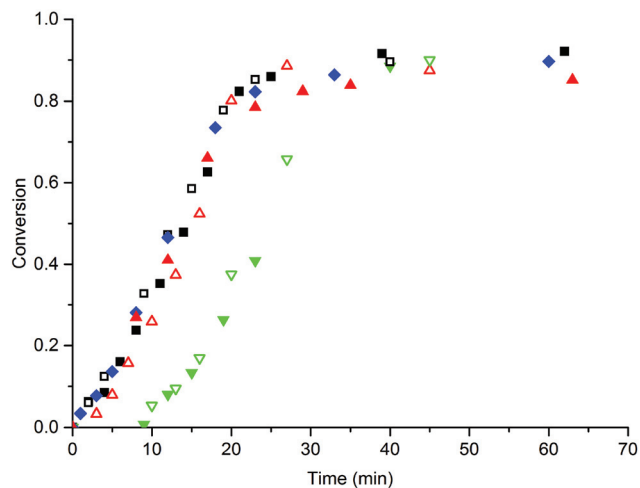
**Scanning electron microscopy and (cryogenic) transmission electron microscopy.** Scanning electron microscopy (SEM) micrographs were obtained using a FEI Quanta 3D FEG instrument with an acceleration voltage of 5 kV. Latexes were gold-coated prior to scanning. (Cryogenic) transmission electron microscopy (cryo-TEM and TEM) measurements were performed on an FEI Tecnai 20, type Sphera TEM instrument equipped with a LaB<sub>6</sub> filament operating at 200 kV. Images were recorded with a bottom-mounted Gatan CCD camera. For cryo-TEM, the sample vitrification procedure was carried out using an automated vitrification robot (FEI Vitrobot Mark III). A 3 μL sample was applied on a Quantifoil grid (R 2/2, Quantifoil Micro Tools GmbH; freshly glow-discharged just prior to use), excess liquid was blotted away, and the formed thin film was shot into melting ethane. The grid containing the vitrified film was immediately transferred to a cryoholder (Gatan 626) and observed at –170 °C.

## Results and discussion

### Emulsion polymerization of methyl methacrylate

First, the emulsion polymerization of MMA in the presence of MAA macromonomers was investigated. In the initial experiments we used SDS to ensure sufficient stabilization of the latex particles and investigated the co-stabilizing effect of the MAA macromonomers. The effects of the amount and the chain length of the MAA macromonomers on the polymerization rate, the particle formation and the particle size distribution in the emulsion polymerization were studied; the macromonomer amount was varied between 1 and 4 wt% and chain lengths ( $DP_n$ ) of 16, 80 and 350 were used. In all cases SDS was added at a concentration of 10 mM (= 1.5 wt%), which is just above its critical micelle concentration (CMC = 9.5 mM at 60 °C).<sup>33</sup> A comparative experiment without the





**Fig. 1** Conversion-time curve of the emulsion polymerization of MMA in the presence of 1.5 wt% (= 10 mM) SDS. The polymerizations were performed in the absence of a macromonomer (◆), 1 wt% (open symbols) and 4 wt% (closed symbols) MAA<sub>16</sub> (■), MAA<sub>80</sub> (▲) and MAA<sub>350</sub> (▼). Standard polymerization conditions as listed in Table 2.

macromonomer was also performed. The conversion *versus* time curves were measured and the results are shown in Fig. 1. All polymerizations proceeded to high monomer conversion and resulted in stable latexes without significant amounts of coagulum.

From the results shown in Fig. 1, it is immediately clear that the addition of MAA<sub>16</sub> or MAA<sub>80</sub> to the system does not significantly affect the polymerization rate as compared to the system that is only stabilized by SDS; only the addition of MAA<sub>350</sub> results in a significantly delay in the onset of polymerization, but then proceeds with a polymerization rate similar to the other systems (the conversion rate  $\approx 0.040 \pm 0.005 \text{ min}^{-1}$  during interval II in all cases). These similar rates imply that the particle numbers are also similar in all reactions ( $N_p \approx (1.3 \pm 0.3) \times 10^{17} \text{ L}^{-1}$ ), determined from  $D_n$ , which in turn suggests that SDS is the main stabilizer in all these reactions, without any significant contribution from the macromonomers. The initial delay in the MAA<sub>350</sub> systems is conceivably explained by the fact that these longer hydrophilic chains

**Table 2** Standard recipe for a (semi-) batch emulsion polymerization;  $T = 60 \text{ }^\circ\text{C}$ , stirring speed = 350 rpm

