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# Fe(TCNQ)<sub>2</sub> nanorod arrays: an efficient electrocatalyst for electrochemical ammonia synthesis *via* the nitrate reduction reaction†

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The electrochemical reduction of nitrate to ammonia (NO<sub>3</sub>RR) catalyzed by metal organic frameworks (MOFs) is a promising and efficient method for reducing nitrate pollution in water while simultaneously producing a valuable product, ammonia. Herein, we report the 3D nanoarray architecture of the metal organic complex Fe-(tetracyanoquinodimethane)<sub>2</sub> Fe(TCNQ)<sub>2</sub> as an efficient electrocatalyst that exhibits a high ammonia yield rate of 11 351.6 μg h<sup>-1</sup> cm<sup>-2</sup> and faradaic efficiency (FE) of 85.2% at -1.1 V vs. RHE and excellent catalytic stability up to 2 days. The excellent catalytic performance is evaluated by ATR-FTIR spectroscopy and a series of control experiments. Density functional-based theoretical calculations are carried out to identify Fe-N<sub>4</sub> active sites in metal-organic network structures. This study showcases the advancement of transition metal-based organic frameworks as very effective electrocatalysts for the reduction of nitrate to ammonia (NH<sub>3</sub>).

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## Introduction

Ammonia (NH<sub>3</sub>) is a vital chemical that is extensively manufactured on a global scale for its utmost importance in the fertilizer sector as well as a feasible intermediate form of hydrogen energy storage and a carbonless energy vector. Thus, to mitigate the energy crisis NH<sub>3</sub> can exclusively serve as a carrier for the conveyance of renewable energy on a worldwide scale.<sup>1-3</sup> The industrially exemplary Haber-Bosch process, which is energy demanding and produces an extensive amount of greenhouse gases, is the primary method for the large scale industrial production of NH<sub>3</sub>.<sup>4-6</sup> A sustainable, environment-friendly, and energy efficient strategy for NH<sub>3</sub> synthesis is the desperate need of the hour. The production of NH<sub>3</sub> from N<sub>2</sub> *via* the nitrogen reduction reaction (NRR) has recently attracted an enormous amount of research interest.<sup>7-10</sup> The bottlenecks of the NRR persist due to the low N<sub>2</sub> solubility implying poor conversion efficiency and slow reaction kinetics because of the high stability of the N≡N bond (bond energy 941 kJ mol<sup>-1</sup>), as well as the competing hydrogen evolution reaction (HER) at the cathode surface. All these factors culminate into extremely low NH<sub>3</sub> yield

and faradaic efficiency (FE) and prevent the scalability process of the NRR.<sup>11-14</sup> On the other end of the spectrum, nitrate (NO<sub>3</sub><sup>-</sup>) ions stand out owing to their high solubility in water and a low dissociation energy (204 kJ mol<sup>-1</sup>) for the N=O bond,<sup>2</sup> hence promoting a reduction in the barrier for mass transfer and minimizing energy consumption during electrolysis, therefore making it an energetically more favorable process than the NRR. Nitrate (NO<sub>3</sub><sup>-</sup>) is one of the most important forms of nitrogen in the environment. It is a key water pollutant which poses a serious threat to human health, causing cancer and methemoglobinemia.<sup>15-18</sup> The electrochemical conversion of waste NO<sub>3</sub><sup>-</sup> into valuable products in the form of N<sub>2</sub>/NH<sub>3</sub> under mild reaction conditions offers a potential solution to the problem of nitrate and/or nitrite pollution.<sup>16,19-24</sup> Additionally, this process presents an environmentally friendly and sustainable alternative to the conventional Haber-Bosch method for ammonia synthesis;<sup>25-27</sup> hence, it is a hot topic in the field of electrocatalysis. The eight electron transfer process associated electrochemical NO<sub>3</sub><sup>-</sup> reduction reaction (NO<sub>3</sub>RR) to NH<sub>3</sub> is regarded as a promising means of converting NO<sub>3</sub><sup>-</sup> without causing secondary contamination.<sup>15,27-34</sup> Nevertheless, it is possible to mitigate the competitive hydrogen evolution reaction (HER) by designing a suitable electrocatalyst. Transition metal organic complexes, including cobalt phthalocyanine (CoPc),<sup>35,36</sup> copper phthalocyanine (CuPc),<sup>10,37</sup> and nickel phthalocyanine-based composites,<sup>14,38,39</sup> are regarded as promising electrocatalysts where the transition metal center is the active center of the electrochemical reduction reactions and organic ring phthalocyanine inhibits the competing HER. Fe based single atom catalysts were extensively studied by various research

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groups for the  $\text{NO}_3\text{RR}$  to ammonia under ambient conditions.<sup>27,28,40</sup> Recently, Fe based conducting metal organic frameworks such as Fe-(tetracyanoquinodimethane)<sub>2</sub> ( $\text{Fe}(\text{TCNQ})_2$ ) have been studied as oxygen evolution reaction electrocatalysts.<sup>41,42</sup> However, to the best of our knowledge,  $\text{Fe}(\text{TCNQ})_2$  nanostructures have not yet been studied as an effective electrocatalyst for the electrochemical  $\text{NO}_3\text{RR}$  to  $\text{NH}_3$ .

In this work, a  $\text{Fe}(\text{TCNQ})_2$  nanorod array has been fabricated on a copper foam (CF) substrate, which is a binder-free electrocatalyst-electrode assembly for  $\text{NO}_3\text{RR}$  studies. FESEM observations confirm the distinct 3-dimensional (3D) nanoarray architecture. Extended X-ray absorption fine structure (EXAFS) spectra identify the distinctive Fe–N<sub>4</sub> coordination environment which is the active center for the  $\text{NO}_3\text{RR}$ . Hence, the 3D  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  system delivered an ammonia yield rate 11 351.6  $\mu\text{g h}^{-1} \text{cm}^{-2}$  and FE 85.2% at  $-1.1 \text{ V vs. RHE}$  along with electrocatalytic stability of more than 2 days. Attenuated total reflection–Fourier transform infrared (ATR-FTIR) spectroscopy confirms the various intermediate species, specifically \*NO, \*NH, and \*NH<sub>2</sub> formed during  $\text{NH}_3$  formation. Furthermore, density functional based theoretical calculations demonstrated the mechanism of the eight electron transfer associated  $\text{NO}_3\text{RR}$ . Additionally, several control assays and isotopic labelling experiments confirm the source of nitrogen in the produced  $\text{NH}_3$ , as well.

