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Hierarchically porous organic polymers: highly enhanced gas uptake and transport through templated synthesis†

Sanjiban Chakraborty,^a Yamil J. Colón,^b Randall Q. Snurr^b and SonBinh T. Nguyen^{*a}

Porous organic polymers (POPs) possessing meso- and micropores can be obtained by carrying out the polymerization inside a mesoporous silica aerogel template and then removing the template after polymerization. The total pore volume (tpv) and specific surface area (ssa) can be greatly enhanced by modifying the template (up to 210% increase for tpv and 73% for ssa) as well as by supercritical processing of the POPs (up to an additional 142% increase for tpv and an additional 32% for ssa) to include larger mesopores. The broad range of pores allows for faster transport of molecules through the hierarchically porous POPs, resulting in increased diffusion rates and faster gas uptake compared to POPs with only micropores.

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Introduction

The past decade has witnessed a surge in the development of porous organic polymers (POPs) due to their wide range of promising applications in catalysis,^{1–7} gas storage,^{8–14} and chemical separations.^{4,15–17} The well-defined micropores of the POPs make them good candidates for such applications. However, the presence of micropores, without additional larger mesopores, can often limit molecular diffusion, as observed in microporous zeolites.¹⁸ Unfortunately, this shortcoming in the transport properties of POP materials has been inadvertently ignored by the majority of POP synthetic strategies reported thus far, especially when the research focus has been on the measurement of static properties. Recently, we have reported that preserving the interparticle mesopores in a microporous porphyrin POP through supercritical CO₂ processing can indeed lead to an increase in the rate of phosphate ester methanolysis by almost an order of magnitude.¹⁹ Given this, we were intrigued by the possibility of engineering mesopores into POPs as part of the synthesis, where POPs are made on a mesoporous template that could eventually be dissolved. Further processing with supercritical CO₂ may then enable us to access even larger interparticle mesopores. The resulting POP materials would

then have a hierarchical pore system where micropores provide the specific molecular-level interactions needed for storage, separation, or catalysis while the larger meso/macropores allow for enhanced diffusion and mass transfer throughout the entire POP volume.

To incorporate larger pores into POPs, we adopted a synthetic strategy that is a cross between those used in the syntheses of mesoporous silica²⁰ and mesopore-containing zeolites.²¹ We selected a mesoporous silica aerogel as a template that can be infiltrated with a solution of the desired monomers

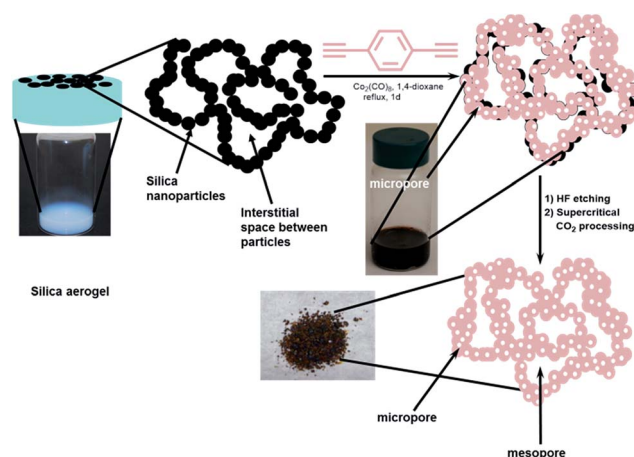


Fig. 1 An illustration of the synthesis of a POP possessing a hierarchy of pores. From left to right: a silica aerogel template is infiltrated with a solution of the monomer and catalyst. After polymerization, HF etching and supercritical CO₂ processing of the resulting monolith afford the desired POP as a powder. In this scheme, the interstitial spaces between the silica nanoparticles that made up the monolithic aerogel template are responsible for the formation of mesopores.

