## **INORGANIC** CHEMISTRY







**FRONTIERS** 

## **RESEARCH ARTICLE**

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**Cite this:** *Inorg. Chem. Front.*, 2025, **12**, 701

# Exploration of functional group effects on $D_2/H_2$ separation selectivity within the UiO-66 framework†

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The efficient separation of deuterium from hydrogen remains a significant challenge due to the limitations of conventional techniques, such as cryogenic distillation and the Girdler-sulfide process combined with electrolysis, which are char-acterized by substantial energy demands and relatively low separation coefficients. In contrast, the quantum sieving effect, based on porous materials, offers a promising approach to overcoming these challenges. This study presents a novel application of strong adsorption sites ( $\mu_3$ -OH group) within the nanoporous metal-organic framework of **UiO-66** for hydrogen isotope separation. By incorporating diverse organic functional groups into **UiO-66**, we successfully synthesized four derivative materials: **UiO-66-NH2**, **UiO-66-CH3**, **UiO-66-NO2**, and **UiO-66-Ph**. Experimental data reveal that the introduction of these functional groups modulated the material's pore size and channel polarity, significantly impacting its adsorption and separation performance for hydrogen isotopes. Notably, **UiO-66-NH2**, with the smallest pore size and highest channel polarity, exhibited superior hydrogen isotope adsorption capacity and selectivity, highlighting its potential as an effective adsorbent for isotope separation.

Received 5th November 2024, Accepted 2nd December 2024 DOI: 10.1039/d4qi02802c

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## Introduction

Deuterium (<sup>2</sup>H, D), a stable isotope of hydrogen (<sup>1</sup>H, H), has been widely utilized in modern industry, scientific research, and as a fuel for nuclear fusion. <sup>1-5</sup> However, its extremely low natural abundance (0.0156%) and near-identical physicochemical properties with other hydrogen isotopes present significant challenges for enrichment. To date, only a few large-scale techniques have been employed for the industrial purification of deuterium. These include electrolysis of heavy water extracted *via* the Girdler-sulfide process and cryogenic distillation at 24 K. Both methods are known to be highly time-consuming and energy-intensive, with relatively low separation efficiencies. This necessitates the exploration of alternative approaches that can meet the requirements for sustainable deuterium production. <sup>6</sup>

One of the most promising alternatives for  $D_2/H_2$  separation is quantum sieving (QS) based on nanoporous materials.

Kinetic quantum sieving (KQS) and chemical affinity quantum sieving (CAQS) effects are often used to achieve high selectivity in hydrogen isotope separation.<sup>7–20</sup> KQS occurs when the difference between pore size and molecular size becomes comparable to the de Broglie wavelength under cryogenic conditions, leading to faster D<sub>2</sub> diffusion through nanoporous material channels. However, the KQS effect demonstrates significant isotope selectivity only at cryogenic temperatures, limiting its practical application. To increase operating temperature, the CAQS effect has been developed. In this process, heavier isotopes are selectively adsorbed at strong binding sites due to differences in zero-point energy (ZPE).

The most extensively studied class of CAQS materials for  $D_2/H_2$  separation is Metal-Organic Frameworks (MOFs). MOFs allow for flexible adjustment of pore size and open metal sites to achieve high  $D_2/H_2$  selectivity. Some MOFs with a high density of metal open sites have successfully achieved efficient  $D_2/H_2$  separation. However, most MOFs containing open metal sites suffer from limited moisture stability, as water readily attacks the metal active sites, leading to material degradation.

Therefore, effectively utilizing the CAQS effect to enhance  $D_2/H_2$  separation performance while maintaining MOF structural stability is a critical issue that needs addressing. **UiO-66**, a well-known zirconium(IV)-containing MOF, has attracted con-

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<sup>†</sup>Electronic supplementary information (ESI) available. See DOI: https://doi.org/10.1039/d4qi02802c

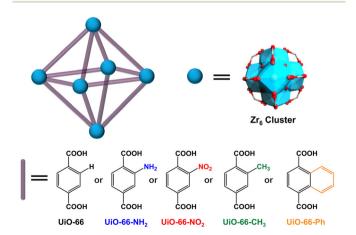
siderable attention due to its exceptional stability, excellent adsorption properties, cost-effective regenerability, and good functional-group tolerance during synthesis. Despite the absence of open metal sites in UiO-66, the  $\mu_3$ -OH group of the Zr<sub>6</sub>O<sub>4</sub>(OH)<sub>4</sub> inorganic cornerstones can serve as strong interaction sites, facilitating intense interactions between the material and hydrogen or deuterium.29

