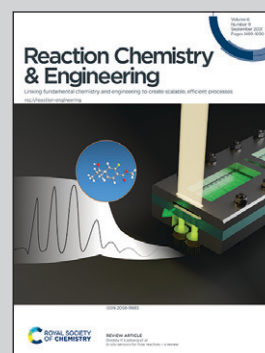


Showcasing research from Dr Hintermair's group and the Dynamic Reaction Monitoring Facility at the University of Bath, United Kingdom.

Engineering aspects of FlowNMR spectroscopy setups for online analysis of solution-phase processes

FlowNMR spectroscopy is a powerful technique for studying dynamic solution phase systems in their native environments in a non-invasive way. In this article, Hintermair *et al.* discuss important engineering considerations and selection of components for setting up effective FlowNMR systems for robust and meaningful operando studies.

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## Engineering aspects of FlowNMR spectroscopy setups for online analysis of solution-phase processes†

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Online analysis and monitoring of solution phase chemistry by way of nuclear magnetic resonance spectroscopy on a recirculating sample from an external reaction vessel (FlowNMR) has proven to be a valuable tool for understanding the dynamic behaviour of complex solution-phase systems in real time. A variety of flow cells and setups have been used at both low and high magnetic field strengths for various applications, and the choice of materials, dimensions and components can have a profound impact on the quality and relevance of the data obtained. Here we review some fundamental engineering aspects of FlowNMR setups to help avoid common pitfalls and work towards establishing good practice quality guidelines (GxP) for FlowNMR investigations in academia and industry.

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### Introduction

High-resolution NMR spectroscopy is a powerful analytical technique due to its high specificity, rich information content, and quantitative, non-invasive nature.<sup>1–3</sup> These attributes make it particularly useful for the analysis of complex mixtures and dynamic molecular systems that are difficult to analyse by alternative methods.<sup>4,5</sup> Applications include virtually all fields of solution phase chemistry such as molecular organic and inorganic synthesis, homogeneous catalysis,<sup>6</sup> supramolecular<sup>7</sup> and polymer chemistry,<sup>8</sup> soft materials,<sup>9</sup> medicinal<sup>10–12</sup> and food chemistry<sup>13,14</sup> as well as metabolomics<sup>15</sup> and biochemistry.<sup>16,17</sup> However, hardware restrictions imposed by the large magnets required to generate stable, homogeneous fields allowing NMR spectroscopy to be performed on carefully equilibrated aliquots of <1 mL make it difficult to use NMR more widely for analysing solution phase processes in their native environments. Mimicking reaction conditions in a sealed sample tube inside the NMR spectrometer can give some insight into the processes in question, but the inaccessibility of the sample and lack of control over heat- and mass-

transport mean that the information obtained from isolated tube experiments may not be truly representative of the system under native conditions.<sup>18</sup> These deviations are particularly relevant to kinetic investigations reliant on obtaining accurate concentration profiles, and may even lead to a different speciation of the system under the restrictions of small, static sample tubes.<sup>18–20</sup> The recent development and commercialisation of benchtop NMR spectrometers based on stable (non-cryogenic) perma-magnets have made NMR spectroscopy more versatile for remote applications,<sup>21–24</sup> but the aforementioned sampling restrictions apply all the same at lower field<sup>25</sup> in addition to the inherent limitations of lower sensitivity and reduced spectral resolution compared to high-field instruments.

FlowNMR spectroscopy (or online NMR spectroscopy as it sometimes referred to) is a simple adaption that alleviates the aforementioned sampling limitations by way of a flow system that continuously circulates an aliquot from an external reaction vessel to the active region of an NMR spectrometer.<sup>4</sup> In this way any changes in sample composition occurring in the external vessel, either as a result of a chemical reaction, biological process or physical change triggered by purposely altered conditions, can be followed and analysed by NMR spectroscopy in real time. Note that the term ‘flow’ in FlowNMR refers to the sample transport, and either batch or continuous flow processes may be investigated with the technique. In this article we shall focus on closed-loop FlowNMR setups for investigating batch processes, but many of the considerations discussed will be relevant to continuous flow application as well.<sup>26,27</sup>

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A number of flow devices have been developed that allow a continuous stream of sample solution to be pumped through the NMR active region of the spectrometer,<sup>28–36</sup> developments that actually date back to early days of NMR spectroscopy in the 1950s.<sup>37</sup> Recent examples include the use of FlowNMR coupled with oxygen probes in the elucidation of the mechanism of amination reactions,<sup>38</sup> the development of low-volume flow system containing biological organisms within the flow tip for solution-state *in vivo* NMR,<sup>39</sup> the use of ultra-fast single scan 2D NMR in flow<sup>40</sup> and the real-time monitoring of oxidative wastewater treatment.<sup>41</sup> Whatever the application, key to obtaining NMR data relevant to the process occurring within the external vessel is an appropriately designed flow system (Fig. 1) that fulfils the following criteria:

a) Full chemical compatibility – the system must not interact with the sample or disturb the system to be studied, and not cause any cross-contamination between different experiments. Conversely, the setup must withstand the conditions used and not be compromised by the application.

b) Provide reaction conditions with appropriate control over key process parameters – all physical parameters of importance to the system studied (light, temperature, pressure, atmosphere, *etc.*) must be sustained throughout the flow path to make the sample inside the NMR representative of the bulk.

c) Deliver a smooth, controlled sample flow throughout the system – minimise sample dispersion and risk of failures, and control any NMR flow effects<sup>42,43</sup> that may influence signal quantification.

d) Safe to use – reliably safe to operate in a multi-user environment and without supervision with highly sensitive and expensive NMR equipment.

With these considerations belonging more to the realm of chemical reaction engineering,<sup>44</sup> teams of molecular scientists and NMR spectroscopists seeking to use FlowNMR spectroscopy for a given application may lack the expertise and practical experience required for efficiently interfacing the reaction vessel with the spectrometer. Several groups have

reported effective FlowNMR setups in the literature,<sup>4,23,41,45–52</sup> but individual solutions differ depending on the specific requirements, and tribal knowledge is rarely shared with the wider community. A general difficulty is that the quality of the NMR spectra obtained are not always indicative of the effectiveness of the setup in fulfilling the above criteria (a–d). Most modern NMR spectrometers will produce high quality spectra even with an inappropriate flow setup that changes the sample on its way from the reaction vessel to the point of detection, so the key issue is how meaningful the data acquired is.

In this paper we highlight and discuss some fundamental engineering aspects of relevance to FlowNMR spectroscopy, evaluate some commonly used hardware solutions, and make recommendations based on our experience to help others to quickly identify appropriate components for safe and effective setups.

Please note that all devices and components used and discussed in this study are commercially available examples that do not necessarily represent the only possible solution or best choice for a given application. Any recommendations made are our personal opinion and do not guarantee safe operation or optimal performance. We invite interested readers to contact us with any questions, comments, or suggestions they may have.

## Results & discussion

### 1. Selection of materials

In its most basic form, a FlowNMR setup comprises a flow device to be used with the spectrometer, some small diameter tubing that creates a closed loop between the reactor and the flow device, and a pump that continuously circulates a portion of the analyte through the system. Fig. 2 illustrates an example using Bruker's InsightMR™ flow tube that may be inserted top-down into a standard NMR spectrometer with a 5 mm or 3 mm probe head. Its design is based on previously published in-out tube assemblies<sup>31,32,53,54</sup> that inject the sample near the bottom of a cylindrical glass tube from where it flows upwards around the central injection capillary and out of the tube again. Alternative designs using flow-through cells and flow probes have been developed<sup>55–57</sup> but few are currently commercially available.<sup>58–63</sup> Characterisation of the sample flow within various flow cells has previously been investigated and will not be covered in this article focussing on the interface of flow device and sample vessel.<sup>64,65</sup>

The tube head is made of PTFE (Teflon) and PEEK (polyether ether ketone) and connects to a flexible umbilical that houses the inlet and outlet sample lines within two larger, concentric Teflon tubings. A heat transfer fluid may be circulated through the latter, and an insulating foam outer layer minimises heat losses to the environment (see section 3) and allows safe handling of the heated flow tube.

The reaction vessel may be any container that suits the application, including simple glassware, multi-compartment

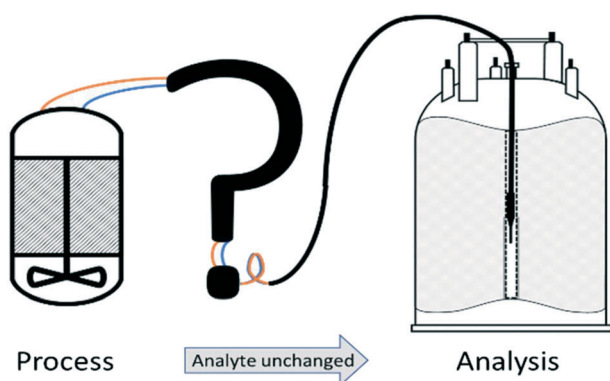


Fig. 1 Schematic illustration of the engineering challenges associated with efficiently interfacing a reaction vessel with an NMR spectrometer.



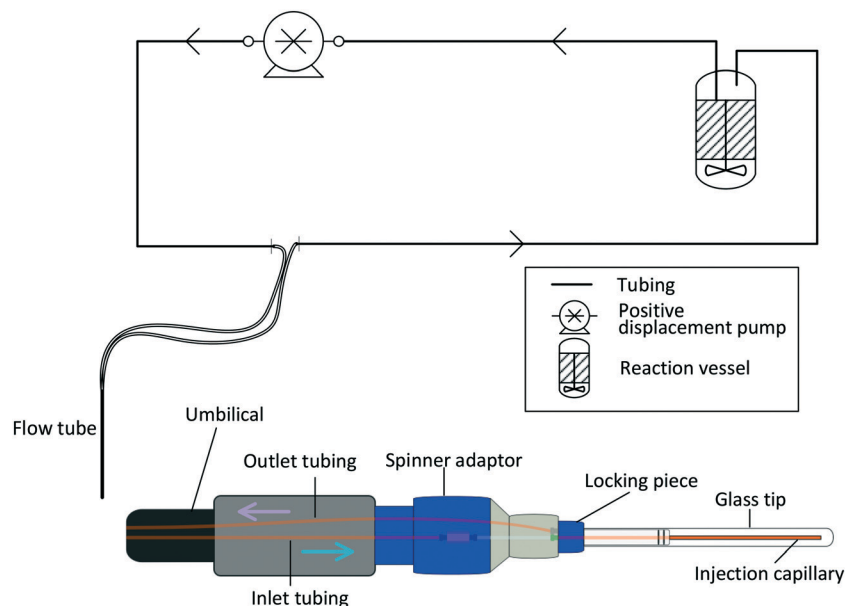


Fig. 2 Schematic piping and instrumentation diagram (P&ID) of a closed-loop recirculating FlowNMR setup with an illustration of a top-down flow tube that can be inserted into an NMR magnet with standard 5 mm probe head. Direction of sample flow is indicated by the arrows.

cells, closed containers (*e.g.* Schlenk flasks), pressure reactors or even biological specimen. As the vessel is typically located beyond the stray field of the NMR magnet any ancillary kit required for process control such as overhead stirrers, heating elements, reflux condensers, dropping funnels, solid addition ports, membranes, electrodes, thermocouples, *etc.* may be used as usual. As long as appropriate mixing is provided to ensure that the sample withdrawn by the pump is representative of the mixture in the vessel at all times, the FlowNMR setup is also independent of scale and may be used with sample volumes from  $\sim 5$  mL (see section 2) up to multi-litre processes. The inlets and outlets of the sample transfer lines inside the vessel should be positioned and secured such that no short-cut of sample flow is possible (*i.e.* at maximum distance to each other, ideally with the mixing element in between), which depending on the application and reaction vessel type may be effected by different means such as clips, rubber seals, glass flanges and polymer or metal fittings.

**1.1. Sample tubing.** In addition to the native reaction vessel, the main wetted materials that contact the sample in such a setup are glass in the tip of the flow tube and the tubing material used for the transfer lines. The use of ferromagnetic materials is not recommended for FlowNMR setups, so common tubing materials are polymers which come with the additional benefits of being lightweight and flexible.<sup>39,40,48,66,67</sup> However, the correct choice of polymer tubing for a given application (*i.e.*, sample composition and reaction conditions) is not trivial, and safety aspects have to be considered in addition to chemical compatibility.<sup>68–71</sup> Table 1 lists some key physical properties of commercially available tubing materials in comparison with austenitic stainless steel as the standard for HPLC applications. While the latter is not recommended for parts of a FlowNMR setup that come close to the magnet it may be used in remote sections of the setup that are safely beyond the stray field of the NMR spectrometer. All of the materials listed in Table 1 are available in various diameters, wall thicknesses and

Table 1 Key physical properties of common tubing materials used in small scale flow setups

Material type	pH range	Temperature range/°C	Pressure rating with 1/16" OD and 0.5 mm ID/bar	Mechanical stability at 23 °C				Gas permeability at 25 °C/10 <sup>-10</sup> cm <sup>3</sup> cm cm <sup>-2</sup> s <sup>-1</sup> cmHg <sup>-1</sup>			
				Tensile strength/ksi	Elongation at break/%	Modulus of elasticity/ksi	Impact strength/ft-lb in <sup>-2</sup>	CO <sub>2</sub>	H <sub>2</sub>	O <sub>2</sub>	N <sub>2</sub>
PEEK <sup>74–76</sup>	0–14	–51 to 100	345	14.00	>50	594	1.57	n.a.	5.28	0.31	0.04
PTFE <sup>77,78</sup>	0–14	–40 to 150	48	4.00	300	58	3.00	6.8	n.a.	n.a.	1.0
FEP <sup>71,76</sup>	0–14	–51 to 50	138	2.90	250–330	n.a.	No break	5.9	1.3	14	2.0
Vespel <sup>79</sup>	1–14	≤200	20	12.47	75	319	1.70	0.5	1	0.1	0.03
Stainless steel (type 316) <sup>80–83</sup>	1–14	–53 to 289	1089	97.61	35	24 000	240	—	—	—	—



lengths from a range of commercial HPLC suppliers. While titanium has long been used for high-pressure NMR tubes<sup>72</sup> and more recently also for recirculating high-pressure NMR reactors<sup>73</sup> there are no reported examples of FlowNMR setups using titanium tubing to date.

As can be seen from Table 1, most polymers have high pH tolerance but notably different pressure and temperature ratings. Their mechanical strengths and elasticities may be viewed as less important once a FlowNMR system is installed, but experience shows that rigid materials like PEEK are noticeably easier to handle and connect securely than the more ductile materials such as Teflon. If the assembly is to be frequently dismantled or reconfigured for different applications mechanical stability becomes relevant for ease of use and prolonging material lifetime.

An important consideration for applications with sensitive reagents and reactions under pressure is the gas permeability of the tubing material (see also section 3), combined with an appreciation that these values may increase when used at elevated temperatures when in contact with organic solvents that may swell the polymer.<sup>84</sup> We also caution that the manufacturer values shown in Table 1 only apply to pristine materials at room temperature, and do not take into account any weakening due to bending, compression, accidental denting or scarring, and fatigue due to prolonged use. Virtually all polymers wear in flow applications and degrade to some degree over time due to a combination of chemical interactions and mechanical stress,<sup>68–70</sup> especially when frequently taken to their limits of temperature, pressure or pH. Unexpected failures can have severe consequences for the user and the valuable equipment, so careful inspection and safety tests are recommended prior to every use, especially when involving harmful or toxic substances or when working with high pressures. Note that the values shown in Table 1 specifically refer to tubing examples with a wall thickness of 540  $\mu\text{m}$ , and different limits apply to thinner or thicker variants.

As mentioned in the introduction, chemical compatibility is a key consideration for choosing the correct tubing material. Stainless steel for instance has a high risk of stress corrosion cracking where in contact with chlorinated solvents and will be attacked by most inorganic and organic acids.<sup>85,86</sup> PEEK is prone to significant solvent uptake and swelling with methylene chloride, tetrahydrofuran and dimethyl sulfoxide,<sup>84</sup> and Vespel is known to be incompatible with amines, dimethyl formamide and dimethyl sulfoxide.<sup>87–89</sup> Many polymer compatibility tables can be found online (for an example see ESI† section 5.0), and in case of doubt confirmation should always be sought from the manufacturer. For studying photochemically active substances by FlowNMR it is important to note that while PTFE and FEP transmit visible light  $>340\text{ nm}$ <sup>90</sup> Vespel, PEEK and stainless steel are non-transparent and protect the sample from UV-vis irradiation.

