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## 1. Introduction

Approximately 60% of all brominated flame retardants contain TBBPA, which is used primarily in printed circuit boards, or as an additive in several types of polymers. In 2004, the global demand for TBBPA was estimated to be 170 000 tons,1 and China produces about 18 000 tons of the material per year. Despite its reactivity, TBBPA and its metabolites are released into the environment from either products treated with additives, or via reactions, and have been identified in samples of air, soil, and sediment,<sup>2</sup> as well as in wastewater.<sup>3</sup> Like most brominated aromatic flame retardants, TBBPA is lipophilic and difficult to degrade, and thus, adversely affects both environmental and biological systems.4 Therefore, the need to develop an effective method of clearing TBBPA from the environment is significant and urgent. Current methods for the removal of TBBPA from water include adsorption, biological degradation, ozonolysis, and catalytic oxidation.5-9 Because TBBPA can be

# Fe<sub>3</sub>O<sub>4</sub>/MWCNT as a heterogeneous Fenton catalyst: degradation pathways of tetrabromobisphenol A<sup>+</sup>

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Tetrabromobisphenol A (TBBPA) is the most widely used brominated flame retardant around the world. In this study, we report that iron oxide decorated on a magnetic nanocomposite (Fe<sub>3</sub>O<sub>4</sub>/MWCNT) was used as a heterogeneous Fenton catalyst for the degradation of TBBPA in the presence of H<sub>2</sub>O<sub>2</sub>. Fe<sub>3</sub>O<sub>4</sub>/MWCNT was prepared by a simple solvothermal method, whereby an iron source (Fe(acac)<sub>3</sub>) and a reductant  $(n-1)^{-1}$ octylamine) were allowed to react in n-octanol solvent. Monodisperse Fe<sub>3</sub>O<sub>4</sub> nanoparticles of consistent shape were uniformly dispersed on the nanotubes. Samples were characterized by transmission electron microscopy, X-ray diffraction, Fourier transform infrared spectroscopy, X-ray photoelectron spectroscopy, Brunauer-Emmett-Teller surface area measurement, and vibrating sample magnetometry. The samples effectively catalyzed the generation of hydroxyl radicals ( $\cdot$ OH) from H<sub>2</sub>O<sub>2</sub>, which degraded and subsequently mineralized the TBBPA. The whole process took four hours at near neutral pH. A degradation pathway for the system was proposed following analysis of intermediate products by gas chromatography-mass spectrometry. The quantification of Fe<sup>2+</sup> and Fe<sup>3+</sup> distribution before and after the recycling test of the composite were explored by X-ray photoelectron spectroscopy, in order to explain the stability and recyclability of the composite. Analysis of the results indicated that the magnetic nanocomposite is a potentially useful and environmentally compatible heterogeneous Fenton's reagent with promising applications related to pollution control.

> broken into small, less toxic or harmless molecules, catalytic degradation is an increasingly important method of controlling this refractory organic pollutant. In 1894 Henry Fenton first reported that alcohols are oxidized in the presence of H<sub>2</sub>O<sub>2</sub> and  $Fe(H_2O)_6^{2^+.10}$  The Fenton system is an attractive catalytic oxidation treatment for effective and exhaustive degradation because of its low cost, lack of toxic reagents (it employs Fe<sup>2+</sup> and  $H_2O_2$ ), circumvention of mass transfer limitations due to its homogeneous catalytic nature, and simplicity.11 However, homogeneous Fenton processes also present certain disadvantages, including a requirement for strong acidity (pH = 3.0), and the formation of a considerable amount of ferric hydroxide sludge during treatment, which requires further separation and disposal.<sup>12-15</sup> Heterogeneous Fenton-like systems using Fe<sub>3</sub>O<sub>4</sub> magnetic nanoparticles (MNPs) have been recently developed to overcome problems associated with homogeneous systems. The iron spinel Fe<sub>3</sub>O<sub>4</sub> (magnetite) is known for high catalytic activity because it contains Fe<sup>2+</sup>, which is necessary for the initiation of the Fenton reaction, according to the classical Haber-Weiss mechanism. The octahedral configuration of ions in magnetite confers additional advantages as these sites can easily accommodate both Fe<sup>2+</sup> or Fe<sup>3+</sup>, allowing the iron species to be reversibly oxidized and reduced without inducing structural changes.16 However, while Fe<sub>3</sub>O<sub>4</sub> MNPs can be easily separated from the reaction medium under a magnetic field, they also

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tend to aggregate into larger clusters as a result of anisotropic dipolar attractions, which inhibits dispersibility and other properties.<sup>17,18</sup>