^aDepartment of Chemistry and the International Institute for Nanotechnology, Northwestern University, 2145 Sheridan Road, Evanston, Illinois, 60208-3113, USA. E-mail: stn@northwestern.edu

^bDepartment of Chemical & Biological Engineering, Northwestern University, 2145 Sheridan Road, Evanston, IL, 60208, USA

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for POP synthesis (Fig. 1). Crosslinking of the building blocks inside the pores of the template, followed by HF-dissolution of the silica, then creates a hierarchically porous structure with a mixture of micropores (from the POP synthesis) and larger mesopores (presumably from the interstitial spaces between the silica particles that made up the aerogel template). As described below, we have successfully synthesized a series of POPs possessing both micro- and mesopores using this aerogel-templating strategy. By modifying the chemical functionalities of the aerogel template and employing supercritical CO₂ processing, the surface areas and the pore size distributions of these POPs can be readily tuned across a broad hierarchy of pore sizes.

Results and discussion

To demonstrate that hierarchically porous POPs can be made using the aerogel-templating strategy, we selected the cobalt-catalyzed trimerization of 1,4-diethynylbenzene (**1**) as the POP-forming reaction. This reaction starts with an abundantly available monomer, can be carried out easily in a broad range of solvents, and has a short reaction time. In addition, the aromatic network that is formed is robust enough to tolerate the final HF-etching step. As Co-catalyzed alkyne trimerization reactions had been carried out in a mixture of water and methanol,²² we were confident that the Co^{II} metal-lacyclopentadiene intermediate in this reaction could tolerate the Si-OH groups of the silica aerogel template. We note that the cobalt-catalyzed trimerization of 1,4-diethynylbenzene has been used previously to produce a POP with a surface area of 1030 m² g⁻¹.²³

We synthesized the silica aerogel template from commercially available Silbond-H, a pre-polymerized tetraethyl orthosilicate (TEOS) precursor (see ESI,[†] Section S2). The aerogel product is a monolithic column that completely filled the bottom portion of the vial without any macroscopic cracks between it and the wall of the vial (Fig. 1, left image). This then allowed the added monomer-catalyst [1 + Co₂(CO)₈] solution to completely fill the volume occupied by the gel monolith and confined the subsequent polymerization to the pores of the aerogel. After polymerization, the silica network in the resulting solid could be dissolved away to leave behind the desired aerogel-templated **POP1**_a as a dark powder (Fig. 1, bottom right image; see also ESI,[†] Section S4). As a comparison, we also made **POP1** in the absence of the aerogel template following the protocol established by Yu, Liu, and coworkers.²³ The SEM images of **POP1** and **POP1**_a (ESI,[†] Fig. S8) suggest that these materials are indeed quite different: while the latter comprises aggregates of clearly defined small nanoparticles, the nanoparticles have “coalesced” into larger pieces in the former, with not much interstitial space between the pieces.

The N₂ gas adsorption-desorption data for **POP1** and the aerogel-templated **POP1**_a (Fig. 2, top) revealed distinct differences in the nature of the pores in these two materials. The upward slope in the adsorption branch of the isotherm for **POP1**_a, which becomes steeper at higher pressures, has been attributed to the presence of pores that are larger than the