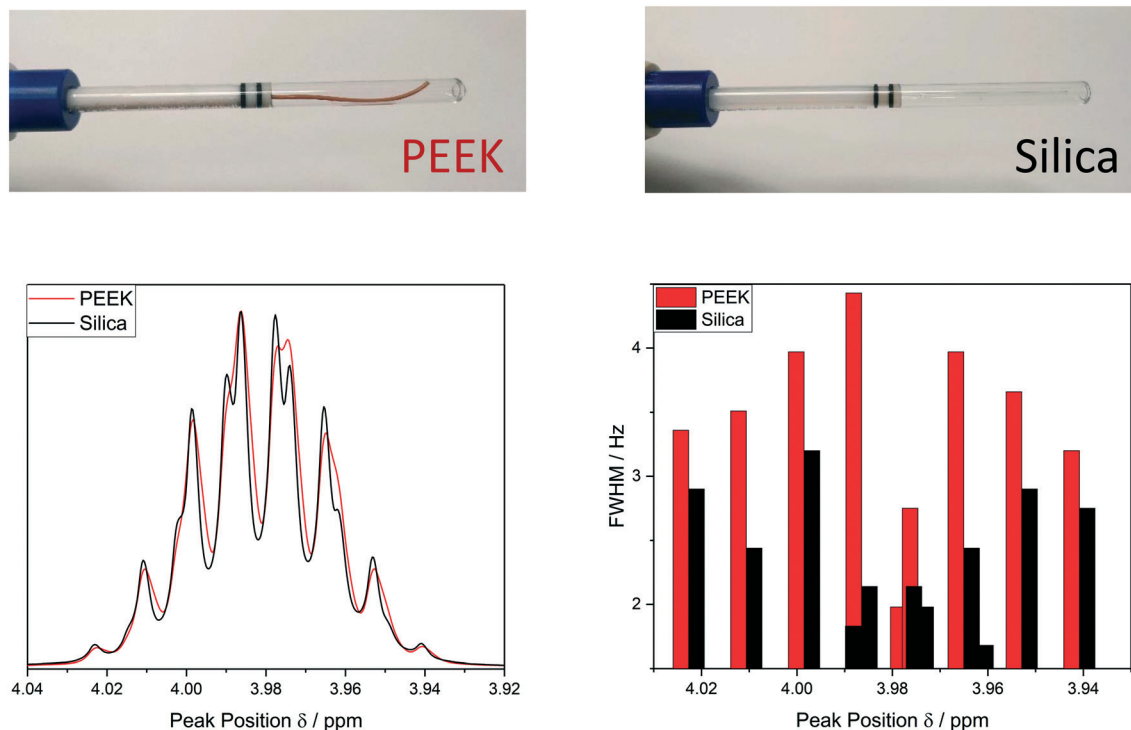
Another consideration for choosing an appropriate tubing material is the potential carry-over of compounds between

different applications. For instance, we have found PEEK to be particularly prone to uptake of small amounts of polar substances such as water, short chain alcohols and acetone (as often used for cleaning) which may then leach back into subsequent applications. Finally, although rather rare, some tubing materials themselves can chemically alter the sample studied. Stainless steel for instance is known to be mildly oxidising and has been observed to trigger radical reactions with  $\text{O}_2$  and peroxides.<sup>86</sup> Thorough control reactions checking the mutual compatibility of sample and flow system are thus recommended at the beginning of every FlowNMR investigation in order to generate meaningful data.

**1.2. Injection capillary.** The design of the flow cell may have implications on the NMR spectral quality obtained.<sup>30</sup> In the example shown in Fig. 2, the sample injection capillary in the glass tip penetrates the active region of the RF coils collecting the FID signal from the sample, and its positioning thus impacts on the field homogeneity during use. Typically, the end of the sample inlet tubing itself is used as the injection capillary, which due to the flexible nature of most polymer tubing (see Table 1) may not always be perfectly straight and concentric. Any deviation from this ideal position can have a negative impact on spectral resolution, particularly when the pressure drop across the system is high (see section 2) and a pump with appreciable pulsation is used (see section 4) which may lead to wiggling of the capillary during the experiment. A useful modification therefore is to install a rigid injection capillary made of fused silica instead, connected to the polymer inlet tubing *via* miniature plastic unions inside the flow tube head (see the ESI† section 6.0 for details). The latter also make the tube head easily detachable from the umbilical for maintenance. Fig. 3 shows a comparison of polymer *versus* silica injection capillaries with examples of their respective  $^1\text{H}$  FlowNMR spectra obtained at 500 MHz. Replacing PEEK with silica reduced  $^1\text{H}$  linewidths in flow by up to 50% in this case, and even larger improvements can be obtained with silica compared to more flexible materials (such as Teflon) and when using more viscous samples. An additional practical advantage of the uniform positioning of the silica capillary is a markedly higher shim reproducibility between different runs that reduces start-up times of new FlowNMR experiments. Although exemplified for a particular commercial flow tube here, these considerations likely apply to any flow tube with an injection capillary inside the NMR active region but not to simple flow-through cells as used in closed flow probes and most low-field instruments.

**1.3. Connections.** A particular focus during the assemblage of a FlowNMR setup should lie on any connection points throughout the system, as these often cause flow restrictions and/or turbulences that make them prone to failure. The safety limits of any flow system are dictated by their weakest point, and connections between different materials should thus receive particular attention. Early examples of FlowNMR setups used simple push-fit connections, sometimes secured with shrink tubing, tape or





**Fig. 3** Top: Photographs of a 1/32" OD (500 μm ID) PEEK injection capillary and a 0.8 mm OD (534 μm ID) fused silica injection capillary fitted to a Bruker InsightMR™ flow tube. Bottom: Comparison of <sup>1</sup>H NMR spectral quality and peak widths achievable at 500 MHz with a standard 'lctshim' routine on a sample of isopropanol flowing at 4 mL min<sup>-1</sup> at 20 °C using a peristaltic pump.

superglue. While perhaps practical and possibly acceptable as a temporary emergency fixes these are generally a reliable recipe for disaster, as they may work for a certain period and then suddenly fail without warning (as experience has shown, typically shortly after the satisfied user has left the room). A wide range of pressure- and temperature-rated small scale HPLC unions and fittings that can be installed and removed without special tools are commercially available from various HPLC suppliers. Single piece finger-tight fittings made of PEEK with "zero volume" PEEK unions from VICI or IDEX have proven very effective in our experience when correctly used with a sharp tubing cutter. Since the sample does in theory not come into contact with either the fitting or the union, they may in principle be used with any sample tubing. However, if the thermal expansion coefficients of the materials used differ too much there will be an inherent risk of leakage or failure when going to low or high temperature.<sup>91</sup> A test run of the targeted reaction conditions with the flow tube safely stored inside a ventilated fume hood is recommended after fitting any new components. The various mechanical strengths of the tubing materials listed in Table 1 are useful indicators for the reusability of the latter in these fittings, with the softer polymers requiring more frequent trimming in order to seal properly against the compression ferrule of the fitting. Some connections to pumps and other components (see section 3) may require different types of fittings (such as flat flange ferrules or NPT threads) for which pressure- and temperature-rated adaptors to standard HPLC fittings can usually be sourced from HPLC

suppliers.<sup>92</sup> Again, we caution against the use of any home-made solutions and recommend keeping a healthy stock of a range of relevant consumables to keep the FlowNMR setup in good working condition. Finally, whatever materials are chosen, particular care should be exercised to eliminate any voids or kinks in all connections throughout the flow path, particularly those involving changes of internal diameter (ID), as these may have a negative impact on the flow profile and residence time distribution of the sample which may influence the analytical results (see section 4). If any unions or connectors come with smaller internal diameters than the sample tubing these can easily be rebored to the required size with a set of microdrills, a quick operation that may save valuable experiment time by reducing the risk of pump failure or blockages during use.

## 2. Volumes, internal diameters, and the importance of pressure drop

For most applications, the user will seek to minimise the amount of sample held inside the flow setup (*i.e.*, the flow tube plus any ancillary tubing and pump) to have maximum control over the bulk of the sample inside the reaction vessel where conditions may be purposely altered or reagents added at a specific point in time. This is especially true for precious analytes and in cases where tight process control is required. As a rule of thumb, we usually scale reactions such that at least 2/3 of the sample reside inside the reactor at any time, which in most cases proves effective to make the reaction



amenable to study by FlowNMR spectroscopy without affecting the kinetics or the speciation of the system in flow. Specific limits for acceptable volume ratios will depend on whether any analyte may respond to potentially different conditions inside the flow system as compared to the reactor (for example an overhead pressure of reaction gas *versus* dissolved gas in solution only) on the time-scale of its journey from the reactor and back, so absolute recommendations can unfortunately not be given. For fast reactions where delay and travel times may be critical, we recommend varying the flow rate during the experiment<sup>‡</sup> to test if different species are observed as a function of the mean residence time of the sample in the flow system.

Due to the size and geometry of high field NMR instruments (even those with shielded magnets) several metres of tubing are typically required for creating a closed loop FlowNMR setup connected to an external sample vessel. Length scales are thus dictated by local restrictions of how close to the magnet the setup may be placed and operated in a safe manner. Total path lengths of 8–14 m for the entire flow loop are common, but even setups with >20 m of tubing have been realised in laboratories where access to the NMR machine was more restricted. With a fume cupboard housing the reactor and pump about 1.5 m away from a shielded 500 MHz NMR magnet, our FlowNMR setup has a total path length of 12.4 m (Fig. 4).

With the given internal volumes of the flow device§ and pump used (see also section 4), the main parameter to vary for reducing internal volumes is the tubing internal diameter. 1/16" and 1/32" OD HPLC tubing (the most common sizes used for small scale flow applications) are available with a range of internal diameters of 100–1000 µm.¶ Table 2 compares some exemplary volumes, flow velocities, residence times and Reynolds numbers that these dimensions translate to for a tubing length of 10 m at a volumetric flow rate of 4 mL min<sup>-1</sup>.

Reynolds numbers for typical organic solvents are in the laminar flow regime for all dimensions shown in Table 2, and even low viscosity liquids like acetone would not flow turbulently at 4 mL min<sup>-1</sup> through 100 µm ID tubing at room temperature (Re < 3000). It may thus seem that small tubing IDs would be best to minimise sample volumes and travel times. While this is true, we caution that the smaller the ID the higher the sensitivity of the setup to blockages from accumulation of solids which can cause loss of valuable experiment time (see also section 3.4). From our experience we recommend 500 µm as the minimum tubing ID that can be used efficiently with most liquids and commonly used

pumps (see also section 4), but smaller IDs may be usable with appropriate precautions if required by the application. A practical limitation to minimising the tubing ID is the pressure drop (or flow resistance) generated by shear forces within the sample and with the tubing walls that need to be overcome by the pump. While such relatively low levels of hydrostatic pressure are unlikely to have a noticeable effect on sample composition or the NMR analysis, flow resistance places additional stress on the tubing, flow cell and all connections throughout the setup, in addition to contributing to pump wear.<sup>93–97</sup> The Darcy–Weisbach equation allows calculating pressure drops of incompressible liquids flowing laminarily through a cylindrical pipe using empirically derived friction factors.<sup>98,99</sup> For the conditions applying to the scales of FlowNMR setups (see Table 2), the equation can be rearranged to express the flow resistance ( $\Delta p$ ) as a function of the flow rate ( $Q$ ), the dynamic viscosity of the fluid ( $\eta$ ), and the length ( $L$ ) and internal diameter ( $D_c$ ) of the tubing (eqn (1), see ESI† section 7.0 for derivation).

$$\Delta p = \frac{Q \cdot \eta}{147.26} \sum \frac{L}{D_c^4} \quad (1)$$

Using this relationship, pressure drops may be calculated to determine whether the setup will be able to operate safely and effectively under the conditions chosen. As indicated in Fig. 4, we have opted for a combination of tubing IDs throughout our FlowNMR system to strike a balance between minimising volumes and travel times while keeping the overall pressure drop manageable. The short sample tubing between the reaction vessel and the pump inlet has a relatively large ID of 1 mm to minimise suction pressure drops that can lead to pumping issues (see section 4), and smaller IDs of 500 µm are used for quickly delivering the sample to the NMR tip for detection. The tubing returning the sample to the vessel has an intermediate ID of 762 µm not to add too much flow resistance but keep overall volumes manageable. Using eqn (1) additively for each section of different ID, Fig. 5 shows some calculated pressure drops of various solvents through the entire flow setup shown in Fig. 4 at different temperatures to illustrate the effect of solvent viscosity. Note that if the same setup was built using 100 µm ID tubing throughout (see Table 2), pressure drops at 4 mL min<sup>-1</sup> would be in the order of 700–2300 bar!

We have found eqn (1) to be fairly accurate, and measuring the pressure drop of solvent flowing through the system thus serves as a reliable indicator for how healthy a FlowNMR setup is prior to use. Roughened internal surfaces from polymer degradation, kinks and bends in the flow path as well as ID restrictions from fitting compression all contribute to increased flow resistances. In our experience a FlowNMR setup functions well with up to 25% higher-than-ideal flow resistance values in practice, and monitoring the pressure drop of a setup over time serves as a useful indicator for developing blockages and progressive wear.

<sup>‡</sup> Note that changing the flow rate may also affect flow correction factors required for accurate signal quantification.

<sup>§</sup> 3 mm glass tips can be fit to most flow tubes with a 0.8 mm O.D. injection capillary to reduce internal volumes but come at the expense of reduced NMR sensitivity when used with a standard 5 mm probe.

<sup>¶</sup> As pointed out in the discussion of Table 1, the individual temperature and pressure ratings for the respective tubing wall thicknesses should always be checked.



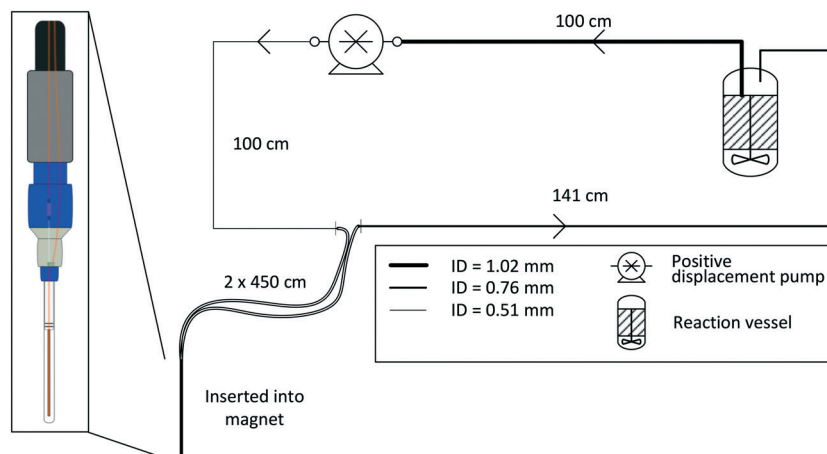


Fig. 4 P&ID schematic of a closed-loop recirculating FlowNMR setup with exemplary length scales and tubing ID (indicated by line thickness).

Table 2 Key flow parameters calculated for sample tubing of different internal diameter

Tubing I.D./ $\mu\text{m}$	Flow velocity <sup>a</sup> /m s <sup>-1</sup>	Reynolds number <sup>b</sup>	Internal volume <sup>c</sup> /mL	Residence time <sup>a,c,d</sup> /s
100	8.5	600–2000	0.1	1.5
500	0.3	150–400	2.0	30
1000	0.09	50–250	7.9	119

<sup>a</sup> For a volumetric flow rate of 4 mL min<sup>-1</sup>. <sup>b</sup> Range for common organic solvents at room temperature. <sup>c</sup> For a total tubing length of 10 m.

<sup>d</sup> Theoretical values applying to the tubing only; see section 4 for residence time distribution analyses of complete FlowNMR setups.

### 3. Devices and considerations for process control and safety

A FlowNMR setup bears many similarities to small-scale continuous flow synthesis setups for which similar engineering considerations apply.<sup>100,101</sup> Indeed, many components useful for FlowNMR spectroscopy have become commercially available thanks to flow chemistry pushing the development and adaption of what used to be mere add-ons and consumables for high pressure liquid chromatography.

**3.1. Pressure.** As mentioned in the preceding section, pressure sensors are a useful addition to a FlowNMR setup in order to monitor pressure drops as an indicator for unusual flow resistances within the system. Although some liquid pumps come with in-built pressure sensors, we have found that these are rarely designed for uniform sample flow and often have internal volumes in excess of 1 mL with less-than-ideal geometries (particularly HPLC pumps). We recommend bypassing these if possible in order to minimise sample hold-up, and insert several miniature flow-through pressure sensors in the sample path instead. The QuickStart™ series from IDEX are an example of an easy to use low-pressure solution up to 200 psi or 13.8 bar (proofed to 400 psi or 28 bar) that can be powered by and read out to a computer *via* USB connection. Their 1.2 mm ID bore with 50  $\mu\text{L}$  internal volume contains PEEK, Viton and stainless steel as the wetted materials. Alternative solutions with higher pressure ratings of up to 2500 psi or 172 bar and fully inert, straight-bore titanium sensing channels of 11  $\mu\text{L}$  volume are available from other suppliers such as DJ Instruments. Note that although most of these devices have declared temperature limits of 50–60 °C, if the sensor body including electrical connections remain at room temperature these can often be used with much higher sample temperatures (in our experience up to 120 °C as long as heating rates do not exceed 10 °C min<sup>-1</sup>). The advantage of having more than one measurement point throughout the flow path is that any restrictions may be more easily narrowed down to certain sections of the setup for quick, targeted maintenance and repair.

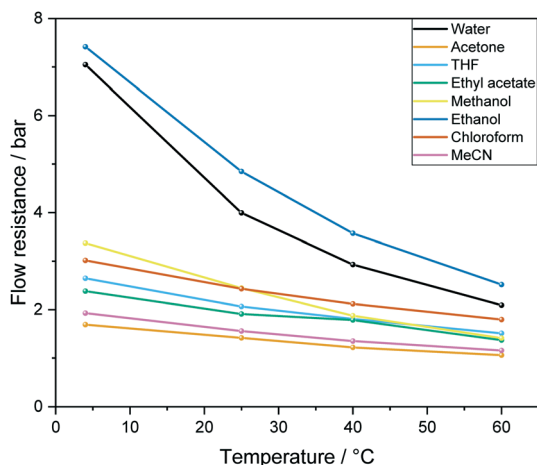


Fig. 5 Calculated overall flow resistance (pressure drop) from 12.4 m PEEK tubing as detailed in Fig. 4 caused by a range of solvents at different temperatures at a flow rate of 4 mL min<sup>-1</sup> according to eqn (1).



