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Shaping of porous metal–organic framework granules using mesoporous ρ -alumina as a binder†

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The shaping of metal–organic frameworks (MOFs) on a macroscopic level is a vibrant area in MOF research. For practical application of MOFs, the fine microcrystalline powder should be converted into a shaped body while preserving the powder's intrinsic properties. In this study, we prepared millimetre-scale spheres of MIL-100(Fe), MIL-101(Cr), UiO-66(Zr), and UiO-66(Zr)_NH₂ using the wet granulation method. The use of mesoporous ρ -alumina (MRA) as a binder resulted in well-shaped MOF bodies which retained their intrinsic properties after shaping. Furthermore, the performance of the MOF spheres was compared to that of compressed pellets in terms of NH₃ adsorption using a breakthrough test, and CO₂ and N₂ adsorption performance was compared using adsorption isotherms at 298 K between the powder and spheres of MOFs for future industrial applications.

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1. Introduction

Metal–organic frameworks (MOFs) are a class of promising porous crystalline materials for potential application in gas storage and separation, chemical sensing, heterogeneous catalysis, *etc.*^{1–5} They have unique structural and texture characteristics like large surface areas, tunable pore-size distributions, and coordinatively unsaturated metal sites (CUSs).^{6–8} Over the past decade, many researchers and companies have attempted to find a commercial use for these appealing porous materials.^{9–12} However, there are several problems that need to be addressed in order to successfully use MOFs for industrial and chemical engineering applications. The fundamental issue with commercial applications is the highly pulverulent property of MOFs. One of the major strategies to overcome this problem has been to produce macroscopic MOF bodies using various shaping processes.

Shaped MOF bodies have been produced in the form of pellets, tablets, monoliths, granules, and spheres using typical shaping techniques like pressing, extrusion, granulation, and spray drying.^{13–17} In general, the shaped body of a porous material provides improved handling, improved bulk density,

and reduced pressure drop for fluid flow in packed bed systems. However, the chemical and mechanical sensitivities of MOFs to binders, pressure-shaping process, *etc.* limit our ability to form them into shaped bodies without losing their novel properties.^{18,19} Therefore, to understand the pivotal importance of the shaping of MOFs, the prime objective of the current investigation was to develop a facile shaping method using a versatile binder suitable for use with various MOFs while preserving their specific properties.

Recently, new strategies have been reported for fabricating macroscopic MOFs on a millimeter scale. Blom *et al.* prepared agglomerated spheres of CPO-27(Ni) using hydrocolloids and gelling agents as natural polymer binders by the “molecular gastronomy” method.²⁰ CPO-27(Ni) powder was formed into nicely shaped spheres 2.5–3.5 mm in size and containing more than 84 wt% of MOFs with minor loss in their weight-specific surface area (WSSA); the resulting spheres showed good mechanical strength. In another example, large-scale continuous neat melt-phase synthesis of ZIF-8 under solvent-free or low-solvent conditions was successfully demonstrated by James *et al.*²¹ This enhanced extrusion technique provided shaped bodies with high space-time yields (STY) of up to $144 \times 10^3 \text{ kg m}^{-3}$. In the past, several research groups including ours reported the preparation of well-shaped MOFs using polymer, graphite and silica sol binders for a wide range of applications.^{16,22–28} However, the thermal stability of the shaped MOF bodies decreased owing to the low degradation temperature of the polymer binder. MOFs have also been shaped by deposition onto range of metal surfaces, also with follow-up the addition/coating of binders.^{29–32}

Although most studies have focused on the shaping methods, processes, or application of shaped MOFs, very few

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studies have investigated the effect of the shaping process on the intrinsic chemical properties of MOFs.^{33,34} Here, we present a simple but effective granulation process to fabricate macroscopic MOF bodies using amorphous-phase mesoporous ρ -alumina (MRA) as a binder. MRA can be used as hydratable and bondable alumina in the presence of a small amount of a hydrophilic polar dispersion medium like water or alcohol.^{35,36} The corresponding properties can be potential use for binding MOF particles during the shaping process under ambient condition. Indeed MRA requires no additional additives where all the shaping process can be completed through wet granulation and subsequent drying in ambient air or elevated temperature. In this study, we prepared millimeter-scale spheres of MIL-100(Fe), MIL-101(Cr), UiO-66(Zr), and UiO-66(Zr)-NH₂ using the wet granulation method. MRA bonded with the MOFs without the substantial loss of the fundamental properties for example initial sorption capacity of the crystals. Thus, the formation of well-shaped bodies which can be easy-to-handle and also is scalable in large amount shown in the present work can be considered as a significant step toward the industrial-scale application and commercial application of MOFs.

2. Results and discussion

2.1. Porous and morphological properties of MRA binder

Fig. 1a and b show the N₂ adsorption–desorption isotherms at 77 K and the Barrett–Joyner–Halenda (BJH) pore-size distribution of the alumina binder, respectively. The BET surface area of the alumina binder was 218 m² g⁻¹. The N₂ adsorption–desorption isotherm (Fig. 1a) was type IV, showing a broad hysteresis loop in the relative pressure (p/p_0) range of 0.5 to 0.9, which confirms the mesoporosity of MRA. MRA had an average pore diameter of ~4 nm, which was calculated using the BJH method. The transmission electron microscopy (TEM) image of MRA (inset of Fig. 1b) shows mesopores with a disordered structure, and the pore diameter agrees well with the results of the BJH method. Therefore, the corresponding mesoporous binder is suitable for the shaping of thermally and chemically sensitive MOFs because it compensates for the loss in surface area. It is also useful for the diffusion of gases in adsorption/separation processes.

2.2. Characterization of shaped MOF bodies

2.2.1. Porous and mechanical properties. The shaping of MOFs is also governed by the interactions between the powder and the binder/dispersion medium in the wet granulation process.^{38–40} Scheme 1 shows the preparation of a well-shaped body from a mixture of MOF crystals and MRA. We prepared shaped bodies of four discrete MOFs: MIL-100(Fe) (CUS, mesopore), MIL-101(Cr) (CUS, mesopore, high surface area ~4000 m² g⁻¹), UiO-66(Zr) (micropore), and UiO-66(Zr)-NH₂ (micropore, functionalized linker). These selected MOFs are known for their unique features like high surface area, functionality, stability, and pore size.^{37,41–43} The preparation process of the spherical MOFs is given in the Experimental section. All the shaped bodies containing 5 wt%

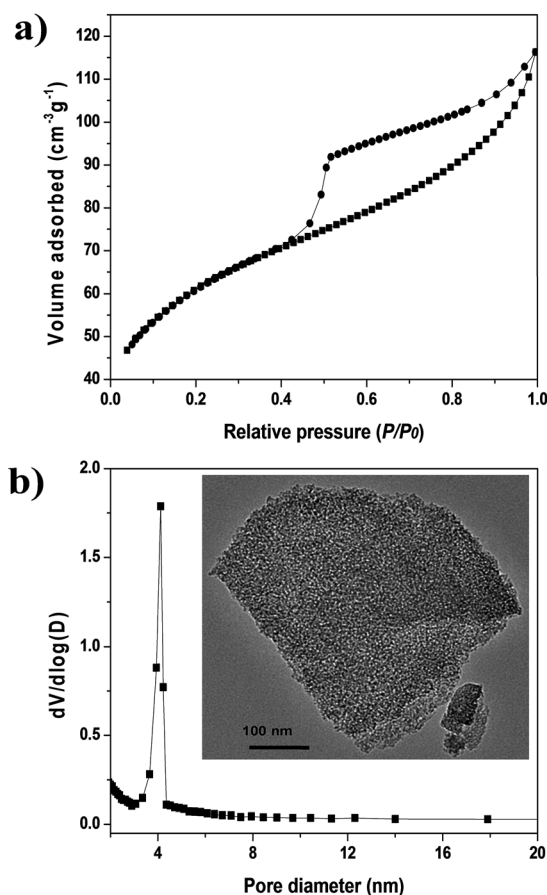
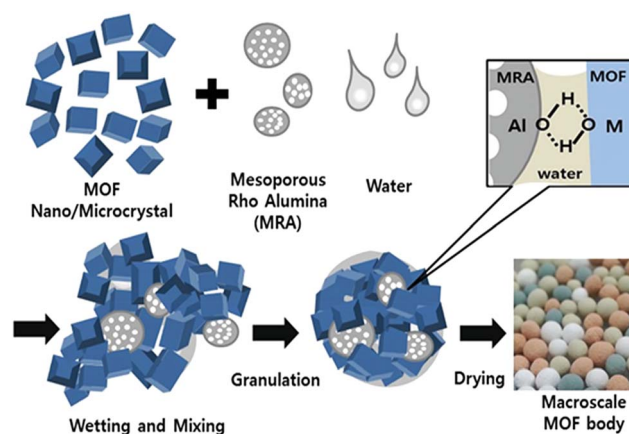


Fig. 1 Characterization of MRA binder: (a) N₂ adsorption–desorption isotherms at 77 K and (b) pore-size distribution calculated from BJH method (inset of (b) is the TEM image of MRA binder).