## Results and discussion

The growth mechanism of the catalyst showcases (Fig. 1a) the feasibility of employing cationic exchange under low-

temperature conditions to fabricate a nanorod array of  $\text{Fe}(\text{TCNQ})_2$  on a copper foam (CF) substrate.

Prior to this, a nanorod array of  $\text{Cu}(\text{TCNQ})$  had been successfully synthesized on a copper foam substrate defined as  $\text{Cu}(\text{TCNQ})/\text{CF}$ . The transformation of  $\text{Cu}(\text{TCNQ})/\text{CF}$  into  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  involved a controlled cationic exchange process, where  $\text{Fe}^{2+}$  ions effectively exchange  $\text{Cu}^+$  ions.<sup>42</sup> This innovative  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  nanorod array configuration served as a conductive electrode in the realm of electrochemical nitrate reduction, yielding notably enhanced performance in the context of the nitrate reduction reaction. The influence of the morphology of the resultant metal-TCNQ composites was systematically examined through scanning electron microscopy (SEM) and transmission electron microscopy (TEM). The FESEM depiction of the  $\text{Cu}(\text{TCNQ})$  specimen unveils developed growth of  $\text{Cu}(\text{TCNQ})$  nanorods achieved through the surface coverage of Cu foam, as demonstrated in Fig. 1b and c. Upon investigating the  $\text{Fe}(\text{TCNQ})_2$  sample subsequent to the cationic exchange process, its distinct nanoarray architecture is observed to persist, as evident in Fig. 1d. And Fig. 1e shows a TEM image of  $\text{Fe}(\text{TCNQ})_2$  where the nanorods are  $\sim 150\text{--}160 \text{ nm}$  in width.

To gain insight into the structural properties of the catalyst, we conducted X-ray diffraction (XRD) analysis. Fig. 2a shows the XRD patterns of both  $\text{Cu}(\text{TCNQ})/\text{CF}$  and  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ . The distinct peaks in the XRD plot correspond to the X-ray diffraction patterns of  $\text{Cu}(\text{TCNQ})$  and  $\text{Fe}(\text{TCNQ})_2$ , thereby revealing important information about their crystal structures which is well matched by the previous data.<sup>42,43</sup> The X-ray photoelectron spectroscopy (XPS) spectrum of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  is depicted in Fig. S1† and shows that the catalyst is composed of the elements Fe, C, N and Cu. The oxygen (O) element may appear due to



Fig. 1 (a) Growth mechanism of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ , (b, c) FESEM images of  $\text{Cu}(\text{TCNQ})/\text{CF}$ , (d) FESEM image of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ , and (e) TEM image of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ .



Fig. 2 (a) XRD patterns of CuTCNQ/CF and Fe(TCNQ)<sub>2</sub>/CF, (b) high resolution XPS N 1s scan of Fe(TCNQ)<sub>2</sub>/CF, (c) high resolution XPS C 1s scan of Fe(TCNQ)<sub>2</sub>/CF, (d) high resolution XPS Fe 2p scan of Fe(TCNQ)<sub>2</sub>/CF, (e) XANES spectra of Fe(TCNQ)<sub>2</sub>/CF, Fe foil and Fe<sub>2</sub>O<sub>3</sub>, (f)  $k^3$ -weighted FT-EXAFS spectra ( $R$  space fitting curves) corresponding to the Fe K-edge, and (g–i) wavelet transform contour plots for Fe foil, Fe(TCNQ)<sub>2</sub>/CF and Fe<sub>2</sub>O<sub>3</sub>.

material contamination or oxidation on the product surface.<sup>42</sup> At about 398.6 eV, an XPS N 1s spectrum peak (Fig. 2b) is observed due to Fe–N=C; also a shake-up peak comes at 400.1 eV in the Fe(TCNQ)<sub>2</sub>/CF system. The peaks with binding energy at 284.58 and 285.94 eV are produced by carbon bonds (C–H) and nitrile carbon bonds (C–N) in the TCNQ system, respectively (as shown in Fig. 2c). In addition, the unsaturated carbon bond produces a satellite at 288.1 eV. The two main binding energies for Fe 2p<sub>3/2</sub> and Fe 2p<sub>1/2</sub> are shown in Fig. 2d at 712.7 and 724.1 eV, respectively.<sup>41,42,44</sup> To elucidate the distinctive Fe–N<sub>4</sub> coordination and to unravel the intricate structural attributes of the catalytically active sites within the developed Fe(TCNQ)<sub>2</sub>/CF catalyst, a comprehensive investigation employing X-ray absorption spectroscopy (XAS), encompassing both X-ray absorption near edge structure (XANES) and extended X-ray absorption fine structure (EXAFS) spectra, was carried out. Fig. 2e illustrates the XANES absorption edge of Fe in the Fe(TCNQ)<sub>2</sub>/CF catalyst, positioned intermediate to the reference standards of elemental Fe foil and Fe<sub>2</sub>O<sub>3</sub>. This positioning of the absorption edge signifies that the average valence state of Fe