Ingredient	Amount
Water	120 g
Na <sub>2</sub> CO <sub>3</sub>	0.4 g (0.02 M)
Macromonomer	1.5 g (5 wt% <sup>b</sup> , varied between 0–11 wt%)
SDS	0.3 g (1.5 wt% <sup>b</sup> , varied between 0–1.5 wt%)
Monomer <sup>a</sup>	30 g (solids content 20%)
KPS	0.08 g (0.25 wt% <sup>b</sup> ; $2.5 \times 10^{-3} \text{ M}$ )

<sup>a</sup> Batch: all monomer was added at the start; semi-batch: 10% of the monomer was added initially, the remaining monomer was added at a rate of  $5 \text{ mL h}^{-1}$ , starting 1 h after initiation. <sup>b</sup> wt% = weight percentage relative to the monomer (= g per 100 g of monomer).

**Table 3** Summary of final particle diameters of pMMA latexes stabilized by 1.5 wt% SDS and MAA-MM

	MAA-MM (wt%)	DLS		SEM <sup>a</sup> $D_n$ (nm)
		$D_n$ (nm)	PdI	
MAA <sub>16</sub>	1	56	0.47	$88 \pm 10$
	4	72	0.10	$87 \pm 5$
MAA <sub>80</sub>	1	58	0.75	$86 \pm 13$
	4	68	0.25	$85 \pm 9$
MAA <sub>350</sub>	1	41	0.13	$76 \pm 12$
	4	75	0.24	$86 \pm 12$
Only SDS	0	73	0.30	$78 \pm 8$

<sup>a</sup> Number mean particle diameter calculated after particle count >100.

require the addition of more hydrophobic MMA units before they become surface-active and as such initially act as a kind of “propagating radical sink”. This is supported by the observation that during the experiments with MAA<sub>350</sub> the viscosity of the latex increased because of flocculation, which is indicative of the presence of a water-soluble polymer.<sup>34</sup>

Particle size distributions (PSD) of the latexes were measured as a function of the conversion. The polydispersity index (PdI) starts for all reactions at around 0.1 and increases significantly at higher conversions (not shown). A summary of the PSD characteristics of the final latexes is given in Table 3. The DLS results in this table suggest an increasing  $D_n$  with an increasing macromonomer content (which is at odds with similar polymerization rates observed in Fig. 1), but this increase is clearly not observed in our SEM images (see Fig. 2).

In Fig. 2, the SEM images of the final latexes produced using 1 wt% and 4 wt% MAA<sub>80</sub> are shown. These images show monomodal distributions suggesting that the high PdI values observed in the DLS measurements are caused by the (reversible) aggregation of particles. The number mean particle diameter of both latexes obtained by SEM is around 85 nm (particle count >100).

From the results presented thus far it is safe to conclude that the presence of the MAA macromonomers in the emulsion polymerization does not significantly affect the polymerization rate and the particle size, and that SDS dominates the particle stabilization. In order to study the stabilizing properties of the macromonomers explicitly, we performed emulsion polymerizations using decreasing amounts of SDS and a constant amount of macromonomer (4 wt%). In Fig. 3 conversion *versus* time curves of the emulsion polymerization of MMA with 4 wt% MAA<sub>80</sub> and variable amounts of SDS are shown (for MAA<sub>16</sub> and MAA<sub>350</sub>, see ESI†). It is clear from this figure that the polymerizations using 1.0 and 1.5 wt% SDS result in high monomer conversions and stable latexes, but in the absence of SDS it was impossible to reach a conversion of higher than 40%. In the latter polymerization and that carried out using 0.5 wt% of SDS, a strong increase in the viscosity was observed above 40% conversion. This viscosity increase was caused by heavy flocculation and therefore trapping of water inside the flocs.<sup>34</sup> In both cases the flocs eventually collapsed and the polymer particles sedimented.



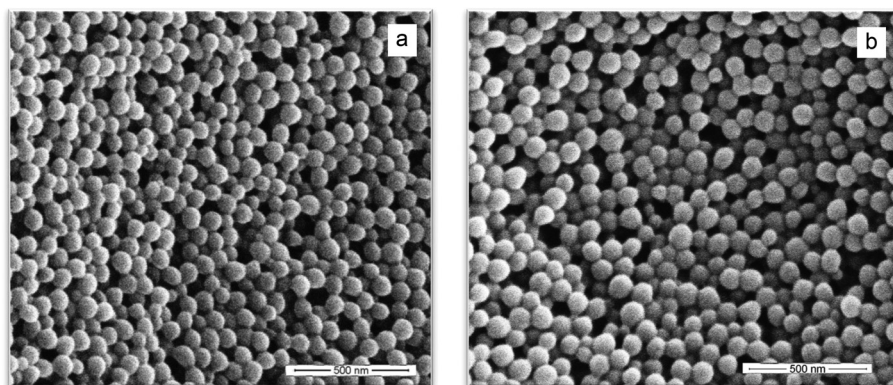


Fig. 2 SEM images of the final latex made using 1.5 wt% of SDS and (a) 1 wt% and (b) 4 wt% of MAA<sub>80</sub>.

