

## A facile approach for the synthesis of monolithic hierarchical porous carbons – high performance materials for amine based CO<sub>2</sub> capture and supercapacitor electrode†

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Luis Estevez,<sup>‡a</sup> Rubal Dua,<sup>‡b</sup> Nidhi Bhandari,<sup>a</sup> Anirudh Ramanujapuram,<sup>a</sup> Peng Wang<sup>\*b</sup> and Emmanuel P. Giannelis<sup>\*a</sup>

An ice templating coupled with hard templating and physical activation approach is reported for the synthesis of hierarchically porous carbon monoliths with tunable porosities across all three length scales (macro- meso- and micro), with ultrahigh specific pore volumes  $\sim 11.4 \text{ cm}^3 \text{ g}^{-1}$ . The materials function well as amine impregnated supports for CO<sub>2</sub> capture and as supercapacitor electrodes.

Recently, hierarchical porous carbons (HPCs) possessing well-defined macropores and interconnected meso- and micropores, have attracted much attention.<sup>1–18</sup> HPCs can combine in one system: improved mass transport facilitated by the macropores and high surface area and pore volume from micro-/mesopores.<sup>19–22</sup> Such hierarchically porous carbons provide better accessibility and active sites for several energy and environmental applications including electrode materials for batteries,<sup>9,21</sup> supercapacitors,<sup>13,19,20,23,24</sup> fuel cells,<sup>25,26</sup> and capacitive deionization,<sup>27,28</sup> as well as sorbents for CO<sub>2</sub> capture.<sup>6</sup>

A large number of techniques have been explored for the synthesis of HPCs.<sup>29,30</sup> In general, most of the techniques for producing carbons combining macro- and mesoporosity are based on a dual templating strategy, where two templates with dimensions at different length scales are combined to generate the multimodal pores. These techniques either involve two hard templates<sup>31,32</sup> or a combination of hard and soft templates.<sup>33,34</sup> Removal of the templates, either through decomposition or etching leaves behind a porous scaffold. Other techniques involve template replication of hierarchical inorganic materials,<sup>35,36</sup> with hierarchical silica being the most commonly used

### Broader context

The move from a fossil fuel based energy economy to a renewable energy based economy is currently underway. In order to realize this goal, it is vital to mitigate the environmental affects of the current fossil fuel infrastructure, while advancing the effectiveness of renewable energy alternatives. Advances in novel hierarchical porous carbon (HPC) materials with high surface area and pore volume can address both goals. By providing a scaffold support for amine impregnation, HPCs can be used to fabricate effective CO<sub>2</sub> capture materials; while the open, vascular structure of HPCs can be used to produce effective EDLC supercapacitors for energy storage and high power output. In this work we developed a facile and scalable synthesis technique for producing a family of highly tunable HPC materials. The HPCs showed an excellent capability to be used as effective EDLC electrodes with a maximum charge storage capability of 6 W h kg<sup>-1</sup> and a maximum power density of 14 kW kg<sup>-1</sup>; and an exceptional ability when used as scaffolds for amine based CO<sub>2</sub> capture, achieving a maximum CO<sub>2</sub> capacity of 4.2 mmol g<sup>-1</sup>.

template. The sol–gel method is another widely used technique for the production of hierarchical carbon, commonly termed as either carbon aerogels<sup>29,37</sup> or carbon cryogels.<sup>38,39</sup> Ice templating has been also explored for assembling micropore–mesopore dominated carbon materials, such as CNTs, into 3D interconnected hierarchical carbon materials.<sup>26,40</sup>

A major challenge to date has been the development of HPCs, which can exhibit high surface areas, pore volumes and porosities at all three different length scales: macro-, meso-, and micro, in a simple material platform. Additional challenges with the synthesis techniques include the requirement to synthesize porous inorganic materials or special nanoparticles as hard templates, which involve multiple steps and are thus time consuming and costly. Furthermore, most of the soft templates used are based on surfactants and block-copolymers, which are rather expensive and non-renewable.<sup>30</sup> Moreover, the size of the mesopores can also be difficult to tune because of aggregation of the nanoparticles in the polymerizing carbon precursor matrix.<sup>41</sup> In addition, techniques like sol–gel suffer from the critical drawback associated with the long synthesis

<sup>a</sup>Department of Materials Science and Engineering, Cornell University, Ithaca, NY 14853, USA. E-mail: [epg2@cornell.edu](mailto:epg2@cornell.edu)

<sup>b</sup>Water Desalination and Reuse Center, Biological and Environmental Science and Engineering Division, King Abdullah University of Science and Technology (KAUST), Thuwal 23955-6900, Saudi Arabia. E-mail: [peng.wang@kaust.edu.sa](mailto:peng.wang@kaust.edu.sa)

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‡ Authors contributed equally.