within the Fe(TCNQ)<sub>2</sub>/CF catalyst falls within the range of 0 to +3. The detailed structural insight derived from Fig. 2f showcases the  $k^3$ -weighted Fourier transform (FT) of the Fe K-edge EXAFS spectra for Fe(TCNQ)<sub>2</sub>/CF, Fe foil, and Fe<sub>2</sub>O<sub>3</sub>. The distinct peak observed near 1.42 Å in the Fe(TCNQ)<sub>2</sub>/CF sample corresponds to Fe–N coordination, a significant indicator of the active sites for the NO<sub>3</sub>RR process. Contrastingly, the negligible presence of peaks at 2.19 Å and 2.55 Å, which signify Fe–Fe metal pair interaction, establishes the uniqueness of the Fe(TCNQ)<sub>2</sub>/CF catalyst.<sup>45,46</sup> This analysis collectively points towards a practical coordination number of around 4 for Fe–N<sub>4</sub> in the Fe(TCNQ)<sub>2</sub>/CF catalyst (Table S1†), strongly implicating its role as the dominant active site for the NO<sub>3</sub>RR.<sup>45,46</sup> Additionally, a wavelet transform (WT) analysis was undertaken on the  $k^3$ -weighted EXAFS signal to offer further clarity on atom backscattering, as depicted in Fig. 2g–i. In this context, the distinctive Fe foil exhibited a WT maximum at 7.3 Å<sup>-1</sup>, aligned with Fe–Fe interactions. Conversely, the reference Fe<sub>2</sub>O<sub>3</sub> displayed two prominent WT maxima at 7.4 and 3.2 Å<sup>-1</sup>, corresponding to Fe–Fe and Fe–O interactions, respectively. Also, the Fe(TCNQ)<sub>2</sub>/CF catalyst

showcased a singular WT maximum situated at  $2.9 \text{ \AA}^{-1}$ , unequivocally attributed to Fe-N<sub>4</sub> interactions, thereby corroborating its structural significance in the catalytic process.<sup>45,46</sup>

Evaluation of the catalytic efficiency of metal-TCNQ/CF electrodes regarding nitrate reduction was performed using a conventional three-electrode system (H-type cell), as detailed in the Experimental methods section. Validation of the electrocatalytic performance for NO<sub>3</sub><sup>-</sup> reduction was established by observing the amplified current density within the linear sweep voltammogram (LSV) profile following the introduction of 0.2 M NaNO<sub>3</sub> in 0.1 M Na<sub>2</sub>SO<sub>4</sub> (illustrated in Fig. 3a). Furthermore, electrochemically active surface area (ECSA), obtained *via* double-layer capacitance ( $C_{dl}$ ) assessment (Fig. 3b and S20), revealed significant insights. In particular, the Fe(TCNQ)<sub>2</sub>/CF configuration exhibited an  $C_{dl}$  and corresponding ECSA of  $11.2 \text{ mF cm}^{-2}$  and  $252 \text{ cm}^2$ , which exceeded both CuTCNQ/CF ( $4.2 \text{ mF cm}^{-2}$  and  $94.5 \text{ cm}^2$ ) and CF ( $0.43 \text{ mF cm}^{-2}$  and  $9.7 \text{ cm}^2$ ), thereby confirming its higher internal factoring intrinsic reduction rate. To comprehensively assess the catalyst's

catalytic proficiency, electrochemical impedance spectroscopy (EIS) plots were harnessed to elucidate its charge transfer (CT) kinetics. The parameters extracted from these measurements were effectively modeled using a Randles circuit, incorporating solution resistance ( $R_s$ ) and charge transfer resistance ( $R_{ct}$ ), yielding an accurate representation of the Nyquist plots' complexities (Fig. 3c). Impressively, Fe(TCNQ)<sub>2</sub>/CF exhibited notably diminished  $R_{ct}$  values in stark comparison to CF and CuTCNQ, indicative of the heightened conductivity and enhanced proton transfer facilitation intrinsic to Fe(TCNQ)<sub>2</sub>/CF, ultimately underscoring its superior nitrate reduction efficacy. For a comprehensive exploration of the ammonia production efficiency within the catalytic system, chronoamperometry (CA) experiments were performed over 1 h reduction time, as exemplified in Fig. S13.† After 1 h of testing, all electrolyte solutions were used for indophenol blue method for ammonia detection by UV-vis spectroscopy (details in the ESI†). The UV-vis spectra of the electrolyte solutions (after electrolysis) exhibited increasing peak intensities at different