Carbon nanotubes (CNT) are a new class of small, adsorbent molecules that exhibit large specific surface areas, with hollow and layered structures. These CNT represent a class of adsorbents that are important for their potential ability to remove many kinds of organic compounds.19 Studies have demonstrated that CNT act as good supports for Fe<sub>3</sub>O<sub>4</sub> MNPs, exhibiting high specific surface areas and low diffusion resistance. Studies have also reported the development of iron oxide/ carbon nanostructures.<sup>20-23</sup> For example, Deng et al.<sup>23</sup> synthesized Fe<sub>3</sub>O<sub>4</sub>/MWCNT magnetic nanocomposites and used them as a Fenton-like catalyst to decompose acid orange II. These composites displayed higher activity (90% degradation) than Fe<sub>3</sub>O<sub>4</sub> nanocomposites (38% degradation). However, the use of Fe<sub>3</sub>O<sub>4</sub>/MWCNT magnetic nanocomposites in a heterogeneous Fenton system to catalyze TBBPA degradation has not yet been reported.

In order to implement effective TBBPA degradation, we report in this work the preparation of  $Fe_3O_4/MWCNT$  using a simple solvo-thermal method. This new magnetic nanocomposite exhibits improved features, such as improved monodispersion and size control of the  $Fe_3O_4$  nanoparticles on MWCNT, compared to our previous work.<sup>24,25</sup> Moreover, this new  $Fe_3O_4/MWCNT$  exhibits high specific surface area and excellent stability, and can be used in a heterogeneous Fentonlike system for TBBPA degradation. Potential mechanisms of the degradation were proposed following analysis by gas chromatography-mass spectrometry (GC-MS).

# 2. Experimental

## 2.1. Chemicals and materials

MWCNT (diameter, 10–20 nm) were purchased from Chengdu Organic Chemical Co. Ltd, Chinese Academy of Sciences (AR, Chengdu, China). TBBPA was obtained from Xilong Chemical Co. Ltd (AR, Guangzhou, China). Fe(acac)<sub>3</sub> (purity, 99.9%) was purchased from Sigma-Aldrich (AR, United Kingdom). *N*-Octyl-amine and *n*-octyl alcohol were purchased from Sinopharm Chemical Reagent Co. Ltd (AR, Shanghai, China). The  $H_2O_2$  was purchased from Guangfu Chemical Co. Ltd (30%, Tianjin, China).

## 2.2. Preparation of Fe<sub>3</sub>O<sub>4</sub>/MWCNT

The preparation of  $Fe_3O_4/MWCNT$  involved a modified solvothermal method in which  $Fe(acac)_3$  acted as the iron source, *n*-octylamine acted as the reductant, and *n*-octanol was used as the solvent.<sup>26,27</sup> In a typical experiment,  $Fe(acac)_3$  (0.7416 g) and different weights of MWCNT (1.4832 g, 0.7416 g, or 0.3708 g) were mixed with 4 mL *n*-octylamine and 12 mL *n*-octanol. Following ultrasonic dispersion for 1 min (KQ-100, 40 kHz, 100 W), the mixture solution (16 mL) was heated to 110 °C for 1 h, under a flow of nitrogen, to remove trace oxygen and moisture. The pretreatment solution was then transferred to a 50 mL Teflon-lined stainless steel autoclave and heated to 240 °C for 2

h. After cooling to room temperature, the residual solvent was removed by magnetic separation, and the black material was washed thoroughly with ethanol for 12 h in a Soxhlet extractor. Finally, the composite material was dried in a vacuum oven at 30 °C. This process (Scheme 1) produced composites of Fe<sub>3</sub>O<sub>4</sub>/ MWCNT in the following ratios: 1:2, 1:1 and 2:1.

#### 2.3. Instrumentation

The morphology of prepared Fe<sub>3</sub>O<sub>4</sub>/MWCNT was characterized using a transmission electron microscope (TEM, Tecnai  $G^2$ F30). Powder X-ray diffraction (XRD, Rigaku D/MAX-2400 X-ray diffractometer with Ni-filtered Cu Ka radiation) was used to qualitatively assess the structure of the Fe<sub>3</sub>O<sub>4</sub>/MWCNT. Fourier transform infrared spectroscopy (FT-IR, American Nicolet Corp. Model 170-SX, using the KBr pellet technique.) and X-ray photoelectron spectroscopy (XPS), were used to verify the composition of the Fe<sub>3</sub>O<sub>4</sub>/MWCNT. The N<sub>2</sub> adsorptiondesorption isotherm was measured at liquid nitrogen temperature (76 K) using a Micromeritics ASAP 2010M instrument. The specific surface area was calculated using the Brunauer-Emmett-Teller (BET) method. Magnetic properties were characterized by vibrating sample magnetometry (VSM, LAKE-SHORE-7304) at room temperature. The pH of the solutions was determined using a pH meter (HI 9025, HANNA instruments, Romania).

