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ALD SnO<sub>2</sub> protective decoration enhances the durability of a Pt based electrocatalyst†Catherine Marichy,<sup>ab</sup> Giorgio Ercolano,<sup>c</sup> Gianvito Caputo,<sup>‡d</sup> Marc G. Willinger,<sup>e</sup> Deborah Jones,<sup>c</sup> Jacques Rozière,<sup>c</sup> Nicola Pinna<sup>\*d</sup> and Sara Cavaliere<sup>\*c</sup>

Electrospinning and atomic layer deposition (ALD) have been coupled to prepare functional hetero-structures with potential application in fuel cells. Electrocatalysts comprising platinum (Pt) nanoparticles dispersed onto electrospun carbon fibers were selectively decorated with tin dioxide (SnO<sub>2</sub>) using ALD. The presence of SnO<sub>2</sub> led to a considerable enhancement of the catalyst durability during voltage cycling.

## Introduction

Research on proton exchange membrane fuel cell (PEMFC) electrocatalysts has been mainly focused on understanding and improving their activity towards the kinetically limiting oxygen reduction reaction (ORR) at the cathode (and methanol/ethanol oxidation reaction at the direct alcohol fuel cell anode). Significant advances in this regard have been achieved by tuning the size and morphology of the Pt nanocatalyst and elaborating alloys.<sup>1</sup> However, performance degradation over time has emerged as a critical aspect complementary to the electrocatalyst efficiency, and has been extensively studied.<sup>2</sup> This issue, together with the low abundance of Pt in the Earth's crust and thus its cost, has a great impact on hindering the commercialization of PEMFC and the consequent development of a sustainable hydrogen-based economy. The two predominant and interacting processes affecting electrocatalyst lifetime are the corrosion of the carbon-based support and the agglomeration and detachment of the Pt nanoparticles leading to the loss of active surface area under specific cell operating conditions.

At potential higher than 0.207 V vs. RHE (reversible hydrogen electrode), carbon is oxidized into CO<sub>2</sub>.<sup>3</sup> At potentials encountered in normal PEMFC operation (0.6–0.9 V) the kinetics of the

oxidation reaction are sluggish, while under dynamic processes, such as start-up and shut down, it is accelerated as a direct consequence of high potential values reached by the cathode, for example due to local fuel starvation<sup>4</sup> ( $\geq 1.2$  V). Furthermore, the presence of Pt particles accelerates the phenomenon catalyzing the reaction by providing highly reactive transient oxygen radicals.<sup>5</sup> Carbon corrosion results in detachment/agglomeration of catalyst nanoparticles and a decrease in active surface area and performance, as well as in an increase in hydrophilicity and loss of porosity of the catalyst layer which negatively affect the mass-transport of gases and water management.<sup>2b</sup> Concerning the degradation of the nanocatalyst, it must be considered that under standard conditions platinum is thermodynamically unstable at pH values lower than 0 and at potentials greater than 1.0 V, and that the increase in potential and temperature is detrimental for the catalyst stability.<sup>6</sup> Together with the detachment related to support oxidation, three other mechanisms are reported in literature:<sup>2e,7</sup> Pt nanocrystal migration and coalescence, and Pt dissolution and re-precipitation on the support (electrochemical Ostwald ripening) or in the membrane ("Pt band"). Poisoning of the Pt surface with contaminants from the fuel and air, such as CO<sub>x</sub>, NO<sub>x</sub>, SO<sub>x</sub>, H<sub>2</sub>S, NH<sub>3</sub> and small organics, leads to the loss of electrocatalyst activity and fuel cell performance.<sup>8</sup>

Several strategies are employed to mitigate the degradation of PEMFC electrodes. To enhance the stability of the Pt based electrocatalyst, several alloys with noble and non-noble metals in binary and ternary catalysts have shown to be an effective route against dissolution and detachment.<sup>9</sup> Use of core-shell nanoparticles and tuning of the catalyst morphology have also proved to be elegant approaches to improve the performance of Pt-based electrocatalysts.<sup>10</sup> In order to avoid support corrosion, novel carbon nanostructured materials *e.g.* carbon nanotubes and nanofibers have been developed demonstrating improved stability.<sup>11</sup> In this regard electrospinning has emerged as a straight-forward and readily up-scalable method to prepare 1D nanomaterials applicable in fuel cell electrodes.<sup>12</sup> Another

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approach is to replace carbon by alternative materials such as transition metal oxides, *e.g.*  $\text{TiO}_2$  and  $\text{SnO}_2$ , with intrinsic high electrochemical stability.<sup>13</sup> The interaction of such oxides with platinum may also promote electrocatalytic activity through the so-called strong-metal-support-interaction.<sup>14</sup> Nevertheless, the drawback of metal oxides in general, is their low electrical conductivity that can in some cases be overcome by doping<sup>15</sup> or by using carbon based composite materials.<sup>16</sup>

In this work a promising composite electrocatalyst support material was elaborated based on electrically conducting carbon nanofibres (CFs) prepared by electrospinning and decorated with non-conducting stabilizing  $\text{SnO}_2$  using atomic layer deposition (ALD). In particular, the protecting tin oxide was deposited directly onto the Pt decorated CFs. This approach has been recently applied in heterogeneous catalysis, where porous  $\text{Al}_2\text{O}_3$  ALD film stabilized Pd particles<sup>17</sup> and in electrocatalysis where  $\text{ZrO}_2$  was deposited around Pt particles previously protected with an organic layer.<sup>18</sup> Morphology, surface analysis, electrocatalytic properties towards ORR and the electrochemical degradation of such novel electrocatalysts were investigated. The addition of  $\text{SnO}_2$  permitted a remarkable increase of the catalyst durability without reducing Pt activity. So far ALD has been coupled to electrospinning to prepare a Pt electrocatalyst on fibers.<sup>19</sup> Here ALD allows the protection of both the electrocatalyst and the support, while keeping intact their intrinsic catalytic activity and electrical conductivity, respectively. The unhindered activity may result from the very low and controlled amount of material deposited on the one hand, and the preferential growth of tin dioxide on the carbon fibers on the other hand.

