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# Origin of the N-coordinated single-atom Ni sites in heterogeneous electrocatalysts for CO<sub>2</sub> reduction reaction†

Yu Wang,  ‡<sup>a</sup> Liming You<sup>a</sup> and Kun Zhou  \*<sup>ab</sup>

Heterogeneous Ni–N–C single-atom catalysts (SACs) have attracted great research interest regarding their capability in facilitating the CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR), with CO accounting for the major product. However, the fundamental nature of their active Ni sites remains controversial, since the typically proposed pyridinic-type Ni configurations are inactive, display low selectivity, and/or possess an unfavorable formation energy. Herein, we present a constant-potential first-principles and microkinetic model to study the CO<sub>2</sub>RR at a solid–water interface, which shows that the electrode potential is crucial for governing CO<sub>2</sub> activation. A formation energy analysis on several NiN<sub>x</sub>C<sub>4–x</sub> (x = 1–4) moieties indicates that the predominant Ni moieties of Ni–N–C SACs are expected to have a formula of NiN<sub>4</sub>. After determining the potential-dependent thermodynamic and kinetic energy of these Ni moieties, we discover that the energetically favorable pyrrolic-type NiN<sub>4</sub> moiety displays high activity for facilitating the selective CO<sub>2</sub>RR over the competing H<sub>2</sub> evolution. Moreover, model polarization curves and Tafel analysis results exhibit reasonable agreement with existing experimental data. This work highlights the intrinsic tetrapyrrolic coordination of Ni for facilitating the CO<sub>2</sub>RR and offers practical guidance for the rational improvement of SACs, and this model can be expanded to explore mechanisms of other electrocatalysis in aqueous solutions.

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## Introduction

The high dependence of non-renewable fossil resources in modern economics has resulted in increasing concerns regarding energy and the environment. A promising solution to address this issue is to electrochemically convert waste CO<sub>2</sub> to fuels to achieve a carbon-neutral cycle.<sup>1–3</sup> Unfortunately, due to its sluggish kinetics and the concomitant hydrogen evolution reaction (HER), the feasibility of implementing such a CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) process on industrial scales suffers from the coupled problems of poor energy efficiency and low product selectivity. In particular, electrodes composed of earth-abundant metals generally exhibit low activity and/or selectivity for facilitating the CO<sub>2</sub>RR. Research on developing effective CO<sub>2</sub>RR catalysts has brought about the advent of a new class of

heterogeneous electrocatalysts, namely, M–N–C single-atom catalysts (SACs), which feature atomically dispersed single-metal-atom sites.<sup>4–8</sup> These metal sites exhibit unique electronic and structural properties compared with their bulk counterparts, thereby endowing M–N–C SACs with outstanding catalytic performance.<sup>9</sup>

Ni–N–C, one of the most represented CO<sub>2</sub>RR SACs, has been established to possess great potential for facilitating selective CO<sub>2</sub>-to-CO conversion. Determining the role of coordination environments is beneficial for implementing strategic improvements to CO<sub>2</sub>RR catalysts. While significant efforts have been expended to investigate the fundamental nature of the active Ni sites through employing physical characterizations and modern quantum mechanics methods, a common consensus pertaining to such an issue has not been reached.<sup>3,9,16,17</sup> Several pioneering studies have proposed a pyridinic-type NiN<sub>4</sub> moiety (referred to as “ $\alpha$ -NiN<sub>4</sub>” herein) in which a central Ni atom is coordinated by four pyridinic N atoms, and CO<sub>2</sub>RR processes on such a moiety were explored through comprehensive density functional theory (DFT) calculations.<sup>6–8</sup> It should also be noted that pyridinic-type MN<sub>4</sub> is a prototypical moiety that has been successfully established for describing the oxygen reduction reaction (ORR) on various M–N–C SACs.<sup>18–22</sup> However, a detailed examination of the computational results of the CO<sub>2</sub>RR on  $\alpha$ -NiN<sub>4</sub> indicates a failure to reproduce the observed CO<sub>2</sub>RR activities of Ni–N–C SACs since large theoretical overpotentials  $\eta^t$  (>1.6 V) are involved.<sup>6–8</sup>

<sup>a</sup>Environmental Process Modelling Centre, Nanyang Environment and Water Research Institute, Nanyang Technological University, 1 CleanTech Loop, Singapore 637141, Singapore. E-mail: kzhou@ntu.edu.sg

<sup>b</sup>School of Mechanical and Aerospace Engineering, Nanyang Technological University, 50 Nanyang Avenue, Singapore 639798, Singapore

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‡ Current address: Jiangsu Collaborative Innovation Centre of Biomedical Functional Materials, Jiangsu Key Laboratory of New Power Batteries, School of Chemistry and Materials Science, Nanjing Normal University, 1 Wenyuan Road, Nanjing 210023, China.