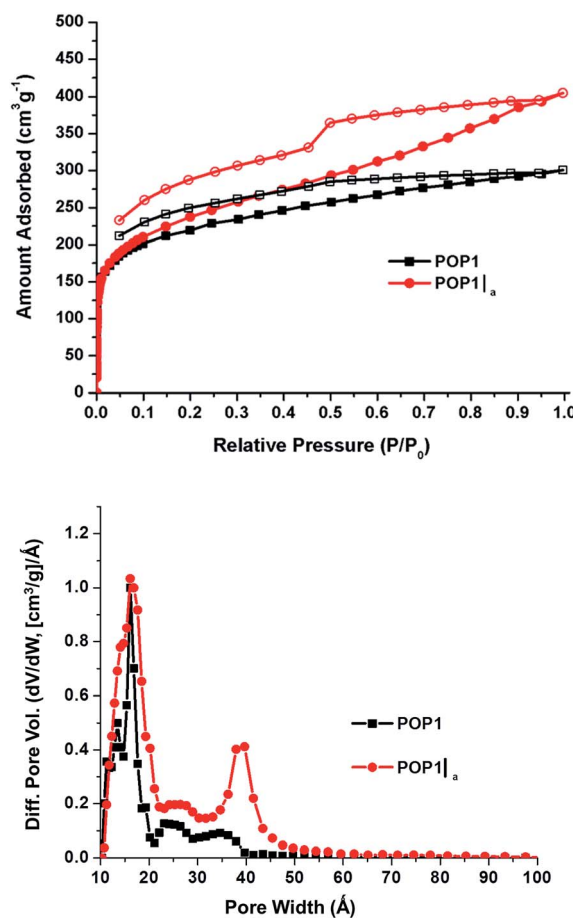


Fig. 2 (Top) N₂ isotherms, measured at 77 K, of **POP1** (black squares) and **POP1**_a (red circles). Closed symbols, adsorption; open symbols, desorption. (Bottom) Pore size distributions based on DFT calculations (slit-pore model) for **POP1**_a (red circles) and **POP1** (black squares).

typical micropores.²⁴ The hysteresis in the isotherm for **POP1**_a has a distinct step in the desorption branch, indicating that the pores are not all slit-like.²⁴ Not surprisingly, **POP1**_a has an increased surface area¹ (910 m² g⁻¹, Table 1, entry 2) compared to that of **POP1** (800 m² g⁻¹, Table 1, entry 1). Notably, the total pore volume of **POP1**_a (0.59 cm³ g⁻¹, Table 1, entry 2) has increased significantly (by 41%) from that of **POP1** (0.42 cm³ g⁻¹, Table 1, entry 1) while its micropore volume (calculated from the *t* plot method) remains the same as that of **POP1**. Thus, the additional gain in pore volume in **POP1**_a can indeed be attributed to the introduction of larger pores through the aerogel template. This gain is more apparent in the pore size distribution plot for **POP1**_a, which exhibits a broad peak (~40 Å) in the mesopore region (Fig. 2, bottom). As expected, **POP1**_a shows a corresponding increase in the external surface area—*i.e.*, the surface area of all non-micropores—(410 m² g⁻¹, Table 1, entry 2) compared to that of **POP1** (250 m² g⁻¹; Table 1, entry 1).

To assess whether it is necessary to have a monolithic²⁵ aerogel template firmly affixed in a vial for the confined synthesis of **POP1**_a, we crushed an aerogel monolith into a



Table 1 Pore and surface properties of hierarchically porous POPs

Entry	POP	Specific surface area (ssa) (m ² g ⁻¹)	Total pore volume ^b (tpv) (cm ³ g ⁻¹)	Micropore volume ^a (cm ³ g ⁻¹)	Micropore surface area ^a (m ² g ⁻¹)	External surface area ^a (m ² g ⁻¹)	Percent increase in tpv and (ssa) (%)
1	POP1	800	0.42	0.23	550	250	0 (0)
2	POP1 _a	910	0.59	0.22	500	410	41 (14)
3	POP1 _a -TMS	1380	1.30	0.23	490	890	210 (73)
4	POP1 _a -Ph	1250	0.99	0.21	490	760	136 (56)
5	^{scp} POP1 _a	1590	1.70	0.19	450	1150	305 (99)
6	^{scp} POP1 _a -TMS	1640	1.90	0.20	440	1200	352 (105)
7	^{scp} POP1 _a -Ph	1640	1.90	0.19	430	1210	352 (105)

^a Obtained using *t* plot method (see ESI, Section S1). ^b Total pore volume is obtained from BET data up to $P/P_0 = 1$ and is defined as the sum of micropore volume and volumes of larger pores.