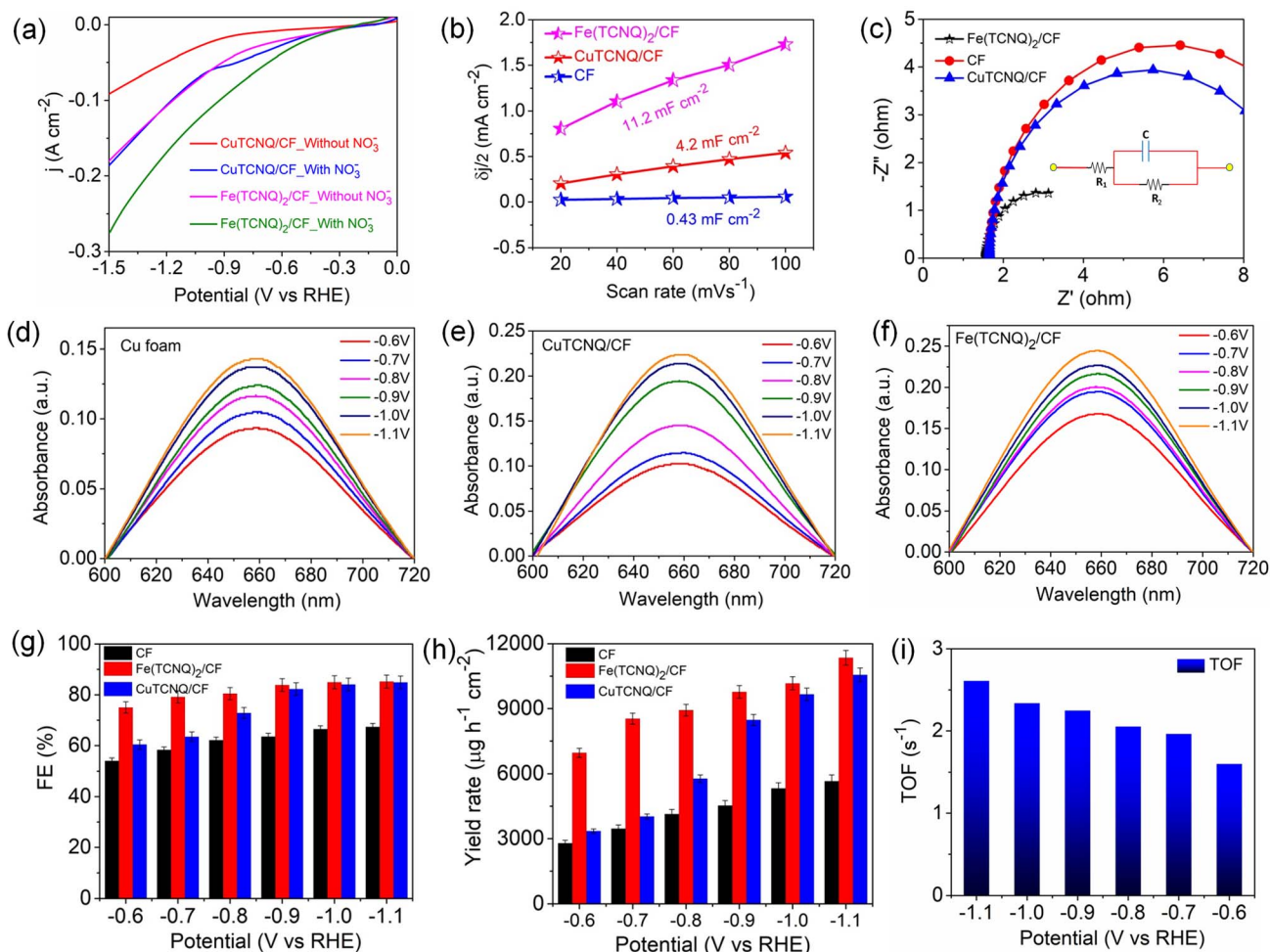


Fig. 3 (a) LSV profile of the catalyst with and without nitrate containing electrolyte, (b) electrochemical double layer capacitance analysis of the electrocatalysts, (c) EIS plot of CF and CuTCNQ/CF, Fe(TCNQ)<sub>2</sub>/CF, (d–f) UV-vis absorption spectra of ammonia solution at various potentials (after certain dilution) of CF, CuTCNQ/CF and Fe(TCNQ)<sub>2</sub>/CF respectively, (g) bar chart of the NH<sub>3</sub> yield rate at different potentials of the various electrocatalysts, (h) bar chart of FE (%) at various potentials of the various electrocatalysts, and (i) bar chart of TOF at various potentials of Fe(TCNQ)<sub>2</sub>/CF.

applied potentials (Fig. 3d–f).  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  manifested an exceptional electrocatalytic prowess in catalyzing the  $\text{NO}_3\text{RR}$ , achieving an impressive maximum faradaic efficiency (FE) of 85.2% at  $-1.1\text{ V}$  vs. RHE (Fig. 3g), accompanied by a peak ammonia yield rate of up to  $11\,351.6\ \mu\text{g h}^{-1}\text{ cm}^{-2}$  at  $-1.1\text{ V}$  vs. RHE (Fig. 3h). Similarly, both the FE and ammonia yield rate of  $\text{CuTCNQ}/\text{CF}$  ( $84.8\%$  &  $10\,562\ \mu\text{g h}^{-1}\text{ cm}^{-2}$ ) and CF ( $67.3\%$  &  $5661\ \mu\text{g h}^{-1}\text{ cm}^{-2}$ ) outperformed expectations for the  $\text{NO}_3\text{RR}$ .

These collective findings serve to underline the remarkable potential of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  as a superior electrocatalytic agent for nitrate reduction, signifying significant strides in the field of

electrochemical nitrogen fixation. To quantitatively gauge catalytic activity, the turnover frequency (TOF,  $\text{s}^{-1}$ ) was meticulously calculated based on ammonia production rates at various potentials. The distinctive histograms of TOF plotted against potential in Fig. 3i vividly depict the ammonia generation rates at Fe sites within the  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  systems. Specifically, at a potential of  $-1.1\text{ V}$ ,  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  exhibited a noteworthy peak TOF of  $2.6\ \text{s}^{-1}$ . A series of control experiments were systematically conducted to unequivocally confirm the generation of ammonia during the nitrate reduction reaction ( $\text{NO}_3\text{RR}$ ) (Fig. 4a). Initially, no signal was observed for

