Ni-based bimetallic heterogeneous catalysts for energy and environmental applications

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Bimetallic catalysts have attracted extensive attention for a wide range of applications in energy production and environmental remediation due to their tunable chemical/physical properties. These properties are mainly governed by a number of parameters such as compositions of the bimetallic systems, their preparation method, and their morphostructure. In this regard, numerous efforts have been made to develop “designer” bimetallic catalysts with specific nanostructures and surface properties as a result of recent advances in the area of materials chemistry. The present review highlights a detailed overview of the development of nickel-based bimetallic catalysts for energy and environmental applications. Starting from a materials science perspective in order to obtain controlled morphologies and surface properties, with a focus on the fundamental understanding of these bimetallic systems to make a correlation with their catalytic behaviors, a detailed account is provided on the utilization of these systems in the catalytic reactions related to energy production and environmental remediation. We include the entire library of nickel-based bimetallic catalysts for both chemical and electrochemical processes such as catalytic reforming, dehydrogenation, hydrogenation, electrocatalysis and many other reactions.

1. Introduction

Population increase, urbanization, and rising living standards have rapidly increased global energy consumption and environmental burdens in the last half century. Energy consumption is expected to continue to increase dramatically in the coming years along with its associated environmental issues. Although there is no universal solution to solve all energy and environment-related problems, catalysis certainly plays a critical role in the design of efficient processes and systems able to maximize the value of starting materials while minimizing waste generation and energy requirements. Metal-based catalysts, in this regard, have been of immense importance in a wide range of diverse catalytic applications with high efficiency. However, fine-tuning of the structure and the properties of these catalysts is highly desirable to meet the stringent requirements in energy and environmental applications.

Nickel is one of the most widely used elements in metal based catalysts (see Fig. 1). It is the fourth most abundant transitional metal on earth after Fe, Ti and Zr. It currently costs 3.8 USD per lb, which is only 1/5000 of the price of gold. In fact, nickel has a long history in modern catalysis – its first application as a hydrogenation catalyst dates back to the 19th century which led to the Nobel Prize in Chemistry in 1912. Afterwards
Ni was found to be active in a number of processes, in particular in hydrogenation and reforming reactions. Despite the huge success and wide applications of the Ni catalyst in industry, single component Ni catalysts are not able to meet the activity, selectivity, and stability requirements in many emerging applications related to energy and environments.

Bimetallic catalysts, which often have electronic and chemical properties that are distinct from those of their parent metals, may show enhanced performances. Since the pioneering and systematic work by Exxon Research and Engineering in the early 1960s, the library of bimetallic catalysts has been significantly enriched, particularly in the past two decades. Among all bimetallic catalysts, platinum-group metals are the most studied catalyst components. However, high cost and low availability limit their applications in large scale processes. Therefore, attention turned towards nickel, a low-cost alternative, which has similar electronic properties and can perform many of the same elementary reactions as palladium or platinum. In fact, Ni is known for its high alloying efficiency with all noble metals as well as many transition metals in different mass ratios, which makes it easier to develop a wide range of composition-dependent bimetallic Ni systems for diversified catalytic applications. Recently, there have been many reports on the facile synthesis of bimetallic Ni systems, which have shown the potential to replace expensive noble metal catalysts in terms of catalytic activity and stability.

After a detailed survey of recent publications on bimetallic Ni, we found that the majority of them were focused on catalytic reactions relating to energy, and to a lower extent the environment, which reflects the growing concern of bimetallic heterogeneous catalysis in these domains. This contribution aims to provide a critical overview of the entire library of Ni-based heterogeneous bimetallic catalysts with their recent synthesis protocols in view of their applications in a wide range of chemical processes. A rationalized approach is provided to identify suitable metal combinations that may be able to provide improved activities in selected applications compared to conventional

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and/or presently reported systems. Different energy-related catalytic processes will be discussed where the influence of modification of the Ni catalysts by other metals and the relation to their catalytic properties, will be introduced. Additionally, a brief discussion on the fundamental approach using classical theories of chemistry (such as the d-band theory) to understand the origin of the improved efficiency and stability of the bimetallic systems will also be provided.

Recently, several reviews based on homogeneous Ni-based complexes were published focusing mainly on the C–C coupling reactions.7,8 Two excellent reviews based on heterogeneous Ni-based catalysts were published focusing exclusively on reforming reactions.9,10 Nevertheless, to the best of our knowledge, there is currently no review focused on bimetallic Ni-based catalysts that provides a detailed discussion on their energy and environmental applications. We hope that this contribution will be a good addition to the existing literature, and will provide useful information for future research.

2. Preparation of bimetallic Ni catalysts

A number of factors are responsible for the structure of bimetallic catalysts (see Fig. 2). At present, there are many well-established methods for preparing bimetallic catalysts (either unsupported colloidal NPs or supported bimetallic NPs).2,3 The choice of method often depends on the desired surface and the bulk structure of the catalyst. For instance, the co-impregnation process is mainly used to produce supported bimetallic or alloy type materials. On the other hand, the sequential impregnation method is often adopted to obtain core–shell type materials, where a less active metal (generally a 3d transition metal) core is prepared first and then the active metal (generally a noble metal) is deposited onto it. Wet impregnation methods are widely applicable for the syntheses of bimetallic catalysts with well-controlled shape, size, and composition.11,12 Various wet-chemical schemes have been applied to synthesize bimetallic NPs. They can be classified into two categories according to the formation mechanisms: seed-mediated growth and one-pot co-reduction. The two strategies have similar fundamental principles. In the seed-mediated growth process, the metal seeds of the comparatively inactive metal are first prepared and then dispersed in a solution of active metal precursors. The controlled reduction of the second metal forms uniform layers over the seeds and a core–shell structure is obtained. In the one-pot co-reduction method, two metallic precursors are added at the same time. In this case, the reduction potentials of the metals play a key role in determining the final architecture. Two possibilities arise here: (1) metals with a similar reduction potential are reduced simultaneously and form an alloyed structure, and (2) metals with different reduction potentials are reduced in a successive manner and form a core–shell structure. However, there is no straightforward relationship between reduction kinetics and reduction potential. The reduction kinetics also depends on the synthesis conditions applied. For example, the use of surfactants, stronger reducing agents (such as NaBH₄) or high temperature solvothermal processes can simultaneously reduce metals with different reduction potentials resulting in an alloyed structure.13–16 Alongside the wet impregnation processes, much attention has been paid to colloidal chemistry to synthesize unsupported NPs with controlled size, shape, and stability.17 While colloidal chemistry is highly applicable towards the syntheses of noble metal bimetallic systems, its application in 3d transition metals is less studied.
Apart from the preparation methods, another factor that determines the structure of a bimetallic system is the relative position of two metals in the periodic table. A solid solution or miscible system is formed when the two metals are very close in the periodic table. For example, nickel is miscible with Co, Cu, Rh, Pd, and Ir at any proportions as shown in Fig. 3, and therefore can easily form alloys. The metals which are further from nickel generally form intermetallic compounds. For example, Pt forms different intermetallic compounds with Ni at different specific ratios, among which Pt₃Ni is the most stable compound and is very well known for its electrocatalytic applications. Although the predicted structure can be derived from the experimental data presented in the periodic table, it is not necessary that the final structure should be similar to that of the predicted one. Different variable structures can also be obtained by using a controlled preparation method. The reduction potential of the metal plays a crucial role in the formation of a definite structure since in most cases the bimetallic catalysts are prepared by reducing their salt precursors. In fact, multiple factors need to be considered when predicting the relationship between the predicted and experimentally obtained structure of a bimetallic system.

Structural modification largely enhances the capability of tuning the catalytic performance, therefore it is important to have the knowledge of the surface structure and properties of the catalyst to derive the relationship between their structural features and catalytic activity. In the past decade, significant efforts have been made to understand the surface properties of bimetallic systems using advanced characterization techniques (e.g. Auger electron spectroscopy (AES), X-ray photoelectron spectroscopy (XPS), extended X-ray absorption fine structure (EXAFS) spectroscopy, low-energy electron diffraction (LEED), etc.) as well as theoretical calculations (e.g. density functional theory (DFT)). To reveal the origin of the novel catalytic properties, bimetallic surfaces have also gained a considerable amount of interest in surface science research. Since the characterization methods for bimetallic systems have already been discussed in some excellent reviews, we would like to pay our attention to discussing how different structures of bimetallic Ni catalysts are obtained depending on their synthesis method.

### 2.1 Core–shell structure

In principle, bimetallic core–shell structures can be obtained either by seed-mediated growth or by one-pot co-reduction of metallic precursors. In particular, for the bimetallic Ni@noble metal core–shell structure, Ni serves as a core and the noble metal serves as a shell. This kind of structure is generally prepared using a seed-mediated growth process, where Ni cores are prepared by reducing their salt precursor prior to the deposition of the noble metal on their surface. In most cases, capping ligands are used in this step to prevent aggregation. It should be noted that the one-pot co-reduction method cannot form this structure because of the higher reduction potential of noble metals than that of Ni. In this case, noble metals will be reduced first and Ni will be deposited subsequently as a shell over the noble metal core.

The reverse structure, i.e. noble metal@Ni core–shell, can be obtained in a one-pot sequential reduction. For example, the preparation of Au@Ni core–shell NPs with varying Ni shell thicknesses was reported by mixing both metal precursors in one-pot in the presence of oleylamine and 1-octadecene. The reduction of the Au precursor to Au NPs was achieved by using NaBH₄ as the reducing agent at room temperature. At an increased temperature (210 °C), the as-formed Au seeds acted as the nucleation sites on which nickel ions were reduced. The different shell thicknesses could be controlled by using different ratios of two precursors. Because of the higher electron density, noble metal cores sometimes induce the reduction of Ni, which is termed as noble-metal induced reduction where no external reducing agent is required.

The core-multishell is a more complex architecture in this category, which is well known for its good optical and electronic properties. More precise kinetic control over the reaction is required to achieve the structure. Recently, well-shaped Pd–Ni–Pt core–sandwich–shell NPs were synthesized using cubic and octahedral Pd substrates in the aqueous phase at low temperature with a cationic surfactant as the capping agent and hydrazine as the reducing agent. The combination of shaped Pd substrates and mild reduction conditions directed the overgrowth of Ni and Pt in an oriented, layer-by-layer fashion. Scheme 1 demonstrates how Pd cubes function as shaped crystal substrates to catalyze and direct the oriented overgrowth of Ni. Pt ions were added after the Ni overgrowth to “trap” the metallic Ni phase and complete the layer-by-layer synthesis of the shaped ternary metal NPs.

Post-modification of an alloy precursor through dealloying and surface oxidation is another way to prepare a core–shell structure. This method was recently applied by the Strasser group to prepare IrNi@IrOₓ core–shell NPs from IrNiₓ precursor alloys. Ni-rich bimetallic Ir–Ni NPs were first prepared using a conventional polyol method involving 1,2-tetradecanediol as the reducing agent and oleylamine along with oleic acid as the capping ligands. The hybrid IrNiₓ@IrOₓ core–shell materials were prepared in two ways (Fig. 4). In the first approach, the IrNiₓ NP precursor alloys (PA-IrNiₓ) were electrochemically dealloyed to
form metallic core–shell NPs (“D-IrNi”x) with an Ir enriched surface, and subsequently they were selectively surface oxidized to form “SO-IrNi@IrOx,” metal oxide core–shell NPs. Alternatively, the dealloying and oxidation could be performed directly in one step to obtain DO-IrNi@IrOx.

2.2 Allo yed structure

Alloy systems are formed when two metal atoms have a homogeneous distribution in one particle. Some metals are thermodynamically more stable when mixing together, while for others the reaction kinetics must be rigidly controlled to produce an alloyed structure. One approach is to use strong reducing agents that reduce all metal precursors simultaneously to form a homogeneous mixture of metals. For example, bimetallic Ni–Fe alloy NPs could be formed using NaBH₄ as the reducing agent, although these two metals cannot be mixed with a random ratio thermodynamically.⁵,¹² The appropriate selection of surfactants or counterions adjusts the redox potentials of metals through specific adsorption or coordination, leading to the simultaneous reduction of different metal ions.⁵³ Surfactants can also play a key role in directing the reaction and crystal growth pathways in yielding particles with a desired geometry. For example, (111) surface-dominant Pt₃Ni alloy nanocrystals – the best-known catalyst for the oxygen reduction reaction (ORR) – can be prepared by reducing the metal precursors using CO₂, in the presence of oleylamine (OAm) and oleic acid (OA) as the capping ligands.⁵⁴,⁵⁵

Well-faceted nanocrystal alloys were also reported to form without any capping agents. Carpenter et al. reported the solvothermal synthesis of ORR active Ni–Pt alloy catalysts using a mild reducing agent, N,N-dimethylformamide, which also served as the solvent.¹⁵ The effect of temperature on the reduction kinetics of the metal precursors was studied. It was observed that Ni(acac)₂ was more difficult to reduce than Pt(acac)₂ and did not react up to 150 °C. When the temperature was further increased to 200 °C, 90% Ni reduction was observed. Another controlled reaction with only the Ni precursor at the same temperature showed merely 42% Ni reduction, suggesting that the presence of Pt and/or Pt(acac)₂ enhances the deposition of Ni. The converse also appeared to hold true because the apparent reaction onset temperature of the mixed precursor solution (115 °C) was lower than that of the Pt(acac)₂-only solution (137 °C). These observations suggest that the free energy of formation of the Ni–Pt alloy NPs from the reaction mixture is more negative than the free energy of formation of platinum NPs from the same solution. Another probable reason could be that under the reaction conditions Pt proto-particles of only a few atoms were formed initially and acted as seed crystals for subsequent Ni and Pt₃Ni deposition, which was also supported by the previous finding by Deivaraj et al. that the reduction of Ni ions by hydrazine at room temperature requires the presence of Pt nuclei.³⁶ This method was recently extended to prepare trimetallic Pt–Ni–Co alloy NPs at 130 °C.³⁷

Alongside the wet chemistry methods, gas phase synthesis has also been reported for bimetallic Ni alloys.³⁸ As a “bottom-up” approach, the gas phase method is more complex since it starts from atomic-level precursors and needs better control over nucleation and growth of nanocrystals. The advantage of this method is that it does not require any reducing agent or surfactant. Lin and Sankaran reported a plasma-assisted scalable method for the synthesis of NiCu alloys from the vapors of organometallic precursors, bis(cyclopentadienyl)nickel [Ni(Cp)₂] and copper acetylacetonate [Cu(acac)₂].³⁸ By carefully combining precursor vapors and varying the flow rates, a wide range of compositionally controlled alloyed NPs (less than 5 nm) with narrow size distributions were obtained.

2.3 Porous structure

Generally, bimetallic alloys form crystalline particles with very low surface areas, which is a limitation for applications in catalytic processes. The surface area is one of the crucial factors for a good catalytic performance. As such, porous structured alloys – which have the advantages of high surface area, high gas permeability, high mass diffusion ability and low density – are more promising in catalytic applications than their solid counterparts. In 1927, Murray Raney produced porous Ni (Raney Ni) by selective leaching of a block of Ni–Al alloy (NiAl and Ni₂Al₃) with concentrated sodium hydroxide;³⁹ this has been used as a heterogeneous catalyst for more than 80 years due to its low cost and high catalytic activity. After this report, chemical dealloying became a widely accepted route to develop many porous alloys and is still used in many applications.
Wang et al. developed a facile chemical dealloying process to produce porous NPs using nanocrystalline alloys as precursors.  

The non-noble metal components were selectively dissolved with an excess amount of concentrated nitric acid to obtain a nanoporous residue. This general pathway could be applied to any nanocrystalline alloys of noble and non-noble metals (such as Ni–Pt, Ni–Rh) to produce the corresponding nanoporous NPs with increased surface areas and narrow pore-size distributions.