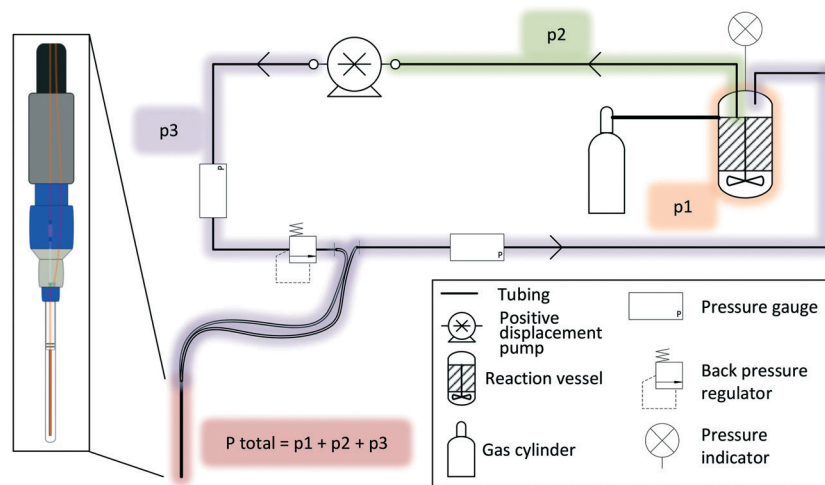


When liquid phase reactions under a positive gas pressure are being investigated, an independent pressure sensor in the reactor headspace is recommended, as the total pressure in the setup will be the sum of any gas pressure applied to the reactor plus the pressure drop from the inherent flow resistance of the liquid travelling through the tubing (Fig. 6). It is important to know and monitor the highest pressure throughout the system in order not to exceed the safety limits of any components used. Compact digital pressure transmitters such as the A-10 model from WIKA (made of stainless steel and available with a range of seal materials for various pressure and temperature ranges) allow monitoring reactor headspace pressure at the point of use *via* a digital display while also logging the data on a computer (see section 5). A very useful safety feature that we warmly recommend for any FlowNMR setup is to add a back pressure regulator (BPR) to a T piece in the flow path directly before the most vulnerable section (in most cases the flow tube, whose glass tip typically has the lowest pressure rating of all components and would cause maximum damage in case of failure).<sup>102</sup> A range of small-scale BPRs made of PEEK that connect to standard 1/16" fittings are available from various HPLC suppliers with a range of pressure ratings. Unlike bursting discs, spring-loaded BPRs close again after relieving any excess pressure without permitting air or moisture into the sample stream, so are an ideal choice for protecting both the valuable equipment and the sensitive sample during unsupervised long-term operation.

As mentioned in section 1, the various polymeric tubing materials used for FlowNMR setups have different gas permeabilities (see Table 1). This means that some degree of gas loss over time is to be expected from a pressurised FlowNMR setup *via* diffusion through the tubing wall. Fig. 7 exemplifies pressure loss with three different reaction gases as measured in the reactor headspace during an experiment that circulated toluene through the flow setup shown in Fig. 4 at room temperature.

As can be seen from the results shown in Fig. 7, PTFE has a four times higher hydrogen permeability than PEEK, and H<sub>2</sub> passes more easily through PEEK than CO and CO<sub>2</sub> do. Note that the initial pressure drops in Fig. 7 reflect gas dissolution into the liquid phase and not diffusion through the tubing walls. The exact magnitudes of gas loss from a FlowNMR experiment will depend on the tubing wall thicknesses, solvent and temperature used, but the representative results in Fig. 7 show that noticeable pressure loss may occur during a FlowNMR experiment by way of diffusion even in the absence of any leaks. A 40% pressure loss may have significant effects on the kinetics of a hydrogenation reaction for example and potentially even change the speciation of the catalyst,<sup>46,103</sup> so the choice of tubing material can be important in generating meaningful results from a FlowNMR investigation. As none of the polymer tubings we are aware of have negligible gas permeabilities like metal, headspace pressure drop curves measured during FlowNMR experiments do not necessarily correlate with the reaction progress seen in the liquid phase by NMR spectroscopy. Thus, reactions under gas pressure are best conducted with the reactor open to a gas cylinder or buffer vessel maintaining constant pressure throughout the experiment to simplify the kinetics. From a health and safety point of view, while most NMR laboratories are already equipped with oxygen depletion alarms for safeguarding against the risk of asphyxiation from He and N<sub>2</sub> boil-off, the addition of portable sensors for hazardous gases is recommended for any FlowNMR applications using H<sub>2</sub>, CO and other toxic or flammable gases.

**3.2. Sample flow.** The volumetric flow rate of the sample not only determines its residence time in the tubing and the pressure drop across the system, but also has direct consequences on the NMR results obtained. Both in-flow effects that may reduce peak integrals and out-flow effects that shorten the apparent spin relaxation times are directly flow rate dependent, and thus knowledge of and control over



**Fig. 6** Representation of the additive nature of pressure along the flow path where the NMR tip experiences pressure equal to that applied to the reaction vessel plus the hydrostatic pressure drop caused by the action of flow through the small ID tubing.



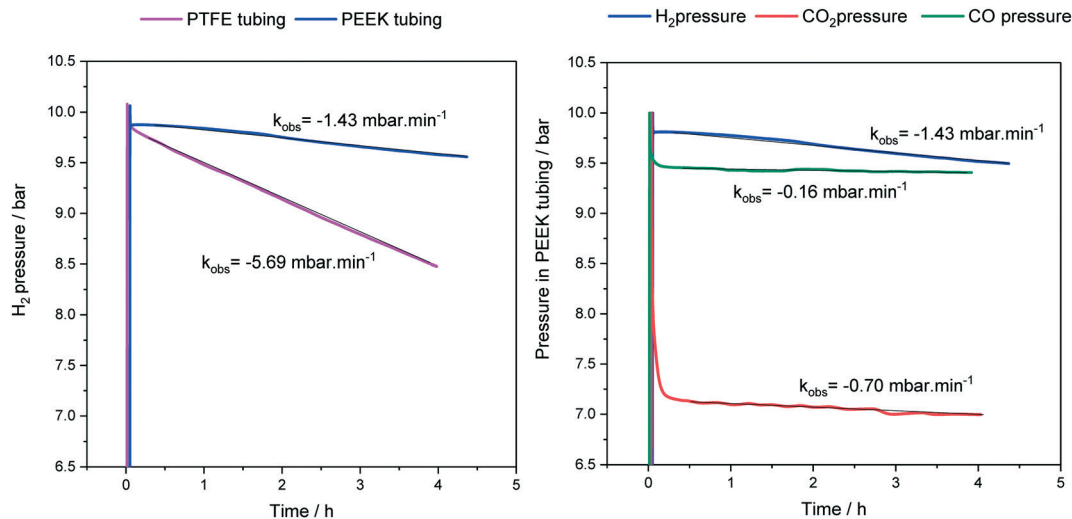


Fig. 7 Headspace pressures and gas loss rates during continuous toluene circulation (15 mL) through the flow setup shown in Fig. 4 at 25 °C and 4 mL min<sup>-1</sup>.

the actual flow rate applied is important.<sup>42,43,64,65</sup> The selection and use of pumps will be discussed in more detail in section 4, but with any setup deviations or fluctuations of sample flow need to be known in order to generate accurate results from a quantitative FlowNMR experiment. Miniature flow meters are useful devices in this respect, however, not many measuring principles lend themselves for inert, non-restrictive flow quantification of mixtures of unknown or variable physical properties (density, viscosity, thermal conductivity, *etc.*). Although a relatively expensive option (>£3000), Coriolis flow meters are most suitable for this task as they provide an accurate response directly proportional to mass flow irrespective of the phase behaviour, in a completely non-invasive way. The mini Cori-Flow M13 from Bronkhorst for example is rated for samples up to 200 bar and >100 °C (again, as long as the instrument body remains at room temperature) and is available with 1/16" fittings and a 500 µm ID capillary loop. While it can be used to actively control pumps *via* an appropriate electronic interface (see section 5) we typically only use the flow meter to calibrate and periodically check our pumps without including the meter permanently in the flow path due to the added internal volume (~1.1 mL incl. fittings) and sample heat loss to the large stainless steel body required for dampening vibrational noise. For applications where the former issues are less critical the use of an actively regulated pump may be advantageous, however, great care must be exercised to ensure that no deposits build up on the Coriolis capillary as even minor changes of its mass will falsify the readings. We also caution that blockages in the Coriolis capillary are very expensive to repair.

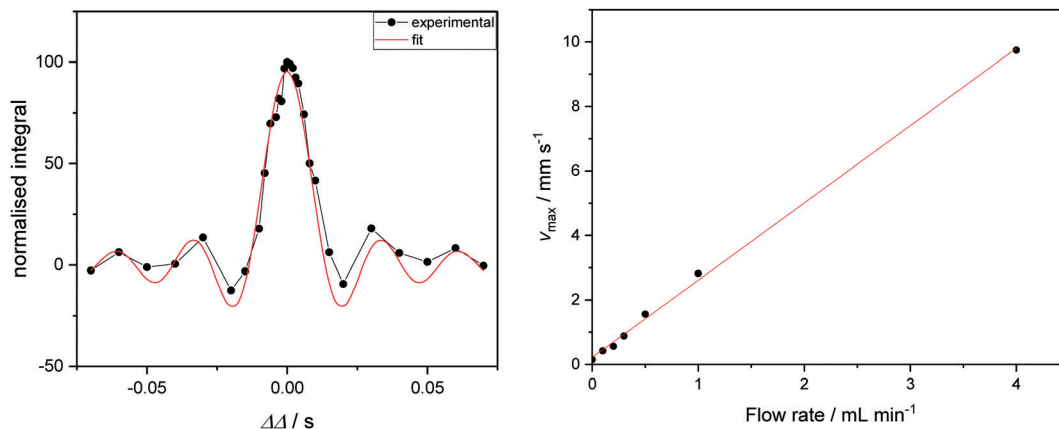
If the investment in a Coriolis flow meter cannot be justified, the maximum flow velocity of sample through a FlowNMR setup may alternatively be measured by one-dimensional velocity imaging experiments. Varying a deliberate diffusion delay imbalance ( $\Delta\Delta$ ) during a pulsed

field gradient experiment on a flowing solution of a paramagnetic relaxation agent such as [Cr(acac)<sub>3</sub>] allows quantification of sample flow in the *z* direction. Signals from species in solution acquire a phase shift proportional to their velocity and to  $\Delta\Delta$ , which gives rise to a loss of signal intensity for non-zero  $\Delta\Delta$  (Fig. 8, left). Fitting the integral data yields linear displacement velocities that may be used to correlate with the volumetric flow rate supplied by the pump (Fig. 8, right).<sup>104</sup> Although not an absolute, independent measure of flow rate such as provided by a flow meter, these measurements may be used in conjunction with simple flow tests (using a graduated cylinder or analytical balance) to ensure pump linearity and flow rate consistency by NMR spectroscopy.

Many FlowNMR setups include a bypass loop consisting of a short piece of tubing between the entrance and exit of the flow device that allows isolating the sample in the NMR spectrometer from the reactor for either more detailed analysis or safety reasons.<sup>42</sup> While in principle a useful feature, we have found most multi-position valves used for manually selecting the sample flow path to have some slip (especially with heated samples under pressure) that increases with use over time, as the bypass offers the liquid a lower pressure drop pathway to being forced through the 9 m long flow tube. Having a part of the sample slipping through the bypass instead of flowing through the NMR is a potentially serious source of error that can be difficult to notice, and we thus we recommend either using high-grade pressure rated switching valves or simply omitting any bypass loops. In our experience, stopping the pump is just as easy and effective as switching the sample to flow through the bypass if needed.

**3.3. Temperature.** Even for room temperature FlowNMR applications accurate control over sample temperature is imperative, as the magnetic field homogeneity and thus spectral quality are sensitive to temperature gradients and





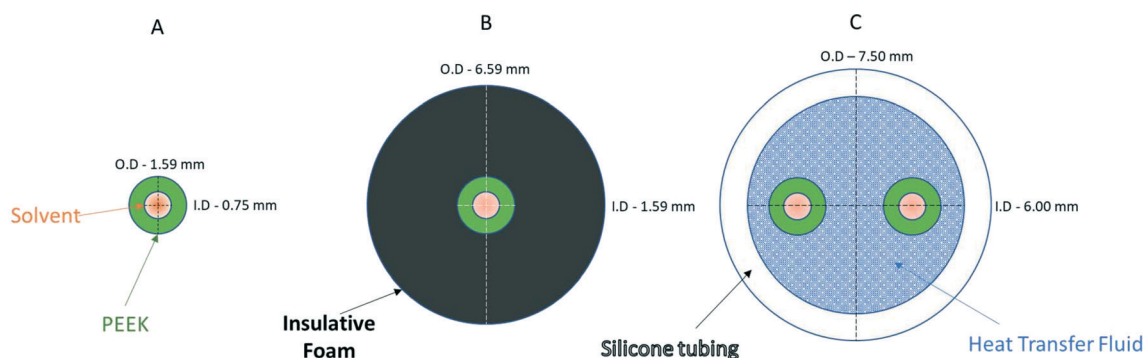
**Fig. 8** Left: Signal intensity as a function of  $\Delta\Delta$  for a flowrate of  $1.0 \text{ mL min}^{-1}$  (see ESI† for graphs of other flow rates). Curve fitting gives access to the maximum velocity. Right: Correlation of linear sample velocities derived from  $\Delta\Delta$  fitting with volumetric flow rates supplied by the peristaltic pump.

convection within the sample.<sup>104</sup> Reaction rates and equilibrium positions may also be affected by the heat of a reaction occurring in the sample, so ensuring isothermal conditions is important for virtually all FlowNMR applications. While the volume in the NMR-active region of a flow tube or probe may be thermostated by the gas flow of the spectrometer,<sup>105</sup> and the sample vessel temperature would be controlled *via* application-typical means (heating bath, blocks or cartridges, cooling baths, Peltier elements, *etc.*), any sample travelling from the reactor to the NMR is more challenging to heat or cool accurately and uniformly.<sup>56</sup> In order to illustrate temperature stability throughout a typical flow path we have modelled the heat loss from liquid samples flowing laminarily through  $1/16''$  PEEK tubing in three different scenarios: (A) bare tubing in air, (B) with passive insulation, (C) with active regulation using a heat transfer fluid (Fig. 9). Applying eqn (2) iteratively over  $1.0 \text{ cm}$  increments of tubing length using the relevant heat capacities, thermal conductivities and heat transfer coefficients of all materials used yields an accurate prediction of any heat transfer occurring under these conditions (as verified experimentally, see ESI† section 9.2 for details).

$$T_{\text{out}} = T_{\text{in}} - \frac{kA\Delta T}{C_p\rho\dot{V}} \quad (2)$$

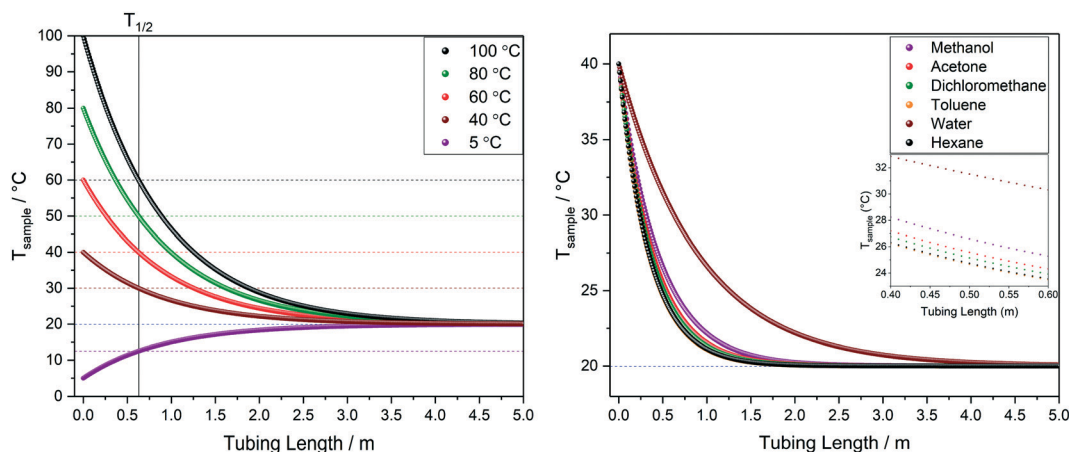
Using water at  $4 \text{ mL min}^{-1}$  as an example, heat loss from bare  $1/16''$  PEEK tubing is significant as shown by the temperature profiles over path length shown in Fig. 10 (left), and is even more pronounced for samples with lower heat capacities such as organic solvents (Fig. 10, right). Note that the model was applied to tubing only and does not account for additional sample heat loss through other devices such as pump heads. The model also does not take convection into account, so any air flow over the tubing (*e.g.* from a fume hood or other active ventilation) will cause even more rapid cooling than what is calculated here.

The calculated temperature profiles for uninsulated tubing in Fig. 10 show that most samples would experience complete heat loss to reach room temperature within 2–4 m of travel under these conditions (less than half the path length of a typical FlowNMR setup). Hence, if for example a sample aliquot left the reactor at  $100 \text{ }^\circ\text{C}$ , with no insulation it will have cooled to room temperature before it reaches the



**Fig. 9** Cross-sectional diagrams of scenarios for no heat regulation (A), passive heat insulation (B), and active heat regulation (C). Models use  $1/16''$  PEEK tubing, insulative foam and general-purpose silicone tubing filled with a 50 : 50 ethylene glycol/water mixture (see the ESI† section 9.0 for details).