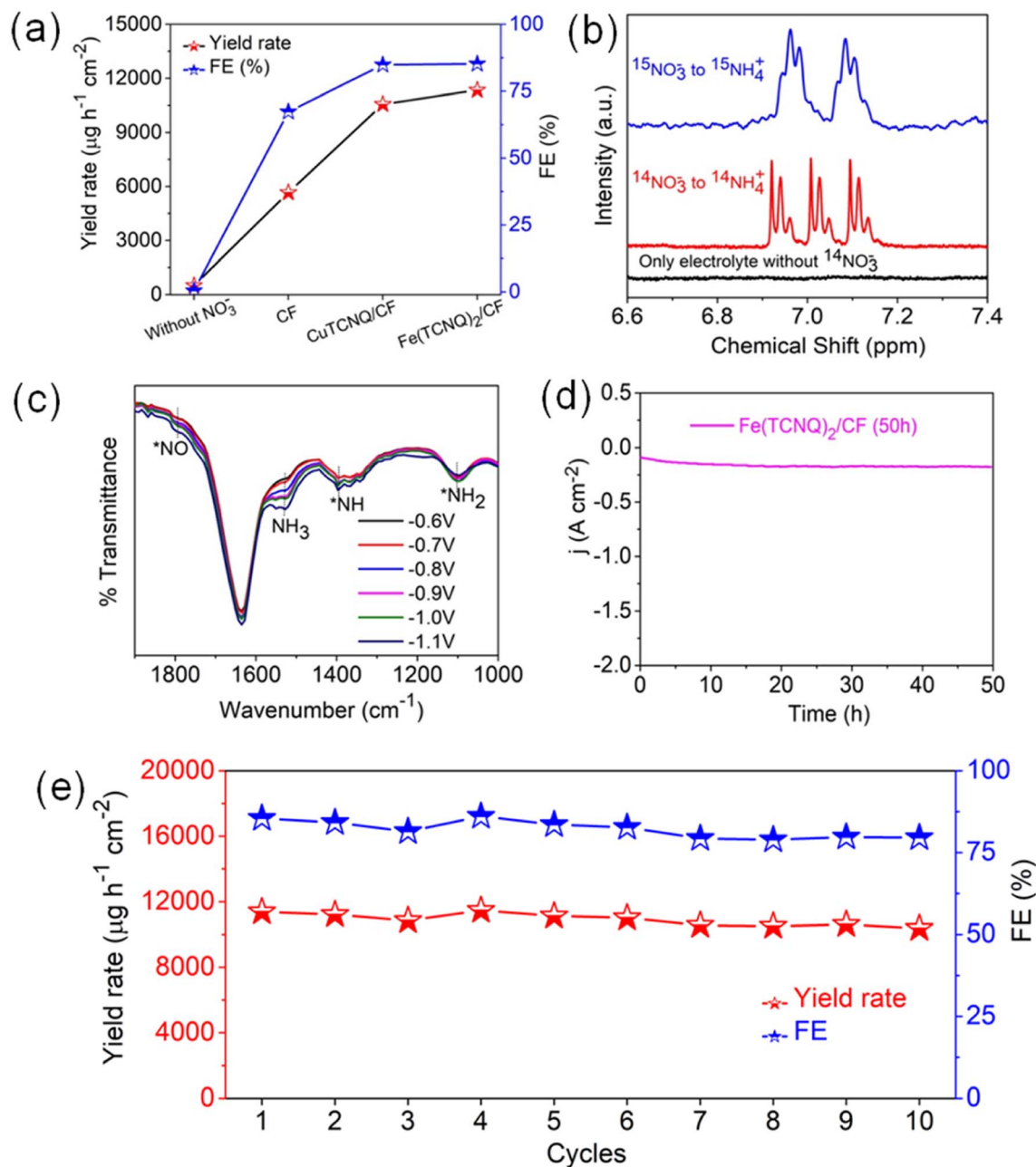


Fig. 4 (a) Control experiments without  $\text{NO}_3^-$ , CF,  $\text{CuTCNQ}/\text{CF}$ , and  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  for the  $\text{NO}_3\text{RR}$ , (b)  $^1\text{H-NMR}$  for nitrate to ammonia production conformation using  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ , (c) ATR-FTIR spectra at various potentials of electrolyte solution of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ , (d) long term stability curve of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ , and (e) recyclability test of  $\text{Fe}(\text{TCNQ})_2/\text{CF}$ .

nitrate free electrolyte solution also and a moderate signal was discerned in a solution composed of 0.2 M  $\text{NaNO}_3$  and 0.1 M  $\text{Na}_2\text{SO}_4$  in the absence of metal-TCNQ catalyst growth copper foam (CF). Subsequently, the CuTCNQ/CF system produced ammonia during the  $\text{NO}_3\text{RR}$ . In parallel, the Fe (TCNQ) $_2$ /CF system evaluation within a solution composed of 0.1 M  $\text{Na}_2\text{SO}_4$  and 0.2 M  $\text{NaNO}_3$  unambiguously established the occurrence of ammonia production during the  $\text{NO}_3\text{RR}$ . To unequivocally establish the provenance of ammonia from  $\text{NO}_3^-$  ions, we conducted  $^1\text{H}$ -nuclear magnetic resonance (NMR) analysis employing a  $^{14}\text{N}$  and  $^{15}\text{N}$ -labeled  $\text{NO}_3^-$  electrolyte solution, showcased in Fig. 4b.<sup>16</sup> The resultant  $^1\text{H}$ -NMR spectra depicted a distinctive doublet peak corresponding to  $^{15}\text{NH}_4^+$ , providing unambiguous confirmation of ammonia's genesis *via* the electrochemical reduction of nitrate ions ( $^{15}\text{N}$ -labeled), eliminating any confounding influences of extraneous factors. Equally noteworthy, in experiments using a  $^{14}\text{NO}_3^-$  containing electrolyte, a distinct triplet peak corresponding to  $^{14}\text{NH}_4^+$  further reaffirmed the specific nitrate-driven ammonia formation. Crucially, in scenarios where nitrate was absent within the electrolyte during the electroreduction process, the absence of detectable ammonia served as a definitive confirmation of the dependency on nitrate for ammonia production. Subsequent to the electrolytic process, we conducted attenuated total

reflection-Fourier transform infrared (ATR-FTIR) spectroscopy (Fig. 4c). Evident within the FTIR spectrum was a deformation vibration signal at  $1637\text{ cm}^{-1}$ , which is characteristic of  $\text{H}_2\text{O}$ . Remarkably, discernible peaks at  $1795\text{ cm}^{-1}$ ,  $1395\text{ cm}^{-1}$ , and  $1101\text{ cm}^{-1}$  were attributed to various intermediate species, specifically  $^*\text{NO}$ ,  $^*\text{NH}$ , and  $^*\text{NH}_2$ . The primary formation of  $\text{NH}_3$  was conclusively ascertained through the prominent peak at  $1530\text{ cm}^{-1}$ .<sup>47-49</sup> Intriguingly, spectral analysis revealed a direct correlation between applied potentials and ammonia intensity, substantiating the influence of potential on product yield. As relevant to catalyst evaluation, stability analysis is paramount. Obviously, a prolonged electrolysis test at  $-1.1\text{ V}$  was performed to measure the long-term stability of Fe(TCNQ) $_2$ /CF (Fig. 4d). Impressively, as depicted in Fig. 4d, a marginal decrease in current density was observed only after 50 h of continuous operation, which underscores the exceptional stability of Fe(TCNQ) $_2$ /CF under practical working conditions. Addressing reusability, an important aspect for practical application, the nitrate reduction protocol was subjected to ten consecutive cycles, each lasting one hour (illustrated in Fig. 4e). Also, the catalyst consistently maintained high faradaic efficiency (FE) and yield rates throughout these cycles, firmly establishing its recyclability for the  $\text{NO}_3\text{RR}$ . The XRD pattern (Fig. S21 $^\dagger$ ) and FESEM image (Fig. S22 $^\dagger$ ) observed for post-electrolysis