Recently, an electrochemical dealloying technique was reported using an improved and more selective process for leaching of an alloy precursor material to form porous alloys. The dealloying mechanism is based on the selective dissolution of the less-noble component from a binary or multicomponent solid solution at a potential where the remaining more-noble component is free to diffuse along the surface at which 3D porosity evolves. The process intrinsically forms a core–shell nanoporous structure where the surface is passivated by the more-noble component and the interior of the ligaments maintains a significant residual fraction of the less-noble component. Chen et al. reported a nanoporous PdNi (np-PdNi) bimetallic catalyst fabricated by electrochemically dealloying a Pd$_{20}$Ni$_{80}$ alloy in an acid solution at a low applied potential.  

The key advantage of this process is that the residual Ni in the nanoporous alloy could be easily controlled by tuning the dealloying potentials. The electrochemical dealloying was also applied to make nanoporous Ni–Pt alloy NPs with a hierarchical structure and a high surface area. 

Apart from the dealloying process, templating pathways can also be used to generate a porous structure. For example, porous Ni@Pt core–shell nanotubes were prepared via the electrodeposition method using ZnO nanorods as templates.

Scheme 2 describes the synthetic pathway for well-defined porous Ni@Pt core–shell nanotube arrays. ZnO nanorod arrays were first synthesized on conductive substrates utilized as templates. Then, the electrodeposition of Ni layers was carried out on the surfaces of the ZnO nanorods to prepare ZnO@Ni core–shell nanorod arrays, and Pt thin layers were further deposited on the surfaces of the Ni shells to prepare ZnO@Ni@Pt triple-layered core–shell nanorod arrays. Finally, porous Ni@Pt core–shell nanotube arrays were synthesized from the ZnO@Ni@Pt triple-layered core–shell nanorod arrays by dissolving ZnO in a weak alkali solution.

This method is facile and suitable for large-scale and low-cost production under mild conditions in the absence of organic surfactants.

An analogous method was reported to prepare a Ni–Pt framework structure using a metal–organic framework as the template (Fig. 5). In the first step, a Ni-enriched truncated octahedral Ni–Pt alloy was prepared through a surfactant-assisted solvothermal method, which was then dispersed in N,N-dimethylformamide containing an appropriate amount of dihydroxyterephthalic acid and autoclaved at 110 °C for 12 h to form a Ni–Pt frame@Ni-MOF. Finally, the Ni–Pt frame@Ni-MOF was dispersed in dilute acetic acid to decompose the Ni-MOF, resulting in the formation of a bare Ni–Pt frame. This is an example of using combined top-down and bottom-up strategies, where organic linkers captured the abandoned Ni$^{2+}$ ion during the dealloying process, to build a shell of MOFs on the surface of the Ni–Pt alloy in situ.

### 2.4 Others

Apart from the discussions above (i.e. core–shell, alloy and porous structures), some other structures are also reported for bimetallic Ni catalysts. For example, hollow bimetallic (Ni/Au, Ni/Ag, Ni/Pt, and Ni/Pd) spheres were synthesized via a decomposition and reduction route by using hollow nickel hydroxide spheres as precursors. Hollow Ni(OH)$_2$ microspheres were first prepared through a hydrothermal method and subsequently calcined in air to produce a NiO sphere. Hollow metallic nickel spheres were then obtained by the H$_2$ reduction of NiO hollow spheres. Different hollow bimetallic spheres were then obtained via a replacement reaction route by using hollow metallic Ni spheres and the corresponding noble metal precursors, where the Ni spheres acted as sacrificial templates. The driving force of these reactions comes from the large standard reduction potential gap between the Ni$^{2+}$/Ni redox pair (−0.25 V vs. standard hydrogen electrode (SHE)) and the Mn$^{2+}$/Mn redox pair (1.00 V for AuCl$_4^{-}$/Au, 0.80 V for Ag$^+/Ag$, 0.74 V for PtCl$_6^{3-}$/Pt, and 0.83 V for Pd$^{2+}$/Pd vs. (SHE), respectively).
3. Modification of the surface properties of bimetallic Ni catalysts: fundamental understanding

Understanding the origins of the novel catalytic properties of bimetallic surfaces has gained considerable interest in fundamental surface science research. Two critical factors can be considered. First, the formation of heteroatom bonds changes the electronic environment of the metal surface, thereby modifying its electronic structure through the ligand effect. Second, the geometry of the bimetallic structure is typically different from that of the parent metals (e.g. the average metal–metal bond lengths change, resulting in the strain effect that can modify the electronic structure of the metal through changes in the orbital overlap). Theoretical approaches, such as density functional theory (DFT), have recently been extensively applied for a better understanding of the surface properties and design principles of different bimetallic systems. In this section, we will emphasize the fundamental roles of added guest metals in modifying the catalytic behavior of the host metal.

In a bimetallic system, the catalytic reactivity depends on the combined electronic effect of two metal components. d-Band theory can be applied to understand the combined effect of two metal species. The chief principle underlying the d-band theory is that the binding energy of an adsorbate to a metal surface is largely dependent on the electronic structure of the surface itself. The metal d-band hybridizes with the bonding (σ) orbital of the adsorbate to form bonding (d–σ) and antibonding (d–σ)* states (Fig. 6a). For the metals we are concerned with, the (d–σ) state is full, but the extent of filling of the (d–σ)* state depends on the local electronic structure of the metal at the surface, i.e. the surface density of states. An increased filling of the antibonding (d–σ)* state corresponds to a destabilization of the metal–adsorbate interaction and hence weaker binding, which induces higher activity.

Fig. 6 (a) Hybridization of the d-band of metal and the σ orbital of the adsorbate. (b) d-Band center with respect to the Fermi level and dissociative absorption energy as a function of Pd content (figure generated from data in ref. 48).
Using a polycrystalline Pt foil as the substrate, the Ni atoms were found to undergo inward diffusion upon exposure to H₂ and surface segregation after exposure to O₂. This reversible behavior was also applicable to bimetallic Ni–Pt NPs. Fig. 7 shows the XPS Ni/Pt intensity ratio, which oscillates with the oxidation–reduction cycles. The XPS results indicate that the Ni–Pt NP surface is NiO-rich in oxidizing gases and Pt-terminated in reducing gases. In turn, such structural changes modify the catalytic performance in both hydrogenation and oxidation reactions, and could be the main reason behind the observation that the subsurface Pt–Ni–Pt structure works better in hydrogenation reactions, while the surface Ni–Pt–Pt structure is more suitable for oxidation or reforming reactions.

4. Catalysis applications of bimetallic Ni catalysts

Since Ni has similar electronic properties as Pd and Pt, its application is widely explored in similar reactions as the other two. Here we will critically discuss recent advances in bimetallic Ni catalysts where both noble metals (Ru, Rh, Ir, Pd, Pt, Au, and Ag) and transition metals (Fe, Co, and Cu) have been used as guest metal counterparts (see Fig. 8). However, in some cases Ni also acts as a guest metal or promoter to modify the catalytic activity of reactive noble metals. One issue with Ni-based bimetallic catalysts is that Ni is often partially oxidized when exposed on the catalyst surface due to its relatively low reduction potential. However, oxidation of Ni is not necessarily detrimental since Ni in the oxidized form can enhance catalytic performance by changing the geometric and/or electronic environment of the second metal. For this reason, we will include those examples in the discussion even if both metal elements are not in the metallic state.

This section will be divided into two subsections focusing on energy and environmental applications, respectively. The first section is further divided by the type of energy carrier, including hydrogen, hydrocarbons, oxygenates, and electricity, whereas the second section on environmental remediation is categorized by the type of targeted pollutant. Wherever possible, we will compare the catalytic activities of bimetallic Ni catalysts with those of their monometallic counterparts, and provide reasons for the improved activities on the basis of their electronic and geometric configuration. We will also look into fundamental studies of bimetallic Ni catalysts in order to understand the catalytic mechanisms at the molecular level.

4.1 Energy production

4.1.1 Production of H₂ as an energy carrier. Hydrogen is foreseen to become a major energy carrier in the future. The establishment of a sustainable hydrogen-based energy infrastructure forces us to develop clean/renewable hydrogen production, efficient hydrogen storage, and convenient distribution. Catalysis is not only essential for hydrogen production, but also plays an important role in hydrogen storage. Numerous research efforts have been made in the storage of H₂ by both physical and chemical approaches. In physical storage, H₂ remains in physical forms, i.e. as gas, supercritical fluid, adsorbate, or molecular inclusions. Although physical storage by means of pressurizing could hold higher hydrogen densities, it is complicated by several safety concerns and logistical obstacles. A limitation with other physical H₂ storage approaches (such as using adsorbing materials) is their low storage capacity. Conversely, chemical H₂ storage offers a high storage performance due to the strong binding of hydrogen and the high storage densities. In recent years, hydrogen storage materials and methods – including metal hydrides, metal–organic frameworks, on-board reforming of hydrocarbon into hydrogen, and organic materials – have been investigated extensively. In all cases, catalytic materials are of immense importance in making the process effective and highly feasible. Noble metal catalysts work excellently, but bimetallic Ni catalysts with a small amount of noble metals were recently shown to be very promising as well. In this section, we will discuss the developments of bimetallic Ni catalysts in different hydrogen
production processes such as catalytic reforming, dehydrogenation, water–gas shift (WGS) reaction, and electrocatalysis.

4.1.1.1 Catalytic reforming. Catalytic reforming is a widely used technique for the production of hydrogen from different resources such as natural gas, oil, coal, and alcohols. Specifically, high-temperature steam reforming of hydrocarbons (i.e. methane at over 800 °C) accounts for a significant portion of worldwide commercial hydrogen generation (about 50%).60 Another potential application of steam reforming is the on-board hydrogen generation for fuel-cell powered vehicles.62 Noble metals are known to be the best catalysts for hydrocarbon and alcohol reforming due to their greater ability to break C–C bonds.57,61,64 However, recent attention has been slightly shifted to 3d transition metals, preferably Ni-based catalysts, which are also effective in breaking C–H and C–C bonds.10 Nevertheless, nickel-based catalysts are very sensitive to deactivation by sintering and carbon deposition.63 Unfortunately, both desired reforming reaction and undesired coke deposition are plausibly initiated by the same elementary hydrocarbon activation step,66 and under steam-reforming conditions metal surfaces are covered with various CHx intermediates. Without a fast steam gasification step to convert these intermediates to CO and H2, these adsorbed CHx species on Ni can undergo further dehydrogenation, polymerization, and rearrangement into highly stable carbon.67 It has been reported that the addition of noble metals to Ni catalysts can promote the reducibility of Ni, and stabilize it during the catalytic process.68,69 Indeed, significant efforts have been made in the formulation of bimetallic Ni catalysts during the last decade, with major research focused on how to prevent catalyst deactivation by carbon deposition. In this section, we will include some specific examples of these bimetallic systems and discuss the fundamental role of each component in overcoming this issue.

4.1.1.1.1 Reforming of hydrocarbons. Steam reforming and dry reforming of light hydrocarbons, such as methane and butane provide a promising method for hydrogen production. Although steam reforming of methane yields synthesis gas with a high H2:CO ratio of about 3:1, dry (CO2) reforming of methane has certain advantages since it utilizes two abundantly available green-house gases to produce industrially important syngas and can reduce net emissions of these gases.57 However, compared to H2O reforming, CO2 reforming causes more severe coke formation because of the increased C/H molar ratio in the feedstock. Therefore, the development of a coke-resistant catalyst is the major challenge for CO2 reforming of hydrocarbons.

Dry reforming of methane (DRM) has been investigated over both noble (Rh, Ru, Pd and Pt) and non-noble metal (Ni, Co and Fe) based catalysts.70,71 In spite of the high cost, noble metal catalysts have drawn attention due to their superior coking resistance, higher stability, and activity especially for higher temperature applications (> 750 °C). Among different noble metals, Rh has been identified as the best candidate with the following trend observed in the catalytic activity and stability of a series of alumina supported noble metal catalysts: Rh/γ-Al2O3 > Ru/γ-Al2O3 > Ir/γ-Al2O3 > Pd/γ-Al2O3 > Pt/γ-Al2O3.72 The addition of a small amount of Rh to the Ni catalyst, encouragingly, further enhanced catalytic activity without any coke formation. According to Rostrup-Nielsen, the coke resistance of Ni-based catalysts can be enhanced by the adsorption of steam (in the case of the steam reforming process) or CO2, by enhancing the rate of the surface reaction, or by decreasing the rate and the degree of methane activation and dissociation.73 Various promoters such as alkali or alkaline earth metals can be used to achieve this.71 However, major research has been focused on noble metals as promoters because of their high activity and excellent coking resistance. It has been proved that carbon formation occurs less on noble metals than on Ni, mainly because the lower solubility of carbon in noble metals favors the gasification of carbon. In fact, many previous works have reported that Ni catalysts can exhibit high efficiency and better resistance against carbon deposition when modified with noble metals such as Pd,74 Pt,75–78 Ru,84,85 Rh,86–91 Ir,92 Au,93–97 and Ag.98–100 The effects of these secondary noble metals are diverse; they may function to reduce and stabilize the metal particle size of the Ni catalysts (e.g. Pt,75,77,78 Rh91), to tailor the ensemble size of the Ni catalysts (e.g. Ag,98 Au93), to block the step sites (e.g. Au93), or to modify the surface electronic properties of the Ni catalysts (e.g. Au93). The modification of Ni catalysts with noble metals was reviewed in some early reviews and it has been demonstrated as a promising approach to design catalysts with excellent performances in methane reforming.69,77,82,103 We will mainly focus on the fundamental role of noble metals in altering the catalytic and coke resistance properties of bimetallic Ni systems.

A landmark paper by Nørskov and co-workers reported that the Au/Ni surface alloy on the Ni particles (supported on MgAl2O4) was active for steam reforming and more resistant towards carbon formation than the pure Ni catalyst.93 The catalyst was designed based on the fact that when Au is added to any of the low index Ni surfaces, an alloy is formed in the first atomic layer.104 Since the Au atoms have a high electron density, the neighboring Ni atoms experience an enhanced electron density and a higher effective coordination number simultaneously. The advantage of Ni surface modification by Au can be determined by two factors: (i) the ability of the surface to activate hydrocarbon molecules and (ii) the tendency of the surface to bind C and form graphite. The abstraction of the first H atom from CH4 is considered as the rate-limiting step in the steam-reforming process over pure Ni catalysts. The addition of Au to the Ni surface could slightly increase the energy barrier of the CH4 dissociation step, as confirmed through DFT calculations and experimental methods. Therefore, Au impeded CH4 dissociation as expected. However, when the effect of Au addition was considered for the second factor, i.e. tendency to bind C, it was observed that the Au-modified Ni surface had a much lower ability to adsorb C. On the pure Ni surface, the most stable adsorption site was the threefold hexagonal close-packed site. However, the threefold sites adjacent to a gold atom were unstable, and even the threefold sites that were the next nearest neighbors to the Au atoms were substantially destabilized. The effect of Au on atomic C adsorption was thus considerably stronger than the effect on CH4 activation, and eventually led to a coke resisting catalyst without much compromise of activity.
Bimetallic Ni–Pt catalysts behave in a similar way to Ni–Au. In a recent work, supported Ni/Pt bimetallic NPs with a controlled surface composition and structure were prepared. The surface restructuring of the bimetallic catalysts upon thermal treatment was investigated, which demonstrated the structure evolution of the bimetallic NPs from Pt monolayer island-modified Ni NPs to core–shell bimetallic NPs composed of a Ni-rich core and a Ni/Pt alloy shell. The surface modification of the Ni-based catalysts by adding Pt atoms effectively enhanced the catalytic activities and resistance towards carbon formation in the dry reforming process. To assess the surface and bulk structure according to Pt/Ni elemental composition, a series of alumina-supported Ni/Pt bimetallic NPs with various Pt coverages were prepared and tested. DFT calculations suggested that the addition of Pt to the Ni surface might facilitate the CH oxidation pathway and inhibit the carbon oxidation pathway. This led to enhanced catalytic activity and suppressed carbon formation as the Pt coverage increased.