MRA were spherical or pseudo-spherical with diameters of 2–2.5 μ m (Fig. 2). The sizes of the spheres could be controlled to 0.5–10 μ m or more by adjusting the process conditions such as pan rotation speed, time, and the amount of wetting medium for the agglomerated granules.⁴⁴ Rod-like shapes could also be fabricated by using the extrusion process (Fig. S1†).



Scheme 1 Preparation of MOF granules/spheres through agglomeration of MOF and MRA particles by wet granulation process.



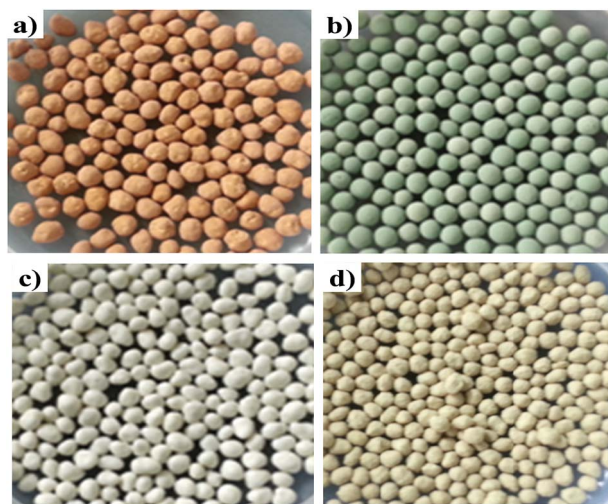


Fig. 2 Photographs of shaped bodies containing 5 wt% MRA binder: (a) MIL-100(Fe), (b) MIL-101(Cr), (c) UiO-66(Zr), and (d) UiO-66(Zr)-NH₂.

The nitrogen gas adsorption isotherms at 77 K for all the shaped MOF bodies showed a negligible decrease in nitrogen uptake (volume) compared to their pristine powders; however, no change in the isotherm patterns was observed (Fig. 3). Furthermore, the multistep features apparent in the powder samples (Fig. 3a and b) remained unchanged, indicating no alterations in pore dimensions; this was further supported by the pore-size distribution curves presented in Fig. S2.† Mercury porosimetry was used to gain further information on the porous characteristics of the shaped MOFs. The hierarchical pore structures (mesoporosity and macroporosity) obtained from mercury porosimetry for all the MOF spheres because of inter-

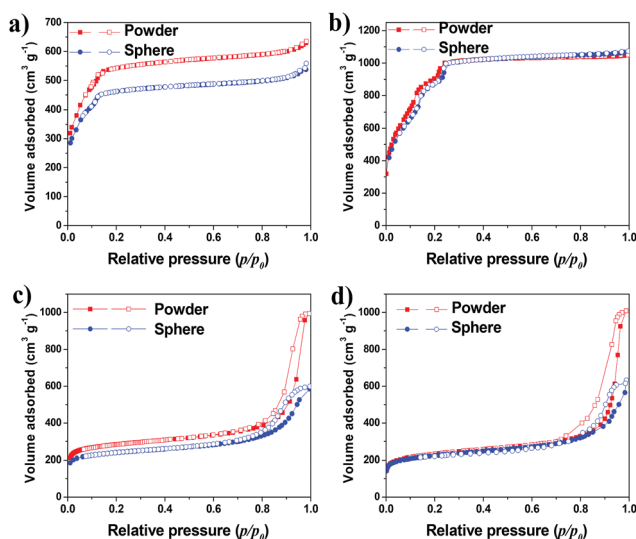


Fig. 3 N₂ adsorption-desorption isotherms at 77 K for MOFs (powder and sphere containing 5 wt% MRA binder) degassed overnight at 423 K: (a) MIL-100(Fe), (b) MIL-101(Cr), (c) UiO-66(Zr), and (d) UiO-66(Zr)-NH₂.

particle voids generated during shaping process (Fig. 4). However, the pore-size distributions of the spheres were dependent on the particle size, shaping process parameters and the interaction and affinity between the spheres and MRA.

The fundamental properties of MOF spheres containing 95 wt% MOF and 5 wt% binder are given in Table 1. The loss in WSSA for all the MOFs were in the range of 1.0–7.7% after shaping into spheres, probably due to difference in the intrinsic properties of the MOFs, the preparation conditions, and the interaction between the MOFs and the MRA binder. The average crushing strengths and bulk densities of spheres were also measured and were found to depend on the physicochemical properties of the MOFs and on a number of adjustable process parameters during granulation.³⁹ The crushing strength of the spheres could be controlled by fine-tuning the binder amount in the spheres. Increasing the concentration of the binder from 5 to 10 wt% improved the crushing strength of the MIL-100(Fe) spheres more than 30%.

2.2.2. Structural and morphological properties. The X-ray diffraction (XRD) patterns (Fig. 5) indicated that all the MOFs used in this study were highly crystalline, and the peak positions were in accordance with the literature data reported previously.^{11,12,43,45} There were no extra peaks associated with the binder because of its amorphous nature. The shaped bodies exhibited slightly lower crystallinities with respect to the powder because of inclusion of the binder by weight. However, many shaping methods reported in the past significantly hampered or deteriorated the crystalline structure, sometimes even leading to an amorphous phase.^{18,19}

Macroscale shaped bodies were built *via* the binding of MOF and MRA particles through interaction of hydroxyl groups present on the surfaces of the particles (Scheme 1). The FT-IR spectra of the MIL-100(Fe) shaped bodies with different binder amounts (Fig. 6) showed interfacial binding between the MRA and MOF particles. The vibrational stretching frequencies of the Fe-OH group of MIL-100(Fe) at approximately 3600–3700 cm⁻¹ were generated from the coordination of water or OH groups to Fe³⁺.^{46,47} As compared to the original powder, the intensity of the ν(OH) peaks decreased and their peak positions shifted to lower wavenumbers. This fact can be explained in two ways. First, the MOF and MRA particles were mixed and granulated into spheres in the presence of water, leading to intimate interactions through hydrogen bonding. The hydrophilic OH groups promoted initial wetting and good dispersion of the MRA binder on the surfaces of the MOF particles in the presence of polar liquids such as water and alcohol. The OH groups present on the surfaces of the binder particles, along with the dispersion medium, led to strong adhesion and the dipolar attraction of OH groups from the surfaces of adjacent MOF particles to produce intermolecular hydrogen bonding. This solid-solid interfacial hydrogen bonding in the presence of water shifted the peak position to lower wavenumbers in the shaped MIL-100(Fe). Second, the reduced peak intensity is a function of the amount of binder present in the shaped bodies. MRA has a strong affinity for adsorption on oxide particles dispersed in water.³⁵