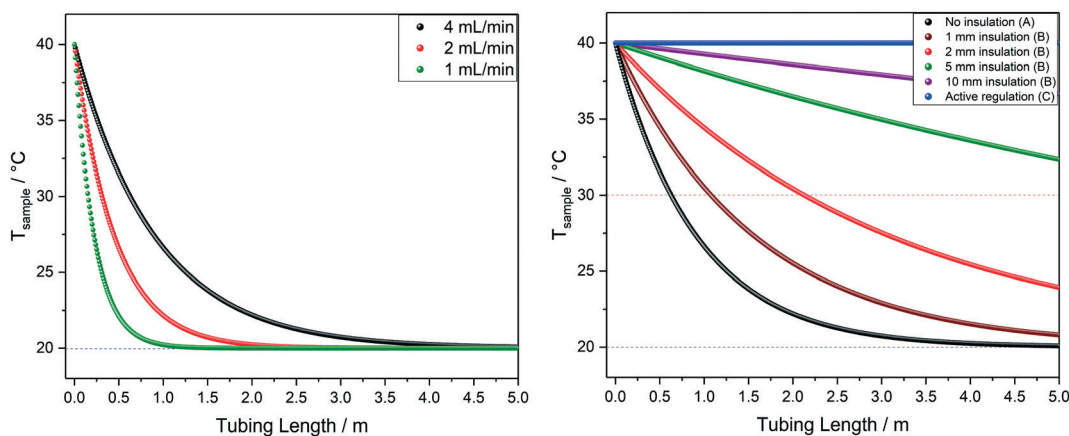
**Fig. 10** Left: Modelled temperature profile of water over tubing length at different starting temperatures. Right: Comparison of temperature profiles for different solvents starting at 40 °C. All at 4 mL min<sup>-1</sup> flow rate through 1.6 mm OD/0.76 mm ID PEEK tubing in air at 20 °C (blue dotted line) corresponding to scenario A in Fig. 9.

NMR active region, causing significant convection and spectral distortion if the probe temperature is set to higher temperatures in anticipation of studying the reaction at 100 °C. Such temperature swings may also have negative effects on the sample itself, including a change of speciation, reaction rates or even homogeneity if any component is near their solubility limit under process conditions. As heat transfer between regions of different temperatures is a first-order process driven by  $\Delta T$ ,  $T_{1/2}$  values can be derived from the heat loss curves shown in Fig. 10 which may be useful metrics to remember: uninsulated 1/16" tubing will cause losing half the initial temperature difference within 30–60 cm for organic solvents or water flowing at 4 mL min<sup>-1</sup>.

The influences of tubing diameter, material type and wall thickness on heat transfer rates were found to be relatively small (Fig. S12<sup>†</sup>), but heat loss is directly proportional to the residence time of the sample as determined by the flow rate applied (Fig. 11, left). At 1 mL min<sup>-1</sup> water will have lost half

its initial temperature difference after 16 cm of travel and will have fully equilibrated with the environment after another meter (*i.e.* four times faster than at 4 mL min<sup>-1</sup>).

Finally, Fig. 11 (right) shows the effect of adding various thicknesses of insulating foam around the sample tubing (passive insulation, scenario B in Fig. 9) compared to active heat regulation with a heat transfer fluid (C in Fig. 9). From the profiles shown it can be seen that 1 cm thick insulating foam can help to limit sample heat loss to the environment relatively well, but only active heat regulation provides steady and uniform sample temperatures throughout the flow path. As mentioned above in section 1, the InsightMNR™ flow tube is set up for the use of a heat transfer fluid as depicted in Fig. 9 C, and we hope that the data shown here will convince users to make use of it and take appropriate heat management precautions for the rest of their FlowNMR setup as well. A large variety of recirculating heat exchangers with different bath volumes, pump capacities and temperature ranges are



**Fig. 11** Left: Modelled temperature profiles of water at 40 °C flowing through 1.6 mm OD/0.76 mm ID PEEK tubing in air at 20 °C (blue dotted line) at various flow rates, corresponding to scenario A in Fig. 9. Right: Modelled temperature profiles of water at 40 °C flowing through 1.6 mm OD/0.76 mm ID PEEK tubing in air at 20 °C (blue dotted line) at 4 mL min<sup>-1</sup> with different levels of insulation, comparing scenarios A, B and C from Fig. 9.



commercially available from suppliers such as Julabo, Huber, Lauda and Thermo Fisher. Simple water–ethylene glycol mixtures can be used from  $-50$  to  $100$  °C,<sup>106</sup> and synthetic oils based on polydimethylsiloxane offer wider temperature ranges of  $-100$  to  $>250$  °C if needed. Considering the relatively long tubing pathways of 10 m (or more) used in a typical FlowNMR setup, we recommend using several recirculating heat exchangers for different sections of the setup in order to minimise temperature gradients from heat loss of the thermofluid. Fig. 12 illustrates how we have used three independent circuits to regulate different sections of the setup: the sample vessel or reactor (red), the transfer tubing (yellow) and the flow tube (blue), in addition to the sample tip that is controlled by the NMR probe gas flow. Having independent temperature control over different sections of the flow setup also opens up possibilities for *controlled* temperature gradients that may be useful for resolving NMR spectral features that may be obscured by dynamic exchange phenomena at process temperature without causing spectral distortions by *uncontrolled* temperature gradients.<sup>107</sup> Fig. 13 illustrates the NMR spectral changes resulting from non-uniform sample heating throughout the flow path at 500 MHz.

Note that the perfect temperature stability of actively regulated sample tubing shown in Fig. 11 (right) is based on the assumption that any heat loss of the thermofluid to the environment is negligible during its residence time throughout the flow path. This is of course only true if the outer surface of the tubing is well insulated, and a sufficiently high flow rate of heat transfer fluid is applied to compensate for any loss. Quantitative heat transfer predictions become less accurate with increasing numbers of materials and

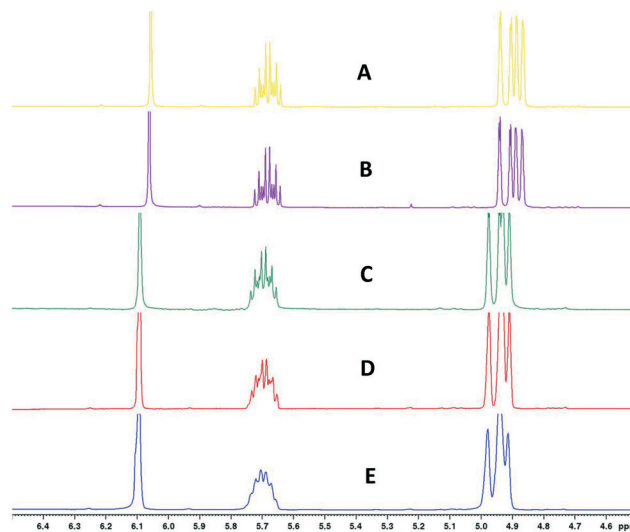


Fig. 13  $^1\text{H}$  FlowNMR spectra of 1-hexene and 1,3,5-trimethoxybenzene at different heat regulation conditions. A) Entire FlowNMR setup at room temperature without heat regulation. B) Entire FlowNMR setup regulated to  $25$  °C with the three heat exchangers as shown in Fig. 12. C) Reactor (heat exchanger 3) at  $50$  °C, flow tube (heat exchanger 2) at  $60$  °C and sample tubing (heat exchanger 1) at  $60$  °C. D) Reactor (heat exchanger 3) at  $50$  °C, flow tube (heat exchanger 2) at  $50$  °C and sample tubing (heat exchanger 1) at  $50$  °C. E) Reactor (heat exchanger 3) at  $50$  °C, flow tube (heat exchanger 2) at  $0$  °C and sample tubing (heat exchanger 1) at  $25$  °C.

interfaces, especially if some of the liquids flow in counter-current mode, so these scenarios become difficult to model accurately. However, due to the high mass ratio of heat exchange fluid *versus* sample used in the dimensions shown

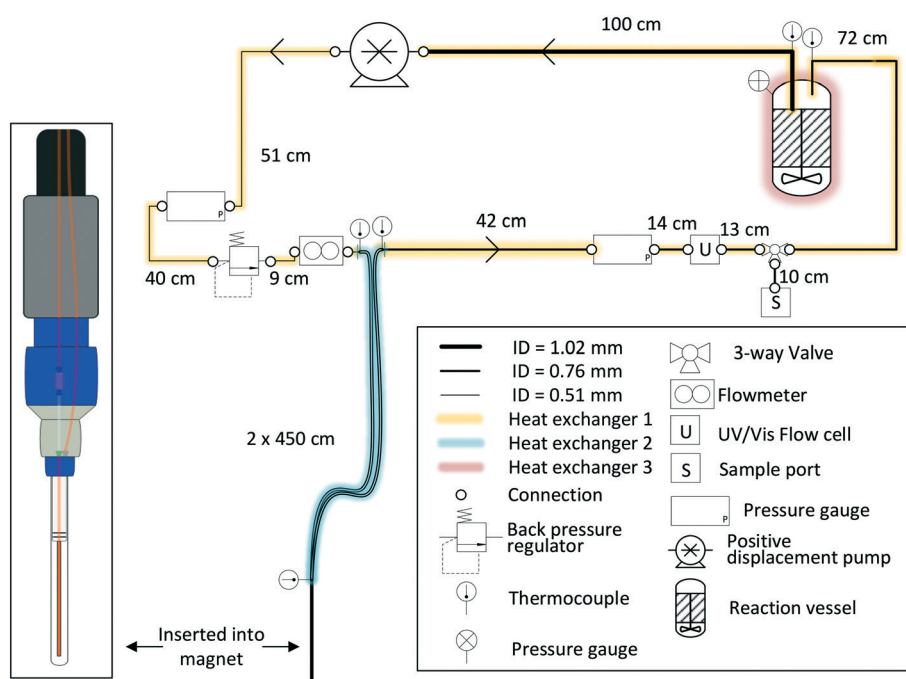


Fig. 12 P&ID schematic of a closed-loop recirculating FlowNMR setup with exemplary length scales and tubing ID (indicated by line thickness), and indication of sequential temperature control by use of three independent heat exchangers (colour coding).



in Fig. 9 (C), the heat exchange fluid temperature becomes a valid approximation for the sample temperature in its core. Thus, monitoring the heat exchange fluid temperature throughout the flow path using a series of thermal sensors is a useful feature for ensuring appropriate process conditions. Metallic K-type thermocouples using a Ni–Cr/Ni–Al alloy combination that translate a thermal junction at their tip to an electrical voltage are a cost-effective and easy to use solution that provide sufficient precision for most FlowNMR applications ( $\pm 1$  °C after calibration). With their 1.5 mm OD and flexible nature they may be conveniently inserted into the thermofluid stream, sample flow and the reactor itself using 1/16" HPLC fittings. More precise resistive thermal detectors such as a Pt100 (with a precision of up to  $\pm 0.1$  °C) may be used instead if needed, although they will require more careful fitting than thermocouples.

We have found that active heat regulation with three thermofluidic circuits along all sections of accessible tubing as shown in Fig. 12 combined with passive insulation using 1.5 cm thick foam on any exposed sections (such as connections to instruments or devices) works well to provide uniform sample temperatures with less than 10% variance throughout the fluid path. If available, thermal imaging with an infrared camera (nowadays available as add-ons for smartphones) is useful for locating any hot/cold spots, and help understanding any temperature changes the sample might experience on its journey through the setup for applications where accurate heat management may be important for reasons of reactivity, solubility or safety (see ESI† section 9.2 for examples). Absolute temperature differences between the values set on the heat exchangers and those within the circuit in the order of 5–20 °C may still prevail depending on how well insulated the heat transfer tubing is, but can easily be compensated for after verification of the sample temperature in the tip using the methanol or ethylene glycol NMR thermometer.<sup>108</sup> Depending on whether high or low critical temperature limits apply to a given process (for reasons of exothermicity or solubility for example), heat regulation may be based on either the hottest or the coldest point of measurement throughout the flow path. From our experience, an absolute temperature accuracy of  $\pm 2$  °C is achievable with the precautions described in this section.

**3.4. Some notes on sample homogeneity.** With the sensitivity of solution phase NMR spectroscopy to sample inhomogeneities and the small internal dimensions of FlowNMR setups there comes a great emphasis on excluding any solids from the system. Blockages in the flow path during a run do not only ruin the experiment and endanger the expensive equipment but can be difficult to rectify and rather frustrating to deal with. Good maintenance and care of the setup (including thorough cleaning routines, pressure drop monitoring, and efficient heat regulation) help significantly in reducing the possibility of cross-contamination and build-up of solids between experiments. In our experience, the time and effort dedicated to proven cleaning and testing routines prior

to every experiment pay off several-fold in the quantity and quality of data obtained in the long run, in addition to prolonging equipment lifetime. For any new applications, ascertaining the homogeneity of the sample under the exact conditions chosen for FlowNMR investigation is recommended good practice. As different users may have different perceptions of sample homogeneity, a useful objective test is to pass the reaction solution through disposable syringe filters with 0.2  $\mu\text{m}$  membranes (available with a range of materials and capacities) both at the beginning and at the end of the reaction to see if any solids are present. While it is possible to investigate the liquid phase of slurries with FlowNMR spectroscopy using large surface area inlet filters on the sample tubing in the reactor, applications that form precipitates over the course of the investigation are very difficult to deal with, as solids may appear uncontrollably in different parts of the setup. For instance, the mechanical action of positive displacement pumps on the sample can cause nucleation and initiate solid precipitation in a place where it is not particularly desirable. Inline filters in various forms (discs, cartridges and even miniature frit-in-a-ferrule solutions) are available as HPLC consumables, however, we do not recommend their inclusion in a FlowNMR setup for the simple reason that they will add flow resistance and block more easily than a well-designed and maintained setup with no undue restrictions. Our recommended best practice includes the above precautions combined with a thorough filtration of all components through appropriate 0.2  $\mu\text{m}$  syringe filters prior to use. The amounts of solids from traces of insoluble impurities (salts, desiccants, chromatography phases) and adventitious dust that can thus be removed from reagent solutions that look perfectly clear to the human eye can be astounding.

#### 4. Selection of pumps

A key component of an effective and reliable FlowNMR setup is a suitable liquid pump for circulating the sample through the system. Although perhaps deceptively simplistic to molecular scientists and spectroscopists, the correct selection, installation, use and maintenance of pumps is an area of reaction engineering of appreciable technical complexity. Due to the importance of pumps for industrial manufacturing<sup>109</sup> a wealth of literature is available on applied aspects of large-scale pump installations,<sup>110–112</sup> however, much less guidance is available for small scale specialist applications. The preceding sections have already touched on some considerations relevant to pump selection (flow rates, pressure drop, temperature and pressure), and a more detailed analysis and discussion will be provided in this section.

**4.1. Pump types and working principles.** Key criteria of pump selection for FlowNMR applications include i) high accuracy and precision of flow rate, ii) the ability to work under moderate pressures of up to 20–30 bar, iii) temperature ranges of up to 100 °C, and iv) the ability to reliably pump a range of liquids of various densities and



viscosities. As steady flow rates in the order of 0.5 to 5 mL min<sup>-1</sup> are typically used for FlowNMR, precise metering, rapid start/stop capabilities, or generation of particularly low or high flow rates are less important. Pump efficiencies as often assessed in thermodynamic testing cycles for large-scale applications<sup>113</sup> are also of less importance for FlowNMR, as long as pump performance and stability are not compromised by undue stress and wear.

Of the three major pump types centrifugal (CF), axial flow (AF) and positive displacement (PD) the latter is most suitable for controlled liquid delivery on small scale in accordance with the considerations (i-iv) above. Unfortunately, PD pumps are also the most diverse and complex class of pumps, and their performance heavily depends on their individual design and proper installation and use.<sup>114</sup> In general, all PD pumps operate by repeatedly enclosing a small volume of liquid and moving it mechanically from the suction side (inlet) to the discharge side (outlet), intercepting the liquid stream temporarily with each cycle. This repeating motion can be provided by vanes, gears, diaphragms or pistons, and the fluid delivery is often assisted by one-way valves that ensure directionality of the flow against pressure differentials. The speed of the internal movement (stroke velocity) and the amount of liquid moved per cycle (displacement volume) determine the suction

pressure on the sample at the inlet as well as the pulsation of liquid flow delivered through the outlet. With non-compressible liquids the flow is theoretically independent of pressure, as long as the pump drive is powerful enough to sustain the cycle. As the displacement volume is constant, the volumetric flow rate is independent of sample density and viscosity. Reciprocating PD pumps using diaphragms or pistons moving backwards and forwards tend to have larger displacement volumes and higher stroke velocities than rotary PD pumps using vanes or gears. Hence, the latter often have lower pulsation and suction pressure than the former but are more susceptible to wear and have a higher tendency of slippage.<sup>115</sup>

The PD pumps most commonly used for small scale laboratory applications include a) HPLC single or dual piston pumps, b) rotary multi-piston pumps, c) annular gear pumps, d) diaphragm pumps, and e) peristaltic tube pumps. Their principal components and functioning are illustrated schematically in Fig. 14. Note that linear PD pumps such as syringe pumps (f), which are ideal for metering applications and rapid injection devices as used in stopped-flow analyses, do not lend themselves for continuous sample recirculation in FlowNMR setups.<sup>116</sup> However, as they deliver the smoothest flow of all PD pumps, a syringe pump is included in the following as a comparison.