The concentrations of TBBPA were analyzed by HPLC (LC-10AVP Plus, Shimadzu, Japan), equipped with a C-18 column under the following conditions: the mobile phase was an 80 : 20 (v/v) mixture of methanol and water; flow rate, 1.0 mL min<sup>-1</sup>; detection wavelength, 230 nm; column temperature, 30 °C; and retention time, 9.253 min.

Chemical analyses of the intermediates of TBBPA Fenton degradation were carried out using a GC-MS system (QP2010 Plus, Shimadzu, Japan) equipped with a fused silica capillary column (HP-5MS; length = 30 m; i.d. = 0.25 mm; film thickness = 0.25  $\mu$ m). The column temperature was programmed as follows: 3 min at 80 °C; a temperature increase of 3 °C min<sup>-1</sup> up to 300 °C; and 30 min at 300 °C. The helium gas flow rate was 1.0 mL min<sup>-1</sup>, and the sample size was 2  $\mu$ L.

## 2.4. Procedures and analysis

The effects of correlating factors, including pH,  $H_2O_2$  concentration, quality ratio of Fe(acac)<sub>3</sub> and MWCNT, and Fe<sub>3</sub>O<sub>4</sub>/MWCNT concentration, were investigated through batch experiments. The solution pH was adjusted using a minute quantity of 0.1 mol L<sup>-1</sup> HCl and/or 0.1 mol L<sup>-1</sup> NaOH. Stock solutions of 100 mg L<sup>-1</sup> of standardized TBBPA and 180 mmol L<sup>-1</sup> of H<sub>2</sub>O<sub>2</sub> were prepared. Experimental solutions of the desired concentrations were obtained by dilution. The initial



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Fig. 1 TEM images of 1 : 2 Fe<sub>3</sub>O<sub>4</sub>/MWCNT (a and b), 1 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT (c and d) and 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT (e and f).

concentrations of TBBPA test solutions were 10 mg L<sup>-1</sup> for all experiments. The appropriate amounts of Fe<sub>3</sub>O<sub>4</sub>/MWCNT and 10 mL TBBPA solution were added to the reactor, and after thorough mixing, 0.5 mL aliquots of H<sub>2</sub>O<sub>2</sub> solution were added every hour. Samples were then transferred to a constant temperature oscillator (150 rpm, 30 °C). After an appropriate time, samples were removed to measure the concentration of TBBPA.

Table 1 The data of surface area, pore volume and pore size for different ratio of  $Fe_3O_4/MWCNT$  and pure MWCNT.

Sample	${S_{ m BET} \over ({ m m}^2~{ m g}^{-1})}$	Pore volume $(cm^3 g^{-1})$	Pore size (nm)
2 : 1 Fe <sub>3</sub> O <sub>4</sub> /MWCNT 1 : 1 Fe <sub>3</sub> O <sub>4</sub> /MWCNT 1 : 2 Fe <sub>3</sub> O <sub>4</sub> /MWCNT	145 164 174	0.6911 0.6570 0.6982	19.09 16.07 16.08
MWCNT	224	1.1771	26.07

The residue rate of TBBPA (R, %) was calculated using eqn (1):



Fig. 2 XPS spectra of 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT. (a) Wide scan, (b) O 1s spectrum, (c) Fe 2p spectrum, (d) C 1s spectrum.



Fig. 3 Magnetic hysteresis curves for different ratios of Fe $_3O_4/$  MWCNT and Fe $_3O_4.$ 



Fig. 4 Effect of quality ratio between Fe(acac)<sub>3</sub> and MWCNT on the degradation of TBBPA. Reaction conditions: temperature 303 K; 10 mg L<sup>-1</sup> TBBPA; 5.0 mg Fe<sub>3</sub>O<sub>4</sub>/MWCNT; 100 mmol L<sup>-1</sup> H<sub>2</sub>O<sub>2</sub>; pH = 5.0.



Fig. 5 Degradation and adsorption performance of TBBPA over time under different conditions. Reaction conditions: temperature 303 K; 10 mg L<sup>-1</sup> TBBPA; 5.0 mg Fe<sub>3</sub>O<sub>4</sub>/MWCNT, Fe<sub>3</sub>O<sub>4</sub> or MWCNT; 100 mmol L<sup>-1</sup> H<sub>2</sub>O<sub>2</sub>; pH = 5.0.

$$R = \frac{C_t}{C_0} \times 100\% \tag{1}$$

where  $C_0$  and  $C_t$  are, respectively, the initial and remnant concentrations of TBBPA.