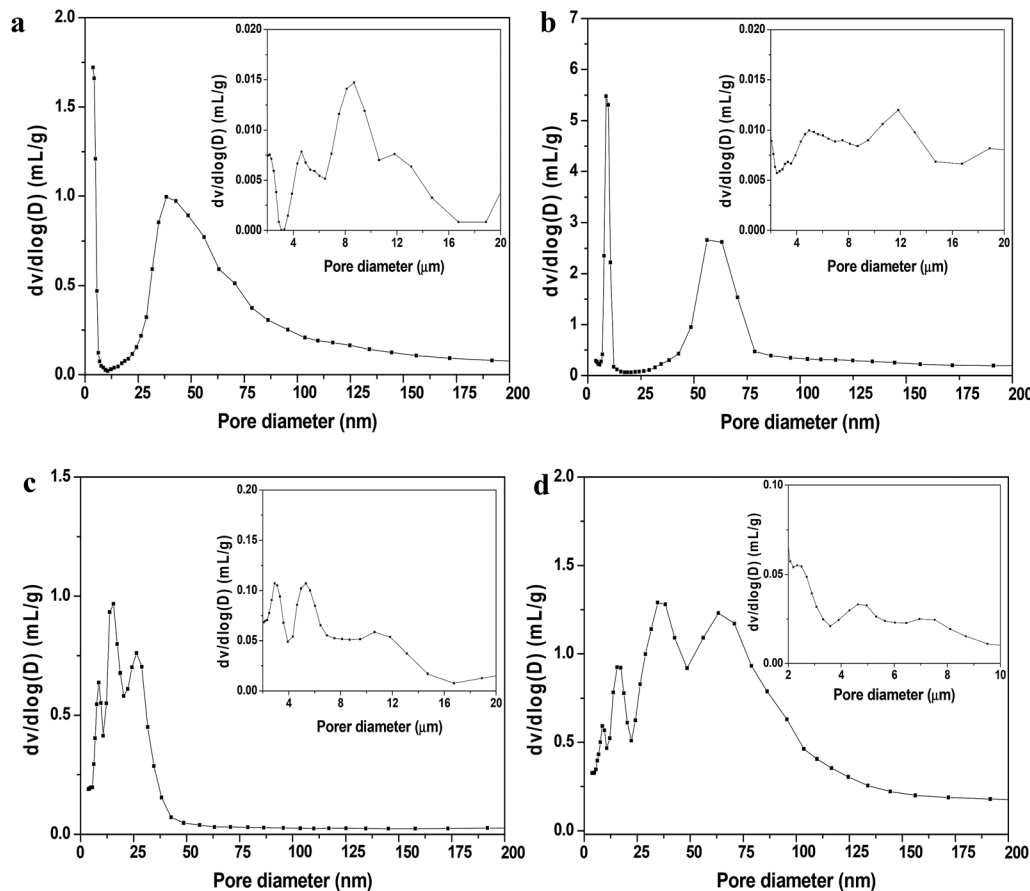


Fig. 4 Mesopore- and macropore-size distribution profiles of shaped MOFs were measured by mercury intrusion porosimetry: (a) MIL-100(Fe), (b) MIL-101(Cr), (c) UiO-66(Zr), and (d) UiO-66(Zr)_{NH₂}. Insets show small numbers of macropores in the range of 0.5 to 10 or 20 μm.

Table 1 Characterization data of the shaped MOF bodies containing 5wt% MRA binder and their powder constituents

MOF	Surface area (m ² g ⁻¹)		Pore volume (cm ³ g ⁻¹)		Loss in WSSA ^a after shaping (%)	Average crushing strength (N)	Average sphere density (g cm ⁻³)
	Powder	Sphere	Powder	Sphere			
MIL-100(Fe)	2088	1831	1.0	0.9	7.7	6.7	0.63
MIL-101(Cr)	4066	3685	1.6	1.6	4.6	4.1	0.57
UiO-66(Zr)	1050	911	1.5	0.9	8.7	4.7	0.67
UiO-66(Zr) _{NH₂}	875	823	1.6	1.0	1.0	2.5	0.56

^a WSSA: weight-specific surface area.

Recent advances in visualization strategies on a microscale have been utilized in several studies to unlock the inner complexity of materials.^{48–52} Therefore, in order to obtain some insight into the internal arrangement of MOF crystals and MRA particles, we characterized the shaped bodies using microscopic analysis. SEM analysis of the alumina binder showed a wide range of particle sizes (Fig. S3†), and there were clear-cut differences in the particle sizes of alumina and MOFs. The alumina particles were in the micrometer range, whereas all the MOF particles were in the sub micrometer range. No visible difference in the morphologies of the powder and spherical forms of the MOFs was observed. It was not easy to identify

alumina particles in the interior of spheres using SEM, possibly owing to the low alumina concentration and its good dispersion in the spheres. EDS (X-ray energy-dispersive spectroscopy) elemental mapping was used to determine the spatial distribution of elements in the spheres. As shown in Fig. 7a, EDS elemental mapping revealed that alumina particles were distributed uniformly throughout the sphere, even at the higher alumina concentration (20 wt%). The images of the other sample morphologies showed similar results (Fig. S4†). The homogeneity of the binder within the spheres can be explained by the breaking up of agglomerates and the continued exchange of particles during granule growth in the granulation process.³⁹



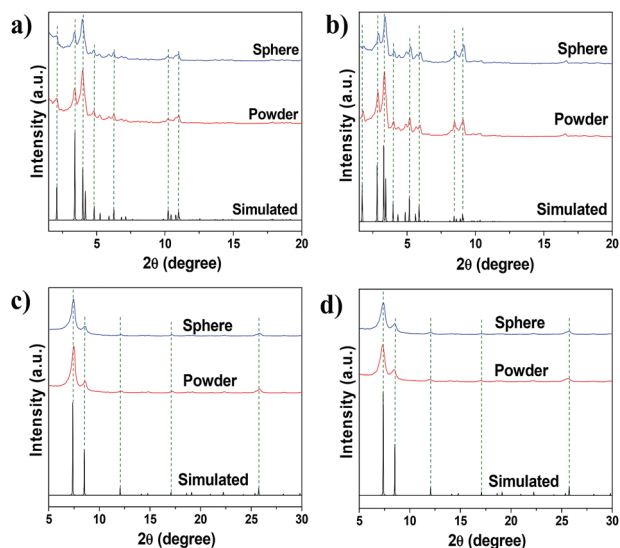


Fig. 5 Simulated and experimental XRD patterns of MOF powders and shaped bodies (containing 5 wt% MRA binder): (a) MIL-100(Fe), (b) MIL-101(Cr), (c) UiO-66(Zr), and (d) UiO-66(Zr)-NH₂ since, crystallographic information file (CIF) for UiO-66(Zr)-NH₂ was not available simulated XRD pattern of parent UiO-66(Zr) was used.

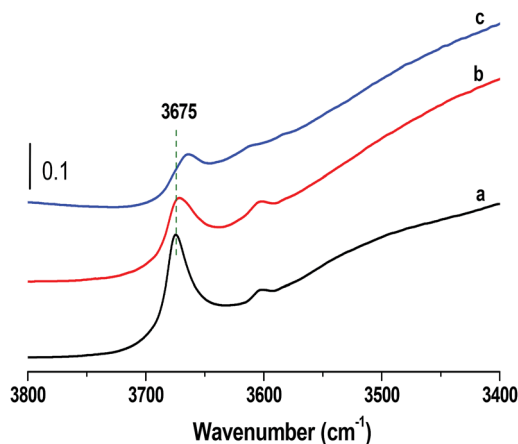


Fig. 6 FTIR spectra of powder and shaped forms of MIL-100(Fe) with different MRA binder contents: (a) powder MIL-100(Fe), (b) sphere MIL-100(Fe)-5 wt% MRA binder, and (c) sphere MIL-100(Fe)-10 wt% MRA binder.

To provide further insights into the morphological behavior, we performed TEM elemental mapping. Fig. 7b shows that agglomeration of MRA (5 wt%) and MIL-100(Fe) particles occurred when single large MRA binder particles were surrounded by small aggregated particles of MIL-100(Fe). This interparticle interaction between MRA and MOF was the major reason for the formation of mesopores (~ 50 nm) and macropores (~ 10 μm) in the shaped bodies, as evident from the mercury porosimetry analysis (Fig. 4). Therefore, the agglomeration of MOFs with the present MRA binder particles resulted in additional benefits in the form of a hierarchical pore system.