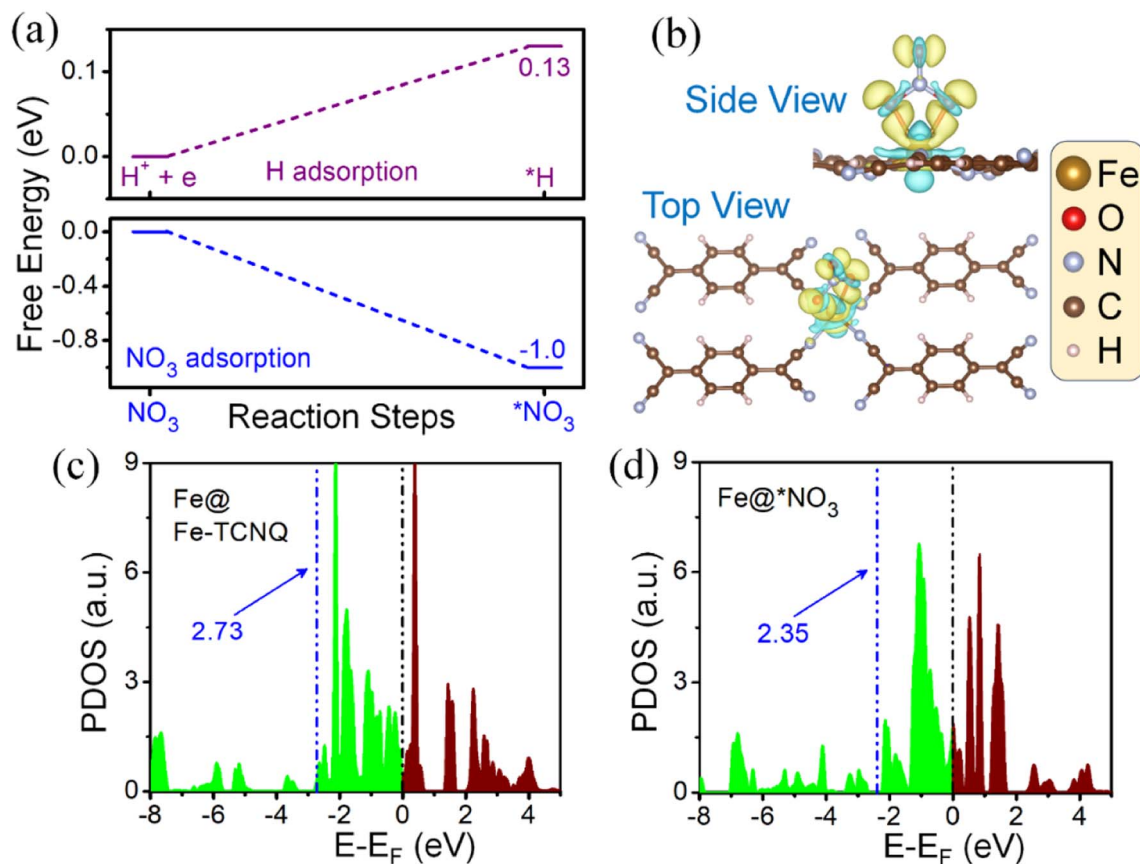


Fig. 5 (a) Difference between free energy changes of  $\text{NO}_3$  and H adsorption respectively, (b) top and side views of the charge density difference with  $\text{NO}_3$  adsorbed on the metal centre, (c) partial density of states (PDOS) of d-electrons of the Fe atom before  $\text{NO}_3$  adsorption and (d) PDOS of d-electrons of the Fe atom after  $\text{NO}_3$  adsorption.  $^*\text{NO}_3$  indicates the adsorbed case of  $\text{NO}_3$  on the metal centre.

Fe(TCNQ)<sub>2</sub>/CF specimens (as depicted in respective figures) provide further compelling evidence of the extraordinary durability of our catalyst under operational conditions. This comprehensive analysis substantiates the absence of deleterious species and further underscores the catalyst's impeccable stability.

Theoretical studies of the NO<sub>3</sub>RR, on the catalyst Fe-TCNQ, have been carried out by introducing an optimized model structure of Fe-TCNQ (Fig. S23<sup>†</sup>), where the lattice parameters of the system are 6.88 Å, 11.27 Å and 20 Å along *a*, *b* and *c* axes respectively. Along the *c*-axis, a length of 20 Å is incorporated to nullify the false interactions due to the virtual image. The

theoretical study comprises three sections; the first one is about checking for improved NO<sub>3</sub> adsorption on the metal site of the catalyst over hydrogen adsorption and in the next part we have illustrated the reaction mechanism and corresponding free energy diagram with a possible pathway for the NO<sub>3</sub>RR. In the last section, we have discussed the catalytic activity of the given catalyst.

Since the HER is taking part as a major competitor, hampering the reaction phenomena parallelly by blocking active sites, it plays a crucial role while forming NH<sub>3</sub> from NO<sub>3</sub> reduction. We have found that the adsorption process of NO<sub>3</sub>, on the Fe-TCNQ catalyst, is more exothermic in nature than the