## Results and discussion

The CFs comprise electrospun polyacrylonitrile fibers stabilized at 280 °C and graphitized under inert atmosphere at 1000 °C. The as-obtained fibers present an  $I_D/I_G$  ratio in Raman spectroscopy of 1.7 comparable to that of commercial carbon nanotubes.<sup>20</sup> Investigation of the electrical properties using a four probe method demonstrates electrical conductivity comparable to that of carbon black Vulcan XC-72, a conventional electrocatalyst support.<sup>21</sup>

Pt nanoparticles (NPs) were deposited onto the fibers using a microwave assisted polyol method.<sup>22</sup> TEM images (Fig. 1) show a quite good Pt dispersion with a few aggregates. The size distribution (see Table SI.1 in ESI† and Fig. 1b) is centered at  $2.3 \pm 1.0$  nm, while a domain size of 2.9 nm was determined by XRD. A small amount of  $\text{SnO}_2$  was deposited in a controlled manner using a non-aqueous sol-gel ALD approach.<sup>23</sup> The number of ALD cycles was set for ~1 nm thick  $\text{SnO}_2$  coating on Si reference wafer. No noticeable change on Pt nanoparticle distribution (Fig. 1 and Table SI.1†) was observed after deposition. It was previously demonstrated that the  $\text{SnO}_2$  deposition approach used leads to granular rather than continuous coating, especially on graphitized carbon.<sup>23,24</sup> However, no clear evidence of  $\text{SnO}_2$  is visible in TEM images due to the very low amount of  $\text{SnO}_2$  deposited and the amorphous state of the oxide.<sup>22</sup>

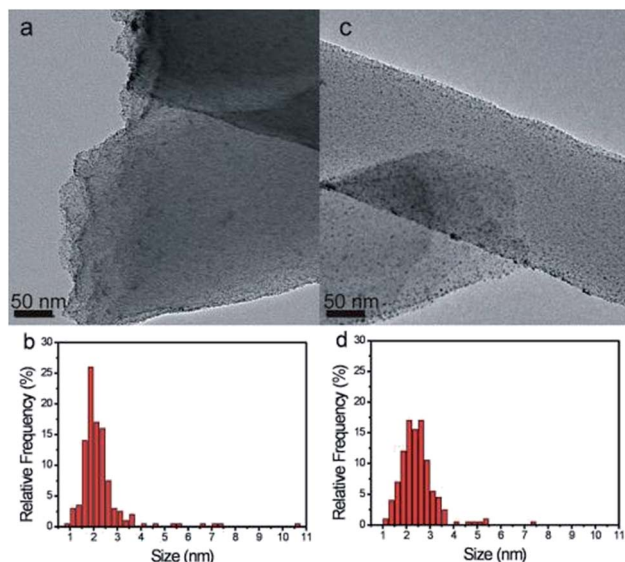


Fig. 1 (a and c) TEM images and (b and d) particle distribution obtained from TEM analysis of (a and b) Pt/CFs, (c and d)  $\text{SnO}_2$ /Pt/CFs before cyclic voltammetry.

Indeed, the HRTEM images in Fig. 2 show that after ALD the Pt surface remains clean and comparable to uncoated CFs. Dark field STEM image recorded on coated samples (Fig. 2d) reveals tiny clusters (red arrows), almost not visible in bright field (Fig. 2c), dispersed onto the carbon, which could be attributed to  $\text{SnO}_2$ .

XPS analyses were performed on  $\text{SnO}_2$ -coated samples to confirm the presence of the metal oxide and the Pt loading. Table SI.2† reports the weight percentage of Pt, Sn, O and C in the sample. In the high resolution scan across the Sn 3d region of Fig. 3a the two Sn 3d<sub>5/2</sub> peaks at 486.9 eV and 495.3 eV confirm the presence of tin in an oxidized state.<sup>23,25</sup> The

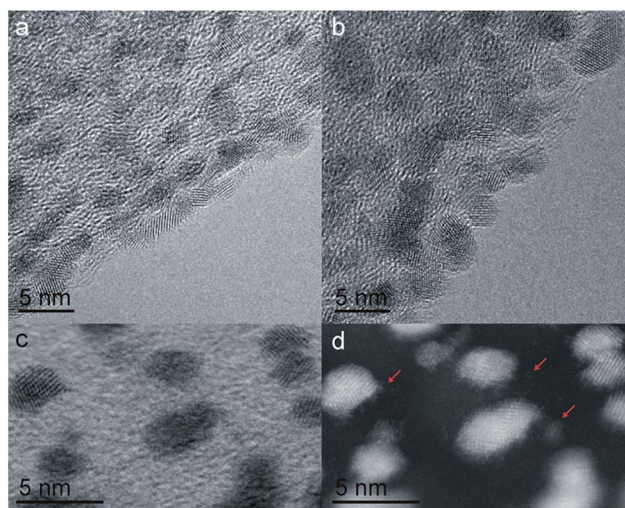


Fig. 2 (a and b) HRTEM images of Pt/CFs and  $\text{SnO}_2$ /Pt/CFs before cyclic voltammetry. (c and d) STEM images of  $\text{SnO}_2$ /Pt/CFs in bright and dark field.