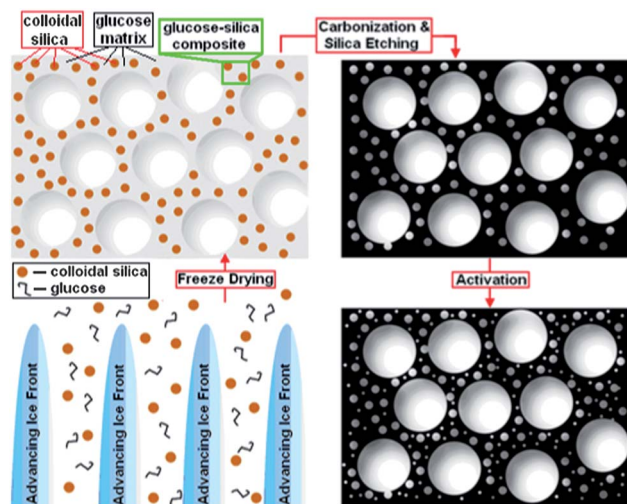


period required for gelation, solvent exchange and supercritical drying in the case of aerogels.<sup>29</sup>

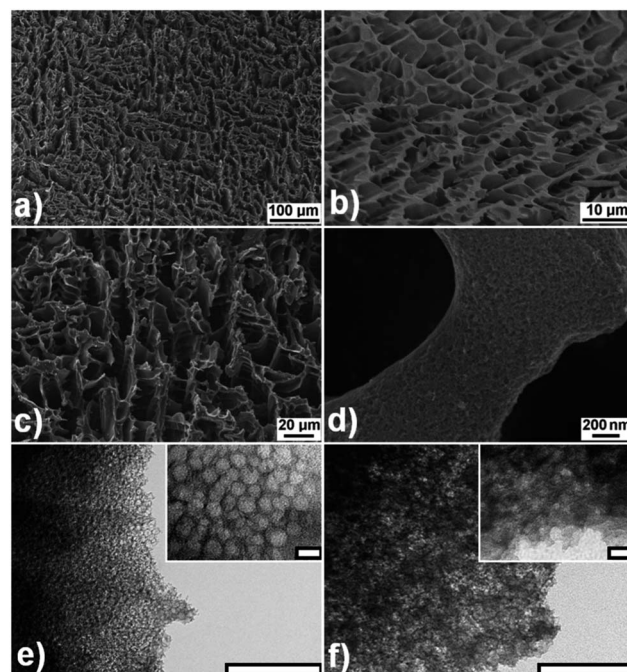
Here we demonstrate a novel strategy to synthesize HPCs with high surface areas, large pore volumes (up to 2096 m<sup>2</sup> g<sup>-1</sup> and 11.4 cm<sup>3</sup> g<sup>-1</sup>, respectively), and more importantly, tunable micro/meso/macro porosities. Our approach is based on combining, ice templating alongside a hard template (colloidal silica), and physical activation for generating interconnected macro-, meso-, and microporosity, respectively. We also demonstrate that the newly developed HPCs are promising candidates for amine supported sorbents for CO<sub>2</sub> capture and as electrode materials for an electric double-layer capacitor (EDLC). This new, simple, and inexpensive technique provides a suitable platform for producing state of the art HPCs for these applications and beyond. In addition, because of their easy tunability, the new HPCs provide excellent model systems to understand the effect of different types of porosity (*e.g.* macro, meso and micro) on their performance in a series of applications.