powder and carried out POP synthesis using the same conditions described above (see ESI,† Section S5). The N₂ gas adsorption–desorption and pore size distribution data for these POP1|_a-crushed materials (ESI,† Fig. S4) are essentially the same as those for POP1: there is no gain in either the external surface area or the amount of mesopores (ESI,† Table S2). This clearly illustrates the need for a monolithic template that completely fills the reaction volume in which the POP synthesis takes place. When the monolith is broken into loosely packed individual chunks that resemble chromatographic silica gel powder, the total volume that this powder occupies decreases compared to that of the monolith and there is a large amount of macroscopic “empty” space where the silica is not present. In such a case, if we employ the same polymerization reaction volume as that used in the monolith, a significant portion of the polymerization will occur in this “empty” volume and the resulting polymer will have mostly micropores. As a result, the final POP1|_a-crushed material is actually quite similar to POP1, the POP synthesized without template, and no enhancement in mesoporosity is observed.

Our model (Fig. 1) suggests that the mesopores in POP1|_a primarily arise from the extensive mesoporous interstitial space between the silica gel nanoparticles in the aerogel template (>94% of the ssa is external surface area and >99% of the total pore volume is mesopore volume; see ESI,† Table S1).²⁶ If this is indeed the case, while our initial gain in external surface area (~160 m² g⁻¹) for POP1|_a is promising, it is only a fraction of the very large portion of external surface area that was present in the original aerogel template.²⁷ We hypothesize that this discrepancy may be caused by the loss of the mesopores upon dissolution of the silica gel template. Specifically, if the polymerization shown in Fig. 1 does not generate a mechanically robust network of cross-linked polymer, dissolution of the silica gel template may result in the collapse of such mesopores and a subsequent loss of external surface area (Fig. 3, top).

One strategy for avoiding potential collapse of the templated POP network upon work up, and increasing the retention of mesoporosity in the resulting POP, is to strengthen the polymer network. This may be accomplished by increasing the interaction between the organic component (monomer/polymer) and the inorganic silica aerogel template during polymerization.

Such increased interaction may lead to a thicker polymer “coating” of the silica nanoparticles during the polymerization process and a more mechanically robust network of cross-linked polymer (Fig. 3, bottom). Such a network would be better able to retain the mesopores upon dissolution of the silica gel template, resulting in a higher external surface area for the final POP.

To explore the aforementioned hypothesis, we post-synthetically modified the surface hydroxyl groups of the silica aerogel with either trimethylchlorosilane (TMCS) or phenyltriethoxysilane (PTES) (ESI,† Section S3). Such “capping” with hydrophobic organic groups does not significantly change the surface area of the aerogel (ESI,† Fig. S2) but should allow the resulting surface to interact strongly with the hydrophobic dialkyne monomer **1** and the Co-based propagating species, creating a more mechanically robust network. The resulting POP materials can then better tolerate the processing conditions and have larger total pore volumes and external surface

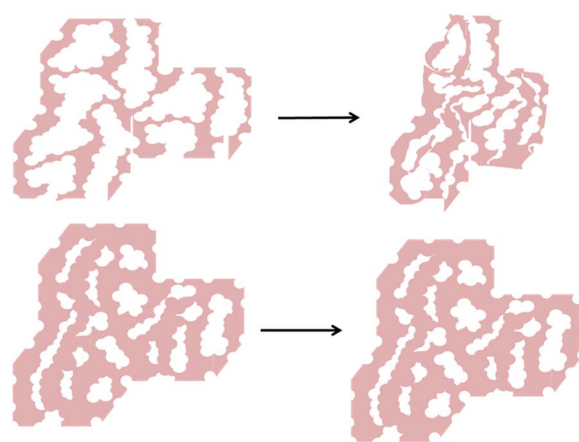


Fig. 3 A schematic illustration of the benefit of having a polymer network with “thicker” features. A polymer network with “thin” features may collapse more easily by the capillary action during work up (top) and lose a significant portion of the mesoporosity that arose from the interstitial spaces between the silica nanoparticles. In contrast, a network with “thicker” features is not as easily collapsed (bottom), retaining a higher portion of mesoporosity.