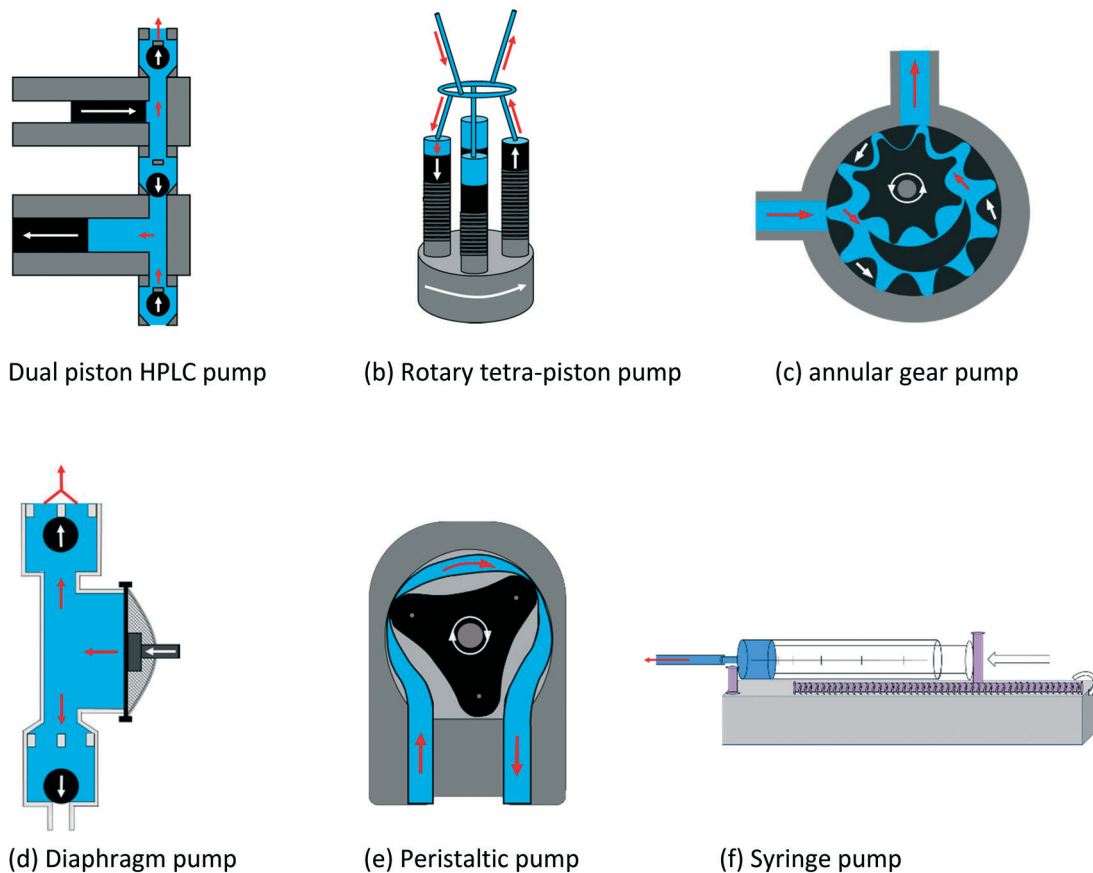


Fig. 14 Schematic working principles of common positive displacement pumps used for small scale laboratory applications. Mechanical movements indicated by white arrows, fluid flow indicated by red arrows.



**Table 3** Comparison of commercially available positive displacement pumps for use in FlowNMR applications

Pump type	Make & model	Flow range/mL min <sup>-1</sup>	Temperature range/°C	Pressure limit/bar	Viscosity limit	Wetted materials
HPLC (a)	Knauer Azura P 4.1S	0.001–10	–40–200	400	100 mPa	PTFE, titanium, sapphire, ceramic, FKM
Rotary multi-piston (b)	Vici M6 HP	0.065–5	0–50	33	100 mPa	PTFE, PAEK, Valcon P, sapphire, Viton
Annular gear (c)	HNP-M mzt-6355	0.024–144	–5–60	80	0.3–1000 mPa	Stainless steel, FFKM, FFPM, EPDM, SiC, Al <sub>2</sub> O <sub>3</sub> , ZrO <sub>2</sub> ceramics
Annular mini gear (c)	HNP-M mzt-2921	0.03–18	–20–60	3	0.3–100 mPa	Stainless steel, WC, Ni-based ceramics, epoxy resin
Diaphragm (d)	Tacmina QI-10-6T	0.1–10	0–40	20	100 mPa	Stainless steel, PTFE, FFKM
Peristaltic (e)	VapourTec SF-10 V-3	0.02–10	0–60	10	Solutions, suspensions, light slurries and gases	Red tube: FKM, ePTFE Blue tube: perfluoroelastomer, ePTFE
Syringe (f)	Masterflex 74900-05	0.0001–4 <sup>a</sup>	5–40	1 <sup>a</sup>	n.a.	PVC <sup>a</sup>

<sup>a</sup> Depending on syringe used.

As the individual advantages and limitations of these different PD pumps for use in FlowNMR applications are not immediately obvious, we compare some key characteristics using commercially available examples for each type in the following (Table 3).

Note that many of the models listed in Table 3 are available with different pump head materials that may be chosen to suit the chemical compatibility demands of the application. In some cases, these can easily be interchanged (like for the peristaltic pump (e)) whereas in most situations a separate pump head needs to be purchased. The larger annular gear pump (mzt-6355) is equipped with a powerful magnetically coupled drive to limit exposure of the internal mechanics to the sample, whereas the simpler model (mzt-2921) has a smaller direct drive. HPLC pumps naturally have the largest pressure range, followed by annular gear pumps and rotary piston pumps. Peristaltic pumps often have very low-pressure ratings due to their flexible tubing and plastic rollers but are least sensitive to solids and mixtures and offer minimal contact to wetted materials. Electrical heating mantles are available for both gear pumps (c), and a fluid heat exchanger module (allowing both heating and cooling) is available for pump (a). All other pumps operate at room temperature and may only be passively insulated with foam to minimise sample heat loss. In the following we will test and compare some key performance characteristics of (a)–(f) relevant to FlowNMR applications.

**4.2. Pump priming and use – the importance of suction pressure and cavitation.** All PD pumps only work as intended when fully primed, *i.e.* when the displacement volume inside the pump is completely filled with incompressible liquid. While most rotary PD pumps (such as (c) and (e)) are self-priming due to their cyclic movements, reciprocating PD pumps (such as (a) and (d)) typically are not and can suffer from entrapped gas bubbles that limit pump efficiency and decrease the actual flow rate delivered. The ease of pump priming also depends on the internal layout of the flow path

through the pump, and generally the more complex the design the more difficult the pump will be to prime. An important practical parameter that determines how effectively a pump can be primed, and one that also limits its maximum flow rate once primed (see below), is the suction pressure at the pump inlet.<sup>117</sup> The lower the liquid level in the sample reservoir relative to the pump inlet, the larger the suction pressure and hence difficulty of pump priming. In order to minimise suction pressure we recommend to always keep the pump at a lower height than the fill level in the reaction vessel if possible, and use gentle positive feeding (either *via* a manually actuated syringe or moderate gas pressure on the sample in the reaction vessel) when priming the pump at a low flow rate. If the pump allows its setting to be changed, a slow start-up rate (or low P term in the PID controller) further helps reducing cavitation when flow rates are ramped up from zero. Once fully primed all PD pumps will easily displace one liquid with another (as long as they are fully miscible), so if priming cannot be done directly with sample solution we recommend priming the pump with a compatible solvent and then changing over to the analyte.

In addition to any height differences between the sample reservoir and the pump, the tubing between the two provides an intrinsic flow limitation that constitutes an important consideration during pump operation (*i.e.* even once fully primed). The pressure drop calculations from eqn (2) do not only apply to the discharge side as a flow resistance (section 2), but also to the suction side of the pump in the form of a suction resistance. The internal diameter and length of the

|| Somewhat confusingly, in pump hydrodynamics and irrigation engineering the difference between the pump inlet level and the maximum height of water the pump can sustain in a vertical pipe at a given flow rate is historically referred to as the pump “head”. This practical measure is equivalent to the outlet pressure of the pump at that flow rate plus any positive inlet pressure from the fill level in the reservoir and is not to be confused with any mechanical parts of the pump.





suction path determine how much pull the pump exerts on the resting liquid at the flow rate applied. With the small internal dimensions, low sample viscosities and moderate flow rates typically used in FlowNMR setups it is not uncommon for this suction resistance to lead to outgassing of the liquid and even vaporisation of the solvent itself.\*\* This process collectively known as cavitation (Fig. 14, left) means that some amount of vapour may enter the pump or form within it, leading to decreased flow rates and even pump wear.†† The net positive inlet pressure required (NPIP-R) is an important metric in pump engineering that defines the minimum fluid inlet pressure required to avoid cavitation.<sup>117</sup> The NPIP-R of a PD pump setup is flow rate, temperature and solvent dependent, and suction-side pipework design must ensure a suitable safety margin referred to as net positive inlet pressure available (NPIP-A). NPIP-R thresholds can be calculated using eqn (2) if the limiting internal diameters and path lengths of the suction side are known, and comparing these to the vapour pressure lines of the lowest boiling component in the sample allows defining the NPIP-A under the conditions applied. Fig. 15 (right) contrasts two exemplary suction pressure curves for water and ethanol against their vapour pressure lines at various temperatures to illustrate NPIP-A and cavitation regimes, respectively. Note that the results shown assume stroke velocities no higher than the average flow rate selected and that there are no restrictions inside the pump smaller than the ID of the inlet tubing. Filters and check valves (as often used in HPLC and diaphragm pumps) may cause additional restrictions due to their small IDs and thus lead to higher NPIP-R thresholds. Similarly, if a PD pump has particularly high stroke velocities, the NPIP-R will inherently be higher.

The values in Fig. 15 show that with the tubing IDs and flow rates typically used in FlowNMR setups one can easily get close to NPIP-R thresholds with moderately volatile solvents (with any pump). In order to limit the risk of cavitation and increase the NPIP-A margin for safe and effective pump operation during FlowNMR experiments requiring accurate and precise flow rates, several steps can be taken: i) minimise any undue restrictions in the suction side flow path, ii) use a maximum ID tubing of minimum length for the suction side, iii) operate pump below the fill level of the sample reservoir, iv) if using temperatures close to the boiling point apply an overpressure of inert gas on the sample reservoir. Our decision to use a 100 cm long inlet tubing of 1 mm ID on the suction side to our pumps (see Fig. 4 and 12) was motivated by such NPIP considerations and has greatly facilitated pump priming and use. We hope that this brief discussion of fluid pressure phenomena in PD pumps will be useful to other FlowNMR users and help avoid

frustration over pumps not delivering any flow under conditions where it is physically impossible for them to work.

**4.3. Sample dispersion and tailing from residence time distribution measurements.** For FlowNMR analyses the internal volume of the pump used is ideally minimal and swept uniformly so that there is no sample hold-up or back-mixing (= ideal plug flow conditions). Not all PD pumps are necessarily designed for these conditions, however, and some insight into the fluid dynamics can be valuable information for deciding whether a certain pump is suitable for a given application. Total internal volumes are typically available from the supplier but do not give any information on the distribution of swept volume + dead volume under process conditions. Residence time distribution (RTD) measurements<sup>120,121</sup> of the entire setup (including flow tube and pump) are thus useful experiments to quantify the actual swept volume of the system and determine any degree of broadening and sample tailing due to non-ideal plug flow. To this end we have investigated pumps (a–e) at flow rates of 1–6 mL min<sup>-1</sup> using fluorescein as marker detected by a UV-vis flow cell situated at the exit of the flow setup (see ESI† section 2.0). Fig. 16 shows data for the peristaltic pump (e) as an example, and the results of all other pumps can be found in the ESI† section 10.1.

RTD profiles at higher flow rates are sharper and are shifted towards lower residence times than for lower flow rates, as expected for laminar plug flow (see Table 1). The mean hydrodynamic residence times  $\tau$  derived from these measurements allow calculating the system total volumes *via* the volumetric flow rate applied. Using the syringe pump (f) attached to the entry of the system (without adding any internal pump volume) as a baseline result, the swept volumes of pumps (a–e) can be derived from their averaged  $\tau$  values (Table 4).

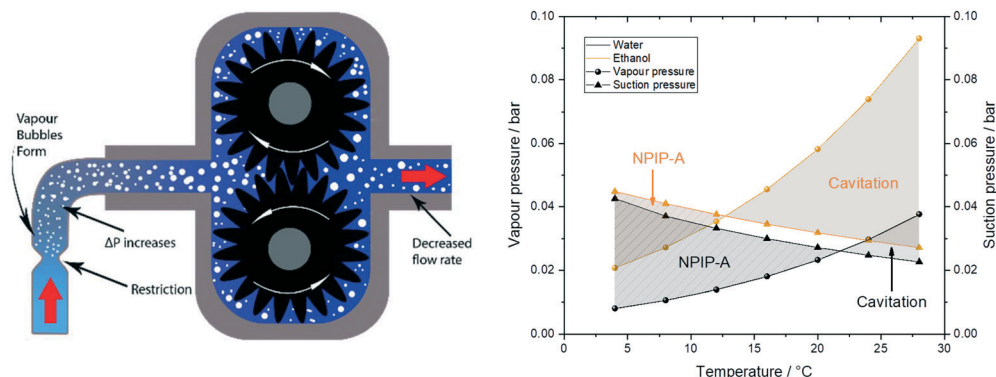
As can be seen from the values in Table 4, our FlowNMR system including the InsightMR™ tube and all sensors and safety features as shown in Fig. 12 but without any pump has an internal volume of 4.4 mL. This is a typical value for FlowNMR setups, but systems with internal volumes of less than 2 mL have been realised for applications with precious samples using minimally short sections of small ID tubing and 3 mm glass tips.<sup>122</sup> The additional internal volumes of the pumps (a–e) tested varied significantly, spanning the range from 150  $\mu$ L to 2.4 mL, which is also reflected in the comparison shown in Fig. 17.

RTD peak shapes may be analysed for their degree of symmetrical broadening that are caused by shearing and diffusion by fitting a Gaussian to the curve.<sup>123</sup> The fit peak width (= sample dwell time) is a measure for the degree of plug flow ideality, expressed by either the vessel number  $n$  of a theoretical cascade of infinitesimally small continuous stirred tank reactors (CSTRs) or the dimensionless Bodenstein number: the higher  $n$  or  $Bo$ , the more ideal the plug flow (for details see ESI† section 10.1 and 10.2). Fig. 18 (left) shows a comparison of vessel numbers for pumps (a–e) at various flow rates. It can be seen that all

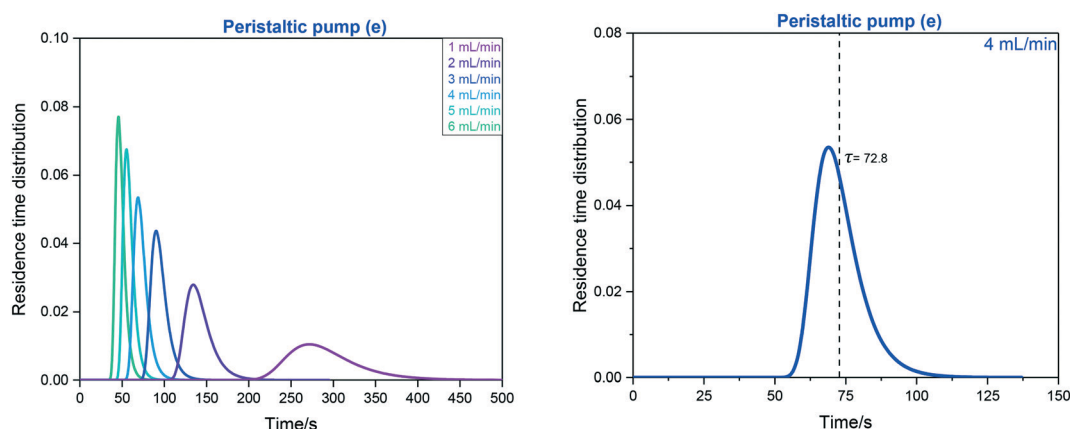
\*\* Solvent degassing is thus a common procedure to limit this phenomenon in HPLC applications, but vaporisation cavitation cannot be prevented this way.

†† Gas entrainment into the suction side due to leaking seals or fittings is referred to as aspiration cavitation.





**Fig. 15** Left: Schematic illustration of a local suction resistance causing cavitation in a gear pump. Note that more extreme suction pressure differentials may cause complete sample evaporation that can lead to significant pump damage by imploding vapour bubbles and solids precipitating inside the pump. Right: Solvent suction resistance calculated for water and ethanol at ambient pressure and  $4 \text{ mL min}^{-1}$  through  $1 \text{ m}$  of  $1 \text{ mm}$  ID PEEK tubing using eqn (2) versus their vapour pressures at various temperatures.<sup>118,119</sup>



**Fig. 16** Left: RTD profiles of the FlowNMR apparatus shown in Fig. 12 with peristaltic pump (e) as derived from FlowUV-vis spectroscopy at  $334 \text{ nm}$  using  $12 \text{ mM}$  fluorescein in acetone as the marker in a step change displacement experiment. Right: Determination of mean residence time at  $4 \text{ mL min}^{-1}$ .

**Table 4** Comparison of pump internal volumes derived from RTD measurements (for details see ESI† section 10.1)

Pump	HPLC (a)	Rotary multi-piston (b)	Annular gear (c)	Annular gear (c)	Diaphragm (d)	Peristaltic (e)	Syringe (f)
Total internal volume of flow system	4.78 mL $\pm 0.06$	4.56 mL $\pm 0.03$	6.80 mL $\pm 0.10$	4.76 mL $\pm 0.06$	6.10 mL $\pm 0.09$	4.85 mL $\pm 0.03$	4.41 mL $\pm 0.02$
Swept internal volume of pump	0.37 mL	0.15 mL	2.40 mL	0.36 mL	1.70 mL	0.44 mL	0.00 mL

pumps struggled a bit at low flow rates but delivered relatively constant flow qualities above  $2 \text{ mL min}^{-1}$  (using acetone at room temperature), and that the HPLC pump (a), the rotary multi-piston pump (b) and the small gear pump (c) produced the most ideal plug flows (*i.e.* sharpest RTDs). Their vessel and Bodenstein numbers being close to those obtained with the syringe pump (f) show that (a–c) do not add significant amounts of RTD dispersion to the system, and that the values seen are the limitations of the tubing and flow tip used. Further improvements, if desired, would require streamlining the sample flow into and out of the tip of the flow tube<sup>42</sup> which has previously been shown to cause dispersion as the sample expands from the narrow injection

capillary into the  $5 \text{ mm}$  glass tube and then squeezes back through a small hole at the top leading into the outlet tubing. The peristaltic pump (e), the diaphragm pump (d) and the larger gear pump (c) added increasing amounts of back-mixing to the flow as shown by their significantly lower vessel and Bodenstein numbers. As a simple rule of thumb, the degree of sample back-mixing (or flow dispersion) induced by the various pumps broadly correlates with their swept internal volumes: the larger, the worse.