## 3. Results and discussion

#### 3.1. Characterization of Fe<sub>3</sub>O<sub>4</sub>/MWCNT

Samples containing  $Fe_3O_4$  and MWCNT at ratios of 1:2, 1:1, and 2:1 were observed by TEM under different magnifications (Fig. 1). Uniform, homogeneous, and non-agglomerated Fe<sub>3</sub>O<sub>4</sub> MNPs were found decorated onto the surfaces of the MWCNT. Individual Fe<sub>3</sub>O<sub>4</sub> MNPs or MWCNT were not observed, indicating that the preparation method was effective. The use of different ratios of Fe(acac)<sub>3</sub> and MWCNT achieved different coverage densities of Fe<sub>3</sub>O<sub>4</sub> on the MWCNT. The lowest iron content led to relatively low coverage density by small Fe<sub>3</sub>O<sub>4</sub> particles (average diameter 4.19 nm; Fig. 1(a and b)). Increasing the iron content allowed for larger Fe<sub>3</sub>O<sub>4</sub> particle growth, so the 1:1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT sample exhibited 5.72 nm Fe<sub>3</sub>O<sub>4</sub> particles (Fig. 1(c and d)), while a relatively high coverage density of 6.43 nm Fe<sub>3</sub>O<sub>4</sub> particles was achieved in the sample with the highest iron content (Fig. 1(e and f)). The increasing  $Fe(acac)_3$  concentration resulted in higher concentrations of Fe<sub>3</sub>O<sub>4</sub>, which facilitated the thermodynamically stable growth of larger particles.

Fig. S1<sup>†</sup> shows the XRD patterns of both the pure Fe<sub>3</sub>O<sub>4</sub> and the composite. The composite exhibited a different peak at  $2\theta =$ 25.78°, which can be indexed to the (002) reflection of the graphite structure of the MWCNT.<sup>28</sup> The other peaks represent the pure Fe<sub>3</sub>O<sub>4</sub> nanoparticles, as the signals at 30.05°, 35.12°, 43.50°, 54.14°, and 63.01°, are respectively consistent with standard data from the (220), (311), (400), (422), (511), and (440) reflections of the cubic spinel crystal structure of bulk magnetite (JCPDS file no. 19-0629).29 No obvious peaks from other phases were observed. The main Fe<sub>3</sub>O<sub>4</sub> peaks appeared broadened, indicating a very small crystalline portion of the Fe<sub>3</sub>O<sub>4</sub> MNPs. According to the full width at half maximum (FWHM) of (311) reflections, the average sizes of the  $Fe_3O_4$  nanocrystalline particles from pure Fe<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>O<sub>4</sub>/MWCNT were calculated to be 5.7 nm and 5.9 nm based on the Debye-Scherrer formula, respectively. The almost similar crystallite of bare and decorated Fe<sub>3</sub>O<sub>4</sub> suggests that MWCNT can be better support for the growth of metal oxide nanoparticles, without apparent agglomeration.

We observed a signal at 582 cm<sup>-1</sup> in the FT-IR spectrum related to the Fe–O–Fe stretching vibration of Fe<sub>3</sub>O<sub>4</sub><sup>30</sup> and a strong adsorption at 3438 cm<sup>-1</sup> assigned to O–H stretching of multiwall CNT, which is consistent with previous research indicating a large number of carboxyl and hydroxyl groups on the surface of multiwall CNT (Fig. S2†).<sup>31</sup> Results of the FT-IR indicated that the Fe<sub>3</sub>O<sub>4</sub> MNPs were loaded successfully onto the MWCNT.

Samples were also analyzed by XPS (Fig. 2). The wide scan spectrum revealed photoelectron lines at binding energies of approximately 285, 528, and 711 eV (Fig. 2(a)), which were

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**Fig. 6** Catalytic activity of  $2:1 \text{Fe}_3\text{O}_4$ /MWCNT for different cycling numbers (a); magnetic hysteresis curves for  $2:1 \text{Fe}_3\text{O}_4$ /MWCNT and  $\text{Fe}_3\text{O}_4$  after recycling 10 times (b); XPS spectrum of Fe on  $2:1 \text{Fe}_3\text{O}_4$ /MWCNT before (c) and after (d) degradation of TBBPA; XPS spectrum of Fe on  $\text{Fe}_3\text{O}_4$  before (e) and after (f) degradation of TBBPA. Reaction conditions in each cycle: temperature 303 K; 10 mg L<sup>-1</sup> TBBPA; 5.0 mg  $2:1 \text{Fe}_3\text{O}_4$ /MWCNT and  $\text{Fe}_3\text{O}_4$ ; 100 mmol L<sup>-1</sup> H<sub>2</sub>O<sub>2</sub>; pH = 5.0.