areas. This is indeed the case. BET analyses of **POP1**_{a-TMS} and **POP1**_{a-Ph}—the two materials producing by polymerizing 1,4-dialkynebenzene inside the trimethyl- and phenyl-modified aerogels, respectively—revealed highly enhanced surface areas (1380 and 1250 m² g^{−1}, respectively; ESI,† Fig. S5). Most impressive are the large gains in total pore volumes (68–120%) and external surface areas (85–117%) for both of these materials compared to **POP1**_a (Table 1, cf. entries 2–4). Of course, we cannot discount contributions from increases in the interstitial space between the organic-modified aerogel particles that might have occurred as a result of the steric “capping” by TMS and Ph groups. Such modification of the surface of the silica gel nanoparticles has been shown to prevent them from excessive shrinking upon drying^{28,29} (see also ESI,† Fig. S12) and can contribute to the increased external surface area of the modified templates. Due to the lengthy modification process (ESI,† Section S3), we have not attempted to control the extent of modification and determine the relative contributions of these two factors. Interestingly, while the pore size distributions for **POP1**_{a-TMS} and **POP1**_{a-Ph} are very different from those of **POP1** and **POP1**_a (Fig. 4 and Table 1), they are very similar to each other.

Up to this point, our results clearly indicate that the confined syntheses of **POP1** inside silica aerogel templates can indeed generate a significant amount of mesopores. While this is quite exciting, the surface area and porosity data that we have obtained thus far are for materials that have been thermally activated (*i.e.*, heat-treated under vacuum) prior to surface characterization. Although thermal activation is a commonly employed protocol for many porous solids such as zeolites, mesoporous silica, and MOFs, recent research has indicated that fast solvent removal during such a process may lead to strong capillary actions that collapse interstitial pores or pore apertures, resulting in low overall surface areas and pore accessibilities for both MOFs^{30,31} and POPs.¹⁹ Following the protocol established by Totten *et al.*,¹⁹ we activated all three of our hierarchically porous POPs using supercritical CO₂ processing instead of thermal activation. Gratifyingly, the

supercritical CO₂-processed POPs (^{scp}**POP1**_a, ^{scp}**POP1**_{a-TMS}, and ^{scp}**POP1**_{a-Ph}) display significant increases in both external surface areas (34–179%) and total pore volumes (46–188%) in comparison to the thermally activated samples (Table 1, cf. entries 5–7 and entries 2–4). Most notably, the N₂ isotherms for the supercritical CO₂-processed materials are all Type II with pronounced hysteresis (Fig. 5, top panel; see also ESI,† Fig. S6). The presence of pores that are larger than 20 Å is clearly indicated by the steep upward-sloping trend of the isotherm at high pressures ($P/P_0 > 0.9$). Indeed, the pore size distributions for these materials all display broad mesoporous regions with several peaks extending over a wide range of pore diameters (Fig. 5, bottom panel; see also ESI,† Fig. S7). Comparing to the data shown in Fig. 4, these data suggest that even larger mesopores (>50 Å) exist in the interstitial space between the POP nanoparticles and can indeed be preserved by supercritical CO₂ processing.

To assess the transport advantage of having large mesopores integrated into **POP1**, we compared the time-dependence for propane uptake in **POP1**, **POP1**_a, ^{scp}**POP1**_a, **POP1**_{a-TMS}, and **POP1**_{a-Ph} at 0.3 bar and 298 K (Fig. 6). The hierarchically porous POPs (**POP1**_a, ^{scp}**POP1**_a, **POP1**_{a-TMS}, and **POP1**_{a-Ph}) all adsorb