The single RTD in Fig. 16 (right) shows some degree of unsymmetrical broadening towards longer residence times indicative of sample tailing (= longer dwell times), and the overlay of RTD curves from pumps (a–e) at  $4 \text{ mL min}^{-1}$  shown



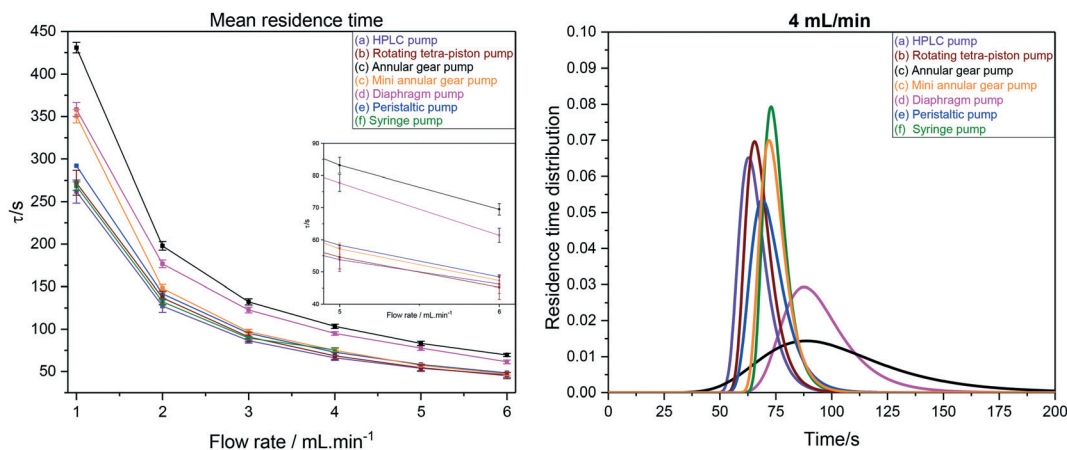


Fig. 17 Left: Mean hydrodynamic residence times as derived from RTD measurements of the FlowNMR apparatus shown in Fig. 12 with pumps (a–f). Right: Comparison of RTD profiles of pumps (a–f) at 4 mL min<sup>-1</sup>.

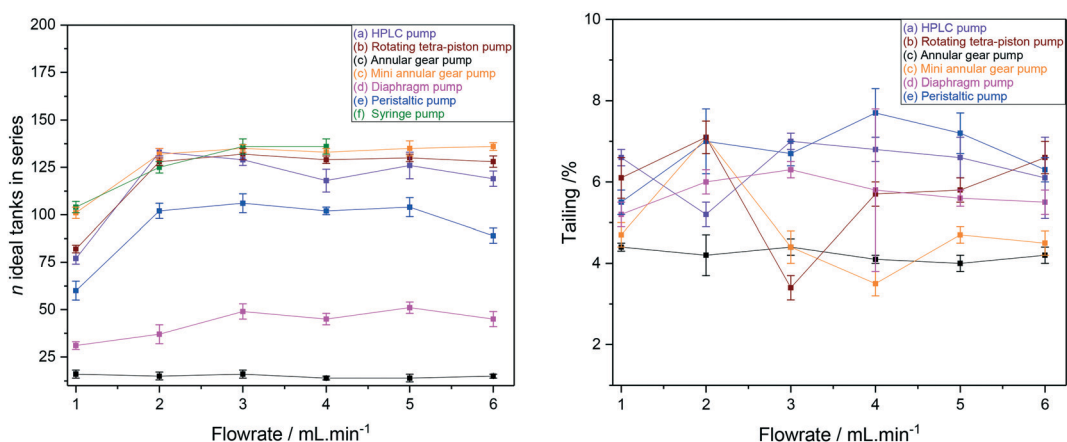


Fig. 18 CSTR cascade vessel numbers for the FlowNMR setup shown in Fig. 12 with pumps (a–f) as derived from Gaussian fits of their RTD profiles (left) and sample tailing from surface area differences (right).

in Fig. 17 (right) suggests that the different pumps may induce various amounts of sample hold-up in addition to flow dispersion. Fig. 18 (right) however shows that the degrees of tailing relative to dispersion caused by the pump internal volumes are actually quite small and similar for all pumps investigated. Sample hold-up and tailing are thus not a major concern for selecting a suitable PD pump for FlowNMR systems under the conditions applied in this study.<sup>‡‡</sup>

For applications where compositional changes induced by deliberate changes to the sample in the reaction vessel (e.g. the addition of solid, liquid or gaseous reagents, application of an electrical current or irradiation with light) are to be followed by time-resolved FlowNMR spectroscopy, the transit time from the vessel to the tip of the flow tube is an important quantity to know. The same RTD measurements as carried out for the full system round-trip by UV-vis spectroscopy above can be performed by fast pulse NMR

<sup>‡‡</sup> Note that these results have been obtained with an optimised flow setup and streamlined pump configurations that had all filters bypassed. Including these may yield significant dispersion and sample tailing that are not caused by the pump.

spectroscopy to gain sample RTD profiles from the reactor to the point of detection. Using a continuous series of single 30 degree pulses with minimal acquisition times allows measuring <sup>1</sup>H NMR spectra of simple solvent mixtures every 400 ms, affording sufficient temporal resolution for RTD measurements (see ESI<sup>†</sup> section 10.1 for details). Fig. 19 shows some results obtained with the peristaltic pump (e) at various flow rates.

The mean hydrodynamic residence times show the internal volume of this section of the setup (in this case including pump (e)) to be in the order of 2.2 mL, giving a transit time (or sampling delay) of 32 seconds under typical flow conditions of 4 mL min<sup>-1</sup>. The observation that a similar amount of tailing was seen in this data as for the round-trip RTD results shown above (~5%) confirms that most sample hold-up occurs within the flow tube tip itself.

**4.4. Flow pulsation and pump performance under gas pressure.** As all flow effects on NMR acquisition are directly flow rate dependent, a critical characteristic of a pump for use in FlowNMR is maximum stability of the selected flow rate. While pump calibrations (→ accuracy) can periodically



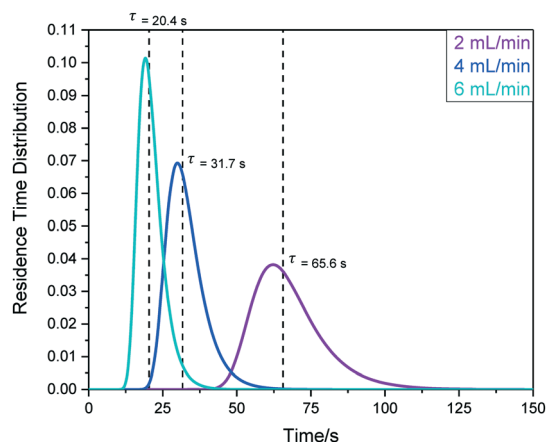


Fig. 19 RTD profiles for sample travel from the reaction vessel to the tip of the InsightMR™ flow tube using peristaltic pump (e) as derived from fast pulse  $^1\text{H}$  NMR spectroscopic measurements using hexane to acetone in a step change displacement experiment.

be performed with the help of flow meters or by other external means, any variations in the flow rate delivered ( $\rightarrow$  precision) during a FlowNMR experiment are potentially problematic as they may distort compound quantification by peak integration. This does not only include gradual drifts to higher or lower average flow rates (for example, due to incomplete priming at the beginning or rising flow resistance from an increase in sample viscosity) but equally applies to any periodic or random oscillations of the average flow rate delivered. Due to their working principle flow pulsation is an inherent feature of all PD pumps (sometimes referred to as the heartbeat), but its extent varies significantly depending on the pump type. §§ The higher the stroke velocity and displacement volume of the pump, the more pronounced the pressure pulse on the discharge side when delivering, causing a temporary spike in the flow rate that is followed by a drop when the pump refills from the suction side. Multi-piston pumps such as (a) and (b) limit such periodic oscillations by anti-phasic piston movements similar to multi-cylinder combustion engines, while diaphragm pumps try to minimise pulse intensities by using a large and flexible, slowly moving element. Gear pumps promise to produce the least amount of pulsation due to their small displacement volumes and steady, cyclic motion. While these qualitative differences are well known and many pumps advertised as “low pulsation solution” by commercial suppliers, the absolute amount of any flow oscillations and their frequencies are rarely provided by the manufacturers, making the selection of a suitable pump for FlowNMR applications difficult. We have thus measured flow rate stability and pulsation of the exemplary pumps (a–e) investigated here with a high-resolution Coriolis flow meter. Fig. 20 shows the

§§ Flow pulsation dampeners based on flexible diaphragms or bladders are available to smoothen out pump cycles, but due to their added internal volume and potential sample hold-up are not recommended for FlowNMR applications.

degree of variation around the average flow rate delivered with an indication of their frequencies.

As can be seen from the data in Fig. 20, the peristaltic pump (e) produced the largest flow rate variations of  $\pm 14\%$  with a steady frequency of 0.33 Hz at  $4 \text{ mL min}^{-1}$ . This result was somewhat surprising given its circular motion and must be the result of the three heavy rollers ticking over during operation. The diaphragm pump (d) was less pulsed with flow rate variations in the range of  $\pm 9\%$  at a higher frequency of 2.5 Hz, indicating a smoother but still noticeable heartbeat from the large Teflon membrane. The dual piston pump (a) afforded lower pulsations of  $\pm 0.6\%$ , and the rotary tetra-piston pump (b) and the two annular gear pumps (c) produced the lowest flow rate variations of 0.3% at irregular (but insignificant) frequencies. These results were expected for (c) as discussed above, but (b) and (a) were also surprisingly good at limiting pulsation from their small, reciprocating pistons. Lower flow rates yield lower pulsation frequencies in all cases, and for some pumps even larger flow rate variations (see ESI† section 10.3 for details).

In order to demonstrate how such oscillations in sample flow may affect FlowNMR data, quantitative fast pulse  $^1\text{H}$  NMR measurements were carried out on neat solvent circulated with pumps (c), (d) and (e) at the same nominal flow rate. Absolute integral values as measured over time (uncorrected) are shown in Fig. 21.

With an acquisition time of 0.25 seconds, the flow oscillations of the peristaltic pump (e) and the diaphragm pump (d) were clearly visible in the  $^1\text{H}$  FlowNMR integrals.<sup>40</sup> Thus, if precise NMR data with a high acquisition rate is required, a high-precision pump with minimum pulsation must be used.

For most FlowNMR applications the pressure profile throughout the setup as a result of steady pump operation does not change significantly over time. However, in cases where a sample is to be analysed under variable pressure (*e.g.* from a reaction gas applied to the reactor headspace), the pump response to an increase or decrease of inlet pressure becomes an important factor.<sup>46,102,103</sup> Fig. 22 shows the variations in flow rates delivered by pumps (a–d) during pressure stepping between ambient and 15 bar as measured by a Coriolis flow meter.

Interestingly, both the double piston HPLC pump (a) and the diaphragm pump (d) showed a sharp increase in sample flow rates delivered when 5 bar of headspace pressure was applied, but no further changes when the pressure was raised further up to 15 bar. The initial increase was significant (54–66%) and probably reflected incomplete pump priming at the beginning of the experiment despite all best efforts to prevent this (see section 4.2). The sudden increase in inlet pressure expelled remaining gas pockets in the pump, leading to much higher-than-calibrated flow rates. These data show the difficulty of priming some reciprocating PD pumps with check valves and demonstrate what consequences this may have in FlowNMR applications under variable pressure:



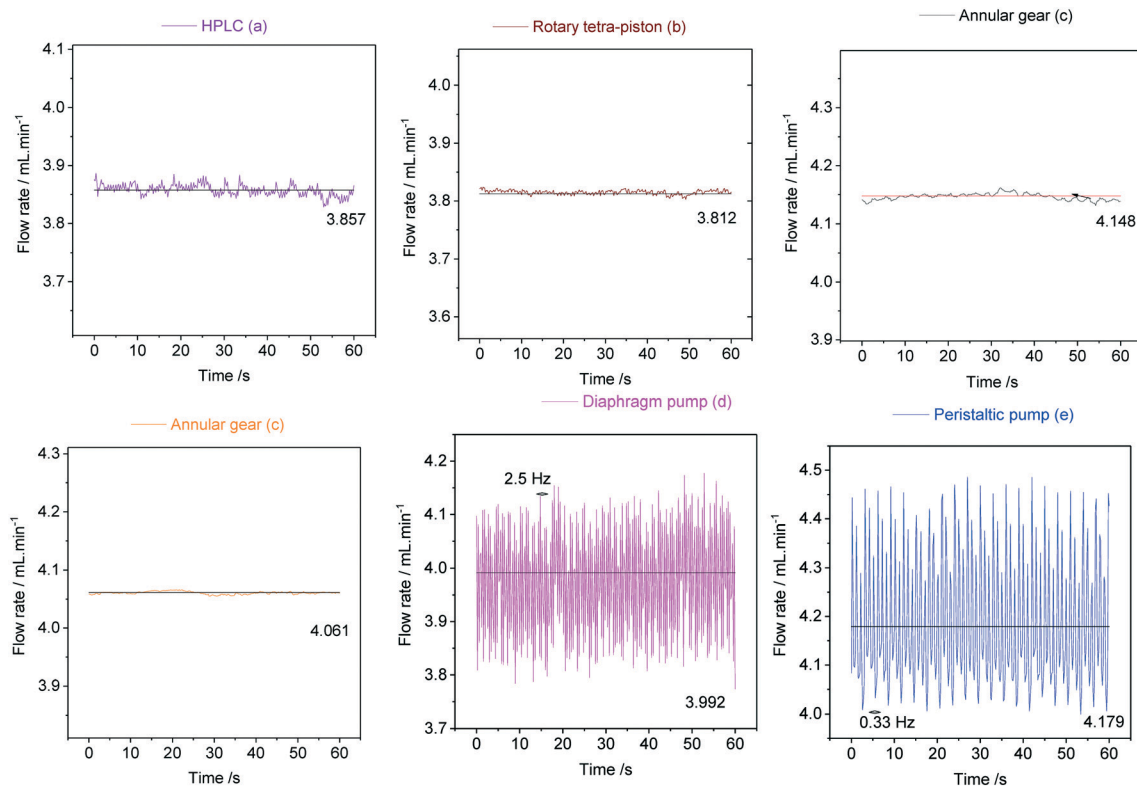


Fig. 20 Flow rate oscillations due to pump pulsation as measured with a Bronkhorst mini Cori-Flow M13 (situated before the entry to the flow tube) for pumps (a–e) at a nominal flow rate of  $4 \text{ mL min}^{-1}$  acetone circulated through  $1/16''$  PEEK tubing at room temperature. Black lines indicate the average flow rates delivered after external calibration.

a sudden  $>50\%$  increase in flow rate will lead to significant quantification errors due to changes in flow correction factors.<sup>42</sup> Once fully primed both (a) and (d) did perform well under pressure though, so if this effect can be reliably excluded (either through pressurised priming procedures or an actively flow-regulated pump control loop) these pumps may be suitable for FlowNMR applications under variable pressure. The rotary piston pump (b) and the high pressure

gear pump (c) did not show any sign of this behaviour (neither in the limited data shown here nor during any other applications for which we have used them), and delivered stable flow rates from ambient to 15 bar (Fig. 22). Thus, such pumps are both easier to use and more reliable for pressure applications. However, all pumps showed a large drop of liquid flow rate delivered upon depressurisation from 15 bar to ambient as the autoclave was slowly vented over the course of  $\sim 60$  seconds. Such pressure decreases lead to solvent outgassing throughout the system (sometimes bubbles be even observed in the tip of the flow tube) and cause cavitation inside the pump head that lead to significantly reduced and rather erratic flow rates until the pump has managed to expel all gas and reprimed itself. Care should thus be taken when decreasing gas pressures during a FlowNMR experiment with any PD pump, especially when using highly soluble gases such as  $\text{CO}_2$ .

**4.5. Pump comparison.** From the data shown and discussed in sections 4.1 to 4.5 it becomes clear that pump selection for FlowNMR applications is not trivial, and a number of factors (some of which may not be known before purchase and need to be tested with the given setup) will need to be considered. The general requirements for high accuracy and precision of flow rate, and the ability to reliably work with a wide range of fluids will apply to all FlowNMR applications, but the specific demands in terms of chemical

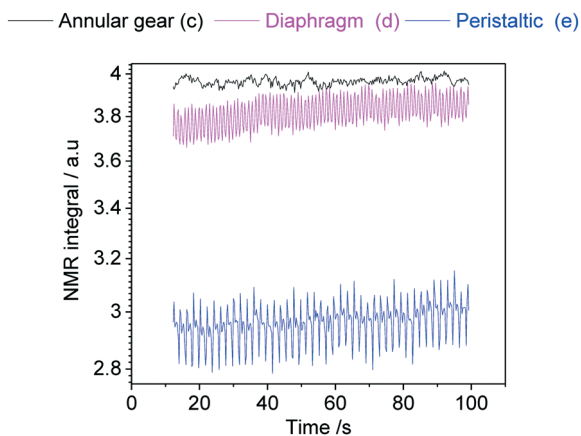


Fig. 21 Absolute  $^1\text{H}$  NMR integral values of acetone flowing through the setup shown in Fig. 12 at a nominal flow rate of  $2 \text{ mL min}^{-1}$  at room temperature using different PD pumps.



