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ARTICLE

A new post-synthetic route to graft amino groups in porous organic polymers for CO₂ captureQihao Yue Wang ^{a†}, Lin Lin ^{a†}, Li Jiang ^a, Zihao Wang ^a, Yina Zhang ^a, Qiance Han ^a, Xin Huang ^a, Changyan Zhu ^a, Jiangtao Jia ^{a*}, Zheng Bian ^{a*}, Guangshan Zhu ^{a*}Received 00th January 20xx,
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Herein, we report the development of a post-synthetic modification approach to introduce a high loading of formyl groups onto porous aromatic framework (PAF)-5 via Friedel-Crafts alkylation followed by hydrolysis. Rigorous characterization by NMR, X-ray photoelectron spectroscopy, and Fourier-transform infrared spectroscopy authenticated the successful integration of aldehyde moieties into PAF-5, affording PAF-5-CHO. Subsequent functionalization of PAF-5-CHO with various amines produced three amine-functionalized PAF derivatives. Notably, PAF-5-C=N-EDA exhibited a 78% enhancement in carbon dioxide (CO₂) adsorption capacity, reaching 3.78 mmol g⁻¹ at 1 bar and 298 K relative to PAF-5-CHO. Breakthrough experiments demonstrated that PAF-5-C=N-EDA could effectively separate CO₂ from simulated flue gas (CO₂/N₂ = 15:85, v/v; 10 mL min⁻¹). In-situ infrared spectroscopy, density functional theory calculations and temperature-programmed desorption studies provided insights into the CO₂ adsorption mechanism.

Introduction

Since the Industrial Revolution in the 18th century, the excessive exploitation and combustion of carbon-based fossil fuels such as coal, oil, and natural gas have driven a remarkable increase in carbon dioxide (CO₂) emissions across the globe.¹ As a result, severe environmental issues have emerged, including the greenhouse effect, ocean acidification, sea-level rise, and climate change, all of which pose significant threats to human well-being. Replacing traditional fossil fuels with clean energy sources such as solar, hydrogen, wind, or nuclear energy represents a promising strategy for mitigating CO₂ emissions. However, the current exploitation and implementation of clean energy fall short of meeting the established emission reduction targets.² Therefore, CO₂ capture and storage (CCS), a process that separates CO₂ from the flue gas of coal-fired power plants and stores it underground, remains a key strategy for reducing global CO₂ emissions during the transition to clean energy.³

There are five principal methods for capturing CO₂: membrane separation, solvent-based absorption, physical adsorption, cryogenic separation, and chemical looping.⁴ Among these, aqueous amine solutions, which capture CO₂ via the formation of carbamates or bicarbonates, remain the most mature and widely applied technology. However, aqueous

amine systems suffered from significant drawbacks, including volatility, oxidative degradation, equipment corrosion, and high operational costs.⁵ Due to these limitations, several new CCS methods have emerged in recent years, among which solid porous materials, such as activated carbons, metal-organic frameworks (MOFs), porous organic polymers (POPs), silica, and zeolites, have received considerable attention and extensive research.^{6–11} These materials offer advantages like high adsorption efficiency, low energy consumption, stability, and ease of regeneration.

Post-synthetic modification (PSM) is a vital approach for developing and enhancing solid materials such as MOFs and POPs, offering extensive functionality and broad applicability.^{12–19} Incorporating CO₂-philic functional groups into porous materials by PSM has been proven to enhance strong interactions between CO₂ and materials, significantly improving their selectivity for CO₂ capture.^{20–24} Porous aromatic frameworks (PAFs), a subset of POPs, possess high specific surface areas and porosities, which significantly enhance gas contact efficiency. PAFs are typically constructed through C–C covalent bonds, and their robust skeletons confer high chemical stability, enabling them to withstand harsh conditions for PSM process. In previous studies, PSM has been used to introduce functional groups such as –SH, –NH₂, –SO₃H, and –Cl into PAFs frameworks, enabling their applications in areas such as seawater desalination, gas adsorption, and catalysis.^{25–36} In addition, PAFs are ideal candidates for incorporation of CO₂-philic functional groups, which can strongly interact with CO₂ and thus facilitate efficient capture.