attributed to C 1s, O 1s, and Fe 2p orbitals, respectively. The O 1s spectrum indicates the presence of O 1s (528 eV) from the Fe<sub>3</sub>O<sub>4</sub> (Fig. 2(b)).<sup>32</sup> Fe 2p 1/2 and Fe 2p 3/2 peaks were observed at 710 and 725 eV (Fig. 2(c)), further confirming that the oxide in the sample was Fe<sub>3</sub>O<sub>4</sub>.<sup>33</sup> The electron binding energy of C 1s at 285 eV was attributed to adsorbed carbon in the composites from the MWCNT (Fig. 2(d)).<sup>34</sup>

Nitrogen adsorption-desorption isotherms and pore size distributions were measured for all three samples and pure MWCNT (Fig. S3†). The BET method and Barrett-Joyner-Halenda (BJH) models were used to calculate specific surface area and porosity, respectively. The surface areas, pore volumes, and pore sizes of the different samples are summarized in Table 1. The specific surface area of pure MWCNT was 224 m<sup>2</sup> g<sup>-1</sup>, and this value decreased with increasing iron content. The high specific surface areas shown by the magnetic CNT (145–174 m<sup>2</sup> g<sup>-1</sup>) were greater than those of similar materials synthesized by other methods, which did not exceed 120 m<sup>2</sup> g<sup>-1</sup>.<sup>35,36</sup> Increases in specific surface area resulting from the present solvo-chemical route may be particularly beneficial to

the adsorption and degradation of organic pollutants. This observed synergy is believed to result from the adsorptive properties of the support, which increase the rate of substrate degradation. Similar effects were reported by Hu *et al.*<sup>37</sup> who determined that the degradation of pollutants, such as  $17\alpha$ -methyltestosterone, could be accelerated by their adsorption onto multi-walled carbon nanotubes.

The magnetic behaviors of the different  $Fe_3O_4/MWCNT$  samples and pure  $Fe_3O_4$  exhibited typical S-type hysteresis loops with no residual magnetism or coercivity (Fig. 3), indicating that the nanoparticles were superparamagnetic. Saturation magnetization for three samples with increasing iron content increased by 6.91, 12.56, and 18.98 emu g<sup>-1</sup>, which was attributed to the strong magnetic properties of the  $Fe_3O_4$ . Although the composites exhibited lower saturation magnetization than pure  $Fe_3O_4$  (73.29 emu g<sup>-1</sup>), they could still be easily separated from solution using an external magnetic field, which is a useful method for recycling biodegradable materials and reducing the cost of wastewater treatment.



#### 3.2. Optimization of experimental conditions

**3.2.1.** Effects of pH. Fenton reactions are very strongly affected by pH. Reactions in a traditional Fenton system proceed smoothly only at pH  $3.0.^{38}$  In this study, the degradation of TBBPA was examined at pH 2.0, 3.0, 5.0, 7.0, 9.0, and 11.0 (Fig. S4†). Degradation trends of TBBPA with changing pH were similar for both the composites and the pure Fe<sub>3</sub>O<sub>4</sub>, with optimal values identified at 5.0 and 3.0, respectively. It is worth mentioning that less than 7.5% of the TBBPA remained at pH < 7.0, indicating that TBBPA was almost completely degraded at or near neutral pH in our Fenton system, and the wide range of conditions under which TBBPA could be degraded demonstrated the efficiency of the composite catalyst.

Two kinds of mechanisms have been proposed to explain the strong oxidization associated with the Fenton reagent. The first mechanism involves the formation of high-valent iron–oxo intermediates, such as  $Fe=O^{2+}$ , as reported by Bray and Gorin in 1932, and as illustrated by eqn (2) and (3) below:<sup>39</sup>

$$Fe^{2+} + H_2O_2 \rightarrow FeO^{2+} + H_2O$$
 (2)

$$FeO^{2+} + H_2O_2 \rightarrow Fe^{2+} + H_2O + O_2$$
 (3)

A related study by Churchill *et al.*<sup>40</sup> reported the synthesis of a new molecular probe capable of detecting  $Fe^{3+}$  *via* fluorescence enhancement, which would allow for discrimination between  $Fe^{2+}$  and  $Fe^{3+}$  during the Fenton reaction. Results of that study confirmed the formation of a ferryl group (FeO<sup>2+</sup>) as an oxidative intermediate *via* DFT.