Recently, a variety of hybrid pyridinic N and C coordination environments with respect to the Ni sites have been proposed. For instance, Zhao *et al.* demonstrated that a pyridinic-type  $\text{NiN}_1\text{C}_3$  moiety (referred to as “ $\alpha\text{-NiN}_1\text{C}_3$ ” herein) is considerably active for facilitating the  $\text{CO}_2\text{RR}$  with a small  $\eta^{\ddagger}$  value of 0.48 V and exhibits high selectivity toward CO over  $\text{H}_2$ .<sup>10</sup> Such a hybrid moiety was also suggested in a recent grand canonical DFT study by Li and co-workers;<sup>23</sup> their calculations also revealed that the charge capacity and the formation of hydrogen bonds between the adsorbates and the surrounding water molecules play vital roles in facilitating the activation of  $\text{CO}_2$ . In contrast, Hossain *et al.* showed that pyridinic-type  $\text{NiN}_2\text{C}_2$  and  $\text{NiN}_3\text{C}_1$  moieties (referred to as “ $\alpha\text{-NiN}_2\text{C}_2$ ” and “ $\alpha\text{-NiN}_3\text{C}_1$ ” herein) are responsible for facilitating the  $\text{CO}_2\text{RR}$  at an electrode potential of  $-0.8$  V.<sup>24</sup>

While previous studies have predicted that Ni moieties containing fewer N atoms, *i.e.*,  $\alpha\text{-NiN}_x\text{C}_{4-x}$  ( $x = 1-3$ ), exhibit excellent  $\text{CO}_2\text{RR}$  activity, a general situation in which the formation energy of an  $\text{MN}_4$  moiety is much lower than those of  $\text{MN}_x\text{C}_{4-x}$  ( $x = 1-3$ ) moieties has been overlooked.<sup>25-27</sup> From a thermodynamics perspective, the predominant moieties of M–N–C SACs are expected to have the formula of  $\text{MN}_4$  instead of  $\text{MN}_x\text{C}_{4-x}$  ( $x = 1-3$ ). Indeed, the research of Li *et al.* indicated that no Ni–C bond exists in the Ni–N–C SACs they synthesized on the basis of the C K-edge X-ray absorption spectroscopy (XAS) characterization of the Ni–N–C SACs and a control N–C system.<sup>6</sup> Moreover, numerous experimental and computational studies on the ORR occurring on M–N–C SACs have demonstrated that the dispersed metal sites are mainly contributed by  $\text{MN}_4$ .<sup>18-22</sup> Therefore, none of the commonly studied  $\alpha\text{-NiN}_x\text{C}_{4-x}$  moieties are responsible for the excellent  $\text{CO}_2\text{RR}$  performance of Ni–N–C SACs. This situation presents an ambiguity regarding the structure–activity of the Ni sites of heterogeneous Ni–N–C SACs, which requires the development of (operando) characterization techniques and modelling approaches with high sensitivity and resolution.

In this study, we addressed this ambiguity by employing first-principles calculations and microkinetic modelling to investigate pyrrolic-type  $\text{NiN}_x\text{C}_{4-x}$  ( $\beta\text{-NiN}_x\text{C}_{4-x}$ ) moieties as well as  $\alpha\text{-NiN}_x\text{C}_{4-x}$  moieties, in tandem with a constant-potential method and the explicit treatment of solvents.  $\beta\text{-NiN}_x\text{C}_{4-x}$  moieties were explored because pyrrolic-type moieties have been demonstrated to inherently exist (or coexist with pyridinic-type moieties) in heterogeneous M–N–C SAC,<sup>28-32</sup> but little is known of their  $\text{CO}_2\text{RR}$  mechanisms. Remarkably, we demonstrated that the electrode potential is crucial for governing  $\text{CO}_2$  activation, and in contrast to other moieties that are inactive and/or exhibit low-selectivity, the  $\beta\text{-NiN}_4$  moiety not only possesses a favourable formation energy but also exhibits considerable activity and selectivity for  $\text{CO}_2$ -to-CO conversion.

## Results and discussion

### Structural models of Ni–N–C SACs and their formation energy

Good knowledge of the active structure of a catalyst is a solid foundation for understanding its catalytic nature.<sup>33,34</sup> It has been established that the local coordination environment of



Fig. 1 Twelve different N-coordinated single-atom Ni configurations: (a) the commonly studied pyridinic-type Ni moieties in literature,  $\alpha\text{-NiN}_x\text{C}_{4-x}$  ( $x = 1-4$ ); (b) the pyrrolic-type Ni moieties,  $\beta\text{-NiN}_x\text{C}_{4-x}$ . The grey, blue, orange, and white spheres represent C, N, Ni, H atoms, respectively. Calculated formation energy of (c)  $\alpha\text{-NiN}_x\text{C}_{4-x}$  and (d)  $\beta\text{-NiN}_x\text{C}_{4-x}$ . The formation energy values of  $\alpha\text{-NiN}_4$  and  $\beta\text{-NiN}_4$  are set as zero.

a single-atom metal site is essential for determining its catalytic performance.<sup>35,36</sup> We began by constructing the potential configurations of single-atom Ni sites and evaluating their formation energy values. For the local structure of the Ni sites of Ni–N–C SACs, the central Ni atom adopts a (quasi-)planar tetra-coordination configuration, and as mentioned earlier, the ligand species can be either pyridinic N, pyrrolic N, or C. Interestingly, the prototypical  $\alpha\text{-NiN}_x\text{C}_{4-x}$  can be conveniently constructed by creating a double-vacancy in the basal plane of graphene and replacing certain C atoms with N atoms (Fig. 1a), which may explain why  $\alpha\text{-NiN}_x\text{C}_{4-x}$  moieties are typically chosen as structural models for XAS fitting and DFT calculations in existing literature.<sup>6-15,23,24</sup>

In contrast, the construction of the  $\beta\text{-NiN}_x\text{C}_{4-x}$  moieties requires more skilful manipulation of the C atoms to create pyrrolic-type coordination environments (Fig. 1b), and according to previous studies,<sup>28-30</sup> the unsaturated C atoms have been terminated by H atoms. Such pyrrolic-type moieties have been demonstrated to typically exist within the micropores of graphene nanosheets.  $\alpha\text{-NiN}_2\text{C}_2$  exhibits three possible configurations that correspond to different combinations of its N and C ligands; each of these configurations have been explored in various studies, such as  $\alpha\text{-NiN}_2\text{C}_2\text{-a}$ ,<sup>10</sup>  $\alpha\text{-NiN}_2\text{C}_2\text{-b}$ ,<sup>12,23</sup> and  $\alpha\text{-NiN}_2\text{C}_2\text{-c}$ .<sup>24</sup> Similarly to  $\alpha\text{-NiN}_2\text{C}_2$ ,  $\beta\text{-NiN}_2\text{C}_2$  also corresponds to three possible configurations. In this work, only the configurations with a relative low formation energy were adopted in the later  $\text{CO}_2\text{RR}$  calculations for  $\text{NiN}_2\text{C}_2$ .