Modification by Ag follows a different mechanism to improve the catalytic and coke resistance properties of the Ni catalysts. Kang et al. reported a Ni/Ag/MgAl2O4 catalyst containing equimolar amounts of Ni and Ag for the steam reforming of butane. During butane reforming, the Ag and Ni components played a role in the oxidation of the feed gases. The main products from steam reforming over the Ni/MgAl2O4 catalyst without the Ag component were H2, CO, CO2, and CH4 with a small amount of C2-. However, the addition of Ag reduced the degree of carbon deposition and improved the H2 product selectivity by eliminating the formation of all C2- products. The unmodified Ni/MgAl2O4 catalyst experienced strong Ni sintering at a high temperature. It was also proved that the catalytic performances differed according to the order in which the metal precursors were added. Fig. 9 illustrates the phase changes of different catalysts during the butane reforming process. Simultaneous addition of Ag/Ni depressed the NiAlO4 spinal structure and induced catalytic deactivation due to their strong sintering. When Ag was added between Ni and Al, deactivation was reduced significantly, while simultaneously improving the catalytic activity.

In addition to carbon deposition on the catalysts, sulfur poisoning is another serious issue, which is often seen during the steam reforming of hydrocarbons due to sulfur contaminants. The bimetallic Ni–Rh catalyst on the CeO2–Al2O3 support exhibited better sulfur tolerance than their monometallic counterparts at 550 °C, although the catalytic performance of the bimetallic catalyst was inferior compared with the pure Rh catalyst. Unlike the Ni catalyst, the Rh catalyst dramatically improved its sulfur tolerance upon increasing the temperature to 800 °C. The superior sulfur tolerance of the Rh catalyst at this high temperature could be associated with its better capability in sulfur oxidation than Ni, which formed different sulfur species on the metal surface. It was observed that the metal sulfide and organic sulfide were the dominant sulfur species on the Ni catalyst, while sulfonate and sulfate predominated on the Rh catalyst. The presence of sulfur induced the formation of nickel sulfide which suppressed the carbon gasification and caused severe carbon deposition on the Ni catalyst at 800 °C. This could be one of the reasons for the lower activity of the bimetallic Rh–Ni catalyst compared with pure Rh.

Along with the use of noble metal promoters, 3d transition metals, especially Fe, Co and Cu, also improved the activity and coke resistance properties in the methane reforming reaction. In a recent study, a series of bimetallic Fe–Ni/MgAl2O4 catalysts with Fe/ Ni ratios between 0 and 1.5 were examined for methane dry reforming at 650–800 °C. In H2-TPR, Fe2O3 and NiO were reduced above 700 °C to form a Fe–Ni alloy, constituting the active phase for the methane dry reforming reaction (Fig. 10). This alloy remained stable in a flowing gas stream of CO2 during reoxidation until 627 °C, but was decomposed to metallic Ni and Fe. The probability of carbon deposition was lower. The process of dry reforming on Ni–Fe could be described by the Mars–van Krevelen mechanism, where CO2 oxidizes Fe to FeO and CH4 is activated on the Ni sites to form H2 and surface carbon. This surface carbon was oxidized by FeO, lattice oxygen to produce CO, thereby reducing the probability of carbon deposition.

4.1.1.1.2 Reforming of oxygenates. The production of H2 from renewable resources such as ethanol and other small molecule oxygenates (i.e. acetone, glycerol, ethylene glycol, etc.) has received special attention in recent years. Among different metal catalysts investigated, late transition metals such as Ni, Co, Pt, and Ru are still the major active components due to their high activity in breaking C–H and C–C bonds. Although oxygenate reforming requires comparatively lower temperature than that of hydrocarbons, coke formation on the metal surface
is more inclined to take place. In a recent review article, Li and Gong explained the different possible pathways of alcohol reforming on oxide and supported metal catalysts, where the metal surface is proposed to be the primary active site for the reforming process.10 In the case of Ni, carbon deposition becomes severe upon the aggregation of Ni particles.124 Therefore, metal dispersion and inhibition of metal sintering are critical in the development of an efficient nickel reforming catalyst.

Skeletal Ni is considered to be a highly active catalyst due to its considerable nickel dispersion and large exposed surface area. Gong et al. reported low-temperature steam reforming of ethanol using skeletal Ni (Ni–Al alloy powder prepared from 50 wt% Ni and 50 wt% Al)-based catalysts in combination with different assistant metals such as Pt, Cu, and Co.125 It was observed that three different assistant metals play different roles in the reaction; Pt and Cu suppress the methanation and enhance H2 production, while Co promotes the methanation and increases CH4 selectivity. It has been proved that dissociative adsorption of CO is generally suppressed from left to right and from 3d to 5d in the periodic table of transition-metal elements.126 Therefore, it can be rationalized that Cu and Pt could suppress the dissociation of CO on the Ni surface, and consequently suppress the methanation reaction, whereas Co would enhance the dissociation of CO on the Ni surface.

The incorporation of noble metals such as Pt and Rh can simultaneously improve the reforming activity and prevent the catalyst deactivation.117–123 Aqueous phase reforming of ethylene glycol over supported Ni–Pt/C and Ni–Pt/γ-Al2O3 catalysts revealed that the enhanced activity of the bimetallic catalysts was correlated with the changes in the catalyst structure.129 Under the reaction conditions, Ni segregated to the surface of the catalysts, resembling Ni-terminated bimetallic surfaces that were more active than Pt as identified in theoretical and experimental studies on model surfaces. Very recently, Moraes et al. investigated the effect of Pt addition on the performance of a Ni/CoO2 catalyst for low temperature steam reforming of ethanol.127,128 Based on different characterization techniques, they provided an explanation addressing why Ni/CoO2 deactivated more extensively than Ni–Pt/CoO2. In the first step, both catalysts are able to decompose the ethoxy species, the dehydrogenated species (acetaldehyde, acetyl species), and the acetate species into H2, CO, and CH4. Following that, there are two possibilities: (i) the CHx species can be hydrogenated and desorbs as methane or may react with water producing H2 and CO or, (ii) these CHx species may be further dehydrogenated to carbon.123 Therefore, when the rate of this reaction pathway is higher than the rate of desorption of CHx species such as CH4, carbon is accumulated over the surface and the catalyst deactivates. In situ X-ray absorption studies revealed the formation of a nickel carbide phase during the reforming process over the Ni/CoO2 catalyst, which was associated with amorphous carbon deposition and catalyst deactivation. The addition of Pt to the Ni/CoO2 catalyst promoted the decomposition of dehydrogenated and acetate species into hydrogen, methane, CO and carbonate species (Fig. 11). The segregated Pt effectively produced reactive hydrogen species by dissociative adsorption of hydrogen and spillover of adsorbed hydrogen atoms to the Ni surface. These highly reactive hydrogen atoms hydrogenated the adsorbed carbon precursor species, which eventually desorbs as methane. As such, the segregation of Pt on the surface of the Ni particles minimized the formation of nickel carbide and promoted the catalyst stability (Table 1).

Among the noble metal-free catalysts, bimetallic Ni–Cu catalysts are one of the most studied bimetallic systems for ethanol steam reforming.116,119,134,135,137–142 It has been shown that the addition of Cu to Ni catalysts highly promotes the WGS reaction to instantly convert the adsorbed CO into CO2. Furthermore, Cu addition induces the decomposition of CHxCHO, which is one of the intermediates in the coke formation process.139 Apart from the dry reforming and steam reforming processes, another promising alternative way to produce syngas is the partial oxidation of methane (POM) and other hydrocarbons. POM is an exothermic catalytic process in which methane is converted to form H2 and CO in the presence of a limited amount of oxygen (or air). Compared to the early success of methane steam reforming, catalytic partial oxidation remained almost unexplored until 1990. Since the first reports by Huszar et al. and Gavalas et al., a significant amount of research has been carried out on Ni/Al2O3.143 However, deactivation occurred in all cases due to the formation of NiAl2O4. Furthermore, carbon deposition was another major issue on nickel catalysts, which reduced the number of active sites of the catalysts. It was observed that both the support and the promoter had a considerable effect on the activity and the stability of the catalysts.144 Al2O3 could be replaced by other supports such as La2O3, MgO, SiO2, CeO2, ZrO2, and TiO2, which act as promoters and reduce the sintering of the active Ni phase into the support. Different bimetallic Ni catalysts consisting of noble metals such as Pt,145 Ru,146–149 Rh,150 and Ir151 as well as non-noble metals such as Co149,152,153 Cu,154 lanthanides (Pr, Gd, Lu)155 and actinides (Th, U)156 have been studied. In all cases, the added second metals exhibited increased reducibility and higher coke resistance of the catalysts as observed in the bimetallic Ni catalysts for reforming reactions.

4.1.1.2 Production of H2 through dehydrogenation and hydrolysis. Developing hydrogen storage materials is essential for a viable
### Table 1  Catalytic performance of bimetallic Ni catalysts in the reforming reaction of hydrocarbons and oxygenates

<table>
<thead>
<tr>
<th>Catalyst</th>
<th>M/Ni (wt/wt)</th>
<th>Synthesis method</th>
<th>Reaction</th>
<th>T (°C)</th>
<th>Catalytic performance</th>
<th>Note</th>
<th>Ref.</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ni–Ptγ-Al₂O₃</td>
<td>0.33</td>
<td>IWI</td>
<td>DRM</td>
<td>700</td>
<td>69% CH₄ conv.</td>
<td>Ni increased the electron-withdrawing ability of Pt</td>
<td>76</td>
</tr>
<tr>
<td>Ni–Ptγ-Al₂O₃</td>
<td>0.05</td>
<td>IWI</td>
<td>DRM</td>
<td>750</td>
<td>78% CH₄ conv.</td>
<td>Carbon deposition was markedly lowered</td>
<td>79</td>
</tr>
<tr>
<td>Ni–Pt@Holl S-1</td>
<td>0.34</td>
<td>IWI</td>
<td>DRM</td>
<td>800</td>
<td>&gt; 70% CH₄ conv.,</td>
<td>Hollow silicate shell prevented coke deposition on encapsulated Ni</td>
<td>82</td>
</tr>
<tr>
<td>Ni–Pd/ZrO₂–La₂O₃</td>
<td>0.25</td>
<td>IWI</td>
<td>DRM</td>
<td>700</td>
<td>73% CH₄ conv.</td>
<td>Segregation of metals led to the formation of Ni-rich surface alloy</td>
<td>74</td>
</tr>
<tr>
<td>Ni–Rh/Al₂O₃</td>
<td>0.33</td>
<td>IWI</td>
<td>DRM</td>
<td>700</td>
<td>87% CH₄ conv.</td>
<td>Higher activity and stability due to the presence of the redox couple Ce⁴⁺/Ce³⁻ and Rh⁰/Rh⁺</td>
<td>86</td>
</tr>
<tr>
<td>Ni–Rh/CeO₂–Al₂O₃</td>
<td>0.1</td>
<td>IWI</td>
<td>DRM</td>
<td>750</td>
<td>85% CH₄ conv.</td>
<td>Ce-Zr mixed oxide support increased the gasification of surface coke</td>
<td>90</td>
</tr>
<tr>
<td>Ni–RhCe₂Zr₃.5₁</td>
<td>0.1</td>
<td>Pseudo sol–gel</td>
<td>DRM</td>
<td>800</td>
<td>&gt; 90% CH₄ conv.</td>
<td>Au prevented the formation of carbon nanotubes</td>
<td>97</td>
</tr>
<tr>
<td>Ni–Au/MgAl₂O₄</td>
<td>0.057</td>
<td>IWI</td>
<td>DRM</td>
<td>800</td>
<td>100% CH₄ conv.</td>
<td>Defective CeOₓ–ZrOᵧ crystalline lattice increased carbon oxidation</td>
<td>108</td>
</tr>
<tr>
<td>Ni–CoO₂–ZrO₂</td>
<td>1.5</td>
<td>DP, HT</td>
<td>DRM</td>
<td>800</td>
<td>&gt; 55% CH₄ conv.</td>
<td>Co produced more H₂ and maintained the reduced state of Ni</td>
<td>109</td>
</tr>
<tr>
<td>Ni–CoO₂–ZrO₂</td>
<td>1.0</td>
<td>IWI</td>
<td>DRM</td>
<td>750</td>
<td>90% CH₄ conv.,</td>
<td>Co induced the formation of spinel-type NiCo₂O₄ solid solution to result in d-electron transfer from Co to Ni</td>
<td>112</td>
</tr>
<tr>
<td>Ni–Co/MSN</td>
<td>1.0</td>
<td>In situ electrolysis</td>
<td>DRM</td>
<td>783</td>
<td>97% CH₄ conv.,</td>
<td>Surface carbon oxidized FeOₓ lattice oxygen</td>
<td>107</td>
</tr>
<tr>
<td>Ni–Fe/MgAl₂O₄</td>
<td>0.7</td>
<td>IWI</td>
<td>DRM</td>
<td>800</td>
<td>51% CH₄ conv.</td>
<td>Oxidized Ni and Rh species increased the activity</td>
<td>117</td>
</tr>
<tr>
<td>Ni–Rh/CeZrO₂</td>
<td>0.017</td>
<td>IWI</td>
<td>DRM</td>
<td>680–740</td>
<td>H₂ yield 10.6 mol mol⁻¹ n-butane</td>
<td>High activity due to high dispersion, high metal area and high reducibility of Ni</td>
<td>109</td>
</tr>
<tr>
<td>Ni–Ru/CeO₂–Al₂O₃</td>
<td>0.1</td>
<td>Sol–gel</td>
<td>ATR of n-dodecane</td>
<td>750</td>
<td>H₂ yield 1.6 mol mol⁻¹ n-dodecane</td>
<td>Addition of Ag increased H₂ selectivity by reducing C₂⁻ products</td>
<td>99</td>
</tr>
<tr>
<td>Ni–Ag/MgAl₂O₄</td>
<td>0.11</td>
<td>IWI</td>
<td>SR of n-butane</td>
<td>700</td>
<td>100% butane conv., 68% H₂ yield</td>
<td>Ni modified the crystallite and electronic structure of Pt</td>
<td>130</td>
</tr>
<tr>
<td>Ni–Pt/CeO₂–Al₂O₃</td>
<td>0.08</td>
<td>IWI</td>
<td>SRE</td>
<td>500</td>
<td>60.8% H₂ yield</td>
<td>Lewis acidic NiAl₂O₄ phase decreased coke formation</td>
<td>119</td>
</tr>
<tr>
<td>Ni–Pt/CeO₂–Al₂O₃</td>
<td>0.17</td>
<td>IWI</td>
<td>APR of glycerol</td>
<td>240</td>
<td>86% H₂ yield</td>
<td>High activity due to bimetallic and support effects</td>
<td>117</td>
</tr>
<tr>
<td>Ni–Rh₂O₃–Al₂O₃</td>
<td>0.13</td>
<td>IWI</td>
<td>SRE</td>
<td>402</td>
<td>44.9% H₂ yield</td>
<td>Cu enhanced the WGS reaction and favored acetaldhey decomposition and reforming over the ethanol dehydrogenation</td>
<td>134</td>
</tr>
<tr>
<td>Ni–Cu/ZrO₂</td>
<td>0.54</td>
<td>DP</td>
<td>OSR of methanol</td>
<td>360</td>
<td>60% H₂ yield</td>
<td>Ni suppressed undesirable methanation reaction</td>
<td>135</td>
</tr>
<tr>
<td>Ni–Cu/ZrO₂</td>
<td>0.33</td>
<td>Urea co-precipitation</td>
<td>SRE</td>
<td>600</td>
<td>84% H₂ yield</td>
<td>Ni suppressed undesirable methanation reaction</td>
<td>136</td>
</tr>
<tr>
<td>Ni–Cu/MWNT</td>
<td>0.08</td>
<td>Reflux</td>
<td>APR of glycerol</td>
<td>240</td>
<td>72% H₂ yield</td>
<td>Ni suppressed undesirable methanation reaction</td>
<td>135</td>
</tr>
</tbody>
</table>

IWI: incipient wet impregnation; DP: deposition–precipitation; HT: hydrothermal method; DRM: dry reforming of methanol; SRE: steam reforming of ethanol; ATR: auto-thermal reforming; OSR: oxidative steam reforming; APR: aqueous phase reforming.
hydrogen economy. An ideal hydrogen storage material should satisfy several technical requirements. These include: sufficiently high volumetric and gravimetric capacities, facile release of hydrogen at a reasonably low temperature, and efficient regeneration at a practical temperature.\textsuperscript{59,157} Hydrides of boron and nitrogen have drawn significant interest because they are light atoms with high gravimetric hydrogen capacities. In addition, hydridic B–H and protic N–H bonds can thermally or catalytically dissociate to yield hydrogen. Many chemical storage materials, such as ammonia, ammonia borane, hydrazine, hydrazine borane, and formic acid, are reported, where two main processes, dehydrogenation and hydrolysis, are generally involved in the production of $\text{H}_2$.