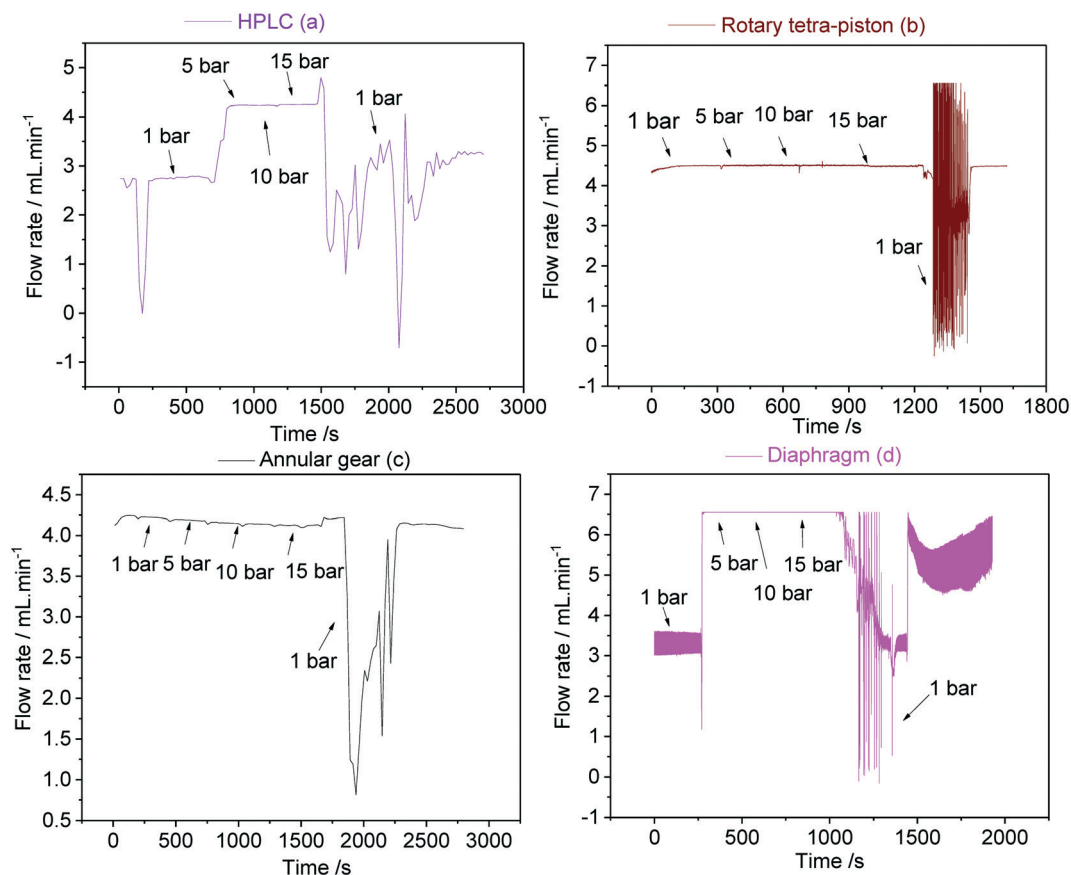


Fig. 22 Sample flow rates as measured with a Bronkhorst mini Cori-Flow M13 for pumps (a–d) at a nominal flow rate of 4 mL min<sup>-1</sup> toluene circulated through 1/16" PEEK tubing at 50 °C. Variation of headspace pressure by application of an Ar/H<sub>2</sub> mix (9:1) to the reactor indicated by black arrows.

Table 5 Qualitative comparison of PD pumps (a–e) for use in FlowNMR applications

	Double-piston HPLC pump (a)	Rotary tetra-piston pump (b)	Large annular gear pump (c)	Small annular gear pump (c)	Diaphragm pump (d)	Peristaltic pump (e)
Ease of priming	☹️	😊	😊	😊	☹️	😊
Ability of working dry	☹️	😊	☹️	☹️	😊	😊
Swept volume	😊	😊	☹️	😊	☹️	☹️
Flow pulsation	☹️	😊	😊	😊	☹️	☹️
Performance under variable pressure	☹️	😊	😊	☹️	☹️	☹️
Ease of use & reliability	☹️	😊	😊	😊	☹️	😊
Price	\$\$	\$\$	\$\$\$\$	\$\$	\$\$\$	\$

compatibility, internal volume, temperature range and performance under pressure will depend on the nature of the investigation. Practical considerations including the ease of priming and maintenance, and robustness and longevity may be additional factors to consider if the setup is to be used frequently. Table 5 summarises our collective experience with the six PD pumps evaluated here as a qualitative guide to pump selection for FlowNMR setups.

As a final remark on pump selection, we caution that depending on their design and wetted materials each pump requires specific operating and cleaning procedures. In addition to the general precautions against the build-up of solids suggested in section 3.4, we recommend adhering to the manufacturer's recommendations for regular pump maintenance and care (including periodic replacement of valves, seals, *etc.*).



## 5. Process automation and control

The focus of FlowNMR experiments naturally lies on the analytical data obtained from the spectroscopic measurement, and any accompanying process data may perhaps be regarded as less important. Although it is of course possible to assemble and use an effective FlowNMR setup with standalone components and passively operating devices only, the option of unifying instrument control and data logging *via* a computer system should be given due consideration.<sup>124</sup> Although the more complex data streams coming from the NMR spectrometer can be difficult to integrate into a larger control software, the small instrumentation mentioned in this article all lend themselves to remote control and live read-out. Unifying instrument control electronically offers many advantages, including:

- Retaining quantitative process information that may be relevant to the FlowNMR data (*e.g.*, temperature and pressure profiles).
- Addition of meta-data to FlowNMR profiles (*e.g.*, electronic timepoints marking the addition of reagents, stirrer or light source turned on, *etc.*).
- Higher degrees of process control *via* active self-regulation (*e.g.*, use of a flow meter to control the pump, regulation of heat exchangers based on specific thermocouples, *etc.*).
- Automated alarm and safety mechanisms based on predefined process limits (T, p, even NMR results *via* live export of selected attributes).
- Remote monitoring and control of the system for unsupervised long-term operation.

A large (and increasing) number of interfaces and modules, as well as scripts and software packages are available either from the device manufacturers or from third party suppliers.<sup>125</sup> Many small devices used for FlowNMR setups come with their own control software,

although this is not the case universally. These software packages are typically simple to use, with the downside that the more pieces of equipment are integrated into the system, the more software packages need running, and the user needs to have a knowledge of all of these. We have thus found it useful to control, monitor and record within the same software package, and certainly from the same computer.

In our experience, National Instrument's LabVIEW presents an accessible graphical user interface (GUI) which is beneficial to general users once the program is established. For writing the so-called virtual interface (VI) there is a graphical coding mechanism that is relatively straightforward to use even for those researchers with a limited or non-existent coding background. We have also found that many vendors of small instrumentation have LabVIEW applications (sub-VIs) available for download, which can be integrated into a larger VI for unified instrument control and data logging, and manufacturers working to National Instruments suggested standards can provide certified drivers.<sup>126</sup> Fig. 23 illustrates the peripheral equipment in our system as connected to the main computer controlled *via* a single LabVIEW VI.

Alternative options include coding in the programmer's language of choice (*e.g.*, Python), possibly incorporating single-board computers (a common example of which is the Raspberry Pi), or the use of MATLAB which is a common platform that many academic institutions will have licences for and experience using. Whatever software is being used, if the main computer is connected to a network we recommend turning off auto-updates from the operating system and minimise remote access permissions in order not to corrupt data collection and instrument control during an experiment.

It has been identified that accessibility of data, in terms of both standardisation and sharing, is important as we

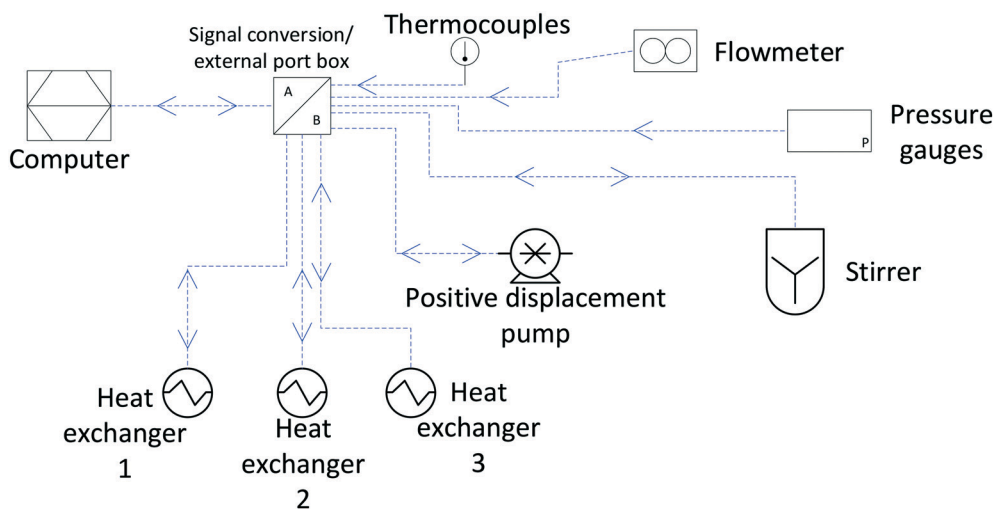


Fig. 23 Data connections of instrumentation in flow path to computer mediated by an external port box with signal conversion/smoothing. Arrows indicate data flows (read-out only or read-out & control).



progress further into a digital world.<sup>127</sup> Although many instruments will have different connections, communication frequencies and transmission standards, process and metadata collected through a unified control software such as LabVIEW allows exporting all relevant data in universal csv format at the desired temporal resolution. If tagged with an absolute time stamp from the operating system all profiles can easily be aligned for post-acquisition processing and analysis without compromising data storage and sharing.

The digitisation of chemical synthesis and particularly flow chemistry is well afoot,<sup>125</sup> allowing researchers to study reactions in a more time-effective and data-dense manner. Automated laboratory equipment, self-optimisation tools<sup>128</sup> and concepts such as cyber-physical twinning,<sup>129</sup> are increasingly used to enable a variety of chemical research. It is useful to keep in mind other areas of areas of chemical digitisation which may be intertwined with FlowNMR analysis in order to facilitate progress. Self-regulating flow chemistry set-ups could be linked to FlowNMR where the spectral data generated could be used to dictate changes required to the system. An example of this possibility would be self-optimisation processes using PID controllers<sup>130</sup> in a system where the required dosing of reagents is dependent on a certain chemical shift movement.

## Conclusion

We hope that this review of some fundamental engineering aspects of small-scale flow setups and components of relevance to FlowNMR spectroscopy will be useful to other researchers for making informed choices on methods and materials to quickly assemble effective and safe setups that reliably generate meaningful data. Our own and others' experience have shown that there often is a certain learning curve when starting to use FlowNMR spectroscopy, but once overcome very insightful experiments and unique measurements become possible with this technique. In addition to obtaining valuable insights into the speciation of and interactions within complex, dynamic solution-phase systems in their native environments, a key advantage of a well-designed FlowNMR setup is the possibility of hyphenating the NMR analysis with other complementary online techniques using miniature flow cells and sampling ports for orthogonal analysis and comprehensive reaction monitoring that allows for signal verification and instrument cross-calibration. We believe there is much potential for such integrated setups in many areas of science and engineering, and many exciting applications await to be explored with advanced online analysis in real time.

## Conflicts of interest

The authors declare no conflicts of interest.

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## References

- 1 T. D. W. Claridge, *High-Resolution NMR Techniques in Organic Chemistry*, Elsevier, Amsterdam, 3rd edn, 2016.
- 2 H. Günther, *NMR Spectroscopy: Basic Principles, Concepts and Applications in Chemistry*, Wiley-VCH, Weinheim, 3rd edn, 2013.
- 3 N. Saito, T. Komatsu, T. Suematsu, T. Miyamoto and T. Ihara, *Anal. Chem.*, 2020, **92**, 13652–13655.
- 4 D. A. Foley, E. Bez, A. Codina, K. L. Colson, M. Fey, R. Krull, D. Piroli, M. T. Zell and B. L. Marquez, *Anal. Chem.*, 2014, **86**, 12008–12013.
- 5 M. S. A. Tampieri, F. Medina and H. Gulyás, *Phys. Sci. Rev.*, 2020, **6**, 1–86.
- 6 E. M. Viviente, P. S. Pregosin and D. Schott, *Mechanisms in Homogeneous Catalysis*, ed. B. Heaton, Wiley, Weinheim, 1st edn, 2005, ch. 1, pp. 1–80.
- 7 A. Pastor and E. Martínez-Viviente, *Coord. Chem. Rev.*, 2008, **252**, 2314–2345.
- 8 J. U. Izunobi and C. L. Higginbotham, *J. Chem. Educ.*, 2011, **88**, 1098–1104.
- 9 V. Badilita, R. C. Meier, N. Spengler, U. Wallrabe, M. Utz and J. G. Korvink, *Soft Matter*, 2012, **8**, 10583–10597.
- 10 B. Ross, T. Tran, P. Bhattacharya, D. Martin Watterson and N. Sailasuta, *Curr. Top. Med. Chem.*, 2011, **11**, 93–114.
- 11 U. Holzgrabe, *Prog. Nucl. Magn. Reson. Spectrosc.*, 2010, **57**, 229–240.
- 12 A.-H. Emwas, K. Szczepski, B. G. Poulson, K. Chandra, R. T. McKay, M. Dhahri, F. Alahmari, L. Jaremko, J. I. Lachowicz and M. Jaremko, *Molecules*, 2020, **25**, 1–63.
- 13 L. A. Colnago, R. B. V. Azeredo, A. Marchi Netto, F. D. Andrade and T. Venâncio, *Magn. Reson. Chem.*, 2011, **49**, S113–S120.