2.2.3. Acidic properties of pristine and shaped MIL-100(Fe). Considering the wide application of the MIL-100(Fe) in

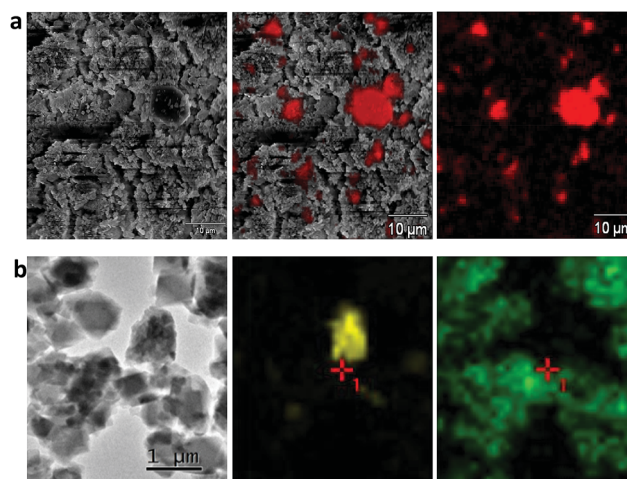


Fig. 7 (a) Cross-sectional SEM/EDS elemental mapping image of 20 wt% MRA binder in MIL-100(Fe) shaped body and (b) TEM/EDS elemental mapping images of 5 wt% MRA binder in MIL-100(Fe) shaped body. In the images of (a), red areas represent Al from MRA binder. In the image of (a) red area represents Al from MRA binder. In the mapping image of (b), yellow and green areas represent Al from MRA and Fe from MOF respectively.

heterogeneous catalysis and gas or vapor sorption,^{53–58} it is important to study the impact of shaping on its chemical performance or acidic sites (or CUS concentration). We therefore performed NH₃-TPD and pyridine-IR analyses. NH₃-TPD analysis illustrated the acidic sites present in the MOF material and pyridine-IR analysis further distinguished the nature of the acidity.

The NH₃-TPD profiles of the MIL-100(Fe) powder and shaped bodies with different MRA concentrations are shown in Fig. 8a. Considering the lower degradation temperature of MIL-100(Fe) (548 K), the TPD temperature was increased from 323 to 573 K with a ramping rate of 5 K min⁻¹. The samples were pretreated at 523 K for 12 h prior to analysis to generate CUSs by removal of the terminal water molecule and the hydroxyl group from the framework and to avoid NH₃ adsorption onto physically bonded water through hydrogen bonding.⁵⁸ The MRA binder plays an important role in determining the properties of the resulting shaped MOF bodies because binder particles can cover the pore windows and active surfaces (such as CUSs) of the MOFs. Indeed, the NH₃-TPD profiles of the MIL-100(Fe) powder and the MRA-containing shaped bodies were similar, which indicates that the chemically active sites of MIL-100(Fe) were well preserved in its shaped form.

To further clarify this phenomenon, we carried out pyridine-IR analysis of the powder and shaped samples of MIL-100(Fe) (Fig. 8b). The pyridine-IR results of MIL-100(Fe) were well summarized in a previous study.⁴⁶ The Lewis acid sites in MIL-100(Fe) generated from coordination of pyridine with Fe³⁺ and Fe²⁺ at 1014 cm⁻¹ and 1005 cm⁻¹, respectively, were retained in the spheres with 5–20% MRA. The presence of Fe²⁺ in MIL-100(Fe) was generated due to removal of OH or F group from trimeric cluster because of high temperature treatment prior to pyridine-IR analysis [for further details, see the *in situ* IR study



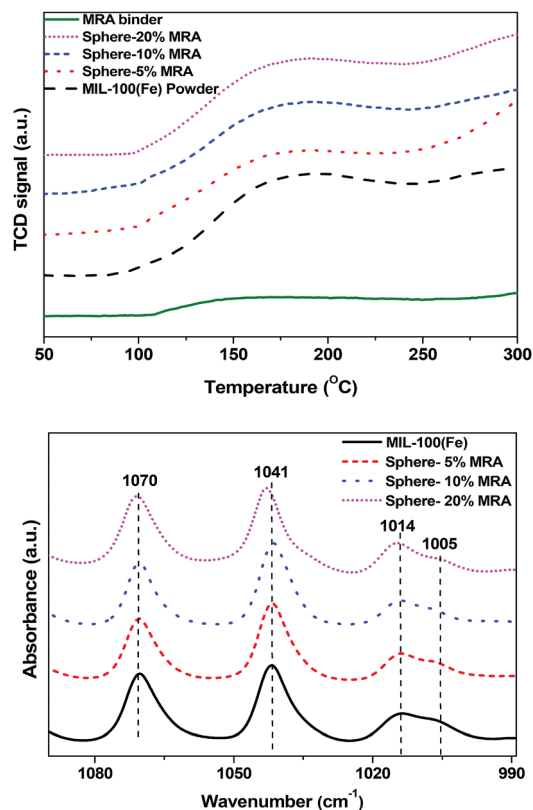


Fig. 8 (a) NH₃-TPD profiles and (b) pyridine-IR spectra of MIL-100(Fe) powder and spheres with 5, 10, and 20 wt% MRA binder.

of MIL-100(Fe) in the ESI, Fig. S5†].⁴⁶ No significant variation in the strength of the peaks was observed. The decrease in the acidity was proportional to the binder content, which can dilute the acidity of MOFs. A similar dilution effect was observed for H-ZSM-5 zeolite by IR and TPD analyses after being shaped into granules using an attapulgite clay binder.⁵⁹ The aforementioned results confirmed that the CUSs of MIL-100(Fe) were unaffected by the shaping process and the use of MRA binder.

2.3. Ammonia adsorption on shaped bodies of MIL-100(Fe)

Recently, toxic gas adsorption, particularly that of ammonia, over porous solid materials has attracted the attention of many researchers.^{58,60–62} Considerable effort has been made to choose a potential material for the adsorption of ammonia gas. Bandoz *et al.* comprehensively studied MIL-100(Fe) and an MIL-100(Fe)-GO composite material for this purpose.⁵⁸ Considering MIL-100(Fe) as a potential candidate for NH₃ adsorption, its practical implementation motivated us to perform NH₃ breakthrough tests using shaped bodies of MIL-100(Fe). We also investigated how the binder and shaping method affect the NH₃ adsorption performance of MIL-100(Fe). Generally, NH₃, with its free lone pair of electrons, tends to bind with electron-deficient species through a coordinative covalent bond. It is well documented that several MOFs, including MIL-100(Fe), have Lewis acidity due to the presence of CUSs.^{8,63} Therefore,

NH₃ can easily form coordinate bonds with the CUSs of MIL-100(Fe).

The NH₃ breakthrough results obtained for granulated and conventional pellets of MIL-100(Fe) are shown in Fig. 9. The test was carried out at 298 K under dry conditions using samples that were pretreated at 423 K for 12 h prior to the breakthrough test. The ammonia uptake capacity of MIL-100(Fe) spheres (4.4 mmol g⁻¹) was higher than that of MIL-100(Fe) pellets (3.6 mmol g⁻¹), which confirms that the pore structure and CUSs of MIL-100(Fe) spheres were not significantly affected by the shaping (granulation) process. The ammonia uptake capacity of MIL-100(Fe) reported here is somewhat higher than that previously reported (4.3 mmol g⁻¹).⁵⁸ On the other hand, shaping MIL-100(Fe) by pressing affects the crystal structure and porosity (Fig. S6†), which subsequently lowers the adsorption of ammonia as compared to the spheres prepared in the present work. We further checked the effect of pressure-dependent pelletization on the physicochemical properties of MIL-101(Cr) in detail (Fig. S7†), and the obtained results were in line with the results obtained for MIL-100(Fe). Additionally, we have summarized the other shaping strategies utilized previously in the literature for shaping of MOFs and their effects on its porous properties [Table S1†].