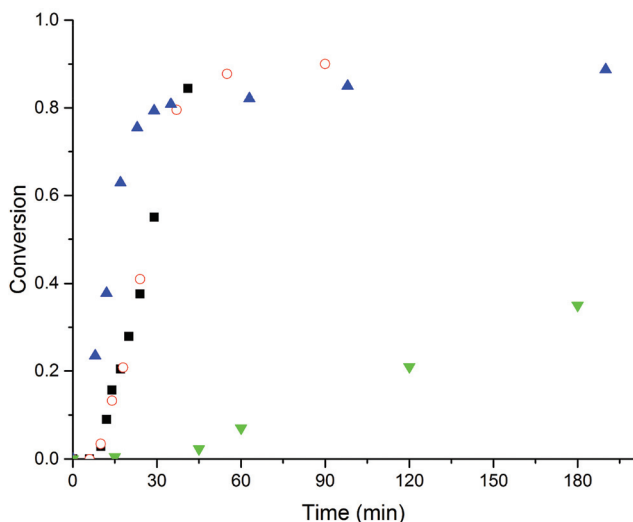


Fig. 3 Batch emulsion polymerization of MMA with 4 wt% MAA<sub>80</sub> and variable amounts of SDS. Concentration SDS: (▼) 0 wt%, (■) 0.5 wt%, (○) 1 wt% SDS and (▲) 1.5 wt%. Standard polymerization conditions as listed in Table 2.

From Fig. 3 it can also be seen that the polymerizations using SDS concentrations below the CMC ( $= 9.5 \text{ mM} \approx 1.4 \text{ wt}\%$ ) show a significant delay in the onset of polymerization. This result can be explained by the fact that in these reactions initially no micellar nucleation takes place and that the MAA macromonomers are converted into surfactants by the addition of a monomer unit *via* a (reversible) addition fragmentation chain transfer<sup>19</sup> (or “sulfur-free RAFT”)<sup>23,24</sup> mechanism; hence particle formation takes place by a “PISA-like” mechanism<sup>25,26</sup> aided by SDS when present. The process, however, is not fast/efficient enough to provide enough stabilization for the particles when no SDS is present. With the aim of reducing the monomer concentration and slowing down the polymerization we changed from a batch process to a semi-batch process (and changing the amounts of the macromonomer); in the case of SDS-free polymerizations, no stable latexes could be obtained.

In summary, it can be concluded that in the case of the emulsion homopolymerization of MMA the synthesized MAA macromonomers are too slowly converted into surfactants to provide sufficient stabilization and that some SDS is always needed. The use of insufficient SDS gives rise to heavy flocculation of the system, ultimately resulting in complete sedimentation of the polymer particles.

#### Emulsion polymerization of butyl acrylate

The emulsion polymerization of *n*-butyl acrylate (BA) was also investigated as this monomer is not only more reactive than MMA, but it also reacts *via* a different mechanism with the MAA-macromonomer as already mentioned in the introduction.<sup>14</sup> Initial experiments showed that in these BA polymerizations the MAA macromonomers provided sufficient stabilization and that no SDS was required; hence no experiments were performed using these combinations. In Fig. 4 the overall

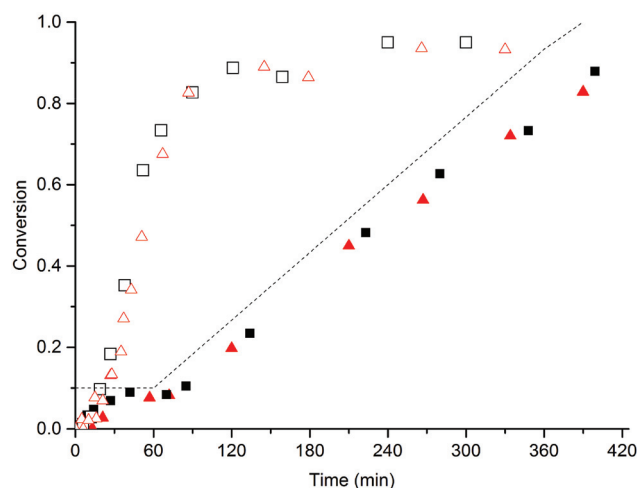


Fig. 4 Batch (open symbols) and semi-batch (closed symbols) emulsion polymerization of BA in the presence of MAA<sub>80</sub>, without SDS. Used concentrations of MAA<sub>80</sub>: 5 (■) and 10 (▲) wt%, respectively. Standard polymerization conditions as listed in Table 2. The dotted line indicates the addition profile of BA in the semi-batch reaction.



conversion of BA is given as a function of time for batch and semi-batch reactions with various amounts of the MAA-macromonomer MAA<sub>80</sub> in the absence of SDS.