The relative formation energy of the  $\alpha\text{-NiN}_x\text{C}_{4-x}$  and  $\beta\text{-NiN}_x\text{C}_{4-x}$  moieties are presented in Fig. 1c and d, in which the formation energy values of  $\alpha\text{-NiN}_4$  and  $\beta\text{-NiN}_4$  are set to be zero. For both the  $\alpha\text{-NiN}_x\text{C}_{4-x}$  and  $\beta\text{-NiN}_x\text{C}_{4-x}$  moieties, the



formation energy increases significantly as the number of N atoms decreases. In particular, the difference in formation energy values between  $\text{NiN}_1\text{C}_3$  and  $\text{NiN}_4$  reaches up to 2.90 eV for the pyridinic-type configuration and 4.44 eV for the pyrrolic-type configuration. These results suggest that compared with N, the C ligand is not a good support for anchoring single-atom Ni species.

Please note that such formation energy calculations were performed to provide a general demonstration of the single-atom Ni sites based on a thermodynamics criterion, and they do not indicate whether the sites are pyridinic or pyrrolic. Additionally, they do not exclude the presence of energetically unfavourable  $\text{NiN}_x\text{C}_{4-x}$  ( $x = 1-3$ ) moieties existing in nature. Indeed, the local structure of the single metal site should be determined by a synthesis parameter, such as the precursor materials, synthetic atmosphere, and pyrolysis temperature. However, the favourable formation energy of  $\text{NiN}_4$  over that of  $\text{NiN}_x\text{C}_{4-x}$  ( $x = 1-3$ ) provides clear evidence that in principle, the predominant Ni moieties of Ni-N-C SACs are expected to correspond to the formula of  $\text{NiN}_4$ .

### CO<sub>2</sub> reduction reaction on the pyrrolic-type NiN<sub>4</sub>

We next assessed the intrinsic CO<sub>2</sub>RR activities of the Ni moieties by employing a constant-potential/hybrid-solvent model. First, the constant-potential method considers the surface charge effect to determine potential-dependent energy values. Please note that the surface charge of an electrocatalyst is essential for assessing its chemical reactivity.<sup>23,24,37-39</sup> Secondly, the explicit solvent model of the electrochemical

interface allows the interactions between intermediates and the surrounding water molecules to be captured. Thirdly, the implicit solvation model accurately describes long-range electrostatic interactions and takes advantage of the fact that the electrostatic potential goes to zero in the electrolyte region. More details can be found in the Methods section.

Taking  $\beta\text{-NiN}_4$ , a Ni moiety with a favourable formation energy, as an example, the geometric structures of its CO<sub>2</sub>RR reaction species are shown in Fig. 2a. For each species, five individual simulations with system charge values of  $-1.75e$ ,  $-1.5e$ ,  $-1.25e$ ,  $-1e$ , and  $-0.75e$  were conducted. Based on these calculations, the electrode potential ( $U$ ) of each species for a given charge can be determined (Fig. 2b). A wider range of charge values (nine groups from  $-0.25e$  to  $-2.25e$ ) has also been sampled, and negligible difference was found between the results (Fig. S1†). Due to the non-identical electronic structures of these species, the same charge does not correspond to the same value of  $U$ . However, the total energy of each species can be described as a continuous function of  $U$  by fitting five potential-energy points (Fig. 2c and Table S1†). With these potential-energy curves, the energy of these species for a specific value of  $U$  can be obtained, and the corresponding free energy changes  $\Delta G$  of the reaction steps can be determined by further considering contributions of the zero-point energy, enthalpy, and entropy (Fig. 2d).

It can be observed from Fig. 2d that CO<sub>2</sub> adsorption on  $\beta\text{-NiN}_4$  (CO<sub>2</sub>\* formation step) is exothermic in nature below  $U = -0.26$  V and is more energetically favourable than the competing H\* formation above  $U = -1.20$  V. This suggests that  $\beta\text{-NiN}_4$  can efficiently activate CO<sub>2</sub> molecules at typical working



Fig. 2 (a) Views of the geometric structures of adsorbate-free  $\beta\text{-NiN}_4$  slab (\*), CO<sub>2</sub>\*, COOH\*, and CO\* optimized using a charge value of  $-1.25e$ . The blue dashed lines represent hydrogen bonds. (b) Calculated electrode potentials of the studied species at charge values of  $-1.75e$ ,  $-1.5e$ ,  $-1.25e$ ,  $-1e$ , and  $-0.75e$ . (c) Total energy of the studied species as a function of the electrode potential. (d) Free energy changes  $\Delta G$  of the reaction steps as a function of the electrode potential. (e) Total energy of physisorbed and chemisorbed CO<sub>2</sub>. (f) The Ni-C length of CO<sub>2</sub>\* as a function of the electrode potential. The insets are geometric structures that were optimized using charge values of  $-1.5e$  (left) and  $-0.25e$  (right).



potentials while maintaining high selectivity for the CO<sub>2</sub>RR compared with the HER over a wide range of  $U$ . The conversion of CO<sub>2</sub>\* to COOH\* (COOH\* formation step) is the potential-limiting step, which becomes exothermic at  $U = -0.79$  V. Subsequently, COOH\* is reduced to CO\* (CO\* formation step) with a negative  $\Delta G$  value, and the adsorbed CO molecule can be easily released from the  $\beta$ -NiN<sub>4</sub> surface. A more appropriate comparison of the onset potentials and overpotentials with experimental data can be established based on microkinetic modelling, as discussed later.