Ice templating<sup>42,43</sup> has been used previously to synthesize macroporous<sup>44</sup> and even hierarchical materials<sup>45,46</sup> due to its simplicity and versatility. However this is the first time ice-templating has been used to synthesize HPCs with tunable porosity by combining it with hard templating and physical activation. Our approach offers several key additional advantages: (1) the range, size and extent of porosity can be easily controlled. For example, the distribution of the mesopores and the extent of mesoporosity can be simply tuned by either using silica of different size or varying the silica to carbon precursor weight ratio. The excellent control of the mesopore size distribution (*vide infra*) alleviates the need of using costly surfactants,<sup>41</sup> fast stirring speeds and/or dilute carbon precursor concentrations.<sup>47</sup> In addition, as has been shown in literature,<sup>48,49</sup> the macropore size and structure can be controlled by controlling the dipping rate (of the colloidal silica–glucose mixture in liquid nitrogen), concentration of carbon precursor, concentration and size of colloidal particle and by other established techniques. Furthermore the activation reaction conditions can control the microporosity. (2) The synthesis is simple, reproducible, greener, and uses inexpensive and widely available starting materials (water/ice for macropores, silica for mesopores, CO<sub>2</sub> for micropores), all of which make the process highly scalable.

Scheme 1 shows a graphical representation of the synthesis technique (the details of the synthesis technique are provided in the ESI†). The solidification of water, as a result of plunging the mixture into the liquid nitrogen, expels both the silica particles and glucose molecules away from the growing ice crystals. The ice is then simply removed by sublimation. Care must be taken during the freeze-drying process to prevent the ice templated glucose–silica material from melting. The glucose–silica composite scaffold (shown in Fig. S1†) is then carbonized, resulting in a macroporous carbon–silica structure. The network of interconnected macropores formed after sublimation (Fig. S1a†) remains intact during pyrolysis and after silica etching (Fig. S1b†). Fig. 1(a, c and d) shows the SEM images of the resultant HPC material after the silica etching using NaOH.



**Scheme 1** Schematic showing the basic steps and the material thus produced after each step. The four steps shown clockwise from bottom left are: (1) (side view) ice templating – ice front movement through the glucose and colloidal silica aqueous suspension forming ice crystals, (2) (top view) freeze drying – the glucose–silica composite material with macropores after removal of ice, (3) (top view) carbonization and silica etching – macro-mesopore dominated carbon and finally, (4) (top view) physical activation – hierarchical carbon. Note: for simplification, the pores are not shown as interconnected. For convenience the samples are denoted by KCU-C *x–y–z*, where *x* represents the average colloidal silica size (nm), *y* represents the mass ratio of silica to glucose and *z* represents the time (h) for CO<sub>2</sub> activation.



**Fig. 1** (a–d) SEM images of HPC scaffolds. Images show: (a) the monolithic character of the HPCs, (b) the interconnected macroporous structure evident before etching of the colloidal silica and (c) a similar interconnected macroporous structure after etching. (d) Higher resolution SEM shows a roughened morphology consistent with mesopores. Representative TEM images of (e) KCU-C 12–1 (f) KCU-C 12–2 (scale bars for TEM images are 200 nm for the larger images and 20 nm for the inset images).



The SEM images are consistent with an HPC scaffold whose macroporous walls are made up of an interconnected mesoporous carbon. This is further confirmed by TEM images (Fig. 1(e and f) and Fig. S2†) that reveal an extensive network of mesopores. The mesopores seen in the TEM images are in good agreement with the  $N_2$  adsorption data (*vide infra*).

The surface area and pore volume of the macropores measured by mercury porosimetry are  $11 \text{ m}^2 \text{ g}^{-1}$  and  $9.1 \text{ cm}^3 \text{ g}^{-1}$  respectively for the KCU-C 4-1 sample. Care was taken to vary the pressure applied under mercury porosimetry so that any pores under 50 nm were not analyzed and incorporated into the results. The macropore size distribution obtained *via* mercury porosimetry measurements (Fig. S3†) is in good agreement with those seen in SEM images in Fig. 1. These results are consistent with expectations from previous work<sup>44</sup> that within the range of colloidal silica nanoparticles used, macroporosity is controlled mostly by the speed of ice formation (*i.e.* freezing speed).