In this study, we propose a new PSM strategy to enhance the CO₂ capture efficiency of PAFs. This method allows for the

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simple and efficient introduction of aldehyde groups into the PAF framework by way of Friedel-Crafts reaction, resulting in the synthesis of PAF-5-CHO. Notably, direct PSM of $-\text{CHO}$ groups in the frameworks has not yet been reported. The aldehyde group has the potential to be transformed into different functional groups.^{37, 38} Accordingly, the PAF-5-CHO was further functionalized with amino groups via Schiff base reactions with organic amines aiming to enhance CO_2 capture performance. The resulting series of amino-functionalized PAFs exhibit excellent CO_2 capture and separation properties.

Results and discussion

Synthesis and characterization of PAF-5-CHO

PAF-5 was synthesized as reported³⁹ and the detailed synthesis method of PAF-5-CHO was described in the Experimental section. The dichloromethylation of PAF-5 in chloroform under the activation of anhydrous AlCl_3 and subsequent hydrolysis afforded PAF-5-CHO (Figure 1a). In the solid-state carbon ^{13}C NMR spectrum of PAF-5 (Figure 1b), the peaks at 135 ppm and 120 ppm correspond to the substituted and unsubstituted carbons on phenyl rings, respectively.³⁹ Compared to PAF-5, the spectrum of PAF-5-CHO (Figure 1c) showed similar peaks at 133 ppm and 120 ppm for the substituted and unsubstituted carbons on phenyl rings, but with a different signal at 183 ppm. According to the literature,⁴⁰ this peak was attributed to the carbon of the aldehyde group, confirming the successful introduction of functional aldehyde groups. The signal at 40 ppm and 67 ppm were attributed to the carbon of $-\text{CHCl}-$ and

$-\text{CHCl}_2$ group⁴¹, respectively, indicating that partial $-\text{CHCl}_2$ groups and $-\text{CHCl}-$ groups remained unhydrolyzed due to steric effect or dead-end pore (Figure S1). Additionally, in the Fourier transform infrared (FTIR) spectrum (Figure 1d), the peak at 1700 cm^{-1} was characteristic of $\text{C}=\text{O}$ bond of aldehyde groups,²³ while the peak at 783 cm^{-1} was attributed to the unhydrolyzed $\text{C}-\text{Cl}$ bond.²⁷ The formation mechanism of aldehyde groups in PAF-5-CHO by way of Friedel-Crafts alkylation and acidic hydrolysis was illustrated in Figure 1e. Notably, the method to introduce $-\text{CHCl}_2$ groups by Friedel-Crafts alkylation is limited to the rigid organic framework. In rigid aromatic porous material, these $-\text{CHCl}_2$ groups can't further react with other aromatic units, making them completely stay on the framework.

Additionally, the high-resolution $\text{C } 1\text{s}$ XPS spectrum of PAF-5 (Figure S2) shows only a single peak corresponding to $\text{C}-\text{C}$ bonds. In contrast, the $\text{C } 1\text{s}$ spectrum of PAF-5-CHO displays new peaks at 286.5 eV and 288.7 eV, corresponding to $\text{C}-\text{Cl}$ and $\text{C}=\text{O}$ bonds, respectively.⁴² Elemental oxygen analysis of PAF-5-CHO (Table S1) reveals an oxygen content of 7.475 wt%, indicating the introduction of approximately 1.5 aldehyde groups per structural unit of PAF-5. However, thermogravimetric analysis (TGA) results (Figure S3a) show a weak thermal stability for PAF-5-CHO compared to PAF-5 due to the lower pyrolysis temperature of $-\text{CHO}$ groups than aromatic groups. Furthermore, the scanning electron microscope (SEM) images (Figure S4a-c) exhibit no marked changes after the modification process. Powder X-ray diffraction (PXRD) patterns (Figure S5) indicates that PAF-5-CHO remains an amorphous material.