Specifically, we determined that the consideration of  $U$  is crucial for reproducing the experimentally observed chemisorption of CO<sub>2</sub> on the Ni sites of Ni–N–C SACs. As shown in Fig. 2e and f, the adsorption of CO<sub>2</sub> on  $\beta$ -NiN<sub>4</sub> preferentially adopts a chemisorption configuration when the  $U$  is lower than  $-0.27$  V, while a physisorption configuration is dominant above this potential value. Chemisorption configurations can be distinguished from physisorption configurations by the formation of a Ni–C bond. For example, a CO<sub>2</sub> molecule is bent when adsorbed onto  $\beta$ -NiN<sub>4</sub> while forming a Ni–C bond (1.97 Å) at  $U = -0.59$  V ( $q = -1.5e$ ), but it remains straight with a Ni–C distance of 3.09 Å at  $U = 0.03$  V ( $q = -0.25e$ ), which is within the range of typical vdW interactions. Please note that the different adsorption configurations were obtained by employing different initial structures (*i.e.*, different Ni–C distances). The surrounding water molecules are also essential for the chemisorption of CO<sub>2</sub> since the hydrogen bonds between them

stabilize the CO<sub>2</sub>\* intermediates.<sup>23</sup> The removal of the surrounding water molecules can also result in the adsorption of CO<sub>2</sub> transiting from chemisorption to physisorption.

### Comparison of the CO<sub>2</sub>RR performance of different Ni moieties

The constant-potential results of other Ni moieties are shown in Fig. 3a, b, S2 and S3†, and their energy–potential relationships are summarized in Tables S2–S8.† For  $\alpha$ -NiN<sub>4</sub>, another Ni moiety exhibiting a favourable formation energy, its CO<sub>2</sub>\* and COOH\* formation steps are only exothermic at very negative potentials ( $-0.81$  and  $-1.10$  V, respectively), as shown in Fig. 3a. This suggests that  $\alpha$ -NiN<sub>4</sub> is inactive for facilitating the CO<sub>2</sub>RR.

While the CO<sub>2</sub>\* and COOH\* formation steps of  $\alpha$ -NiN<sub>1</sub>C<sub>3</sub> are more energetically favourable than its H\* formation step, the latter surpasses the CO<sub>2</sub>\* formation step below  $U = -0.45$  V (Fig. 3b). On  $\alpha$ -NiN<sub>1</sub>C<sub>3</sub>, the location of H\* with the lowest energy is the Ni–C bridge site instead of the Ni top site (Fig. 3c), which differs from both  $\alpha$ -NiN<sub>4</sub> and  $\beta$ -NiN<sub>4</sub> that preferentially adopt the Ni-top H\* configuration (Fig. 3d and e). Although it appears that H\* could be weakly adsorbed onto the Ni top sites of  $\alpha$ -NiN<sub>1</sub>C<sub>3</sub>,<sup>23</sup> the strong binding of H\* on the Ni–C bridge sites prevents the reduction of CO<sub>2</sub>, thereby resulting in poor CO<sub>2</sub>RR selectivity. Meanwhile, strong H\* adsorption on the bridge sites has also been identified in other Ni moieties that involve the hybrid C and N coordination (Fig. S4†).



**Fig. 3** (a and b) Free energy changes of the reaction steps of (a)  $\alpha$ -NiN<sub>4</sub> and (b)  $\alpha$ -NiN<sub>1</sub>C<sub>3</sub> as a function of the electrode potential. (c) Total energy of H\* on the Ni top site and Ni–C bridge site of  $\alpha$ -NiN<sub>1</sub>C<sub>3</sub> as a function of the electrode potential  $U$ . The insets present the atomic moieties of H\* adsorbed on the Ni top site (upper) and Ni–C bridge site (bottom). (d and e) Views of the atomic structures of H\* adsorbed onto (d)  $\alpha$ -NiN<sub>4</sub> and (e)  $\beta$ -NiN<sub>4</sub>. (f) Free energy changes of CO<sub>2</sub>\* formation, COOH\* formation, and H\* formation on the Ni moieties at  $U = -0.60$  V. For NiN<sub>2</sub>C<sub>2</sub>, the configurations with a relatively lower formation energy, *i.e.*,  $\alpha$ -NiN<sub>2</sub>C<sub>2</sub>-a and  $\beta$ -NiN<sub>2</sub>C<sub>2</sub>-b, were adopted for energy calculations. (g) Difference in free energy between H\* formation and CO<sub>2</sub>\* formation at  $U = -0.60$  V. A more positive value corresponds to higher CO<sub>2</sub>RR selectivity, and *vice versa*.