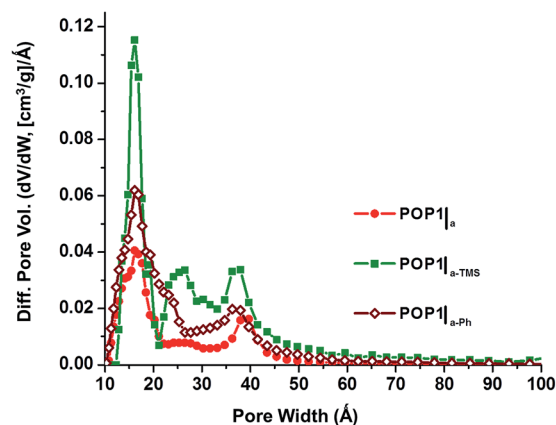


Fig. 4 Pore size distributions based on DFT calculations (slit-pore model) for **POP1**_a (red circles), **POP1**_{a-TMS} (green squares), and **POP1**_{a-Ph} (brown diamonds).

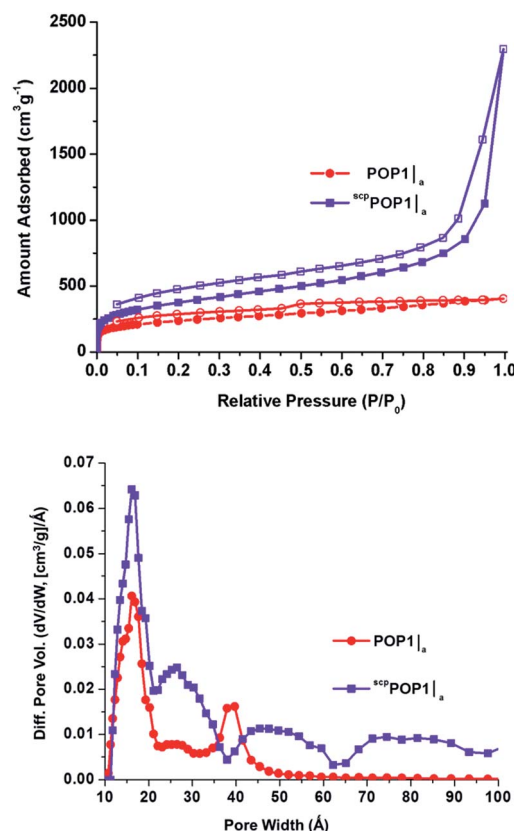


Fig. 5 (Top) N₂ isotherms measured at 77 K of **POP1**_a (red circles) and supercritical CO₂-processed POP-A (^{scp}**POP1**_a – purple squares). Closed symbols, adsorption; open symbols, desorption. (Bottom) pore size distributions based on DFT calculations (slit-pore model) for **POP1**_a (red circles) and ^{scp}**POP1**_a (purple squares). See ESI† for the isotherms (Fig. S6) and pore size distributions (Fig. S7) of other supercritical CO₂-processed POPs.