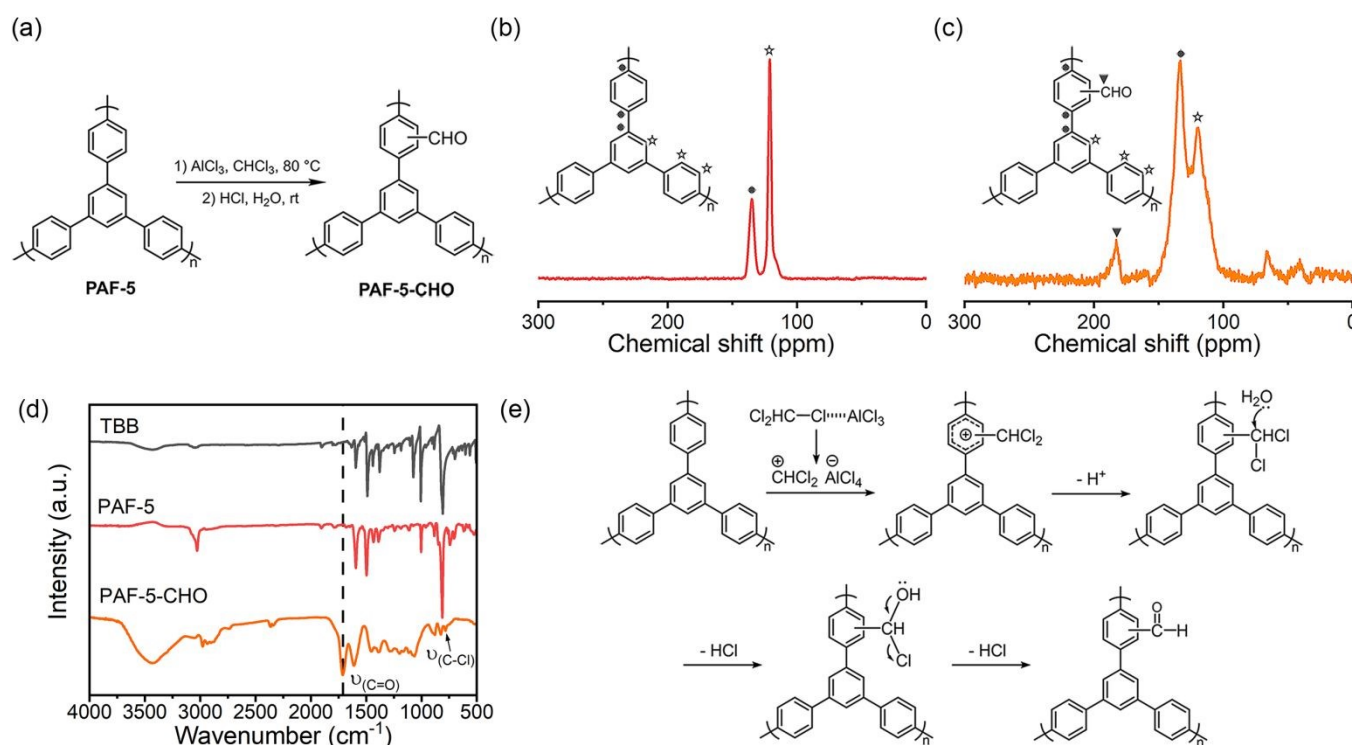


Figure 1 (a) The synthesis of PAF-5-CHO; (b) ^{13}C CP/MAS NMR spectrum of PAF-5; (c) ^{13}C CP/MAS NMR spectrum of PAF-5-CHO. (d) FTIR spectra of PAF-5-CHO, PAF-5, TBB (1,3,5-Tris(4-bromophenyl) benzene); (e) The formation mechanism of $-\text{CHO}$ groups.



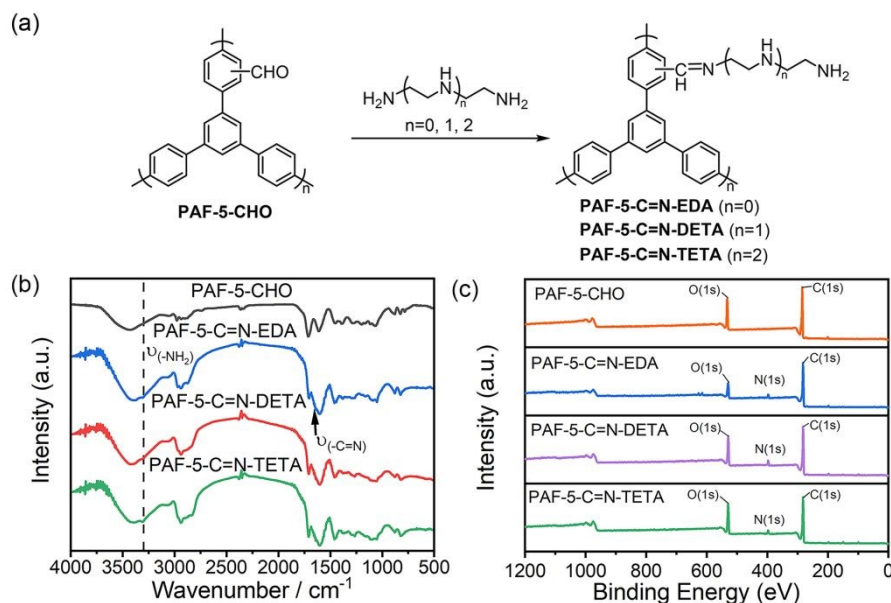


Figure 2 (a) Synthetic route to organic amine-modified PAF-5; (b) FTIR spectra of PAF-5-C=N-TETA, PAF-5-C=N-DETA, PAF-5-C=N-EDA and PAF-5-CHO; (c) XPS full-spectrum of PAF-5-CHO, PAF-5-C=N-TETA, PAF-5-C=N-EDA and PAF-5-C=N-DETA.