Fig. 3f shows the values of  $\Delta G$  for the three key reaction steps, *i.e.*,  $\text{CO}_2^*$  formation,  $\text{COOH}^*$  formation, and  $\text{H}^*$  formation, of the studied Ni moieties at  $U = -0.60$  V, at which a partial current density of CO can be detected experimentally for Ni–N–C SACs.<sup>10–15</sup> The results for the  $\text{CO}^*$  formation and CO desorption steps are excluded since the two steps are typically exothermic. At  $U = -0.60$  V,  $\text{CO}_2^*$  formation on  $\alpha\text{-NiN}_4$  remains endothermic by 0.20 eV, and  $\text{COOH}^*$  formation is endothermic by 0.41 eV. These results indicate that  $\alpha\text{-NiN}_4$  displays a low activity for facilitating the  $\text{CO}_2\text{RR}$ , which is consistent with previous studies.

Although the  $\text{CO}_2^*$  formation steps of the  $\alpha$ - and  $\beta\text{-NiN}_x\text{C}_{4-x}$  ( $x = 1-3$ ) moieties correspond to negative  $\Delta G$  values, their  $\text{H}^*$  formation steps are highly exothermic. Since  $\text{H}^*$  formation is more energetically favourable than  $\text{CO}_2^*$  formation, the  $\alpha$ - and  $\beta\text{-NiN}_x\text{C}_{4-x}$  ( $x = 1-3$ ) moieties are expected to facilitate the HER preferentially instead of the  $\text{CO}_2\text{RR}$  at  $U = -0.60$  V. Evidently, such a situation directly contradicts the experimental observation of Ni–N–C SACs exhibiting high selectivity for the  $\text{CO}_2\text{RR}$ . Hence, apart from  $\alpha\text{-NiN}_4$ , Ni moieties with hybrid C and N coordination environments, *i.e.*, the  $\alpha$ - and  $\beta\text{-NiN}_x\text{C}_{4-x}$  ( $x = 1-3$ ) moieties, cannot be responsible for the excellent  $\text{CO}_2\text{RR}$  performance of Ni–N–C SACs.

Remarkably,  $\beta\text{-NiN}_4$  exhibits a negative  $\Delta G$  value for  $\text{CO}_2^*$  formation ( $-0.19$  eV) and a positive  $\Delta G$  value for  $\text{H}^*$  formation (0.40 eV), as shown in Fig. 3f, which indicates that at  $U =$

$-0.60$  V,  $\text{CO}_2$  molecules can be activated effectively over  $\beta\text{-NiN}_4$ , and the competing HER process is suppressed. Please note that the difference in energy between  $\text{CO}_2^*$  formation and  $\text{H}^*$  formation is as large as 0.59 eV (Fig. 3g); such a value implies that  $\beta\text{-NiN}_4$  possesses high selectivity toward the  $\text{CO}_2\text{RR}$ . Moreover, for  $\text{COOH}^*$  formation, it can be shown from Fig. 3f that aside from  $\alpha\text{-NiN}_1\text{C}_3$  ( $-0.04$  eV), the other Ni moieties exhibit positive  $\Delta G$  values at  $U = -0.60$  V; however, the  $\Delta G$  values of  $\alpha\text{-NiN}_2\text{C}_2$ ,  $\beta\text{-NiN}_4$ , and  $\beta\text{-NiN}_1\text{C}_3$  are only slightly positive, indicating that  $\text{COOH}^*$  formation on these three moieties is still feasible. Overall, the above results have established that among these Ni moieties, only  $\beta\text{-NiN}_4$  has a favourable formation energy value and is active and selective toward the  $\text{CO}_2\text{RR}$ . Such characteristics of  $\beta\text{-NiN}_4$  may potentially account for the experimentally observed high  $\text{CO}_2\text{RR}$  performance of Ni–N–C SACs.

### Kinetics and free energy diagrams

To obtain more insight into the  $\text{CO}_2\text{RR}$  occurring on the active  $\beta\text{-NiN}_4$  moiety, we further explored the kinetics of the key reaction steps involved, and the thermodynamic and kinetic energy values were compiled in a free energy diagram (Fig. 4a). The potential dependence of the kinetic barrier  $\Delta G^\ddagger(U)$  was determined through multiple barrier calculations at varying potentials (Fig. 4b and c). According to our calculations, at  $U = -0.60$  V,  $\beta\text{-NiN}_4$  exhibits a small barrier of 0.05 eV for  $\text{CO}_2^*$



Fig. 4 (a) Free energy diagram of the  $\text{CO}_2\text{RR}$  and competing HER on  $\beta\text{-NiN}_4$  at  $U = -0.60$  V. The insets are snapshots of the transition states (TS). The arrow symbols indicate the directions of the HER and  $\text{CO}_2\text{RR}$  processes. (b and c) Calculated kinetic barriers  $\Delta G^\ddagger$  for the (b)  $\text{CO}_2\text{RR}$  and (c) HER on  $\beta\text{-NiN}_4$  as a function of the electrode potential  $U$ .



formation and a moderate barrier of 0.69 eV for COOH\* formation, while it displays a quite high barrier of 1.31 eV for H\* formation (Volmer reaction). After the formation of the COOH\* or H\* intermediates, the subsequent protonation steps are kinetically feasible, *e.g.*,  $\Delta G^\ddagger(-0.6 \text{ V}) = 0.42 \text{ eV}$  for the reduction of COOH\* to CO\* and  $\Delta G^\ddagger(-0.6 \text{ V}) = 0.10 \text{ eV}$  for the reduction of H\* to H<sub>2</sub> (Heyrovsky reaction). By extrapolating these thermodynamic and kinetic energy values, we thereby conclude that at  $U = -0.60 \text{ V}$ , the efficient conversion of CO<sub>2</sub> to CO on  $\beta\text{-NiN}_4$  can be achieved.