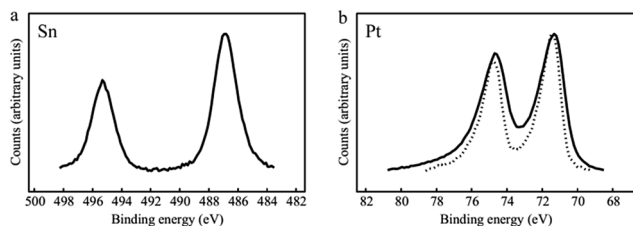


Fig. 3 XPS spectra of SnO<sub>2</sub>/Pt/CFs (full line) and Pt/CFs (dotted line). High resolution scans across (a) the Sn 3d and (b) Pt 4f edges, respectively.

calculated stoichiometric ratio Sn/O in our samples, utilizing the O 1s peak at 530.7 eV attributed to the metal oxide, is 0.54, in good agreement with value reported in the literature<sup>15a</sup> and confirms the presence of tin in the oxidation state (IV).<sup>26</sup> Platinum, tin, oxygen and carbon were also observed in the survey spectrum. Looking at the high resolution scan across the Pt 4f region (Fig. 3b) mostly Pt in 0 oxidation state is detected. It is worthy to note a very small shift of the two Pt 4f<sub>5/2</sub> and Pt 4f<sub>7/2</sub> peaks to lower binding energy compared to Pt/CFs, which can be attributed to a slight increase of the local electron density due to charge transfer from SnO<sub>2</sub> to Pt resulting from strong metal-metal oxide interaction.<sup>27</sup>

In order to evaluate the impact of the presence of tin oxide on the electrocatalyst accessibility and performance, cyclic voltammetry (CV) in a N<sub>2</sub> saturated 0.5 M aqueous H<sub>2</sub>SO<sub>4</sub> was performed and is presented in Fig. 4a. Similar profiles are observed for Pt/CFs with and without SnO<sub>2</sub>. Both electrocatalysts clearly showed H adsorption and desorption peaks at 0.05–0.3 V (ref. 28) as well as PtO formation and reduction peaks at 0.7–0.9 V. The Pt electrochemically active surface area (ECSA) was determined from H adsorption and desorption: no significant change of ECSA is noted between Pt/CFs (27 m<sup>2</sup> g<sub>Pt</sub><sup>−1</sup>) and SnO<sub>2</sub>-decorated Pt/CFs (29 m<sup>2</sup> g<sub>Pt</sub><sup>−1</sup>). Similar and comparable values have been previously reported for other carbon nanofiber based Pt catalysts with similar loading.<sup>11c,29</sup> Thus, the presence of SnO<sub>2</sub> does not seem to influence the overall electrochemical behavior of the samples, proving that the coating does not prevent reacting species from reaching the catalyst. One can therefore conclude that the deposited SnO<sub>2</sub> particles does not cover the Pt NPs, but must be preferentially deposited onto the carbon support. This is also supported by the fact that a retarded nucleation process on noble metal substrates was

already demonstrated in the literature.<sup>30</sup> Indeed an onset of deposition was noted on a Pt support;<sup>30a</sup> in the case of HfO<sub>2</sub> ALD from HfCl<sub>4</sub> and H<sub>2</sub>O, 30–50 cycles are required to initiate the growth.<sup>30c</sup> This behavior has been attributed to the relative inertness of noble metals toward hydroxylation that is required for the creation of anchoring sites.<sup>30b</sup> No oxide is present to initiate the growth and different mechanisms that on oxide or silicon may occur at the early stage, *e.g.* it was shown that Pt surface provides a different bonding environment for ALD HfO<sub>2</sub>.<sup>31</sup> Furthermore a significant lattice mismatch between Pt and metal oxide may also restrict the nucleation of grains leading to a nucleation delay.<sup>30b</sup> Considering the growth rate and the low number of cycles performed here (20 cycles), no real growth on the Pt NP surface may occur as the offset may have not been reached, even though deposition of few SnO<sub>2</sub> clusters on the metal particles cannot be completely excluded. On the other hand, the functional groups available on the surface of carbon fibers promote the nucleation of SnO<sub>2</sub> even after only few cycles.<sup>32</sup> Therefore, SnO<sub>2</sub> should grow preferentially from oxygen functional groups present onto the carbon substrate in proximity to the Pt catalyst nanoparticles, permitting a strong metal-metal oxide interaction without significant shielding effect. A schematic representation of the electrocatalyst surface is shown in Fig. 5.

To confirm that the electrocatalyst activity is not hindered by the presence of tin dioxide, ORR was performed in an O<sub>2</sub> saturated 0.5 M aqueous H<sub>2</sub>SO<sub>4</sub> at different rotating electrode speeds (Fig. SI.2†). No loss of the performance was noted in the presence of the metal oxide as shown by the ORR mass activities (Table SI.3†). The calculated number of electrons involved in the oxygen reduction mechanism using the Koutecky-Levich analysis is ~4 for both electrocatalysts as expected for Pt, suggesting a mechanism that does not involve production of H<sub>2</sub>O<sub>2</sub>.<sup>33</sup> Furthermore, the corresponding kinetic currents involved were calculated and are reported in the Tafel plot in Fig. 4b. Even though at low current density similar kinetic currents are noted for unprotected Pt/CFs and SnO<sub>2</sub>/Pt/CFs, a significant decrease in potential is observed for Pt/CFs compared to the SnO<sub>2</sub> decorated electrocatalyst. This suggests a beneficial effect of SnO<sub>2</sub>-coated fibers at higher potential values, which we attribute to the proximity of platinum to the metal oxide and its promoting catalytic effect (Fig. 5).