First, two batch reactions were performed using 5 and 10 wt% of MAA<sub>80</sub>, respectively. It is clear from Fig. 4 that the amount of the macromonomer has no large influence on the conversion rate. Furthermore, monomer droplets were visible in samples taken up to monomer conversions of about 30% during these batch polymerizations. In order to prevent these potentially complicating monomer droplets we also performed semi-batch reactions. As is clear from the results in Fig. 4, the conversion of the BA in the semi-batch reaction closely follows the addition profile, indicating a near-full instantaneous conversion. Although in all cases minor coagulation is visible just after reaction (mostly around the stirrer and on the reactor wall), the latexes remained stable for periods of over 12 months. These results all suggest that efficient stabilizers are formed in these polymerizations.

The characteristics of the final latexes are summarized in Table 4 and two things are immediately clear from this table: (i) the particles obtained in the batch process are much larger than those obtained in the semi-batch process and (ii) increasing the amount of the macromonomer leads to a decrease in particle size. The first observation is consistent with a particle growth that is relatively fast as compared to stabilizer formation in the batch process, so after nucleation has started the newly formed stabilizers are used to stabilize the fast growing particles rather than form new particles. In the semi-batch process the initial batch period is mainly used for stabilizer and particle formation; the low amount of monomer precludes fast particle growth and additionally increases the probability of radicals to react with the macromonomers. Hence more surfactants are available for particle nucleation in the batch than in the semi-batch process. The second observation is more easily explained; increasing the amounts of the MAA macromonomer lead to increasing stabilizer concentrations, which in turn lead to increasing particle numbers (and concomitant decreasing particle diameters).

The particle diameters in the batch reactions are high compared to that of a reference latex stabilized with 1.5 wt% SDS ( $D_n = 60$  nm, PdI = 0.1), because fewer micelles are formed initially by the (reacted) macromonomer. Although almost no

coagulation took place immediately during or after the reaction, the latexes obtained from the batch reactions coagulated over time.

In summary, it can be concluded that in the case of the emulsion polymerization of BA the synthesized MAA macromonomers are sufficiently and fast converted into efficient stabilizers. This significantly different behavior as compared to that observed in the MMA polymerization is conceivably explained by one or more of the following reasons: BA reacts faster than MMA, the resulting surfactant in the BA polymerization is different (graft copolymer) as compared to that in MMA polymerization (block copolymer),<sup>14</sup> and finally, BA is more hydrophobic than MMA, so fewer monomer units are required to convert the MAA macromonomer into a surfactant. In what follows, we will investigate this in more detail.

### Emulsion copolymerization of BA and MMA

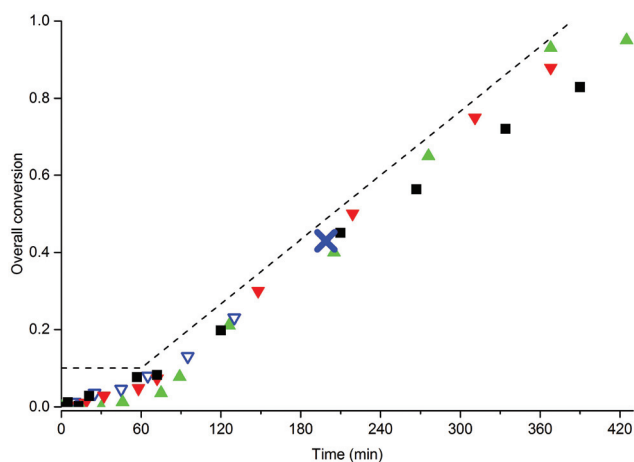
Considering the fact that adequate stabilization was observed in the BA system, we first investigated whether the addition of BA to MMA could also lead to stable latexes. We therefore carried out several different SDS-free emulsion copolymerizations of the two monomers with varying amounts of MAA<sub>80</sub> and in order to avoid the presence of monomer droplets (see the previous section) these polymerizations were carried out in a semi-batch. The conversion-time curves of these polymerizations using 10 wt% of MAA<sub>80</sub> and varying monomer feed compositions are shown in Fig. 5 (for the 5 and 15 wt% data, see ESI†).