2.4. CO₂ adsorption on powder and shaped bodies of MIL-101(Cr), UiO-66(Zr) and UiO-66(Zr)_NH₂

Metal-organic frameworks (MOFs) have been extensively investigated for the adsorption of CO₂.⁶⁴ In recent years, adsorption-based post combustion CO₂ capture has also received great attention.^{65,66} The adsorbents for this process should have high CO₂ uptake at lower pressure (0.15 bar) under ambient temperature such as 298 K, good CO₂/N₂ selectivity and excellent water stability.⁶⁴ MOFs have been demonstrated with great potential for this purpose.⁶⁴ The MOFs reported herein

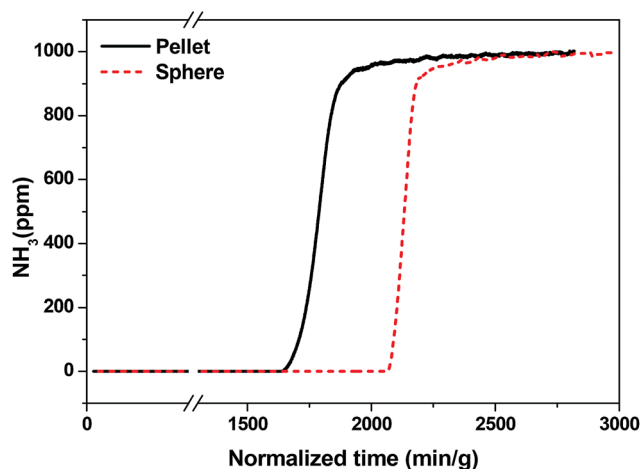


Fig. 9 NH₃ breakthrough test of shaped MIL-100(Fe) bodies (spheres) containing 5 wt% MRA binder and a pellet fabricated by using the pressing method with 3 wt% of graphite as the binder at 298 K. Amounts of NH₃ calculated for sphere (4.4 mmol g⁻¹) and pellet (3.6 mmol g⁻¹) were normalized to the MIL-100(Fe) content present.



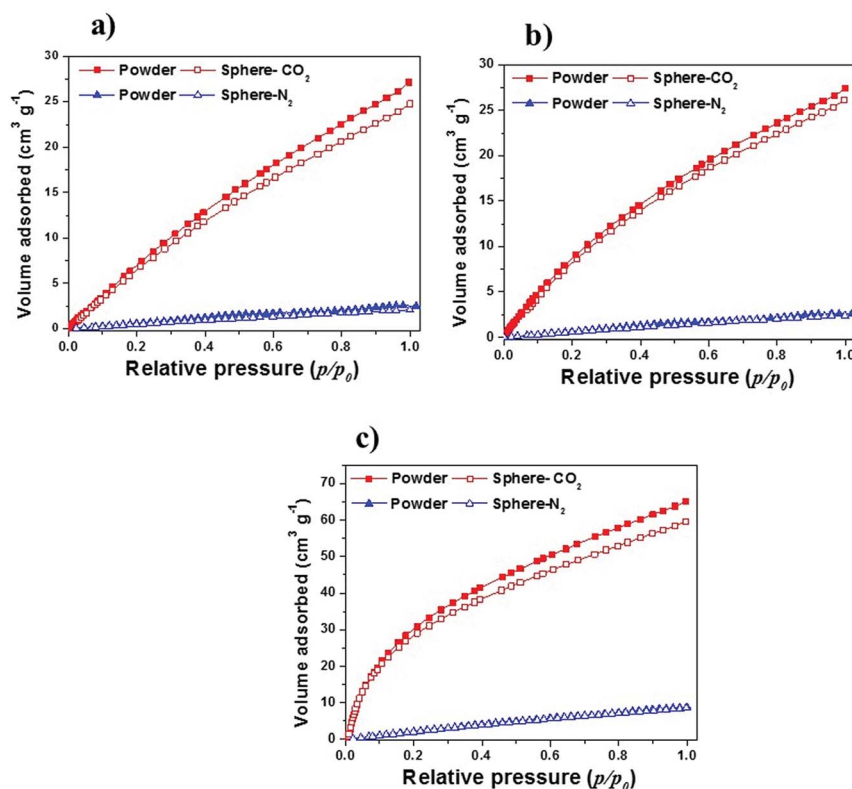


Fig. 10 CO₂ and N₂ adsorption isotherms at 298 K for MOFs powder and sphere (containing 5 wt% MRA binder) degassed overnight at 150 °C: (a) UiO-66(Zr), (b) UiO-66(Zr)-NH₂, and (c) MIL-101(Cr).

have excellent water stability which allowed us to evaluate their performance in CO₂ and N₂ capture at low pressure (up to 1 bar).

There is minor difference in CO₂ adsorbed on the powder with respect to the spheres of MOFs (Fig. 10). This difference in uptakes is in accordance with the difference in surface area of powder and sphere samples (Table 1). MIL-101(Cr) is a very prominent example of MOFs that possess unsaturated metal sites.^{37,45} It can capture CO₂ in its pores through physisorption as well as through a Lewis acid–base interaction between the coordinatively unsaturated Cr(III) sites, and O atoms in CO₂ molecule.⁶⁶ It exhibits high CO₂ adsorption capacity at lower pressure (25.9 cm³ g⁻¹), which has not influenced much after shaping into spheres (24.5 cm³ g⁻¹). At 0.15 bar pressure UiO-66(Zr)-NH₂ adsorb higher CO₂ (6.8 cm³ g⁻¹) compared to pristine UiO-66(Zr) (5.4 cm³ g⁻¹). MOFs containing polar functional groups tend to have stronger interactions with CO₂ leading to higher adsorption volume.^{66–68} However, at higher pressure (1 bar), physisorption occurs which leads to almost similar overall CO₂ adsorption capacity for UiO-66(Zr)-NH₂ and its pristine form (27.4 cm³ g⁻¹). Nevertheless, CO₂ adsorption capacity of UiO-66(Zr) and its NH₂ functionalized analogs did not change much after shaping into spheres. N₂ uptake of powder and spheres of MOFs is almost same. Moreover, CO₂/N₂ sorption ratios at 1.0 bar were 12, 10.9 and 7 for shaped samples of UiO-66(Zr), UiO-66(Zr)-NH₂ and MIL-101(Cr) respectively, which indicating high affinity for CO₂ over N₂ in all MOF samples tested here. Further research is in progress to evaluate the adsorption behavior of series of gasses over various MRA shaped MOFs bodies. These results

strongly imply that physical as well as chemical properties of MOFs (surface area, functionality and CUSs) remain intact after shaping them into spheres using MRA binder.

3. Conclusions

We successfully fabricated shaped bodies of MIL-100(Fe), MIL-101(Cr), UiO-66(Zr), and UiO-66(Zr)-NH₂ using MRA binder. The MOFs were prepared to have a macroscopic structure on a millimeter scale with small loss of WSSA and increased bulk density. Advanced visualization tools were utilized to unlock the inner complexity of the shaped MOF bodies. It is of interest that the MOF shaped bodies retained their intrinsic properties after shaping, which was confirmed by gas adsorption, NH₃-TPD, and pyridine-IR measurements. The possible adverse effect of the binder on the chemical properties of the shaped MOFs was studied in detail in order to determine their potential for practical applications. Additionally, results of an NH₃ breakthrough test using MIL-100(Fe) spheres and CO₂ adsorption using MIL-101(Cr), UiO-66(Zr) and UiO-66(Zr)-NH₂ spheres showed the potential of our shaping method for use in practical applications for MOFs.

4. Experimental section

4.1. MOF synthesis

4.1.1. Synthesis of MIL-100(Fe). MIL-100(Fe) was synthesized using the scaled-up method previously reported by our research group.¹¹ Briefly, Fe(NO₃)₃·9H₂O was completely



dissolved in water. Then, trimesic acid (BTC) was added to the solution; the resulting mixture was stirred at room temperature for 1 h. The final composition was $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O} : 0.67\text{BTC} : x\text{H}_2\text{O}$ ($x = 55\text{--}280$). The reactant mixture was heated at 433 K for 12 h using a Teflon-lined pressure vessel. The synthesized solid was filtered and washed with deionized (DI) water. Further washing was carried out with DI water and ethanol at 343 K for 3 h and purified with a 38 mM NH_4F solution at 343 K for 3 h. The solid was finally dried overnight at less than 373 K in air.