Current research on CAOS primarily focuses on open metal sites, while exploration of interactions between hydrogen isotope gases and non-metal active centers remains limited. This study reports the synthesis of UiO-66 and four of its derivatives (UiO-66-NH<sub>2</sub>, UiO-66-NO<sub>2</sub>, UiO-66-CH<sub>3</sub>, UiO-66-Ph), along with a detailed analysis of their D<sub>2</sub>/H<sub>2</sub> separation capabilities (Scheme 1). Our findings indicate that the incorporation of functional groups into UiO-66 leads to improved separation performance.

#### Results and discussion

The synthesis of UiO-66 and its derivatives was conducted following a modified procedure based on previously published literature.<sup>30</sup> As shown in Fig. 1a, the powder X-ray diffraction (PXRD) patterns of the synthesized materials were compared with simulated PXRD patterns, revealing good phase purity and functional-group tolerance for UiO-66 and its derivatives. Infrared spectroscopic analysis of the derivatives confirmed the successful incorporation of the intended functional groups, as evidenced by characteristic peaks (Fig. S1†).

The porosity of UiO-66 and its derivatives was assessed using nitrogen adsorption isotherms at 77 K. Both UiO-66 and its derivatives displayed typical type I isotherms, indicating their microporous structures (Fig. 1b). The nitrogen adsorption capacities were measured as follows: 328 cm<sup>3</sup> g<sup>-1</sup> for UiO-66, 291 cm<sup>3</sup> g<sup>-1</sup> for UiO-66-NO<sub>2</sub>, 295 cm<sup>3</sup> g<sup>-1</sup> for UiO-66- $NH_2$ , 262 cm<sup>3</sup> g<sup>-1</sup> for UiO-66-CH<sub>3</sub>, and 252 cm<sup>3</sup> g<sup>-1</sup> for UiO-66-Ph. The corresponding specific surface areas determined by the Brunauer-Emmett-Teller (BET) method were



Scheme 1 Synthetic process of pristine UiO-66 and its isoreticular derivatives

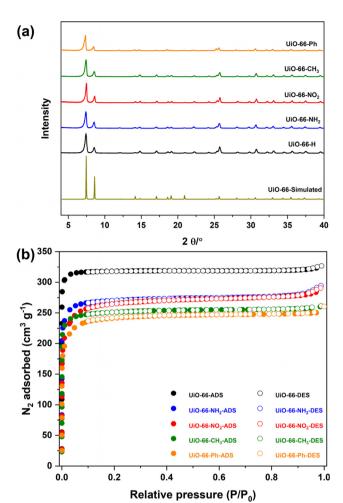


Fig. 1 (a) Simulated and observed PXRD patterns of UiO-66 and its derivatives; (b) N<sub>2</sub> isotherms of UiO-66 and its derivatives at 77 K.

found to be 1250 m<sup>2</sup> g<sup>-1</sup> for **UiO-66**, 985 m<sup>2</sup> g<sup>-1</sup> for **UiO-66**–  $NO_2$ , 1036 m<sup>2</sup> g<sup>-1</sup> for UiO-66-NH<sub>2</sub>, 960 m<sup>2</sup> g<sup>-1</sup> for UiO-66-CH<sub>3</sub>, and 902 m<sup>2</sup> g<sup>-1</sup> for UiO-66-Ph. These data indicate that UiO-66 has the highest BET surface area, with the addition of different functional groups resulting in varying degrees of reduction in specific surface area.

The pore size distribution (PSD) was further analyzed using density functional theory (DFT) calculations. The results demonstrated that the derivatives (UiO-66-NO2, UiO-66-NH2, and UiO-66-CH<sub>3</sub>) possess smaller pore sizes than pristine UiO-66 (Fig. S2†). Contrary to expectations based on group size, UiO-66-Ph would be expected to have a smaller pore size than the other derivatives. However, the opposite result is observed. This discrepancy could be attributed to the orientation of the benzene rings and the presence of defects within the material, which together permit the formation of larger pore sizes.