In order to evaluate the durability of the electrocatalyst, an accelerated degradation protocol was applied by cycling from

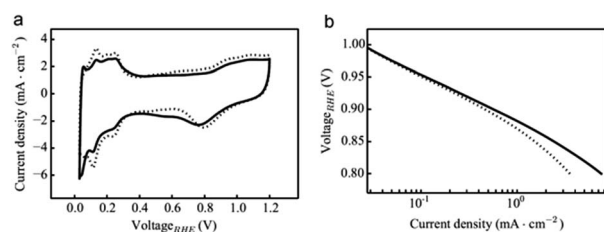


Fig. 4 (a) Cyclic voltammetry at 50 mV s<sup>−1</sup> in a 0.5 M H<sub>2</sub>SO<sub>4</sub> solution saturated with N<sub>2</sub>. (b) ORR Tafel plot for uncoated (dotted line) and SnO<sub>2</sub>-decorated carbon fibers (full line).

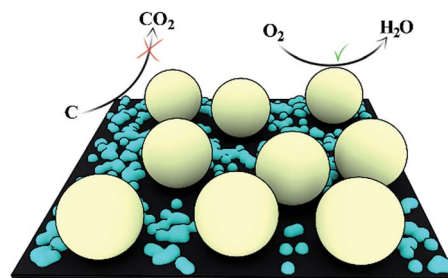


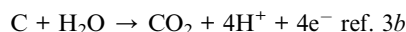
Fig. 5 Schematic representation of the SnO<sub>2</sub>(blue)/Pt(yellow)/CFs (black) surface.





0.6 to 1.2 V at  $100 \text{ mV s}^{-1}$  for 10 000 cycles and monitoring the electrochemical surface area decrease every  $100^{\text{th}}$  cycle performing a CV from 0.05 to 1.2 V at  $50 \text{ mV s}^{-1}$ . Fig. 6 presents the ECSA as a function of the cycle number and shows a reduced ECSA loss for the  $\text{SnO}_2$ -decorated catalysts compared to pristine Pt/CFs electrocatalysts. In a previous study, the significant ECSA loss and thus catalyst degradation over cycling has been defined as the major issue for electrospun CFs.<sup>21</sup>  $\text{SnO}_2$ -decorated Pt/CFs samples maintained an active surface area around  $20 \text{ m}^2 \text{ g}_{\text{Pt}}^{-1}$  by the end of the cycling, while the loss of Pt active surface on unprotected carbon fibers was much more significant. The loss is halved with addition of  $\text{SnO}_2$  as reported in Table SI.4† and thus a positive influence of  $\text{SnO}_2$  decoration with respect to degradation over cycling is clearly demonstrated. This result is in agreement with the high electrochemical stability reported in the literature of the metal oxide, used either as additive or as replacement for conventional carbon-based electrocatalyst supports.<sup>15a,34</sup>

To further confirm the protecting role of the tin oxide component on the Pt/CFs, an accelerated corrosion test was performed in conditions providing information on degradation under fuel starvation and reverse current at the cathode side (1.4 V/RHE,  $80^\circ\text{C}$ ,  $0.5 \text{ M H}_2\text{SO}_4$ , 2 h). The corrosion is quantified in terms of loss of material by the effect of electrochemical oxidation.<sup>35</sup> For carbon based materials the corrosion reaction is well known:



From integration of the oxidation currents over time (oxidation charge) it is possible to estimate the carbon loss into  $\text{CO}_2$  from the Faraday law. Fig. 6b presents the currents obtained *versus* time for ALD  $\text{SnO}_2$  protected and unprotected samples. It is evident that the oxidation charge is lower for the former ( $3.2 \text{ C mg}^{-1}$ , carbon loss 12.6%) than for the pristine CFs ( $5.3 \text{ C mg}^{-1}$ , carbon loss 16.2%). This accelerated test clearly proves that the metal oxide is able to cover and partially protect the carbon support from corrosion (see Fig. 5).

Finally, TEM studies were performed on the 5% Pt loaded CF catalysts with and without  $\text{SnO}_2$  after CV prolonged cycling (Fig. 7a and c). It is evident that the amount of Pt remaining on the fibers after 10 000 cycles is much higher on the  $\text{SnO}_2$  coated

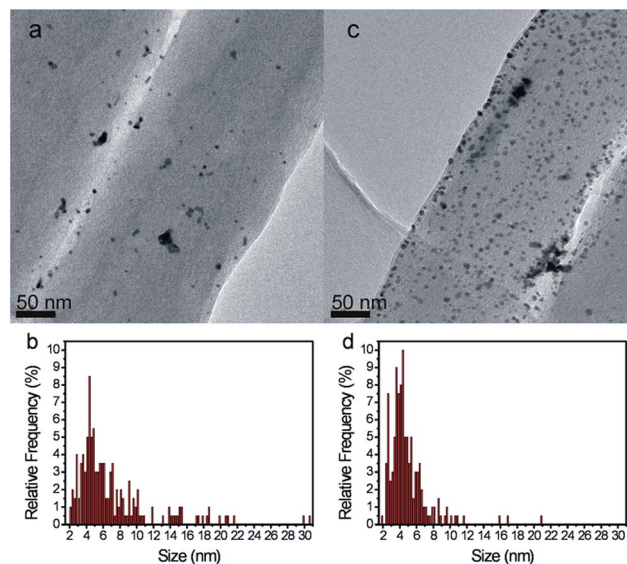


Fig. 7 TEM images (a and c) and (b and d) particle distribution from TEM analysis of (a and b)  $\text{Pt}^{5\%}$ -CFs and (c and d)  $\text{SnO}_2$ - $\text{Pt}^{5\%}$ -CFs after 10 000 potential cycles.