Synthesis of organic amine-modified PAF-5 materials

To introduce CO₂-philic functional groups, we selected three organic amines with different chain lengths and successfully synthesized a series of amine-functionalized PAF-5 materials via Schiff base reactions (Figure 2a). In the FTIR spectra of PAF-5-C=N-EDA, PAF-5-C=N-DETA, and PAF-5-C=N-TETA (Figure 2b), the emergence of -NH₂ vibration at 3300 cm⁻¹ and -C=N vibration at 1640 cm⁻¹ confirms the success happening of the Schiff base reaction.²³ In the XPS total spectrum (Figure 2c), the presence of the N element can be clearly evident. Additionally, in the high-resolution N 1s XPS spectra of PAF-5-C=N-EDA, PAF-5-C=N-DETA, and PAF-5-C=N-TETA (Figure S6), the peaks at 398.6 eV, 398.3 eV, and 398.2 eV are as assigned to C=N bonds, while the three spectra showed the peaks at 399.4 eV, 399.1 eV, and 399 eV correspond to -NH₂ and -NH- species.⁴³⁻⁴⁵ Elemental analysis (Table S2) further supports the formation of imine bonds, showing a significant increase in nitrogen content for the three amine-functionalized materials compared to PAF-5-CHO. Among them, PAF-5-C=N-TETA exhibits the highest nitrogen content at 10.04 wt%, equivalent to approximately 0.8 -NH₂ groups per triphenyl benzene unit of PAF-5. Based on these data, it can be inferred that around 50% of the aldehyde groups participate in the reaction. Moreover, TGA analysis (Figure S3b) demonstrates that the amine-functionalized PAF-5-CHO materials maintain stability in air up to 235 °C. The weight loss observed between 235 °C and 520 °C is attributed to the decomposition of the amine chains.²⁰ SEM images (Figure S4d-f) reveal no significant morphological changes in the materials after amine modification.

Gas adsorption and desorption

The adsorption isotherms of PAF-5, PAF-5-CHO, PAF-5-C=N-EDA, PAF-5-C=N-DETA, and PAF-5-C=N-TETA at 77 K are shown in Figure 3a. Their corresponding Brunauer-Emmett-Teller (BET) surface areas are 1660, 1510, 1423, 1224, and 1101 m² g⁻¹, respectively. The reduction in the BET surface area for PAF-5-

CHO is likely due to the aldehyde groups occupying the pore channels, as evidenced by the decrease in pore width from 1.75 nm to 1.03 nm (Figure S7). PAF-5-C=N-EDA, PAF-5-C=N-DETA, and PAF-5-C=N-TETA, exhibit further reductions in both BET surface area and pore volume relative to PAF-5-CHO. When the transformation of aldehyde groups into long-chains happens, the materials become heavier and the larger amine molecules occupy more pore space. Figures 3b and S8 illustrate the CO₂ adsorption isotherms of PAF-5-CHO and the three amine-functionalized PAF-5 materials at 298 K and 273 K. Across the entire experimental pressure range (0-100 kPa), the CO₂ adsorption capacity of PAF-5-C=N-EDA, PAF-5-C=N-DETA, and PAF-5-C=N-TETA shows a remarkable improvement compared to PAF-5-CHO. This demonstrates that organic amine modification significantly enhances CO₂ adsorption performance. Among the three materials, PAF-5-C=N-EDA shows the greatest improvement in CO₂ adsorption capacity, primarily attributed to its high specific surface area and the high loading of amine. Specifically, at 298 K, the CO₂ adsorption capacity of PAF-5-C=N-EDA is 3.78 mmol g⁻¹, which represents a 78% increase compared to PAF-5-CHO, and the adsorption capacity remains nearly unchanged after six cycles (Figure S9).