The high BET values and microporous structures of UiO-66 and its derivatives motivate our investigation into their adsorption capacities for hydrogen isotopes. The initial stage of the study involved analyzing H2 and D2 gas adsorption data at

temperatures of 77 K and 87 K (Fig. 2 and Table S1†). Due to the change in mass induced by the introduction of functional groups, the amount of adsorbed gas per unit cell was selectively used as a measure of the material's adsorption performance.

At 77 K and 110 kPa, the D<sub>2</sub> adsorption capacities of UiO-66-NH2 and UiO-66-CH3 were nearly equivalent to that of UiO-66, with UiO-66-NO2 showing a slight decrease and UiO-66-Ph exhibiting the most substantial reduction. For H<sub>2</sub> adsorption under identical conditions, the H2 adsorption capacity of UiO-66-NH2 was comparable to that of UiO-66, while both UiO-66-CH3 and UiO-66-NO2 experienced minor decreases, with UiO-66-Ph demonstrating the most significant decline. Notably, at low pressures, the H2 and D2 gas adsorption capacities of UiO-66-NH2, UiO-66-NO2, and UiO-66-CH3 exceeded those of the pristine material UiO-66, indicating an enhanced interaction with hydrogen isotope gases despite the decrease in BET values.

A significant shift in isotope gas adsorption behavior was observed at 87 K. For D<sub>2</sub> adsorption, UiO-66-NH<sub>2</sub> and UiO-66-CH<sub>3</sub> exhibited higher capacities across the entire pressure range compared to UiO-66. UiO-66-NO2 showed increased adsorption in the low-pressure region, with its capacity at 110 kPa nearly matching that of UiO-66, while UiO-66-Ph maintained a lower capacity throughout. The H2 adsorption behavior at 87 K followed a similar pattern to D<sub>2</sub>. As the temperature rose to 87 K, the decrease in H<sub>2</sub> and D<sub>2</sub> adsorption performance for UiO-66-NH2 and UiO-66-CH3 was less than that of UiO-66, suggesting that organic functional groups effectively enhanced the material's affinity for hydrogen isotopes. The reduced adsorption performance of UiO-66-Ph can be primarily attributed to its lower specific surface area and microporous volume (Table S1†).

Additionally, D<sub>2</sub> adsorption capacities at both 77 K and 87 K were higher than those of H<sub>2</sub>, pointing to quantum effects. The isotherms for both H2 and D2 adsorption comple-

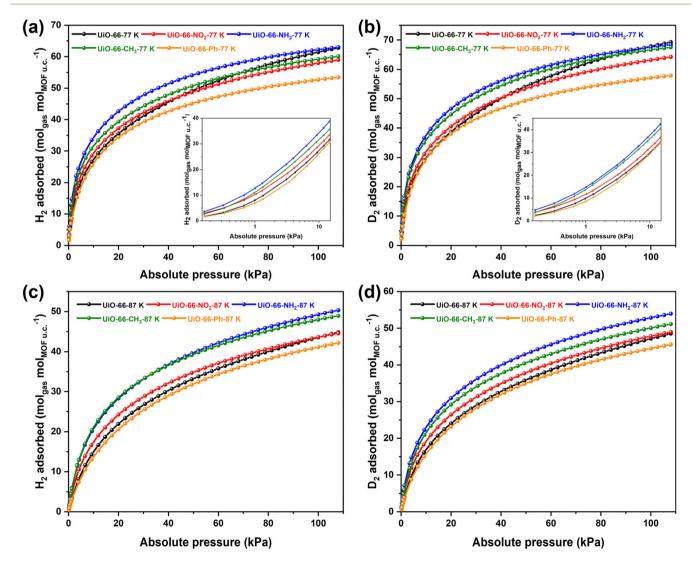


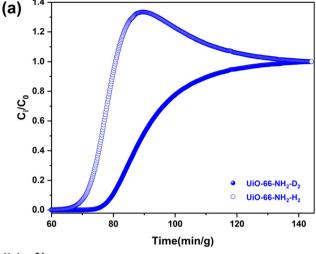
Fig. 2 (a) 77 K H<sub>2</sub>; (b) 77 K D<sub>2</sub>; (c) 87 K H<sub>2</sub> and (d) 87 K D<sub>2</sub> adsorption isotherms of UiO-66 and its derivatives. Inset: Enlarged perspective on the low-pressure section of the adsorption isotherms for H<sub>2</sub> and D<sub>2</sub> at 77 K.