The second mechanism is the Haber–Weiss mechanism, which involves the generation of  $\cdot$ OH from H<sub>2</sub>O<sub>2</sub> as a key step in the degradation process,<sup>41</sup> as summarized in eqn (4) and (5).

$$\mathrm{Fe}^{2+} + \mathrm{H}_2\mathrm{O}_2 \rightarrow \mathrm{Fe}^{3+} + \mathrm{OH}^- + \cdot \mathrm{OH}$$
(4)

$$\mathrm{Fe}^{3+} + \mathrm{H}_2\mathrm{O}_2 \to \mathrm{Fe}^{2+} + \mathrm{H}^+ + \cdot\mathrm{OOH}$$
 (5)

While no experimental methods are currently available to distinguish between these two kinds of mechanisms, we selected the latter method for our analysis. At low pH (<3.0)  $H_2O_2$  can form a stable oxonium ion  $(H_3O_2^+)$ , which enhances the scavenging effect of the  $\cdot$ OH,<sup>42,43</sup> and  $\cdot$ OH exhibits a higher oxidation capacity under acidic conditions, thereby inhibiting the decomposition of  $H_2O_2$  into  $H_2O$  and  $O_2$ .<sup>44</sup> Degradation is also poor under alkali conditions, as this affects the generation of  $\cdot$ OH, and produces hydroxide, which inhibits the catalytic ability of iron.<sup>45,46</sup> Preliminary studies in our laboratory indicated that optimal degradation occurred at pH 5.0, and this pH was maintained for all subsequent degradation experiments.

**3.2.2. Effects of H\_2O\_2 concentration.** Increasing  $H_2O_2$  concentration was found to increase TBBPA degradation: TBBPA residue was reduced from 9.7 to 5.3% as  $H_2O_2$  concentration increased from 27 to 54 mmol  $L^{-1}$  (Fig. S5†). TBBPA degradation is also directly related to the concentration of  $\cdot$ OH produced by the catalytic decomposition of  $H_2O_2$ ; therefore, better decomposition is expected when more  $H_2O_2$  is available to produce  $\cdot$ OH. However, full degradation of TBBPA was achieved at the lowest tested concentration, and significant improvements were not affected by increased  $H_2O_2$  concentration. The lack of further improvement at higher concentrations may have been due to hydroxyl radicals scavenging the  $H_2O_2$  (eqn (6) and (7)) and recombining with each other (eqn (8)),<sup>47,48</sup> which may then reduce the rate of degradation.<sup>49</sup>

$$OH + H_2O_2 \rightarrow HO_2 \cdot + H_2O \tag{6}$$

$$\cdot OH + HO_2 \cdot \rightarrow O_2 + H_2O \tag{7}$$

$$OH + \cdot OH \rightarrow H_2O_2$$
 (8)

All TBBPA degradation experiments were subsequently conducted using 27 mmol  $L^{-1}$  H<sub>2</sub>O<sub>2</sub>, as this concentration produced the highest degradation.

**3.2.3.** Effects of catalyst loading. TBBPA degradation was investigated at different loadings (0.0, 0.25, 0.5, 1.0, 2.0, and 4.0 g  $L^{-1}$ ) as part of the 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT catalyst (Fig. S6†). TBBPA residue rates dropped from 96.3 to 3.2% as the concentration of the composite increased from 0.0 to 4.0 g  $L^{-1}$ . This was due to the increased number of active sites on the oxide surface, which accelerated the decomposition of H<sub>2</sub>O<sub>2</sub> and the dissolution of iron to produce more  $\cdot$ OH.<sup>37,50</sup> A sharp

decrease in TBBPA degradation was observed when the concentration of 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT was lower than 0.5 g L<sup>-1</sup>, while only slight changes were observed when the concentration of 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT exceeded 0.5 g L<sup>-1</sup>. However, at 0.5 g L<sup>-1</sup>, TBBPA could be removed almost completely, so 0.5 g L<sup>-1</sup> of 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT was used in subsequent experiments.