It is immediately clear from this figure that polymerizations with monomer feed compositions of  $w_{BA} \geq 0.3$  all lead to stable latexes, and that only the system with 5% BA resulted in severe coagulation. A summary of the properties of the final latexes is given in Table 5, and comparison with the data in

**Table 4** Characteristics of MAA<sub>80</sub>-stabilized pBA latexes

	MAA <sub>80</sub> (wt%)	DLS		SEM/TEM <sup>a</sup> $D_n$ (nm)	Fraction polymer coagulated <sup>b</sup>
		$D_n$ (nm)	PdI		
Batch	5	1200	0.09	970	0.01
	10	750	0.10	800	0.03
Semi-batch	5	375	0.17	310	0.05
	10	175	0.11	130	0.14

<sup>a</sup>Number mean particle diameter; error 10%. <sup>b</sup>All obtained latexes from the semi-batch reactions showed good stability (>12 months), latexes obtained from the batch reactions coagulated over time.



**Fig. 5** Semi-batch copolymerization of BA and MMA with 10 wt% MAA<sub>80</sub>, no SDS. Monomer feed compositions (weight fractions of BA):  $w_{BA} = 1$  (■),  $w_{BA} = 0.5$  (▲),  $w_{BA} = 0.3$  (▼) and  $w_{BA} = 0.05$  (▽). Standard polymerization conditions as listed in Table 2. The dotted line indicates the addition profile of the semi-batch reaction. The cross in the data set for  $w_{BA} = 0.05$  indicates major coagulation.



**Table 5** Summary of characteristics of MAA<sub>80</sub>-stabilized p(BA-co-MMA) latexes

$w_{BA}$	MAA <sub>80</sub> (wt%)	$D_n$ (nm)	PdI	Fraction polymer coagulated <sup>a</sup>
1.0	5	375	0.10	0.05
	10	175	0.10	0.10
	15	175	0.17	0.01
0.7	15	120	0.05	0.01
0.5	5	500	0.08	0.05
	10	300	0.12	0.10
	15	—	—	—
0.3	5	—	—	—
	10	400	0.12	0.02
	15	145	0.16	0.03
0.05	5	Coagulated		
	10	Coagulated		
	15	Coagulated		

<sup>a</sup> All obtained latexes showed good long term stability (>12 months).

Table 4 shows that particle sizes are very similar and that increasing macromonomer concentrations lead to decreasing particle sizes. TEM and SEM images of the final latexes are shown in the ESI.†

In summary, it can be concluded that the addition of ≥30 wt% of BA to MMA results in the formation of efficient stabilizers for the SDS-free emulsion polymerization and that stable latexes are obtained. This result is of practical importance for coating applications, where these two monomers are often copolymerized.

### Effects of monomer reactivity and hydrophobicity on emulsion polymerization

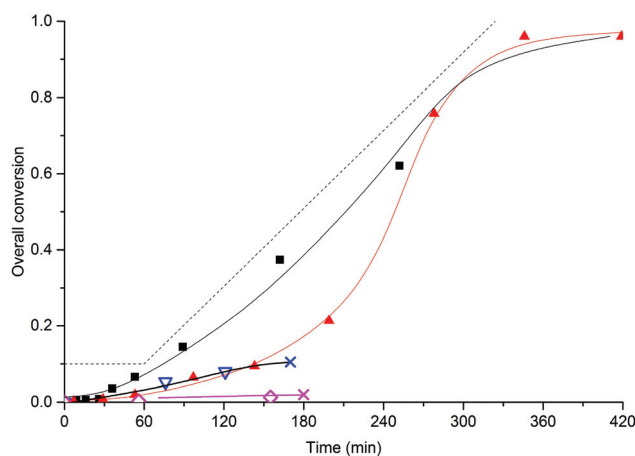
In order to investigate in more detail whether the higher reactivity and/or higher hydrophobicity are the cause of the better stabilization in the BA system, we studied the emulsion polymerizations of ethyl acrylate (EA) and *n*-butyl methacrylate (BMA). The former monomer has a similar reactivity to BA, but a hydrophobicity similar to MMA, and the latter monomer has a similar reactivity to MMA, but a hydrophobicity similar to BA. Both batch and semi-batch reactions were performed using these monomers in the presence of 5 wt% MAA<sub>80</sub> and the absence of SDS. Conversion-time curves and the particle size distributions in the final latexes of both batch and semi-batch emulsion polymerizations of EA and BMA with MAA<sub>80</sub> are shown in the ESI.† Only the BMA polymerization resulted in stable latexes when performed in batch ( $D_n = 475$  nm, PdI = 0.40), whereas the EA batch polymerization resulted in severe coagulation at around 30% monomer conversion. The semi-batch reactions resulted in stable latexes for both monomers, although all reactions showed some minor amounts of coagulum (mainly around the stirrer and on the reaction walls). After removal of the coagulum all latexes remained stable in the long term (the pEA latex produced in semi-batch coagulated after about one month). The particle diameter of the semi-batch latex of pBMA ( $D_n = 350$  nm, PdI = 0.06) is similar to that observed in the pBA latex produced under similar con-