tely overlapped, indicating no diffusion barrier for hydrogen isotopes within the pores. The primary cause of the differential adsorption between H2 and D2 is attributed to strong adsorption sites, predominantly driven by the interaction between the hydrogen isotope gases and the  $\mu_3$ -OH group of the Zr<sub>6</sub>O<sub>4</sub>(OH)<sub>4</sub> inorganic cornerstones. The incorporation of organic functional groups (-NH2, -CH3, -NO2) has effectively modulated pore size and polarity, further enhancing the material's interaction with isotope gases.

To gain further insight into the affinity of UiO-66 and its derivatives for hydrogen isotopes, the isosteric heats of adsorption  $(Q_{st})$  were calculated (Fig. S3-S14†). At zero loading, the  $Q_{\rm st}$  values for  $D_2$  in UiO-66-NH<sub>2</sub> (9.3 kJ mol<sup>-1</sup>), UiO-66-NO<sub>2</sub>  $(8.9 \text{ kJ mol}^{-1})$ , and **UiO-66-CH**<sub>3</sub>  $(9.0 \text{ kJ mol}^{-1})$  were higher than those of pristine UiO-66 (8.7 kJ mol<sup>-1</sup>). Notably, the  $Q_{\rm st}$ value for D2 in UiO-66-NH2 exceeds that of some porous materials reported in the literature, such as USTC-700 (4.0 kJ  $\text{mol}^{-1}$ ), <sup>31</sup> **FJI-Y9** (6.2 kJ  $\text{mol}^{-1}$ ), <sup>32</sup> **FJI-Y11** (7.9 kJ  $\text{mol}^{-1}$ ), <sup>33</sup> FIR-29 (6.1 kJ mol<sup>-1</sup>),<sup>32</sup> Co(pyz)[Pt(CN)<sub>4</sub>] (8.0 kJ mol<sup>-1</sup>),<sup>34</sup> and Cu-BDC-NH<sub>2</sub> (7.1 kJ mol<sup>-1</sup>).<sup>35</sup> The high adsorption enthalpy of UiO-66-NH2 is predominantly attributed to its smaller pore size distribution and channel polarity. However, the  $Q_{\rm st}$  value for D<sub>2</sub> in UiO-66-Ph (8.3 kJ mol<sup>-1</sup>) was lower than that in UiO-66 due to its low pore volume and reduced channel polarity. These findings are similarly applicable to the  $Q_{\rm st}$ values of H2. Compared with UiO-66 and other derivatives, a larger  $\Delta Q_{\rm st}$  (0.6 kJ mol<sup>-1</sup>) between D<sub>2</sub> and H<sub>2</sub> in UiO-66-NH<sub>2</sub> suggests that this material may possess good D2/H2 separation properties.

To investigate the practical separation performance of UiO-66-NH2, breakthrough studies were conducted on D2/H2/Ne (3-3-94, v/v) ternary mixtures at 77 K (Fig. S15-S18†). The results showed that H<sub>2</sub> broke through the adsorption bed first, followed by a time lag before D<sub>2</sub> slowly eluted and reached equilibrium. This indicates that UiO-66-NH2 preferentially adsorbs D2 over H<sub>2</sub>. Additionally, a roll-up behavior for H<sub>2</sub> was observed, likely due to the partial replacement of adsorbed H<sub>2</sub> on the adsorption sites by more strongly adsorbing  $D_2$  in the gas mixture (Fig. 3a).

Furthermore, the separation performance of UiO-66 and other derivatives has also been characterized. Breakthrough experiments suggest that materials modified with organic functional groups generally show improved separation performance. However, while UiO-66-CH3, UiO-66-NO2, and UiO-66-Ph exhibited increased separation coefficients compared to UiO-66, they experienced a decrease in H2 adsorption capacity to varying degrees. In contrast, UiO-66-NH2 maintained high D2 adsorption capacity while also enhancing selectivity. For an equimolar mixture of D<sub>2</sub>/H<sub>2</sub>, the calculated separation factor was 1.38 (Fig. 3b, Table S2†). For practical industrial application, it is crucial that the ideal adsorbent have good recycling performance. Multiple D<sub>2</sub>/H<sub>2</sub> mixed-gas dynamic breakthrough experiments were performed under consistent operating conditions. The separation performance of D<sub>2</sub>/H<sub>2</sub> did not significantly change within three continuous cycles, indicating that UiO-66-NH2 is robust and a promising candidate for  $D_2/H_2$  separation (Fig. S19†).