Flue gas emitted from coal-fired power plants contains approximately 15% CO₂ at 100 kPa, thus the CO₂ adsorption capacity at 15 kPa is highly relevant for practical applications. At 298 K and 15 kPa, among the three amine-functionalized materials, PAF-5-C=N-TETA exhibits the highest CO₂ adsorption capacity (Figure S10). Despite having the lowest BET surface area, PAF-5-C=N-TETA shows the highest nitrogen content—10.004% (Table S2). This indicates that at low pressure, CO₂ adsorption is more strongly influenced by the amine group content rather than BET surface area. Specifically, at 298 K, 15 kPa, the CO₂ adsorption capacity of PAF-5-CHO is 0.41 mmol g⁻¹, while that of PAF-5-C=N-TETA reaches 1.18 mmol g⁻¹, representing a twofold increase compared to PAF-5-CHO.



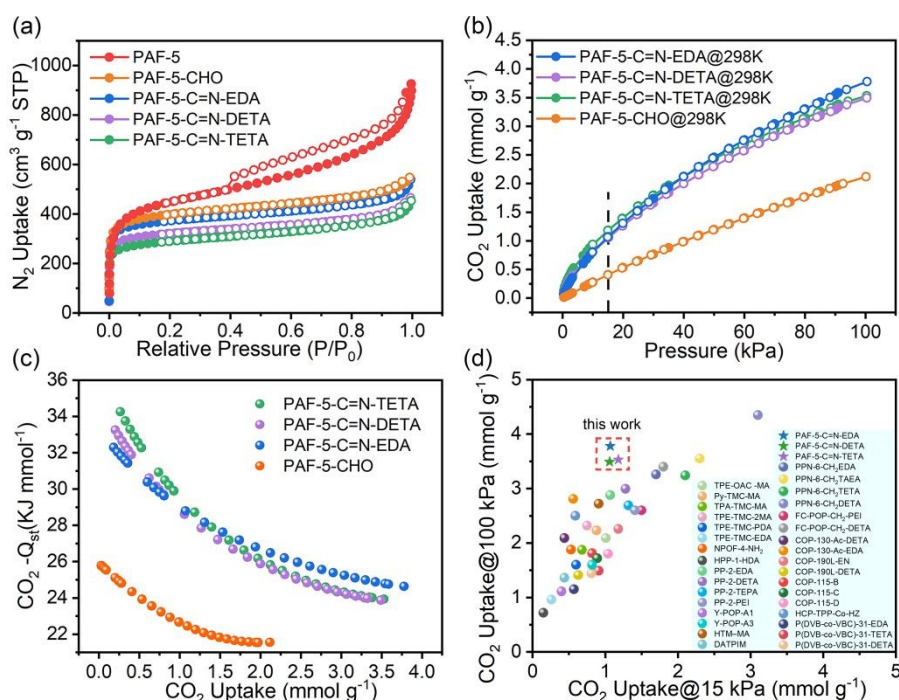


Figure 3 (a) N₂ uptake at 77 K; (b) CO₂ uptake of PAF-5-CHO and its derivations at 298 K; (c) CO₂-Q_{st} of PAF-5-CHO and its derivation; (d) Comparison of CO₂ uptake with other amine-functionalized POPs at 15 kPa and 100 kPa.^{20, 46-57}