CFs (Fig. 7b) than on the non-protected CFs (Fig. 7a). A better dispersion of the particles is also observed in the presence of the oxide. For both samples, growth of Pt nanoparticles is noted with a size distribution (Table SI.1†) increasing from  $\sim 2 \text{ nm}$  before to either  $7 \text{ nm}$  or  $4.9 \text{ nm}$  after cycling for Pt/CFs and  $\text{SnO}_2/\text{Pt}/\text{CFs}$ , respectively, indicating that Ostwald ripening is almost suppressed by  $\text{SnO}_2$  surrounding the noble metal particles (Fig. 5). It must be also noted that a narrower particle distribution is obtained in the presence of the metal oxide (Fig. 7b and d). Therefore the improved durability is probably related not only to the protection of carbon from corrosion but also to a better stability, adhesion and confinement onto CFs of Pt NPs in presence of  $\text{SnO}_2$ .

## Experimental

Polyacrylonitrile (PAN,  $M_w = 150\,000$ , Sigma Aldrich) based carbon fibers were prepared combining electrospinning with thermal treatment as already reported.<sup>21</sup> 8% (w/w) PAN solution in *N,N*-dimethylformamide (DMF, 98%, Sigma Aldrich) was feed to a metallic needle *via* a syringe pump with a flow rate of  $1 \text{ ml h}^{-1}$ . An electric field of  $15 \text{ kV}$  was applied between the needle and a metallic rotating drum collector (from Linari Engineering) placed  $10 \text{ cm}$  away. As-prepared PAN fibers were collected in the form of non-woven mats. Fiber carbonization was realized by a two-step thermal treatment. First an oxidative stabilization was performed at  $280^\circ\text{C}$  for  $1 \text{ h}$  followed by a carbonization for  $1 \text{ h}$  under  $\text{N}_2$  at  $1000^\circ\text{C}$  using a heating ramp of  $1^\circ\text{C min}^{-1}$ .

CFs were loaded at 20% (w/w) with Pt NPs synthesized by a microwave assisted polyol synthesis.<sup>15a</sup> Thermogravimetric analysis was performed in air up to  $800^\circ\text{C}$  ( $10^\circ\text{C min}^{-1}$ ) using a Netzsch TG 439 thermobalance to determine the Pt loading on Pt/CF electrospun fibers.

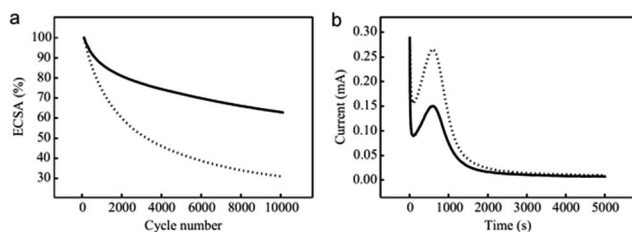


Fig. 6 (a) ECSA of Pt/CFs (dotted line) and  $\text{SnO}_2/\text{Pt}/\text{CFs}$  (full line) calculated from cyclic voltammetry at  $50 \text{ mV s}^{-1}$  in a  $\text{N}_2$  saturated  $0.5 \text{ M H}_2\text{SO}_4$  solution every 100 cycles performed at  $100 \text{ mV s}^{-1}$ . (b) Oxidation/corrosion characteristics for Pt/CFs (dotted line) and  $\text{SnO}_2/\text{Pt}/\text{CFs}$  (full line) at  $1.4 \text{ V/RHE}$ .



After Pt deposition, the differently heat-treated CFs were coated with SnO<sub>2</sub> by nonaqueous ALD.<sup>23</sup> Based on approaches used for CNT coating,<sup>36</sup> Pt/CFs were contained during the deposition inside of a “tea bag” made of Kevlar mat. Tin *tert*-butoxide and acetic acid were used as metal and oxygen source, respectively.<sup>23</sup> Depositions took place in exposure mode home-made reactor at 175 °C and 20 ALD cycles were performed.

Structural characterization was performed by X-ray diffraction on a PANalytical X'pert powder diffractometer equipped with CuK $\alpha$  radiation ( $\lambda = 1.542 \text{ \AA}$ ). The Pt crystallite size was estimated by the Scherrer equation using the Pt (111) diffraction line at 39.7°.

Bright field TEM images were acquired on a Philips CM 200 LaB6 microscope operated at 200 kV. Phase contrast and STEM images were acquired on a Jeol-ARM200F equipped with a cold field emission gun and operated at 200 kV.