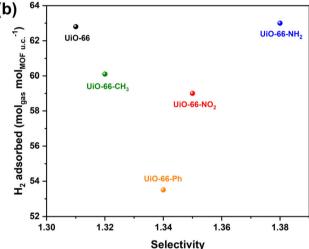


Fig. 3 (a) The dynamic breakthrough curves of UiO-66-NH<sub>2</sub>; (b) comparison of H<sub>2</sub> uptake and separation factor for UiO-66 and its derivatives.

## Conclusions

This study delves into the influence of incorporating various organic functional groups into the UiO-66 framework on the adsorption-separation efficiency for hydrogen isotopes. The findings substantiate that by selectively modifying the pore size and channel polarity through the strategic introduction of organic functional groups, a substantial enhancement in the material's affinity for hydrogen isotopes can be achieved, thereby improving its overall separation performance. Notably, UiO-66-NH<sub>2</sub> emerges as an outstanding candidate due to its high capacity for adsorbing hydrogen isotopes and superior selectivity. This research underscores that, aside from the presence of metal open sites, precise adjustment of pore size and channel polarity is a viable strategy to elevate the separation performance of hydrogen isotopes in CAQS studies. UiO-66-NH<sub>2</sub> demonstrates exceptional potential for isotope separation applications, highlighting the importance of tailored material modifications in enhancing adsorption-separation efficiency.

## **Experimental**

#### Materials and general methods

Infrared (IR) spectra were collected using KBr pellets over a range of  $3000\text{-}400~\text{cm}^{-1}$ , recorded on a Nicolet Magna 750 FT-IR spectrometer. Powder X-ray diffraction (PXRD) patterns were obtained using Cu K $\alpha$  radiation ( $\lambda$  = 1.5406 Å) on a Rigaku Mini 600 X-ray diffractometer. Gas adsorption–desorption measurements were conducted with an automatic volumetric adsorption apparatus (Micromeritics, ASAP2020 PLUS).

#### Synthesis of UiO-66 and its derivatives

In a typical synthesis, terephthalic acid (9.3 mg, 0.08 mmol) and  $\rm ZrCl_4$  (13.2 mg, 0.04 mmol) were ultrasonically dissolved in a 10 mL solution of *N,N*-dimethylformamide (DMF), followed by the addition of 2.3 mL of acetic acid. The resulting mixture was then transferred into a sealed vial and heated at 120 °C for 24 hours. After gradually cooling to room temperature, the white powders were collected. Yield: 7.5 mg, 80%. Synthesis of other derivatives followed a similar procedure, with substitutions on the terephthalic acid to introduce the corresponding functional groups on the organic ligand.

#### **Breakthrough measurements**

The breakthrough experiments were carried out using a dynamic gas breakthrough equipment (BSD Instrument, BSD-MAB). Activated samples were carefully transferred into a 2 mL quartz column, which was sealed at both ends with quartz wool. The column was subsequently heated to 100 °C for 12 hours, with a flow of Ne gas at 8 mL min<sup>-1</sup> passing through it. Prior to the measurement, the column was precooled by immersed in a Dewar flask containing liquid nitrogen for approximately 20 minutes. After this preparation, a gas mixture of H<sub>2</sub>/D<sub>2</sub>/Ne (3/3/94, vol%) was introduced into the column at a flow rate of 15 mL min<sup>-1</sup>. The inlet gas flow was precisely managed by a mass flow controller (MFC), and the outlet gas composition was continuously monitored using a mass spectrometer. To regenerate the sample, it was purged with Ne gas at 10 mL min<sup>-1</sup> at a temperature of 100 °C for 120 minutes.

## Data availability

The data supporting this article have been included as part of the ESI.†

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This work was supported by National Nature Science Foundation of China (22275191, 22275186); the Self-deploy-

ment Project Research Program of Haixi Institutes, Chinese Academy of Sciences (CXZX-2022-GH01, CXZX-2022-JQ11); the Nature Science Foundation of Fujian Province (No. 2022I0037).

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