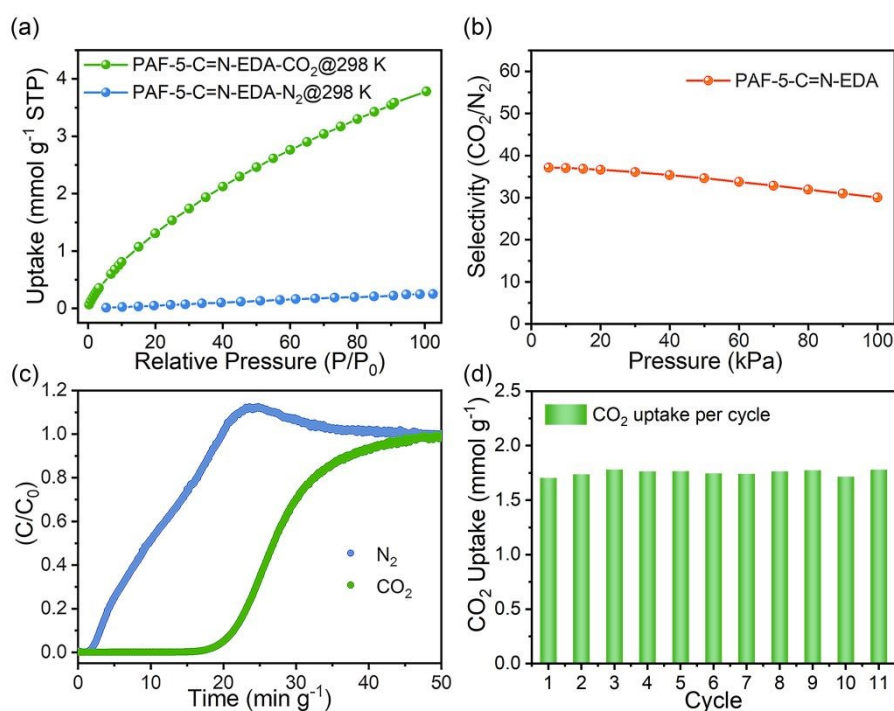


Figure 4 (a) N₂ and CO₂ uptake of PAF-5-C=N-EDA at 298 K; (b) CO₂/N₂ selectivity of PAF-5-C=N-EDA; (c) Breakthrough curves of PAF-5-C=N-EDA for a CO₂/N₂ (15:85, v/v) gas mixture with a total flow of 10 mL min⁻¹ at 298 K and 1 bar; (d) CO₂ uptakes of PAF-5-C=N-EDA derived from the breakthrough cycling measurement.

Furthermore, the isosteric enthalpy of adsorption (Q_{st}) plot (Figure 3c) determined from adsorption isotherm calculations at 273 K and 298 K shows that all three materials obtained after organic amine modification are significantly improved

compared to PAF-5-CHO. The $-Q_{st}$ of PAF-5-CHO is 25 kJ mol⁻¹, whereas PAF-5-C=N-TETA, PAF-5-C=N-DETA, and PAF-5-C=N-EDA exhibit higher $-Q_{st}$ values of 34, 33, and 32 kJ mol⁻¹, respectively. Moreover, the CO₂ desorption isothermal curves



of these three materials do not exhibit significant hysteresis loops, indicating their excellent cycling potential. Compared to other amine-functionalized POPs (Figure 3d), the three materials presented in this study exhibit higher adsorption capacities at both 15 kPa and 100 kPa. Thus, these materials demonstrate considerable promise for utilization in CO₂ capture and recovery applications.

Separate ability of PAF-C=N-EDA

Based on a comprehensive evaluation of the CO₂ adsorption performance and the cost of the adsorbents, we selected PAF-5-C=N-EDA for subsequent CO₂/N₂ separation experiments. Using the CO₂ and N₂ adsorption isotherms of PAF-5-C=N-EDA at 298 K (Figure 4a), the CO₂/N₂ selectivity was calculated using the Ideal Adsorbed Solution Theory (IAST) method. Figure 4b shows that the CO₂/N₂ selectivity of PAF-5-C=N-EDA is

approximately 37. To evaluate its actual separation performance, breakthrough experiments were conducted using 0.075 g of PAF-5-C=N-EDA powder. At 298 K and 1 bar, a CO₂/N₂ (15:85, v/v) gas mixture was passed through a tightly packed fixed-bed column containing PAF-5-C=N-EDA at a flow rate of 10 mL min⁻¹. As shown in Figure 4c, N₂ breakthrough occurred almost immediately, while CO₂ breakthrough was delayed for a retention time (15 min g⁻¹), demonstrating excellent CO₂ separation performance. The CO₂ capture capacity calculated from a single breakthrough experiment was 1.00 mmol·g⁻¹, consistent with the results from the CO₂ adsorption isotherm. After eleven consecutive breakthrough cycles (Figures S11 and S12), the material maintained good separation performance, with an average CO₂ adsorption capacity of 1.75 mmol·g⁻¹ during the breakthrough process.