X-ray photoelectron spectroscopy was performed using a Physical Electronics PHI 5700 spectrometer with a non-monochromatic Mg K $\alpha$  radiation (300 W, 15 kV,  $h\nu = 1253.6 \text{ eV}$ ) as excitation source. Spectra were recorded at a 45° take-off angle by a concentric hemispherical analyzer operating in the constant pass energy mode at 25.9 eV, using a 720  $\mu\text{m}$  diameter analysis area. Core level C 1s, O 1s, Pt 4f and Sn 3d signals were recorded. Powdered solids were mounted on a sample holder without adhesive tape and kept overnight in a high vacuum chamber before they were transferred inside the analysis chamber of the spectrometer. Each region was scanned with several sweeps until a good signal to noise ratio was observed. The pressure in the analysis chamber was maintained below  $10^{-7} \text{ Pa}$ . PHI ACCESS ESCA-V6.0 F and Multipak 8.2b software packages were used for acquisition and data analysis. A Shirley-type background was subtracted from the signals. Recorded spectra were always fitted using Gauss–Lorentz curves in order to determine the binding energy of the different element core levels more accurately. The accuracy of the binding energy (BE) values was within  $\pm 0.1 \text{ eV}$ . Electrochemical analyses were carried out in a three-electrode cell comprising a gold (chronoamperometry) or glassy carbon (other voltammetric characterizations) rotating disk electrode (RDE) (working electrode geometric area  $0.196 \text{ cm}^2$ ), a reversible hydrogen electrode (RHE, reference electrode) and a platinum wire (counter electrode), and a Pine bipotentiostat model AFCBP1. All the potential values are referred to the RHE. Catalyst ink was prepared by mixing 10 mg Pt/CF catalyst with  $108.5 \mu\text{l}$  of 5% (w/w) aqueous/alcoholic solution of Nafion,  $300 \mu\text{l}$  of ethanol and  $30 \mu\text{l}$  of DI water. After 20 min of sonication,  $7 \mu\text{l}$  of ink was deposited onto the electrodes and dried for 10 min to obtain a total Pt loading of  $32 \mu\text{g}$  on the RDE tip. CV was performed in  $0.5 \text{ M H}_2\text{SO}_4$  solution saturated with either N<sub>2</sub> or O<sub>2</sub> on glassy carbon electrode after deposition of the electrocatalyst. In particular ECSA determination was performed by CV in  $0.5 \text{ M H}_2\text{SO}_4$  solution saturated with N<sub>2</sub> cycling between 0.05 and 1.2 V (vs. RHE) at a speed of  $50 \text{ mV s}^{-1}$  while ORR tests were performed by linear sweep voltammetry in  $0.5 \text{ M H}_2\text{SO}_4$  saturated with O<sub>2</sub> between 0.2 and 1.2 V (vs. RHE) at a scan speed of  $20 \text{ mV s}^{-1}$  and RDE rotating speeds of 400, 900, 1600 and 2500 RPM.

Cyclic voltammetry based accelerated degradation tests were performed by cycling between 0.6 and 1.2 V at  $100 \text{ mV s}^{-1}$  for 10 000 cycles measuring the ECSA every 100<sup>th</sup> cycle at  $50 \text{ mV s}^{-1}$ .

Potentiostatic accelerated stress tests were performed by holding the gold working electrode potential at 1.4 V vs. RHE for 2 h in  $0.5 \text{ M H}_2\text{SO}_4$  at 80 °C. Pt/CFs before and after SnO<sub>2</sub> ALD were characterized by TEM.

## Conclusions

By combining original synthetic approaches, *i.e.* electrospinning, microwave-assisted synthesis and atomic layer deposition, a novel electrocatalyst was elaborated with significantly improved stability over cycling. The addition of SnO<sub>2</sub> permitted a remarkable increase of the catalyst durability and even a slight increase in the Pt activity. Regarding the different characterizations presented in this work, it can be safely concluded that ALD of SnO<sub>2</sub> allows the protection of both the electrocatalyst and the support, while keeping intact their intrinsic catalytic activity and electrical conductivity, respectively. Lower corrosion of the carbon support, moderate aggregation of Pt particles and improved stability, adhesion and confinement on CFs of Pt NPs were observed when the electrocatalyst is decorated with tin oxide. The protection of Pt/CFs with metal oxide halves the degradation of the electrocatalyst over prolonged electrochemical cycling. Furthermore unhindered activity of Pt was observed suggesting no growth on the noble metal and preferential grow of tin dioxide on the carbon fibers although metal – metal oxide interaction seems to occur due to the proximity between these CF-supported components. It must be stressed that the successful selective SnO<sub>2</sub> decoration is only based on the difference in reactivity and density of anchoring sites of the Pt and CFs, without need of a protective organic layer around Pt, for example. Finally, this work certainly paves the way to the elaboration of modified carbon-based electrodes for fuel cells and related energy applications.

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## Notes and references

- 1 A. Rabis, P. Rodriguez and T. J. Schmidt, *ACS Catal.*, 2012, **2**, 864–890.
- 2 (a) R. Borup, J. Meyers, B. Pivovar, Y. S. Kim, R. Mukundan, N. Garland, D. Myers, M. Wilson, F. Garzon, D. Wood, P. Zelenay, K. More, K. Stroh, T. Zawodzinski, J. Boncella, J. E. McGrath, M. Inaba, K. Miyatake, M. Hori, K. Ota, Z. Ogumi, S. Miyata, A. Nishikata, Z. Siroma, Y. Uchimoto, K. Yasuda, K.-I. Kimijima and N. Iwashita, *Chem. Rev.*, 2007, **107**, 3904–3951; (b) L. Dubau, L. Castanheira, F. Maillard, M. Chatenet, O. Lottin, G. Maranzana, J. Dillet,