The kinetic barriers of a prototypical Ni moiety,  $\alpha\text{-NiN}_1\text{C}_3$ , were also investigated. The geometric structures of its transition states are shown in Fig. S5.† As expected, at  $U = -0.60 \text{ V}$ ,  $\alpha\text{-NiN}_1\text{C}_3$  was predicted to exhibit a relatively favourable  $\Delta G^\ddagger$  value for COOH\* formation (0.39 eV) compared with  $\beta\text{-NiN}_4$ . However, upon considering the lowest-energy location of the H\* intermediate (*i.e.*, H\* adsorption on the Ni–C bridge sites), the value of  $\Delta G^\ddagger$  for H\* formation (0.36 eV) was found to be lower than that for COOH\* formation. Therefore, the kinetic results have also established the poor CO<sub>2</sub>RR selectivity of  $\alpha\text{-NiN}_1\text{C}_3$ , which has already been identified by the above thermodynamic calculations.



Fig. 5 (a) Schematic plot of reaction steps considered in the microkinetic modelling. (b) Simulated partial CO current density of  $\beta\text{-NiN}_4$  compared with existing experimental data (catalyst loading:  $1.0 \text{ mg cm}^{-2}$  in ref. 11 and  $0.75 \text{ mg cm}^{-2}$  in ref. 12). For the polarization curve simulation,  $e\rho_{\text{Ni}} = 10.5 \mu\text{C cm}^{-2}$  was adopted; the term  $\rho_{\text{Ni}}$  is the density of active single-Ni-atom sites. (c) Tafel plot of  $\beta\text{-NiN}_4$ .

## Microkinetic modelling

Finally, we constructed a microkinetic model to further examine the CO<sub>2</sub>RR performance of the active  $\beta\text{-NiN}_4$  moiety and to provide a qualitative comparison with existing experimental data of Ni–N–C SACs. Fig. 5a shows the reaction steps of the CO<sub>2</sub>RR ( $i = 1-5$ ) and HER ( $i = 6, 7$ ) processes considered in our model. The terms CO<sub>2</sub>(aq) and CO<sub>2</sub>(dl) represent CO<sub>2</sub> molecules within the electrolyte and at the catalyst–electrolyte interface, respectively. The term  $k_i$  is the rate constant of the step  $i$ , which depends directly on the potential-based kinetic barrier  $\Delta G^\ddagger(U)$  in accordance with the transition state theory, and  $k_{-i}$  is the rate constant for the reverse reaction. The CO partial current density can be estimated by solving these rate equations at a steady state. Further details are summarized in the Methods section.

Fig. 5b displays the model partial CO current density ( $j_{\text{CO}}$ ) as a function of the electrode potential. The onset-potential of  $\beta\text{-NiN}_4$  was calculated to be  $-0.55 \text{ V}$ , beyond which the value of  $j_{\text{CO}}$  increases continuously with  $U$  and reaches  $10 \text{ mA cm}^{-2}$  at  $U = -0.77 \text{ V}$ . Such a curve is consistent with its experimentally measured counterparts.<sup>11,12</sup> Please note that the current density is highly dependent on the catalyst morphology and electrochemical measurement parameters (*e.g.*, electrode material, catalyst mass loading, and CO<sub>2</sub> diffusion rate), and the present calculation was performed to provide a qualitative demonstration of CO<sub>2</sub>RR activity as the effective density of active Ni sites ( $\rho_{\text{Ni}}$ ) is unknown experimentally, even though the Ni content and loading can be determined.

A Tafel analysis was further conducted (Fig. 5c). According to our calculations, the Tafel slope of  $\beta\text{-NiN}_4$  was estimated to be  $\sim 101 \text{ mV dec}^{-1}$ , which is in reasonable agreement with the typical values for Ni–N–C SACs in experiments ( $\sim 108 \text{ mV dec}^{-1}$ ).<sup>6,8,10,11</sup> The polarization curve for the competing HER is shown in Fig. S6,† in which the poor HER activity of  $\beta\text{-NiN}_4$  is revealed ( $U = -1.57 \text{ V}$  at  $10 \text{ mA cm}^{-2}$ ). This also implies that the experimentally observed concomitant H<sub>2</sub> production at  $U < -0.7 \text{ V}$  may be attributed to the HER occurring on the N-neighbouring C sites of Ni–N–C SACs, considering that the N-doped graphene nanosheets are active for facilitating the HER.<sup>11</sup>

## Conclusions

In summary, we have presented a fundamental understanding of the CO<sub>2</sub>RR occurring on heterogeneous Ni–N–C SACs by considering twelve possible single-atom Ni moieties. We discovered that an intrinsic tetrapyrrolic coordination environment with respect to Ni, *i.e.*,  $\beta\text{-NiN}_4$ , can boost the CO<sub>2</sub>RR activity, which rationalizes existing experimental observations. Such an understanding is based on the first-principles and microkinetic modelling of reaction processes at a solid–water interface, in which a constant-potential/hybrid-solvent model was adopted. According to an analysis of the formation energy, the predominant Ni moieties in Ni–N–C SACs are expected to correspond to the formula of NiN<sub>4</sub>. After determining the potential-dependent thermodynamic and kinetic energy values of the studied Ni moieties, we found that among them, only  $\beta\text{-NiN}_4$  exhibits considerable activity for the selective CO<sub>2</sub>-to-CO



conversion compared with the competing H<sub>2</sub> production. Specifically, its theoretical polarization curve and Tafel plot show reasonable agreement with existing experimental data. Our work discloses the activity origin of an important model SAC, offers practical guidance for the rational design of electrocatalysts, and serves as a prime example for future studies exploring the underlying mechanisms of other heterogeneous electrocatalysis in aqueous solutions.