- 14 E. Hatzakis, *Compr. Rev. Food Sci. Food Saf.*, 2019, **18**, 189–220.
- 15 A.-H. Emwas, R. Roy, R. T. McKay, L. Tenori, E. Saccenti, G. A. N. Gowda, D. Raftery, F. Alahmari, L. Jaremko, M. Jaremko and D. S. Wishart, *Metabolites*, 2019, **9**, 1–39.
- 16 W. A. McGee and L. J. Parkhurst, *Anal. Biochem.*, 1990, **189**, 267–273.
- 17 N. A. J. Van Nuland, V. Forge, J. Balbach and C. M. Dobson, *Acc. Chem. Res.*, 1998, **31**, 773–780.
- 18 D. A. Foley, A. L. Dunn and M. T. Zell, *Magn. Reson. Chem.*, 2016, **54**, 451–456.
- 19 D. G. Blackmond, *Angew. Chem., Int. Ed.*, 2005, **44**, 4302–4320.
- 20 J. Burés, *Angew. Chem., Int. Ed.*, 2016, **55**, 16084–16087.
- 21 M. V. Silva Elipse and R. R. Milburn, *Magn. Reson. Chem.*, 2016, **54**, 437–443.
- 22 W. G. Lee, M. T. Zell, T. Ouchi and M. J. Milton, *Magn. Reson. Chem.*, 2020, **58**, 1193–1202.
- 23 A. Friebel, E. von Harbou, K. Münnemann and H. Hasse, *Ind. Eng. Chem. Res.*, 2019, **58**, 18125–18133.
- 24 D. Kreyenschulte, E. Paciok, L. Regestein, B. Blümich and J. Büchs, *Biotechnol. Bioeng.*, 2015, **112**, 1810–1821.
- 25 F. Dalitz, M. Cudaj, M. Maiwald and G. Guthausen, *Prog. Nucl. Magn. Reson. Spectrosc.*, 2012, **60**, 52–70.
- 26 J. H. Vrijsen, I. A. Thomlinson, M. E. Levere, C. L. Lyall, M. G. Davidson, U. Hintermair and T. Junkers, *Polym. Chem.*, 2020, **11**, 3546–3550.
- 27 S. T. Knox, S. Parkinson, R. Stone and N. J. Warren, *Polym. Chem.*, 2019, **10**, 4774–4778.
- 28 M. A. Bernstein, M. Štefinović and C. J. Sleight, *Magn. Reson. Chem.*, 2007, **45**, 564–571.
- 29 A. Blanzas, T. W. T. Bristow, S. R. Coombes, T. Corry, M. Nunn and A. D. Ray, *Magn. Reson. Chem.*, 2017, **55**, 274–282.
- 30 D. A. Foley, C. W. Doecke, J. Y. Buser, J. M. Merritt, L. Murphy, M. Kissane, S. G. Collins, A. R. Maguire and A. Kaerner, *J. Org. Chem.*, 2011, **76**, 9630–9640.
- 31 C. A. Fyfe, M. Cocivera, S. W. H. Damji, T. A. Hostetter, D. Sproat and J. O'Brien, *J. Magn. Reson.*, 1976, **23**, 377–384.
- 32 M. Khajeh, M. A. Bernstein and G. A. Morris, *Magn. Reson. Chem.*, 2010, **48**, 516–522.
- 33 M. Maiwald, H. H. Fischer, Y.-K. Kim, K. Albert and H. Hasse, *J. Magn. Reson.*, 2004, **166**, 135–146.
- 34 A. Scheithauer, A. Brächer, T. Grützner, D. Zollinger, W. R. Thiel, E. Von Harbou and H. Hasse, *Ind. Eng. Chem. Res.*, 2014, **53**, 17589–17596.
- 35 M. Bornemann, S. Kern, N. Jurtz, T. Thiede, M. Kraume and M. Maiwald, *Ind. Eng. Chem. Res.*, 2019, **58**, 19562–19570.
- 36 P. Giraudeau and F.-X. Felpin, *React. Chem. Eng.*, 2018, **3**, 399–413.
- 37 G. Suryan, *Proc. - Indian Acad. Sci., Sect. A*, 1951, **33**, 107–111.
- 38 J. M. Merritt, J. Y. Buser, A. N. Campbell, J. W. Fennell, N. J. Kallman, T. M. Koenig, H. Moursy, M. A. Pietz, N. Scully and U. K. Singh, *Org. Process Res. Dev.*, 2014, **18**, 246–256.
- 39 M. Tabatabaei Anaraki, R. Dutta Majumdar, N. Wagner, R. Soong, V. Kovacevic, E. J. Reiner, S. P. Bhavsar, X. Ortiz Almirall, D. Lane, M. J. Simpson, H. Heumann, S. Schmidt and A. J. Simpson, *Anal. Chem.*, 2018, **90**, 7912–7921.
- 40 C. Jacquemmoz, F. Giraud and J.-N. Dumez, *Analyst*, 2020, **145**, 478–485.
- 41 B. Wu, R. D. Majumdar, D. H. Lysak, R. Ghosh Biswas, M. Tabatabaei-Anaraki, A. Jenne, X. You, R. Soong, D. Lane, P. A. Helm, A. Codina, V. Decker, M. J. Simpson and A. J. Simpson, *Chem. Eng. Sci.*, 2021, **405**, 1–11.
- 42 A. M. R. Hall, J. C. Chouler, A. Codina, P. T. Gierth, J. P. Lowe and U. Hintermair, *Catal. Sci. Technol.*, 2016, **6**, 8406–8417.
- 43 A. Friebel, T. Specht, E. Von Harbou, K. Münnemann and H. Hasse, *J. Magn. Reson.*, 2020, **312**, 1–9.
- 44 S. Simons, *Concepts of Chemical Engineering for Chemists*, Royal Society of Chemistry, Cambridge, 2nd edn, 2016.
- 45 A. M. R. Hall, R. Broomfield-Tagg, M. Camilleri, D. R. Carbery, A. Codina, D. T. E. Whittaker, S. Coombes, J. P. Lowe and U. Hintermair, *Chem. Commun.*, 2018, **54**, 30–33.
- 46 J. Y. Buser and A. D. McFarland, *Chem. Commun.*, 2014, **50**, 4234–4237.
- 47 P. A. Keifer, in *Annual Reports on NMR Spectroscopy*, ed. G. A. Webb, Academic Press, 2007, vol. 62, pp. 1–47.
- 48 M. V. Gomez and A. D. Hoz, *Beilstein J. Org. Chem.*, 2017, **13**, 285–300.
- 49 N. Zientek, K. Meyer, S. Kern and M. Maiwald, *Chem. Ing. Tech.*, 2016, **88**, 698–709.
- 50 J. Ollig and G. Hägele, *Comput. Chem. Eng.*, 1995, **19**, 287–294.
- 51 M. V. Silva Elipse, A. Cherney, R. Krull, N. Donovan, J. Tedrow, D. Pooke and K. L. Colson, *Org. Process Res. Dev.*, 2020, **24**, 1428–1434.
- 52 E. Luchinat, L. Barbieri, T. F. Campbell and L. Banci, *Anal. Chem.*, 2020, **92**, 9997–10006.
- 53 P. V. Yushmanov and I. Furó, *J. Magn. Reson.*, 2005, **175**, 264–270.
- 54 D. B. Green, J. Lane and R. M. Wing, *Appl. Spectrosc.*, 1987, **41**, 847–850.
- 55 J. Bart, A. J. Kolkman, A. J. Oosthoek-De Vries, K. Koch, P. J. Nieuwland, H. Janssen, J. Van Bentum, K. A. M. Ampt, F. P. J. T. Rutjes, S. S. Wijmenga, H. Gardeniers and A. P. M. Kentgens, *J. Am. Chem. Soc.*, 2009, **131**, 5014–5015.
- 56 A. Brächer, S. Hoch, K. Albert, H. J. Kost, B. Werner, E. von Harbou and H. Hasse, *J. Magn. Reson.*, 2014, **242**, 155–161.
- 57 A. J. Oosthoek-De Vries, J. Bart, R. M. Tiggelaar, J. W. G. Janssen, P. J. M. Van Bentum, H. J. G. E. Gardeniers and A. P. M. Kentgens, *Anal. Chem.*, 2017, **89**, 2296–2303.
- 58 Flow NMR Probe, <https://www.bruker.com/pl/products-and-solutions/mr/nmr/probes/Flow-NMR-Probe.html>, (accessed 20/05/2021).
- 59 FLOWTHRU CapNMR Probe, [http://www.protasis.net/blog/?page\\_id=460](http://www.protasis.net/blog/?page_id=460), (accessed 20/05/2021).
- 60 MICCS (MICRO Channeled Cell for Synthesis monitoring), <https://www.jeol.co.jp/en/products/detail/MICCS.html>, (accessed 20/05/2021).
- 61 InsightMR, <https://www.bruker.com/en/products-and-solutions/mr/nmr-pharma-solutions/InsightMR.html>,



- (accessed 20/05/2021).
- 62 NMRReady-flow, <https://www.nanalysis.com/nmready-flow>, (accessed 20/05/2021).
- 63 Reaction Monitoring, <https://magritek.com/applications/reaction-monitoring/>, (accessed 20/05/2021).
- 64 F. Dalitz, M. Maiwald and G. Guthausen, *Chem. Eng. Sci.*, 2012, **75**, 318–326.
- 65 M. Kespe, E. Förster, H. Nirschl and G. Guthausen, *Appl. Magn. Reson.*, 2018, **49**, 687–705.
- 66 V. Sans, L. Porwol, V. Dragone and L. Cronin, *Chem*, 2015, **6**, 1258–1264.
- 67 A. Friebel, E. von Harbou, K. Münnemann and H. Hasse, *Chem. Eng. Sci.*, 2020, **219**, 115561.
- 68 T. Moussa and C. Tiu, *Chem. Eng. Sci.*, 1994, **49**, 1681–1692.
- 69 M. J. Harding, S. Brady, H. O. Connor, R. Lopez-rodriguez, M. D. Edwards, S. Tracy, D. Dowling, G. Gibson, P. Girard and S. Ferguson, *React. Chem. Eng.*, 2020, **5**, 728–735.
- 70 O. B. Searle and R. H. Pfeiffer, *Polym. Eng. Sci.*, 1985, **25**, 474–476.
- 71 Tubing Selection Guide, <https://www.coleparmer.com/tech-article/tubing-selection-guide>, (accessed 20/05/2021).
- 72 I. T. Horvath and J. M. Millar, *Chem. Rev.*, 1991, **91**, 1339–1351.
- 73 N. J. Beach, S. M. M. Knapp and C. R. Landis, *Rev. Sci. Instrum.*, 2015, **86**, 104101.
- 74 PEEK Tubing, <https://www.vici-jour.com/tubing/peek.php>, (accessed 20/05/2021).
- 75 L. Monson, S. I. Moon and C. W. Extrand, *J. Appl. Polym. Sci.*, 2013, **127**, 1637–1642.
- 76 Fluidic & optical products and information, <https://www.idx-hs.com/wp-content/uploads/2018/07/Fluidics-and-Optics-Catalog.pdf>, (accessed 20/05/2021).
- 77 Choosing the Right Masterflex® Tubing Formulation, <https://www.google.com/url?sa=t&rct=j&q=&esrc=s&source=web&cd=&ved=2ahUKewiMkqeolbPxAhXDR0EAHZehD1UQFjALegQIEhAD&url=https%3A%2F%2Fpim-resources.coleparmer.com%2Fselection-guide%2F4248-mflex-tubing-selection-guide.pdf&usg=AOvVaw0EKiuZFOENzKXIVrklqjm>, (accessed 20/05/2021).
- 78 Properties of PTFE and some other insulating materials, <https://www.drufon.com/ptfeprop.html>, (accessed 20/05/2021).
- 79 Polyimide (PI) Material Information, <http://www.goodfellow.com/E/Polyimide.html>, (accessed 20/05/2021).
- 80 All About 304 Steel (Properties, Strength, and Uses), <https://www.thomasnet.com/articles/metals-metal-products/all-about-304-steel-properties-strength-and-uses/>, (accessed 20/05/2021).
- 81 Stainless Steel Seamless Tubing and Tube Support Systems, <https://www.swagelok.com/downloads/webcatalogs/en/ms-01-181.pdf>, (accessed 20/05/2021).
- 82 K. A. Mohammad, E. S. Zainudin, S. Salit, N. I. Zahari and A. Ali, *Adv. Mater. Res.*, 2013, **701**, 77–81.
- 83 Stainless Steel: Tables of Technical Properties, [https://www.worldstainless.org/Files/issf/non-image-files/PDF/Euro\\_Inox/Tables\\_TechnicalProperties\\_EN.pdf](https://www.worldstainless.org/Files/issf/non-image-files/PDF/Euro_Inox/Tables_TechnicalProperties_EN.pdf), (accessed 20/05/2021).
- 84 Chemical Resistance of PEEK and Other Polymers, <https://www.vici-jour.com/support/resistance.php#:~:text=PEEK%20is%20compatible%20with%20almost,may%20cause%20swelling%20in%20PEEK>, (accessed 20/05/2021).
- 85 S. M. Alves, F. K. Dutra-pereira and T. C. Bicudo, *Fuel*, 2019, **249**, 73–79.
- 86 F. Loeker and W. Leitner, *Chem. – Eur. J.*, 2000, **6**, 2011–2015.
- 87 Chemical Compatibility Table, <https://www.hoseflex.com/wp-content/uploads/2015/06/Chemical-Compatibility-Table.pdf>, (accessed 20/05/2021).
- 88 Chemical Resistance of Plastics, <https://www.curbellplastics.com/Research-Solutions/Chemical-Resistance-of-Plastics>, (accessed 20/05/2021).
- 89 Chemical compatibility guide, <http://www.hanwel.be/wp-content/uploads/2014/04/Chemical-Compatibility-Guide-090413-Deel-1.pdf>, (accessed 20/05/2021).
- 90 S. Tripathi, S. M. Haque, K. D. Rao, R. De, T. Shripathi, U. Deshpande, V. Ganesan and N. K. Sahoo, *Appl. Surf. Sci.*, 2016, **385**, 289–298.
- 91 S. X. Lu, P. Cebe and M. Capel, *Polymer*, 1996, **37**, 2999–3009.
- 92 Periodic Table of The Analytical Fittings, [https://www.idx-hs.com/wp-content/uploads/2019/09/IDX2904\\_PeriodicTable\\_Update\\_R2-FNL-LR.pdf](https://www.idx-hs.com/wp-content/uploads/2019/09/IDX2904_PeriodicTable_Update_R2-FNL-LR.pdf), (accessed 20/05/2021).
- 93 L. Tan, B. Zhu, S. Cao and Y. Wang, *Sci. Bull.*, 2013, **58**, 949–952.
- 94 L. Friedel, *J. Loss Prev. Process Ind.*, 1988, **1**, 31–38.
- 95 C. P. Holvey, D. M. Roberge, M. Gottsponer, N. Kockmann and A. Macchi, *Chem. Eng. Process.*, 2011, **50**, 1069–1075.
- 96 M. Ghobadi and Y. S. Muzychka, *Exp. Therm. Fluid Sci.*, 2014, **57**, 57–64.
- 97 L. Brinkert, P. Paris, M. Renner, J. M. Espenan and P. Aptel, *J. Membr. Sci.*, 1994, **92**, 131–139.
- 98 F. P. Incropera and D. P. DeWitt, *Fundamentals of Heat and Mass Transfer*, Wiley, New Jersey, 5th edn, 2001.
- 99 G. O. Brown, *Environmental and Water Resources History*, ed. A. J. Fredrich and J. R. Rogers, American Society Civil Engineers, Washington, D.C., 2004, ch. 4, vol. 38, pp. 34–43.
- 100 M. B. Plutschack, K. Gilmore and P. H. Seeberger, *Chem. Rev.*, 2017, **117**, 11796–11893.
- 101 J. Britton and C. L. Raston, *Chem. Soc. Rev.*, 2017, **46**, 1250–1271.
- 102 K. C. H. Tijssen, B. J. A. van Weerdenburg, H. Zhang, J. W. G. Janssen, M. C. Feiters, P. J. M. van Bentum and A. P. M. Kentgens, *Anal. Chem.*, 2019, **91**, 12636–12643.
- 103 A. Bara-Estaún, C. L. Lyall, J. P. Lowe, P. G. Pringle, P. C. J. Kamer, R. Franke and U. Hintermair, *Faraday Discuss.*, 2021, **229**, 422–442.
- 104 I. Swan, M. Reid, P. W. A. Howe, M. A. Connell, M. Nilsson, M. A. Moore and G. A. Morris, *J. Magn. Reson.*, 2015, **252**, 120–129.
- 105 R. Wei, A. M. R. Hall, R. Behrens, M. S. Pritchard, E. J. King and G. C. Lloyd-Jones, *Eur. J. Org. Chem.*, 2021, **2021**, 2331–2342.



- 106 Ethylene Glycol Heat-Transfer Fluid, [https://www.engineeringtoolbox.com/ethylene-glycol-d\\_146.html](https://www.engineeringtoolbox.com/ethylene-glycol-d_146.html), (accessed 20/05/2021).
- 107 D. B. G. Berry, A. Codina, I. Clegg, C. L. Lyall, J. P. Lowe and U. Hintermair, *Faraday Discuss.*, 2019, **220**, 45–57.
- 108 D. S. Raiford, C. L. Fisk and E. D. Becker, *Anal. Chem.*, 1979, **51**(12), 2050–2051.
- 109 A. R. Bogdan and A. W. Dombrowski, *J. Med. Chem.*, 2019, **62**, 6422–6468.
- 110 P. S. M. E. Shashi Menon, *Working Guide to Pumps and Pumping Stations*, Elsevier, Amsterdam, 2010.
- 111 H. P. Bloch, in *Pump Wisdom: Problem Solving for Operators and Specialists*, Wiley, New Jersey, 2011, ch. 2, pp. 15–22.
- 112 M. Volk, *Pump Characteristics and Applications*, CRC Press, Boca Raton, 3rd edn, 2014.
- 113 E. W. Thorne and A. N. Neal, *Proc. Inst. Mech. Eng., Part A*, 2000, **214**, 255–268.
- 114 R. P. O'Connor, *Positive Displacement Pumps: A Guide to Performance Evaluation*, Wiley, New Jersey, 1st edn, 2007.
- 115 Pumps and systems: Gear Pumps: A Simple Solution for Metering Applications, <https://www.michael-smith-engineers.co.uk/mse/uploads/resources/useful-info/Positive-Displacement-Pumping-Guides/Gear-Pumps-for-Metering-Applications.pdf>, (accessed 20/05/2021).
- 116 M. S. Cubberley and W. A. Hess, *J. Chem. Educ.*, 2017, **94**, 72–74.
- 117 Understanding Net Positive Suction Head, <https://www.michael-smith-engineers.co.uk/mse/uploads/resources/useful-info/Positive-Displacement-Pumping-Guides/NPSHR-%26-it%27s-effect-on-Rotary-PD-Pumps.pdf>, (accessed 25/05/2021).
- 118 Liquid Dynamic Viscosity, <http://ddbonline.ddbst.com/VogelCalculation/VogelCalculationCGI.exe>, (accessed 27/05/2021).
- 119 B. González, N. Calvar, E. Gómez and Á. Domínguez, *J. Chem. Thermodyn.*, 2007, **39**, 1578–1588.
- 120 E. B. Nauman, *Ind. Eng. Chem. Res.*, 2008, **47**, 3752–3766.
- 121 O. Levenspiel, *Chemical Reaction Engineering*, Wiley, Danvers, 3rd edn, 1998.
- 122 R. Horst, K. A. Farley, B. L. Kormos and J. M. Withka, *J. Biomol. NMR*, 2020, **74**, 509–519.
- 123 H. S. Fogler, *Elements of chemical reaction engineering*, Prentice Hall, New Jersey, 3rd edn, 1999.
- 124 K. Meyer, S. Kern, N. Zientek, G. Guthausen and M. Maiwald, *Anal. Chem.*, 2016, **83**, 39–52.
- 125 G. R. D. Prabhu and P. L. Urban, *Chem. Rev.*, 2020, **120**, 9482–9553.
- 126 Instrument Driver Guidelines, [https://www.ni.com/devzone/idnet/library/instrument\\_driver\\_guidelines.htm](https://www.ni.com/devzone/idnet/library/instrument_driver_guidelines.htm).
- 127 Digital Futures - A new frontier for science exploration and discovery, <https://www.rsc.org/new-perspectives/discovery/digital-futures>, (accessed 13/07/2021).
- 128 A. D. Clayton, J. A. Manson, C. J. Taylor, T. W. Chamberlain, B. A. Taylor, G. Clemens and R. A. Bourne, *React. Chem. Eng.*, 2019, **4**, 1545–1554.
- 129 C. Czwiek and R. Anderl, *Procedia CIRP*, 2020, **90**, 584–588.
- 130 A. Kiam Heong, G. Chong and L. Yun, *IEEE Trans. Control Syst. Technol.*, 2005, **13**, 559–576.