- A. Lamibrac, J.-C. Perrin, E. Moukheiber, A. ElKaddouri, G. de Moor, C. Bas, L. Flandin and N. Caqué, *Wiley Interdiscip. Rev.: Energy Environ.*, 2014, **3**, 540–560; (c) J. C. Meier, C. Galeano, I. Katsounaros, A. A. Topalov, A. Kostka, F. Schüth and K. J. J. Mayrhofer, *ACS Catal.*, 2012, **2**, 832–843; (d) Y. Shao, G. Yin and Y. Gao, *J. Power Sources*, 2007, **171**, 558–566; (e) Y. Shao-Horn, W. C. Sheng, S. Chen, P. J. Ferreira, E. F. Holby and D. Morgan, *Top. Catal.*, 2007, **46**, 285–305; (f) S. Zhang, X.-Z. Yuan, J. N. C. Hin, H. Wang, K. A. Friedrich and M. Schulze, *J. Power Sources*, 2009, **194**, 588–600.
- 3 (a) F. N. Büchi, M. Inanba and T. J. Schmidt, *Polymer Electrolyte Fuel Cell Durability*, Springer-Verlag, New York, 2009; (b) S. Maass, F. Finsterwalder, G. Frank, R. Hartmann and C. Merten, *J. Power Sources*, 2008, **176**, 444–451; (c) Y. Yu, H. Li, H. Wang, X.-Z. Yuan, G. Wang and M. Pan, *J. Power Sources*, 2012, **205**, 10–23.
- 4 C. A. Reiser, L. Bregoli, T. W. Patterson, J. S. Yi, J. D. Yang, M. L. Perry and T. D. Jarvi, *Electrochem. Solid-State Lett.*, 2005, **8**, A273–A276.
- 5 (a) M. Cai, M. S. Ruthkosky, B. Merzougui, S. Swathirajan, M. P. Balogh and S. H. Oh, *J. Power Sources*, 2006, **160**, 977–986; (b) J. Willsau and J. Heitbaum, *J. Electroanal. Chem. Interfacial Electrochem.*, 1984, **161**, 93–101; (c) K. Kinoshita and J. A. S. Bett, *Carbon*, 1974, **12**, 525–533.
- 6 B. M. J. N. Pourbaix, J. van Muylder and N. de Zoubov, *Platinum Metals Review*, 1959, **3**, 47–53.
- 7 (a) P. J. Ferreira, G. J. la O', Y. Shao-Horn, D. Morgan, R. Makharia, S. Kocha and H. A. Gasteiger, *J. Electrochem. Soc.*, 2005, **152**, A2256–A2271; (b) K. G. Gallagher, R. M. Darling and T. F. Fuller, in *Handbook of Fuel Cells: Advances in Electrocatalysis, Materials, Diagnostics and Durability*, ed. W. Vielstich, H. Yokokawa and H. A. Gasteiger, John Wiley and Sons, Chichester, 2003, vol. 6, pp. 819–829; (c) B. Vion-Dury, M. Chatenet, L. Guétaz and F. Maillard, *ECS Trans.*, 2011, **41**, 697–708.
- 8 (a) O. Yamazaki, Y. Oomori, H. Shintaku and T. Tabata, *ECS Trans.*, 2007, **11**, 287–295; (b) X. Cheng, Z. Shi, N. Glass, L. Zhang, J. Zhang, D. Song, Z.-S. Liu, H. Wang and J. Shen, *J. Power Sources*, 2007, **165**, 739–756.
- 9 (a) S. Chen, H. A. Gasteiger, K. Hayakawa, T. Tada and Y. Shao-Horn, *J. Electrochem. Soc.*, 2010, **157**, A82–A97; (b) H. R. Colón-Mercado, H. Kim and B. N. Popov, *Electrochem. Commun.*, 2004, **6**, 795–799; (c) J. Xi, J. Wang, L. Yu, X. Qiu and L. Chen, *Chem. Commun.*, 2007, 1656–1658; (d) J. Zhang, K. Sasaki, E. Sutter and R. R. Adzic, *Science*, 2007, **315**, 220–222.
- 10 M. Cao, D. Wu and R. Cao, *ChemCatChem*, 2014, **6**, 26–45.
- 11 (a) Z. Lin, L. Ji, W. E. Krause and X. Zhang, *J. Power Sources*, 2010, **195**, 5520–5526; (b) S. Park, Y. Shao, R. Kou, V. V. Viswanathan, S. A. Towne, P. C. Rieke, J. Liu, Y. Lin and Y. Wang, *J. Electrochem. Soc.*, 2011, **158**, B297–B302; (c) D. Sebastián, A. G. Ruíz, I. Suelves, R. Moliner, M. J. Lázaro, V. Baglio, A. Stassi and A. S. Aricò, *Appl. Catal., B*, 2012, **115–116**, 269–275.
- 12 (a) S. Cavaliere, S. Subianto, I. Savych, D. J. Jones and J. Rozière, *Energy Environ. Sci.*, 2011, **4**, 4761; (b) V. Thavasi, G. Singh and S. Ramakrishna, *Energy Environ. Sci.*, 2008, **1**, 205–221.
- 13 (a) Y. Shao, J. Liu, Y. Wang and Y. Lin, *J. Mater. Chem.*, 2009, **19**, 46–59; (b) Y.-J. Wang, D. P. Wilkinson and J. Zhang, *Chem. Rev.*, 2011, **111**, 7625–7651; (c) I. Savych, S. Subianto, Y. Nabil, S. Cavaliere, D. Jones and J. Rozière, *Phys. Chem. Chem. Phys.*, 2015, **17**, 16970–16976.
- 14 S. J. Tauster, *Acc. Chem. Res.*, 1987, **20**, 389–394.
- 15 (a) S. Cavaliere, S. Subianto, I. Savych, M. Tillard, D. J. Jones and J. Rozière, *J. Phys. Chem. C*, 2013, **117**, 18298–18307; (b) N. R. Elezović, B. M. Babić, V. R. Radmilović and N. V. Krstajić, *J. Electrochem. Soc.*, 2013, **160**, F1151–F1158; (c) A. Masao, S. Noda, F. Takasaki, K. Ito and K. Sasaki, *Electrochem. Solid-State Lett.*, 2009, **12**, B119–B122.
- 16 (a) A. Bauer, C. Song, A. Ignaszak, R. Hui, J. Zhang, L. Chevallier, D. Jones and J. Rozière, *Electrochim. Acta*, 2010, **55**, 8365–8370; (b) K. Miyazaki, K.-I. Kawakita, T. Abe, T. Fukutsuka, K. Kojima and Z. Ogumi, *J. Mater. Chem.*, 2011, **21**, 1913–1917.
- 17 J. Lu, B. Fu, M. C. Kung, G. Xiao, J. W. Elam, H. H. Kung and P. C. Stair, *Science*, 2012, **335**, 1205–1208.
- 18 N. Cheng, M. N. Banis, J. Liu, A. Riese, X. Li, R. Li, S. Ye, S. Knights and X. Sun, *Adv. Mater.*, 2015, **27**, 277–281.
- 19 Q. Du, J. Wu and H. Yang, *ACS Catal.*, 2014, **4**, 144–151.
- 20 J.-P. Tessonier, D. Rosenthal, T. W. Hansen, C. Hess, M. E. Schuster, R. Blume, F. Girgsdies, N. Pfänder, O. Timpe, D. S. Su and R. Schlögl, *Carbon*, 2009, **47**, 1779–1798.
- 21 I. Savych, J. Bernard d'Arbigny, S. Subianto, S. Cavaliere, D. J. Jones and J. Rozière, *J. Power Sources*, 2014, **257**, 147–155.
- 22 Y. Lin, S. Zhang, S. Yan and G. Liu, *Electrochim. Acta*, 2012, **66**, 1–6.
- 23 C. Marichy, N. Donato, M.-G. Willinger, M. Latino, D. Karpinsky, S.-H. Yu, G. Neri and N. Pinna, *Adv. Funct. Mater.*, 2011, **21**, 658–666.
- 24 C. Marichy, P. A. Russo, N. Donato, M. Latino, G. Neri and N. Pinna, *J. Phys. Chem.*, 2013, **117**, 19729–19739.
- 25 L. Jie and X. Chao, *J. Non-Cryst. Solids*, 1990, **119**, 37–40.
- 26 J.-M. Themlin, M. Chtaib, L. Henrard, P. Lambin, J. Darville and J.-M. Gilles, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 1992, **46**, 2460–2466.
- 27 (a) A. Lewera, L. Timperman, A. Roguska and N. Alonso-Vante, *J. Phys. Chem. C*, 2011, **115**, 20153–20159; (b) G. Samjeske, S.-I. Nagamatsu, S. Takao, K. Nagasawa, Y. Imaizumi, O. Sekizawa, T. Yamamoto, Y. Uemura, T. Uruga and Y. Iwasawa, *Phys. Chem. Chem. Phys.*, 2013, **15**, 17208–17218.
- 28 G. Jerkiewicz, *Electrocatalysis*, 2010, **1**, 179–199.
- 29 E. Yli-Rantala, A. Pasanen, P. Kauranen, V. Ruiz, M. Borghei, E. Kauppinen, A. Oyarce, G. Lindbergh, C. Lagergren, M. Darab, S. Sunde, M. Thomassen, S. Ma-Andersen and E. Skou, *Fuel Cells*, 2011, **11**, 715–725.
- 30 (a) A. J. Niskanen, T. Ylinen-Hinkka, M. Pusa, S. Kulmala and S. Franssila, *Thin Solid Films*, 2010, **519**, 430–433; (b) K. Kukli, M. Ritala, T. Pilvi, T. Aaltonen, J. Aarik, M. Lautala and M. Leskelä, *Mater. Sci. Eng. B*, 2005, **118**,