## Methods

### First-principles computations

The first-principles calculations were performed with Vienna *Ab initio* Simulation Package (VASP),<sup>40,41</sup> and the projector-augmented wave approach was employed to describe the ion–electron interactions.<sup>42</sup> The electronic exchange–correlation energy was modelled using the BEEF-vdW functional,<sup>43</sup> which accurately describes vdW interactions while retaining a good description of chemisorption of adsorbates on surfaces. All calculations included spin polarization and were performed using a cutoff energy of 400 eV with a Gaussian smearing of 0.1 eV for slabs and 0.01 eV for gas-phase species. The *k*-space samplings were set as 3 × 3 × 1. The optimized lattice parameters of the α-NiN<sub>x</sub>C<sub>4-x</sub> slabs were *a* = 8.39 Å and *b* = 12.43 Å, and those of the β-NiN<sub>x</sub>C<sub>4-x</sub> slabs were *a* = 8.12 Å and *b* = 12.02 Å. For all slabs, the distance of the vacuum space was set as ~25 Å to minimize interactions between periodic images. The lowest energy location of each intermediate was reported.

### Formation energy calculations

The formation energy of a NiN<sub>x</sub>C<sub>4-x</sub> (*x* = 1, 2, 3, or 4) moiety is defined as:

$$E_{\text{form}} = E_{\text{NiN}_x\text{C}_{4-x}} - N_{\text{C}}\mu_{\text{C}} - N_{\text{N}}\mu_{\text{N}} - N_{\text{H}}\mu_{\text{H}} - \mu_{\text{Ni}} \quad (1)$$

where  $E_{\text{NiN}_x\text{C}_{4-x}}$  is the total energy of a NiN<sub>x</sub>C<sub>4-x</sub> slab, and  $N_{\text{C}}$ ,  $N_{\text{N}}$ , and  $N_{\text{H}}$  are the number of C, N, and H atoms in the NiN<sub>x</sub>C<sub>4-x</sub> slab, respectively. The term  $\mu$  denotes the chemical potential of a species, and herein  $\mu_{\text{C}}$ ,  $\mu_{\text{N}}$ ,  $\mu_{\text{H}}$ , and  $\mu_{\text{Ni}}$  were taken as the total energy of one C atom of pristine graphene, one N atom of a N<sub>2</sub> molecule, one H atom of a H<sub>2</sub> molecule, and one Ni atom of bulk Ni, respectively. According to this definition, a NiN<sub>x</sub>C<sub>4-x</sub> moiety with a lower formation energy corresponds to a higher likelihood of being present in Ni–N–C SACs.

### Constant-potential/hybrid-solvent model

A constant-potential/hybrid-solvent model was employed to determine the potential-dependent thermodynamic and kinetic energy values of reactions at the catalyst–solvent interface. A water bilayer containing 24 H<sub>2</sub>O molecules was constructed to explicitly describe the interactions between intermediates and the surrounding water molecules. The Poisson–Boltzmann implicit solvation model was utilized to establish the relationship between the system charge and electrode potential *U*, as implemented in the VASPsol.<sup>44,45</sup> This model takes advantage of the fact that the

electrostatic potential goes to zero in the electrolyte region. The effective surface tension parameter was set as zero as the cavitation energy is negligible.<sup>45</sup> For an electrochemical system, the electrostatic potential is analogous to the workfunction. We added additional electrons (a net charge) and subsequently calculated the workfunction of the charged slab ( $\Phi_{\text{slab}}$ ), which is reflected by the Fermi level with respect to the electrostatic potential in the electrolyte region. After determining the value of  $\Phi_{\text{slab}}$ , the electrode potential of the slab on the standard hydrogen electrode (SHE) scale,  $U_{\text{SHE}}$ , can be calculated by

$$U_{\text{SHE}} = \Phi_{\text{slab}}/e - U^0 \quad (2)$$

where  $U^0$  is the absolute potential of the SHE. The value of  $U^0$  was predicted to be 4.6 V from the VASPsol simulation,<sup>45</sup> which is in good agreement with experimental estimates (4.4–4.8 V).<sup>46</sup> To facilitate comparisons between our results and existing experimental data, the values of  $U_{\text{SHE}}$  were regulated with respect to the reversible hydrogen electrode (RHE) scale by a potential shift of  $k_{\text{B}}T \times \text{pH} \times \ln 10$ . In this work, the pH was taken as 7, as the measurements of the CO<sub>2</sub>RR on Ni–N–C SACs are typically performed in a near neutral environment (*e.g.*, CO<sub>2</sub>-saturated 0.5 M KHCO<sub>3</sub>). The total energy of a charged slab was further determined by considering energy corrections regarding the background charge and the electrostatic potential shift of the charged slab with respect to an uncharged slab.<sup>47–52</sup>

### Potential-dependent kinetic barrier

For adsorbates, the zero-point energy ( $E_{\text{ZPE}}$ ), enthalpy ( $\int C_{\text{p}} dT$ ), and entropy ( $-TS$ ) contributions to free energy were calculated by vibrational frequencies calculations, in which all 3N degrees of freedom are treated as harmonic vibrational motions. For molecules, these contributions were obtained from the NIST database. Electronic energy corrections were applied to the calculations of  $E_{\text{DFT}}$  of CO<sub>2</sub> (+0.33 eV) and H<sub>2</sub> (+0.09 eV) molecules because of the errors residing in the description of the OCO backbone and H<sub>2</sub> from the BEEF-vdW functional.<sup>53</sup> Based on the above constant potential simulations and free energy contributions, the free energy change ( $\Delta G$ ) for each reaction step can be determined by the following equation:

$$\Delta G = \Delta E + \Delta E_{\text{ZPE}} + \Delta \int C_{\text{p}} dT - T\Delta S \quad (3)$$

where  $\Delta E$ ,  $\Delta E_{\text{ZPE}}$ ,  $\Delta \int C_{\text{p}} dT$ , and  $T\Delta S$  are the electronic energy difference, zero point energy difference, enthalpy difference and entropy difference, respectively.