The total BET surface area and pore volume (excluding macropores) for a series of samples is summarized in Table 1. It is important to note that these pore volumes, calculated from  $N_2$  sorption, for the KCU-C  $x-2$  samples (from  $3.0$  to  $4.1 \text{ cm}^3 \text{ g}^{-1}$ ) are among the highest values measured for mesoporous carbon materials.<sup>50,51</sup> In contrast to macroporosity, the silica to glucose ratio and the size of silica affects the mesoporosity. For HPCs synthesized using silica to glucose ratio of 1 the surface area and pore volume decrease as the silica particle size increases. No such dependence is seen for the silica to glucose ratio of 2, where the surface area is generally the same regardless of silica size. For a given silica particle size, the surface area and the pore volume increase as the silica to glucose ratio increases from 1 to 2. The percent increase in surface area is much more pronounced for the 12 and 20 nm silica particles (the increase for all particle sizes are 1, 11, 36 and 53% for the 4, 8, 12 and 20 nm silica, respectively). The specific surface area and extent of microporosity can be further increased by  $\text{CO}_2$  activation. Under  $\text{CO}_2$  activation, the duration and flow rate of  $\text{CO}_2$  are important factors in determining the increase in microporosity and surface area.  $\text{CO}_2$  activation was performed on the KCU-C 4-1 sample, for different time holds at  $950 \text{ }^\circ\text{C}$ , at a constant  $\text{CO}_2$  flow rate of  $50 \text{ cm}^3 \text{ min}^{-1}$ . 3-4 hours of activation time was found to be optimal. The thus synthesized KCU-C 4-1-4 sample had a BET surface area of  $2096 \text{ m}^2 \text{ g}^{-1}$  and pore volume of

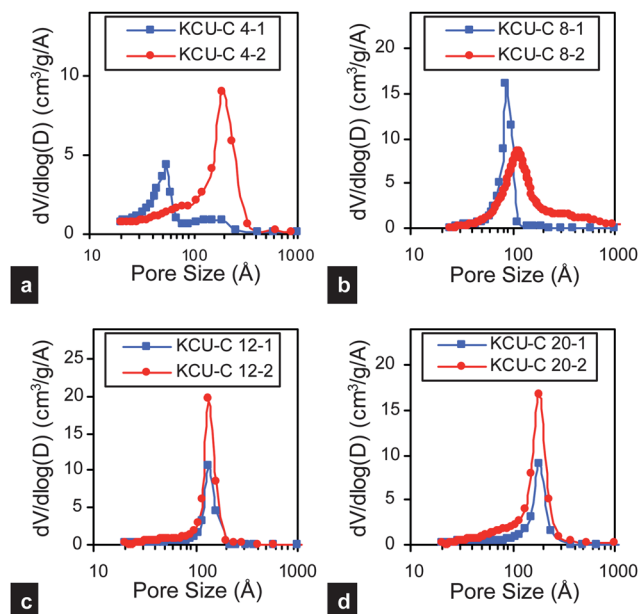
$3.0 \text{ cm}^3 \text{ g}^{-1}$ , comprising of increased microporous content and broadened mesoporosity (see Fig. S4†).

A distinct advantage of our approach is the ability to easily control the pore sizes. For example, the size of the mesopores can be easily tuned by using different size silica particles. Fig. 2 shows the pore size distribution calculated using the BJH model for a series of HPCs, synthesized using different size silica nanoparticles (4, 8, 12 and 20 nm). In the past, special efforts were devoted to ensure that the pore size of the resulting carbons is the same as the size of the starting template.<sup>41,47</sup> Such efforts typically focused on preventing aggregation of the hydrophilic silica nanoparticles within the pyrolyzing (and becoming increasingly hydrophobic) carbon precursor matrix. In our approach, the instantaneous locking of the silica nanoparticles within the glucose matrix and subsequent carbonization minimize such aggregation and phase separation. Note the high fidelity of the process in generating mesopores especially for the 1 : 1 ratio of silica to glucose; the size of the resulting mesopores corresponds well with the size of the silica nanoparticles used in the process (Fig. 2). This fidelity holds true for the 20 nm silica particles even for  $\text{SiO}_2/\text{glucose}$  ratio of 2. However at this higher silica/glucose ratio of 2, as the particle size decreases, aggregation of the particles during freezing leads to larger pore sizes and this is especially true for the 4 nm silica particles. Note that as the number of silica nanoparticles (relative to the glucose) increases, the amount of glucose present between the nanoparticles decreases, resulting in aggregation at higher ratios.