**3.2.4.** Effects of iron content. The different  $Fe_3O_4/MWCNT$  samples were prepared at different quality ratios of  $Fe(acac)_3$  and MWCNT (1 : 2, 1 : 1, and 2 : 1), and their abilities to degrade TBBPA were compared (Fig. 4). Improved degradation was observed with increasing iron content, as the three samples exhibited decreasing residue rates of 23.26, 11.13, and 4.65%, respectively. The increased activity of the composites, resulting from increased iron content, was attributed to an increase in the number of active sites, which are visible in the TEM (Fig. 1). This reaction was considered a pseudo-first-order reaction, with the concentration  $C_t$  of TBBPA at reaction time t being described as follows:<sup>51</sup>

$$C_t = C_0 \exp(-kt) \tag{9}$$

where  $C_0$  was the initial concentration of TBBPA, and k was the pseudo first-order rate constant. Logarithmic plots of the concentration of TBBPA as a function of degradation time appear as well-behaved straight lines ( $R^2 > 0.98$ ), indicating that the degradation reaction was pseudo-first-order. The rate constant k was calculated from the slope of the line, while values of 0.0061, 0.0098, and 0.0132 min<sup>-1</sup> were calculated for the three samples by increasing iron content, respectively. Each of these values was greater than the  $1.8 \times 10^{-4}$  min<sup>-1</sup> reported for a Fe<sub>2.02</sub>Ti<sub>0.98</sub>O<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> system for the degradation of TBBPA.

# 3.3. TBBPA degradation experiments by heterogeneous Fenton reaction

The catalytic degradation efficiencies of TBBPA by  $2:1 \text{ Fe}_3\text{O}_4/$ MWCNT and Fe<sub>3</sub>O<sub>4</sub> were evaluated under optimal conditions. In order to differentiate between degradation and adsorption, adsorption tests were also conducted using the three kinds of materials (2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT, pure Fe<sub>3</sub>O<sub>4</sub> and pure MWCNT). As seen in Fig. 5, the adsorption of TBBPA was almost negligible in the presence of pure Fe<sub>3</sub>O<sub>4</sub>, which might have been due to its low surface areas. The increased surfaces areas of both 2:1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT and pure MWCNT resulted in predictable increases in adsorption performance, with TBBPA residual rates of 52.34 and 33.55%, respectively. However, when H<sub>2</sub>O<sub>2</sub> was added, The TBBPA residual rate for 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT dropped to 4.87%, while the TBBPA rate when pure  $Fe_3O_4$  was used as a catalyst for TBBPA degradation was 60.56%. These comparisons were made based on equal weights of the catalysts. Results of these experiments indicated that the degradation efficiency of 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT was two times higher than that of Fe<sub>3</sub>O<sub>4</sub>, and that approximately twice as much TBBPA was degraded as adsorbed. This significant activity enhancement can be attributed to homogeneous dispersion of the Fe<sub>3</sub>O<sub>4</sub> nanoparticles, which appears to increase the number of active sites for substrate access.

#### 3.4. Stability of Fe<sub>3</sub>O<sub>4</sub>/MWCNT

The stability and recyclability of both 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT and pure Fe<sub>3</sub>O<sub>4</sub> were evaluated via their successive use in TBBPA degradation (Fig. 6). After 10 cycles, the TBBPA residual rate remained at 6.8% (Fig. 6(a)), and the saturation magnetization of composite after 10 cycles was 16.93 emu  $g^{-1}$  (Fig. 6(b)), which represented only a 1.1% decrease from its original value. By contrast, the saturation magnetization of pure Fe<sub>3</sub>O<sub>4</sub> after 10 cycles was 61.69 emu  $g^{-1}$  (Fig. 6(b)), which represented a 15.8% decrease from its original value. To further demonstrate the stability of the structures, XPS was used to analyze the catalysts before and after the Fenton reaction. The details of the Fe 2p peaks (Fe 2p 1/2 and Fe 2p 3/2) of the 2 : 1 Fe<sub>3</sub>O<sub>4</sub>/MWCNT and pure Fe<sub>3</sub>O<sub>4</sub> before and after their use during TBBPA degradation are presented in Fig. 6(c-f) and Table S1.<sup>†</sup> The Fe 2p 1/2 peak for  $Fe_3O_4$  was deconvoluted into the  $Fe^{3+}$  and  $Fe^{2+}$  peaks. Before use, the corresponding binding energy values were 712.00 eV and 711.00 eV, respectively (Fig. 6(c)), and these values did not change significantly after 10 cycles of use for TBBPA degradation (711.80 eV and 710.90 eV: Fig. 6(d)). Calculation of the peak areas indicated that 67.6% of the total iron surface atoms were Fe<sup>3+</sup>, while 32.4% were in the Fe<sup>2+</sup> state, which was consistent with the Fe<sub>3</sub>O<sub>4</sub> crystal structure. For samples evaluated after 10 cycles of TBBPA degradation, the concentration of Fe<sup>3+</sup> on the surface increased to 70.0%, while Fe<sup>2+</sup> decreased to 30.0%, which indicated that some of the Fe<sup>2+</sup> on the outermost layer of the catalyst was oxidized into Fe<sup>3+</sup> during the Fenton reaction. Meanwhile, we used the same methods to analyze the pure Fe<sub>3</sub>O<sub>4</sub>. Before use, the corresponding binding energy values were 711.91 eV and 710.62 eV, respectively (Fig. 6(e)). After 10 cycles of use for TBBPA degradation, these values were 712.20 eV and 711.05 eV (Fig. 6(f)). Fe<sup>2+</sup> surface concentration was 32.7% in the pure Fe<sub>3</sub>O<sub>4</sub> before use, but only 27.8% after use. It is well known that the oxidation of the ferrous iron by  $H_2O_2$  is much faster than the reduction of the ferric iron by H<sub>2</sub>O<sub>2</sub>. Thus, in order to speed up the redox cycle between ferrous and ferric species, it should improve the reduction of the ferric iron by H<sub>2</sub>O<sub>2</sub>.<sup>23</sup> Obviously, the reduction of the ferric iron in the Fenton system use Fe<sub>3</sub>O<sub>4</sub>/MWCNT was more efficient than use pure Fe<sub>3</sub>O<sub>4</sub>. Collectively, these results suggested excellent stability and durability of the composite.