### 4.1.1.2.1 Dehydrogenation of ammonia

Decomposition of ammonia has recently gained increased attention due to the potential of ammonia to be used as a hydrogen storage medium. Ammonia can be liquefied easily at a pressure of 8 atm at 20 °C, leading to high energy densities. As a result of its high hydrogen storage capacity, ammonia can serve as a fuel to provide CO\textsubscript{2} free hydrogen through catalytic decomposition.\textsuperscript{158} It has been shown that the heat of nitrogen chemisorption is a good descriptor for ammonia synthesis and decomposition.\textsuperscript{159,160} The binding energy of the nitrogen atom to the surface must be strong enough for dehydrogenation of the $\text{NH}_3$ species to occur, but sufficiently weak that the nitrogen recombines to desorb from the surface to complete the catalytic cycle. Initial studies on single-metal catalysts showed that Ru is the most active decomposition catalyst,\textsuperscript{161} but it is expensive and therefore not employable for large scale applications. Later on, studies on bimetallic catalysts showed that Co–Mo is even more active than Ru, which triggered more exploration on a series of transition metal-based bimetallic systems that can potentially replace the precious single noble metals.\textsuperscript{159,160}

Vlachos et al. reported an interesting, rational approach to designing bimetallic Ni catalysts with a comparable ammonia decomposition activity to Ru.\textsuperscript{162,164} Using microkinetic modeling combined with DFT studies, the Ni–Pt–Pt(111) surface was predicted to be a catalytically active surface. According to the calculation, the Ni–Pt–Pt(111) bimetallic surface has a nitrogen binding energy of 130.7 kcal mol\textsuperscript{-1}, slightly lower than Ru (141.6 kcal mol\textsuperscript{-1}), and is a potentially active catalyst. While on the other hand, the subsurface configuration, Pt–Ni–Pt(111), and the parent metals, Pt(111) and Ni(111), were expected to have lower activities because of their weaker nitrogen binding energies (87.5, 102.1 and 113.8 kcal mol\textsuperscript{-1} respectively). This was verified using temperature-programmed desorption and high-resolution electron energy loss spectroscopy experiments. 3 L (where L indicates Langmuir, $1 \text{ L} = 1 \times 10^{-6}$ Torr s) of ammonia was dosed at 350 K, then the temperature was ramped at a heating rate of 3 K s\textsuperscript{-1} and desorption of nitrogen was monitored using a mass spectrometer. The Ni–Pt–Pt surface was the only one that showed activity towards ammonia decomposition under these conditions, as indicated by the peak at 626 K (Fig. 12). This confirmed the model predictions of the Ni–Pt–Pt surface being active towards ammonia decomposition based on an optimal nitrogen binding energy and the other three surfaces being inactive due to a nitrogen binding energy that was too low. The activity of the Ni–Pt–Pt surface was also compared with that of the Ru(0001) surface. In a previous study of ammonia decomposition on Ru(0001), an exposure of 3500 L of ammonia was dosed at 500 K to achieve a nitrogen saturation coverage.\textsuperscript{165} In comparison, saturation coverage was achieved with 3 L at 375 K on the Ni–Pt–Pt surface. The significantly lower dosing temperature and ammonia exposure clearly indicated that the overall dehydrogenation barrier was much lower than that for the bimetallic surface. Along with the success of the Ni–Pt catalyst, noble metal-free Ni-based bimetallic catalysts (such as Ni–Fe alloy NPs, and core–shell Ce–NiO@SiO\textsubscript{2}) were also explored for the decomposition of ammonia.\textsuperscript{166,167} However, the temperature applied in these cases was very high (773–1073 K) to achieve a high conversion.

### 4.1.1.2.2 Hydrolysis of ammonia borane

Although ammonia is easily available and can be stored safely, for on-board applications it is desirable that the storage materials are able to release hydrogen at a moderate temperature. Consequently, an air stable compound ammonia borane ($\text{NH}_3\text{BH}_3$, AB), which has a hydrogen capacity of 19.6 wt%, which is well above the US Department of Energy targets (2015) of a gravimetric density (9 wt%),\textsuperscript{59} and can be catalytically hydrolyzed at room temperature, received considerable attention.

There are many reports on Ni–noble metal catalytic systems for the hydrolysis of AB. Noble metal containing hollow bimetallic (Ni/Au, Ni/Ag, Ni/Pt, and Ni/Pd) catalysts were prepared via a decomposition and reduction route and tested for hydrogen generation from AB.\textsuperscript{45} The Ni/Pt catalyst was most active among all the combinations. In another study, the same results were found using a combination of Pt and transition metals such as Fe, Co and Ni.\textsuperscript{168} Ni–Pt NPs with a ratio of 1:4 exhibited the best catalytic activity. The Ni oxidation state in the Ni–Pt NPs seems to be responsible for the corresponding catalytic activity in AB decomposition. As confirmed by a XANES study, Ni remains in a metallic state in the Ni–Pt (1:4) NPs but a higher oxidation state...
of Ni is found in the Ni–Pt (1 : 1) NPs and Ni–Pt (4 : 1) NPs leading to a reduced catalytic performance (Fig. 13).

Chen et al. reported ultra-small magnetic Ni@Ru core–shell NPs, which showed enhanced activity in the hydrolysis of AB. A TOF value of 114 min⁻¹ was achieved for the Ni@Ru NPs which was higher than that of monometallic Ru NPs (31.5 min⁻¹). The same group reported Ni₄Ru₁₋ₓ (x = 0.56–0.74) alloy NPs with different Ni/Ru ratios, among which the Ni₀.7₄Ru₀.2₆ sample performed as the best catalyst for AB hydrolysis. The hydrolysis activation energy for the Ni₀.7₄Ru₀.2₆ alloy catalyst was approximately 37 kJ mol⁻¹, which is considerably lower than the values measured for monometallic Ni (∼70 kJ mol⁻¹) and Ru NPs (∼49 kJ mol⁻¹). This value is also lower than that previously reported for Ni@Ru (∼44 kJ mol⁻¹) and most of the noble metal-containing bimetallic NPs reported in the literature. Ru@Ni core–shell NPs supported on graphene were synthesized via one-step in situ co-reduction, affording a TOF value of 340 min⁻¹. The number is much higher than the reversed Ni@Ru NPs, which could be due to the presence of a more reactive Ru in the shell.

Ni–Au NPs of 3–4 nm diameter embedded in silica nanospheres were prepared via in situ reduction in an aqueous solution of NaBH₄/ NH₄BH₃. Compared to monometallic Au@SiO₂ and Ni@SiO₂, the as-synthesized Ni–Au@SiO₂ catalyst showed a higher catalytic activity and better durability in the hydrolysis of ammonia borane, generating a nearly stoichiometric amount of hydrogen at 18 °C. Triple-layered Ag@Co@Ni core–shell NPs containing a silver core, a cobalt inner shell, and a nickel outer shell were prepared via an in situ chemical reduction method. Compared with its bimetallic core–shell counterparts, this catalyst showed a higher catalytic activity for the hydrolysis of AB. Ni–Co double shells surrounding the silver core in the special triple-layered core–shell structure provided increasing amounts of active sites on the surface to facilitate the catalytic reaction.

3d transition metal-based catalysts comprised of Ni were also explored for the hydrolysis of AB with good activity, where Ni–Fe and Ni–Cu combinations were found to be the most active. Xu and coworkers reported magnetically recyclable Fe₁₋ₓNiₓ nano-alloy catalysts which exhibited Pt-like high catalytic activity. Kim et al. prepared bimetallic NiCu nanorods (NRs) incorporated into carbon nanofibers (NFs) that showed superior catalytic activity toward H₂ release from AB as well as excellent recyclability and chemical stability. The activation energy (∼28.9 kJ mol⁻¹) for the reaction was very low over the catalyst. Recently, CeO₂ supported bimetallic Ni–Fe NPs were reported as efficient noble-metal-free catalysts for AB hydrolysis. The catalyst is comprised of highly disperse and partially oxidized amorphous Ni–Fe NPs stabilized by strong interactions with the CeO₂ support via Ni–O–Ce and Fe–O–Ce bonding. The influence of Fe/Ni ratio on catalytic activity revealed a volcano-shaped relationship with a maximum at Fe/Ni = 1 : 1 (Fig. 14). The volcano-shaped activity order clearly suggested that the formation of a uniform FeNi alloy structure (at Fe/Ni = 1 : 1) on the surface of CeO₂ and the synergistic effect originated from the integration of Fe with Ni.

### 4.1.1.2.3 Dehydrogenation of hydrazine and hydrazine borane.

Anhydrous hydrazine (N₂H₄) is another promising hydrogen storage material because of its high H₂ content (12.5 wt%) and its liquid state at room temperature. However, the direct use of anhydrous hydrazine is restricted because it is extremely toxic, highly reactive, and potentially explosive. Therefore, hydrous hydrazine (N₂H₄·H₂O) is often used due to safety concerns. Complete decomposition of hydrazine yields only hydrogen and nitrogen according to the following equation:

\[
\text{N}_2\text{H}_4 \rightarrow \text{N}_2(g) + 2\text{H}_2(g) \quad [\Delta H = -95.4 \text{ kJ mol}^{-1}] (1)
\]

![Fig. 14](image-url) Effect of the Fe/Ni molar ratio in the hydrogen production from AB. The inset shows the TON versus Ni content. (Copyright 2015 Wiley-VCH.)
Meanwhile, hydrazine can also incompletely decompose into ammonia and nitrogen, as follows:

\[ 3\text{N}_2\text{H}_4 \rightarrow 4\text{NH}_3(g) + \text{N}_2(g) \quad [\Delta H = -157 \text{ kJ mol}^{-1}] \quad (2) \]

From the perspective of hydrogen storage, reaction (1) must be selectively promoted and reaction (2) restrained. The dissociation pathways depend significantly on the catalyst and reaction conditions. Initial research findings showed that noble metals such as Ir and Rh were highly effective for the decomposition of hydrazine.\(^\text{178,179}\) However, hydrogen selectivity is highly dependent on the reaction conditions (mainly temperature) and the nature of the catalysts. Earlier studies achieved maximum hydrogen selectivity up to only 43.8%, which was due to these two competing reactions during the decomposition. Later on, non-noble metals such as Ni were incorporated to reduce the material cost and Ni-based bimetallic catalysts such as Ni–Ir,\(^\text{180,181}\) Ni–Rh,\(^\text{13,182–187}\) Ni–Pt,\(^\text{14,188–197}\) and Ni–Pd,\(^\text{198,199}\) and exhibited a superior catalytic performance compared to their monometallic counterparts.

Xu and coworkers reported that the combination of Rh, Pt, and Ir with Ni could catalyze the complete decomposition of hydrous hydrazine at room temperature with 100% H\(_2\) selectivity.\(^\text{13,180,188}\) A surfactant-assisted co-reduction process was applied to synthesize bimetallic Rh–Ni catalysts with different Rh/Ni ratios. Despite nickel itself being inactive to the reaction, the presence of nickel drastically enhanced H\(_2\) selectivity to a maximum of 100% at Rh/Ni = 4:1 (Fig. 15).\(^\text{13}\) Physically mixed Rh NPs and Ni NPs with the same Rh/Ni ratio did not show any activity enhancement over Rh, confirming the role of the bimetallic synergistic effect. Alloying of Rh and Ni led to a modification of the catalyst surface and tuned the interactions of Rh with the N–N and N–H bonds as well as the stability of the reaction intermediates on the catalyst surface. Although the catalytic activity of this Rh–Ni catalyst is very impressive, the use of a high amount of Rh (80 mol% in Rh\(_x\)Ni\(_{1-x}\)) is not appealing from an economical point of view. Therefore, the same group synthesized Ni–Pt and Ni–Ir catalysts with much lower noble metal content (7 mol% Pt and 5 mol% Ir, respectively) and achieved similar results to the Ni–Rh catalysts.\(^\text{180,188}\) The surfactant-assisted process enhanced the activity by suppressing the agglomeration of the NPs, without affecting the bimetallic compositions of the NPs.

In spite of the quantitative selectivity, sluggish reaction kinetics is a major issue in hydrazine decomposition. In the above discussed work by Xu et al., the addition of surfactants during the preparation of the NPs makes it difficult to separate the catalysts from the reactants and also significantly reduces the reaction rate.\(^\text{13,180,188}\) Wang et al. reported a surfactant-free method to prepare a supported catalyst by depositing Ni–Rh NPs on graphene oxide, where the support played a key role in obtaining highly dispersed Ni–Rh NPs.\(^\text{183}\) Ni–Rh catalysts prepared this way exhibited 100% H\(_2\) selectivity and remarkably high activity to complete the decomposition reaction of hydrous hydrazine within only 49 min in the presence of NaOH at room temperature, which was more than three times faster than that of the previously reported single metallic catalysts.\(^\text{174,200–201}\)

Luo et al. proposed a facile liquid impregnation approach for the immobilization of ultrafine bimetallic Ni–Pt NPs inside the pores of MIL-101 (Fig. 16).\(^\text{194,195}\) Highly dispersed bimetallic Ni–Pt NPs with different compositions were obtained that showed remarkable activity, selectivity, and durability towards hydrogen generation from aqueous alkaline solution of hydrazine. The catalysts showed composition dependent catalytic activity, among which Ni\(_{35}\)Pt\(_{65}\)/MIL-101 exhibited the highest catalytic activity, with a turnover frequency (TOF) value of 375.1 h\(^{-1}\) at 50 °C and 65.2 h\(^{-1}\) at room temperature. The same group reported Ni–Pt NPs dispersed on MIL-96, which exhibited a TOF of 114.3 h\(^{-1}\) and 100% hydrogen selectivity at room temperature with a composition of Ni\(_{40}\)Pt\(_{60}\)/MIL-96.\(^\text{193}\) In both cases, excellent catalytic performances were due to the synergistic effect of the metal organic framework (MOF) support and Ni–Pt NPs, since Ni–Pt NPs supported on other conventional supports – such as SiO\(_2\), carbon black, γ-Al\(_2\)O\(_3\), poly(N-vinyl-2-pyrrolidone) (PVP), and the physical mixture of Ni–Pt and MIL-96 – exhibited inferior catalytic activities. Unfortunately, the exact nature of the interaction between the metal NPs and MOF was not clear. When comparing the activities of the two catalysts, Ni\(_{35}\)Pt\(_{65}\)/MIL-101 and

---

**Fig. 15** Selectivity for hydrogen generation from hydrous hydrazine (0.5 M) catalyzed by Rh\(_x\)Ni\(_{1-x}\) (x = 0–64; y = 0–16) with Rh/NiH\(_4\) = 1:10 at room temperature.\(^\text{13}\) (Copyright 2009 American Chemical Society.)