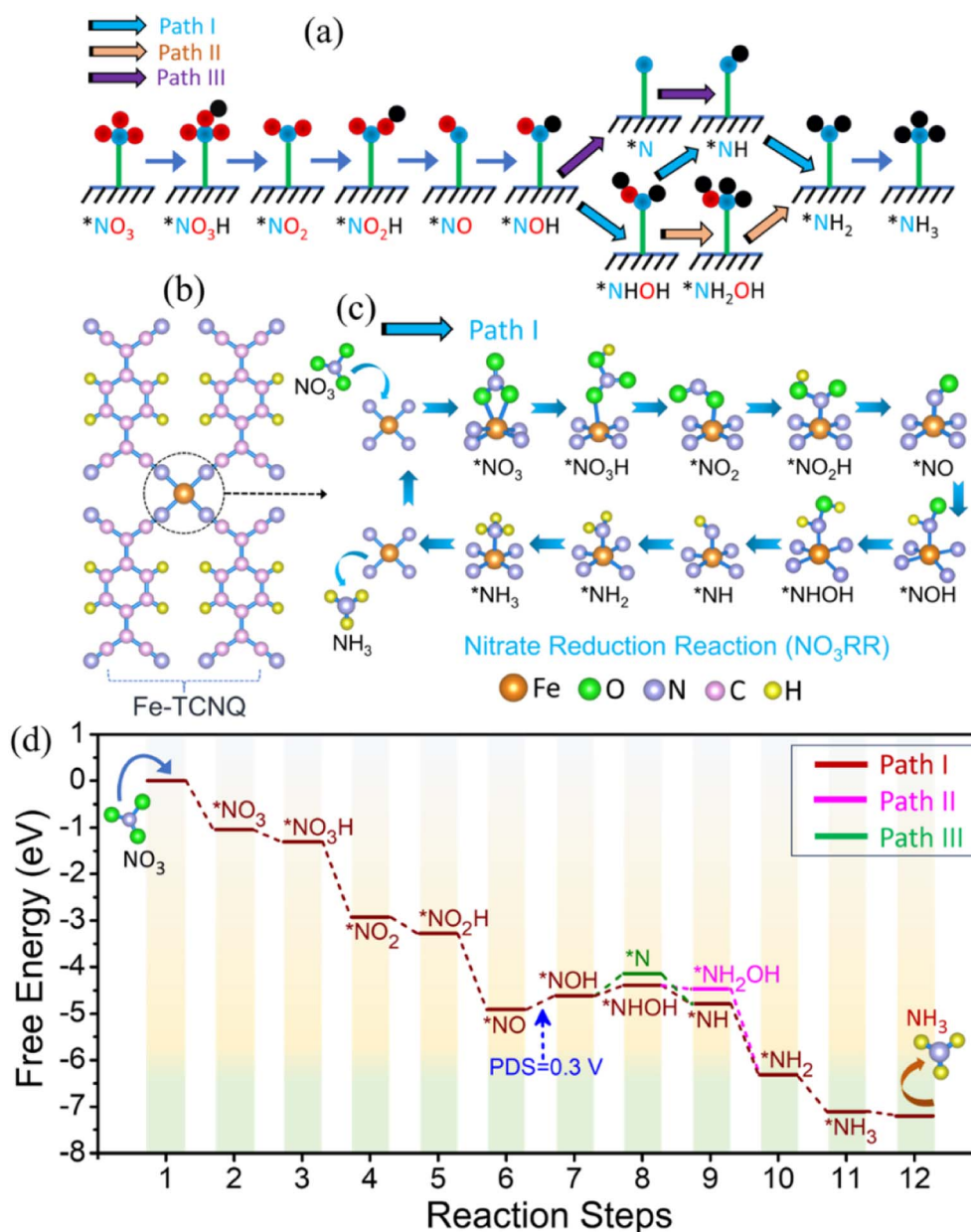


Fig. 6 (a) Three possible pathways of forming NH<sub>3</sub> from the NO<sub>3</sub> reduction reaction on the Fe-TCNQ catalyst, (b) optimized structure of the reporting catalyst (Fe-TCNQ), (c) reaction mechanism of the NO<sub>3</sub>RR through Path I with optimized structures of intermediates and (d) the full free energy profile for the NO<sub>3</sub>RR to form NH<sub>3</sub> by catalysing Fe-TCNQ along with three possible pathways.

same for hydrogen with free energy changes of  $-1.04$  eV and  $0.13$  eV respectively as shown in Fig. 5a, indicating that reaction selectivity moves towards the  $\text{NO}_3\text{RR}$ .<sup>50,51</sup> Now, when  $\text{NO}_3$  comes and sits on the active metal site, it gets reduced by taking charges from valence orbitals of the metal atom. We have verified this reduction phenomenon quantitatively and qualitatively by using Bader charge analysis and a known parameter, called the d-band centre<sup>35</sup> respectively. The charges associated with the metal atom, before and after adsorption of  $\text{NO}_3^-$ , are estimated to be  $6.82e$  and  $6.686e$  respectively. The shifting of the d-band centre from  $2.73$  eV to  $2.35$  eV, after adsorption of  $\text{NO}_3^-$  towards the Fermi level, points out that charge transfer occurred. To visualise the difference in charge density *i.e.*, loss and gain of charges by respective atoms after  $\text{NO}_3^-$  adsorption, we have presented Fig. 5b and shifting of the d-band centre is depicted in Fig. 5c and d.

To understand the reaction mechanism of the  $\text{NO}_3\text{RR}$  on the given catalyst, we have considered three known possible pathways (Fig. 6a), reported in the literature<sup>52</sup> for metal surfaces and single atom catalysts *etc.*, where protonation takes place at the 2<sup>nd</sup> step of the possible reaction pathway *i.e.*,  $\text{NO}_3^- \rightarrow *NO_3 \rightarrow \text{NO}_3\text{H}$  and all the free energy calculations of the respective intermediates are improved by adding the correction term ( $E_{\text{ZPE-TS}}$ ). In Fig. 6b–d, we have demonstrated the reaction mechanism, along the most favourable pathway *i.e.*, Path I (chosen by the lowest  $\Delta G$  of the potential determining step), and corresponding full free energy profile for the  $\text{NO}_3\text{RR}$  respectively. From the free energy diagram, it is observed that  $\text{NO}_3^-$  comes and easily gets adsorbed on the active metal site and forms the intermediate  $*NO$ , by crossing a series of exothermic steps with a free energy change of  $-1.04$  eV (step 1),  $-0.26$  eV (step 2),  $-1.62$  eV (step 3),  $-0.35$  eV (step 4) and  $-1.63$  eV (step 5) respectively. During this five step process, two  $\text{H}_2\text{O}$  molecules are liberated into the electrolyte in the following way:  $*NO_3\text{H} + 3\text{H}^+ + 3e^- \rightarrow *NO + 2\text{H}_2\text{O}$ . In the next step, protonation takes place in an endothermic way by the ( $\text{H}^+ + e^-$ ) pair and forms the intermediate  $*NOH$ , which is recognized as the potential determining step (PDS),<sup>53</sup> with a free energy change of  $0.30$  eV. After this, the ( $\text{H}^+ + e^-$ ) pair attacks serially and causes the generation of a series of intermediates that follow Path I ( $*NOH \rightarrow *NHOH \rightarrow *NH \rightarrow *NH_2 \rightarrow *NH_3$ ), where the first step is endothermic and the rest of the intermediates are formed spontaneously with a free energy change of  $0.22$  eV,  $-0.63$  eV,  $-1.53$  eV, and  $-0.79$  eV respectively. At last, desorption of  $\text{NH}_3$  also, from the surface of the catalyst, takes place spontaneously. Now, estimation of the highest energy barrier known as the PDS for two pathways, along Path I of  $*NOH \rightarrow *NHOH$  and Path III of  $*NOH \rightarrow *N$ , tells us that Path I is more favourable over Path III.