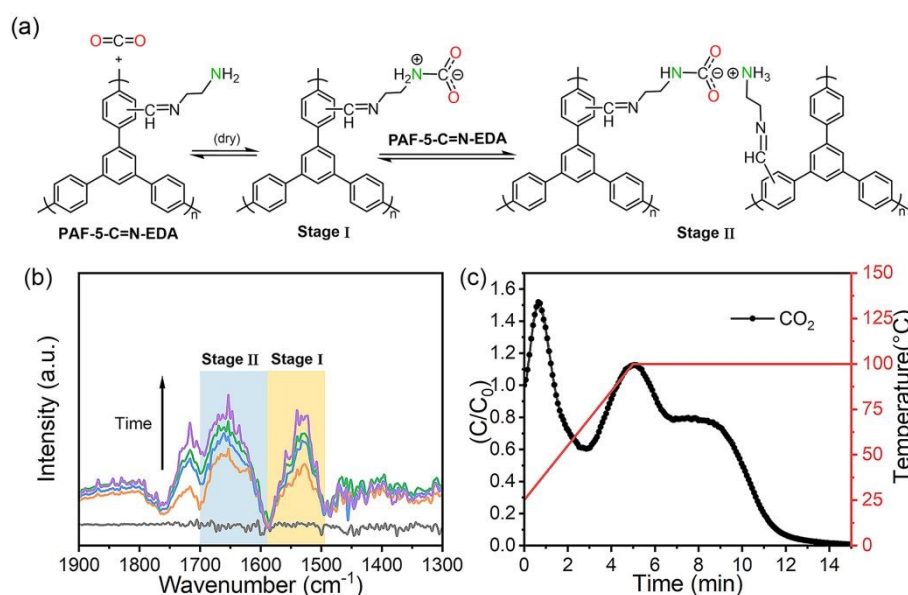


Figure 5 (a) Chemisorption mechanism of amines and CO₂ in dry conditions; (b) IR absorbance spectra of adsorbed species on PAF-5-C=N-EDA at 25 °C taken at different times during CO₂ adsorption; (c) Adsorbed phase analysis of PAF-5-C=N-EDA by using Temperature Programmed Desorption (TPD).

CO₂ adsorption mechanism

To analyze the CO₂ adsorption mechanism, we first performed density functional theory (DFT) simulations to investigate the potential interactions between the PAF-5-C=N-EDA framework and CO₂ molecules. Five potential CO₂ adsorption configurations were constructed and optimized (Figure S13). The calculated adsorption energies reveal that the interaction between the amine group and the C atom of CO₂ represents the dominant contribution, exhibiting the lowest adsorption energy (-0.31 eV). This suggests that the amine groups serve as the most favorable active sites for CO₂ adsorption. In this configuration, the N-C distance measures 2.76 Å, which is shorter than their sum of van der Waals radius. Additionally, the O-C-O angle of the adsorbed *CO₂ deviates slightly from linearity, changing from 180° to 175.0°. Charge transfer analysis indicates electron donation from PAF-5-C=N-EDA to the adsorbed *CO₂, with a Bader charge of 0.14 |e| localized on *CO₂. These results demonstrate that the adsorbed *CO₂

undergoes activation, consistent with the observed negative adsorption energy. To further assess the diffusion rate of CO₂ molecules on PAF-5-C=N-EDA model, we examined the diffusion pathway and the corresponding energy barrier of a single CO₂ molecule moving between two adjacent amine active sites (Figure S14). The computed diffusion barrier is remarkably low (0.09 eV), suggesting that CO₂ molecules can diffuse rapidly through the porous structure of the material.

We conducted in situ IR spectroscopy to monitor the adsorption process of CO₂ on PAF-5-C=N-EDA. During the experiment, CO₂ gas flowed through the PAF-5-C=N-EDA adsorbent. The absorption spectra shown in Figure S15 were obtained by collecting the PAF-5-C=N-EDA absorption spectra as a background, and the band produced by adsorbed CO₂ at 2360 cm⁻¹ can be observed.⁵⁸ In the IR spectra of PAF-5-C=N-EDA with adsorbed CO₂ (Figure 5b), the following features were identified: (i) The O=C=O⁻ band of carbamate NHCOO⁻ at 1532 cm⁻¹, (ii) The *N-H band of NH₃⁺ at 1656 cm⁻¹. The adsorption



mechanism inferred from the in-situ IR analysis is illustrated in Figure 5a, and the process occurs in two stages. To further confirm the adsorption mechanism, temperature-programmed desorption (TPD) of the post-breakthrough sample was performed (Figure 5c). The first desorption peak corresponds to weakly adsorbed CO₂ on the adsorbent and the column walls, while the second peak, appearing at temperatures above 100 °C, corresponds to the intermediate species described as Stage I in the mechanism diagram. A third peak represents the desorption of CO₂ species associated with Stage II of the mechanism temperatures above 100 °C, corresponding to the intermediate species described as Stage I in the mechanism diagram. A third peak represents the desorption of CO₂ species associated with Stage II of the mechanism.

Conclusion

We reported a post-modification method for PAFs that can introduce aldehyde groups into the framework of PAF-5 in a simple and efficient manner. Materials modified with aldehyde groups can be subjected to the subsequent reactions, and in this paper, we prepared a series of amino-modified PAFs by using the aldehyde group for the Schiff base reaction. Such materials were characterized by CO₂ adsorption-desorption isotherms and CO₂/N₂ dynamic breakthroughs, and we observed that PAF-5-C=N-EDA has excellent performance in capturing post-combustion CO₂. Through the investigation of the CO₂ adsorption mechanism, it was found that there are two distinct adsorption sites involved in the process. This study highlights the potential of this class of materials in post-combustion CO₂ capture technology.