#### 3.5. Reaction mechanism

The mechanism of this Fenton system was investigated *via* GC-MS analysis of the products of degradation after 4 h. Five main intermediate products were detected, and their likely molecular structures and fragment ion peaks are summarized in Table S2.<sup>†</sup> A proposed mechanism associated with this reaction is presented in Scheme 2.<sup>53</sup> In this scheme, path (a) illustrates the conversion of  $H_2O_2$  to  $OH^-$  and  $\cdot OH$  in the presence of  $Fe^{2+}$ , which was generated on the surface of  $Fe_3O_4$  MNPs. Path (b) illustrates the transformation of  $Fe^{3+}$  on the surface of  $Fe_3O_4$  MNPs to  $Fe^{2+}$ . In subsequent pathway, the TBBPA was oxidized into intermediates 1–5 by the activated  $\cdot OH$ . Product 1 was identified as bisphenol A, which resulted from the oxidation of TBBPA by  $\cdot OH$  and the loss of its Br

atoms.<sup>52</sup> The presence of product 2 likely resulted from the reaction of  $\cdot$ OH with product 1. Homolytic cleavage of the C–C bond between the quaternary carbon and the aromatic ring in TBBPA was responsible for the creation of product 3. Phenol may have resulted from the oxidation of product 3 by  $\cdot$ OH. Additionally, the phenol might then have been oxidized into product 4, which was further oxidized (following ring opening) to generate open chain alcohols, such as product 5. All the intermediates could eventually be mineralized into H<sub>2</sub>O and CO<sub>2</sub>.<sup>54</sup> The proposed mechanism suggests that the composite exhibits good activity and high specific surface area, which provides a great activated surface for the Fenton system,<sup>22,55</sup> and that the Fe<sub>3</sub>O<sub>4</sub> MNPs may provide sufficient electrons to facilitate the degradation reactions.<sup>22,50</sup>

# 4. Conclusions

In our work, Fe<sub>3</sub>O<sub>4</sub>/MWCNT catalysts were prepared using a modified solvothermal method. Shape-controlled and monodisperse Fe<sub>3</sub>O<sub>4</sub> nanoparticles were found to be uniformly dispersed on the MWCNT. The resulting high activity was attributed to the Fe<sub>3</sub>O<sub>4</sub> nanoparticles' narrow size distribution, and good dispersion on MWCNT. The specific surface area exhibited by the composites was 145 m<sup>2</sup> g<sup>-1</sup>, which increased the number of available active sites for MWCNT access, and improved degradation. The composites were then used as heterogeneous Fenton reagents to catalyze the degradation of TBBPA by H<sub>2</sub>O<sub>2</sub>. Degradation was optimized at pH 5.0 using 0.5 g L<sup>-1</sup> catalyst and 27 mmol L<sup>-1</sup> H<sub>2</sub>O<sub>2</sub>. The detailed XPS studies of composite and pure Fe<sub>3</sub>O<sub>4</sub> indicated that the composite was stable and retained strong activity after 10 cycles of reuse. The ability of the catalyst to degrade TBBPA at near neutral pH, and it's excellent stability and activity, suggest that it may have many useful applications. Careful analysis of the main intermediate products for this reaction led to a proposed mechanism of TBBPA degradation, which suggested multiple pathways of action on TBBPA by hydroxyl radicals.

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