**Fig. 16** (a) Synthesis of NiPt@MIL-101 nanocatalysts. (b) Time course plots and (c) durability test for the decomposition of aqueous solution of hydrazine over NiPt@MIL-101 with NaOH (0.5 M) at 50 °C (catalyst = 0.1 g; N\(_2\)H\(_4\)-H\(_2\)O = 0.1 mL).\(^\text{194}\) (Copyright 2014 American Chemical Society.)
Ni₈₅Pt₁₅/MIL-96, MIL-96-supported catalysts showed better activity at room temperature. This could be understood by the structures of these two MOF materials. The pore size of MIL-96 is about 1.2 nm, which is much smaller than that of MIL-101 (2.9 nm). As a result, most of the metal NPs are expected to remain on the surface of MIL-96 instead of going inside the pores. Therefore, it is expected that the Ni–Pt NPs on the surface of MIL-96 are more exposed to the substrate molecules. However, at an increased temperature (50 °C), the Ni₈₅Pt₁₅/MIL-101 catalyst showed increased activity, which could likely be due to the higher diffusion of the substrate through the pores and better contact with the Ni–Pt NPs located inside the pores. In a recent work, Luo and Cheng reported ultrafine monodisperse bimetallic Ni–Pt NPs on graphene by the co-reduction of nickel acetylacetonate and platinum acetylacetonate with borane-tert-butylamine in oleylamine. The catalyst with a composition of Ni₃₃Pt₆₆/graphene exhibited the highest TOF of 415 h⁻¹ with 100% hydrogen selectivity at 50 °C.

The development of a noble-metal-free catalyst is of economic advantage and is crucial for promoting the potential application of hydrazine as a hydrogen storage material. Many groups reported the Ni–Fe combination to be an effective catalyst for the dehydrogenation of hydrous hydrazine. Xu et al. reported high-performance bimetallic Ni–Fe alloy NPs for the complete and selective decomposition of hydrazine hydrate under moderate conditions. The H₂ selectivity was 80% at 50 °C and 100% at 70 °C in the presence of 0.5 M NaOH, but the catalyst was inactive at room temperature. Tang et al. prepared monodispersed Ni₃Fe single-crystalline nanospheres on carbon with a specific surface area of 182.3 m² g⁻¹ which resulted in 100% H₂ selectivity and exceedingly high activity (TOF = 528 h⁻¹) at room temperature. Wei and co-workers synthesized bifunctional Ni–Fe alloy/MgO catalysts containing both an active center and a solid base center. The catalyst showed a comparable activity to most reported noble metal catalysts, exhibiting 100% conversion and 99% H₂ selectivity at room temperature. The strong basic MgO support excluded the requirement of an externally added base (such as NaOH), which was used in many other studies to increase activity. Hydrazine borane (N₂H₄BH₃, HB) is another H₂ storage material which has a gravimetric hydrogen storage capacity of 15.4 wt% and can be easily prepared by mixing sodium borohydride and hydrazine hemisulfate at room temperature. The aqueous solution of HB is stable against spontaneous decomposition for 15.4 wt% and can be easily prepared by mixing sodium borohydride and hydrazine hemisulfate at room temperature.

A series of Ni-based bimetallic systems were investigated with Pt, Ru, Rh, or Ir as the second metal. The results showed that most of the NiₓMₓ nanocatalysts outperformed the monometallic Ni, Pt, Ru, Rh, and Ir catalysts. The best performance achieved was 5.1 ± 0.05 mol (H₂ + N₂) per mol (HB) with Ni₅₀Pt₅₀, Ni₆₀Ru₄₀, Ni₅₀Rh₅₀, Ni₅₀Ir₅₀, Ni₆₀Ru₄₀Pt₂₀, Ni₅₀Rh₅₀Pt₂₀, Ni₅₀Ir₅₀Pt₂₀ and Ni₅₀Rh₅₀Ir₂₀. Using Ni₅₀Ru₄₀Pt₂₀ and Ni₅₀Rh₅₀Pt₂₀ NPs, 5.79 ± 0.05 equiv. (H₂ + N₂) per HB could be released, corresponding to a H₂ selectivity as high as 93 ± 1%. The NiₓMₓPtₓ NPs were capable of hydrolyzing the BH₃ group of HB and then decomposing the N₂H₄ group at 50 °C, whereas the monometallic Ni and Pt were inactive for the second reaction. Xu and co-workers reported a sodium-hydroxide-assisted reduction approach to synthesize ultrafine surfactant-free bimetallic Ni–Pt NPs supported on nanoporous carbon, Maxsorb MSC-30. The catalyst exhibited remarkable catalytic activity towards the complete dehydrogenation of hydrazine borane with 100% H₂ selectivity at room temperature. It has been found that catalytic activity and H₂ selectivity are strongly dependent on the Ni/Pt ratio (Fig. 17). Both monometallic Ni and Pt nanocatalysts showed activity for hydrogen release by hydrolysis of the BH₃ group in HB only, whereas the Ni₁₋ₓPtₓ/Maxsorb MSC-30 catalysts with platinum contents in the range of 15–70 mol% exhibited high catalytic activities and 100% hydrogen selectivity with 5.95 ± 0.05 equiv. (H₂ + N₂) per HB released. NaOH served as an efficient dispersing agent to control the particle size during the formation of NiPt NPs and also played an important role as a catalyst promoter (Table 2).

4.1.1.3 Production of H₂ through the WGS reaction. Water gas shift reaction (WGS) is a reversible exothermic reaction in which carbon monoxide reacts with water (steam) to form carbon dioxide and hydrogen (eqn (3)). WGS is an important reaction typically used during and after reforming to increase the yield of H₂. CO is oxidized by H₂O to produce an additional mole of H₂ with CO₂ as a waste gas. Generally, a two-step WGS reactor is employed in large-scale industrial plants: high-temperature shift (with a Cu/ZnO/Al₂O₃ catalyst) and low-temperature shift (with a Cu/ZnO/Al₂O₃ catalyst). For the low-temperature copper-based WGS catalysts, the first step (H abstraction from H₂O) is rate-limiting for the entire process. Therefore, much importance has been given to develop new WGS catalysts with high activity toward H₂O dissociation at low temperatures.
Cu in the WGS process, which indicates that introducing an Ni component to the Cu-based catalysts may lower the barrier of H₂O splitting and ultimately accelerate the WGS process at low temperatures.

One of the most important detrimental factors in the WGS process is the dissociation of CO which leads to the formation of CH₄. In addition to the high H₂O dissociation activity of Ni, it also has a high activity towards CO activation. Therefore, an optimum concentration of Ni is required to achieve high WGS selectivity by minimizing the undesired methanation reaction. Zhao et al. performed detailed DFT calculations to study H₂O and CO dissociations on a set of Ni–Cu bimetallic surfaces aiming at exploring the optimal Ni ensemble on Cu(111) for an efficient WGS process. Fig. 18 illustrates the favorable process on different bimetallic Ni–Cu catalysts with different compositions. It was found that Ni additives in the Cu(111) surface layer including a Ni monomer remarkably enhance water splitting. As for CO dissociation on the three selected CuNi surfaces (Ni monomer, dimer, and trimer–z), the reaction barrier on the Ni monomer was as high as the value on pure Cu(111), implying that C–O breaking was unfavorable on the Ni monomer. In contrast, CO dissociation on the Ni dimer and trimer–z was highly promoted, and the calculated barriers were very close to that on pure Ni(111). The conclusion from these studies is that increasing Ni loading can induce the promotional effects on C–O bond breaking to facilitate the undesired methane yield.
Therefore, bimetallic Ni–Cu catalysts with highly dispersed Ni ensembles containing a lower Ni concentration are desirable for better activity and selectivity toward WGS.

In the last few years, the WSG reaction has been extensively studied over a bimetallic Ni–Cu system where the main concern was to suppress the methanation reaction by increasing the CO adsorption.216–223 In a recent study, experimental analyses such as CO-TPR-MS, CO-TPD-MS and in situ DRIFTS have proved that the CO adsorption can be enhanced on a Ni–Cu alloy at a high temperature.224 The Ni–Cu/CeO₂ catalyst with a Ni/Cu ratio of one exhibited a high reaction rate with the least methane formation due to the formation of a Ni–Cu alloy phase. Strong CO adsorption strength at a high adsorption temperature implied that the formation of a Ni–Cu alloy prevents the dissociation of CO. At the same time, it can prevent the formation of the carbon species “formate”, which could block the reaction active site and produce methane as an undesired side product. It is noteworthy that the surface lattice oxygen mobility of ceria could be activated with the formation of a Ni–Cu alloy particularly at high reaction temperatures.

4.1.1.4 Production of H₂ through electrocatalysis. Electrocatalytic splitting of water is expected to play a key role in the future sustainable production of hydrogen from electricity. This process can be divided into two half-redox reactions, hydrogen evolution reaction (HER) on the cathode and oxygen evolution reaction (OER) on the anode. The key challenge in electrocatalytic water splitting is the anodic OER of this high overpotential and sluggish surface kinetics in virtually all known materials. Currently, typical catalysts used in water splitting reactions are mostly based on noble metals such as Pt, Ru, Ir, and their alloys/compounds, among which Ir oxide is one of the most appropriated polymer electrolyte membrane electrolyzer OER catalysts providing excellent activity and stability.224–228 However, Ir is an extremely rare element with an abundance 10 times lower than Pt, and therefore the amount of Ir required must be reduced to a minimum to make its application feasible on a large scale.

Recently, Strasser’s group derived dealloyed metal-oxide hybrid IrNi@IrOₓ core–shell NPs, which provide substantial advances towards more efficient and less expensive electrocatalytic water splitting.229 The IrNi@IrOₓ NPs were synthesized from IrNi precursor alloys through selective surface Ni dealloying and controlled surface oxidation of Ir. The final materials contained a nanometer scale, an almost pure IrOₓ surface, while the inner core region became increasingly metallic and enriched with Ni. The catalysts showed 3-fold activity enhancement in the electrochemical OER process over the IrO₂ and RuO₂ benchmark catalysts on a noble metal mass basis. In the next report published by this group, the catalysts were modified by introducing a support, where core–shell IrNiₓ@IrOₓ NPs supported on high-surface-area mesoporous antiimony-doped tin oxide (IrNiOₓ/Meso-ATO) were synthesized from bimetallic IrNiₓ precursor alloys (PA-IrNiₓ/Meso-ATO) using electrochemical Ni leaching and concomitant Ir oxidation.231 This work was designed based on the structural hypothesis regarding the active catalyst/support couple, with the OER proceeding at thin IrOₓ shells on Ir-low/Ir-free cores, thereby reducing the required Ir amount significantly (Fig. 19). The materials were annealed at different temperatures (T = 180, 250, 300, 400, 500 °C) and the effects of thermal treatment on the atomic structure of the PA-IrNiₓ/Meso-ATO-T and on the OER activity of the obtained core–shell catalysts were investigated (Fig. 19). The IrNiOₓ/Meso-ATO-T catalysts with T ≤ 300 °C were significantly more OER active on both the geometric surfaces and on an Ir mass basis compared to the IrOₓ/C and IrOₓ/com.-ATO benchmarks. In fact, the lower annealing temperature maintained the desired IrNi metallic alloy phase and the Ni content in the particle core remained high. It is assumed that, as a result of this, electronic and/or strain effects modified the chemisorption and reactivity of intermediates at the surface. In contrast, the catalysts annealed at 400 °C and 500 °C showed significantly lower OER activities due to the phase segregation into a mixture of NiO and Ir-rich nanophases.

The same group reported Ni–Ir mixed oxide thin film catalysts for the OER with an unprecedented 20-fold improvement in Ir mass-based activity over pure Ir oxide.229 The initial variation of the Ir to Ni ratio resulted in a volcano type OER activity curve with a maximum at high Ni contents (67–79 at%) (Fig. 20a). The intuitive model for the formation of the active state of the catalytic surface suggested that the coverage of the reactive surface hydroxyls serves as a useful descriptor for OER activity (Fig. 20c). During the electrocatalytic OER protocol, Ni is leached from these oxides, yielding Ir-rich oxides. Consequently, oxygen atoms lose binding partners and take up protons from the electrolyte to form surface hydroxyl groups. Upon Ni leaching the surface OH fraction increased significantly up to 67 at% initial Ni content (Fig. 20b). Interestingly, the surface-specific OER activity revealed a rather similar trend to the OH fraction,
increase in temperature leads to the formation of methane in a higher yield.

\[
\text{CO}_2 + 4\text{H}_2 \rightarrow \text{CH}_4 + 2\text{H}_2\text{O} \quad [\Delta H_{298K} = -165 \text{ kJ mol}^{-1}] \quad (4)
\]

\[
\text{CO} + 3\text{H}_2 \rightarrow \text{CH}_4 + \text{H}_2\text{O} \quad [\Delta H_{298K} = -206 \text{ kJ mol}^{-1}] \quad (5)
\]

\[
(2n + 1)\text{H}_2 + n\text{CO} \rightarrow C_n\text{H}_{2n+2} + n\text{H}_2\text{O} \quad (6)
\]

According to the thermodynamics, methanation of CO₂ and CO is the most advantageous reaction as it is considerably faster than other reactions which form hydrocarbons or alcohols.\(^{239}\) However, the process needs effective catalysts to occur. In fact, a huge number of studies have been performed on the design of effective methanation catalysts during the past few years.\(^{240-242}\) Since the earliest work by Sabatier and Senderens in 1902, nickel-based catalysts have been considered as the most active catalysts for the methanation process.\(^{241}\) In 1975, M. A. Vannice compared the specific activity and product distributions of group VIII metals dispersed on \(\text{Al}_2\text{O}_3\) in the production of hydrocarbons from \(\text{H}_2\text{CO}\) mixtures and found that CO methanation can occur readily over these metals.\(^{243,244}\) The specific activity followed the order of \(\text{Ru} > \text{Fe} > \text{Ni} > \text{Co} > \text{Rh} > \text{Pd} > \text{Pt} > \text{Ir}\), and the reaction rate of CO methanation was observed to be closely related to CO dissociation. Among all these catalysts, Ni supported on \(\text{Al}_2\text{O}_3\) is one of the most widely studied catalysts in methanation reactions due to its high performance-cost ratio. However, the performance of Ni catalysts toward methanation is dependent on various parameters such as the effect of support, Ni loading, the presence of a second metal and the preparation method. In this section, we will focus our discussion on the influence of the second metals on the activity of various Ni-based catalysts for the methanation of CO₂ and CO.

In the earlier section on the dry reforming process, we discussed that conventional Ni-based catalysts suffer from severe catalyst deactivation due to carbon deposition as a result of the CO₂ methanation reaction. The same strategy is also applied here to overcome this problem, where the addition of second metal such as Fe, Zr, Co, Cu, Mn, La, Y, and Mg has been attempted to enhance the stability and the catalytic activity of the nickel-based catalysts.\(^{245-255}\) Hwang \textit{et al.} reported the effect of a second metal (\(\text{M} = \text{Fe}, \text{Zr}, \text{Ni}, \text{Y}, \text{and} \text{Mg}\)) in mesoporous Ni (35 wt%)-M (5 wt%)-alumina xerogel (denoted as 35Ni5MAX) catalysts for methane production from CO₂ and \(\text{H}_2\).\(^{247}\) In the CO₂ methanation reaction, the yield of CH₄ decreased in the order 35Ni5FeAX > 35Ni5ZrAX > 35Ni5NiAX > 35Ni5YAX > 35Ni5MgAX. This indicated that the catalytic performance was greatly influenced by the identity of the second metal in the CO₂ methanation reaction. The CO dissociation energy and metal-support interaction of the catalyst played key roles in determining the catalytic performance of the 35Ni5MAX catalysts in the reaction, in which the 35Ni5FeAX catalyst retained the most optimal CO dissociation energy and the weakest metal-support interaction, and exhibited the best catalytic performance in terms of conversion of CO₂ and yield of CH₄.