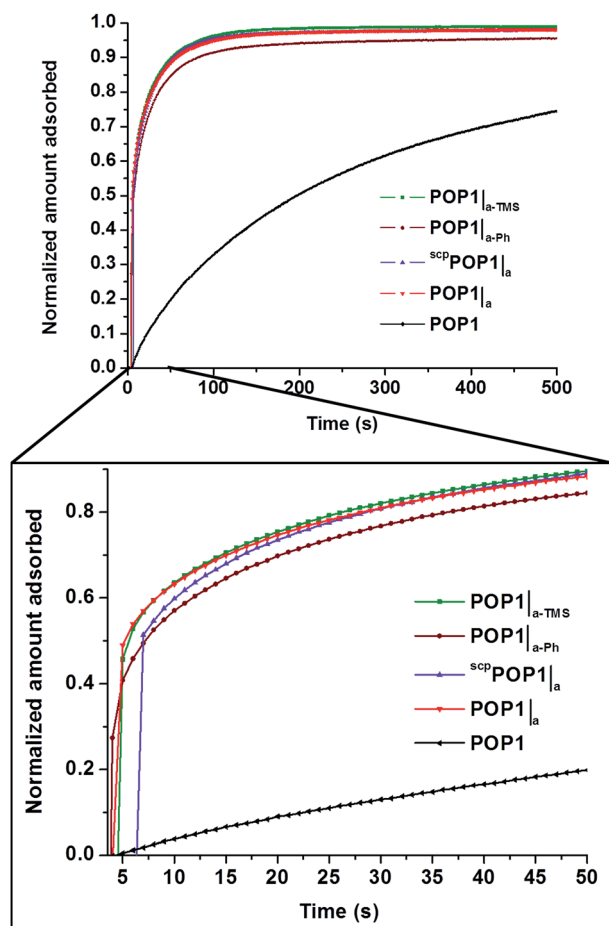


Fig. 6 Time-dependent propane-uptake profiles for POP1, POP1|_a, scpPOP1|_a, POP1|_a-TMS, and POP1|_a-Ph at 0.3 bar and 298 K. Data in each profile were normalized to the maximum uptake values at 15 000 s (see complete set of data in the ESI,† Fig. S13).

propane much faster than the parent POP1. As quantified by the diffusional time constants for propane transport through the POP materials (given by D/r^2 , where D is the diffusion coefficient and r is the characteristic length scale, as defined in the ESI,† Section S15), the hierarchically porous POPs adsorb propane at a rate that is a factor of 4 to 8 times faster than that for POP1 (see ESI,† Table S4). These improved diffusion characteristics may comprise a clear advantage for applications in separation, catalysis, and sensing.

Conclusions

In summary, we have demonstrated that hierarchically porous POPs containing both meso- and micropores can be realized by carrying out the synthesis of a microporous POP inside a monolithic mesoporous silica aerogel template followed by dissolving away the template in a manner that preserves the larger pores. The total pore volumes and specific surface areas can be increased (up to 210 and 73%, respectively) without altering the micropore volumes through the use of a hydrophobic aerogel template that interacts better with the monomer

and polymer. Supercritical CO₂ processing of these POPs can further enhance the total pore volumes (by an additional 142%) and specific surface areas (by an additional 32%) and by preventing the loss of large (*i.e.*, >50 Å) interparticle mesopores during thermal activation. The utility of having the additional hierarchy of mesopores in POPs is clearly apparent through the faster uptake of propane by the hierarchical POPs, illustrating highly facile diffusion that should be highly advantageous in catalysis, separation, and sensing. We are currently exploring such applications.

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Notes and references

- 1 Y. Zhang and S. N. Riduan, *Chem. Soc. Rev.*, 2012, **41**, 2083–2094.
- 2 Z. Xie, C. Wang, K. E. deKrafft and W. Lin, *J. Am. Chem. Soc.*, 2011, **133**, 2056–2059.
- 3 A. M. Shultz, O. K. Farha, J. T. Hupp and S. T. Nguyen, *Chem. Sci.*, 2011, **2**, 686–689.
- 4 N. B. McKeown and P. M. Budd, *Chem. Soc. Rev.*, 2006, **35**, 675–683.
- 5 H. J. Mackintosh, P. M. Budd and N. B. McKeown, *J. Mater. Chem.*, 2008, **18**, 573–578.
- 6 P. Kaur, J. T. Hupp and S. T. Nguyen, *ACS Catal.*, 2011, **1**, 819–835.
- 7 J.-X. Jiang, C. Wang, A. Laybourn, T. Hasell, R. Clowes, Y. Z. Khimyak, J. Xiao, S. J. Higgins, D. J. Adams and A. I. Cooper, *Angew. Chem., Int. Ed.*, 2011, **50**, 1072–1075.
- 8 T. Ben, H. Ren, S. Ma, D. Cao, J. Lan, X. Jing, W. Wang, J. Xu, F. Deng, J. M. Simmons, S. Qiu and G. Zhu, *Angew. Chem., Int. Ed.*, 2009, **48**, 9457–9460.
- 9 Q. Chen, M. Luo, P. Hammershøj, D. Zhou, Y. Han, B. W. Laursen, C.-G. Yan and B.-H. Han, *J. Am. Chem. Soc.*, 2012, **134**, 6084–6087.
- 10 A. I. Cooper, *Adv. Mater.*, 2009, **21**, 1291–1295.
- 11 B. G. Hauser, O. K. Farha, J. Exley and J. T. Hupp, *Chem. Mater.*, 2013, **25**, 12–16.
- 12 M. G. Rabbani and H. M. El-Kaderi, *Chem. Mater.*, 2011, **23**, 1650–1653.