On the other side, the thermodynamic step  $*NHOH \rightarrow *NH$  is more spontaneous than the step  $*NHOH \rightarrow *NH_2\text{OH}$ ; hence there would be very little chance for Path II to occur. Therefore, based on the above discussion we can conclude that reduction of  $\text{NO}_3^-$  to  $\text{NH}_3$  on the Fe-TCNQ catalyst takes place smoothly through Path I over Path II and Path III. To find the catalytic activity of the proposed catalyst, there are so many factors to be investigated, *e.g.*, limiting potential or the PDS, HER selectivity,

change in free energy during desorption of  $\text{NH}_3$  from the catalyst surface *etc.* In this DFT study, we have obtained a lower value of limiting potential  $0.30$  V (Fig. 6d) and the given catalyst is observed to suppress the side reaction, HER phenomena that we already mentioned in the above section, resulting in higher selectivity towards the  $\text{NO}_3\text{RR}$ . Besides, the change in free energy in the case of the desorption process of  $\text{NH}_3$  from the surface of the host catalyst is negative,  $-0.09$  eV, which signifies that Fe-TCNQ is an efficient catalyst making the reduction process more feasible.

## Conclusion

In summary, a 3D nanorod array of  $\text{Fe}(\text{TCNQ})_2$  has been fabricated on a copper foam (CF) substrate using a controlled cationic exchange procedure for the electrochemical  $\text{NO}_3\text{RR}$ . The phase purity, chemical constituents, and morphology of the nanostructures were confirmed by XRD, XPS, and FESEM studies, respectively. The local Fe- $\text{N}_4$  coordination environment of the  $\text{Fe}(\text{TCNQ})_2$  electrocatalyst was studied by EXAFS analysis. The chemically synthesized 3D  $\text{Fe}(\text{TCNQ})_2/\text{CF}$  system showed electrocatalytic stability for 2 days, with a maximum ammonia yield rate of  $11\,351.6\ \mu\text{g}\ \text{h}^{-1}\ \text{cm}^{-2}$  and FE of  $85.2\%$  at  $-1.1$  V vs. RHE. Different intermediate species, including  $*NO$ ,  $*NH$ , and  $*NH_2$ , were confirmed by attenuated total reflection Fourier transform infrared (ATR-FTIR) spectroscopy. Density-functional-based theoretical computations confirmed active sites responsible for the  $\text{NO}_3\text{RR}$  and possible reaction mechanisms too. Multiple tests confirming the source of nitrogen in the produced  $\text{NH}_3$  include control experiments and isotopic labeling experiments. This finding opens up new avenues to explore other transition metal-TCNQ-based electrocatalysts for the electrochemical  $\text{NO}_3\text{RR}$  and NRR to  $\text{NH}_3$  synthesis.

## Experimental section

### Materials

7,7,8,8-Tetracyanoquinodimethane (TCNQ) (Merck), copper foam (Merck),  $\text{FeSO}_4$  (Merck), acetonitrile (Merck), methanol (Merck), and ethanol (Merck), HCl (Merck) were used. A Millipore system was utilised to purify the water used in each experiment.

### Preparation of CuTCNQ/CF

A meticulously pre-treated piece of copper foam that had its surface oxide and impurities removed using 1N HCl, ethanol, and deionized water multiple times was wetted in 6 mL of acetonitrile containing 8.58 mg of TCNQ for 2.5 hours at  $60\ ^\circ\text{C}$ . The colour of the solution changed to green, signifying the production of CuTCNQ. Before using, the sample was dried and washed multiple times with deionized water.

### Preparation of $\text{Fe}(\text{TCNQ})_2/\text{CF}$

By means of cationic exchange,  $\text{Fe}(\text{TCNQ})_2$  nanorods on copper foam were synthesised. For four hours at  $60\ ^\circ\text{C}$ , the precursors were submerged in 20 mL of methanol that contained 20 mg of



FeSO<sub>4</sub>. Deionized water was used to rinse the sample multiple times before it was dried.

### Materials characterization and electrochemical set-up

A Bruker D8 Advance Eco X-ray powder diffractometer apparatus with Cu-K<sub>α</sub> radiation was used to perform the X-ray diffraction (XRD) investigation. A Shimadzu UV-3600 plus UV-vis spectrophotometer was used to acquire absorbance data. Shimadzu's IRAffinity-1S was used to get FTIR data. The surface morphology of the synthesized electrocatalysts was monitored using an FESEM (Zeiss-Germany) and transmission electron microscope (JEOL-JEM 2100F). All measurements involving the electrocatalytic reduction of nitrate to synthesise ammonia were performed using a CHI 760E electrochemical instrument, which featured a three-electrode system with Fe(TCNQ)<sub>2</sub>/CF acting as the working electrode, platinum (Pt) foil acting as the counter electrode, and Ag/AgCl (in 3.5 M KCl) acting as the reference electrode.

### Author contributions

UKG conceived the idea and designed the experiments. NM synthesized the catalyst and performed XRD, FTIR, and UV-vis. NM and AA carried out all the electrochemical measurements and analyzed the results. NB and RT performed the theoretical (DFT) calculations. RT, NB, UKG and NM analyzed the DFT results. NM and AA analyzed the NMR result. NM, RU, BG and AA analyzed the XANES and EXAFS. AA and NM analyzed the XPS results. NM and UKG wrote the original manuscript. All authors contributed to writing the final version of the manuscript. UKG supervised the project.

### Conflicts of interest

There are no conflicts of interest to declare.

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