ditions ( $D_n = 375$  nm, PdI = 0.17) and is much smaller than that observed in the semi-batch pEA latex ( $D_n = 1000$  nm, PdI = 0.19). From both the batch and the semi-batch results it can be concluded that stabilizer formation is more efficient in the BMA system than in the EA system, implying that hydrophobicity is more important than reactivity. A higher reactivity, however, is advantageous, as can be concluded from the fact that the semi-batch EA polymerization does lead to stable latexes, whereas this was not possible for MMA.

### Emulsion copolymerization of BMA and MMA

In order to investigate whether the addition of small amounts of BMA to MMA could lead to stable SDS-free all-methacrylate latexes, we investigated the semi-batch emulsion copolymerization of BMA and MMA with several different monomer feed compositions. Conversion-time curves for monomer feed compositions with weight fractions of BMA ( $w_{BMA}$ ) down 0.5 are shown in Fig. 6 and it is immediately clear that more than 70% BMA is required for obtaining stable latexes.

In the cases with using  $w_A \leq 0.70$  very low polymerization rates were observed and major coagulation occurred after 5 to 10% conversion; both of these observations are indicative of insufficient stabilization, which in turn is caused by a too slow production rate of the stabilizer. When comparing the other two systems, *i.e.*, the BMA homopolymerization and the copolymerization with  $w_{BMA} = 0.85$ , there is a very large difference in the polymerization rates. Although the homopolymerization proceeds roughly at the same rate as the monomer addition rate, the copolymerization is much slower in the beginning. This is indicative of a lower particle number in the latter case, which in turn is caused by a slower stabilizer production. This is also evident from the respective particle diameters (see Table 6); the particle size is much larger for the copolymerization as compared to that in the homopolymerization.



**Fig. 6** Semi-batch copolymerization of BMA and MMA with 5 wt% MAA<sub>80</sub>. Monomer feed compositions (weight fractions of BMA):  $w_{BMA} = 1$  (■),  $w_{BMA} = 0.85$  (▲),  $w_{BMA} = 0.7$  (▽) and  $w_{BMA} = 0.5$  (◇). Standard polymerization conditions as listed in Table 2. The dashed line is the addition profile for the semi-batch reactions, full curves are guides to the eye. Crosses indicate that major coagulation takes place.



**Table 6** Summary of characteristics of *p*(BMA-*co*-MMA) latexes stabilized by 5 wt% MAA<sub>80</sub>

$w_{\text{BMA}}$	$D_n$ (nm)	PdI	Fraction polymer coagulated <sup>a</sup>
1.00	350	0.06	0.15
0.85	1300	0.08	0.08
0.70	Coagulated		
0.50	Coagulated		

<sup>a</sup> Long term stability of all latexes good >12 months.