Experimental

Materials

All starting materials and solvents, unless otherwise specified, were obtained from Innochem Co. and used

Synthesis of PAF-5 as reported

In a glovebox, 1,5-cyclooctadiene (cod) (0.93 mL, 7.92 mmol), bis(1,5-cyclooctadiene) nickel (0) (Ni(cod)₂) (2.18 g, 7.93 mmol), 2,2'-bipyridyl (1.24g, 7.94 mmol), and anhydrous *N,N'*-dimethylformamide (DMF) (40 mL) were added to a 250 mL double-neck flask. A solution of 1,3,5-tris(4-bromophenyl) benzene (TBB) in DMF (80 mL) was then slowly added to the mixture at 80 °C. The resultant system was further kept at 80 °C for 48 h. After cooling to room temperature, 6 M HCl was added to the mixture, and the mixture was stirred for 1 hour until it turned green with a snowflake-like solid formation, washed and dry to obtain the product.

Synthesis of PAF-5-CHO

PAF-5 (100 mg), anhydrous AlCl₃ (200 mg, 1.5 mmol) and CHCl₃ (40 mL) were added to a 100 mL flask. The mixture was stirred vigorously, heated to 80 °C and the reaction continued for one day. After quenching with 50 mL of methanol, the solid was filtered, and washed using 1 M hydrochloric acid and water

successively. After drying under vacuum, a brownish yellow solid was obtained.

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General procedure for the amine-functionalized materials

Take the synthesis of PAF-5-C=N-EDA as an example: the PAF-5-C=N-EDA (100 mg) and ethylenediamine (EDA, 10 mL) were added to a sealed flask. The mixture was kept at 80 °C for 3 days. The solid was filtered, washed with water and methanol, and then dried in vacuo to produce PAF-5-C=N-EDA as a brown powder in quantitative yield.

Materials and physical measurements

Fourier transform infrared spectroscopy (FTIR) spectra were recorded using a Nicolet IS50 Fourier transform infrared spectrometer. Solid-state ¹³C cross-polarization magic angle spinning nuclear magnetic resonance (NMR) spectra were acquired with a Bruker Avance III 400 MHz NMR spectrometer at a MAS rate of 5 kHz. X-ray photoelectron spectroscopy (XPS) spectra were obtained on a KRATOS Axis UltraDLD system, equipped with an Al Kα ray source (hν = 1486.6 eV) under a high vacuum of 9.8 × 10⁻¹⁰ Torr. N₂ isotherms at 77 K and vapor isotherms were measured using an Autosorb adsorptometer (JW-TB 400 and JW-ZQ 100). Thermal gravimetric analysis (TGA) was performed on a METTLER-TOLEDO TGA/DSC 3+ analyzer at a heating rate of 10 °C min⁻¹ under an air gas flow of 60 mL min⁻¹. Scanning electron microscope (SEM) images were captured using a Hitachi SU-70 microscope. Powder X-ray diffraction (PXRD) was performed on the Rigaku Smartlab X-ray diffractometer with Cu-Kα radiation, 40 kV, 200 mA with a step of 0.01. Elemental analysis was carried out with Eurovector EA3000 Analyzer. Elemental Oxygen analysis was carried out with Vario EL cube.

Breakthrough experiments

Breakthrough experiments were performed using a dynamic gas breakthrough device, mixSorb S (3P Instruments). The sample was heated under a vacuum at 100 °C for 8 h. A 0.075 g sample of PAF-5-C=N-EDA was loaded onto a stainless-steel column (1 mL volume, 0.45 cm inner diameter). A CO₂/N₂ (15:85, v/v) gas mixture was allowed to flow into the column. Use a mass spectrometer (Master 400) to monitor the gas flow from the column.

Author contributions

J. J., G. Z., Z. B. conceptualized and supervised. Q. W. planned research, synthesis; Q. W., L. L. analysed data. Q. W., L. L. wrote the manuscript. L. J, Z. W., Y. Z. synthesized and analysed for discussion. Q. H. SEM characterization, J. J., G. Z. revision.

Conflicts of interest

"There are no conflicts to declare".

Data availability

The data is available in supporting information.



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The data is available in supporting information.