- 112–116; (c) K. Kukli, T. Aaltonen, J. Aarik, J. Lu, M. Ritala, S. Ferrari, A. Hårsta and M. Leskelä, *J. Electrochem. Soc.*, 2005, **152**, F75.
- 31 C. L. Platt, N. Li, K. Li and T. M. Klein, *Thin Solid Films*, 2010, **518**, 4081–4086.
- 32 C. Marichy, J.-P. Tessonnier, M. C. Ferro, K.-H. Lee, R. Schlögl, N. Pinna and M.-G. Willinger, *J. Mater. Chem.*, 2012, **22**, 7323–7330.
- 33 (a) H. S. Wroblowa, P. Yen Chi and G. Razumney, *J. Electroanal. Chem. Interfacial Electrochem.*, 1976, **69**, 195–201; (b) N. M. Marković, T. J. Schmidt, V. Stamenković and P. N. Ross, *Fuel Cells*, 2001, **1**, 105–116.
- 34 (a) A. Rabis, E. Fabbri, A. Foelske, M. Horisberger, R. Kötz and T. J. Schmidt, *ECS Trans.*, 2013, **50**, 9–17; (b) K. Kanda, Z. Noda, Y. Nagamatsu, T. Higashi, S. Taniguchi, S. M. Lyth, A. Hayashi and K. Sasaki, *ECS Electrochem. Lett.*, 2014, **3**, F15–F18; (c) P. Zhang, S.-Y. Huang and B. N. Popov, *J. Electrochem. Soc.*, 2010, **157**, B1163–B1172.
- 35 P. L. Antonucci, F. Romeo, M. Minutoli, E. Alderucci and N. Giordano, *Carbon*, 1988, **26**, 197–203.
- 36 C. K. Devine, C. J. Oldham, J. S. Jur, B. Gong and G. N. Parsons, *Langmuir*, 2012, **27**, 14497–14507.