Our approach also offers the possibility to easily make HPCs with bimodal mesoporosity distribution, by merely starting with two different sized silica nanoparticles. The bimodal nature of the mesoporosity can be clearly seen, in the pore size distribution shown in Fig. S5 in the ESI,† for the sample synthesized using 4 nm and 20 nm silica.

**Table 1** Textural characteristics of the synthesized carbons

Sample name	BET surface area ( $\text{m}^2 \text{ g}^{-1}$ )	$N_2$ adsorption pore volume ( $\text{cm}^3 \text{ g}^{-1}$ )
KCU-C 4-1-4	2096	3.0
KCU-C 4-1	1316	2.3
KCU-C 4-2	1327	4.1
KCU-C 8-1	1129	2.0
KCU-C 8-2	1265	3.6
KCU-C 12-1	893	1.9
KCU-C 12-2	1216	3.0
KCU-C 20-1	841	1.9
KCU-C 20-2	1289	3.7



**Fig. 2** BJH pore size distributions for the KCU-C  $x-y$  samples. The BJH pore size distributions of the activated HPCs can be found in the ESI (Fig. S4†).



Another advantage of this approach is the flexibility it offers to produce carbon scaffolds either in powder form or as monoliths of desired shape and size, just by altering the mold used (see Fig. S6†). SEM imaging and adsorption measurements confirm that the monoliths possess surface area, specific pore volume and pore size distribution similar to the powder samples. The apparent density of the cylindrical monoliths was found to be approximately  $0.09 \text{ g cm}^{-3}$ , by measuring the bulk samples' weight and apparent volume, and was confirmed *via* Hg porosimetry. The modulus of the monoliths evaluated using compression testing was  $\sim 1 \text{ MPa}$ , consistent with other porous carbon materials.<sup>52</sup> Further discussion of the mechanical properties can be found in Fig. S7.†

Lately there has been much interest in developing multi-modal (macropore and mesopore dominated) support materials (metal oxides<sup>53–55</sup>) for amine based  $\text{CO}_2$  capture. However, the synthesis of most of such porous metal oxide based sorbents involve the use of costly non-renewable chemicals such as surfactants or pore expanders, which limits their use for large scale  $\text{CO}_2$  capture. Our HPCs with their inherent high pore volumes and specifically, the samples with large pore sizes appear to be excellent alternative candidates for amine based  $\text{CO}_2$  capture. Thus, a KCU-C 4–3 sample, with ultralarge mesopores of  $\sim 50 \text{ nm}$ , was synthesized (Fig. S8†), impregnated with polyethyleneimine (PEI), achieving a PEI loading of 73 wt% and its  $\text{CO}_2$  capture capacity was briefly evaluated. As shown in Fig. 3(a), a sharp weight gain was observed after the sorbent was exposed to  $\text{CO}_2$  in the first 5 min and 97% of the adsorption

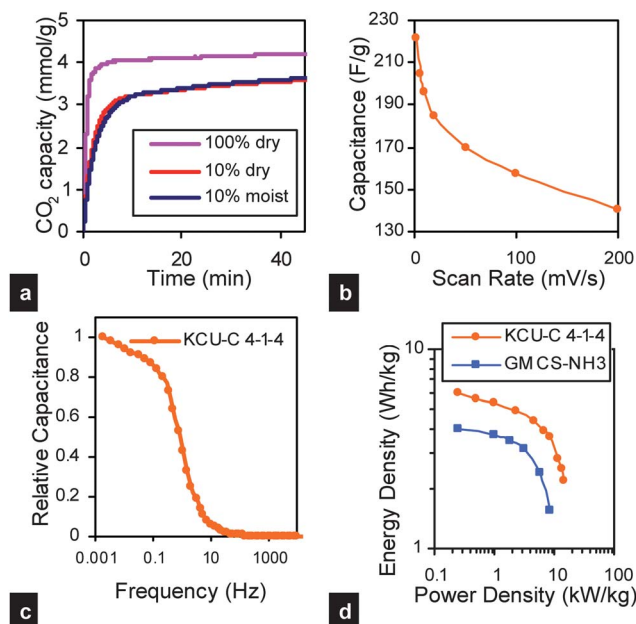
( $4.1 \text{ mmol g}^{-1}$ ) was obtained after 10 min. A capacity of up to  $4.2 \text{ mmol g}^{-1}$  was achieved after 45 min, which is among the highest reported value for amine-impregnated carbon-based sorbents.<sup>56</sup> More importantly, for dilute  $\text{CO}_2$  (10%  $\text{CO}_2$ –90%  $\text{N}_2$  gas mixture), the sorption capacity measured under dry and moist conditions was the same, unlike physisorption of moist dilute  $\text{CO}_2$  in microporous carbons, which is severely effected by the presence of moisture.<sup>57</sup>