4.1.2. Synthesis of MIL-101(Cr). MIL-101(Cr) was synthesized according to a previous report.³⁷ In brief, H_2BDC (1 mmol), $\text{Cr}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ (1 mmol), hydrofluoric acid (0.25 mmol), and H_2O (265 mmol) were mixed in a Teflon-lined hydrothermal reactor and heated at 493 K for 8 h. The obtained green solid product was filtered and washed with DI water. Next, the solid was immersed in an ethanol/water mixture (95% ethanol and 5% water) and stirred at 343 K for 24 h. Further purification of the solid was carried out by treating it with a 30 mM aqueous solution of NH_4F at 343 K for 10 h. Finally, the sample was dried at 373 K for 12 h in a vacuum oven.

4.1.3. Synthesis of UiO-66(Zr). The scaled-up synthesis of UiO-66(Zr) was carried out in a 5 L glass reactor (Reactor Master, Syrris, equipped with reflux condenser and a Teflon-lined mechanical stirrer) according to a previously reported method.⁴² In short, 462 g (2.8 mol) of H_2BDC (98%) was initially dissolved in 2.5 L of dimethyl formamide (DMF, 2.36 kg, 32.3 mol) at room temperature. Then, 896 g (2.8 mol) of $\text{ZrOCl}_2 \cdot 8\text{H}_2\text{O}$ (98%) and 465 mL of 37% HCl (548 g, 15 mol) were added to the mixture. The molar ratio of the final $\text{ZrOCl}_2 \cdot 8\text{H}_2\text{O}/\text{H}_2\text{BDC}/\text{DMF}/\text{HCl}$ mixture was 1 : 1 : 11.6 : 5.4. The reaction mixture was vigorously stirred to obtain a homogeneous gel. The mixture was then heated to 423 K at a rate of 1 K min^{-1} and maintained at this temperature for 6 h in the reactor without stirring, leading to a crystalline UiO-66(Zr) solid. The resulting product (~510 g) was recovered from the slurry by filtration, redispersed in 7 L of DMF at 333 K for 6 h under stirring, and recovered by filtration. The same procedure was repeated twice, using methanol (MeOH) instead of DMF. The solid product was finally dried at 373 K overnight.

4.1.4. Synthesis of UiO-66(Zr)-NH₂. UiO-66(Zr)-NH₂ was synthesized by the reflux method. Initially, 250 mL of DMF was poured into a 500 mL round-bottom flask. Next, $\text{ZrOCl}_2 \cdot 8\text{H}_2\text{O}$ (16.11 g, 0.05 mol), 2-amino-1,4-benzenedicarboxylic acid (9.06 g, 0.05 mol), and HCl (8.35 mL, 0.27 mol) were added to the round-bottom flask containing DMF. The reaction solution was heated to 426 K and held at this temperature for 24 h. After cooling to room temperature, the yellow precipitate was filtered off and washed with DMF, followed by MeOH (twice) at 333 K for 2 h to remove unreacted ligand moieties from the pores. The purified yellowish powder was then dried at 373 K in an oven for 12 h.

4.2. Preparation of MRA binder

$\text{Al}(\text{OH})_3$ (7 μm , KC Chemical Corp.) was used as the starting material to prepare mesoporous alumina by the flash pyrolysis

method. The preparation method of the alumina binder was reported by Cho and co-workers.^{35,36} Briefly, $\text{Al}(\text{OH})_3$ was pyrolyzed for a few seconds at 800–1000 K in order to obtain flash-calcined alumina. To achieve such a fast dehydration, $\text{Al}(\text{OH})_3$ was dropped into a tubular furnace under vigorous vibration that had been preheated to the desired temperature. The powder was collected at the bottom of the furnace. The bulk density of the obtained powder was measured to ensure the flash calcination upon dehydration and subsequently was sealed tightly in polypropylene bottle for further use during the hydration in tubular furnace, $\text{Al}(\text{OH})_3$ was converted into mesoporous rehydratable alumina (MRA).

4.3. Preparation of spheres and pellets

Spheres of the various MOFs were prepared using the conventional granulation method. In brief, known amounts of MOF powder (for *e.g.* 10–100 g), MRA binder (5–20 wt% for MOF powder), and dispersion medium (water) were mixed using a hand-made pan-type granulator. During the mixing process, the requisite amount of water was briefly sprayed onto the samples to achieve the desired particle growth. Granules with a wider size distribution were thus produced. After sieving, the granules (2.0–2.5 mm) were rolled using a roller machine to enhance the spherical shape. The samples were then dried from room temperature to 383 K for 12 h in a vacuum oven to remove the water from the spheres.

Pellets were prepared by mixing a known amount of MOF powder (50–100 mg) and 3 wt% graphite binder powder. This powder mixture then transferred into a multiple cylindrical dies (diameter 3 mm, length 10 mm) and the dies were closed using a stainless steel dowels. The assembly was pressed in manual hydraulic press to 5000 psi (34 MPa) and held this pressure for 1 min. The prepared pellets were 3.0 mm in diameter and 4.0 mm in length.

4.4. Characterization

Powder X-ray diffraction patterns of all MOF powders and shaped bodies were obtained by a Rigaku diffractometer (D/MAX IIB, 2 kW) using Ni-filtered Cu K α radiation (40 kV, 30 mA, $\lambda = 1.5406 \text{ \AA}$). The N₂ adsorption isotherms were measured at 77 K using a Micromeritics Tristar 3000 system. The samples were dehydrated under vacuum at 423 K for 12 h prior to analysis. The specific surface areas were evaluated using the Brunauer–Emmett–Teller (BET) method and the pore volume was determined by the single-point method at $p/p_0 = 0.99$. The macro-scale pore-size distribution of the MOF spheres was measured using a mercury porosimeter (Micromeritics, Autopore III 9420). The sphere densities were estimated from the mass and physical dimensions of individual spheres. Ten well-shaped spheres were selected to calculate the average sphere density. The crushing strengths of the spheres and pellets were measured using the strength meter described in our previous paper.²² For each sample, the average crushing strength of at least 10 individual spheres or pellets was considered. The internal cross sections of the spheres were examined to study the distribution of the binder particles, as well as their arrangements with MOF



particles, using scanning electron microscopy (SEM) (Tescan Mira 3 LMU FEG with an accelerating voltage of 10 kV) and X-ray energy-dispersive spectroscopy (EDS) (Bruker, Quantax 200 equipped with a Si Drift Detector). Scanning transmission electron microscopy (STEM)-EDS measurements were taken on a FEI Tecnai G2 T20 S microscope with an accelerating voltage of 200 kV. The NH₃ temperature-programmed desorption (TPD) profiles of the binders, MOF powders, and spheres were measured on a Micromeritics AutoChem II 2920 V3.05 system equipped with a thermal conductivity detector. Samples were activated at 523 K for 12 h in He flow prior to the adsorption step. Subsequently, the activated samples were exposed to NH₃ at 373 K for 1 h at a flow rate of 50 mL min⁻¹. Physically adsorbed NH₃ was removed by purging with helium gas at the same temperature for 1 h. TPD data was recorded from 313 to 673 K at a heating rate of 5 K min⁻¹. The Fourier-transform infrared (FT-IR) spectra of adsorbed pyridine (Aldrich, 99.8%) were obtained at room temperature using a Nicolet FT-IR spectrometer (iS50). For this purpose, the MIL-100(Fe) powder was pelletized to a wafer (10 mg cm⁻²) and evacuated for 2 h at 423 K and 523 K under vacuum (~10⁻⁶ Torr), respectively. After the adsorption of pyridine at room temperature, the adsorbed pyridine was evacuated for 30 min at 298–523 °C, respectively. For temperature-dependent FT-IR analyses, samples were pressed into self-supported wafers and the spectra were recorded at 323 K after evacuation for 2 h under vacuum (~10⁻⁶ Torr) at the same temperature.