- 13 J. Weber and A. Thomas, *J. Am. Chem. Soc.*, 2008, **130**, 6334–6335.
- 14 D. Yuan, W. Lu, D. Zhao and H.-C. Zhou, *Adv. Mater.*, 2011, **23**, 3723–3725.
- 15 M. G. Rabbani and H. M. El-Kaderi, *Chem. Mater.*, 2012, **24**, 1511–1517.
- 16 G. Peterson, O. Farha, B. Schindler, P. Jones, J. Mahle and J. Hupp, *J. Porous Mater.*, 2012, **19**, 261–266.
- 17 O. K. Farha, A. M. Spokoyny, B. G. Hauser, Y.-S. Bae, S. E. Brown, R. Q. Snurr, C. A. Mirkin and J. T. Hupp, *Chem. Mater.*, 2009, **21**, 3033–3035.
- 18 C. M. A. Parlett, K. Wilson and A. F. Lee, *Chem. Soc. Rev.*, 2013, **42**, 3876–3893.
- 19 R. K. Totten, Y.-S. Kim, M. H. Weston, O. K. Farha, J. T. Hupp and S. T. Nguyen, *J. Am. Chem. Soc.*, 2013, **135**, 11720–11723.
- 20 F. Hoffmann, M. Cornelius, J. Morell and M. Fröba, *Angew. Chem., Int. Ed.*, 2006, **45**, 3216–3251.
- 21 H. Chen, J. Wydra, X. Zhang, P.-S. Lee, Z. Wang, W. Fan and M. Tsapatsis, *J. Am. Chem. Soc.*, 2011, **133**, 12390–12393.
- 22 M. S. Sigman, A. W. Fatland and B. E. Eaton, *J. Am. Chem. Soc.*, 1998, **120**, 5130–5131.
- 23 S. Yuan, B. Dorney, D. White, S. Kirklin, P. Zapol, L. Yu and D.-J. Liu, *Chem. Commun.*, 2010, **46**, 4547–4549.
- 24 P. Pandey, O. K. Farha, A. M. Spokoyny, C. A. Mirkin, M. G. Kanatzidis, J. T. Hupp and S. T. Nguyen, *J. Mater. Chem.*, 2011, **21**, 1700–1703.
- 25 Herein, we employed the definition of monolith as “being casted as a single macroscopic piece.” Morphologically, the aerogel monolith is made up of chain of silica gel particles. See the ESI,† Fig. S12 for SEM images of the aerogels.
- 26 While some of the mesopores in **POP1**_a may be generated from the dissolved-away silica nanoparticles (~10–20 nm in size, see N. Leventis, *Acc. Chem. Res.*, 2007, **40**, 874–884) that make up the gel, this portion is probably insignificant.
- 27 R. Al-Oweini and H. El-Rassy, *Appl. Surf. Sci.*, 2010, **257**, 276–281.
- 28 P. B. Sarawade, J.-K. Kim, A. Hilonga and H. T. Kim, *Solid State Sci.*, 2010, **12**, 911–918.
- 29 A. P. Rao, A. V. Rao and G. M. Pajonk, *Appl. Surf. Sci.*, 2007, **253**, 6032–6040.
- 30 A. P. Nelson, O. K. Farha, K. L. Mulfort and J. T. Hupp, *J. Am. Chem. Soc.*, 2008, **131**, 458–460.
- 31 O. K. Farha and J. T. Hupp, *Acc. Chem. Res.*, 2010, **43**, 1166–1175.