Iron has been widely used as the second metal in Ni catalysts to improve CO₂ conversion and CH₄ yield.\(^{248-251}\) The performance of the catalysts is greatly influenced by the type of second metal, and the activity and stability of the catalysts significantly depend on the ratio of weakly bonded surface hydroxyls to the total oxide related oxygen (hydroxyl groups and both lattice oxygen species) as determined by XPS. (c) Model of Ni leaching from the surface of Ni–Ir mixed oxides.\(^{229}\) (Copyright 2015 American Chemical Society.)

[Fig. 20] (a) Electrocatalytic measurements of OER activity and stability of Ni–Ir mixed oxide films with different Ir to Ni ratios. (b) Hydroxyl group (OH) fraction to the total oxide related oxygen (hydroxyl groups and both lattice oxygen species) as determined by XPS. (c) Model of Ni leaching from the surface of Ni–Ir mixed oxides.\(^{229}\) (Copyright 2015 American Chemical Society.)
the catalysts was highly dependent on the metal loading, the nature of the support and the preparation methods. For example, supported Ni-Fe catalysts with a total metal loading containing 75 wt% Ni and 25 wt% Fe showed a significantly better CO2 conversion and higher CH4 yield compared to the Ni and Fe supported catalysts.256 Kang et al. studied the effect of Fe metal on NiAl2O3 for CO2 methanation and their results showed that the Ni0.7Fe0.3/Al2O3 catalyst achieved the maximum carbon conversion and CH4 selectivity.248 The increase in Fe content led to the enhancement of the water gas shift reaction and hydrocarbon production. Therefore, achieving the optimum ratio of the two metals is important in order to obtain a maximum CH4 yield. Pandey and Deo studied CO2 methanation over different oxide supports (such as Al2O3, ZrO2, TiO2, SiO2 and Nb2O5) containing a bimetallic Ni–Fe catalyst in the ratio of 3:1.251 It was observed that the relative enhancement in yield for the most active catalyst of each series was support dependent, and that the maximum enhancement was achieved over Al2O3 supported catalysts. The authors proposed that the maximum enhancement for the Al2O3 supported catalysts was due to the ability of the support to adsorb CO2. However, the effect of CO2 adsorption on the supported catalysts was not studied to support the statement.

Among the noble metals, Ru shows the highest activity for CO2 methanation and therefore it has been used to promote the catalytic efficiency of Ni catalysts.256,257 The effect of Ru content in the mesoporous Ni (35 wt%)-Fe (5 wt%)-Ru (x wt%)-alumina xerogel (denoted as 35Ni5Fe-xRuAX) catalysts was investigated.256 Both the conversion of CO2 and the yield of CH4 showed volcano-shaped trends with respect to Ru content, which indicates that optimal Ru content was required for the maximum production of CH4 (Fig. 21). The metal surface area and the amount of desorbed CO2 of the catalysts also showed the same trends with respect to Ru content, which explained the good correlation between the catalytic performance and their physicochemical properties. Zhen et al. reported CO2 methanation over γ-Al2O3-supported bimetallic Ni–Ru NPs, which were prepared by co-impregnation and sequential impregnation methods.257 The catalytic activities were found to be highly dependent on the preparation sequence. Catalysts prepared by the co-impregnation method showed higher catalytic activities, selectivities, and excellent stabilities for CO2 methanation. It was also found that the segregation phenomenon of Ru occurred on the catalyst surface in the co-impregnation method, by which more active Ni and Ru species (metallic Ru) could be provided on the surface of the catalyst. Based on these characterizations, a possible reaction mechanism was proposed, where the individual role of each metal site was explained (Fig. 22). In the first step, CO2 was dissociated and activated to form carbon species (COads) on the Ru species surface. At the same time, H2 was dissociated into H on the metallic Ni surface. In the second step, carbon species (COads) was dissociated into C and O on the catalyst surface. Finally, the C species could react with H to produce CH4 on metallic Ru, and H and O atoms formed H2O.

Product selectivity is one of the major concerns in the FT process. In the FT process, the product composition primarily includes paraffins, olefins, and different classes of oxygenates (alcohols in major fraction). Therefore, one of the primary interests in this research is to generate a higher olefin fraction, which can then be further oligomerized to generate the target transportation fuel or chemicals and reduce/avoid CH4 and CO2 formation from the syngas hydrogenation. In a recent work by Ramasamy et al., a dual bed configuration has been introduced to convert oxygenates generated in the CO hydrogenation process to produce targeted hydrocarbon compounds.258 In the first reactor of the multi-step process, the Ni-Co bimetallic catalyst containing a total metal loading less than 10 wt% was introduced, which produced 40% of short-chain olefinic compounds (C2-C7) along with 10% oxygenates. An acidic alumina containing reactor was added following the Ni-Co containing reactor for the deoxygenation of oxygenates, which could effectively reduce the oxygenate products from 10% to 1.3%.

4.1.3 Production of oxygenates as energy carriers. Alongside the hydrocarbon-based fuels, a number of oxygenated compounds have drawn considerable attention due to their excellent fuel properties. Although the oxygenated compounds have a lower energy density than commonly used gasoline and diesel, some compounds have a higher research octane number (e.g. ethanol, DMF) and cetane number (e.g. DME), which make them suitable blends as transportation fuels. There are

![Fig. 21](https://example.com/fig21.png) Conversion of CO2 and yield of CH4 in the methanation of CO2 plotted as a function of Ru content of 35Ni5Fe-xRuAX catalysts.256 (Copyright 2013 Elsevier.)
numerous resources containing oxygen functionalities, such as lignocellulosic biomass, which are readily convertible into different oxygenate molecules via catalytic transformation. Nevertheless, selective biomass conversion is not simple because of the high oxygen content and the presence of diverse functional groups. The major complexity in oxygenated biomass or biomass-derived platform molecules is related to the comparable strength in C-O and C-C bonds, resulting in a remarkable challenge to achieve the selective cleavage of one bond while keeping the other intact. CO2 is another excellent platform for deriving oxygenate molecules such as methanol and formic acid which serve as potential energy carriers. In this section, we will provide a brief account of bimetallic Ni systems for the conversion of biomass feedstock and CO2 into energy carrier molecules via different reaction pathways like hydrogenation, hydrolysis, and hydrodeoxygenation, etc.

### 4.1.3.1 Hydrogenation of cellulose and glucose

Cellulose and glucose can be directly converted into various polyols (e.g. ethylene glycol (EG), propylene glycol, sorbitol, and mannitol) through hydrogenation or hydrolysis over metal catalysts. Gallezot et al. studied the effect of adding promoters such as Sn, Mo, Cr and Fe to RANEY Ni and found that the addition of Cr increased the rate of glucose hydrogenation by up to 5 times. Cr(II) acted as a Lewis acid to adsorb glucose and favor the nucleophilic attack on the carbon atom by H2 dissociated on Ni. Shrotri et al. reported an aqueous phase hydrolysis/hydrogenation process to convert cellulose into sorbitol using a bimetallic Ni–Pt catalyst. Mono- and metallic Ni catalysts showed little activity for the reaction, but the addition of a small amount of Pt to Ni (Ni:Pt = 22:1 atom ratio) greatly enhanced the catalytic activity. The bimetallic Ni–Pt catalysts supported on mesoporous alumina gave a hexitol (sorbitol + mannitol) yield of 32.4% compared to 5% with the pure Ni catalyst. The presence of Pt promoted the protonation of water and hydrogen, which could spill over to Ni sites creating in situ acid sites to catalyze the hydrolysis of cellulose. In another report, hydrogenation of cellulose was performed over bimetallic Ni catalysts supported on mesoporous carbon (MC). By efficiently coupling the hydrolysis reaction and “in situ” hydrogenation of oligosaccharides, the hexitol yield reached 59.8%. The monometallic Ni catalyst (20%Ni/MC) produced a 42.1% hexitol yield at a cellulose conversion of 84.5%, while the addition of Rh and Ir showed increasing activity, producing 59.8% and 57.5% hexitols, respectively. The stability of the catalyst also increased upon addition of promoters. The monometallic Ni catalyst deactivated rapidly, and a 20% yield of hexitols was achieved after 5 cycles, while 4%Ir/4%Ni/MC retained its activity for 4 cycles with yields around 60%.

A highly active bimetallic Ni–Pt/ZSM-5 was reported for the hydrolytic hydrogenation of cellulose in hot-compressed water. Ni–Pt NPs were formed with a Pt-enriched alloy surface in the catalyst. A remarkable yield of hexitols (76.9%) was obtained on Ni–Pt/ZSM-5 which was higher than the 52.7% obtained on Ni/ZSM-5 at similar conversion levels, indicating that the presence of a Pt-enriched alloy surface significantly enhances the selectivity to hexitols. The Ni–Pt/ZSM-5 presented much higher hydrogenation activity compared to Ni/ZSM-5. The H2-TPD of Ni–Pt/ZSM-5 showed that more H species migrate from the Pt-like sites to the Ni-like ones, which means that more activated hydrogen species can participate in glucose hydrogenation.

The product distribution of the cellulose hydrogenation/hydrogenolysis process depends on the nature of the second metal used. For example, noble metals such as Pt and Ru show improved hydrogenation properties along with Ni to produce mainly hexitols as observed in previous cases. In contrast, tungsten species are very effective for cellulose degradation due to their high activity in breaking the C–C bond and as a result, lower polyols (such as ethylene glycol) are obtained through the hydrogenolysis process. However, the yield of polyols with pure tungsten catalysts is low because of the poor hydrogenation properties. Ni, in principle, can act here as a promoter to increase the hydrogenation ability to obtain ethylene glycol with a higher yield.

### 4.1.3.2 Hydrogenation of furfurals and levulinic acid

Biomass-derived platform molecules such as fural, 5-hydroxymethylfurfural (HMF) and levulinic acid (LA) are of immense importance because they can be upgraded into other useful chemicals and fuels by oxidation, hydrogenation, aldol condensation, etherification and many other reactions. Here we will focus on hydrogenation and hydrogenolysis, as these are the reactions where bimetallic Ni catalysts can be used.

2,5-Dimethylfuran (DMF) has received increasing attention as a promising liquid transportation fuel lately. DMF can be obtained via selective hydrogenation of HMF over metal-based catalysts. However, obtaining a high selectivity of DMF is challenging due to the highly reactive nature of HMF. HMF reductive chemistries include C=O bond reduction, hydrogenation of the furan ring as well as C–O hydrogenolysis. Therefore, the catalysts must be carefully designed to perform the desired reaction to achieve the desired product. Huang et al. reported a highly efficient non-noble bimetallic catalyst based on nickel–tungsten carbide for the hydrogenolysis of HMF to DMF with excellent yields. Using different catalysts, metal ratios and reaction conditions, a maximum DMF yield of 96% was obtained. To understand the role of Ni and W2C components in the hydrogenolysis reaction, Ni/AC and W2C were prepared and individually tested. The results suggested two different roles of metals: Ni particles mainly contributed to hydrogenation activity while W2C offers an additional deoxygenation activity. The W2C catalyst is well known for its bifunctional nature, which contains both acidic and metallic sites, and can therefore catalyze both deoxygenation and hydrogenation reactions. The addition of Ni was proved to be essential for increasing the active hydrogen concentration to improve the hydrogenation rates. Higher Ni loadings were also shown to result in a remarkable improvement in the hydrogenolysis reaction upon increasing the hydrogenation ability. Despite the in-depth studies on the individual roles of the two components, the interactions between Ni and W2C, and the structures and properties of the interface remain elusive.

Recently, a carbon nanotube-supported bimetallic Ni–Fe (Ni–Fe/CNT) catalyst was investigated for the selective hydrogenation and
hydrogenolysis of HMF with H₂ as the hydrogen donor. Two different metal components presented different behaviors when used individually. The Fe/CNT catalyst showed low catalytic activity at both low and high temperatures, which confirmed the poor hydrogenolysis properties of Fe. Meanwhile, the monometallic Ni/CNT catalyst showed high conversion but poor selectivity under the same conditions. Scheme 3 represents the pathway of HMF conversion over different catalysts, which shows that different byproducts including the decarbonylation product [5-methylfurfural (MF)], the ring hydrogenation product [2,5-dimethyltetrahydrofuran (DMTHF)], the ring-opening product [1,2-hexanediol (HD)], and the etherification product were detected over Ni/CNTs. The combination of Ni and Fe in an appropriate atomic ratio of Ni/Fe (2:0.0) significantly increased the selectivity to 2,5-furandimethanol or 2,5-dimethylfuran depending on the reaction temperature. The selectivities to 2,5-furandimethanol and 2,5-dimethylfuran were as high as 96.1% at 383 K and 91.3% at 473 K, respectively. The improved selectivity could be attributed to the formation of Ni–Fe species, which was beneficial for the selective cleavage of the C–O bond.

Sitthisa et al. investigated SiO₂-supported Ni and Ni–Fe bimetallic catalysts for the conversion of furfural. Furfuryl alcohol and furan were primary products over monometallic Ni/SiO₂, resulting from hydrogenation and decarbonylation of furfural. Comparatively, Fe–Ni bimetallic catalysts predominantly produced 2-methylfuran (2-MF) with reduced yields of furan and C₄ products. The results proved that the addition of Fe suppressed the decarbonylation activity of Ni and at the same time promoted C–O hydrogenation (at low temperatures) and C–O hydrogenolysis (at high temperatures). The strong interaction between O (from the carbonyl group) and the oxyphilic Fe atoms resulted in a preferential hydrogenolysis reaction on the bimetallic alloy. On the other hand, the pure Ni surface promoted the conversion of η¹(C,O) species into a surface acyl species, which was subsequently decomposed into furan and CO. In another report, furfural was converted into cyclopentanone (CPO) over Ni–Cu bimetallic catalysts in an aqueous medium under a H₂ atmosphere. Furfuryl alcohol, 4-hydroxy-2-cyclopentenone and 2-cyclopentenone were identified as three key intermediates during the transformation. The rearrangement of the furan ring was independent of catalytic hydrogenation, starting from furfuryl alcohol rather than furfural. The opening and closure of the furan ring were closely related to the attack of the H₂O molecule in the 5-position of furfuryl alcohol. The Ni/SBA-15 catalyst produced 39% CPO selectivity at a furfural conversion of 46%, while on the Ni–Cu-50/SBA-15 catalyst (Cu : Ni = 50% in atomic ratio), nearly complete conversion of furfural was achieved with 62% selectivity of CPO. Chen et al. recently reported liquid-phase hydrogenation of furfural using bimetallic Ni–Pd catalysts supported over TiO₂–ZrO₂ binary oxides. The addition of a small proportion of Pd directly transferred the catalytic performance of supported Ni from the partial hydrogenation catalyst to the total hydrogenation catalyst. The yield of the total hydrogenation product, tetrahydrofurfuryl alcohol (THFA), was 93.4% using the catalyst with a Ni–Pd molar ratio of 5 : 1.