4.5. Ammonia breakthrough test

To perform the NH₃ breakthrough test, ~0.246 mL of 60–70-mesh-sieved samples was loaded into a 3.96 mm (i.d.) quartz tube reactor. Before the breakthrough test, each sample was activated for 12 h at 423 K under 20 mL min⁻¹ He flow. The concentration of the mixed ammonia/air balanced gas was 1000 ppm and the total flow rate was 43.6 mL min⁻¹. The contact time and linear velocity of the 1000 ppm NH₃/air mixture gas penetrating the samples were 0.399 s and 5.9 cm s⁻¹, respectively. During the breakthrough test for ammonia, the concentration of effluent gas was determined using a tunable diode-laser NH₃ gas detector. The amount of adsorbed NH₃ was calculated by integrating the breakthrough curve for the sample subtracted from the integration of the breakthrough curve for the blank test.

4.6. CO₂ adsorption

CO₂ sorption isotherms of MOFs were measured up to 1 bar using a Micromeritics Tristar 3020 analyzer. Before the measurements, the sample (~150 mg) was degassed under reduced pressure at 423 K for 12 h. The CO₂ adsorption volumes for MOFs at 298 K were then measured.

Conflicts of interest

There are no conflicts to declare.

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References

- 1 J. A. Mason, M. Veenstra and J. R. Long, *Chem. Sci.*, 2014, **5**, 32–51.
- 2 J. R. Li, R. J. Kuppler and H. C. Zhou, *Chem. Soc. Rev.*, 2009, **38**, 1477–1504.
- 3 L. E. Kreno, K. Leong, O. K. Farha, M. Allendorf, R. P. Van Duyne and J. T. Hupp, *Chem. Rev.*, 2012, **112**, 1105–1125.
- 4 J. Liu, L. Chen, H. Cui, J. Zhang, L. Zhang and C. Y. Su, *Chem. Soc. Rev.*, 2014, **43**, 6011–6061.
- 5 A. H. Valekar, K.-H. Cho, S. K. Chitale, D.-Y. Hong, G.-Y. Cha, U.-H. Lee, D. W. Hwang, C. Serre, J.-S. Chang and Y. K. Hwang, *Green Chem.*, 2016, **18**, 4542–4552.
- 6 G. Ferey, *Chem. Soc. Rev.*, 2008, **37**, 191–214.
- 7 M. Eddaoudi, J. Kim, N. Rosi, D. Vodak, J. Wachter, M. O’Keeffe and O. M. Yaghi, *Science*, 2002, **295**, 469–472.
- 8 D. Y. Hong, Y. K. Hwang, C. Serre, G. Ferey and J. S. Chang, *Adv. Funct. Mater.*, 2009, **19**, 1537–1552.
- 9 A. U. Czaja, N. Trukhan and U. Muller, *Chem. Soc. Rev.*, 2009, **38**, 1284–1293.
- 10 N. Stock and S. Biswas, *Chem. Rev.*, 2012, **112**, 933–969.
- 11 Y. K. Seo, J. W. Yoon, J. S. Lee, U. H. Lee, Y. K. Hwang, C. H. Jun, P. Horcajada, C. Serre and J. S. Chang, *Microporous Mesoporous Mater.*, 2012, **157**, 137–145.
- 12 F. Ragon, P. Horcajada, H. Chevreau, Y. K. Hwang, U. H. Lee, S. R. Miller, T. Devic, J. S. Chang and C. Serre, *Inorg. Chem.*, 2014, **53**, 2491–2500.
- 13 R. Zacharia, D. Cossement, L. Lafi and R. Chahine, *J. Mater. Chem.*, 2010, **20**, 2145–2151.
- 14 A. M. Ribeiro, M. C. Campo, G. Narin, J. C. Santos, A. Ferreira, J. S. Chang, Y. K. Hwang, Y. K. Seo, U. H. Lee, J. M. Loureiro and A. E. Rodrigues, *Sep. Purif. Technol.*, 2013, **110**, 101–111.
- 15 A. F. P. Ferreira, J. C. Santos, M. G. Plaza, N. Lamia, J. M. Loureiro and A. E. Rodrigues, *Chem. Eng. J.*, 2011, **167**, 1–12.
- 16 M. G. Plaza, A. M. Ribeiro, A. Ferreira, J. C. Santos, U. H. Lee, J. S. Chang, J. M. Loureiro and A. E. Rodrigues, *Sep. Purif. Technol.*, 2012, **90**, 109–119.
- 17 A. Carne-Sanchez, I. Imaz, M. Cano-Sarabia and D. Maspoch, *Nat. Chem.*, 2013, **5**, 203–211.
- 18 Y. H. Hu and L. Zhang, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 2010, **81**, 174103–174105.
- 19 K. W. Chapman, G. J. Halder and P. J. Chupas, *J. Am. Chem. Soc.*, 2009, **131**, 17546–17547.
- 20 A. I. Spjellkavik, Aarti, S. Divekar, T. Didriksen and R. Blom, *Chem.–Eur. J.*, 2014, **20**, 8973–8978.