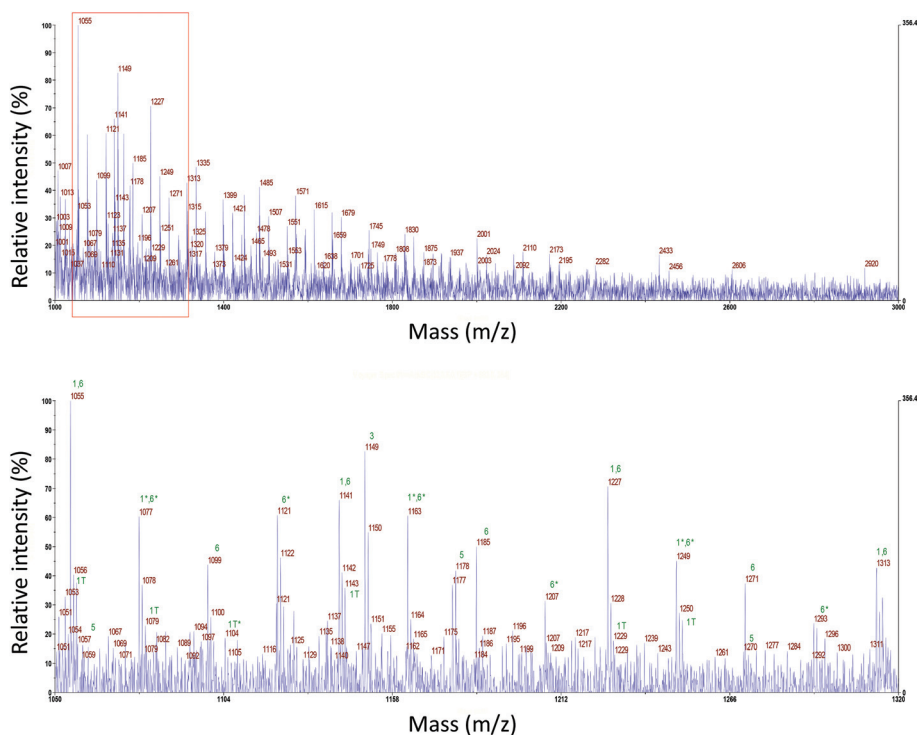
In the homopolymerization, stabilizer production is relatively fast as the addition of a few monomer units to the MAA macromonomer quickly leads to a surface-active block copolymer and combined with a slow particle growth, this leads to a larger number of particles that can be nucleated. This is in contrast to the copolymerization case. Since MMA is more water-soluble than BMA, it is likely that the chain extension of the MAA macromonomer will involve a significant number of MMA units and therefore a longer block ( $\approx$  more addition steps) is required to obtain a surface-active block copolymer. Hence stabilizer production will now be slowed down as compared to particle growth and the newly formed stabilizer during the polymerization is used to stabilize the growing particles, rather than to form new particles. This reasoning is completely analogous to that used for the explanation of the differences in particle sizes observed in the BA homopolymerizations in batch and semi-batch processes (see above, Fig. 4).

Finally on comparing these BMA-MMA copolymerizations with the BA-MMA copolymerizations, it is clear that not only the hydrophobicity of the comonomer is important, but also the rate at which the stabilizer is formed.

### Structure analysis of the *in situ* formed copolymers

It is clear from the results so far that the MAA macromonomers were converted into efficient stabilizers most effectively in the emulsion polymerization of BA and in order to obtain more detailed structural information on these stabilizers we examined a sample of the initially formed product at a conversion of 5% by MALDI-ToF MS. The obtained spectrum is shown in Fig. 7 and it is immediately clear that this spectrum is quite complex and does not originate from a single population of polymer chains only differing in degree of polymerization.

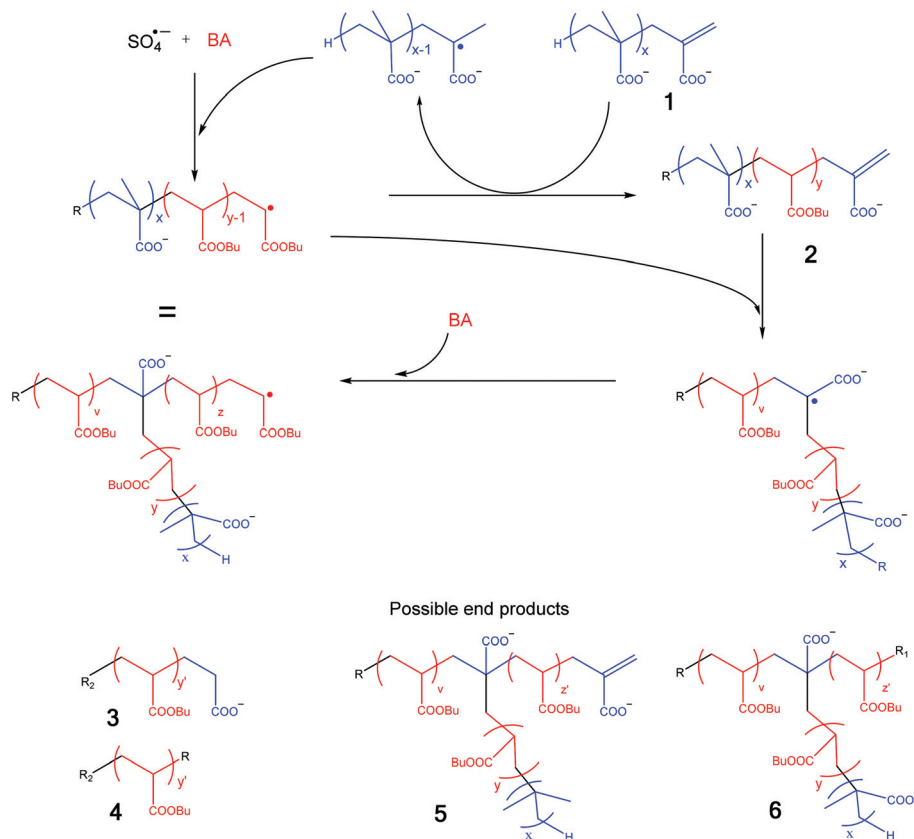
In order to simplify the discussion of this spectrum it is useful to consider the copolymerization of the MAA macromonomers with BA and so identify the potential structures in the MALDI spectrum. This process is schematically shown in Scheme 2.<sup>14</sup> Propagating BA radicals (initially formed by the addition of  $\text{SO}_4^{\cdot-}$  radicals to BA and later in the process this could be any propagating radical) will undergo an addition fragmentation chain transfer (AFCT) reaction with the MAA macromonomer (1).<sup>22</sup> This results in a MAA radical (which can propagate with BA) and a new macromonomer now containing a BA penultimate unit (2). This new macromonomer now will