The potential dependence of the kinetic barrier,  $\Delta G^{\ddagger}(U)$ , was obtained *via* multiple barrier calculations at varying potentials (different system charges). The transition state was determined using the climbing-image nudged elastic band (CI-NEB) approach<sup>54</sup> with a given charge and has been further verified by vibrational frequency calculations (only one imaginary frequency). The values of  $\Delta G^{\ddagger}$  have been corrected by considering the zero-point energy, but no configurational entropies were included according to the transition state theory.



## Microkinetic model

The rate equation of each species in the CO<sub>2</sub>RR process is summarized in eqn (4)–(9), and they are presented as follows:

$$\frac{\partial \theta_{\text{CO}_2(\text{dl})}}{\partial t} = k_1 x_{\text{CO}_2(\text{aq})} - k_{-1} x_{\text{CO}_2(\text{dl})} - k_2 x_{\text{CO}_2(\text{dl})} \theta_{*_{\text{Ni}}} + k_{-2} \theta_{\text{CO}_2^*} \quad (4)$$

$$\frac{\partial \theta_{*_{\text{Ni}}}}{\partial t} = -k_2 x_{\text{CO}_2(\text{dl})} \theta_{*_{\text{Ni}}} + k_{-2} \theta_{\text{CO}_2^*} + k_5 \theta_{\text{CO}^*} - k_{-5} p_{\text{CO}} \theta_{*_{\text{Ni}}} \quad (5)$$

$$\frac{\partial \theta_{\text{CO}_2^*}}{\partial t} = k_2 x_{\text{CO}_2(\text{dl})} \theta_{*_{\text{Ni}}} - k_{-2} \theta_{\text{CO}_2^*} - k_3 \theta_{\text{CO}_2^*} + k_{-3} \theta_{\text{COOH}^*} \quad (6)$$

$$\frac{\partial \theta_{\text{COOH}^*}}{\partial t} = k_3 \theta_{\text{CO}_2^*} + k_{-3} \theta_{\text{COOH}^*} - k_4 \theta_{\text{COOH}^*} + k_{-4} \theta_{\text{CO}^*} \quad (7)$$

$$\frac{\partial \theta_{\text{CO}^*}}{\partial t} = k_4 \theta_{\text{COOH}^*} - k_{-4} \theta_{\text{CO}^*} - k_5 \theta_{\text{CO}^*} + k_{-5} p_{\text{CO}} \theta_{*_{\text{Ni}}} \quad (8)$$

where  $\theta$  and  $x$  are the coverage and mole fraction of a species, respectively. In this work,  $x_{\text{CO}_2(\text{aq})}$  is set to be  $5.79 \times 10^{-4}$ , corresponding to CO<sub>2</sub> gas in equilibrium with aqueous CO<sub>2</sub>;  $p_{\text{CO}}$  denotes the effective CO pressure, which is taken to be 1 bar and has been identified to exert a negligible influence on the theoretical polarization curve of  $\beta$ -NiN<sub>4</sub> due to its weak CO binding (Fig. S7†). According to the transition state theory, the rate constant  $k_i$  is calculated by

$$k_i = A' \exp\left(-\frac{\Delta G^\ddagger(U)}{k_B T}\right) \quad (9)$$

where  $A'$  is an effective prefactor. For CO<sub>2</sub> adsorption and CO desorption steps,  $A'$  is taken as  $1 \times 10^8 \text{ s}^{-1}$ ; for electrochemical steps,  $A'$  is set to  $\frac{k_B T}{h} \text{ s}^{-1}$ . The current density is calculated by

$$j = 2e\rho_{\text{Ni}} \text{TOF} \quad (10)$$

where  $\rho_{\text{Ni}}$  is the density of active Ni sites. In this simulation, the concentration of the active Ni sites in the Ni–N–C catalysts was assumed to be  $\sim 1.5 \text{ at\%}$ , which corresponds to  $\rho_{\text{Ni}} \sim 6.6 \times 10^{13} \text{ cm}^{-2}$  based on a graphene slab model. The value of the turnover frequency (TOF) was determined by numerically solving the above rate equations of reaction species at a steady state. The effective CO<sub>2</sub> species that can participate in the CO<sub>2</sub>RR over the catalyst surface has been treated as CO<sub>2</sub> diffusing from the bulk electrolyte CO<sub>2</sub>(aq) to the catalyst–electrolyte interface CO<sub>2</sub>(dl); the reaction rate  $k_1$  was set as  $1 \times 10^6 \text{ s}^{-1}$ , and the resultant polarization curve well matches existing experimental data. Overall, we expected to give a qualitative description for the CO<sub>2</sub>RR performance instead of a quantitative demonstration.

## Author contributions

Y. W. performed the calculations. Y. W., L. Y., and K. Z. analysed the data and wrote the paper. K. Z. supervised the study.

## Conflicts of interest

There are no conflicts to declare.

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