Levulinic acid is another important building block that can be converted into various fuel units including ethyl levulinate (EL), γ-valerolactone (GVL), and 2-methyltetrahydrofuran (2-MeTHF). Hydrogenation of levulinic acid to GVL has attracted a significant amount of interest recently, as GVL can be used as a fuel blend, as a solvent, or be converted into other liquid fuels. Hydrogenation of LA was performed over a composition-tuned bimetallic Ni–Ru catalyst supported on ordered mesoporous carbons. Ru₀.₄Ni₀.₆–OMC catalysts demonstrated unprecedented catalytic activity (TOF > 2000 h⁻¹), producing a 97% yield of GVL. The high activity of the catalyst could be ascribed to the homogeneous distribution and strong metal–support interaction. The non-noble metal-based bimetallic Ni–Cu/Al₂O₃ catalyst exhibited synergistic effects allowing higher activity and improved selectivity compared to the monometallic catalysts in the hydrogenation of LA to 2-MeTHF. The activity of the Ni-based catalytic system was highly dependent on the solvent. Water resulted in high GVL yields but inhibited MTHF formation. In contrast, hydrogen donating solvents (such as 2-ProOH) facilitated the transformation of the highly stable GVL intermediate into MTHF.

### 4.1.3.3 Lignin upgrading

Lignin has shown significant potential as a source for the sustainable production of fuels and bulk chemicals. Hydrogenolysis of the C–O linkages in lignin is regarded as an effective way to transform lignin into depolymerized aromatic platform compounds. Different bimetallic systems including noble metals combined with a transition metal (e.g. Fe, Ni, Cu, Zn or Sn) have also been found to be highly selective for the removal of oxygen even under mild HDO conditions. Among the non-noble metal-based catalysts, Ni catalysts have shown promising activity for the selective C–O cleavage in lignin model compounds under mild reaction conditions. However, pure Ni-based catalysts are unsatisfactory for β-O–4-C bond hydrogenolysis in real lignin, due to both their limited activity (TOFs of 5–30 h⁻¹) and low dispersions.
In our recent work, we developed a series of core–shell bimetallic catalysts, NiM (M = Ru, Rh, Pd, and Au), to achieve a better performance in the hydrogenolysis of lignin model compounds and organosolv lignin. Due to the difference in the reduction kinetics, the bimetallic catalysts have a core–shell structure and Ni was enriched in the shell. XPS and XANES studies confirmed the charge transfer from noble metals to Ni, which made the Ni surface electron-enriched. In addition, the core–shell bimetallic catalysts were formed in ultrasmall size, typically much smaller than the pure Ni catalyst (∼2 nm for Ni₈₅Ru₁₅ and Ni₈₅Rh₁₅, and ∼4 nm for Ni₈₅Au₁₅), which afforded an enhanced fraction of surface atoms. The as-prepared bimetallic Ni catalyst showed an excellent synergistic effect in the hydrogenolysis of a lignin model compound, 2-phenoxyl-1-phenylethanol, plausibly due to an electron transfer from noble metals to Ni. While the pure Ni catalyst achieved a high selectivity to monomer products (desired hydrogenolysis products) with a low conversion, and pure Ru and Rh catalysts exhibited a high catalytic activity with low selectivity towards the desired monomer products, all the bimetallic core–shell catalysts demonstrated a high conversion as well as a high selectivity towards monomers. Our synthesized catalysts were also applied to the hydrogenolysis of organosolv lignin and it was found that the bimetallic catalysts exhibited three to ten times higher activity than pure Ni, Ru, Rh, and Pd NPs.

Sometimes it is observed that the high activity of noble metals results in undesired aromatic ring hydrogenation, which is a severe problem in lignin hydrogenolysis. One possible way to address the issue is to modify the catalyst through partially blocking of the active sites that can hinder the coordination of the aromatic rings on the catalyst surface. Recently, we developed a few effective strategies to modify the bimetallic catalyst surface, thereby making it selective for C–O bond hydrogenolysis over benzene ring hydrogenation. In the approach, the surface of highly active Rh nanoparticles was blocked by inactive NiO₃, which segregates the surface terrace zones into smaller segments, thereby preventing the easy access to the Rh surface for benzene rings (Fig. 23). The introduction of NiO₃ did not exhibit a pronounced electronic interaction with Rh but significantly modified its geometric properties, inhibiting benzene ring hydrogenation without compromising the hydrogenolysis activity in the aryl ethers. The second approach was to use an inert metal such as Ag to decorate the active Ni catalyst surface, thus inhibiting the coordination and hydrogenation of the aromatic rings. These are examples of bimetallic systems where one component shows a detrimental effect on the reactivity of the other components to achieve improved selectivity (Table 3).

### 4.1.3.4 Conversion of CO₂ into oxygenates

Small molecule oxygenates such as methanol, dimethyl ether, and formic acid are considered to be potential energy carriers, which can be produced from CO₂ through catalytic hydrogenation. Several catalytic systems have been studied for CO₂ hydrogenation to methanol; among them Cu-based catalysts have long been recognized as the active catalyst component. There are many reports where different promoters have been introduced to improve the efficiency of Cu catalysts. Early studies have shown that Ni has a very good promotional effect on Cu catalysts for methanol synthesis, where the deposition of Ni leads to a dramatic increase in the rate of methanol formation from CO, CO₂, and H₂. It was also observed that the CuNi/SiO₂ catalyst had the same level of turnover frequency and a slightly higher selectivity to methanol than the best known industrially used Cu/ZnO/Al₂O₃ catalyst. Recently, bimetallic CuₓNiᵧ/γ-Al₂O₃ alloy catalysts were studied for methanol synthesis from CO/CO₂ hydrogenation. The activity was shown to be highly composition dependent where the CuₓNiᵧ/γ-Al₂O₃ catalyst exhibited the highest methanol formation rate of 5.86 mmol g⁻¹ h⁻¹, much higher than the commercial Cu/ZnO/Al₂O₃ catalyst under the same reaction conditions. The highest activity of the CuₓNiᵧ/γ-Al₂O₃ catalyst could be attributed to the larger specific surface area, the smallest alloy particle size and the lower reduction temperature.

A catalyst based on a Ni–Pd alloy on a carbon nanotube–graphene support was used for the production of pure formic acid via CO₂ hydrogenation. The thermodynamics of the pure FA formation from CO₂ hydrogenation is not favorable (ΔG⁻²⁹⁸ K = +3.33 kJ mol⁻¹) even at a high temperature and pressure, and therefore organic/inorganic bases are often added to the reaction mixture to increase the conversions. The authors claimed this to be the first ever report where the heterogeneously catalyzed reaction was carried out under milder conditions (40 °C and 50 bar) in water without any base additive. Nevertheless, the highest formic acid yield obtained was very low (1.92 mmol) with a turnover number of 6.4 and a turnover frequency of 1.2 × 10⁻⁴ s⁻¹. Based on previous results, a reaction mechanism for the formation of formic acid over a Ni–Pd alloy was proposed (Scheme 4). Noble metals (such as Pt, Ru, Rh, and Pd) are active for splitting H₂ into H atoms, while the transition metal (such as Ni) has a high reactivity in CO₂ reduction. DFT calculations also proved that CO₂ is adsorbed as a formate intermediate on the Ni surface and consecutively reacts with subsurface H in Ni, producing formic acid as the final product. The proposed mechanism was derived based on the XPS results, which confirmed the electron transfer from Ni to Pd. The role of the Ni/Pd atomic ratio of the Ni–Pd bimetallic system could also be explained from the mechanism. The experimentally optimized composition of Pd (Ni/Pd = 2.33 for Pd₃Ni₇) was close to the ratio (Ni/Pd = 2) in...
4.1.4 Production of electricity through fuel cells. A fuel cell is an excellent example of a high capacity system that can utilize environmentally sustainable energy sources. Many varieties of fuel cells are currently available, but their working principle is the same. Among the different fuel cells, proton exchange membrane fuel cells (PEMFCs) have attracted considerable attention due to their high efficiency, low operation temperature, and environmentally benign products.\textsuperscript{224,305} Oxygen reduction reaction (ORR) is an important fundamental electrode reaction in PEMFCs for energy storage and conversion devices based on oxygen electrocatalysis, where oxygen is electrochemically reduced to water at the cathode in acidic or alkaline media. On the other hand, the fuel components (such as H\textsubscript{2} and methanol) are introduced at the anode to produce protons. In spite of the high importance of ORR, the sluggish reaction kinetics at the cathode side remains a bottleneck that requires further attention.\textsuperscript{306} To enhance the ORR kinetics, several attempts were made to develop effective fuel cell catalysts over the last two decades.\textsuperscript{307,308}

Because of the high price of Pt-based catalysts, less expensive and more widely available Pd has recently been exploited as a substitute for Pt in ORR.\textsuperscript{41,309,310} Chen et al. reported a nanoporous Ni–Pd (np-Ni–Pd) bimetallic catalyst using the dealloying method where a Pd–Ni alloy was electrochemically dealloyed in an acid solution.\textsuperscript{41} With \textasciitilde{} 9 at\% Ni, the np-Ni–Pd bimetallic catalyst exhibited superior electrocatalytic performances in oxygen reduction in comparison with commercial Pd/C and nanoporous Pd (np-Pd). The excellent electrocatalytic properties of the dealloyed np-Ni–Pd appeared to arise from the combined effect of unique bicontinuous nanoporosity and bimetallic synergistic action. Wang et al. synthesized Ni–Pd hollow NPs \textit{via} a modified galvanic replacement method using Ni NPs as sacrificial templates (Fig. 24).\textsuperscript{309} Compared with the commercially available Pt/C or Pd/C catalysts, the synthesized Ni–Pd/C exhibited a superior electrocatalytic performance towards the ORR process, which could be due to the unique hollow porous structure and changes in the electronic structures when a second metal (Ni) was introduced. Recently, a noble metal free catalyst based on bimetallic Ni–Fe layer double hydroxide (NiFe-LDH) has been reported for fuel cell applications.\textsuperscript{311} The two-phase bifunctional oxygen reduction and evolution (ORR and OER) electrocatalyst (physical mixture of NiFe-LDH and Fe–N–C).

<table>
<thead>
<tr>
<th>Catalyst</th>
<th>M/Ni (wt/wt)</th>
<th>Reactant</th>
<th>Reaction conditions</th>
<th>Key product(s)</th>
<th>Conv. (%) yield (%)</th>
<th>Note</th>
<th>Ref.</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ni5–W25/SBA-15</td>
<td>5</td>
<td>Cellulose</td>
<td>245 °C, 60 bar H\textsubscript{2}, 30 min</td>
<td>Ethylene glycol</td>
<td>100/75.4</td>
<td>W performed C–C cracking and Ni performed hydrogenation</td>
<td>272</td>
</tr>
<tr>
<td>1%Rh–5%Ni/MC</td>
<td>0.33</td>
<td>Cellulose</td>
<td>245 °C, 60 bar H\textsubscript{2}, 30 min</td>
<td>Hexitols (sorbitol + mannitol)</td>
<td>100/59.8</td>
<td>Noble metal enhanced hydrogenation and decreased dehydration of sugars to increase hexitol yield</td>
<td>270</td>
</tr>
<tr>
<td>Ni–Pt/Beta\textsubscript{75}</td>
<td>0.17</td>
<td>Cellulose</td>
<td>200 °C, 50 bar H\textsubscript{2}, 6 h</td>
<td>Hexitols (sorbitol + mannitol)</td>
<td>51.3/36.6</td>
<td>Pt created \textit{in situ} acid sites by protonation and H\textsubscript{2} spillover to catalyze the hydrolysis of cellulose</td>
<td>269</td>
</tr>
<tr>
<td>Ni–W/AC</td>
<td>4</td>
<td>Cellulose</td>
<td>215 °C, 65 bar H\textsubscript{2}, 3 h</td>
<td>Ethylene glycol</td>
<td>88.4/43.7</td>
<td>W performed C–C cracking and Ni performed hydrogenation</td>
<td>273</td>
</tr>
<tr>
<td>Ni–Pt/ZSM-5</td>
<td>0.06</td>
<td>Cellulose</td>
<td>240 °C, 40 bar H\textsubscript{2}, 4 h</td>
<td>Hexitols</td>
<td>100/76.9</td>
<td>Pt showed remarkable hydrogen spillover and inhibited the oxidation of Ni</td>
<td>271</td>
</tr>
<tr>
<td>Ni–Pd/SiO\textsubscript{2}</td>
<td>0.26</td>
<td>HMF</td>
<td>40 °C, 80 bar H\textsubscript{2}, 2 h</td>
<td>BHTF</td>
<td>99/96</td>
<td>Catalyst was more active than commercial RANEY\textsuperscript{®} Ni and more selective than Pd/C</td>
<td>293</td>
</tr>
<tr>
<td>7Ni–30W\textsubscript{2}C/AC</td>
<td>4</td>
<td>HMF</td>
<td>180 °C, 40 bar H\textsubscript{2}, 3 h</td>
<td>DMF</td>
<td>100/96</td>
<td>Ni showed good hydrogenation ability and W\textsubscript{2}C showed good HDO activity</td>
<td>276</td>
</tr>
<tr>
<td>Ni\textsubscript{2}–Fe\textsubscript{4}/CNTs</td>
<td>0.48</td>
<td>HMF</td>
<td>200 °C, 30 bar H\textsubscript{2}, 3 h</td>
<td>DMF</td>
<td>100/91.3</td>
<td>Ni–Fe alloy selectively cleaved the C–O bond</td>
<td>277</td>
</tr>
<tr>
<td>NiCu–50/SBA-15</td>
<td>0.54</td>
<td>Furfural</td>
<td>160 °C, 40 bar H\textsubscript{2}, 4 h</td>
<td>CPO</td>
<td>99/62</td>
<td>High selectivity of CPO was ascribed to the presence of 2-cyclopentenone</td>
<td>279</td>
</tr>
<tr>
<td>CuNi\textsubscript{2}C</td>
<td>2.17</td>
<td>Furfural</td>
<td>130 °C, 50 bar H\textsubscript{2}, 5 h</td>
<td>CPO</td>
<td>99.3/96.9</td>
<td>Porous carbon matrix acted as a supporter and prevented the accumulation of metal particles</td>
<td>294</td>
</tr>
<tr>
<td>Ni–Pd/TiO\textsubscript{2}–ZrO\textsubscript{2}</td>
<td>0.36</td>
<td>Furfural</td>
<td>130 °C, 50 bar H\textsubscript{2}, 6 h</td>
<td>THFA</td>
<td>99/93.4</td>
<td>Addition of Pd transferred the reaction selectivity from partial hydrogenation to total hydrogenation</td>
<td>280</td>
</tr>
<tr>
<td>Ru\textsubscript{0.1}Ni\textsubscript{8.9}–OMC</td>
<td>11.71</td>
<td>LA</td>
<td>150 °C, 45 bar H\textsubscript{2}, 2 h</td>
<td>GVL</td>
<td>99/97</td>
<td>High TOF (\textgreater{} 2000 h\textsuperscript{–1}), catalyst was recyclable up to 15 times</td>
<td>283</td>
</tr>
<tr>
<td>23Ni–12Cu/Al\textsubscript{2}O\textsubscript{3}</td>
<td>0.52</td>
<td>LA</td>
<td>250 °C, 70 bar H\textsubscript{2}, 3 h</td>
<td>2-MeTHF</td>
<td>100/56</td>
<td>Bimetallic catalyst showed improved activity and selectivity for 2-MeTHF</td>
<td>284</td>
</tr>
</tbody>
</table>

BHTF: 2,5-bis(hydroxymethyl)tetrahydrofuran. CPO: cyclopentanone. THFA: tetrahydrofuranylyl alcohol.