The HPCs were also briefly evaluated as electrodes for supercapacitors. The advantage of HPCs for this application is that the presence of mesopores and macropores may provide pathways for fast ionic transport while the micropores provide sites for ion sorption.<sup>20,22</sup> For a material to be used successfully as electrode material, it must have good electrical conductivity as well. The electrical conductivity measured using a four point probe was in the order of  $1 \text{ S cm}^{-1}$  for the various KCU-C materials. Using the KCU 4–1–4 sample in a three electrode setup with  $1 \text{ M H}_2\text{SO}_4$  as the electrolyte, a specific capacitance of  $221 \text{ F g}^{-1}$  was obtained at a scan rate of  $2 \text{ mV s}^{-1}$ , with 64% retention even at a two orders of magnitude higher scan rate of  $200 \text{ mV s}^{-1}$ .

These values compare favorably well with the values reported in the literature for other hierarchical carbons.<sup>1,12</sup> The sample also shows promising capacitive frequency response Fig. 3(c), calculated from electrochemical impedance spectroscopy data<sup>58</sup> (Fig. S9(b)†), retaining 50% of its maximum capacitance even when the frequency increases to  $0.73 \text{ Hz}$ . Symmetric cells prepared from KCU-C 4–1–4 could deliver a specific energy density upto the order of  $6 \text{ Wh kg}^{-1}$  and a power density in the range of  $14 \text{ kW kg}^{-1}$ , measured using galvanostatic charge-discharge testing. For comparison, we include the performance of another hierarchical carbon,  $\text{NH}_3$  treated, graphene mesoporous carbon spheres.<sup>13</sup> Further EDLC data for KCU-C 4–1–4 are presented in the ESI (Fig. S9†). Detailed investigations on use of KCU-Cs as support material for amine based  $\text{CO}_2$  capture and as electrode materials for supercapacitors are currently in progress.

In summary, we report a novel approach to synthesize HPCs, which combine macro-, meso- and microporosity in a simple material platform. Our approach integrates ice templating with hard templating and physical activation to produce HPCs with interconnected porous structure, large surface area, and pore volume. The technique offers tight control and tunability of porosity (macro- meso- and microscale) in terms of both size and extent. It also offers the ability to make HPC monoliths of desired shape and size. The hierarchical carbons show excellent performance as – sorbents for amine based  $\text{CO}_2$  capture and as electrode materials for supercapacitors.

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**Fig. 3** (a)  $\text{CO}_2$  sorption capacity of PEI-KCU-C 4–3 (73 wt% PEI) composite, (b) variation of specific capacitance with sweep rate, measured from cyclic voltammetry data for KCU-C 4–1–4 in  $1 \text{ M H}_2\text{SO}_4$  within the potential range  $0\text{--}1 \text{ V}$  (vs.  $\text{Ag}/\text{AgCl}$ ), (c) capacitive frequency response of KCU-C 4–1–4 measured in symmetrical two electrode configuration (d) Ragone plot for KCU-C 4–1–4 and GMCS- $\text{NH}_3$  ( $\text{NH}_3$  treated, hierarchical, graphene mesoporous carbon spheres<sup>13</sup>) measured in symmetrical two electrode configuration using different current densities in  $1 \text{ M H}_2\text{SO}_4$  within the potential range  $0\text{--}1 \text{ V}$ .



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