**Fig. 7** MALDI-ToF Mass spectrum of the initially formed oligomers in the emulsion polymerization of BA with 15 wt% MAA<sub>80</sub>, overview and enlarged from  $m/z$  1050 to 1320. Each number indicates a reaction product shown in Scheme 2; \* exchange of one or more  $\text{H}^+$  with  $\text{Na}^+$  in MAA chain; 1 T terminated PMAA chain by recombination.







**Scheme 2** Possible pathways for *in situ* formation of amphiphilic copolymers, R = H, OH or SO<sub>4</sub><sup>-</sup>; R<sub>1</sub> = H, OH, SO<sub>4</sub><sup>-</sup>, MAA<sub>C=C</sub>, R<sub>2</sub> = OH or SO<sub>4</sub><sup>-</sup>; y ≥ 1.

not undergo an AFCT reaction with a BA propagating radical, but will copolymerize and form a graft upon further polymerization.<sup>22</sup> It should be noted here that many different grafts are possible as macromonomer **2** may not only contain a homo pBA block, but it could easily contain a pMAA block followed by a pBA block or even contain one or more grafts as any propagating BA radical can react with the initial MAA macromonomer **1**. As an additional complicating factor it should be noted that the degrees of polymerization of all these blocks can vary.

The potential final products (resulting from AFCT and/or termination by recombination and disproportionation) of this process are also shown in Scheme 2 and with this scheme in hand we tried to identify the peaks in Fig. 7.

From Fig. 7, it can be seen that most of the measured oligomers are graft (or block) copolymers (**6**) of MAA and BA; in rare cases also macromonomers (thus terminated with H and vinyl group) (**5**) were formed. Still some of the unreacted macromonomer (**1**) seems to be present, although it should be noted that the *m/z* of this structure is the same as that of copolymer structure **6**. We also observe a small number of peaks from the recombination peaks of two smaller pMAA radicals (**1**<sup>T</sup>). The intermediate reaction product of a growing pBA chain with one MAA macromonomer (**3**) was observed with an OH end group only. The expected endgroup formed with KPS

is SO<sub>4</sub><sup>-</sup>, but depending on the type of the monomer and the reaction conditions also other end groups like OH have been observed.<sup>35,36</sup> No intermediate macromonomers (**2**) or oligomers of BA (**4**) were observed. Larger polymers of pBA, immediately formed during the emulsion polymerization, are above the measuring range of the MALDI-ToF MS. A more elaborate discussion of the spectrum is given in the ESI.†

In summary, it can be concluded that from the start of the emulsion polymerization the MAA macromonomers were copolymerized with BA to form stabilizers *in situ*.

## Conclusions

Methacrylic acid macromonomers prepared *via* catalytic chain transfer polymerization were shown to be suitable precursors for stabilizers in (surfactant-free) emulsion polymerization. It was found that a prerequisite for efficient *in situ* stabilizer formation is that the conversion of the macromonomer into amphiphilic stabilizer molecules should be sufficiently fast. This is not the case in the homopolymerization of MMA, which neither polymerizes quickly with the macromonomer, nor is it very hydrophobic; in all MMA homopolymerizations, the addition of SDS was necessary. Hydrophobic monomers such as BA and BMA, however, convert the macromonomer more



quickly into a stabilizer upon the addition of a few monomer units and the polymerization can be carried out without the addition of SDS. Furthermore, BA reacts more quickly with the MAA macromonomers than MMA (and BMA), which results in a quicker incorporation of hydrophobic units into the precursor/stabilizer. The faster reaction of acrylates also resulted in stable (surfactant-free) emulsion polymerization in the case of ethyl acrylate (with a similar hydrophobicity to MMA), but only in the case of a semi-batch process and not in the batch process; this latter observation can be explained by the fact that particle growth is much slower in the case of a semi-batch process and that there was sufficient time for *in situ* stabilizer formation.

## Conflicts of interest

There are no conflicts to declare.

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