- 21 D. Crawford, J. Casaban, R. Haydon, N. Giri, T. McNally and S. L. James, *Chem. Sci.*, 2015, **6**, 1645–1649.
- 22 P. J. Kim, Y. W. You, H. Park, J. S. Chang, Y. S. Bae, C. H. Lee and J. K. Suh, *Chem. Eng. J.*, 2015, **262**, 683–690.
- 23 N. Chanut, A. D. Wiersum, U.-H. Lee, Y. K. Hwang, F. Ragon, H. Chevreau, S. Bourrelly, B. Kuchta, J.-S. Chang, C. Serre and P. L. Llewellyn, *Eur. J. Inorg. Chem.*, 2016, 4416–4423.
- 24 U.-H. Lee, A. H. Valekar, Y. K. Hwang and J.-S. Chang, in *The Chemistry of Metal–Organic Frameworks: Synthesis, Characterization, and Applications*, ed. S. Kaskel, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim, Germany, 2016, pp. 551–572.
- 25 M. A. Moreira, J. C. Santos, A. F. P. Ferreira, J. M. Loureiro, F. Ragon, P. Horcajada, K.-E. Shim, Y.-K. Hwang, U.-H. Lee, J.-S. Chang, C. Serre and A. E. Rodrigues, *Langmuir*, 2012, **28**, 5715–5723.
- 26 M. Wickenheisser, T. Paul and C. Janiak, *Microporous Mesoporous Mater.*, 2016, **220**, 258–269.
- 27 M. Wickenheisser and C. Janiak, *Microporous Mesoporous Mater.*, 2015, **204**, 242–250.
- 28 A. Permyakova, O. Skrylnyk, E. Courbon, M. Affram, S. Wang, U.-H. Lee, A. H. Valekar, F. Nouar, G. Mouchaham, T. Devic, G. De Weireld, J.-S. Chang, N. Steunou, M. Frère and C. Serre, *ChemSusChem*, 2017, **10**, 1419–1426.
- 29 A. Perea-Cachero, J. Dechnik, R. Lahoz, C. Janiak, C. Telleza and J. Coronas, *CrystEngComm*, 2017, **19**, 1470–1478.
- 30 D. Frohlich, E. Pantatosaki, P. D. Kolokathis, K. Markey, H. Reinsch, M. Baumgartner, M. A. Veen, D. E. De Vos, N. Stock, G. K. Papadopoulos, S. K. Henninger and C. Janiak, *J. Mater. Chem. A*, 2016, **4**, 11859–11869.
- 31 F. Jeremias, D. Frohlich, C. Janiak and S. K. Henninger, *RSC Adv.*, 2014, **4**, 24073–24082.
- 32 F. Jeremias, S. K. Henninger and C. Janiak, *Chem. Commun.*, 2012, **48**, 9708–9710.
- 33 D. Bazer-Bachi, L. Assie, V. Lecocq, B. Harbuzaru and V. Falk, *Powder Technol.*, 2014, **255**, 52–59.
- 34 G. W. Peterson, J. B. DeCoste, T. G. Glover, Y. G. Huang, H. Jasuja and K. S. Walton, *Microporous Mesoporous Mater.*, 2013, **179**, 48–53.
- 35 I. J. Jang, H. S. Shin, N. R. Shin, S. H. Kim, S. K. Kim, M. J. Yu and S. J. Cho, *Catal. Today*, 2012, **185**, 198–204.
- 36 H. J. Lee, J. H. Kim, D.-W. Park and S. J. Cho, *Appl. Catal., A*, 2015, **502**, 42–47.
- 37 G. Ferey, C. Mellot-Draznieks, C. Serre, F. Millange, J. Dutour, S. Surble and I. Margiolaki, *Science*, 2005, **309**, 2040–2042.
- 38 I. T. Cameron, F. Y. Wang, C. D. Immanuel and F. Stepanek, *Chem. Eng. Sci.*, 2005, **60**, 3723–3750.
- 39 P. R. Mort, *Powder Technol.*, 2005, **150**, 86–103.
- 40 S. M. Iveson, J. D. Litster, K. Hapgood and B. J. Ennis, *Powder Technol.*, 2001, **117**, 3–39.
- 41 G. Ferey, C. Serre, C. Mellot-Draznieks, F. Millange, S. Surble, J. Dutour and I. Margiolaki, *Angew. Chem., Int. Ed.*, 2004, **43**, 6296–6301.
- 42 J. H. Cavka, S. Jakobsen, U. Olsbye, N. Guillou, C. Lamberti, S. Bordiga and K. P. Lillerud, *J. Am. Chem. Soc.*, 2008, **130**, 13850–13851.
- 43 M. Kandiah, M. H. Nilsen, S. Usseglio, S. Jakobsen, U. Olsbye, M. Tilset, C. Larabi, E. A. Quadrelli, F. Bonino and K. P. Lillerud, *Chem. Mater.*, 2010, **22**, 6632–6640.
- 44 G. K. Reynolds, J. S. Fu, Y. S. Cheong, M. J. Hounslow and A. D. Salman, *Chem. Eng. Sci.*, 2005, **60**, 3969–3992.
- 45 Y. K. Hwang, D. Y. Hong, J. S. Chang, S. H. Jhung, Y. K. Seo, J. Kim, A. Vimont, M. Daturi, C. Serre and G. Ferey, *Angew. Chem., Int. Ed.*, 2008, **47**, 4144–4148.
- 46 H. Leclerc, A. Vimont, J. C. Lavalley, M. Daturi, A. D. Wiersum, P. L. Llewellyn, P. Horcajada, G. Ferey and C. Serre, *Phys. Chem. Chem. Phys.*, 2011, **13**, 11748–11756.
- 47 A. Vimont, J.-M. Goupil, J.-C. Lavalley, M. Daturi, S. Surble, C. Serre, F. Millange, G. Ferey and N. Audebrand, *J. Am. Chem. Soc.*, 2006, **128**, 3218–3227.
- 48 S. Mitchell, N. L. Michels, G. Majano and J. Perez-Ramirez, *Curr. Opin. Chem. Eng.*, 2013, **2**, 304–311.
- 49 S. Mitchell, N. L. Michels, K. Kunze and J. Perez-Ramirez, *Nat. Chem.*, 2012, **4**, 825–831.
- 50 H. Friedrich, C. J. Gommers, K. Overgaag, J. D. Meeldijk, W. H. Evers, B. de Nijs, M. P. Boneschanscher, P. E. de Jongh, A. J. Verkleij, K. P. de Jong, A. van Blaaderen and D. Vanmaekelbergh, *Nano Lett.*, 2009, **9**, 2719–2724.
- 51 M. H. Kox, K. F. Domke, J. P. Day, G. Rago, E. Stavitski, M. Bonn and B. M. Weckhuysen, *Angew. Chem., Int. Ed.*, 2009, **48**, 8990–8994.
- 52 M. W. Zandbergen, S. D. Jacques, B. M. Weckhuysen and A. M. Beale, *Angew. Chem., Int. Ed.*, 2012, **51**, 957–960.
- 53 R. Canioni, C. Roch-Marchal, F. Secheresse, P. Horcajada, C. Serre, M. Hardi-Dan, G. Ferey, J. M. Greneche, F. Lefebvre, J. S. Chang, Y. K. Hwang, O. Lebedev, S. Turnerf and G. V. Tendeloo, *J. Mater. Chem.*, 2011, **21**, 1226–1233.
- 54 M. Latroche, S. Surble, C. Serre, C. Mellot-Draznieks, P. L. Llewellyn, J. H. Lee, J. S. Chang, S. H. Jhung and G. Ferey, *Angew. Chem., Int. Ed.*, 2006, **45**, 8227–8231.
- 55 M. G. Plaza, A. M. Ribeiro, A. Ferreira, J. C. Santos, Y. K. Hwang, Y. K. Seo, U. H. Lee, J. S. Chang, J. M. Loureiro and A. E. Rodrigues, *Microporous Mesoporous Mater.*, 2012, **153**, 178–190.
- 56 Y. K. Seo, J. W. Yoon, J. S. Lee, Y. K. Hwang, C. H. Jun, J. S. Chang, S. Wuttke, P. Bazin, A. Vimont, M. Daturi, S. Bourrelly, P. L. Llewellyn, P. Horcajada, C. Serre and G. Ferey, *Adv. Mater.*, 2012, **24**, 806–810.
- 57 M. Wickenheisser, A. Herbst, R. Tannert, B. Milow and C. Janiak, *Microporous Mesoporous Mater.*, 2015, **215**, 143–153.
- 58 C. Petit and T. J. Bandoz, *Adv. Funct. Mater.*, 2011, **21**, 2108–2117.
- 59 N. L. Michels, S. Mitchell, M. Milina, K. Kunze, F. Krumeich, F. Marone, M. Erdmann, N. Marti and J. Perez-Ramirez, *Adv. Funct. Mater.*, 2012, **22**, 2509–2518.
- 60 E. Barea, C. Montoro and J. A. Navarro, *Chem. Soc. Rev.*, 2014, **43**, 5419–5430.
- 61 J. B. DeCoste and G. W. Peterson, *Chem. Rev.*, 2014, **114**, 5695–5727.
- 62 G. W. Peterson, J. B. DeCoste, F. Fatollahi-Fard and D. K. Britt, *Ind. Eng. Chem. Res.*, 2013, **53**, 701–707.



- 63 J. W. Yoon, Y. K. Seo, Y. K. Hwang, J. S. Chang, H. Leclerc, S. Wuttke, P. Bazin, A. Vimont, M. Daturi, E. Bloch, P. L. Llewellyn, C. Serre, P. Horcajada, J. M. Greneche, A. E. Rodrigues and G. Ferey, *Angew. Chem., Int. Ed.*, 2010, **49**, 5949–5952.
- 64 K. Sumida, D. L. Rogow, J. A. Mason, T. M. McDonald, E. D. Bloch, Z. R. Herm, T.-H. Bae and J. R. Long, *Chem. Rev.*, 2012, **112**, 724–781.
- 65 S. S. Myers, A. Zanolotti, I. Kloog, P. Huybers, A. D. Leakey, A. J. Bloom, E. Carlisle, L. H. Dietterich, G. Fitzgerald and T. Hasegawa, *Nature*, 2014, **510**, 139–142.
- 66 Z. Hu, Y. Peng, Z. Kang, Y. Qian and D. Zhao, *Inorg. Chem.*, 2015, **54**, 4862–4868.
- 67 J. Shen, G. Liu, K. Huang, Q. Li, K. Guan, Y. Li and W. Jin, *J. Membr. Sci.*, 2016, **513**, 155–165.
- 68 X. Wang, H. Li and X.-J. Hou, *J. Phys. Chem. C*, 2012, **116**, 19814–19821.