Scheme 4 Proposed reaction mechanism of the selective formation of HCOOH from CO\textsubscript{2} hydrogenation over the Ni–Pd bimetallic surface.\textsuperscript{309}

(Copyright 2015 Royal Society of Chemistry.)
Ni. As shown in Fig. 25b, compared with other cases, Ni2Co2 has CO adsorbed on Ni, indicating that CO prefers to bind to Co than the adsorption energies of CH3OH adsorbed on the Ni atom are higher than those of CH3OH adsorbed on the Co atom (Fig. 25a), suggesting that CH3OH prefers to bind to Ni than Co for Ni3Co and Ni2Co. This confirms a fast kinetic rate reaction of CH3OH molecules on the surface of Ni3Co and Ni2Co. The adsorption energies of CO adsorbed on Co are slightly higher than those of CO adsorbed on Ni, indicating that CO prefers to bind to Co than Ni. As shown in Fig. 25b, compared with other cases, Ni2Co2 has a relatively low adsorption energy, resulting in less CO poisoning of catalysts.

4.2 Environmental applications

Rapid developments in industrialization, population expansion, and urbanization have largely contributed to severe air pollution. Carbon monoxide, short hydrocarbons (C2H2, especially methane), different halogenated species, and nitrogen oxides (NOx) are the main pollutants produced by industrial processes and vehicles running on petroleum fuels. Improving air quality has been a hot research topic for the past few decades and many different paths have been taken to try and formulate a solution. Catalytic oxidation is one of the most powerful ways for the remediation of air pollution, which can effectively convert the toxic compounds into less harmful and more ecofriendly compounds. For example, a three way catalyst (TWC) is highly effective for this purpose as it simultaneously removes CO, C2H2, and NOx by both oxidation and reduction pathways.

Oxidation: 2CO + O2 → 2CO2
Reduction: 2NOx → xO2 + N2

4.2.1 Oxidation of CO. Catalytic oxidation of CO and hydrocarbons into CO2 is a major solution to remove them by air depollution treatments. Platinum group metals are very active in CO oxidation. In particular, Pd appeared to be a common choice of catalyst due to its high activity in the low-temperature oxidation reactions and lower price compared with other noble metals. However, the deactivation of Pd catalysts during the long-term usage increased their demand in improvements of the existing catalysts. One possible solution for increasing the catalyst lifetime is the modification of existing catalysts by the addition of a second metal. Commonly, the second metal is chosen from groups 9–11 in the periodic table. Among those metals, Ni has been proven to affect catalytic activity for exhaust gas treatment.325–327 Additionally, Ni can also act as a sulfur scavenger due to its high activity in H2S removal.326

Bimetallic Ni–Pd catalysts have been explored in CO oxidation and have a higher activity than monometallic Pd catalysts.327–329 Ni–Pd nanoalloy catalysts exhibit remarkable tunability in terms of phase state, bimetallic composition, and atomic-scale structure, which are responsible for the origin of the structural synergy for the CO oxidation reaction. Al2O3-supported bimetallic Ni–Pd catalysts were recently tested in CO oxidation to examine the effect of nickel addition on the activity and stability of Pd based catalysts.328 The improved activity could be rationalized by an interaction between Pd and Ni, which improved the reducibility of both Ni and Pd metals.

Apart from Pd, some excellent bimetallic catalysts based on Pt and Au were also reported for CO oxidation.330–332 Mu et al. reported supported sandwich type bimetallic Ni–Pt catalysts, which demonstrated high activity in CO oxidation with 100% CO conversion near room temperature.330 The Ni–Pt(111) surface exhibited the lowest combined OER/ORR overpotential ever recorded in 0.1 M KOH.

Direct methanol fuel cells are a class of PEMFCs where methanol is used as the fuel component to supply the protons. The main reactions occurring within the methanol fuel cell are the cathodic oxygen reduction reaction (ORR) and the anodic methanol oxidation reaction (MOR). Bimetallic 3d transition metal catalysts such as Ni–Mn,312 Ni–Co,313–315 and Ni–Cu316,317 were explored for MOR with good electrochemical activities. Very recently, Cui et al. investigated the role of cobalt in bimetallic Ni9Co6 electrocatalysts for MOR.315 In their study, the composition, the surface morphology, and the crystal phase structure of the bimetallic Ni9Co6 electrocatalysts significantly changed with an increased content of cobalt. The mechanism study based on electrochemical experiments and DFT calculations indicated that doping of Co into Ni9Co6 can significantly improve the surface coverage of the redox species, weaken the CO adsorption, as well as adjust the CH3OH adsorption. Furthermore, the adsorption energies of CH3OH adsorbed on the Ni atom are higher than those of CH3OH adsorbed on the Co atom (Fig. 25a), suggesting that CH3OH prefers to bind to Ni than Co for Ni3Co and Ni2Co. This confirms a fast kinetic rate reaction of CH3OH molecules on the surface of Ni3Co and Ni2Co. The adsorption energies of CO adsorbed on Co are slightly higher than those of CO adsorbed on Ni, indicating that CO prefers to bind to Co than Ni. As shown in Fig. 25b, compared with other cases, Ni2Co2 has a relatively low adsorption energy, resulting in less CO poisoning of catalysts.
consisted of both surface 2D NiO$_{x}$-Ni nanoislands and subsurface Ni atoms. The surface Ni oxide monolayer nanoislands contained coordinatively unsaturated cations at the island edges, which provided active sites for O$_2$ dissociative adsorption. On the other hand, the subsurface Ni atoms enhanced the elementary reaction of CO oxidation, with atomic O species produced at the edges of the surface oxide islands. In another report on the bimetallic Ni–Au catalyst, Au was the predominant species on the surface, while no surface Ni$^0$ or NiO was observed. Based on the reduction potential values of Ni$^{2+}$/Ni and AuCl$_4^-$/Au ($-0.25$ V vs. 1.00 V), Au is expected to be reduced first to form a core–shell structure with Au as the core. However, the synthesis protocol in this study employed a dendrimer stabilization approach combined with decanethiol extraction, which induced the system toward the formation of Ni@Au core–shell NPs. Au is thermodynamically more stable on the particle surface due to its lower work function than Ni. In this case, the difference was further enhanced by introducing a thiol containing extracting agent via the formation of strong Au–S bonds, which provided an additional driving force to bring Au to the NP surface. DFT calculations indicated that the incorporation of Ni into the Au slabs resulted in the stronger adsorption of O and CO on the Au surfaces. Kinetics studies also revealed that the apparent activation energies decreased by more than 50% and that O$_2$ reaction orders increased from 0.2 to 0.9 after Ni incorporation. Despite the promotional effect, the addition of Ni reduced the relative number of active sites on the catalyst.

Bimetallic core–shell Au–Ni NPs supported on a CeO$_2$ support were studied for CO oxidation and compared with their monometallic counterparts. As expected, the Au/CeO$_2$ catalysts exhibited a better catalytic performance than the Ni/CeO$_2$ sample. However, Au–Ni/CeO$_2$ was surprisingly more active than the Au/CeO$_2$ catalyst, even if the characterization data proved that only nickel atoms are exposed on the surface during the reaction. It was believed that the Au atoms in the core of the Au@Ni NPs induced an electronic effect on the local density of the Ni d states via the presence of core Au atoms (Fig. 26), similar to that proposed for the Au–Ni surface alloys earlier.

Iron–nickel hydroxide–platinum nanoparticles were reported by Chen et al. for CO oxidation at room temperature with high efficiency. It was shown that Ni$^{2+}$ played a key role in stabilizing the interface against dehydration. In general, the stability of the Pt/Fe(OH)$_x$ catalyst was highly dependent on the humidity of air. A decline in CO oxidation activity from 100% to 27% in 70 min occurred when the reaction was switched from humid air to dry air. The proposed reason behind the decrease in activity was the instability of the interfacial Fe$^{3+}$–OH–Pt sites with respect to dehydration, considering the fact that CO oxidation is an exothermic process. Since Ni$^{2+}$ can form a stable layered structure of Ni(OH)$_2$ with nearly perfect octahedral coordination, it was incorporated into the Fe(OH)$_x$ sub-monolayer to prevent the dehydration-induced loss of Fe$^{3+}$–OH–Pt sites. The TiO$_2$-supported Pt/FeNi(OH)$_x$ catalyst was stable in the reaction stream for more than 28 h without any decrease in activity at room temperature and achieved 100% CO conversion (Fig. 27). The OH:O ratio in the Pt/FeNi(OH)$_x$ catalyst was maintained at 5.3 even after a 2 hour heat treatment at 453 K under the reaction atmosphere. DFT and isotope-labeling experiments revealed that the OH groups at the Fe$^{3+}$–OH–Pt interfaces readily reacted with CO adsorbed nearby to directly convert the CO into CO$_2$ and simultaneously produce coordinatively unsaturated Fe sites for O$_2$ activation.

**4.2.2 Oxidation of hydrocarbons.** Few examples on bimetallic Ni–Pd catalysts have been reported for the removal of hydrocarbon through oxidation. Three-way catalysts based on Ni–Pd supported on Al$_2$O$_3$ were reported for the oxidation of C$_3$H$_6$ under stoichiometric conditions. A recent study by Shen et al. investigated the role of different preparation methods of Ni–Pd catalysts in inducing different structures of the catalysts with different activities for methane combustion. The traditional impregnation–calcination method produced monometallic Pd particles on a binary NixAl$_{1-x}$O$_y$ support, and in this case, no improvement of activity was observed as the Ni was consumed to form an inactive NixAl$_{1-x}$ spinel. In contrast, the colloidal approach produced Pd and Ni NPs on the parent Al$_2$O$_3$ support and exhibited better activity (Fig. 28). Furthermore, the addition of Ni to Pd during colloidal synthesis prevented the over-growth
of Pd NPs, thereby improving the stability against sintering at a high-temperature in oxidation processes.

### 4.2.3 Hydrodechlorination.

Halogenated compounds emitted into the atmosphere are responsible for the thinning and shrinking of the ozone layer in the stratosphere. They are also treated as severe hazards for ground water pollution even at a very low concentration. Recent research has therefore focused on the development of in situ methods for destroying chlorinated and brominated organic molecules such as CCl₄ (carbon tetrachloride), PCE (tetrachloroethylene), and TCE (trichloroethylene) in ground- and surface-waters. Catalytic hydrodechlorination (HDC) is regarded as an innovative method for transforming toxic hazardous chlorinated organic compounds into recyclable products or even into chemical intermediates of commercial value.³³⁶ Although the catalysts containing noble metals, such as Pd or Pt, are very efficient materials for HDC reactions,³³⁷,³³⁸ they are not ideal due to their high cost and very high ability to activate hydrogen, leading to the formation of fully hydrogenated undesired products during hydrodechlorination. On the other hand, monometallic catalysts of pure 3d transition metals (such as Fe, Ni, and Cu) are not highly effective in the removal of chlorine and deactivate faster due to coke formation, metal sintering and oxidation.

Nickel is a good candidate to promote hydrodechlorination. Indeed, the catalytic properties of Ni have been investigated in the transformation of chlorinated aromatic compounds such as chlorobenzene.³³⁹,³⁴⁰ In the case of vicinal chloroaikanes (such as 1,2-dichloropropane), employing Ni catalysts involved more severe reaction conditions, i.e. high temperature and high hydrogen pressure, than those used for Pd and Pt catalysts.³³⁷ In this regard, Ni catalysts modified by noble metals such as Pd, Ru, Ag and Au are advantageous,³⁴¹–³⁴⁶ where the noble metal shows high activity and Ni shows high selectivity. Simagina et al. reported liquid phase HDC of hexachlorobenzene over carbon supported Ni–Pd bimetallic catalysts, where the catalyst was less active than the pure Pd catalysts for the complete conversion of hexachlorobenzene into benzene, but presented a reasonable activity to obtain the compounds of interest, mono- and di-chlorobenzene.³⁴⁴ The degree of dechlorination was proportional to the surface Pd concentration. Interestingly, isolated Pd atoms located at the surface of Ni rich bimetallic particles were more active than those lying on larger ensembles.

Recently, bimetallic Ni–Cu catalysts were also tested for the HDC process to fully replace the use of noble metals.³⁴⁷–³⁵¹ While hydrodechlorination of 1,2-dichloroethane over pure Ni mainly produces ethane, increasing the Cu content in the bimetallic catalysts results in an increase in ethylene selectivity. The specific consumption rate of 1,2-dichloroethane decreases when Cu loading increases, however, the turnover frequency seems to be independent of the surface composition of the alloy particles.

#### 4.2.4 Others.

NOₓ and SOₓ are among the other major components causing air pollution. Although there are a few reports on catalytic materials for the removal of NOₓ and SOₓ,³⁵²–³⁵⁴ bimetallic Ni catalysts were rarely used for this purpose. Three way catalysts with Ni–Pd supported on different oxides such as Al₂O₃, CeO₂ and ZrO₂ were reported for the elimination of NO under stoichiometric conditions.³²⁴,³²⁵ The activity of the catalysts was shown to depend strongly on the support used. Whereas practically no differences were detected for the Al₂O₃-sustained bimetallic catalyst in comparison with the analogous monometallic Pd system, apparent differences appeared for (Ce,Zr)O₂-containing catalysts. In situ XANES experiments revealed that there was no apparent modification of the Pd electronic properties after Ni incorporation, which seems to be contradictory to the predictions of the d-band theory. This is due to the unique structural features of the catalyst. Using nanoprobe energy-dispersive X-ray (EDX) spectroscopy analysis, Pd was shown to maintain a particular trend in interacting with the Ce–Zr mixed oxide component on the support, while Ni appeared to interact preferentially with the alumina component on the support. As such, these two entities did not exhibit strong interactions with each other. Therefore, the higher NO reduction activities observed for the (Ce,Zr)O₂-supported system could be due to the fact that active contacts between highly dispersed Pd and (Ce,Zr)O₂ were modified either through direct blocking by NiO-type entities or through a certain decrease in the Pd dispersion.

#### 5. Conclusions and perspectives

The present contribution provides an overview on the design principles of different bimetallic nickel catalysts and their use in different types of catalysis processes related to energy production and environmental applications. In most cases, the role of the bimetallic surface and the role of each metal counterpart in the reaction have been critically discussed. Some reactions were favored and proceed on specific surfaces of the
bimetallic catalysts. Consequently, continued efforts on the rational design of surface specific bimetallic catalysts, and the understanding of structure–activity relationships are critical to achieve superior catalytic performances.

In addition to an appropriate catalyst design based on fundamental understanding, another major issue relates to the stability of bimetallic catalysts under the reaction conditions. It is often seen that at high reaction temperatures (such as under reforming conditions), the high diffusion rate of Ni over noble metals causes the destruction of the original structure of the bimetallic catalysts and the loss of its initial activity. Diffusion of Ni can be prevented by introducing a diffusion barrier layer into the surface Ni metal atoms. For instance, replacing bulk Pt with WC in Ni–Pt catalysts can retain the unique catalytic properties of the bimetallic surfaces, i.e. the subsurface Pt–Ni-WC structure for hydrogenation and the surface Ni-WC configuration for reforming reactions. We expect more of such systems to be developed in the future.

Coke and sulfur deposition are serious problems in hydrocarbon reforming processes. Although noble metals can significantly improve the coke or sulfur resistant properties of Ni-based catalysts, their high cost limits their application in industrial processes. Some efforts have been made with 3d transition metals, but their stability under high temperature conditions was not sufficient. One possible way to reduce catalyst costs without compromising their activity/stability could be the introduction of non-metal elements such as boron and phosphorus, since nickel-borides and phosphides have shown high activity and poison resistant properties towards different hydrotreating reactions. Alternatively, “noble-metal-like” compounds can be combined with Ni. For example, tungsten carbide (WC) could be a replacement for Pt since it exhibits “Pt-like” behavior and possesses high chemical stability, resistance to poisoning, and high electronic conductivity. We believe that the introduction of these non-metal additives can further improve the catalytic properties of simple bimetallic Ni–M systems, which is certainly an interesting area with room for further developments.

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Notes and references

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